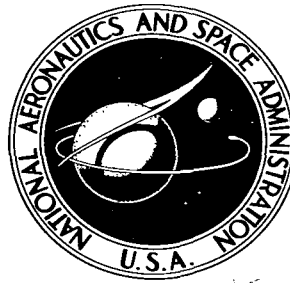


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TURBULENT TEMPERATURE FLUCTUATIONS AND TWO-DIMENSIONAL HEAT TRANSFER IN A UNIFORM SHEAR FLOW

by Jay Fox

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Cleveland, Ohio*

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SUMMARY

Correlation equations for statistically homogeneous fluctuations of velocity and temperature at two points in an infinite uniform shear flow are derived with allowance for a temperature gradient in an arbitrary direction in a plane normal to the flow direction. The initially excited isotropic turbulence decays and becomes anisotropic with time. After Fourier transformations are introduced, the resulting spectral equations are solved for the case of weak turbulence wherein triple correlations are neglected compared with double correlations. Spectra of turbulent heat transfer and temperature fluctuation are calculated. For large nondimensional velocity gradients, the thermal eddy diffusivity in the direction normal to the velocity gradient is much larger than that in the direction of the velocity gradient. The thermal eddy diffusivity in the velocity gradient direction tends to equal the momentum eddy diffusivity at large velocity gradients.

INTRODUCTION

Phenomenological theories of turbulence, which are reviewed in reference 1, have recently received support from statistical turbulence theory. In a uniform shear flow with decaying turbulence, a tendency of the ratio of eddy diffusivities for heat and momentum to approach unity was found for conditions that correspond roughly to steady channel flow (ref. 2). Developments of this nature do not form a basis for supplanting phenomenological theories, which are the only practical means of organizing quantities of experimental evidence. Rather, statistical theories further the understanding of turbulence and may, in some instances, point the way for new extensions of the phenomenological theories when no experimental evidence is available.

A uniform shear flow is described by a constant gradient of mean velocity in a direction normal to the flow direction. No boundaries are present. Transient turbulence, which is spatially homogeneous, is initially established, for instance, by a wire screen, and the turbulence is later studied when it is

weak enough for the triple correlations of velocity or temperature fluctuations to be neglected.

Early statistical investigations of turbulent heat transfer were concerned with the isotropic turbulence that arises in the absence of a mean velocity gradient (refs. 3 and 4). For shear flows, numerical values of the velocity correlations were first presented in reference 5. Additional studies of heat transfer, pressure fluctuations, and velocity correlations were accomplished in references 2, 6, and 7. In the present effort, these studies are extended to include the effects of a temperature gradient with components not only in the direction of the velocity gradient (the subject of ref. 2) but also in the direction normal to both the velocity vector and the velocity gradient. A similar arrangement of vectors occurs in a tube flow with circumferential variations in heat transfer. In the following development, temperature gradient effects are shown to be separable into components; consequently, the results of the present investigation supplement those of reference 2.

Several features of stronger turbulence are present in weak turbulent shear flows, as shown in reference 5. Transfer between eddies of different sizes is present, as is production of turbulence by the action of the mean velocity gradient. The decay of velocity and temperature fluctuations proceeds, however, despite the production effects since they are not strong enough to offset dissipation effects.

SYMBOLS

a	transverse velocity gradient, dU_1/dx_2
a^*	dimensionless transverse velocity gradient, $(t - t_0)dU_1/dx_2$
b, c	transverse temperature gradients, $\partial T/\partial x_2$ and $\partial T/\partial x_3$, respectively
J_0	constant that depends on initial conditions
P, P'	arbitrary points
Pr	Prandtl number, ν/α
p	instantaneous pressure
r	distance from P to P'
\vec{r}	distance vector from P to P'
r_k	component of \vec{r}
T	average temperature
\tilde{T}	instantaneous temperature

T_t	transfer term for temperature fluctuations obtained by integrating $\kappa_1 \partial \delta / \partial \kappa_2$ in eq. (25) over angular coordinates of wave number sphere
t	time
t_0	initial value of t
U_k	average velocity component
\tilde{u}_k	instantaneous velocity component
u_k	fluctuating part of velocity component defined by eq. (4)
x_k	space coordinate
α	thermal diffusivity
Γ_2, Γ_3	spectrum functions of $\overline{u_2}$ or $\overline{u_3}$ defined by eq. (29)
r_j	Fourier transform of $\overline{u_j}$ defined by eq. (15)
r'_i	Fourier transform of $\overline{u_i \tau'}$ defined by eq. (16)
Δ	spectrum function of $\overline{\tau^2}$ defined by eq. (30)
δ	Fourier transform of $\overline{\tau \tau'}$ defined by eq. (17)
δ_{ij}	equals 1 for $i = j$; equals 0 for $i \neq j$
ϵ	eddy diffusivity for momentum transfer defined by eq. (34a)
ϵ_h	eddy diffusivity for heat transfer defined by eqs. (34b)
ζ	Fourier transform of $\overline{\tau p'}$ defined by eq. (19)
ζ'	Fourier transform of $\overline{p \tau'}$ defined by eq. (20)
θ	spherical coordinate in wave number space
K	wave number
K^*	dimensionless wave number, $\nu^{1/2}(t - t_0)^{1/2} K$
\vec{K}	wave number vector
K_i	component of wave number vector
ν	kinematic viscosity
ξ	dummy variable

ρ density
 τ fluctuating part of temperature defined in eq. (3)
 ϕ spherical coordinate in wave number space
 ϕ_{ij} Fourier transform of $\overline{u_i u_j}$ defined by eq. (18)

Subscripts:

i, j, k values equaling 1, 2, or 3 and designating coordinate directions
 $(2), (3)$ scalar quantities that arise from effects of $\partial T / \partial x_2$ or $\partial T / \partial x_3$

Superscripts:

$(')$ point P'
 $(\bar{})$ average value
 $(*)$ dimensionless quantity

ANALYTICAL FORMULATION

The thermal energy equations at two points P and P' can be written for constant properties as

$$\frac{\partial \tilde{T}}{\partial t} + \frac{\partial \tilde{u}_k \tilde{T}}{\partial x_k} = \alpha \frac{\partial^2 \tilde{T}}{\partial x_k \partial x_k} \quad (1)$$

and

$$\frac{\partial \tilde{T}'}{\partial t} + \frac{\partial \tilde{u}_k' \tilde{T}'}{\partial x_k'} = \alpha \frac{\partial^2 \tilde{T}'}{\partial x_k' \partial x_k'} \quad (2)$$

where \tilde{u}_k and \tilde{T} are the instantaneous velocity component and temperature, respectively. Cartesian components of the position vector \vec{x} are designated by the subscript k , which takes on the values 1, 2, and 3. A repeated subscript on a term implies a summation of three terms corresponding to the three values of the subscript. The symbols t and α represent time and thermal diffusivity, respectively. A division of instantaneous quantities into steady and fluctuating components is accomplished by setting

$$\tilde{T} = T + \tau \quad (3)$$

and

$$\tilde{u}_k = U_k + u_k \quad (4)$$

These relations are substituted into equation (1), and the resulting equation

is averaged over a large number of systems that are macroscopically the same but have random fluctuating quantities that are spatially homogeneous in a statistical sense (ensemble average). The averaged equations are subtracted from the unaveraged ones with the result

$$\frac{\partial \tau}{\partial t} + U_k \frac{\partial \tau}{\partial x_k} + u_k \frac{\partial \tau}{\partial x_k} + \frac{\partial \tau u_k}{\partial x_k} - \frac{\partial \overline{\tau u_k}}{\partial x_k} = \alpha \frac{\partial^2 \tau}{\partial x_k \partial x_k} \quad (5)$$

where the bar indicates an averaged quantity. The average of a fluctuating component is necessarily zero. At point P' , the equation corresponding to equation (5) can be visualized from equations (1) and (2). In a similar manner, the Navier-Stokes equations were treated in reference 5 to yield (at point P')

$$\frac{\partial u_j}{\partial t} + u'_k \frac{\partial U'_j}{\partial x'_k} + U'_k \frac{\partial u_j}{\partial x'_k} + \frac{\partial u_j u'_k}{\partial x'_k} - \frac{\partial \overline{u_j u'_k}}{\partial x'_k} = -\frac{1}{\rho} \frac{\partial p'}{\partial x'_j} + \nu \frac{\partial^2 u_j}{\partial x'_k \partial x'_k} \quad (6)$$

