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BURNING OF SOLID ALUMINUM AND MAGNESIUM SPHERES IN HIGH-TEMPERATURE AND HIGH-VELOCITY GASES

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 16. Abstract The burning of solid a temperature and high oxygen, was investig: (6600 to 25 400 cm/s; 18.4 atm or 1.37×10⁵ 355 msec. The time approximately one-ha lated with calculated solid. 	aluminum and magne -velocity gases, pro ated experimentally. ec), temperatures (1 5 to 1.86×10 ⁵ N/m ²) required to heat the lif as long as the tota values using a mode	esium spheres (0.6 oduced by the comb A range of combu- .545 ⁰ to 3198 ⁰ C), gave total burning surface of the sph al burning time. E l based on a heat b	3-cm diam) in high- ustion of hydrogen and ustion gas-stream velocities and pressures (13.6 to times ranging from 125 to ere to the melting point was surning times were corre- alance at the surface of the
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BURNING OF SOLID ALUMINUM AND MAGNESIUM SPHERES IN HIGH-TEMPERATURE AND HIGH-VELOCITY GASES

by Robert D. Ingebo

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SUMMARY

Burning of solid aluminum and magnesium spheres in high-temperature and highvelocity gases, produced by the combustion of hydrogen and oxygen, was investigated experimentally. Metal spheres were 0.63 centimeter in diameter, and the flow environment was varied to produce a Reynolds number of the sphere that varied from approximately 6000 to 31 000. Burning or erosion started at the front surface of the metal sphere. The entire burning process was divided into two phases; the initial phase, during which the sphere was heated to the melting temperature of the metal with no erosion, was called a heating period. The heating period was followed by erosion with combustion stabilized in the wake of the sphere.

The experimental heating and erosion times were correlated with Nusselt numbers by an equation derived from a model using a heat balance at the surface of the solid. The heat balance equation was based on the Reynolds and Nusselt numbers of the initial sphere because it was observed that the erosion rate was constant as the mass of the metal or effective diameter decreased.

INTRODUCTION

Rapid and efficient burning of high-energy fuels such as aluminum and magnesium is difficult to achieve. This is primarily due to combustion-inhibiting processes inherent in metal-fuel combustion. However, metal fuels still appear promising as a source of power. They have been used primarily as additives in solid-fueled rocket engines to improve the specific impulse and stability. Considerable effort has been made to determine the combustion mechanism for metals in quiescent oxidizing gases (refs. 1 to 3). Also, data have been obtained on the combustion of slurry fuels in jet engines (ref. 4). However, very little data is available on metal burning rates under actual combustor conditions and the influence of metals on combustion stability. The development of metal-fueled combustors requires new techniques of injecting, rapidly igniting, and burning metal particles to efficiently control the burning process.

In this investigation of metal fuels, the main purpose was to determine mass and temperature histories of relatively large (0.63-cm diam) aluminum and magnesium spheres burning under simulated rocket combustor conditions. Such data are needed to derive a combustion model that could describe the actual burning process for metal fuels in a rocket engine and possibly explain the influence of metal additives in controlling combustion instability.

SYMBOLS

c _p	specific heat, $g-cal/(g)(^{O}C)$; $J/(g)(^{O}C)$
D _t	nozzle throat diameter, cm
d	sphere diameter, cm
dm/dt	erosion rate, g/sec
Н _f	latent heat of fusion, g-cal/g; J/g
h	heat-transfer coefficient, $g-cal/(sec)(cm^2)(^{o}C)$; $J/(sec)(cm^2)(^{o}C)$
k	thermal conductivity, g-cal/(sec)(cm ²)($^{\circ}C/cm$); J/(sec)(cm ²)($^{\circ}C/cm$)
m	sphere weight, g
Nu	Nusselt number, hd/kg
o/f	mass mixture ratio of oxidant to fuel
Р	pressure, psia; N/m^2 abs
Pr	Prandtl number, $\mu_{g} c_{p,g} / k_{g}$
q	heat-transfer rate, g-cal/sec; J/sec
Re	Reynolds number based on sphere diameter, ${\rm dV_g} ho_{\rm g} / \mu_{\rm g}$
r	sphere radius, cm
Т	temperature, ^o C
t	time, sec

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v	velocity, cm/sec
<i>α</i> 1	absorptivity
^α 2	emissivity
μ	fluid viscosity, P; (N)(sec)/m 2
ρ	fluid density, g/cm 3
σ	Stefan-Boltzmann constant

