# United States Patent [19]

## Chan et al.

#### [54] JOULE THOMSON REFRIGERATOR

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#### [57] ABSTRACT

A bi-directional Joule Thomson refrigerator is described, which is of simple construction at the cold end of the refrigerator. Compressed gas flowing in either direction through the Joule Thomson expander valve and becoming liquid, is captured in a container in direct continuous contact with the heat load. The Joule Thomson valve is responsive to the temperature of the working fluid near the valve, to vary the flow resistance through the valve so as to maintain a generally constant mass flow between the time that the refrigerator is first turned on and the fluid is warm, and the time when the refrigerator is near its coldest temperature and the fluid is cold. The valve is operated by differences in thermal coefficients of expansion of materials to squeeze and release a small tube which acts as the expander valve.

#### 5 Claims, 1 Drawing Sheet



side of the valve at 44. The liquid retention chamber 36 on the second side 44 of the valve captures the liquid portion 46 of the fluid.

The chamber 36 is in direct and continuous thermal contact with the heat load 12 that is to be cooled. There 5 is continuous evaporation of the liquid 46, although there remains some fluid to maintain the heat load 12 at a constant temperature. A portion of the fluid passing in a first direction 47 through the valve that does not liquefy, as well as gas evaporated from the liquid 46, passes 10 through heat exchanger 32 where its temperature is raised to lower the temperature of fluid in the heat exchanger 30, and passes through the precooler 28 and a tube 50 to the compressor 18. At that time, the compressor 18 is operated to draw in fluid. After most of the 15 fluid has passed from the first compressors 16 through the valve 20 to the second compressor 18, the refrigerator is operated in the reverse direction to begin the second half of the cycle. This is accomplished by operating the right side compressor 18 to compress the gase- 20 ous working fluid therein to a high pressure, while the left side compressor 16 is operated to receive working fluid.

During the second half of the cycle, fluid flows in the direction of arrow 52 from the right side compressor 18 25 through the precooler 28 where the fluid drops in temperature, and then through the heat echanger 32 where the fluid undergoes a second drop in temperature. The fluid then passes through a conduit 54, and then through the valve 20 in a second direction 56. Some of the fluid 30 liquefies, and that fluid 60 is captured in the left liquid retention chamber 34. The fluid passing through the valve that is not liquefied, as well as boiloff from the liquid 60 in the left container, moves along a conduit 62 through the heat exchanger 30 and the precooler 26 to 35 the left side compressor 16. The left side liquid retention chamber 34 containing liquefied working fluid, is in direct continual thermal contact with the heat load 12, and may also be in close thermal contact with the other chamber 36.

By operating the refrigerator to liquefy at least some of the working fluid in its passage through the Joule Thomson valve, applicant is able to separate out the coldest portion of the expanded working fluid and create a cold reservoir in the liquid. This enables the cham-45 bers containing the liquid to remain in continuous thermal contact with the heat load, without the need for any thermal switches between the liquid container and the heat load. By avoiding the need for a heat switch between the coldest portion of the working fluid and the 50 heat load at either side of the valve, applicant avoids the additional complexity and inefficiency that would result from the need to use and operate heat switches at very low temperatures.

Applicant prefers to use sorption compressors 16, 18 55 which are well known in the prior art. Each adsorption compressor such as 16 includes a quantity of adsorption material such as charcoal which when cold readily adsorbs the working fluid such as helium, and which when hot desorbs the working fluid. To heat the com- 60 pressor 16 to pump out the working fluid, a first heat switch 70 is closed to couple the adsorption material to a heat source 72'. To adsorb working fluid so as to draw it into the compressor 16, a second heat switch 72 is closed (and the first heat switch, 70, is opened) to thermally couple the adsorption material to a heat source 72'. Sorption compressors can be used with other gas

and sorption material combinations, and the system can be used with mechanical compressors.

In order to assure that a substantial amount of the fluid passing through valve 20 will become liquid, the amount of adsorption material in each compressor such as 16 is made great enough, and the amount of working fluid placed in the system is made sufficient, that a high enough pressure drop occurs across the valve 20 to cause liquefaction. A wide variety of other system parameters are also controlled. For example, the temperature of the heat sink 74 is made low enough (by a high temperature refrigerator, not shown) and an appropriate working fluid is chosen which will liquefy at the attained temperature. Also, it is preferable that no substantial expansion of the pressured working fluid flowing out of a compressor, occur until the fluid passes through the valve 20.