An equation for $\overline{\tau u'_j}$ is obtained by multiplying equation (5) by u'_j and equation (6) by τ , adding, and averaging the resulting equation. In the interest of brevity, the turbulence is assumed weak at this point in the analysis, so that the triple correlations that arise are neglected compared with the double correlations. None of the omitted triple correlations is different from that in reference 2. The averaged equation is

$$\begin{aligned} \frac{\partial \overline{\tau u'_j}}{\partial t} + U_k \frac{\partial \overline{\tau u'_j}}{\partial x_k} + \overline{u_k u'_j} \frac{\partial \tau}{\partial x_k} + \overline{\tau u'_k} \frac{\partial U'_j}{\partial x'_k} + U'_k \frac{\partial \overline{\tau u'_j}}{\partial x'_k} = \\ - \frac{1}{\rho} \frac{\partial \overline{\tau p'}}{\partial x'_j} + \nu \frac{\partial^2 \overline{\tau u'_j}}{\partial x'_k \partial x'_k} + \alpha \frac{\partial^2 \overline{\tau u'_j}}{\partial x_k \partial x_k} \end{aligned} \quad (7)$$

where the independence of fluctuating quantities at one point from the position of the other point has been utilized in placing the quantities inside the spatial derivative signs. In homogeneous turbulence, $(\partial/\partial x'_k)_{x_k} = \partial/\partial r_k$ and $(\partial/\partial x_k)_{x'_k} = -\partial/\partial r_k$ if $\vec{x}' = \vec{x} + \vec{r}$. In the present case of a single steady velocity component U_1 and one velocity gradient dU_1/dx_2 , a simplifying relation exists:

$$(U'_k - U_k) \frac{\partial \overline{\tau u'_j}}{\partial r_k} = \frac{dU_1}{dx_2} r_2 \frac{\partial \overline{\tau u'_j}}{\partial r_1} \quad (8)$$

which reduces equation (7) to

$$\begin{aligned} \frac{\partial \overline{\tau u_j'}}{\partial t} + \frac{dU_1}{dx_2} r_2 \frac{\partial \overline{\tau u_j'}}{\partial r_1} + \overline{u_k u_j'} \frac{\partial T}{\partial x_k} + \overline{\tau u_2'} \delta_{1j} \frac{dU_1}{dx_2} = \\ - \frac{1}{\rho} \frac{\partial \overline{\tau p'}}{\partial r_j} + (\alpha + \nu) \frac{\partial^2 \overline{\tau u_j'}}{\partial r_k \partial r_k} \end{aligned} \quad (9)$$

where $\delta_{1j} = 1$ for $j = 1$ and 0 for $j \neq 1$.

A similar procedure applied to the equations corresponding to equations (5) and (6) at P' and P yields

$$\begin{aligned} \frac{\partial \overline{u_1 \tau'}}{\partial t} + \overline{u_2 \tau'} \delta_{i1} \frac{dU_1}{dx_2} + \overline{u_1 u_k'} \frac{\partial T}{\partial x_k} + \frac{dU_1}{dx_2} r_2 \frac{\partial \overline{u_1 \tau'}}{\partial r_1} = \\ \frac{1}{\rho} \frac{\partial \overline{p \tau'}}{\partial r_1} + (\alpha + \nu) \frac{\partial^2 \overline{u_1 \tau'}}{\partial r_k \partial r_k} \end{aligned} \quad (10)$$

and, likewise, equation (5) at P and the corresponding equation at P' yield

$$\frac{\partial \overline{\tau \tau'}}{\partial t} + \frac{dU_1}{dx_2} r_2 \frac{\partial \overline{\tau \tau'}}{\partial r_1} + \frac{\partial T}{\partial x_k} (\overline{u_k \tau'} + \overline{\tau u_k'}) = 2\alpha \frac{\partial^2 \overline{\tau \tau'}}{\partial r_k \partial r_k} \quad (11)$$

An additional equation is obtained by applying $\partial/\partial x_j'$ to equation (6) and noting the continuity equation $\partial u_j'/\partial x_j' = 0$. This produces

$$\frac{1}{\rho} \frac{\partial^2 \overline{p'}}{\partial x_j' \partial x_j'} = -2 \frac{\partial u_k'}{\partial x_j'} \frac{\partial U_j'}{\partial x_k'} - \frac{\partial^2 u_j' u_k'}{\partial x_j' \partial x_k'} + \frac{\partial^2 u_j' u_k'}{\partial x_j' \partial x_k'} \quad (12)$$

Multiplying equation (12) by τ , averaging, and introducing $r_j = x_j' - x_j$ give

$$\frac{1}{\rho} \frac{\partial^2 \overline{\tau p'}}{\partial r_j \partial r_j} = -2 \frac{dU_1}{dx_2} \frac{\partial \overline{\tau u_2'}}{\partial r_1} \quad (13)$$

Similarly,

$$\frac{1}{\rho} \frac{\partial^2 \overline{p \tau'}}{\partial r_1 \partial r_1} = 2 \frac{dU_1}{dx_2} \frac{\partial \overline{u_2 \tau'}}{\partial r_1} \quad (14)$$

Fourier transforms are introduced:

$$\overline{\tau u_j'}(\vec{r}) = \int_{-\infty}^{\infty} r_j(\vec{k}) \exp(i\vec{k} \cdot \vec{r}) d\vec{k} \quad (15)$$

$$\overline{u_i \tau'}(\vec{r}) = \int_{-\infty}^{\infty} \gamma_i'(\vec{k}) \exp(i\vec{k} \cdot \vec{r}) d\vec{k} \quad (16)$$

$$\overline{\tau \tau'}(\vec{r}) = \int_{-\infty}^{\infty} \delta(\vec{k}) \exp(i\vec{k} \cdot \vec{r}) d\vec{k} \quad (17)$$

$$\overline{u_i u_j'}(\vec{r}) = \int_{-\infty}^{\infty} \phi_{ij}(\vec{k}) \exp(i\vec{k} \cdot \vec{r}) d\vec{k} \quad (18)$$

$$\overline{\tau p'}(\vec{r}) = \int_{-\infty}^{\infty} \zeta(\vec{k}) \exp(i\vec{k} \cdot \vec{r}) d\vec{k} \quad (19)$$

$$\overline{p \tau'}(\vec{r}) = \int_{-\infty}^{\infty} \zeta'(\vec{k}) \exp(i\vec{k} \cdot \vec{r}) d\vec{k} \quad (20)$$

where $|\vec{k}| = \kappa$ is the wave number, which can be interpreted as the reciprocal of an eddy size.

