

2P

Thiokol CHEMICAL CORPORATION

RMD 6062-F

FINAL REPORT

OF₂/Diborane Thrust Chamber Assemblies

17 April 1969



FACILITY FORM 002	N69-33597	
	(ACCESSION NUMBER)	(THRU)
	99	1
	(PAGES)	(CODE)
CR-103837		
(NASA CR OR TMX OR AD NUMBER)		
28		
(CATEGORY)		

REACTION MOTORS DIVISION
DENVER, NEW JERSEY

Reproduced by the
CLEARINGHOUSE
for Federal Scientific & Technical
Information Springfield Va. 22151



RMD 6062-F

FINAL REPORT

OF₂/Diborane Thrust Chamber Assemblies

17 April 1969

RMD Project No. 6062

JPL Purchase Order 952296

Prepared by: *L. VanDerJagt*
L. VanDerJagt
Engineering Specialist

Approved by: *M. J. Webb*
M. J. Webb
Product Engineering
Section Chief

TABLE OF CONTENTS

	<u>Page</u>
I. INTRODUCTION	1
II. DESCRIPTION AND DESIGN SUMMARY	2
1. Requirements	2
2. Design Description	3
3. Design Analysis	6
III. CONCLUSIONS	7

I. INTRODUCTION

This report was prepared as the Final Technical Report for Jet Propulsion Laboratory, Pasadena, California, under Purchase Order 952296 to the Reaction Motors Division, Thiokol Chemical Corporation. The objectives of the program were to design, fabricate and deliver two thrust chamber assemblies to JPL for evaluation with $\text{OF}_2/\text{B}_2\text{H}_6$ propellant combination. This report describes the effort conducted by Thiokol-RMD during the period from 12 September 1968 through 1 May 1969.

The unique thrust chamber approach selected to fulfill the JPL specified requirements is termed the Radiabatic concept (Figure 1). This thrust chamber approach provides increased chamber durability over a wide range of operating conditions with the presently operational and advanced high energy, high flame temperature propellants.

As shown in Figure 1, the Radiabatic concept employs solid pyrolytic graphite pieces as the chamber heat transfer medium analagous to the propellant coolant of a regenerative engine design. In the nozzle region, the heat input from the combustion gases is partially transferred by conduction through the "heat pipes" of anisotropic pyrolytic graphite, arranged to provide high radial and axial conductivity so that the heat is conducted forward toward the injector, where it is rejected to the cool boundary provided by the injector.

There have been a number of concepts in the past which employed solid state multi-dimensional heat transfer. Unfortunately, these approaches have failed, in general, to acknowledge the shortcomings of the anisotropic material, i. e., a tendency toward delamination in a combustion environment and high thermal growth. The Radiabatic concept presented herein uses the best characteristics of pyrolytic graphite and overcomes its shortcoming by proper design. Figure 2 shows a photograph of the two deliverable thrust chambers.

II. DESCRIPTION AND DESIGN SUMMARY

1. Requirements

The purchase order requires that two thrust chamber assemblies be designed and fabricated to meet the following conditions and constraints.

Conditions

. Propellants	$\text{OF}_2/\text{B}_2\text{H}_6$
. Thrust	200 lb
. Chamber Pressure	100 psia
. Duration	1000 seconds
. Core Mixture Ratio	3.0
. Boundary Mixture Ratio	1.0

Constraints

- . Chamber is to interface with JPL injector as defined by Control Drawing No. 10022030, Revision A, dated February 5, 1968
- . Chamber internal dimensions shall conform to JPL Control Drawing No. 10022020, Revision B, dated March 1, 1968
- . Minimum external dimension. Skin temperature not to exceed 600°F during firing
- . Minimum weight
- . Adaptable to future flightweight 60:1 expansion area ratio nozzle
- . Chambers shall be fabricated from one of the following materials or combination thereof:
 - 1) Graphite
 - 2) Pyrolytic Graphite
 - 3) Reinforced Carbon Fibers
 - 4) Any other carbonaceous composites

2. Design Description

The Radiabatic thrust chamber, shown in Figure 1, presents the concept that Thiokol-RMD delivered for the JPL requirements. The interfaces, weight and envelope dimensions are defined in Figure 3. Figure 1 defines the significant features of the Radiabatic thrust chamber which are discussed below.

Liner Assembly

The Radiabatic thrust chamber liner was fabricated from ATJS Graphite. This is a premium grade ATJ graphite and provides a minimum throat erosion. The material is essentially flaw free and, in addition, has excellent thermal shock resistance. The liner is one continuous structure that is retained at the injector end by pyrolytic graphite plates and is permitted to grow axially at the nozzle end. The liner I.D. was contoured as defined in the JPL interface drawing. The liner O.D. was match contoured to the pyrolytic graphite wedges to provide maximum thermal contact.

This improved ATJ type graphite was developed to provide a fine grain with higher physical properties and increased resistance to thermal shock and erosion. The improvements in physical properties is reflected by an increase in density, tensile strength, flexure strength and compressive strength. A lower modulus is a significant factor in the high thermal shock resistance of this grade. Coupled with these physical improvements is a decrease in permeability achieved through fewer pores of decreased diameter. Each of these factors contributes to greater erosion resistance. The liner thickness is increased in the throat area to provide for throat erosion if experienced. Figure 4 shows a photo of the finished liner assembly.

Axial Heat Conduction Wedges

The axial heat conduction wedges were fabricated out of plate pyrolytic graphite with the highly conductive A-B planes oriented parallel to the axial centerline. The graphite liner will conduct the heat into the wedges from whence the heat will be conducted into the outer insulation and transferred back into the chamber gases at the cooler injector end of the chamber. The axial heat is blocked at the injector end by P.G. wafers to provide acceptable temperatures at the interface. The pyrolytic graphite wedges were fabricated in 1/2 inch plates by depositing pyrolytic graphite on a flat mandrel. Pyrolytic graphite plate fabricated in this manner is substrate nucleated with the cone growth from the deposited surface through the plate. This thickness plate can be fabricated with basically no delaminations. Grafoil crushable tape was provided between the wedges to provide for thermal

expansion during operation and precise spacing during fabrication. Figure 5 shows a photo of a finished wedge along with a strip of grafoil tape. Figure 6 shows a photo of the wedge assembly.

Liner/Pyrolytic Graphite Wedge Assembly

It is essential to achieve good thermal transfer from the ATJS liner to the pyrolytic graphite wedges. The following fabrication procedure was followed for this interface:

- 1) Machine the liner to the required contour
- 2) Match contour wedge assembly using liner as a templet
- 3) Lap the interface surfaces between the liner and wedge assembly to obtain intimate contact
- 4) Cement the parts together utilizing compression tooling.

Crushable Retainer Ring

The crushable retainer ring was fabricated from grafoil tape. This ring is designed to retain the pyrolytic graphite wedges against the graphite liner during the thermal transients and will provide a cushion to take up the thermal growth of the pyrolytic graphite radial insulator which is retained on the O.D. by the chamber shell. The grafoil tape crushing strength is considerably less than pyrolytic graphite indicating that the tape will be the component that crushes as is desired.

Radial Insulation Cylinder

The radial insulation cylinder was made from a single piece of pyrolytic graphite. This cylinder provides high temperature insulation between the hot wedges and the chamber shell. The cylinder is designed so that the temperature gradient is sufficient to permit the use of conventional materials for the outer insulation and the chamber shell. Radial thermal expansion was compensated for by the fabrication technique of the pyrolytic graphite and an expansion joint.

The pyrolytic graphite used for the internal insulation was fabricated on a male mandrel. This structure is stress free at 4000F and when it cooled it delaminated in the circumferential direction. This pyrolytic has a slightly lower density and thermal conductivity than a similar part fabricated on the I.D. of a mandrel. This fabrication technique was ideal for this application. When the unit is fired these delaminations will act as spring and reduce the thermal growth loads against the chamber wall. Figure 7 shows a photo of the pyrolytic graphite internal insulation cylinder.

Chamber Jacket Assembly

The chamber jacket assembly was fabricated from C-103 columbium alloy, a medium strength refractory material selected primarily on the basis of its suitability for the application, its excellent fabrication characteristics and its weldability.

A silicide protective coating was applied to provide oxidization and carbide protection for operating temperatures up to 3200°F.

The C-103 columbium alloy has a recrystallization temperature range of 2200F and a brittle ductile transition point below -320F. Since the design temperatures of the columbium approach the recrystallization temperature, the physical properties of recrystallized material will be used. This yields a conservative design.

Figure 8 shows a photo of the jacket assembly with a piece of the outer insulation and the outer shell.

Outer Insulation

The outer diameter insulation was fabricated using Johns-Manville Dyna-Flex. Dyna-Flex is a strong, long fiber, flexible thermal insulation suitable for continuous operating temperatures up to 2700°F. Dyna-Flex is formed from alumina-silica-chromia fibers having a melting point well over 3000°F, and the ability to retain a soft fibrous structure at 2700°F. The material is protected by a thin stainless steel cylinder.

The outer skin at the injector end is insulated by a silica phenolic ring.

Gaskets

A grafoil gasket is encompassed between the silica phenolic insulator and the thrust chamber liner assembly. This gasket provides sealing during thermal expansion of the assembly. Figure 9 shows the mechanical properties of the gasket.

A silicone gasket is installed between the injector adapter flange and the silica phenolic insulator to provide sealing and additional thermal expansion capability.

Other photos of the assembly and details are included as Figures 10 through 16, and are defined as follows:

Figure 10	Thrust Chamber Assembly
Figure 11	Thrust Chamber Liner Assembly
Figure 12	Injector Flange/Insulator/Grafoil Gasket
Figure 13	Thrust Chamber Liner Assembly & Jacket Shell (Injector End)

Figure 14	Thrust Chamber Liner Assembly & Jacket Shell (Nozzle End)
Figure 15	Liner, Wedge Assembly & Radial Insulator
Figure 16	Wedge Assembly

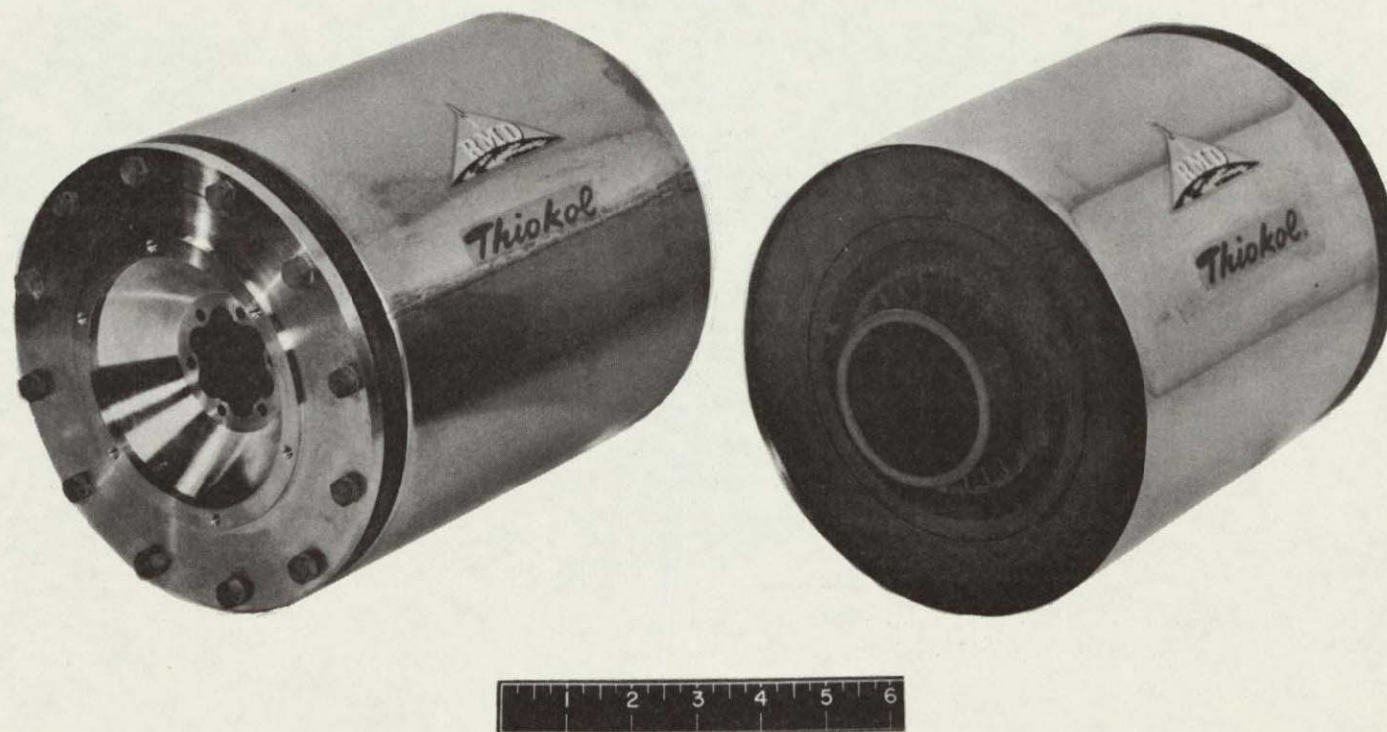
3. Design Analysis

A thermal and stress analysis was performed in conjunction with the design. These reports are included as Appendix A&B and are defined as follows:

Appendix A	DS 100-134	Thermal Analysis of the JPL OF_2 /DB Thrust Chamber
Appendix B	DS 100-135	JPL OF_2 /DB Thrust Chamber Design Analysis.

III. CONCLUSIONS

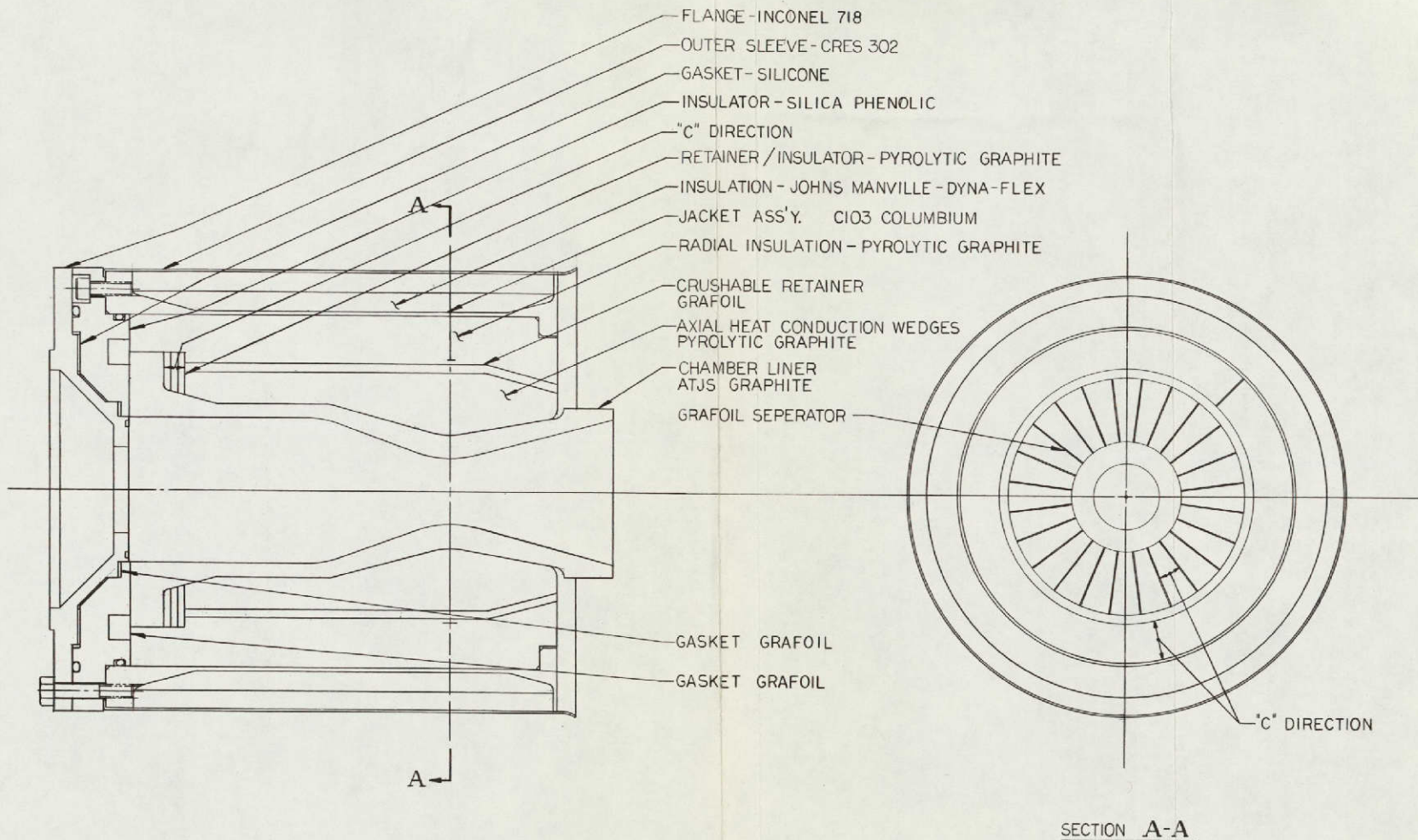
Two Radiabatic thrust assemblies were designed and fabricated to meet the JPL specified conditions and constraints. These thrust chambers will be subjected to experimental testing with $\text{OF}_2/\text{B}_2\text{H}_6$ at JPL later this year.