Subscripts:

\mathbf{avg}	average for sphere lifetime
С	sphere center
с	convection
е	erosion
fs	front surface
g	gas
i	initial
m	metal
mp	melting point
r	radiation
s	surface
t	total
Superscri	pts:

 average

' approximate

APPARATUS AND PROCEDURE

A rocket combustor, shown in figure 1, was used to determine burning histories of solid 0.63-centimeter-diameter aluminum and magnesium spheres inserted into high-velocity and high-temperature gases. The gas stream was produced by burning gaseous hydrogen and liquid oxygen injected 46 centimeters upstream of the spheres at mass mix-ture ratios of oxidant to fuel o/f of 1.7, 5.3, 8, 10, and 12. Three different exhaust



Figure 1. - Diagram of rocket combustor and auxiliary equipment.

nozzles were used having throat diameters of 2.46, 2.01, and 1.49 centimeters, which gave a combustion gas-stream velocity range of 6600 to 25 400 centimeters per second. These operating conditions resulted in a Reynolds number for the metal sphere ranging between 6000 and 31 000. At a given o/f condition, the chamber pressure was approximately the same (within ± 5 percent) for the three exhaust nozzle test conditions. Chamber pressures varied between 13.6 and 18.4 atmospheres (1.37×10⁵ and 1.86×10⁵ N/m²) with different mixture ratios.

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Spheres of aluminum (type 6061, 98 percent pure) and magnesium (type AZ31B, 97 percent pure) were machined from 1/4-inch (0.635-cm) rods. A hole was drilled and tapped to the center of the sphere for mounting on a 1/16-inch (0.159-cm) threaded stainless-steel rod. The spheres were mounted on the ceramic-coated tip of the probe, as shown in figure 1, and rapidly inserted into the center of the test section after equilibrium conditions had been obtained in the combustor. The tests were terminated by rapidly withdrawing the sphere back into the sheltered region cooled by nitrogen gas flow. The time measurement for each test began when the sphere passed out through the opening in the combustor wall and ended when it passed back through the same opening. The time required for the actuator to move the sphere 5.1 centimeters was 2 milliseconds for either insertion or withdrawal.

An iron-constant thermocouple (0.0127-cm-diam wire) was mounted in the center of the sphere to determine its temperature history at that point (r = 0). In obtaining mass histories, the quantity of metal eroded from the sphere was determined by weighing the sphere before and after each burning test. Attempts to determine the weight loss of a sphere by photographing it as it burned inside of the combustor proved unsuccessful since erosion was very nonuniform over its surface.

RESULTS AND DISCUSSION

A typical set of data showing mass and temperature histories of an aluminum sphere is plotted in figure 2(a). Actually, seven spheres weighing 0.350 ± 0.003 gram were tested under identical conditions to obtain the complete history of a single sphere. One of the spheres was instrumented with a thermocouple junction installed in the center of the sphere to obtain the temperature history T_C as a function of time t. In the case of aluminum (fig. 2(a)), the temperature at the center rose from the initial temperature of 20° C to the melting point (660° C) in approximately 250 milliseconds and then remained constant. In the case of magnesium (fig. 2(b)), the temperature at the center of the sphere rose to a constant value considerably below the melting point of magnesium in approximately 150 milliseconds.

Figure 2(a) also shows the mass history of an aluminum sphere. At approximately 170 milliseconds after the sphere was inserted into the gas stream, it was observed, both photographically during the run and visually by inspecting the withdrawn sphere, that erosion was just beginning to occur at the front surface. Erosion at this surface is believed to be due to the fact that the heat-transfer coefficient was considerably greater at the front surface than at the rear surface of the sphere. This is shown by the plots of calculated values of the front surface temperature $T_{\rm fs}$ against time t and the average surface temperature $\overline{T}_{\rm s}$ against time t in figure 2(a). Thus, in 170 milliseconds, the

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(b) Magnesium,

Figure 2, - Weight and temperature histories of 0, 63-centimeter-diameter aluminum and magnesium spheres. Mass mixture ratio of oxidant to fuel, 1, 7; nozzle throat diameter, 2, 01 centimeters.

front surface temperature reached the melting point (660^{\circ} C), whereas the calculated average surface temperature was 30^{\circ} below the melting point.