The Fourier transforms of equations (9) and (13) are

$$\frac{\partial r_j}{\partial t} - \frac{dU_1}{dx_2} \kappa_1 \frac{\partial r_j}{\partial \kappa_2} + \phi_{kj} \frac{\partial T}{\partial x_k} + \delta_{1j} r_2 \frac{dU_1}{dx_2} = - \frac{1}{\rho} i \kappa_j \zeta - (\alpha + \nu) \kappa^2 r_j \quad (21)$$

and

$$- \frac{1}{\rho} i \kappa_j \zeta = 2 \frac{\kappa_1 \kappa_j}{\kappa^2} r_2 \frac{dU_1}{dx_2} \quad (22)$$

where dU_1/dx_2 and $\partial T/\partial x_k$ are constants. Equation (22) can be subtracted from equation (21) and ζ can thus be eliminated from the equations. A similar procedure applied to equations (10) and (14) yields an equation of the same form for γ_i' . In the present study, the case of $r = 0$, $\partial T/\partial x_2 \neq 0$, and $\partial T/\partial x_3 \neq 0$ is considered so that $\gamma_i' = r_j$. The symbols $a = dU_1/dx_2$, $b = \partial T/\partial x_2$, and $c = \partial T/\partial x_3$ are introduced so that the final equations become

$$\frac{\partial r_2}{\partial t} - a \kappa_1 \frac{\partial r_2}{\partial \kappa_2} = - b \phi_{22} - c \phi_{23} + \left[2a \frac{\kappa_1 \kappa_2}{\kappa^2} - \left(\frac{1}{Pr} + 1 \right) \nu \kappa^2 \right] r_2 \quad (23)$$

$$\frac{\partial r_3}{\partial t} - a \kappa_1 \frac{\partial r_3}{\partial \kappa_2} = - b \phi_{32} - c \phi_{33} + 2a \frac{\kappa_1 \kappa_3}{\kappa^2} r_2 - \left(\frac{1}{Pr} + 1 \right) \nu \kappa^2 r_3 \quad (24)$$

and

$$\frac{\partial \delta}{\partial t} - a\kappa_1 \frac{\partial \delta}{\partial \kappa_2} = -2b\gamma_2 - 2c\gamma_3 - 2a\kappa^2\delta \quad (25)$$

where equation (25) is the Fourier transform of equation (11).

SOLUTION OF SPECTRAL EQUATIONS

Isotropic turbulence and zero temperature fluctuations are assumed as initial conditions. Expressions for φ_{22} and φ_{33} that satisfy these initial conditions have been reported in references 5 and 7. The latter is

$$\begin{aligned} \varphi_{33} = & \frac{J_0 \left\{ \kappa_1^2 + [\kappa_2 + a\kappa_1(t - t_0)]^2 + \kappa_3^2 \right\}^2}{12\pi^2(\kappa_1^2 + \kappa_3^2)} \\ & \times \exp \left\{ -2\nu(t - t_0) \left[\kappa^2 + \frac{1}{3} a^2 \kappa_1^2 (t - t_0)^2 + a\kappa_1 \kappa_2 (t - t_0) \right] \right\} \\ & \times \left\{ \frac{\kappa_1^2}{\kappa_1^2 + [\kappa_2 + a\kappa_1(t - t_0)]^2 + \kappa_3^2} + \frac{\kappa_3^2 \kappa_2^2}{\kappa^4} \right. \\ & + \frac{2\kappa_2 \kappa_3^2}{(\kappa_1^2 + \kappa_3^2)^{1/2} \kappa^2} \left[\tan^{-1} \frac{\kappa_2}{(\kappa_1^2 + \kappa_3^2)^{1/2}} - \tan^{-1} \frac{\kappa_2 + a\kappa_1(t - t_0)}{(\kappa_1^2 + \kappa_3^2)^{1/2}} \right] \\ & \left. + \frac{\kappa_3^2}{(\kappa_1^2 + \kappa_3^2)} \left[\tan^{-1} \frac{\kappa_2}{(\kappa_1^2 + \kappa_3^2)^{1/2}} - \tan^{-1} \frac{\kappa_2 + a\kappa_1(t - t_0)}{(\kappa_1^2 + \kappa_3^2)^{1/2}} \right]^2 \right\} \quad (26) \end{aligned}$$

where J_0 and t_0 are constants that depend on the initial conditions.

In reference 7, the solution for $\varphi_{23} = \varphi_{32}$, although nonzero, was found to produce a zero value of $\overline{u_2 u_3}$, which was consistent with the lack of a velocity gradient in the x_2, x_3 -plane. Equations (23) and (24) of this investigation have been solved for the effects of φ_{23} by omission of the terms containing φ_{22} and φ_{33} . (The linearity of the equations permits the addition of solutions.) Zero contributions to $\overline{u_2}$ and $\overline{u_3}$ are obtained from the direct effects of φ_{23} ; however, an indirect effect that does contribute to $\overline{u_3}$ enters equation (24) in the fifth term. This contribution can be traced to the expression of the pressure effect ξ in terms of γ_2 in equation (22). The remaining portion of γ_2 that contributes to $\overline{u_2}$ is the same as that reported in reference 2; it is not repeated herein. In the following solutions to equations (24) and (25), only those expressions that contribute to $\overline{u_3}$ or τ^2 are shown.

For a Prandtl number equal to 1 the Fourier transform of $\overline{u_3}$ is

$$\begin{aligned}
r_3 = & \text{Joc} \left\{ \frac{\kappa_1^2 + \left[\kappa_2 + a\kappa_1(t - t_0) \right]^2 + \kappa_3^2}{12\pi^2 a\kappa_1 (\kappa_1^2 + \kappa_3^2)} \right. \\
& \times \exp \left\{ -2\nu(t - t_0) \left[\kappa^2 + a\kappa_1\kappa_2(t - t_0) + \frac{1}{3} a^2\kappa_1^2(t - t_0)^2 \right] \right\} \\
& \times \left\{ - \frac{a\kappa_1^3(t - t_0)}{\kappa_1^2 + \left[\kappa_2 + a\kappa_1(t - t_0) \right]^2 + \kappa_3^2} + \frac{\kappa_3^2\kappa_2^2}{(\kappa_1^2 + \kappa_3^2)^{1/2}\kappa^2} \right. \\
& \times \left[\tan^{-1} \frac{\kappa_2}{(\kappa_1^2 + \kappa_3^2)^{1/2}} - \tan^{-1} \frac{\kappa_2 + a\kappa_1(t - t_0)}{(\kappa_1^2 + \kappa_3^2)^{1/2}} \right] \\
& \left. \left. + \frac{\kappa_3^2\kappa_2}{(\kappa_1^2 + \kappa_3^2)} \left[\tan^{-1} \frac{\kappa_2}{(\kappa_1^2 + \kappa_3^2)^{1/2}} - \tan^{-1} \frac{\kappa_2 + a\kappa_1(t - t_0)}{(\kappa_1^2 + \kappa_3^2)^{1/2}} \right] \right\} \right\}
\end{aligned}$$