6062-13

FIGURE 2. JPL OF $_2/B_2H_6$ THRUST CHAMBER ASSEMBLIES

RMD 6062-F



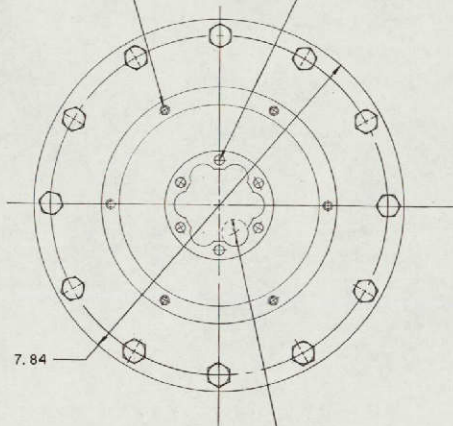
FOLDOUT FRAME

FIGURE 1. RADIABATIC THRUST CHAMBER DESIGN

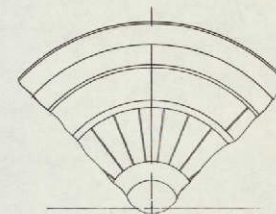
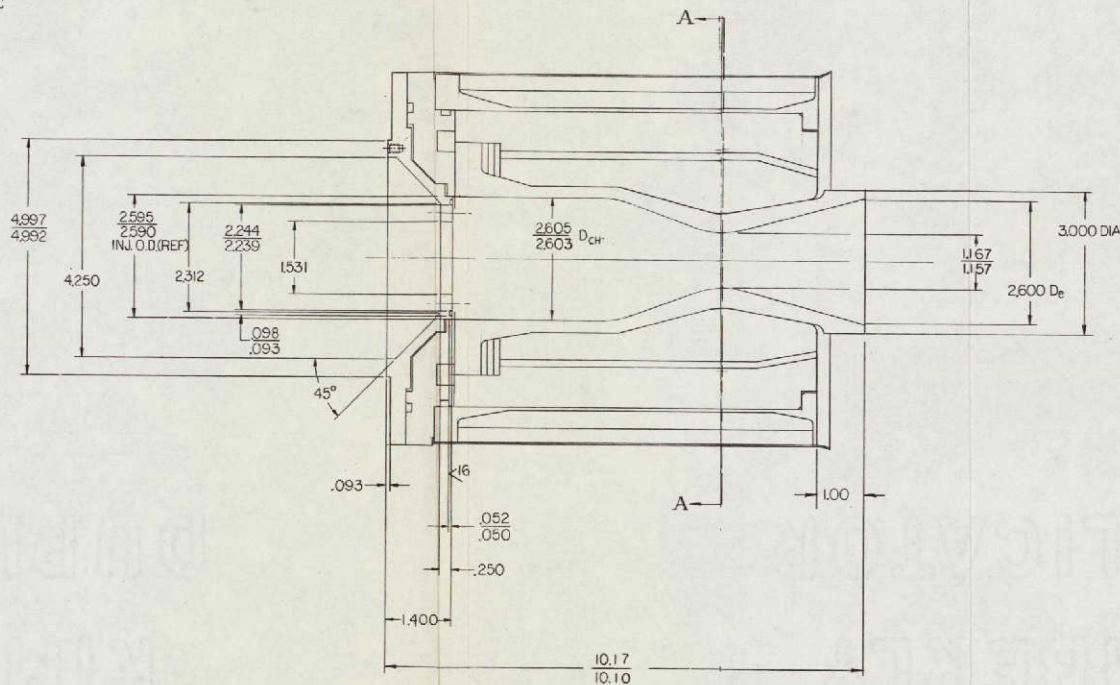
FOLDOUT FRAME

10-32NF-38 -250 DEEP
6 HOLES EQUALLY SPACED
ON A 4.625 DIA. BASIC
⊕ .005 DIA.

.195-.199 DIA THRU
6 HOLES EQUALLY SPACED
ON A 1.900 DIA. BASIC
⊕ .005 DIA.



.562 DIA.
6 HOLES EQUALLY SPACED
ON A 1.344 DIA.