Spheres withdrawn at 205, 255, and 305 milliseconds are shown in figure 2(a). These photographs indicate that erosion was considerably greater at the front than at the rear of the sphere because of the higher heat-transfer coefficient at the leading surface. As a result, the metal spheres did not remain spherical during the erosion period. The mass history of the sphere showed that shortly after erosion began (called ignition) its weight decreased linearly with time.

Heating of Metal Spheres

Data on the sphere heating rate and the time required for it to reach the melting point at the front surface were analyzed in the following manner.

<u>Heating rates</u>. - The heating rate was calculated by writing a heat balance at the surface of the metal sphere as

$$q_{m} = q_{g,c} = \pi r^{2} k_{m} \frac{dT}{dr} \bigg|_{r=r_{s}}$$
(1)

where q_m is the heating rate of the sphere and $q_{g,c}$ is the rate of heat transfer by convection from the gas stream. Heat transferred by radiation was negligible (approx 2 percent of $q_{g,c}$). As discussed in appendix A, the change in sphere temperature with time was obtained from equation (1) by simultaneously solving equations (A1) and (A3) at the desired radii (r = 0 and r = r_s).

Values of the heat-transfer coefficient were assumed to calculate several temperature histories of the sphere. The best results shown in figure 2 were obtained with a heat-transfer coefficient h of 0.202 gram-calorie per second per square centimeter per ^OC (0.847 J/(sec)(cm²)(^OC)). Both figures show that agreement was good between calculated and experimental values of the temperature at the center of the sphere T_c . Also shown in figure 2 are values of \overline{T}_s , the average surface temperature of the sphere.

Values of the average heat-transfer coefficient \bar{h} are given in table I for a range of o/f conditions and corresponding values of the average Nusselt number, the Prandtl number, and the Reynolds number. The aluminum and magnesium spheres were tested at five different o/f conditions. Combustion gas properties used in these calculations are discussed in appendix B. Gas velocities used for these tests are given in table II for a nozzle throat diameter D_{t} of 2.01 centimeter.

			[Nozzle throat	diameter, 2.01 cr	n.]
[Mass	Temper-	Average heat-transfe	er coefficient, \overline{h}	Average
	mixture	ature of	2,40,00	$\frac{2}{2}$	Nusselt
	ratio of	gas,	g-cal/(sec)(cm)(C)	J/(sec)(cm)(C)	number,
	oxidant	T _g ,			Nu
	to fuel,				
1	o/f	-C			

TABLE I. - CALCULATED VALUES FOR HEAT-TRANSFER RATES

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Mass mixture ratio of oxidant to fuel, o/f	Temper- ature of gas, T _g , ^o C	Average heat-transfo g-cal/(sec)(cm ²)(⁰ C)	er coefficient, \overline{h} J/(sec)(cm ²)(^o C)	Average Nusselt number, Nu	Prandtl number, Pr	Reynolds number, Re
1.7	1545	0.2020	0.848	132.5	0,526	21 000
5.3	2977	.1295	.543	93.0	,595	12 130
8	3198	.0967	.406	94.0	,758	10 850
10	3144	.0904	.379	98.5	,744	10 400
12	3054	.0812	.341	94.5	,734	10 380

Nozzle	Mass	Velocity	Reynolds	Average	ļ	Mag	nesium			Alur	ninum	
throat diameter, D _t , cm	mixture ratio of oxidant to fuel, o/f	of gas, V _g , cm/sec	Re	Nusselt number, Nu	Heating time, t _s , msec	Average surface temper- ature, \overline{T}_{S} , ^{O}C	Averag r; (dm/ g/ Experi- mental	e erosion ate, (dt) _{avg} , (sec Calcu- lated	Heating time, t _s , msec	Average surface temper- ature, \overline{T}_{s} , °C	Averag r; (dm/ g/ Experi- mental	e erosion ate, dt) _{avg} , /sec Calcu- lated
			1	ļ	r			(eq. (10))		ļ		(eq. (10))
2.01	1.7 5.3 8 10 12 1.7 5.3 8 10	9 270 8 150 7 530 6 830 6 580 16 900 14 850 13 730 12 450	$ \begin{array}{r} 11 500 \\ 6 650 \\ 5 950 \\ 5 700 \\ 5 680 \\ 21 000 \\ 12 130 \\ 10 850 \\ 10 400 \\ \end{array} $	90.5 67.7 67.3 65.5 65.3 132.5 93.0 94.0 98.5	175 115 140 160 170 110 80 90 95	555 540 524 497 479 525 526 493 476	1.48 2.50 1.84 1.54 1.32 1.84 2.80 2.15 2.00	1.42 2.64 1.78 1.44 1.26 2.02 3.05 2.34 2.06	 170 120 150 160	 630 620 610 603	 2.07 3.27 2.89 2.71	 2.29 3.63 2.91 2.61
	12	12 000	10 380	98.3	100	450	1.77	1.78	175	595	2.43	2.31
2.46	1.7 5.3 8 10 12	25 400 22 300 20 600 18 700 18 000	31 600 18 200 16 300 15 600 15 570	169.5 123.5 125.0 118.5 118.5	90 60 70 75 80	520 497 481 447 431	2.23 3.54 3.08 2.38 2.30	2.56 3.83 3.03 2.65 2.08	135 95 115 125 135	625 614 600 592 585	3.12 4.38 3.76 3.36 3.07	2.94 4.85 3.88 3.15 2.70