For a Prandtl number not equal to 1, r_3 takes the form (27a)

$$\begin{aligned}
r_3 = & - \text{Joc} \left\{ \frac{\kappa_1^2 + \left[\kappa_2 + a\kappa_1(t - t_0) \right]^2 + \kappa_3^2}{12\pi^2 a\kappa_1 (\kappa_1^2 + \kappa_3^2)} \right. \\
& \exp \left\{ \frac{[(1/\text{Pr}) - 1]\nu\kappa_2}{a\kappa_1} \left(\kappa_1^2 + \frac{\kappa_2^2}{3} + \kappa_3^2 \right) \right. \\
& \left. \left. - 2\nu(t - t_0) \left[\kappa^2 + a\kappa_1\kappa_2(t - t_0) + \frac{1}{3} a^2\kappa_1^2(t - t_0)^2 \right] \right\} \right. \\
& \times \int_{\kappa_2}^{\kappa_2 + a\kappa_1(t - t_0)} \exp \left\{ - \frac{[(1/\text{Pr}) - 1]\nu}{a\kappa_1} \xi \left(\kappa_1^2 + \frac{\xi^2}{3} + \kappa_3^2 \right) \right\} \\
& \times \left\{ - \frac{\kappa_1^2}{\kappa_1^2 + \left[\kappa_2 + a\kappa_1(t - t_0) \right]^2 + \kappa_3^2} + \kappa_3^2 \left[\frac{\xi}{\kappa_1^2 + \xi^2 + \kappa_3^2} \right. \right. \\
& \left. \left. + \frac{1}{(\kappa_1^2 + \kappa_3^2)^{1/2}} \left(\tan^{-1} \frac{\xi}{(\kappa_1^2 + \kappa_3^2)^{1/2}} - \tan^{-1} \frac{\kappa_2 + a\kappa_1(t - t_0)}{(\kappa_1^2 + \kappa_3^2)^{1/2}} \right) \right] \right. \\
& \left. \left. \times \left[\frac{\kappa_2}{\kappa^2} + \frac{1}{(\kappa_1^2 + \kappa_3^2)^{1/2}} \left(\tan^{-1} \frac{\kappa_2}{(\kappa_1^2 + \kappa_3^2)^{1/2}} - \tan^{-1} \frac{\kappa_2 + a\kappa_1(t - t_0)}{(\kappa_1^2 + \kappa_3^2)^{1/2}} \right) \right] \right\} d\xi
\end{aligned}$$

(27b)

These expressions for γ_2 and γ_3 verify the fact that the turbulent heat-transfer components $\overline{u_2}$ and $\overline{u_3}$ arise from temperature gradient components in the respective directions $\partial T/\partial x_2$ and $\partial T/\partial x_3$.

The transform of the portion of $\overline{\tau^2}$ that arises from $\partial T/\partial x_3$ is, for a Prandtl number equal to 1,

$$\begin{aligned} \delta_{(3)} = & \frac{J_0 c^2 \left\{ \kappa_1^2 + [\kappa_2 + a\kappa_1(t - t_0)]^2 + \kappa_3^2 \right\}^2}{12\pi^2 a^2 \kappa_1^2 (\kappa_1^2 + \kappa_3^2)} \\ & \times \exp \left\{ -2\nu(t - t_0) \left[\kappa^2 + a\kappa_1\kappa_2(t - t_0) + \frac{1}{3} a^2 \kappa_1^2 (t - t_0)^2 \right] \right\} \\ & \times \left\{ \frac{a^2 \kappa_1^4 (t - t_0)^2}{\kappa_1^2 + [\kappa_2 + a\kappa_1(t - t_0)]^2 + \kappa_3^2} + \frac{\kappa_3^2 \kappa_2^2}{\kappa_1^2 + \kappa_3^2} \right. \\ & \left. \times \left[\tan^{-1} \frac{\kappa_2}{(\kappa_1^2 + \kappa_3^2)^{1/2}} - \tan^{-1} \frac{\kappa_2 + a\kappa_1(t - t_0)}{(\kappa_1^2 + \kappa_3^2)^{1/2}} \right]^2 \right\} \end{aligned} \quad (28)$$

The other portion $\delta_{(2)}$ that is a result of $\partial T/\partial x_2$ is the same as that reported in reference 2.

The convenience of interpreting functions of κ instead of functions of K was pointed out in reference 8. Following that suggestion, the integrations that lead to $\overline{\tau_{(3)}^2}$ and $\overline{u_3}$ are accomplished in two steps, the first of which involves integrating over the angular coordinates of a wave number sphere:

$$\Gamma_3(\kappa) = \int_0^\pi \int_0^{2\pi} \gamma_3(\kappa, \phi, \theta) \kappa^2 \sin \theta \, d\phi \, d\theta \quad (29)$$

and

$$\Delta_{(3)}(\kappa) = \int_0^\pi \int_0^{2\pi} \delta_{(3)}(\kappa, \phi, \theta) \kappa^2 \sin \theta \, d\phi \, d\theta \quad (30)$$

A display of Γ_3 and $\Delta_{(3)}$ shows how the contributions to $\overline{u_3}$ and $\overline{\tau_{(3)}^2}$ are distributed among wave numbers or eddy sizes, since

$$\overline{u_3} = \int_0^\infty \Gamma_3 \, d\kappa \quad \text{and} \quad \overline{\tau_{(3)}^2} = \int_0^\infty \delta_{(3)} \, d\kappa \quad (31)$$

COMPUTED SPECTRA

Numerically calculated spectra of $\overline{\tau u_3}$ and $\overline{\tau^2_{(3)}}$ are displayed in dimensionless form in figures 1 and 2 for several values of the dimensionless velocity gradient a^* . Since time enters all the dimensionless representations,