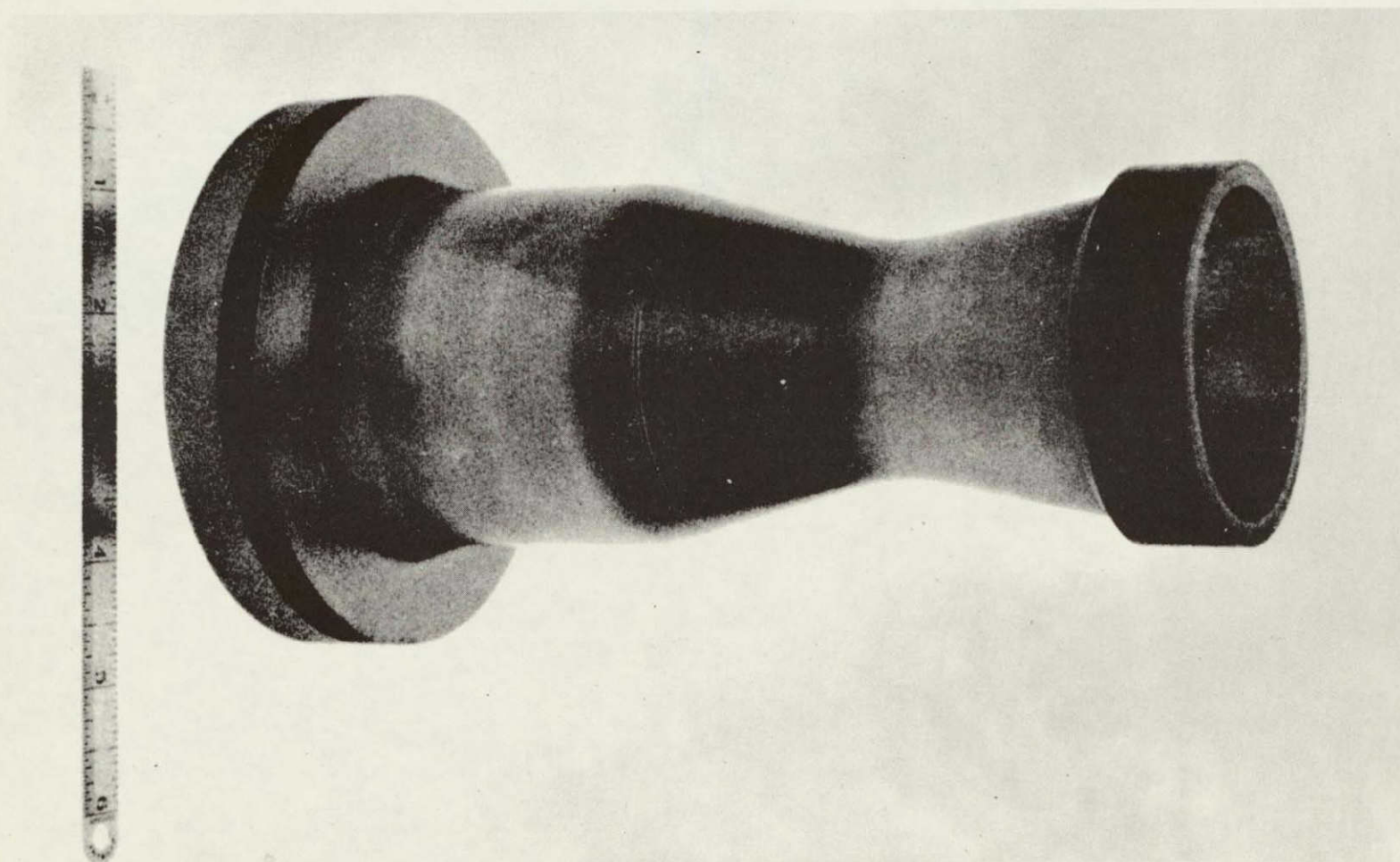
SECTION A-A

ESTIMATED WEIGHT 31.5 LBS

FIGURE 3. RADIABATIC THRUST CHAMBER INTERFACES

FOLDOUT FRAME

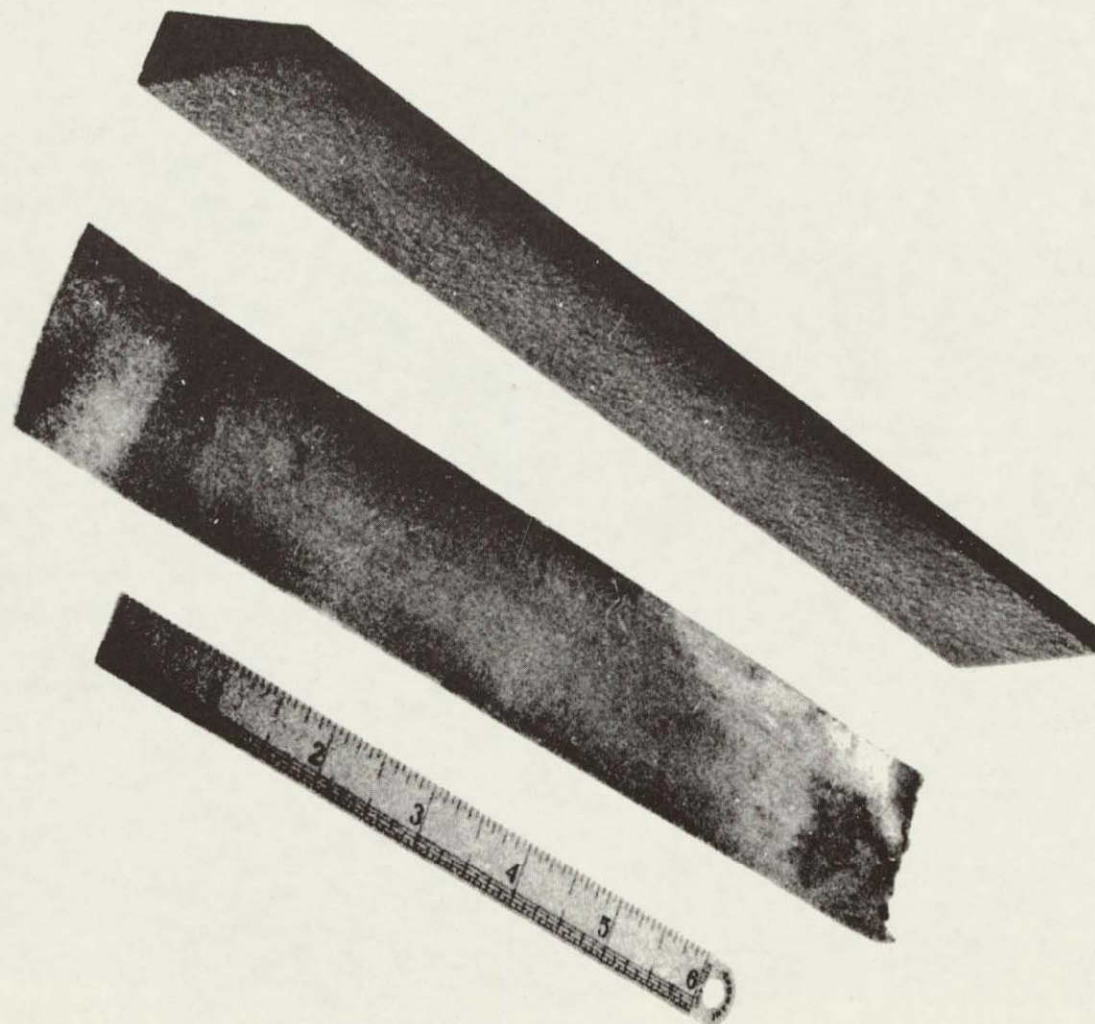
FOLDOUT FRAME



6062-5

FIGURE 4. LINER ASSEMBLY

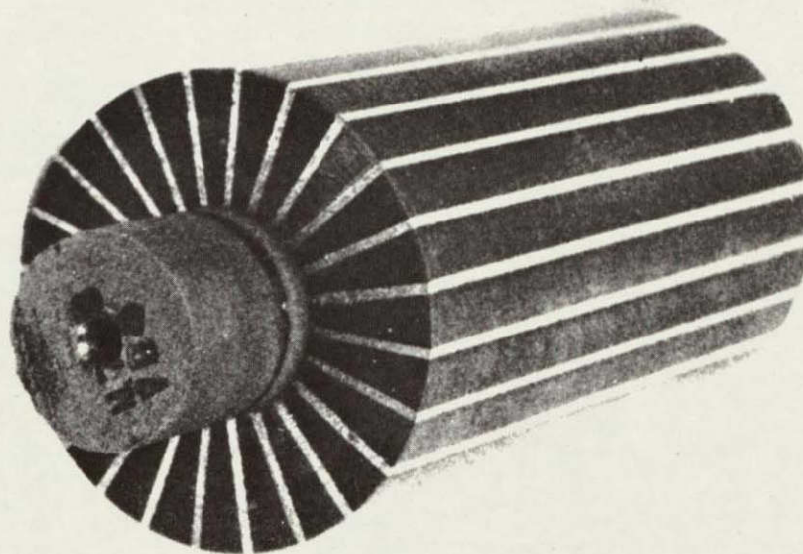
RMD 6062-F



6062-6

FIGURE 5. AXIAL HEAT CONDUCTION WEDGE AND GRAFOIL STRIP

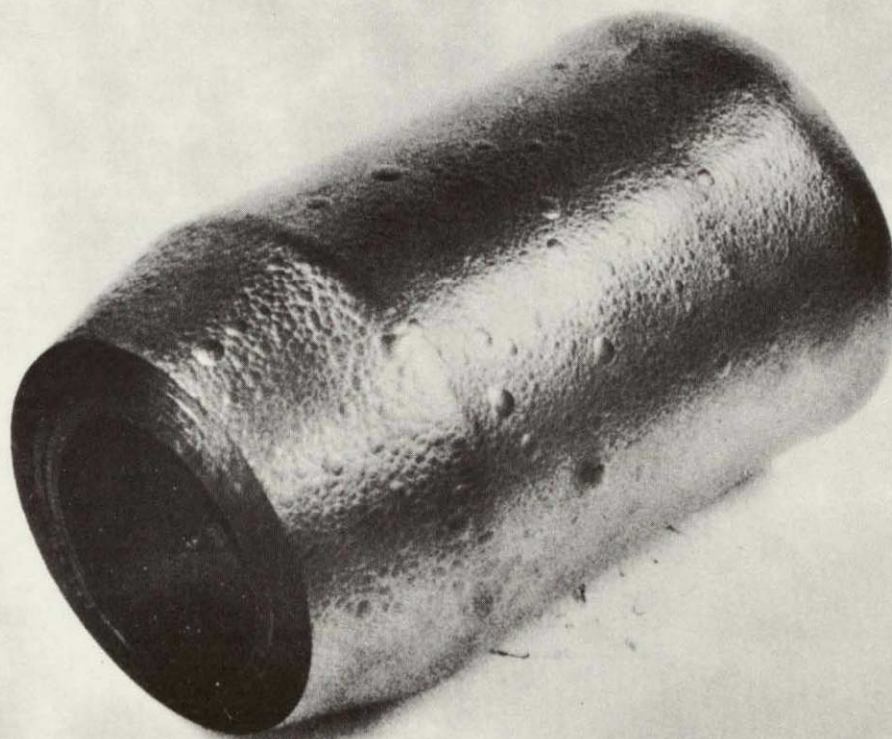
RMD 6062-F



6062-2

FIGURE 6. AXIAL HEAT CONDUCTION WEDGE ASSEMBLY

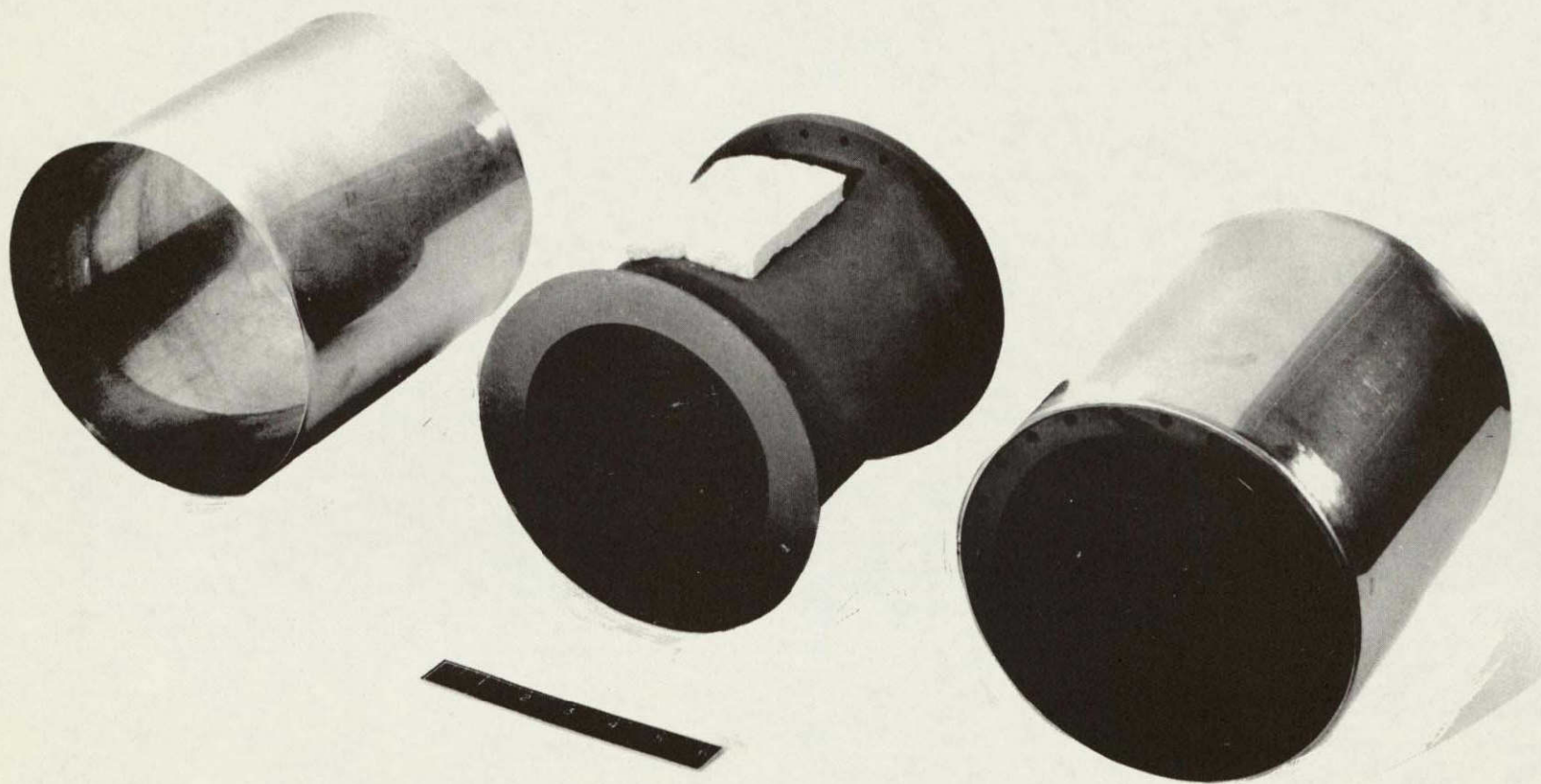
RMD 6062-F



6062-4

FIGURE 7. RADIAL INSULATION CYLINDER

RMD 6062-F



6062-8

FIGURE 8. JACKET/INSULATION/SHELL ASSEMBLY

RMD 6062-F

Compression Relaxation
Grafoil Laminate, Grade GHA
Typical Density 70 lbs/ft³

Thiokol Order C 33876
HTMD No. 4644

Data

- Free Height: .500 in (Ref)
* Installed Height: .380 in
Height @200 psi (Rm temp.): .414 in
* Height @200 psi @ 3100°F: .432

*Design Criteria

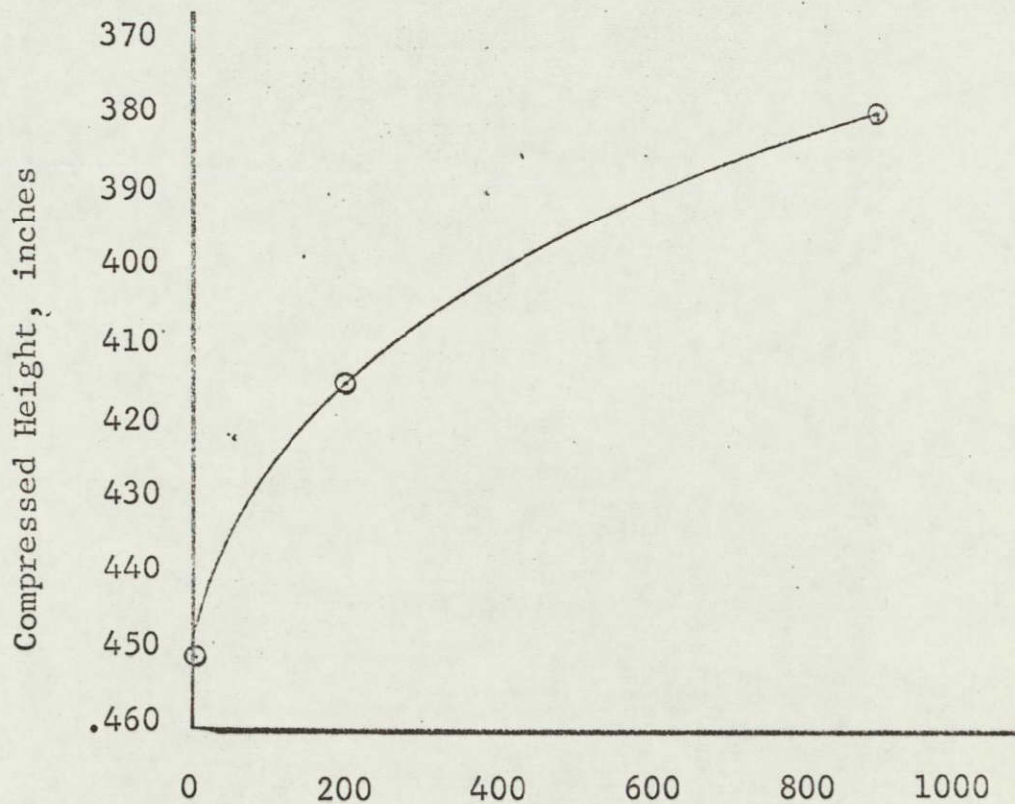


FIGURE 9

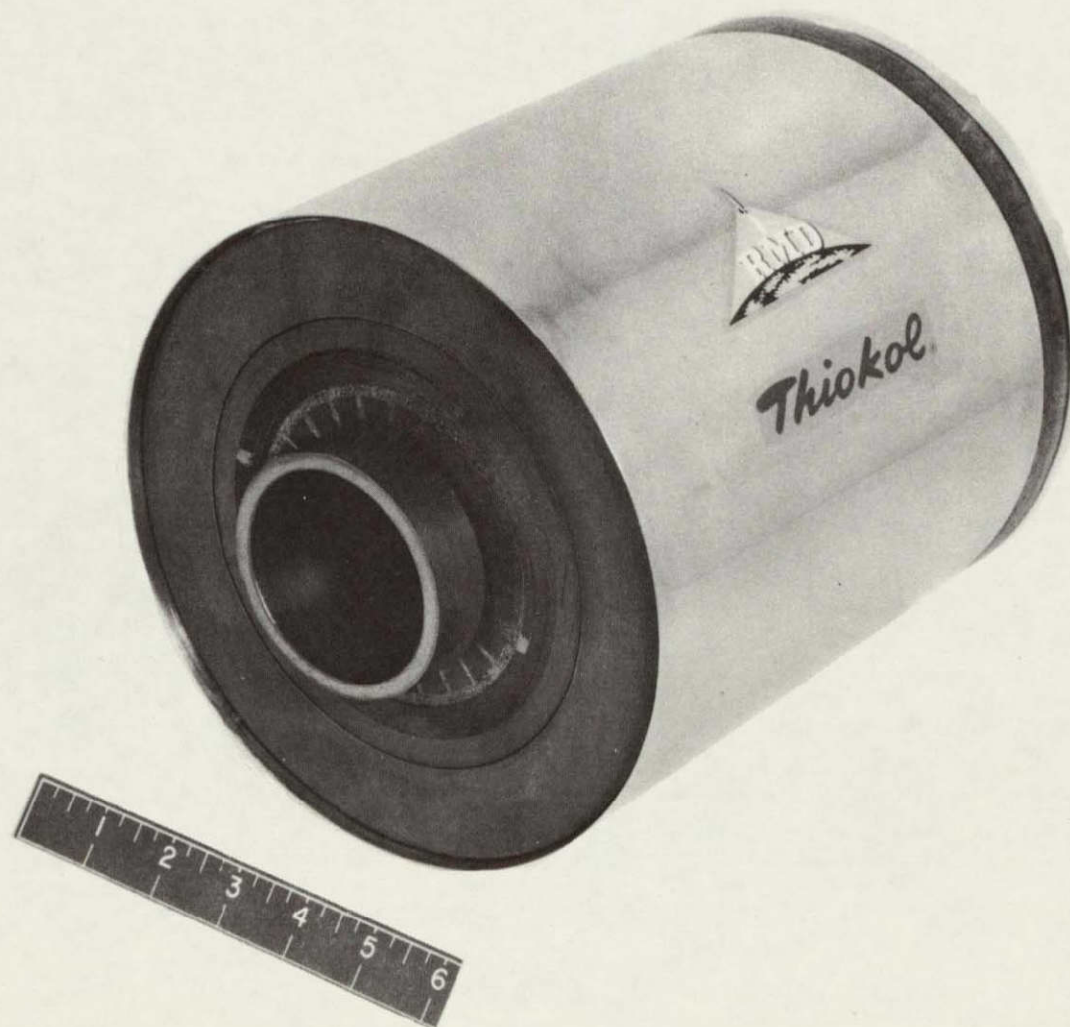


FIGURE 10. THRUST CHAMBER ASSEMBLY

6062-12

RMD 6062-F

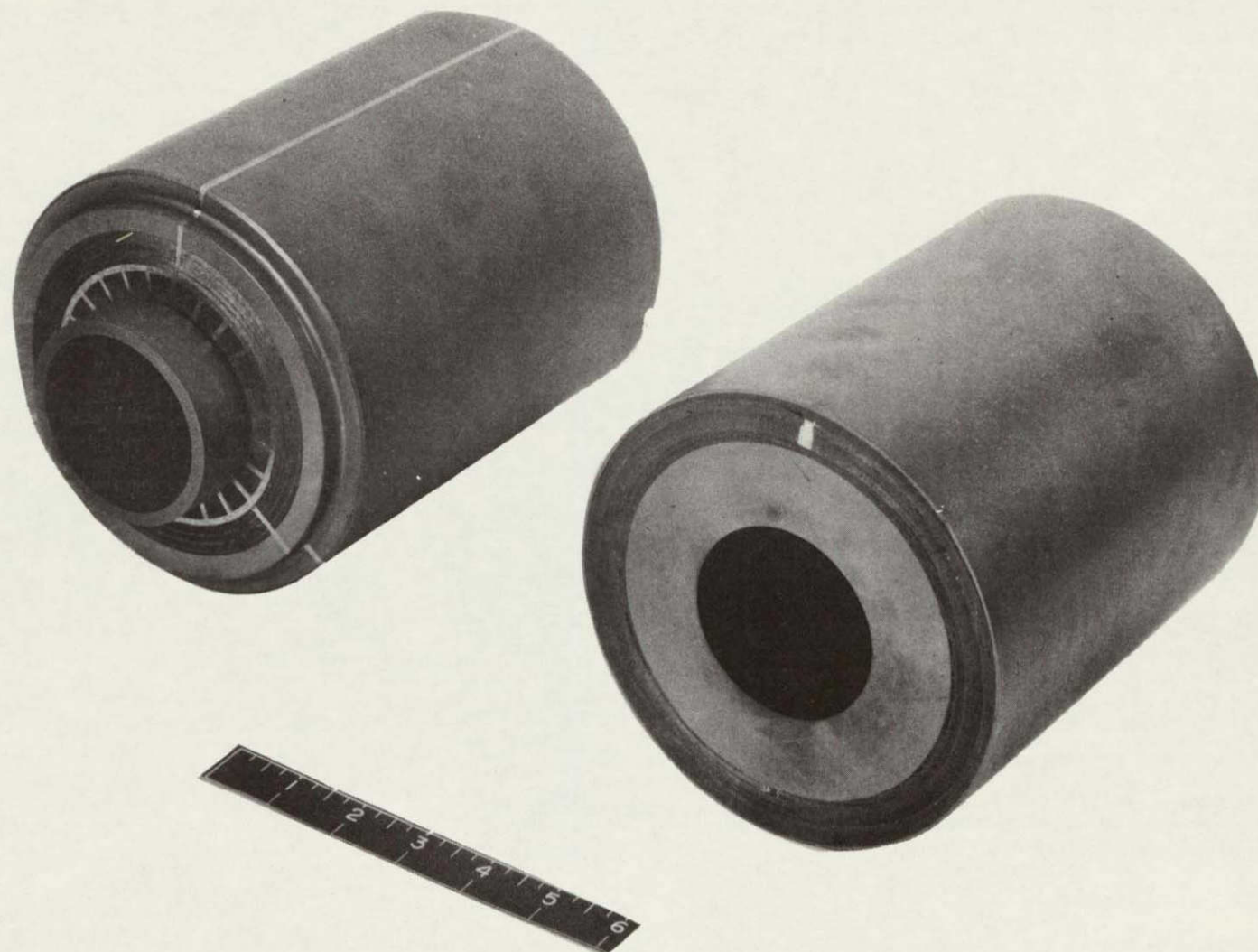
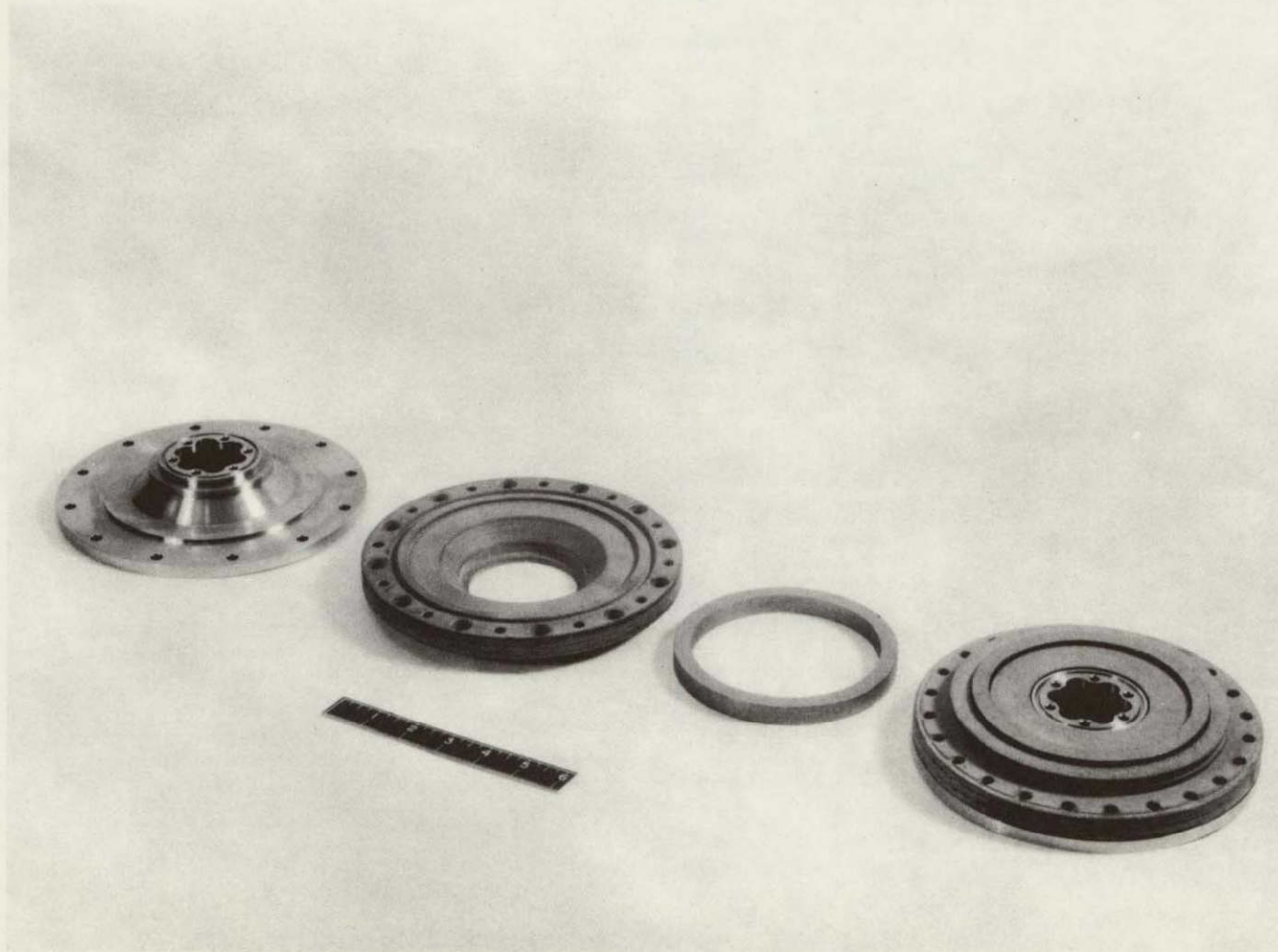