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TABLE II. - EXPERIMENTAL RESULTS

The heat-transfer coefficients were correlated with the dimensionless groups as follows: McAdams (ref. 5) relates the heat-transfer coefficient for solid spheres at large Reynolds numbers with the Nusselt number and Reynolds number as

$$\frac{\overline{hd}}{k_g} = \overline{Nu} = 0.37 \text{ Re}^{0.6}$$
(2)

However, the theoretical minimum value for the Nusselt number is 2 (when Re = 0). Heat-transfer relations have also generally shown that $\text{Nu} \sim \text{Pr}^{0.3}$. Therefore, the preceding expression was modified to

$$\overline{Nu} = 2 + CPr^{0.3}Re^{0.6}$$
(3)

where C is a proportionality constant. To evaluate C, data in table I were plotted as shown in figure 3, and the following expression was obtained for solid spheres:

$$\overline{Nu} = 2 + 0.4 Pr^{0.3}Re^{0.6}$$
(4)

Properties used in equations (2) to (4) are evaluated at the mean temperature of the combustion gases and surface and for static pressures.



Figure 3. - Correlation of Nusselt number with Prandtl and Reynolds numbers.



Figure 4, - Erosion histories,

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<u>Heating times</u>. - From high-speed motion pictures of the spheres, it was observed that melting first occurred at the front surface. Thus, the heating time t_s was determined photographically from the time of insertion of the sphere into the gas stream to the time that melting was first observed at the front surface. Experimental values of the heating time t_s are recorded in table II and plotted as the solid symbols in figure 4 at the breakpoint in the mass history of the sphere.



In order to calculate the heating time t_s from the heating rate (eq. (1) or (A1) and (A3)), it is necessary to know the average surface temperature \overline{T}_s at the time t_s (when $T_{fs} = T_{mp}$). The average surface temperature when melting first occurred varied with flow conditions. Therefore, it was assumed that the nondimensional temperature ratio \overline{T}_s/T_{mp} was a function of the average Nusselt number. Also, \overline{T}_s was considerably lower

for magnesium than it was for aluminum, at the same value of \overline{Nu} . Consequently, it was also assumed that \overline{T}_s/T_{mp} was a function of the ratio of gas to liquid-metal density ρ_g/ρ_m . The following expression was therefore assumed for calculating \overline{T}_s at the time t_s :

$$\frac{\mathrm{T}_{\mathrm{mp}}}{\overline{\mathrm{T}}_{\mathrm{s}}} = 1 + \mathrm{C}(\overline{\mathrm{Nu}})^{\mathrm{m}} \left(\frac{\rho_{\mathrm{g}}}{\rho_{\mathrm{m}}}\right)^{\mathrm{n}}$$
(5)

This is an empirical correlation that might not be valid for other metals.

The exponent m was evaluated by plotting $(T_{mp}/\overline{T}_s) - 1$ against \overline{Nu} (as shown in fig. 5), and m was found to be 0.7. Similarly, a plot of $(T_{mp}/\overline{T}_s^{-1})\overline{Nu}^{-0.7}$ against ρ_g/ρ_m



(shown in fig. 6), gave an n of 3. Finally, T_{mp}/\overline{T}_s was plotted against $Nu^{0.7}(\rho_g/\rho_m)^3$ (fig. 7), and the proportionality constant C was determined to be 1.1×10^8 . Thus, equation (5) was rewritten as







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$$\frac{\mathrm{T}_{\mathrm{mp}}}{\mathrm{T}_{\mathrm{s}}} = 1 + 1.1 \times 10^8 \,\mathrm{Nu}^{0.7} \left(\frac{\rho_{\mathrm{g}}}{\rho_{\mathrm{m}}}\right)^3 \tag{6}$$

which gives the average surface temperature \overline{T}_s when the leading edge reaches the melting temperature, defined as the end of the heating time t_s . This is the time at which heating ends and erosion begins.