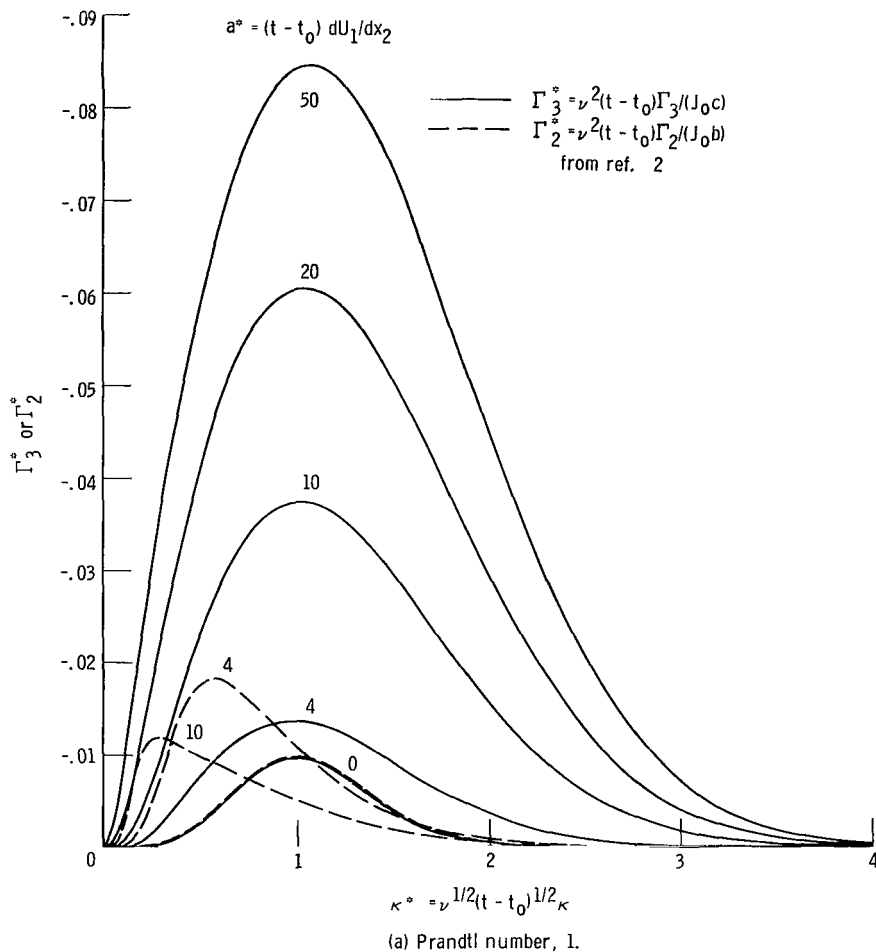


Figure 1. - Dimensionless spectra of $\overline{\tau u_3}$ and $\overline{\tau^2_{(3)}}$ for uniform transverse velocity and temperature gradients and for various Prandtl numbers.

the curves for various a^* show the effect of velocity gradient on the spectra at any given time while the turbulence decays. Dashed curves correspond to those in reference 2 because of separability of solutions. For large Prandtl numbers, the spectra of $\overline{\tau u_3}$ in figure 1 peak at large wave numbers (small eddy sizes).

Isotropic spectra ($a^* = 0$) in figure 1 are the same for $\overline{\tau u_3}$ and $\overline{\tau u_2}$, as previously reported in reference 4. The behavior of the peaks of the spectra of $\overline{\tau u_3}$ and $\overline{\tau u_2}$ is similar to that of the respective production terms $c\phi_{33}$ and $b\phi_{22}$ in equations (23) and (24); ϕ_{22} decreases and shifts toward lower wave numbers as the velocity gradient increases, whereas ϕ_{33} increases

markedly with little shift (see fig. 5 of ref. 5 and fig. 2 of ref. 7).

A shift to higher wave numbers in the spectra of $\overline{\tau^2}$ with increasing velocity gradient is evident in figure 2 both at peak and at moderate values on

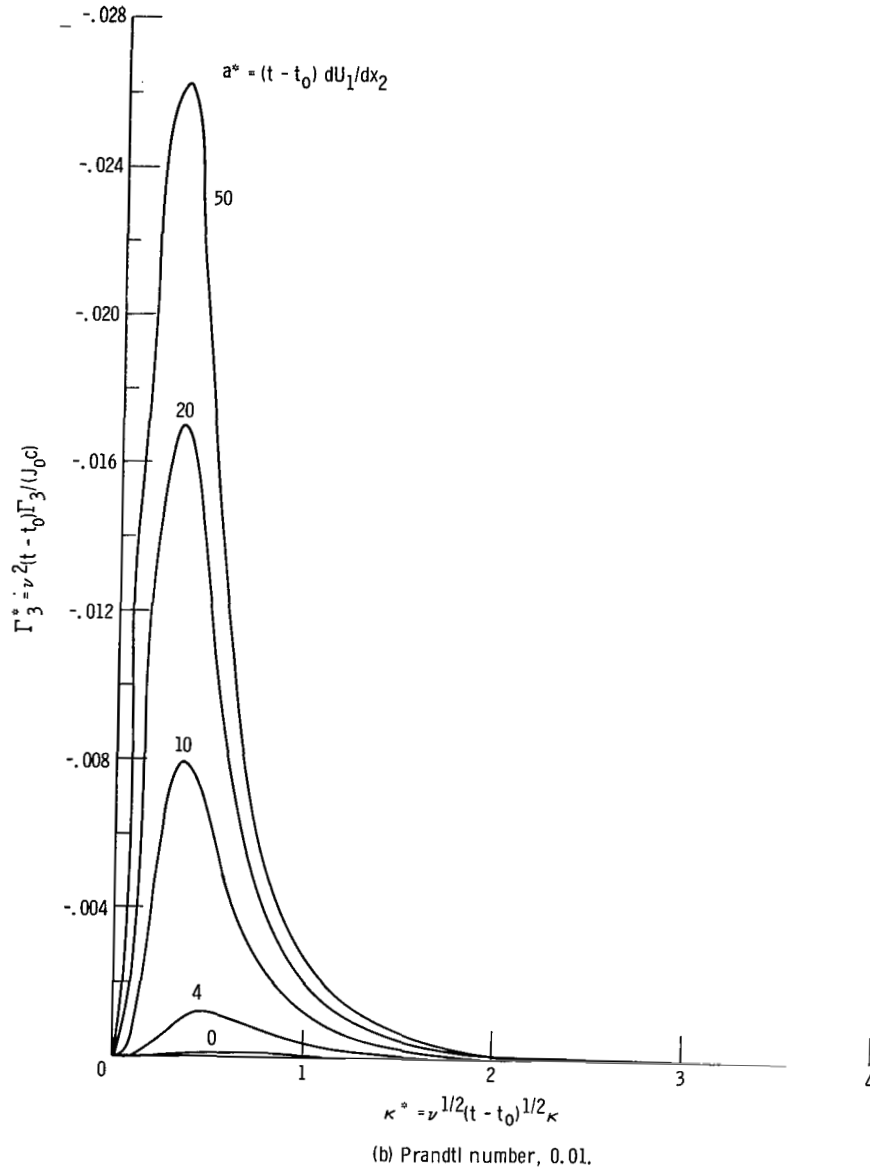


Figure 1. - Continued. Dimensionless spectra of $\overline{\tau u_3}$ and $\overline{\tau u_2}$ for uniform transverse velocity and temperature gradients and for various Prandtl numbers.

the high wave number side; the shift results in an elongation of the spectra toward high wave numbers. This spectral change is evidently due to a transfer of activity from low wave numbers (large eddies) to high wave numbers (small eddies) by the action of the second term in equation (25), which is known as the transfer term. The name stems from the Fourier transform relation