FIGURE 11. THRUST CHAMBER LINER ASSEMBLY

6062-11

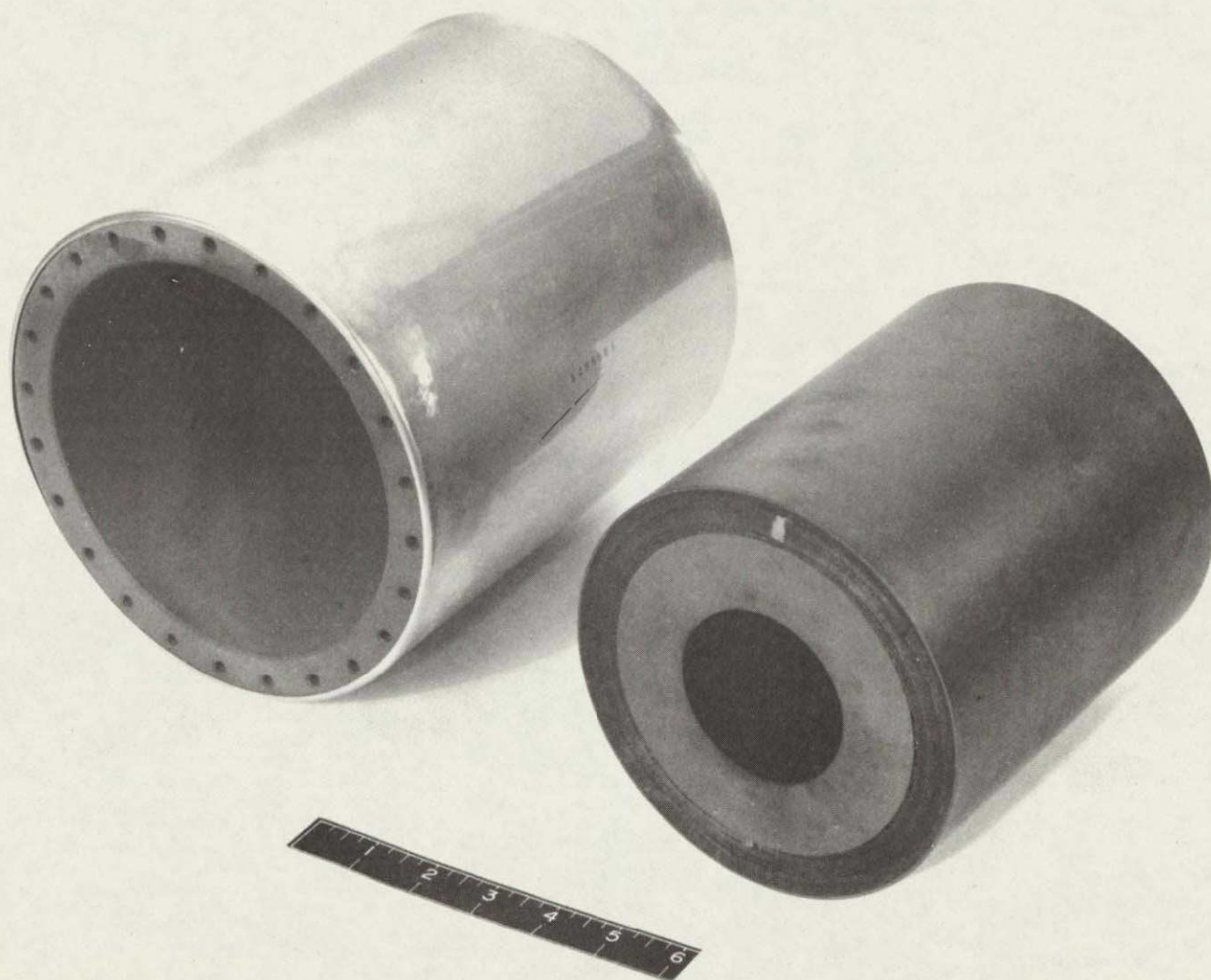
RMD 6062-F



6062-7

FIGURE 12. INJECTOR FLANGE/INSULATOR/GRAFOIL GASKET

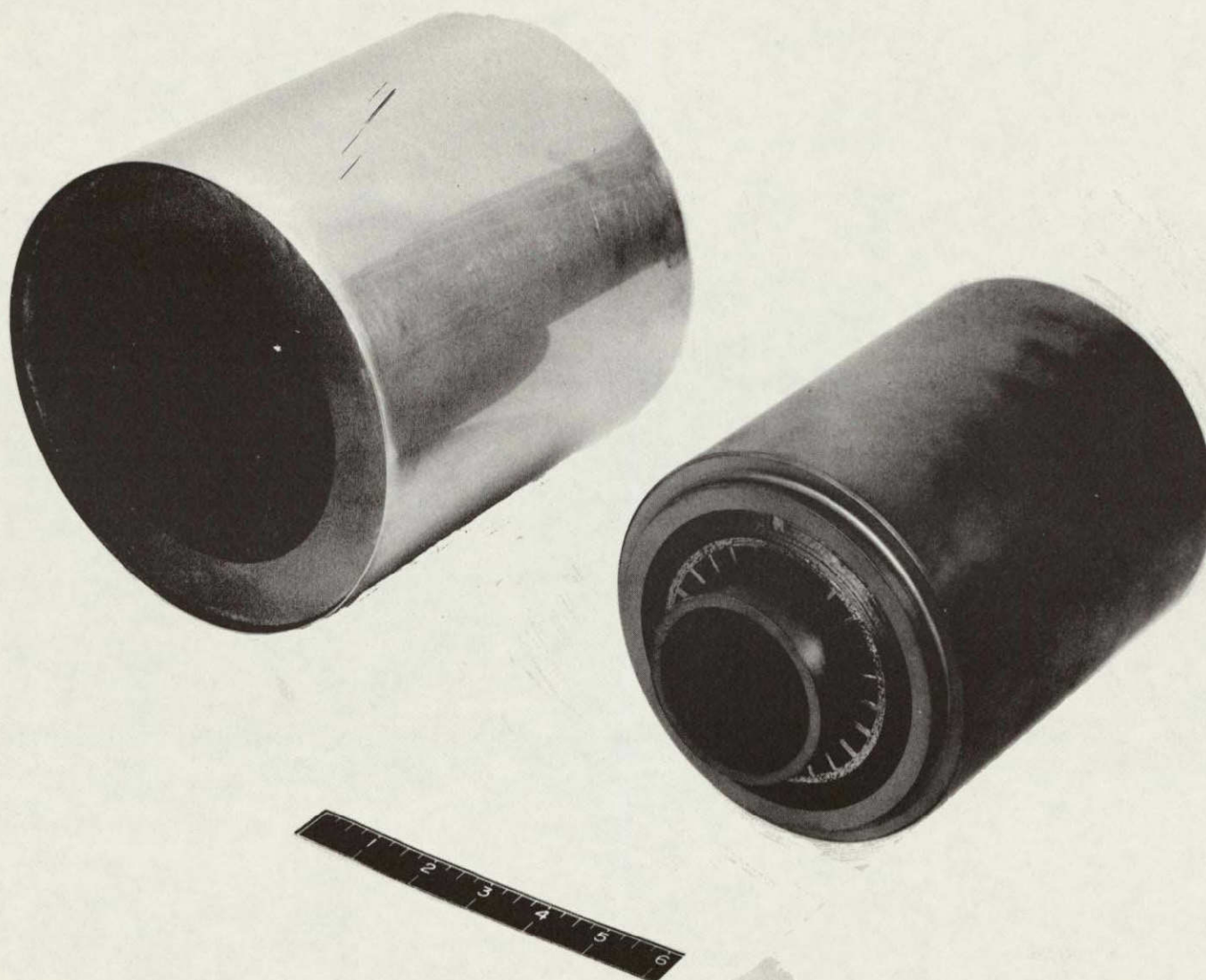
RMD 6062-F



6062-9

FIGURE 13. THRUST CHAMBER LINER ASSEMBLY & JACKET SHELL
(INJECTOR END)

RMD 6062-F



6062-10

FIGURE 14. THRUST CHAMBER LINER ASSEMBLY & JACKET SHELL
(NOZZLE END)

RMD 6062-F



FIGURE 15. LINER, WEDGE ASSEMBLY & RADIAL INSULATOR

6062-1

RMD 6062-F

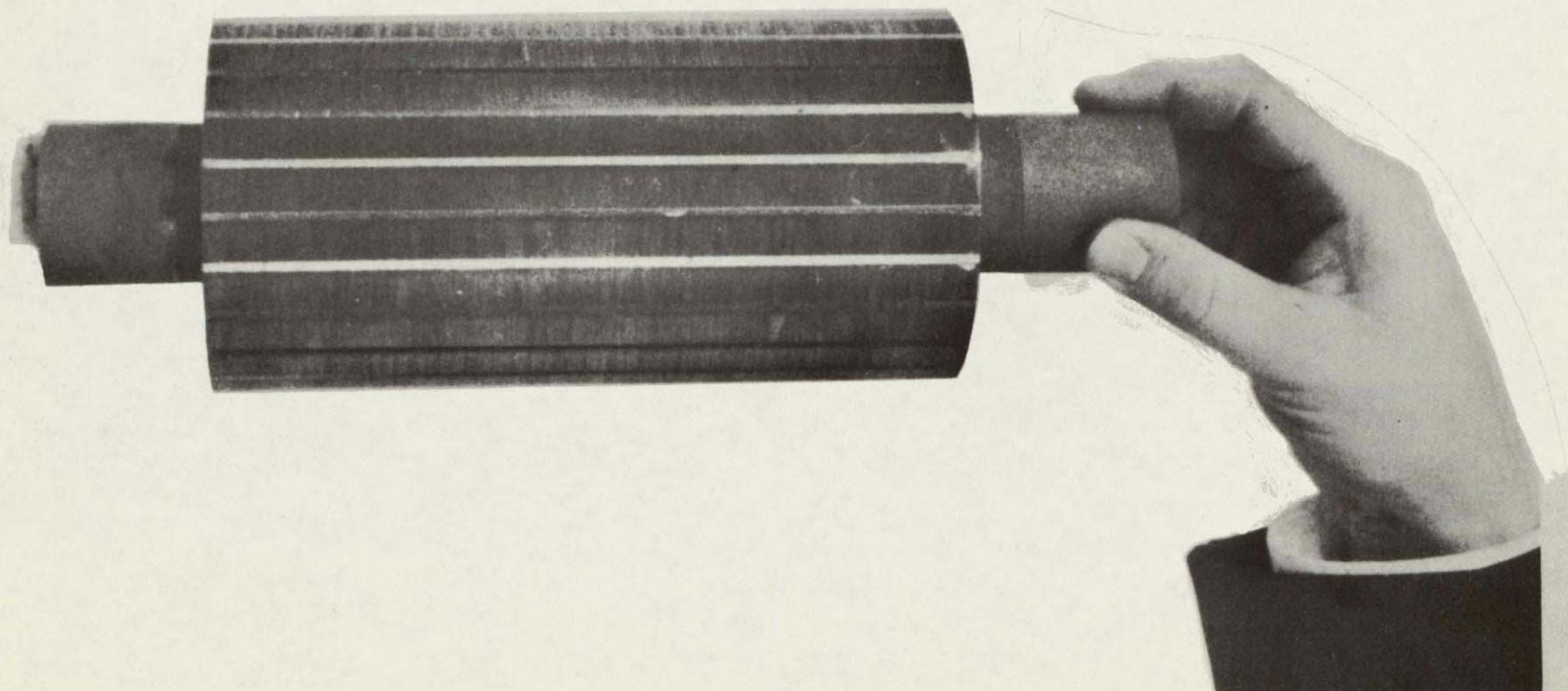


FIGURE 16. WEDGE ASSEMBLY

6062-3

RMD 6062-F

APPENDIX A

JPL OF₂/DB THRUST CHAMBER

THERMAL ANALYSIS

REACTION MOTORS DIVISION

DENVILLE, NEW JERSEY

Thiokol® CHEMICAL CORPORATION

DS 100-134

REPORT NUMBER

CLASS U

TITLE THERMAL ANALYSIS OF THE JPL OF₂/DB THRUST CHAMBER

REPORT PREPARED BY

S. Elkind

10/24/68
(DATE)

REPORT CHECKED BY

J. J. Lovingham

10/24/68
(DATE)

REPORT APPROVED BY

(DATE)

W.O. 6062-11-2000

THIS REPORT INCLUDES 5 PAGES, 3 FIGURES, AND DRAWINGS.

cc: R. W. Seaman
W. Hosek
G. Rabe
C. Nash
R. Novotny

LIBRARY
File: Proj. 6062
W. Monagle

REVISIONS AND ADDITIONS

LETTER	DATE	DESCRIPTION	BY	CHECKED	APPROVED

Thiokol® CHEMICAL CORPORATION

REACTION MOTORS DIVISION

DENVILLE, NEW JERSEY

Design Report

Page i

TITLE: THERMAL ANALYSIS OF THE JPL OF₂/DB THRUST CHAMBER

REPORT NO. DS 100-134

TABLE OF CONTENTS

	<u>Page</u>
ABSTRACT	1
INTRODUCTION	2
DISCUSSION	2
METHOD OF ANALYSIS	3
RESULTS	4
APPENDIX A - DATA USED	5
APPENDIX B - TEMPERATURE - TIME DATA	

Thiokol • CHEMICAL CORPORATION
REACTION MOTORS DIVISION
DENVER, NEW JERSEY

Design Report

Page ii

TITLE: THERMAL ANALYSIS OF THE JPL OF₂/DB THRUST CHAMBER

REPORT NO. DS 100-134

LIST OF FIGURES

Figure

- 1 JPL OF₂/DB Thrust Chamber
- 2 Division of Chamber into Nodes, and Nodal Temperatures
after 1000 Seconds
- 3 Typical Nodal Transient Temperatures

Thiokol CHEMICAL CORPORATION
REACTION MOTORS DIVISION
DENVILLE, NEW JERSEY

Design Report

Page 1

TITLE: THERMAL ANALYSIS OF THE JPL OF₂/DB THRUST CHAMBER

REPORT NO. DS 100-134

ABSTRACT

A Thermal Model was made of the JPL OF₂/DB Thrust Chamber, and nodal temperatures computed, Figure 2. Component temperatures are within material capabilities and JPL thermal requirements are met.