Although machine calculations using equations (1) and (6) were used to determine t_s at \overline{T}_s , a simpler method was derived from the following heat balance at the surface of the sphere:

$$\pi d_{i}k_{g}(T_{g} - \overline{T}_{s})\overline{Nu}_{i} = mc_{p,s}\left(\frac{T_{m}}{\overline{T}_{s}}\right)\frac{d\overline{T}_{s}}{dt}$$
(7)

which may be integrated to give

$$t'_{s} = \frac{mc_{p,s}T_{m}}{\pi d_{i}k_{g}\overline{Nu}_{i}\overline{T}_{s}} \ln \frac{T_{g} - T_{i}}{T_{g} - \overline{T}_{s}}$$
(8)

TABLE III. - COMPARISON BETWEEN CALCULATED AND EXPERIMENTAL

RESULTS FOR MAGNESIUM AND ALUMINUM SPHERES

Metal	Mass	Heating u	ime, msec	Erosion tim	1e, t _e , msec	. Total time, t _t , msec	
	mixture ratio, o/f	Approximate, t's	Experimental, (t _s) exp	Equation (11)	Experimental	Calculated	Experimental
Magnesium	1.7	111	110	114	125	225	235
	5.3	80	80	76	83	156	163
	8	92	90	99	108	191	198
	10	95	95	112	115	207	210
	12	98	100	130	130	228	230
Aluminum	1.7	174	180	153	174	327	354
	5.3	125	120	97	120	222	240
	8	150	150	120	138	270	288
	10	161	160	134	150	295	310
í í	12	171	175	151	169	322	344

[Nozzle throat diameter, 2.01 cm.]

where t'_s is the approximate heating time and T_i is the initial sphere temperature. The agreement between values of t'_s , calculated from equation (8), and experimental values of t_s was good, as shown in table III. Thus, t'_s is the approximate heating time required for the average surface temperature to reach \overline{T}_s and erosion to begin.

Erosion of Metal Spheres

Motion pictures and eroded spheres indicated that molten metal was stripped from the surface of the sphere by the high-velocity gas stream and that the atomized liquid was vaporized and ignited, and combustion was stabilized in the wake of the sphere. A model for this erosion process is shown in figure 8.



Figure 8. - Combustion model for eroding metal spheres.

In this portion of the study, the main objective was to determine erosion (mass removal) rates at the surface of the sphere and to compare them with calculated values. Calculations were made based on a heat balance and mass balance at the surface of the sphere. The use of a mass balance proved unsuccessful since the mass removal or erosion rate was not limited by the diffusion rate of oxidant gases to the surface of the sphere. Thus, a heat balance at the surface of the sphere was used to analyze the erosion data.

Erosion rates. - Applying a heat balance at the surface to the erosion of a metal sphere in high-temperature and high-velocity gas streams gives

$$q_{L} = q_{g}$$
(9)

where q_L is the rate at which heat is gained by the eroding liquid and q_g is the rate of heat transfer from the gas stream. In deriving this expression, the heating rate of the

metal was assumed to be negligible since it decreased rapidly when erosion began, and heat transfer from the flame was assumed negligible. Figure 4 shows that the average erosion rate $(dm/dt)_{avg}$ remained approximately constant with time. This result was attributed to the fact that as the metal eroded it did not remain spherical in shape. Thus, Nu could not be accurately determined during erosion. In fact, the curvature of the front surface became less convex, which tended to increase the front surface Nusselt number although the sphere diameter decreased with time. Therefore, the initial Nusselt number before erosion started was used to define the heat transfer to the surface during erosion. Because of the nonuniformity of the surface temperature of the sphere, the average value of the surface temperature \overline{T}_s was used to evaluate the sensible heat gained by the metal as it was melted and eroded by the gas stream. Thus, \overline{T}_s was also used to evaluate the surface of the surface at the surface of the surface at the surface of the sphere was written as