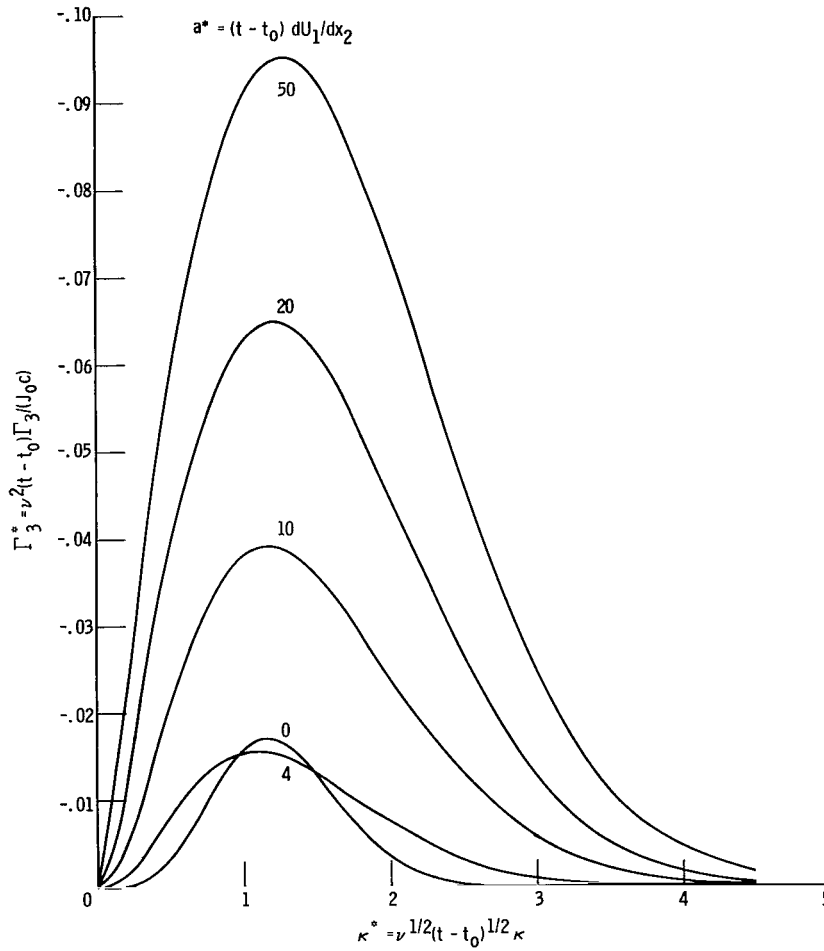
$$r_2 \frac{\partial \overline{\tau \tau'}}{\partial r_1} = - \int_{-\infty}^{\infty} \kappa_1 \frac{\partial \delta}{\partial \kappa_2} \exp(i \vec{\kappa} \cdot \vec{r}) d\vec{\kappa} \quad (32)$$

which becomes, for $r = 0$,

$$\int_{-\infty}^{\infty} \kappa_1 \frac{\partial \delta}{\partial \kappa_2} d\vec{\kappa} = 0 \quad (33)$$

Similar results can be obtained from corresponding terms in equations (23) and (24). Thus, these terms contribute nothing to $\partial \overline{\tau u_3} / \partial t$, $\partial \overline{\tau u_2} / \partial t$, and $\partial \overline{\tau^2} / \partial t$, but they do alter spectral distributions.

The integration shown in equation (33) can be accomplished in two steps by



(c) Prandtl number, 10.

Figure 1. - Concluded. Dimensionless spectra of $\overline{\tau u_3}$ and $\overline{\tau u_2}$ for uniform transverse velocity and temperature gradients and for various Prandtl numbers.

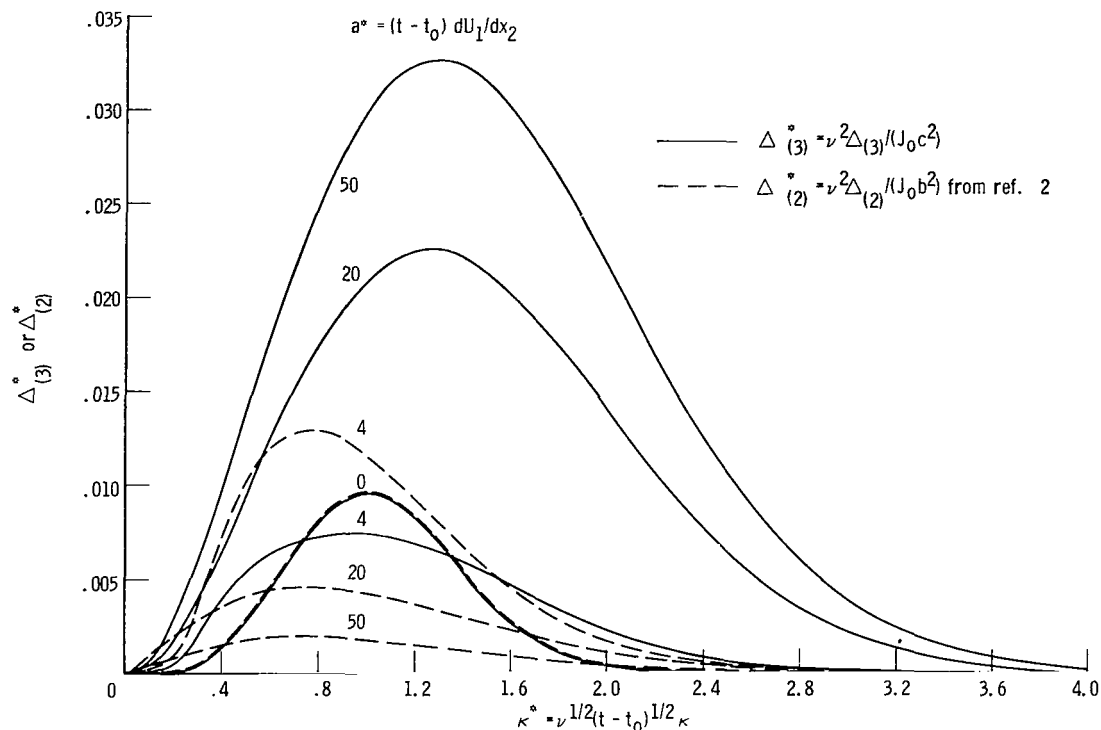


Figure 2. - Dimensionless spectra of $\overline{\tau_{(3)}^2}$ and $\overline{\tau_{(2)}^2}$ for uniform transverse velocity and temperature gradients. Prandtl number, 1.

first integrating over the angular coordinates of a wave number sphere and then integrating over the wave numbers. Of course, the second step yields a trivial result, but the first result is a spectral transfer function. The integrated transfer term corresponding to $\overline{\tau^2}$ is shown in figure 3 for a Prandtl number of 1. Most of the transfer of activity is out of the low wave number spectrum and into the high wave number spectrum, but some reverse transfer occurs at low wave numbers and low velocity gradients. In reference 2 this activity transfer was attributed to a vortex-stretching process, which might also involve vortex compression at low velocity gradients and thereby produce some reverse transfer.

PRODUCTION, TEMPERATURE FLUCTUATION, AND CONDUCTION SPECTRA

Production of temperature fluctuations by the third and the fourth terms in equation (25) is interpreted as a result of the action of the temperature gradient on the respective turbulent heat transfer, $\overline{\tau u_2}$ and $\overline{\tau u_3}$. Conduction or dissipation in the last term reduces local temperature peaks by molecular heat conduction away from hot spots. Production and conduction terms can be integrated over a wave number sphere to yield spectral distributions in the same manner as that used to obtain the temperature fluctuation spectra of $\overline{\tau^2}$ in figure 2. After normalization of the peak values to unity, all three spectra are shown in figure 4 for a Prandtl number of 1 and a high velocity gradient