Thiokol® CHEMICAL CORPORATION

REACTION MOTORS DIVISION

DENVILLE, NEW JERSEY

Design Report

Page 2

TITLE: THERMAL ANALYSIS OF THE JPL OF₂/DB THRUST CHAMBER

REPORT NO. DS 100-134

INTRODUCTION

Thiokol-RMD has designed a thrust chamber for JPL to be used with their OF₂/DB barrier cooled injector. Under WA-6062-11-2000, a study was made to determine whether the RMD design meets JPL's thermal requirements.

DISCUSSION

The JPL OF₂/DB thrust chamber, Figure 1, consists of:

1. An ATJS graphite liner;
2. Pyrolytic graphite wedges with the "a - b" planes in the radial and axial directions;
3. A "Grafoil" foam or "Grafoam" cylinder;
4. A pyrolytic cylinder with the "c" direction radial;
5. A columbium structural shell; and
6. Dyna-quartz insulation held in place by a columbium foil shell.

A silica phenolic block insulates the upstream injector housing from the rest of the chamber.

Operating conditions are:

Propellants	OF ₂ /DB
Chamber Pressure	100 psia
Propellant Flow Rate	.512 pps
Firing Duration	1000 sec
Chamber Gas Film Temperature	4000°F
Nozzle Gas Film Temperature	7000°F
Maximum Skin Temperature	600°F

TITLE: THERMAL ANALYSIS OF THE JPL OF₂/DB THRUST CHAMBER

REPORT NO. DS 100-134

METHOD OF ANALYSIS

Component temperatures throughout the OF₂/DB thrust chamber were determined by means of a finite difference numerical analysis. In brief, the method consists of dividing the chamber into regular geometric volumes, and assuming each volume shrinks to a point, or node. Each node is assumed to retain the thermal characteristics of the volume it represents. Heat balance equations are written for each node, resulting in a set of "n" simultaneous equations for "n" nodes. When forward differences (in time) are used, these equations are explicit in nodal temperatures and easily solved on a digital computer. The procedure is repeated for a finite time period, $\Delta \theta$, later and in this way temperature distributions are computed at time 0, $\Delta \theta$, $2\Delta \theta$, ... $m\Delta \theta$. The time step, $\Delta \theta$, depends on: (1) the component material properties; (2) the division into nodes; and (3) the modes of heat transfer considered. It is also subject to a stability criteria, to insure a stable numerical solution.

The proposed OF₂/DB chamber was divided into 96 nodes as indicated in Figure 2. The nodes have been chosen to obtain a good simulation of the problem, e.g., nodes in the converging section 11, 12, and 13, are closer together than in the chamber 8, 9, and 10. Also, nodes in the pyrolytic cylinder, e.g., 31, 38, 45, and 52, are spaced closer than other nodes to allow better simulation of the anisotropic thermal conductivity of the material. A time step, $\Delta \theta$ of one second was used.

Thiokol • CHEMICAL CORPORATION

REACTION MOTORS DIVISION

DENVILLE, NEW JERSEY

Design Report

Page 4

TITLE: THERMAL ANALYSIS OF THE JPL OF₂/DB THRUST CHAMBER

REPORT NO. DS 100-134

RESULTS

Calculated nodal temperatures after a 1000 second firing are presented in Figure 1. The temperature near the throat, Node 13, is 6102F, while the highest combustion chamber node, 10, is 4359F. These temperatures are well within the capability of the ATJS material.

Typical nodes in the pyrolytic cylinder, 34, 41, 48 and 55, attain 4973F, 3295F, 2397F, and 2014F, respectively. This material functions as a high temperature insulator, with a 2900F drop in the "c" direction.

The fibrous insulation, dyna-quartz, drops the temperature from 2014F at Node 55 to 517F at Node 76. All the shell nodes, 71-77, are below the specified maximum of 600°F.

The highest temperature in the columbium structure, 2536F occurs at Node 50. This can be tolerated by columbium. It should be noted that conduction along the columbium was neglected in order to be able to use a time step of one second. In the flight design it may be necessary to insulate the outer flange of the columbium shell to limit the skin temperature to 600F.

The upstream housing that mates to JPL's injector is represented by Nodes 96, 94, and 95. They reach 1674F, 198F, and 169F respectively. While 1674F may be high at Node 96, this analysis does not include the added thermal mass of the injector and any cooling effects due to propellant flow. Very little heat rejection in this area results in tremendous temperature reduction. For example, in a preliminary analysis, neglect of the housing heat capacity resulted in a temperature of 2700F at Node 96. Thus, the addition of the heat capacity dropped the node almost 1100F.

Typical nodal transient temperatures are indicated in Figure 3. Node 13 near the throat is approaching its steady state value, as evidenced by the decrease in slope. Node 11 is not as close to steady state. Due to its large thermal inertia, the thrust chamber is still in a transient after a 1000 second firing.

The JPL OF₂/DB thrust chamber design, Drawing 318281, meets all JPL thermal requirements and is adequate for its application.

Appendix B is a tabulation of the calculated Nodal temperature from start to 1000 seconds.

Thiokol CHEMICAL CORPORATION

REACTION MOTORS DIVISION

DENVILLE, NEW JERSEY

Design Report

Page 5

TITLE: THERMAL ANALYSIS OF THE JPL OF₂/DB THRUST CHAMBER

REPORT NO. DS 100-134

APPENDIX A

DATA USED IN ANALYSIS

- A. Gas convection coefficients were computed by a modified Colburn equation. The resulting coefficients are:

Node	Diameter, inches	hg, BTU/°F.- HR-FT ²
8, 9, 10	2.60	92
11	2.30	115
12	1.70	198
13, 14	1.20	371

- B. Material Properties

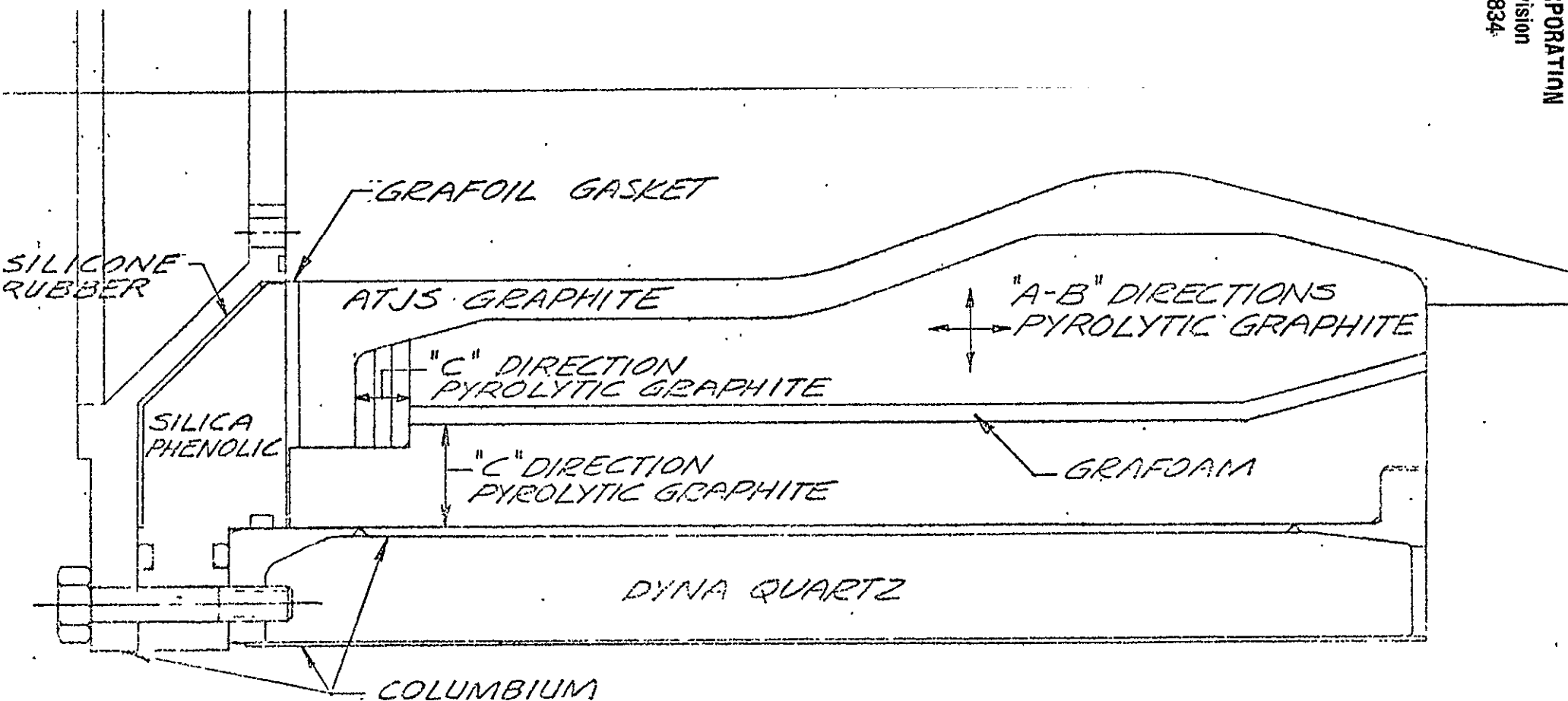
Material	$\bar{T}$	k	ρ	C_p
ATJS	4000	25	114	.50
PYRO "a-b"	4000	40	137	.45
"c"	4000	.5	137	.45
Dyna-Quartz	1800	.085	16	.29
Silica Phenolic	500	.14	108	.30

k = Thermal Conductivity
BTU/HR-FT² - Degree

ρ = Density, lbs per cu. ft.

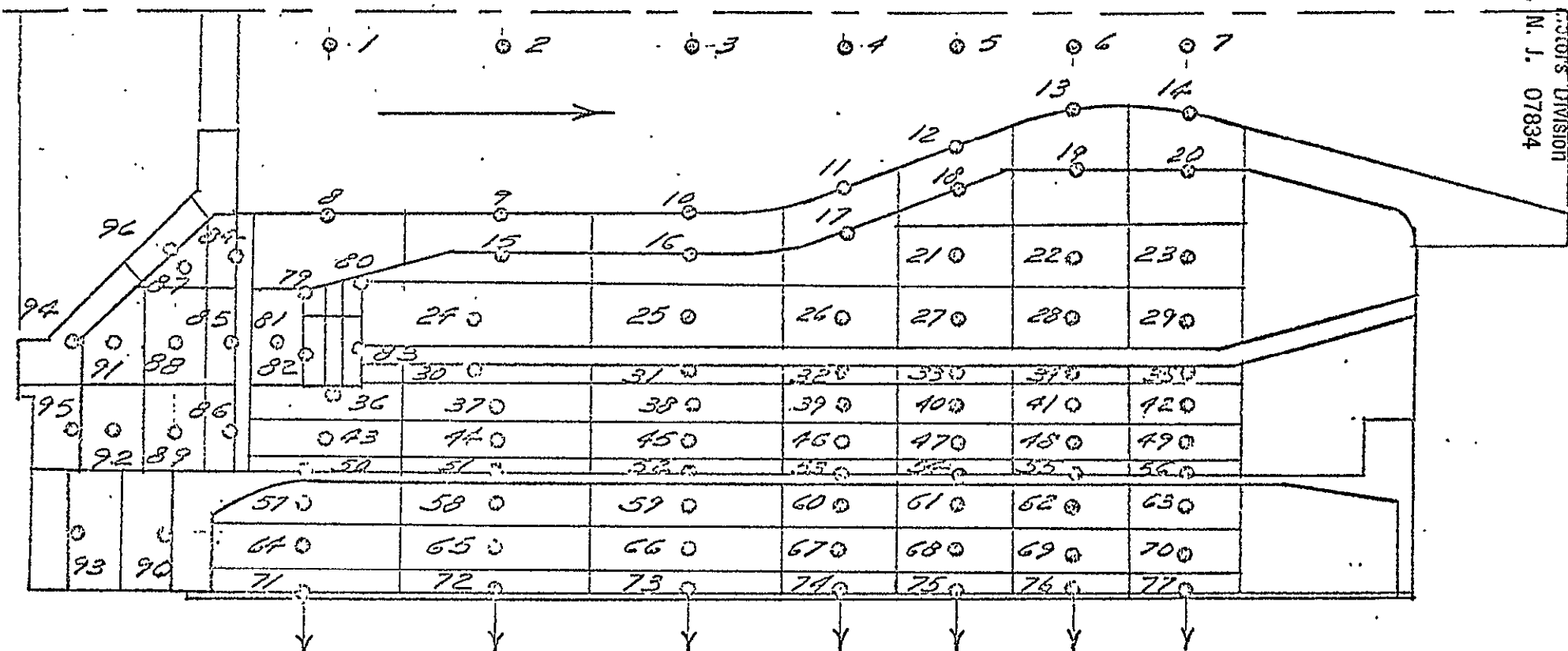
C_p = Specific Heat, BTU/lb - degree

$\bar{T}$ = Average Temperature - °F



JPL OF₂/DB THRUST CHAMBER

FIGURE 1



TIME = 1000.0 SEC ⑦ 78

	1	2	3	4	5	6	7	8	9	10
0	4000.0	4000.0	4000.0	7000.0	7000.0	7000.0	7000.0	3515.9	3800.3	4359.0
10	5178.5	5722.0	6102.4	6184.6	3785.8	4357.6	5017.3	5521.2	5733.8	5826.6
20	5337.8	5520.4	5613.1	3764.5	4347.1	4906.3	5235.0	5427.0	5520.3	3648.9
30	4144.3	4550.7	4804.7	4972.9	5056.2	3105.1	3073.6	3128.2	3201.6	3254.6
40	3295.1	3317.0	2742.8	2567.6	2461.1	2419.3	2402.5	2396.7	2398.5	2535.6
50	2274.2	2112.6	2043.9	2016.9	2014.0	2036.8	1605.7	1528.5	1407.9	1352.3
60	1329.2	1325.6	1333.1	982.8	971.5	896.3	859.5	844.0	843.8	842.3
70	562.8	562.3	532.6	517.2	510.7	516.6	509.5	100.0	3234.6	3549.8
80	3193.6	3172.4	3363.9	3484.6	3140.1	2819.7	1970.4	1259.0	1011.2	292.6
90	382.5	308.3	150.4	198.3	168.5	1673.8				

DIVISION OF CHAMBER INTO NODES, AND
NODAL TEMPERATURES AFTER 1000 SEC.