In one system that applicant has designed, to maintain the heat load 12 at a temperature of 4° K., the working fluid is helium and the adsorption material in each compressor is charcoal. Sufficient working fluid is contained in the system, so that when the compressor 16 is coupled to the heat source 72' which is at 40° K., the pressure of the fluid reaches 20 atmospheres (300 psi). At the same time, the other compressor 18 can be coupled to the heat sink 74 which is at a temperature of 20° K., with a pressure of working fluid in the right compressor 18 being about 1 atmosphere (15 psi). With the left compressor 16 heated and the fluid at a temperature T<sub>1</sub> of 40° K., the fluid passes through the precooler 26 where its temperature at T<sub>2</sub> drops to 20° K.. In downward passage through the heat exchanger 30, the fluid temperature drops to a temperature T<sub>3</sub> of 10° K.. In passage through the valve 20, the fluid drops to a temperature T<sub>4</sub> of 4<sup>•</sup> K. It requires about one minute for almost all of the pressured fluid to pass through the valve 20. Then the cycle is reversed with the right compressor 18 heated and the left compressor 16 cooled, and it requires another minute for completion of 40 the cycle.

During startup of the refrigerator, the working fluid will normally be at a much higher temperature, such as room temperature (22° C. = 295° K.)) which is far above the eventual steady state temperature of the working fluid which may vary between 4° K. and 40° K. in the above example. The density of the working fluid may vary by a ratio of 74 to 1 between 4° K. and 295° K. If the cross-sectional area of the valve is set for efficient operation under steady state conditions, then the area will be too small to allow a large mass flowthrough of fluid at a higher temperature during startup. This results in much less cooling and a much longer time before steady state conditions are achieved. Applicant varies the resistance to flowthrough of fluid of the valve 20, in accordance with the temperature, and therefore density, of the working fluid. When the working fluid has a high temperature, during startup, the resistance is low so that a large volumetric flow of fluid passes through the valve. As the fluid temperature decreases, the resistance increases so there is a smaller volumetric flow through the valve. The change in valve resistance is preferrably made so that fluid passes through the valve at roughly the same mass flow rate, regardless of the temperature of the fluid.

FIG. 2 illustrates details of the valve 20, which includes a tube 80 whose walls 82 can be resiliently compressed to vary the minimum cross-sectional area of the tube passage 84. The valve also includes an anvil or

support 86 with a surface 88 that supports one side of the tube, and a compressor element 90 with a compressing surface 92 that can compress the tube. Applicant relies upon the differential coefficient of expansion of materials to move the element 90 towards and away 5 from the support 86 to vary the resistance of fluid passage through the tube.

The support 86 is part of a frame 94 formed of brass which has a thermal coefficient of expansion (TCE) of about 1.2  $\times 10^{-5}$ /° C. A screw 96 has an upper end 10 threadably coupled at 98 to a location on the frame spaced from the tube 80, and has a lower end 100 closer to the tube and bearing against the element 90. The screw 96 and element 90 together form a compressing device, which can be constructed as a single item. The 15 have been described and illustrated herein, it is recogscrew 96 is constructed of titanium which has a TCE of about  $3.6 \times 10^{-6/4}$  C. When the temperature of the valve increases, the distance 102 along much of the length of the brass frame will lengthen, as to the length 104. The orginal length 102 of the screw between the 20 point 98 and the bottom of the screw 100 will not lengthen much. With the point 98 moving up, the bottom of the screw will move down only to the point 106. The net result is that the bottom of the screw will move up to allow the tube 80 to expand. Similarly, when the 25 temperature of the fluid decreases, the parts will contract and the tube will be squeezed progressively more. The element 90 is formed of molybdenum. As also shown in FIG. 3, the tube 80 extends through a hole 110 in the frame, and is in close thermal contact with the 30 frame, so that the temperature of the frame follows the temperature of the tube and the fluid therein.