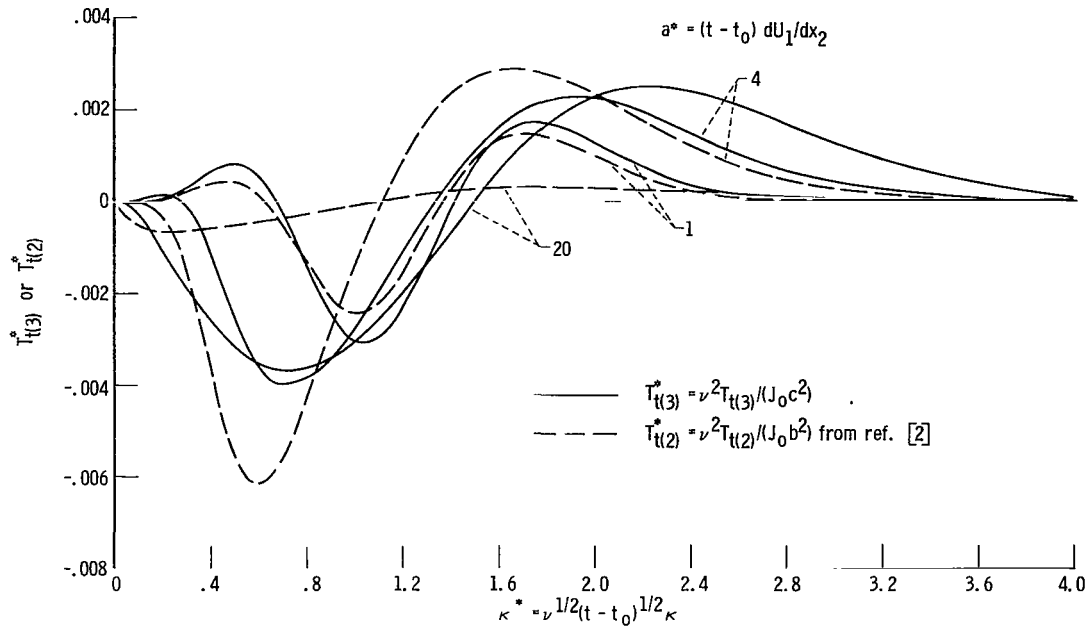


Figure 3. - Dimensionless spectra of transfer terms in spectral equations for $\overline{\tau_{(3)}^2}$ and $\overline{\tau_{(2)}^2}$. Prandtl number, 1.

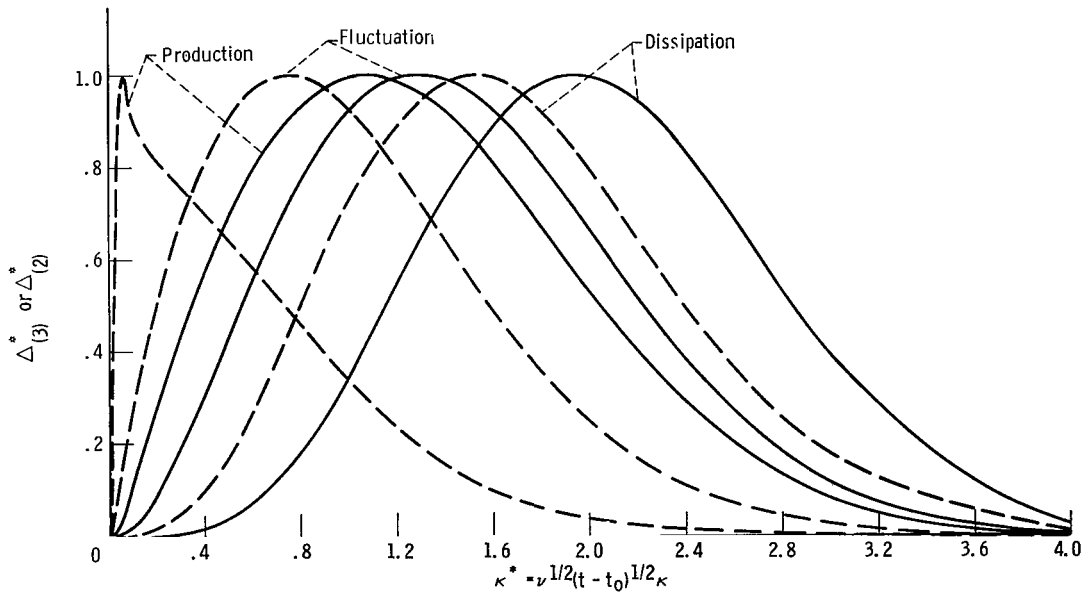


Figure 4. - Comparison of production, temperature fluctuation, and conduction spectra from spectral equations for $\overline{\tau_{(3)}^2}$ and $\overline{\tau_{(2)}^2}$ (solid and dashed curves, respectively) at large velocity gradient. Prandtl number, 1. $a^* = (t - t_0) dU_1/dx_2 = 50$. (Curves normalized to same height.)

($a^* = 50$). Actually, two sets of spectra corresponding to the separate effects of $\partial T/\partial x_3$ and $\partial T/\partial x_2$ (from ref. 2) are displayed in figure 4. For low velocity gradients, the three spectra are close together, like those in figure 4 of reference 2. For a large velocity gradient, production, fluctuation, and conduction spectra in the present figure 4 peak at successively greater wave numbers.

All these effects take place as the turbulence and the turbulent temperature fluctuations decay. Fluctuations are produced in the large eddies (low wave numbers), transferred to the small eddies (high wave numbers), and finally dissipated by molecular conduction.

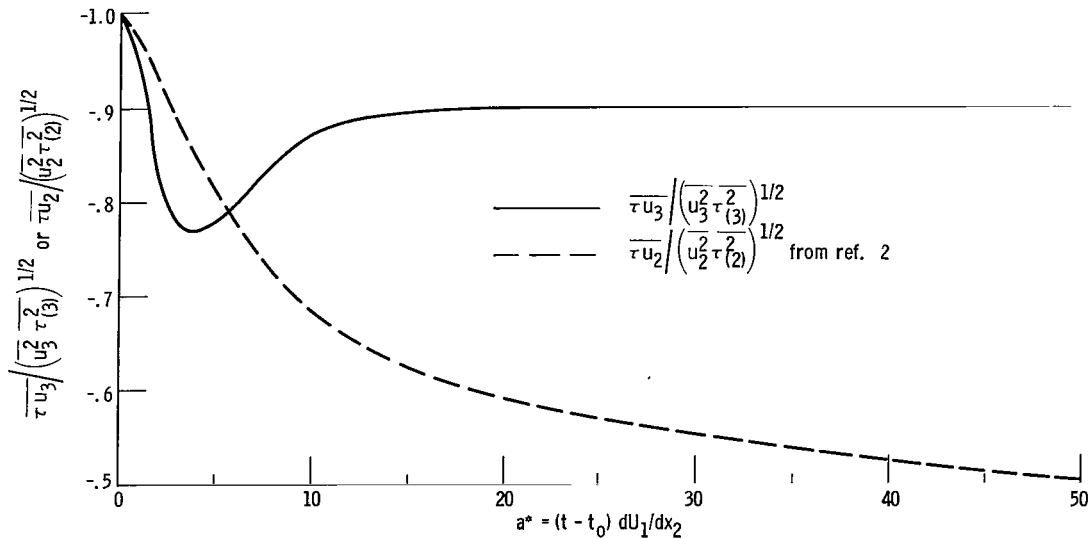


Figure 5. - Temperature-velocity correlation coefficients as a function of dimensionless velocity gradient. Prandtl number, 1.

TEMPERATURE-VELOCITY CORRELATION COEFFICIENT

A temperature-velocity correlation coefficient introduced in reference 3 is modified herein to account for the separate effects of $\partial T/\partial x_2$ and $\partial T/\partial x_3$. Two dimensionless coefficients are utilized,

$$\frac{\overline{\tau u_2}}{(\overline{u^2} \overline{\tau_{(2)}})^{1/2}}$$

and

$$\frac{\overline{\tau u_3}}{(\overline{u^2} \overline{\tau_{(3)}})^{1/2}}$$

the former being the same as that presented in reference 2. The latter coefficient has been calculated from integrals of the curves in figures 1 and 2 and those in figure 2 of reference 7, all for a Prandtl number of 1. Figure 5 is a display of both correlations as a function of velocity gradient, starting with the perfect correlation value of -1 that was obtained in reference 4 for isotropic turbulence ($a^* = 0$). One correlation coefficient

$$\frac{\overline{\tau u_3}}{\left(\overline{u_3^2} \overline{\tau^2(3)}\right)^{1/2}}$$

achieves an asymptotic value of -0.9, whereas the other, by decreasing monotonically, shows a continuous loss of correlation between the temperature and velocity fluctuations as a^* increases.