FIGURE 2

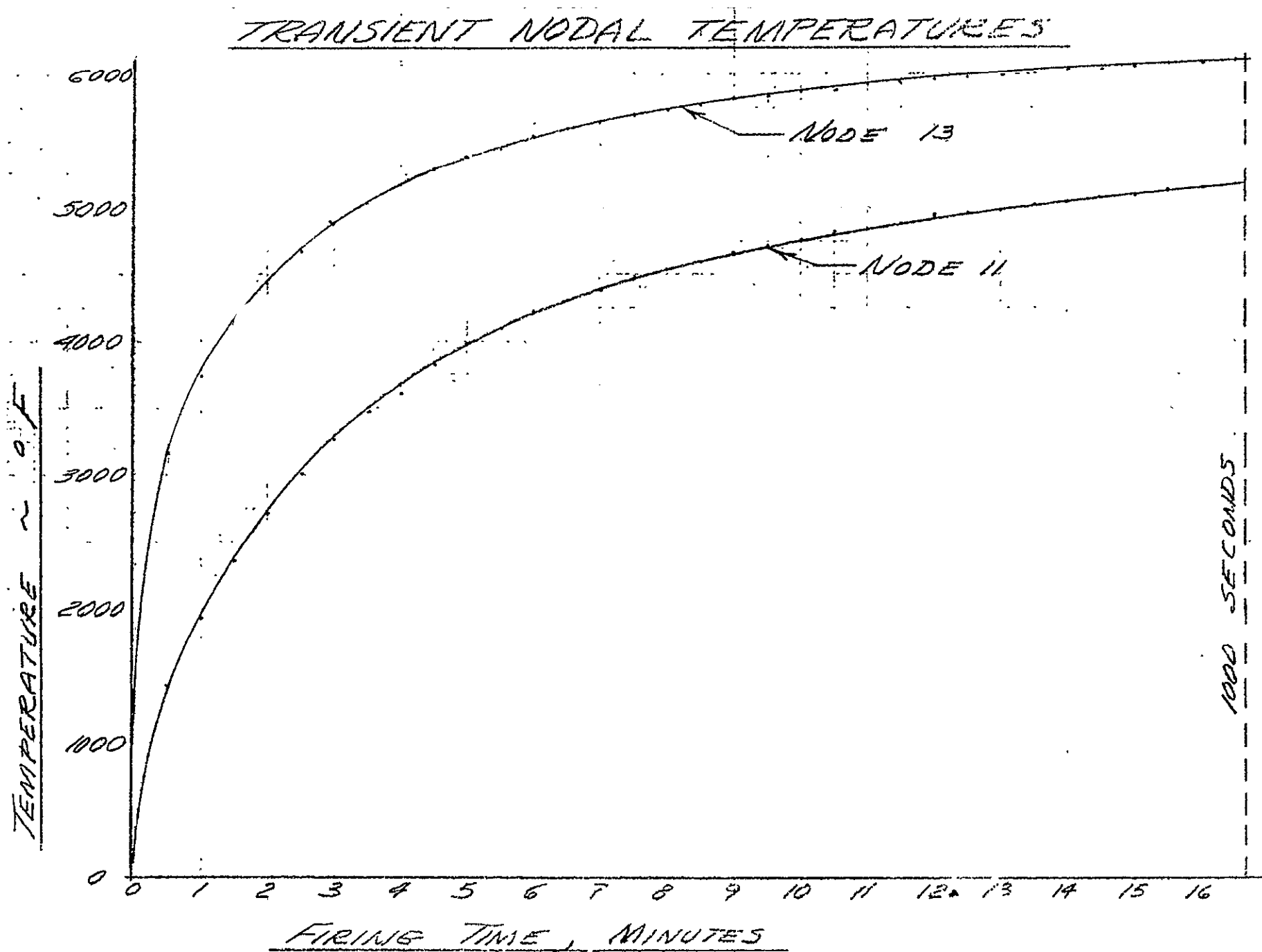


FIG. 3

CALC TIME = 1.0 SEC, PRINTOUT = 30.0 SEC, TOTAL RUN=1000.0
 NO OF ITERATIONS = 0

APPENDIX B

TIME = 30.0 SEC

	1	2	3	4	5	6	7	8	9	10
0	4000.0	4000.0	4000.0	7000.0	7000.0	7000.0	7000.0	779.9	560.8	638.3
10	1412.9	2247.8	3167.9	3277.5	446.4	513.9	925.6	1523.4	1726.0	1783.4
20	974.0	967.8	977.9	357.2	419.6	633.6	713.1	709.4	708.6	202.9
30	218.0	277.7	296.2	290.8	286.3	198.1	117.5	105.2	105.4	105.6
40	105.2	105.0	114.3	101.7	100.2	100.2	100.3	100.7	101.6	106.7
50	100.6	100.1	100.3	101.1	103.6	109.8	100.3	100.0	100.0	100.0
60	100.1	100.4	101.3	100.0	100.0	100.0	100.0	100.0	100.0	100.1
70	100.0	100.0	100.0	100.0	100.0	100.0	100.0	100.0	343.2	393.8
80	287.4	261.4	256.7	703.1	220.4	134.9	127.9	101.3	100.3	100.0
90	100.0	100.0	100.0	100.0	100.0	101.4				

TIME = 60.0 SEC

	1	2	3	4	5	6	7	8	9	10
0	4000.0	4000.0	4000.0	7000.0	7000.0	7000.0	7000.0	1057.8	854.0	1030.2
10	1928.5	2838.5	3741.4	3873.0	743.8	916.4	1478.1	2192.0	2468.0	2564.0
20	1678.4	1771.2	1827.1	652.3	825.4	1200.5	1419.5	1513.5	1558.7	440.1
30	529.9	702.7	807.8	862.0	884.9	354.4	189.3	145.0	145.6	149.3
40	151.9	153.0	176.0	119.3	105.2	103.4	103.5	104.2	105.4	144.3
50	109.4	102.0	101.9	103.5	107.3	114.6	105.4	100.9	100.2	100.2
60	100.6	101.5	103.4	100.5	100.1	100.0	100.0	100.1	100.2	100.6
70	100.1	100.0	100.0	100.0	100.0	100.0	100.1	100.0	551.1	653.5
80	483.9	448.9	467.4	1005.6	418.1	224.3	185.8	108.7	102.7	100.0
90	100.1	100.0	100.0	100.0	100.0	110.1				

TIME = 90.0 SEC

	1	2	3	4	5	6	7	8	9	10
0	4000.0	4000.0	4000.0	7000.0	7000.0	7000.0	7000.0	1255.0	1117.2	1391.9
10	2350.9	3273.0	4129.7	4268.0	1013.7	1289.4	1935.7	2692.3	2997.8	3114.0
20	2220.2	2371.7	2457.3	924.7	1205.2	1678.3	1977.1	2132.8	2210.0	692.9
30	874.5	1138.3	1313.5	1422.9	1475.6	505.7	294.0	225.9	228.3	237.8
40	246.4	251.2	260.1	157.4	122.0	115.1	114.1	114.8	116.2	204.3
50	131.9	109.6	106.2	107.3	111.4	119.0	119.1	105.0	101.3	101.0
60	101.5	103.0	105.7	102.8	100.6	100.1	100.1	100.3	100.6	101.3
70	100.6	100.1	100.0	100.0	100.1	100.0	100.4	100.0	723.8	881.6
80	652.3	613.7	666.4	1208.0	590.5	327.8	247.3	121.9	108.1	100.1
90	100.6	100.2	100.0	100.0	100.0	127.0				

TIME = 120.0 SEC

	1	2	3	4	5	6	7	8	9	10
0	4000.0	4000.0	4000.0	7000.0	7000.0	7000.0	7000.0	1424.7	1356.9	1716.2
10	2706.9	3619.9	4429.6	4569.1	1260.1	1624.1	2322.2	3092.5	3410.1	3536.5
20	2656.4	2842.3	2944.8	1174.6	1546.8	2082.8	2428.8	2620.9	2717.1	934.4
30	1199.0	1527.0	1748.5	1894.2	1966.6	651.9	416.3	336.3	342.4	357.7
40	372.4	380.9	353.8	211.7	153.3	139.1	135.7	135.8	137.1	276.4
50	167.0	125.3	115.7	114.7	118.0	125.5	141.5	114.0	104.6	103.0
60	103.3	105.0	108.3	108.0	102.4	100.7	100.5	100.7	101.2	102.3
70	102.4	100.7	100.2	100.1	100.2	100.2	100.9	100.0	880.9	1090.2
80	807.1	766.8	853.5	1379.1	746.0	436.2	308.3	139.8	116.6	100.3
90	101.5	100.6	100.0	100.1	100.0	150.9				

TIME = 150.0 SEC										
1	2	3	4	5	6	7	8	9	10	
0	4000.0	4000.0	4000.0	7000.0	7000.0	7000.0	7000.0	1579.9	1574.9	2002.4
10	3008.4	3903.2	4669.1	4806.9	1484.5	1919.5	2649.7	3419.4	3740.2	3871.2
20	3013.9	3220.0	3332.1	1402.8	1848.4	2425.7	2799.8	3013.5	3120.7	1158.9
30	1491.7	1863.9	2115.3	2283.7	2368.2	794.3	548.2	464.7	475.5	496.0
40	515.7	527.2	452.9	278.1	198.3	176.0	169.4	168.2	169.2	355.9
50	212.4	149.7	132.2	127.7	129.4	136.4	171.3	128.4	111.0	107.1
60	106.7	108.3	111.9	116.9	106.1	102.1	101.4	101.5	102.2	103.7
70	106.1	102.1	100.6	100.4	100.5	100.5	101.7	100.0	1029.5	1282.8
80	954.3	913.0	1029.8	1534.6	892.6	547.0	368.9	161.7	128.1	100.8
90	102.9	101.2	100.0	100.1	100.1	180.7				

TIME = 180.0 SEC										
1	2	3	4	5	6	7	8	9	10	
0	4000.0	4000.0	4000.0	7000.0	7000.0	7000.0	7000.0	1723.9	1772.7	2253.1
10	3264.6	4137.4	4863.8	4998.7	1688.1	2178.3	2928.1	3689.7	4009.0	4141.6
20	3310.2	3528.1	3645.3	1610.1	2112.8	2717.1	3107.8	3334.3	3447.7	1365.5
30	1752.2	2154.9	2425.4	2608.0	2699.9	932.7	684.6	602.7	618.3	643.2
40	666.7	680.4	555.6	354.0	255.3	224.9	214.8	211.8	212.1	440.6
50	266.1	182.9	156.4	147.7	147.2	153.4	207.3	148.5	121.5	114.1
60	112.4	113.6	117.2	129.6	112.3	104.9	103.2	103.0	103.7	105.5
70	112.2	104.8	101.7	101.1	101.2	101.2	102.6	100.0	1171.4	1460.8
80	1095.5	1053.8	1195.6	1678.9	1033.1	659.0	429.3	187.0	142.4	101.5
90	104.9	102.2	100.1	100.3	100.1	215.4				

TIME = 210.0 SEC										
1	2	3	4	5	6	7	8	9	10	
0	4000.0	4000.0	4000.0	7000.0	7000.0	7000.0	7000.0	1858.1	1951.7	2472.5
10	3483.2	4333.0	5024.2	5155.7	1872.7	2404.9	3165.8	3915.5	4230.9	4363.2
20	3558.1	3782.7	3902.4	1798.3	2344.3	2965.8	3366.0	3599.7	3716.4	1554.9
30	1983.3	2406.8	2689.5	2880.7	2977.0	1066.7	821.9	744.5	764.7	793.2
40	819.6	834.9	660.3	437.2	322.2	284.3	270.5	265.5	265.0	528.9
50	326.9	224.3	188.5	175.3	172.2	177.4	248.4	173.9	136.3	124.7
60	121.3	121.7	125.2	146.2	121.5	109.5	106.3	105.6	106.2	108.2
70	120.9	109.2	103.8	102.5	102.3	102.5	104.0	100.0	1307.0	1625.1
80	1230.9	1189.1	1351.3	1813.3	1168.0	771.1	490.0	215.4	159.5	102.6
90	107.5	103.6	100.1	100.5	100.2	254.2				

TIME = 240.0 SEC										
1	2	3	4	5	6	7	8	9	10	
0	4000.0	4000.0	4000.0	7000.0	7000.0	7000.0	7000.0	1983.0	2113.7	2664.8
10	3670.8	4497.9	5157.9	5285.9	2039.8	2603.5	3370.0	4105.8	4416.0	4547.1
20	3767.5	3995.3	4116.0	1968.8	2547.4	3179.5	3584.3	3821.7	3939.9	1728.2
30	2188.4	2626.0	2916.2	3112.6	3211.4	1195.8	957.8	886.3	910.7	942.0
40	970.5	987.1	766.0	525.7	397.1	352.3	335.1	328.0	326.7	619.8
50	393.6	273.1	228.4	210.6	204.8	209.0	293.8	204.4	155.7	139.4
60	133.9	133.2	136.4	166.4	133.7	116.3	111.1	109.7	110.1	112.1
70	132.3	115.8	107.1	104.8	104.3	104.8	106.0	100.0	1436.2	1776.6
80	1360.3	1318.6	1497.1	1938.6	1297.2	882.2	550.9	246.4	179.0	104.0
90	110.8	105.4	100.2	100.9	100.4	296.4				

TIME = 270.0 SEC										
1	2	3	4	5	6	7	8	9	10	
0	4000.0	4000.0	4000.0	7000.0	7000.0	7000.0	7000.0	2099.2	2260.5	2833.9

10	3832.9	4638.2	5270.5	5395.1	2191.2	2778.2	3546.5	4267.7	4572.2	4701.5
20	3945.9	4174.9	4295.5	2123.5	2726.1	3364.2	3770.5	4009.3	4128.1	1886.7
30	2371.1	2817.8	3112.3	3311.5	3411.7	1319.7	1090.5	1025.6	1053.8	1087.3
40	1117.5	1134.9	871.6	618.1	478.3	427.5	407.0	398.0	395.8	712.2
50	465.1	328.6	275.5	253.2	244.9	248.2	342.7	239.6	179.7	158.5
60	150.5	148.6	151.5	190.0	149.3	125.6	118.1	115.7	115.8	117.6
70	146.1	124.5	112.0	108.3	107.3	108.2	108.9	100.0	1558.9	1916.3
80	1483.7	1442.3	1633.5	2055.2	1420.5	991.8	612.1	279.8	200.9	105.9
90	114.8	107.7	100.4	101.4	100.7	341.7				

TIME = 300.0 SEC

	1	2	3	4	5	6	7	8	9	10
0	4000.0	4000.0	4000.0	7000.0	7000.0	7000.0	7000.0	2207.3	2393.6	2983.3
10	3973.8	4758.5	5366.3	5487.5	2328.6	2932.5	3700.0	4406.6	4705.1	4832.5
20	4099.1	4327.9	4447.9	2264.1	2884.1	3524.8	3930.6	4169.5	4287.9	2031.9
30	2534.2	2986.7	3283.4	3483.8	3584.5	1438.1	1219.0	1161.0	1192.5	1227.8
40	1259.2	1277.2	976.3	712.9	564.1	508.1	484.7	473.9	470.9	805.4
50	540.5	389.9	329.1	302.7	291.9	294.4	394.6	279.0	208.3	181.9
60	171.5	168.2	170.6	216.7	168.2	137.8	127.4	123.8	123.6	125.1
70	162.3	135.7	118.8	113.3	111.6	113.2	113.0	100.0	1675.2	2045.2
80	1600.9	1560.0	1761.0	2163.8	1537.8	1099.1	673.5	315.1	225.0	108.2
90	119.5	110.5	100.6	102.1	101.0	389.5				

TIME = 330.0 SEC

	1	2	3	4	5	6	7	8	9	10
0	4000.0	4000.0	4000.0	7000.0	7000.0	7000.0	7000.0	2307.9	2514.6	3115.8
10	4097.2	4862.5	5448.5	5566.5	2453.6	3069.6	3834.4	4526.8	4819.3	4944.5
20	4231.8	4459.5	4578.5	2392.1	3024.4	3665.5	4069.4	4307.3	4425.0	2165.0
30	2680.6	3136.2	3433.6	3634.2	3734.9	1551.1	1342.7	1291.6	1326.1	1362.9
40	1395.2	1413.6	1079.4	809.1	653.3	592.9	567.1	554.7	551.0	898.5
50	618.9	456.1	388.4	358.4	345.4	347.3	448.8	322.4	241.2	209.7
60	196.7	192.2	194.0	246.1	190.4	152.9	139.4	134.4	133.9	134.9
70	180.4	149.1	127.5	120.1	117.5	119.9	118.5	100.0	1785.3	2164.3
80	1712.1	1671.8	1880.3	2264.9	1649.3	1203.8	734.9	352.0	250.9	111.1
90	124.9	113.8	100.9	102.9	101.5	439.5				