$$\left(\frac{\mathrm{dm}}{\mathrm{dt}}\right)_{\mathrm{avg}} \left[H_{\mathrm{f}} + c_{\mathrm{p,m}}(T_{\mathrm{mp}} - \overline{T}_{\mathrm{s}})\right] = \pi d_{\mathrm{i}}k_{\mathrm{g}}(T_{\mathrm{g}} - \overline{T}_{\mathrm{s}})\overline{\mathrm{Nu}}_{\mathrm{i}}$$
(10)

where $(dm/dt)_{avg}$ is the average erosion rate, H_f is the heat of fusion of the metal, and d_i and \overline{Nu}_i are the diameter and average Nusselt number, respectively, based on the initial sphere diameter. Values of $(dm/dt)_{avg}$ were calculated from equation (10) and plotted as shown in figure 4.

Erosion times. - The erosion time t_{ρ} may be obtained by integrating equation (10):

$$t_{e} = \frac{\rho_{i} d_{i}^{2} \left[H_{f} + c_{p,m} (T_{mp} - \overline{T}_{s})\right]}{6k_{g} (T_{s} - \overline{T}_{s})\overline{Nu}_{i}}$$
(11)

Values of t_e calculated from this equation agree reasonably well with experimental values of t_e , as shown in table III.

<u>Total heating and erosion time</u>. - The total time required for heating and erosion of metal spheres can be calculated from

$$\mathbf{t}_{t} = \mathbf{t}_{s}' + \mathbf{t}_{e} \tag{12}$$

By substituting equations (8) and (11) into equation (12), the following expression was obtained:

$$t_{t} = \frac{\rho_{L} d_{i}^{2} c_{p,m}}{6k_{g} \overline{Nu}_{i}} \left[\frac{\overline{T}_{mp}}{\overline{T}_{s}} \ln \left(\frac{\overline{T}_{g} - \overline{T}_{i}}{\overline{T}_{g} - \overline{T}_{s}} \right) + \frac{H_{f} + c_{p,m} (\overline{T}_{mp} - \overline{T}_{s})}{c_{p,m} (\overline{T}_{g} - \overline{T}_{s})} \right]$$
(13)

A comparison of values of t_t calculated from equation (13) and experimental values is shown in figure 4 and table III. Although no direct comparison could be made with the data given by Maĉek in reference 6, it could be assumed that $\overline{Nu} \simeq 2$ for the 0.0032 centimeter diameter aluminum sphere. This gives $t_t = 1.26$ milliseconds, which agrees fairly well with his data.

Burning Process with Eroding Metal Spheres

High-speed motion pictures of the spheres showed that soon after erosion was initiated the molten metal ignited and combustion was stabilized in the downstream wake of the sphere. A combustion model illustrating this burning with solid spheres is shown in figure 8. As this burning model indicates, there was no evidence of solid-phase combustion at the surface of the sphere, and no oxide shell was formed that would inhibit erosion or burning. The eroded molten metal appeared to be vaporizing and combustion was stabilized in the wake of the sphere with no appreciable amount of heat being transferred from the flame to the surface of the sphere. The luminosity of the flame was greatly increased when the erosion rate was increased and also when the o/f was increased.

SUMMARY OF RESULTS

The burning of solid aluminum and magnesium spheres (0.63-cm diam) in hightemperature and high-velocity gases, produced by the combustion of hydrogen and oxygen, has shown the following:

1. The front surface of a metal sphere was heated to its melting point before it began to erode and burn. There was no evidence of solid-phase burning at the surface of the sphere, and therefore no oxide shell was formed to inhibit the erosion process. Metal combustion was stabilized in the wake of the sphere and did not appreciably affect the erosion rate by transferring heat to the surface of the sphere.

2. Experimental heating and erosion times agreed well with values calculated from a heat balance at the surface of the sphere. The heating time for a metal sphere was approximately one-half as long as the total time required for complete erosion of the sphere.

3. The total burning time t_t (heating time plus erosion time) was correlated with the average Nusselt number \overline{Nu} :

$$t_{t} = \frac{\rho_{m} d_{i}^{2} c_{p,m}}{6 kg \overline{Nu}} \left[\frac{T_{m}}{\overline{T}_{s}} \ln \left(\frac{T_{g} - T_{i}}{T_{s} - \overline{T}_{s}} \right) + \frac{H_{f} + c_{p,m} (T_{mp} - \overline{T}_{s})}{c_{p,m} (T_{g} - \overline{T}_{s})} \right]$$

where ρ_m is the fluid density of the metal, d_i is the initial sphere diameter, $c_{p,m}$ is the specific heat of the metal, k_g is the thermal conductivity of the gas, T_m is the temperature of the metal, \overline{T}_s is the average surface temperature of the sphere, T_g is the temperature of the gas, T_i is the initial temperature of the metal, H_f is the latent heat of fusion, and T_{mp} is the melting point of the metal.