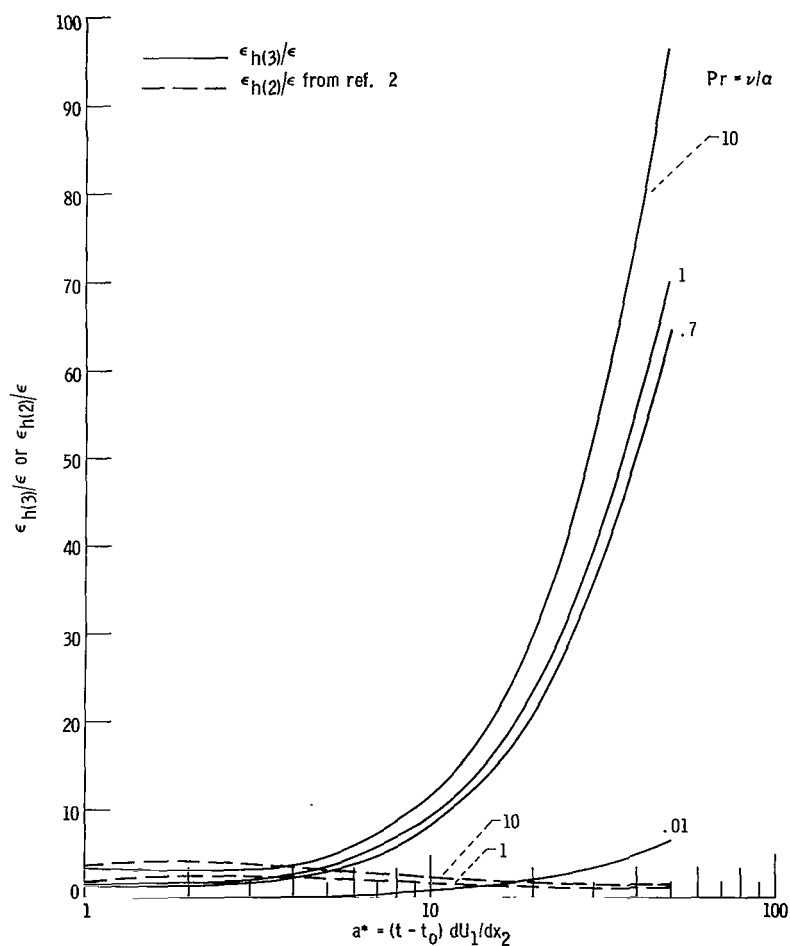


Figure 6. - Ratio of eddy diffusivity for heat transfer to that for momentum transfer as a function of dimensionless velocity gradient.

EDDY DIFFUSIVITIES

The eddy diffusivities of momentum and heat (in the x_2 - and x_3 -directions) are defined by

$$\epsilon = - \frac{\overline{u_1 u_2}}{dU_1/dx_2} \quad (34a)$$

$$\left. \begin{aligned} \epsilon_{h(2)} &= - \frac{\overline{\tau u_2}}{\partial T / \partial x_2} \\ \epsilon_{h(3)} &= - \frac{\overline{\tau u_3}}{\partial T / \partial x_3} \end{aligned} \right\} \quad (34b)$$

Ratios of eddy diffusivities play a large part in phenomenological theories of steady turbulent flows. A unity value of $\epsilon_{h(2)}/\epsilon$ produces the best agreement between experiment and analysis for Prandtl numbers that are not too low (ref. 1). In the transient turbulence analysis of reference 2, a similar tendency of $\epsilon_{h(2)}/\epsilon$ toward unity is obtained at high values of a^* , which correspond roughly to steady turbulent flows. Recent phenomenological analyses (refs. 9 and 10) of circumferential variations of heat transfer in round tubes are based on an assumption of equal eddy diffusivities in the radial and the circumferential directions; that is, $\epsilon_{h(2)} = \epsilon_{h(3)}$ in the present notation.

A dimensionless eddy diffusivity $v^{5/2}(t - t_0)^{3/2} \epsilon_{h(3)}/J_0$ can be obtained by integrating the curves in figure 1. Integration of the curves in reference 5 for ϵ is also necessary for the calculation of $\epsilon_{h(3)}/\epsilon$, which is displayed in figure 6 along with $\epsilon_{h(2)}/\epsilon$ from reference 2. Although the curves for the two ratios are not widely separated at low velocity gradients, which are near the isotropic case ($a^* = 0$), large velocity gradients produce values of $\epsilon_{h(3)}/\epsilon$ that are two orders of magnitude greater than values of $\epsilon_{h(2)}/\epsilon$, except for low Prandtl numbers.

The relative magnitudes of $\epsilon_{h(3)}$ and $\epsilon_{h(2)}$ can be compared with the magnitudes of the turbulent velocity fluctuations (or turbulent energy components) in the two directions $\overline{u_3^2}$ and $\overline{u_2^2}$. References 5 and 7 show that $\overline{u_2^2}$ proceeds rapidly but asymptotically toward zero at large velocity gradients, whereas $\overline{u_3^2}$ decreases slowly from the average of the energy components $\overline{u_1 u_1}/3$, which increases with velocity gradient. Likewise, from physical reasoning, it is clear that the thermal eddy diffusivity is greater in the direction of greater velocity fluctuations.

The existence of greater $\overline{u_3^2}$ than $\overline{u_2^2}$ has long been suspected (ref. 11) and, in recent times, has been verified experimentally in tube and channel flow (refs. 12 and 13) and in boundary layers (ref. 14). In fact, the ordering of all three components of turbulent energy, from largest to smallest, is the same ($\overline{u_1^2}$, $\overline{u_3^2}$, $\overline{u_2^2}$) in those measurements and in the present theory (ref. 7) at large velocity gradients. Apparently, not all features of boundary layers and tube flow depend on the presence of boundaries.

The transient analysis was compared in reference 2 with a steady flow in a boundary layer or tube by taking $K^* \sim 1$ from turbulent energy spectral curves and 0.3δ as a representative length, where δ is the boundary-layer thickness or the tube radius. If U is an average velocity and $dU_1/dx_2 \sim U/\delta$, then a^* is of the order of $0.1 U\delta/\nu$. This implies that $\epsilon_{h(3)}/\epsilon$ is much larger than $\epsilon_{h(2)}/\epsilon$ for Reynolds numbers of 10^4 and over that are encountered in practice.

The results of the present analysis, together with existing velocity-fluctuation measurements, provide no support for an assumption of equal thermal eddy diffusivities in the radial and the circumferential directions ($\epsilon_{h(2)} = \epsilon_{h(3)}$) in turbulent tube flow. Instead, the relation $\epsilon_{h(3)} > \epsilon_{h(2)}$ is indicated.

Lewis Research Center

National Aeronautics and Space Administration
Cleveland, Ohio, February 27, 1964

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2103

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