TIME = 360.0 SEC

	1	2	3	4	5	6	7	8	9	10
0	4000.0	4000.0	4000.0	7000.0	7000.0	7000.0	7000.0	2401.5	2624.9	3234.1
10	4205.8	4953.1	5519.6	5634.7	2567.6	3191.9	3952.9	4631.5	4918.3	5041.3
20	4347.6	4573.6	4691.3	2509.0	3149.6	3789.6	4190.7	4427.0	4543.7	2287.3
30	2812.5	3269.5	3566.5	3766.6	3866.8	1658.8	1461.3	1417.0	1454.2	1492.2
40	1525.1	1543.8	1180.5	905.8	744.7	680.8	652.8	639.1	634.8	991.2
50	699.5	526.3	452.7	419.4	404.6	406.1	504.7	369.1	278.1	241.7
60	226.2	220.4	221.7	277.8	215.6	171.0	154.3	147.8	146.9	147.2
70	200.2	164.8	138.4	128.7	125.3	128.4	125.6	100.0	1889.5	2274.6
80	1817.5	1778.0	1991.9	2359.1	1755.1	1180.5	796.2	390.4	278.5	114.4
90	131.0	117.7	101.3	104.0	102.1	491.2				

TIME = 390.0 SEC

	1	2	3	4	5	6	7	8	9	10
0	4000.0	4000.0	4000.0	7000.0	7000.0	7000.0	7000.0	2488.8	2725.9	3340.1
10	4302.2	5032.7	5581.7	5694.0	2672.0	3301.6	4058.0	4723.4	5004.6	5125.5
20	4449.3	4673.4	4789.7	2616.0	3262.0	3899.7	4297.4	4531.6	4647.2	2400.0
30	2931.9	3389.0	3684.9	3883.9	3983.6	1761.3	1574.8	1537.0	1576.7	1615.7
40	1649.2	1668.1	1279.3	1002.2	837.4	770.7	741.1	726.2	721.5	1082.8
50	781.5	599.9	521.2	485.2	468.7	470.1	562.0	418.8	318.8	277.6

60	259.7	252.8	253.6	311.4	243.7	192.1	172.0	163.9	162.7	162.3
70	221.2	182.5	151.4	139.4	134.9	138.9	134.5	100.0	1988.0	2376.8
80	1917.5	1878.7	2096.5	2447.0	1855.4	1404.1	857.3	429.8	307.6	118.3
90	137.8	122.1	101.8	105.2	102.8	544.5				

TIME = 420.0 SEC

	1	2	3	4	5	6	7	8	9	10
0	4000.0	4000.0	4000.0	7000.0	7000.0	7000.0	7000.0	2570.4	2818.6	3435.7
10	4388.1	5103.0	5636.2	5746.0	2767.8	3400.4	4151.9	4804.7	5080.6	5199.4
20	4539.4	4761.2	4876.0	2714.4	3363.4	3997.9	4391.9	4623.9	4738.2	2504.2
30	3040.4	3496.7	3791.0	3988.7	4087.6	1859.0	1683.1	1651.8	1693.7	1733.5
40	1767.5	1786.6	1375.5	1097.9	930.7	861.9	831.0	815.3	810.2	1173.1
50	864.5	675.9	593.1	554.7	537.1	538.5	620.1	471.1	362.8	317.2
60	297.1	289.2	289.4	346.6	274.4	216.0	192.5	182.9	181.4	180.1
70	243.0	201.9	166.3	152.1	146.6	151.4	145.4	100.0	2081.3	2471.8
80	2012.2	1974.2	2194.7	2529.1	1950.6	1499.6	918.1	470.2	338.1	122.7
90	145.2	127.0	102.4	106.8	103.7	599.0				

TIME = 450.0 SEC

	1	2	3	4	5	6	7	8	9	10
0	4000.0	4000.0	4000.0	7000.0	7000.0	7000.0	7000.0	2646.8	2903.9	3522.2
10	4465.2	5165.6	5684.5	5791.9	2856.1	3490.0	4236.1	4877.1	5147.9	5264.8
20	4619.7	4839.1	4952.4	2805.2	3455.2	4086.2	4476.2	4705.8	4818.8	2600.8
30	3139.6	3594.4	3886.8	4082.9	4180.9	1952.0	1786.6	1761.3	1805.3	1846.0
40	1880.3	1899.6	1469.0	1192.3	1023.9	953.7	921.9	905.5	900.2	1261.8
50	947.9	753.9	667.7	627.5	609.0	610.6	678.7	525.4	409.8	360.2
60	338.1	329.2	329.1	382.9	307.4	242.7	215.9	204.7	203.1	200.8
70	265.2	222.8	183.2	166.7	160.2	165.9	158.2	100.0	2169.6	2560.4
80	2102.1	2065.0	2287.0	2606.0	2040.9	1591.9	978.6	511.3	369.7	127.6
90	153.3	132.5	103.2	108.6	104.8	654.5				

TIME = 480.0 SEC

	1	2	3	4	5	6	7	8	9	10
0	4000.0	4000.0	4000.0	7000.0	7000.0	7000.0	7000.0	2718.4	2982.8	3601.0
10	4534.8	5221.7	5727.5	5832.7	2937.8	3571.6	4312.1	4941.9	5208.0	5322.9
20	4691.6	4908.6	5020.5	2889.1	3538.9	4165.9	4551.9	4779.1	4890.7	2690.6
30	3230.6	3683.4	3973.6	4168.1	4265.1	2040.6	1885.4	1866.0	1911.9	1953.4
40	1988.0	2007.3	1559.7	1285.1	1116.6	1045.6	1013.1	996.3	990.9	1348.8
50	1031.2	833.2	744.3	702.8	683.7	685.7	737.4	581.3	459.4	406.2
60	382.2	372.7	372.1	419.9	342.4	271.9	242.0	229.3	227.5	224.3
70	287.5	244.7	201.7	183.2	175.7	182.2	172.8	100.0	2253.3	2643.2
80	2187.4	2151.2	2373.9	2678.2	2126.7	1681.0	1038.5	553.0	402.3	133.1
90	162.0	138.5	104.0	110.6	106.1	710.7				

TIME = 510.0 SEC

	1	2	3	4	5	6	7	8	9	10
0	4000.0	4000.0	4000.0	7000.0	7000.0	7000.0	7000.0	2785.8	3056.0	3673.0
10	4598.0	5272.2	5766.1	5869.3	3013.6	3646.2	4381.2	5000.4	5261.9	5375.0
20	4756.6	4971.1	5081.5	2967.1	3615.5	4238.3	4620.3	4844.9	4955.2	2774.4
30	3314.5	3764.9	4052.8	4245.6	4341.7	2125.1	1979.7	1965.9	2013.7	2055.9
40	2090.8	2110.3	1647.7	1376.2	1208.3	1137.0	1104.3	1087.3	1081.8	1433.8
50	1114.0	913.3	822.5	780.1	760.6	763.2	796.0	638.6	511.1	454.8
60	429.3	419.2	418.3	457.4	379.0	303.4	270.6	256.4	254.5	250.4
70	309.7	267.3	221.5	201.2	192.9	200.2	189.3	100.0	2332.8	2720.8
80	2268.5	2233.2	2456.0	2746.1	2208.2	1767.0	1098.0	595.0	435.7	139.1
90	171.2	145.0	105.1	113.0	107.6	767.5				

TIME = 540.0 SEC

	1	2	3	4	5	6	7	8	9	10
0	4000.0	4000.0	4000.0	7000.0	7000.0	7000.0	7000.0	2849.2	3124.1	3739.2
10	4655.6	5318.1	5801.0	5902.2	3084.1	3714.7	4444.2	5053.4	5310.7	5422.0
20	4815.5	5027.6	5136.6	3039.8	3685.9	4304.4	4682.4	4904.6	5013.5	2852.7
30	3392.1	3839.8	4125.5	4316.5	4411.6	2205.8	2069.7	2061.4	2111.0	2153.9
40	2189.1	2208.6	1732.8	1465.3	1298.9	1227.8	1195.0	1177.9	1172.6	1516.7
50	1196.2	993.8	901.8	858.7	839.2	842.5	854.1	696.8	564.8	505.7
60	478.8	468.3	467.2	495.0	416.8	336.8	301.4	286.0	284.0	279.1
70	331.4	290.3	242.5	220.7	211.6	219.5	207.4	100.0	2408.4	2793.7
80	2345.6	2311.4	2533.6	2810.1	2285.9	1849.9	1156.9	637.2	469.8	145.5
90	181.0	152.0	106.3	115.7	109.3	824.7				

TIME = 570.0 SEC

	1	2	3	4	5	6	7	8	9	10
0	4000.0	4000.0	4000.0	7000.0	7000.0	7000.0	7000.0	2909.1	3187.7	3800.3
10	4708.4	5359.8	5832.6	5932.1	3150.0	3778.0	4502.0	5101.7	5354.9	5464.6
20	4869.3	5079.0	5186.6	3107.6	3750.9	4365.0	4739.0	4958.8	5066.5	2926.2
30	3464.2	3909.2	4192.4	4381.6	4475.9	2282.9	2155.9	2152.7	2204.1	2247.6
40	2283.1	2302.8	1815.3	1552.3	1388.0	1317.4	1284.8	1267.9	1262.7	1597.6
50	1277.4	1074.3	981.6	938.3	919.0	923.1	911.6	755.5	619.8	558.5
60	530.5	519.8	518.5	532.5	455.6	371.9	334.2	317.7	315.7	310.0
70	352.5	313.3	264.2	241.2	231.5	240.0	226.8	100.0	2480.4	2862.3
80	2419.2	2385.8	2607.2	2870.6	2359.9	1930.0	1215.2	679.5	504.4	152.5
90	191.4	159.5	107.7	118.6	111.3	882.1				

TIME = 600.0 SEC

	1	2	3	4	5	6	7	8	9	10
0	4000.0	4000.0	4000.0	7000.0	7000.0	7000.0	7000.0	2965.8	3247.2	3856.9
10	4757.1	5398.1	5861.5	5959.3	3211.8	3836.7	4555.3	5146.0	5395.4	5503.5
20	4918.6	5126.0	5232.3	3171.3	3811.1	4420.9	4791.1	5008.5	5114.9	2995.3
30	3531.4	3973.5	4254.4	4441.9	4535.2	2356.7	2238.2	2240.1	2293.2	2337.4
40	2373.2	2393.0	1895.1	1637.2	1475.5	1405.9	1373.7	1357.0	1352.1	1676.4
50	1357.5	1154.4	1061.6	1018.3	999.5	1004.5	968.3	814.4	676.0	612.9
60	584.1	573.3	571.9	569.6	494.8	408.3	368.6	351.2	349.2	343.0
70	372.8	336.0	286.3	262.6	252.4	261.3	247.3	100.0	2548.9	2927.1
80	2489.4	2457.0	2677.0	2927.8	2430.5	2007.3	1272.9	721.9	539.5	159.9
90	202.2	167.5	109.2	121.9	113.4	939.6				

TIME = 630.0 SEC

	1	2	3	4	5	6	7	8	9	10
0	4000.0	4000.0	4000.0	7000.0	7000.0	7000.0	7000.0	3019.6	3303.2	3909.6
10	4802.2	5433.3	5888.0	5984.2	3269.8	3891.3	4604.6	5186.8	5432.6	5539.1
20	4964.1	5169.2	5274.2	3231.1	3867.2	4472.6	4839.1	5054.1	5159.3	3060.5
30	3594.3	4033.5	4312.1	4497.8	4590.2	2427.3	2317.1	2323.8	2378.6	2423.5
40	2459.6	2479.5	1972.3	1719.9	1561.3	1492.8	1461.2	1445.0	1440.4	1753.1
50	1436.3	1234.1	1141.6	1098.6	1080.3	1086.4	1023.9	873.3	733.0	668.5
60	639.1	628.3	627.1	606.1	534.4	445.7	404.5	386.3	384.4	377.7
70	392.2	358.2	308.6	284.4	274.0	283.1	268.6	100.0	2614.4	2988.5
80	2556.4	2524.9	2743.4	2982.1	2497.9	2081.9	1329.9	764.2	575.0	167.8
90	213.6	175.9	111.0	125.6	115.9	997.0				

TIME = 660.0 SEC

	1	2	3	4	5	6	7	8	9	10
0	4000.0	4000.0	4000.0	7000.0	7000.0	7000.0	7000.0	3070.7	3355.9	3958.7
10	4844.0	5465.9	5912.5	6007.2	3324.4	3942.2	4650.5	5224.5	5466.8	5572.0

20	5006.1	5209.0	5312.9	3287.5	3919.6	4520.7	4883.5	5096.3	5200.4	3122.1
30	3653.3	4089.6	4365.9	4549.9	4641.4	2495.1	2392.8	2404.1	2460.6	2506.1
40	2542.5	2562.5	2046.9	1800.4	1645.2	1578.2	1547.4	1531.7	1527.4	1827.7
50	1513.6	1312.9	1221.1	1178.6	1161.1	1168.4	1078.5	932.0	790.5	725.0
60	695.2	684.6	683.5	642.0	573.9	483.8	441.5	422.7	420.8	413.9
70	410.7	379.8	330.8	306.4	295.9	305.1	290.4	100.0	2677.0	3046.6
80	2620.5	2590.0	2806.7	3033.7	2562.5	2153.8	1386.2	806.3	610.6	176.1
90	225.3	184.7	112.9	129.5	118.6	1054.4				

TIME = 690.0 SEC

	1	2	3	4	5	6	7	8	9	10
0	4000.0	4000.0	4000.0	7000.0	7000.0	7000.0	7000.0	3119.3	3405.7	4004.8
10	4883.0	5496.2	5935.1	6028.4	3376.1	3990.0	4693.2	5259.6	5498.6	5602.4
20	5045.2	5246.0	5348.7	3340.9	3968.7	4565.6	4924.9	5135.5	5238.4	3180.5
30	3708.9	4142.3	4416.3	4598.7	4689.3	2560.0	2465.3	2481.1	2539.3	2585.4
40	2622.2	2642.3	2119.2	1878.7	1727.2	1661.9	1632.0	1616.9	1613.0	1900.1
50	1589.4	1390.7	1300.0	1258.3	1241.7	1250.1	1131.8	990.1	848.1	782.1
60	752.1	741.8	741.1	677.0	613.1	522.4	479.2	460.1	458.2	451.2
70	428.3	400.6	352.6	328.4	317.8	327.1	312.4	100.0	2736.9	3101.9
80	2681.9	2652.3	2867.1	3082.9	2624.3	2223.4	1441.7	848.3	646.4	184.8
90	237.5	193.9	115.1	133.8	121.6	1111.5				

TIME = 720.0 SEC

	1	2	3	4	5	6	7	8	9	10
0	4000.0	4000.0	4000.0	7000.0	7000.0	7000.0	7000.0	3165.7	3452.8	4048.1
10	4919.6	5524.4	5956.2	6048.2	3425.0	4034.9	4733.3	5292.3	5528.2	5630.7
20	5081.8	5280.5	5382.0	3391.4	4014.9	4607.7	4963.5	5172.0	5273.8	3236.0
30	3761.3	4191.9	4463.7	4644.5	4734.3	2622.4	2535.0	2555.2	2614.9	2661.7
40	2698.8	2719.1	2189.1	1954.8	1807.3	1743.9	1714.9	1700.6	1697.1	1970.5
50	1663.6	1467.4	1378.0	1337.3	1321.7	1331.4	1183.9	1047.4	905.7	839.6
60	809.6	799.6	799.3	711.1	651.9	561.0	517.4	498.1	496.3	489.3
70	445.0	420.5	373.8	350.0	339.6	348.8	334.3	100.0	2794.2	3154.5
80	2740.8	2712.1	2924.8	3129.8	2683.7	2290.5	1496.5	889.9	682.3	193.8
90	250.1	203.5	117.5	138.5	124.8	1168.3				