4. The average surface temperature of the sphere \overline{T}_s was correlated with the average Nusselt number \overline{Nu} and the ratio of gas to liquid-metal density ρ_g/ρ_m :

$$\frac{T_{mp}}{T_{s}} = 1.0 + 1.10 \times 10^{8} \text{ Nu}^{0.7} \left(\frac{\rho_{g}}{\rho_{m}}\right)^{3}$$

5. The following correlation of the average Nusselt number with the Prandtl and Reynolds numbers was obtained:

$$\overline{Nu} = 2 + 0.4 \text{ Pr}^{0.3} \text{Re}^{0.6}$$

This agreed well with data in the literature for heat transfer from air streams to solid spheres.

Lewis Research Center,

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APPENDIX A

HEATING OF SOLID METAL SPHERES IN GAS STREAMS

The conduction of heat in a solid metal sphere may be expressed in spherical coordinates as

$$\frac{{}^{K}m}{\rho_{m}c_{p,m}} \frac{1}{r^{2}} \frac{\partial}{\partial r} \left(r^{2} \frac{\partial T}{\partial t}\right) = \frac{\partial T}{\partial t}$$
(A1)

where $k_m / \rho_m c_{p,m}$ is the thermal diffusivity or ratio of the thermal conductivity to the product of the density and specific heat of the sphere and r is the radial distance of a point from the center of the sphere at temperature T and time t.

The heat balance at the surface of a metal sphere suspended in a high-temperature and high-velocity gas stream may be written as

$$q_{\rm m} = g_{\rm g,c} + q_{\rm g,r} \tag{A2}$$

where q_m is the heating rate of the sphere and $q_{g,c}$ and $q_{g,r}$ are rates of heat transfer from the gas stream by convection and radiation, respectively. Since

$$q_{\rm m} = \pi r^2 k_{\rm m} \frac{dT}{dr}$$
$$q_{\rm g, c} = \pi r^2 h(T_{\rm g} - T_{\rm s})$$

and

$$\alpha_{g,r} = \pi r^2 \left(\alpha_1 T_g^4 - \alpha_2 T_s^4 \right)$$

equation (A2) becomes

$$\frac{\mathrm{dT}}{\mathrm{dr}}\bigg|_{\mathbf{r}=\mathbf{r}_{\mathbf{S}}} = \frac{\mathrm{h}}{\mathrm{k}_{\mathbf{m}}} \left(\mathrm{T}_{\mathbf{g}} - \mathrm{T}_{\mathbf{S}}\right) + \frac{\sigma}{\mathrm{k}_{\mathbf{m}}} \left(\alpha_{1}\mathrm{T}_{\mathbf{g}}^{4} - \alpha_{2}\mathrm{T}_{\mathbf{S}}^{4}\right)$$
(A3)

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where h is the heat-transfer coefficient at the surface of the sphere, σ is the Stefan-Boltzmann constant, and α_1 and α_2 are the absorptivity and emissivity of the polished metal, respectively.

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APPENDIX B

COMBUSTION GAS PROPERTIES

Combustion gas properties were calculated for equilibrium conditions in the combustor by the method given in reference 6. The results are given in table IV for the three exhaust nozzles used in this study.

The viscosity and thermal conductivity of the combustion gas stream were also determined by this method for a range of gas temperatures. The results of these calculations are plotted in figure 9.

Mass mixture	Gas pressure,		Gas temperature,	Gas density,	
ratio,	$\frac{P_g}{psia N/m^2 abs}$		т _g ,	$\rho_{\rm g}^{},$	
0/1			°C	g/cm^3	
1.7	270	18.6×10 ⁵	1818	6.70	
5.3	255	17.5	3250	7.92	
8	230	15.8	3471	8.58	
10	215	14.8	3417	9.18	
12	200	13.7	3327	9.57	

TABLE IV. - COMBUSTION GAS STREAM PROPERTIES



Figure 9. - Combustion gas properties calculated by method given in reference 7.

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