The screw has a knob 112 that can be turned to determine the initial resistance of the tube at a high temperature, and the system can be tested to determine that the 35 valve is operating efficiently at a steady state. The length of the frame, between the location of ths support surface 88 and the point 98 where it engages the thread, is chosen, in conjunction with the difference in thermal coefficient of expansion of the materials, to achieve the 40 desired reduction in tube cross-sectional area as the working fluid decreases in temperature. In a valve constructed as described above, a tube 80 of 0.032 inch outside diameter of stainless steel was used with a frame 94 of overall height of 0.5 inch, and was found to effec- 45 tively vary the flow rate.

It should be noted that the change in flow resistance of the valve does not depend directly upon the temperature of the heat load 12, which may require some time to achieve its steady state temperature after the working 50 fluid has reached its steady state low temperature. Instead, the valve resistance is adjusted in accordance with the temperature of the working fluid passing through the valve, to maintain a substantially constant (less than 7 to 1 variation) mass flow of fluid through 55 the valve during startup when the temperature of the fluid drops greatly, as from room temperature to near absolute zero. The use of a squeezable tube to vary the valve resistance avoids the difficulty of sealing moving parts against the loss of fluid. It would be possible to use 60 a temperature sensor that senses fluid temperature anywhere in the system, or a timer circuit which begins counting when system startup begins, to control a motor that varies valve resistance. However, reliance on differential TCE's can result in a simpler system, and 65 one which is self-actuated.

Thus, the invention provides a Joule Thomson refrigerator which is especially efficient at the cold end of the

refrigerator. In a bi-directional refrigerator, the working fluid undergoes a sufficient pressure drop, starting at a sufficiently low temperature, that much of the fluid becomes liquid. The liquid is captured in a liquid-holding container at each side of the valve, with each container in direct and continuous thermal contact with the heat load. The resistance to fluid passage through the valve is varied according to the temperature of the working fluid, to maintain a more constant mass flow rate of fluid through the valve despite variation in working fluid temperature during startup of the refrigerator, than if the valve passage had a constant crosssectional size.

Although particular embodiments of the invention nized that modifications and variations may readily occur to those skilled in the art, and consequently, it is intended that the claims be interpreted to cover such modifications and equivalents.

What is claimed is:

1. A bi-directional refrigeration system for cooling a heat load comprising:

first and second compressors;

first and second liquid containers;

- a Joule-Thomson gas expansion valve having first and second opposite sides;
- a first conduit extending between said first compressor and said first side of said-valve, and a second conduit extending between said second side of said valve and said second compressor, each container coupled to one of said conduits at a different side of said valve to receive liquid resulting from gas expanding through said valve;
- each container being in continual thermal contact with said heat load.
- 2. The system described in claim 1 wherein:
- said liquid containers are thermally coupled to each other so they are always at substantially the same temperature.
- 3. The system described in claim 1 wherein:
- said valve is adjustable to change the resistance to the flow of gas therethrough; and including
- a working fluid lying in said conduit and containers; and
- means responsive to the temperature of said working fluid for adjusting said valve to increase the resistance to flow therethrough as the temperature of said fluid near said valve decreases.
- 4. A method for cooling a heat load comprising:
- pumping a gaseous working fluid from a first compressor means in a first direction, through a Joule-Thomson valve from a first side to a second side of said valve, wherein the fluid temperature and pressure drop across said valve results in condensation into liquid on said second valve side of at least some of said fluid passing in said first direction;
- catching said liquid in a container from said second valve side, wherein said container is in continual thermal contact with said heat load;
- flowing gaseous working fluid from said second side of said valve to a second compressor means;
- compressing working fluid in said second compressor means and precooling said compressed working fluid and passing said compressed and precooled working fluid in a second direction opposite to said first direction through said valve to condense into liquid on said first valve side at least some of said fluid passing in said second direction;

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- catching said liquid passing in said second direction in a container from said first valve side, wherein said container is in constant thermal contact with said heat load;
- flowing gaseous working fluid from said first side of said valve to said first compressor means; and
- cyclically repeating said steps of pumping fluid in a first direction, catching liquid from said second side, conducting fluid to said second compressor, compressing fluid and passing it in said second

direction, catching liquid from said first side, and conducting fluid to said first compressor.

- 5. The method described in claim 4 including:
- sensing the temperature of said working fluid at a predetermined location, and altering the resistance to fluid passage through said valve to increase the resistance as the fluid becomes colder, whereby to effectively operate during startup when the working fluid is warm, as well as during continuing operation when the working fluid temperature has dropped.

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