TIME = 750.0 SEC

	1	2	3	4	5	6	7	8	9	10
0	4000.0	4000.0	4000.0	7000.0	7000.0	7000.0	7000.0	3210.0	3497.6	4088.9
10	4953.9	5550.9	5975.9	6066.6	3471.5	4077.2	4770.9	5322.9	5555.9	5657.1
20	5116.0	5312.7	5413.1	3439.4	4058.5	4647.2	4999.7	5206.2	5306.9	3288.8
30	3811.0	4238.7	4508.3	4687.6	4776.6	2682.4	2602.0	2626.4	2687.7	2735.2
40	2772.6	2793.0	2256.7	2028.8	1885.4	1824.0	1796.1	1782.6	1779.6	2038.9
50	1736.2	1542.8	1455.1	1415.4	1401.0	1412.0	1234.7	1103.9	963.0	897.0
60	857.2	857.7	858.0	744.3	690.0	599.6	555.8	536.5	534.8	528.0
70	460.8	439.4	394.4	371.2	361.0	370.0	356.0	100.0	2849.3	3204.7
80	2797.3	2769.5	2980.1	3174.6	2740.6	2355.4	1550.6	931.2	718.3	203.3
90	263.1	213.5	120.0	143.5	128.3	1224.7				

TIME = 780.0 SEC

	1	2	3	4	5	6	7	8	9	10
0	4000.0	4000.0	4000.0	7000.0	7000.0	7000.0	7000.0	3252.4	3540.2	4127.5
10	4986.2	5575.7	5994.4	6083.8	3515.7	4117.3	4806.4	5351.7	5581.8	5681.9
20	5148.1	5342.9	5442.3	3485.0	4099.6	4684.5	5033.7	5238.3	5338.0	3339.1
30	3858.2	4283.0	4550.6	4728.4	4816.6	2740.2	2666.5	2694.9	2757.7	2805.9
40	2843.7	2864.3	2322.2	2100.7	1961.5	1902.3	1875.6	1862.8	1860.4	2105.2
50	1807.0	1616.9	1530.9	1492.6	1479.3	1491.7	1284.1	1159.4	1019.8	954.3
60	924.9	915.9	916.8	776.5	727.3	637.8	594.2	575.0	573.4	566.9

70	475.7	457.4	414.1	391.7	381.9	390.6	377.2	100.0	2902.2	3252.7
80	2851.6	2824.7	3033.0	3217.5	2795.3	2418.1	1603.8	972.2	754.1	213.0
90	276.4	223.8	122.9	148.8	132.1	1280.7				

TIME = 810.0 SEC

	1	2	3	4	5	6	7	8	9	10
0	4000.0	4000.0	4000.0	7000.0	7000.0	7000.0	7000.0	3293.0	3580.7	4164.1
10	5016.8	5599.1	6011.7	6100.1	3557.8	4155.2	4839.9	5378.8	5606.2	5705.1
20	5178.4	5371.4	5469.7	3528.6	4138.7	4719.7	5065.9	5268.5	5367.2	3387.2
30	3903.0	4325.1	4590.7	4767.0	4854.4	2795.8	2728.5	2760.9	2825.2	2874.1
40	2912.2	2933.0	2385.5	2170.5	2035.7	1978.7	1953.3	1941.4	1939.5	2169.7
50	1876.2	1689.5	1605.6	1568.5	1556.6	1570.4	1332.2	1213.8	1075.9	1011.2
60	982.3	973.9	975.5	867.7	763.8	675.6	632.4	613.4	612.0	605.9
70	489.8	474.4	433.1	411.5	402.1	410.5	397.8	100.0	2953.0	3298.6
80	2903.9	2977.8	3083.8	3258.6	2847.9	2478.7	1656.3	1012.8	789.9	223.1
90	290.0	234.4	125.9	154.5	136.2	1336.2				

TIME = 840.0 SEC

	1	2	3	4	5	6	7	8	9	10
0	4000.0	4000.0	4000.0	7000.0	7000.0	7000.0	7000.0	3332.0	3619.5	4198.8
10	5045.8	5621.2	6028.1	6115.3	3598.0	4191.3	4871.7	5404.4	5629.2	5727.1
20	5207.1	5398.2	5495.6	3570.2	4175.8	4753.1	5096.2	5297.0	5394.8	3433.2
30	3945.7	4365.2	4628.8	4803.7	4890.4	2849.4	2788.3	2824.4	2890.3	2939.8
40	2978.4	2999.3	2446.9	2238.3	2107.9	2053.2	2029.1	2018.1	2016.8	2232.2
50	1943.6	1760.5	1678.8	1643.2	1632.6	1647.8	1378.9	1266.9	1131.2	1067.5
60	1039.3	1031.5	1033.9	837.9	799.3	712.7	670.1	651.5	650.2	644.7
70	503.1	490.5	451.1	430.5	421.5	429.5	417.6	100.0	3001.9	3342.6
80	2954.2	2928.9	3132.6	3298.1	2898.6	2537.4	1708.1	1052.9	825.5	233.4
90	303.9	245.4	129.1	160.5	140.5	1391.2				

TIME = 870.0 SEC

	1	2	3	4	5	6	7	8	9	10
0	4000.0	4000.0	4000.0	7000.0	7000.0	7000.0	7000.0	3369.4	3656.5	4231.9
10	5073.3	5642.2	6043.6	6129.8	3636.5	4225.6	4901.8	5428.7	5651.0	5747.8
20	5234.2	5423.7	5520.1	3609.9	4211.1	4784.8	5125.1	5324.1	5421.0	3477.2
30	3986.5	4403.4	4665.0	4838.6	4924.6	2901.0	2846.0	2885.8	2953.1	3003.3
40	3042.2	3063.3	2506.3	2304.1	2178.2	2125.9	2103.1	2093.0	2092.3	2292.9
50	2009.3	1830.1	1750.6	1716.5	1707.3	1724.0	1424.2	1318.8	1185.5	1123.0
60	1095.6	1088.6	1091.8	867.1	833.8	749.0	707.3	689.1	688.0	683.2
70	515.6	505.7	468.2	448.6	440.1	447.7	436.7	100.0	3049.0	3384.8
80	3002.6	2978.2	3179.5	3336.0	2947.5	2594.1	1759.0	1092.6	860.9	244.0
90	318.1	256.6	132.6	166.9	145.1	1445.5				

TIME = 900.0 SEC

	1	2	3	4	5	6	7	8	9	10
0	4000.0	4000.0	4000.0	7000.0	7000.0	7000.0	7000.0	3405.3	3692.0	4263.4
10	5099.4	5662.1	6058.3	6143.5	3673.3	4258.3	4930.6	5451.8	5671.7	5767.5
20	5260.1	5447.8	5543.4	3648.1	4244.8	4815.0	5152.4	5349.7	5445.8	3519.5
30	4025.5	4439.9	4699.7	4871.9	4957.3	2950.9	2901.6	2945.0	3013.8	3064.6
40	3103.9	3125.2	2563.8	2367.9	2246.6	2196.7	2175.2	2166.2	2166.0	2351.7
50	2073.2	1898.0	1820.9	1788.4	1780.6	1798.7	1468.3	1369.5	1238.8	1177.7
60	1151.2	1144.9	1149.0	895.4	867.3	784.6	743.8	726.2	725.2	721.1
70	527.5	520.0	484.5	465.8	457.8	465.0	454.9	100.0	3094.4	3425.3
80	3049.3	3025.7	3224.7	3372.4	2994.5	2649.0	1809.1	1131.8	896.0	254.9
90	332.6	268.1	136.3	173.6	150.1	1499.3				

TIME = 930.0 SEC

	1	2	3	4	5	6	7	8	9	10
0	4000.0	4000.0	4000.0	7000.0	7000.0	7000.0	7000.0	3439.9	3726.0	4293.6
10	5124.4	5681.0	6072.3	6156.5	3708.7	4289.6	4958.0	5473.8	5691.4	5786.2
20	5284.7	5470.8	5565.5	3684.6	4277.1	4843.9	5178.5	5374.2	5469.4	3560.1
30	4062.9	4474.7	4732.8	4903.8	4988.5	2999.0	2955.3	3002.2	3072.4	3123.9
40	3163.5	3185.0	2619.5	2429.9	2313.1	2265.6	2245.5	2237.4	2237.8	2408.8
50	2135.5	1964.3	1889.7	1858.8	1852.4	1872.0	1511.0	1418.7	1290.9	1231.3
60	1205.8	1200.3	1205.4	922.7	899.8	819.2	779.5	762.5	761.7	758.4
70	538.8	533.6	499.8	482.2	474.6	481.5	472.3	100.0	3138.2	3464.3
80	3094.4	3071.5	3268.2	3407.5	3040.0	2702.1	1858.4	1170.6	930.9	265.9
90	347.3	279.9	140.3	180.6	155.3	1552.4				

TIME = 960.0 SEC

	1	2	3	4	5	6	7	8	9	10
0	4000.0	4000.0	4000.0	7000.0	7000.0	7000.0	7000.0	3473.3	3758.7	4322.4
10	5148.3	5699.1	6085.6	6168.9	3742.6	4319.6	4984.2	5494.7	5710.1	5804.0
20	5308.1	5492.7	5586.5	3719.8	4307.9	4871.4	5203.4	5397.5	5491.9	3599.1
30	4098.7	4508.2	4764.5	4934.2	5018.3	3045.5	3007.2	3057.4	3129.0	3181.2
40	3221.2	3242.8	2673.5	2490.1	2377.7	2332.7	2314.0	2306.9	2307.9	2464.3
50	2196.0	2028.9	1956.9	1927.6	1922.7	1943.7	1552.4	1466.7	1341.9	1283.9
60	1259.4	1254.7	1260.8	949.0	931.2	852.9	814.4	798.0	797.4	794.9
70	549.4	546.3	514.4	497.7	490.7	497.1	488.8	100.0	3180.5	3501.9
80	3137.9	3115.8	3310.2	3441.3	3083.9	2753.6	1906.9	1208.8	965.5	277.2
90	362.3	291.9	144.5	188.0	160.7	1604.9				

TIME = 990.0 SEC

	1	2	3	4	5	6	7	8	9	10
0	4000.0	4000.0	4000.0	7000.0	7000.0	7000.0	7000.0	3505.4	3790.1	4350.1
10	5171.1	5716.4	6098.3	6180.8	3775.2	4348.3	5009.2	5514.8	5728.0	5821.0
20	5330.5	5513.6	5606.6	3753.5	4337.5	4897.8	5227.3	5419.7	5513.3	3636.7
30	4133.2	4540.2	4794.9	4963.4	5046.9	3090.5	3057.3	3110.8	3183.8	3236.6
40	3277.0	3298.7	2725.8	2548.5	2440.5	2397.9	2380.7	2374.6	2376.2	2518.0
50	2254.9	2091.9	2022.4	1994.8	1991.4	2013.8	1592.6	1513.3	1391.6	1335.4
60	1312.0	1308.1	1315.2	974.5	961.6	885.6	848.4	832.6	832.3	830.6
70	559.5	558.4	528.2	512.5	505.8	511.9	504.5	100.0	3221.3	3538.0
80	3179.9	3158.5	3350.7	3473.9	3126.3	2803.4	1954.7	1246.6	999.8	288.7
90	377.4	304.1	148.9	195.6	166.5	1656.7				

TIME = 1000.0 SEC

	1	2	3	4	5	6	7	8	9	10
0	4000.0	4000.0	4000.0	7000.0	7000.0	7000.0	7000.0	3515.9	3800.3	4359.0
10	5178.5	5722.0	6102.4	6184.6	3785.8	4357.6	5017.3	5521.2	5733.8	5826.6
20	5337.8	5520.4	5613.1	3764.5	4347.1	4906.3	5235.0	5427.0	5520.3	3648.9
30	4144.3	4550.7	4804.7	4972.9	5056.2	3105.1	3073.6	3128.2	3201.6	3254.6
40	3295.1	3317.0	2742.8	2567.6	2461.1	2419.3	2402.5	2396.7	2398.5	2535.6
50	2274.2	2112.6	2043.9	2016.9	2014.0	2036.8	1605.7	1528.5	1407.9	1352.3
60	1329.2	1325.6	1333.1	982.8	971.5	896.3	859.5	844.0	843.8	842.3
70	562.8	562.3	532.6	517.2	510.7	516.6	509.5	100.0	3234.6	3549.8
80	3193.6	3172.4	3363.9	3484.6	3140.1	2819.7	1970.4	1259.0	1011.2	292.6
90	382.5	308.3	150.4	198.3	168.5	1673.8				

Thiokol

CHEMICAL CORPORATION

REACTION MOTORS DIVISION

APPENDIX B

JPL OF₂/DB THRUST CHAMBER

DESIGN ANALYSIS

REACTION MOTORS DIVISION

DENVILLE, NEW JERSEY

Thiokol® CHEMICAL CORPORATION

DS 100-135

REPORT NUMBER

CLASS U

TITLE JPL OF₂/DB THRUST CHAMBER DESIGN ANALYSIS

REPORT PREPARED BY C. F. Nash *C. F. Nash* 3/13/69
(DATE)

REPORT CHECKED BY _____
(DATE)

REPORT APPROVED BY R. H. Sawyer *R. H. Sawyer* 3/13/69
(DATE)

THIS REPORT INCLUDES 50 PAGES, _____ FIGURES, AND _____ DRAWINGS.

cc:

L. Van Der Jagt
Stress
Library

REVISIONS AND ADDITIONS

LETTER	DATE	DESCRIPTION	BY	CHECKED	APPROVED

Thiokol CHEMICAL CORPORATION
REACTION MOTORS DIVISION
DENVER, NEW JERSEY

Design Report

Page 1

TITLE: JPL OF₂/DB THRUST CHAMBER DESIGN ANALYSIS

REPORT NO. DS 100-135

SUMMARY

The JPL OF₂/DB Thrust Chamber Assembly meets the design requirements of JPL as specified by RMD WA 6062-11-3000.

INTRODUCTION

This report documents the design analysis performed to assure the structural integrity of the JPL OF₂/DB Thrust Chamber Assembly defined by RMD Drawing 318281, and Figure 1 of this report.

DESIGN CRITERIA

The assembly has been analyzed for the following conditions as outlined by WA 6062-11-3000:

a. Thermal Effects

- Expansion
- Heat Transfer (Thermal Gradients)

b. Pressure Loads

- Ignition Spike (200 psia for 5 millisecs)
- Steady State (100 psia at 1000 sec. temperature profile)

The heat transfer analysis is found in RMD Report DS 100-134. Figure 2 of Appendix A of this report presents the critical temperature profile.

Thiokol • CHEMICAL CORPORATION

REACTION MOTORS DIVISION

DENVILLE, NEW JERSEY

Design Report

Page 2

TITLE: JPL OF₂/DB THRUST CHAMBER DESIGN ANALYSIS

REPORT NO. DS 100-135

DISCUSSION

The design analysis presented in Appendix A was performed in conjunction with the design layout and, therefore, represents the analysis leading to the final design.

One of the major problems in the design of a high temperature system made up of several individual elements is to provide for differential thermal growth.

Radial growth has been allowed for by using a crushable Grafoil Laminate cylinder which readily deforms without creating any significant forces.

The same solution was provided to account for circumferential thermal growth; i. e., Grafoil Laminate is used as an expansion media for the inner P. G. wedges and the outer P. G. split ring.

Differential thermal growth in the axial direction tends to alleviate the compression in the Grafoil gasket used to seal the combustion gases. The calculated seal backoff is 0.05 inches maximum. This has been allowed for by providing a gasket that requires a 900 psi compressive force at room temperature and maintains a 330 psi compressive force after a 0.05 inch backoff. Note that this compressive force is well above the 100 psi operating pressure and should provide an adequate seal.

The inner ATJS liner has been analyzed with regard to thermal stresses. The most critical area is the nozzle throat at $t = 30$ seconds which is the time at which the thermal gradient is the highest and the strength is still relatively low (strength increases with temperature). The calculations indicate adequate margins of safety.

Thiokol® CHEMICAL CORPORATION

REACTION MOTORS DIVISION

DENVILLE, NEW JERSEY

Design Report

Page 3

TITLE: JPL OF₂/DB THRUST CHAMBER DESIGN ANALYSIS

REPORT NO. DS 100-135

DISCUSSION (continued)

The detailed design analysis, found in Appendix A, shows adequate margins of safety for all structural components.

Vibratory problems are not anticipated.

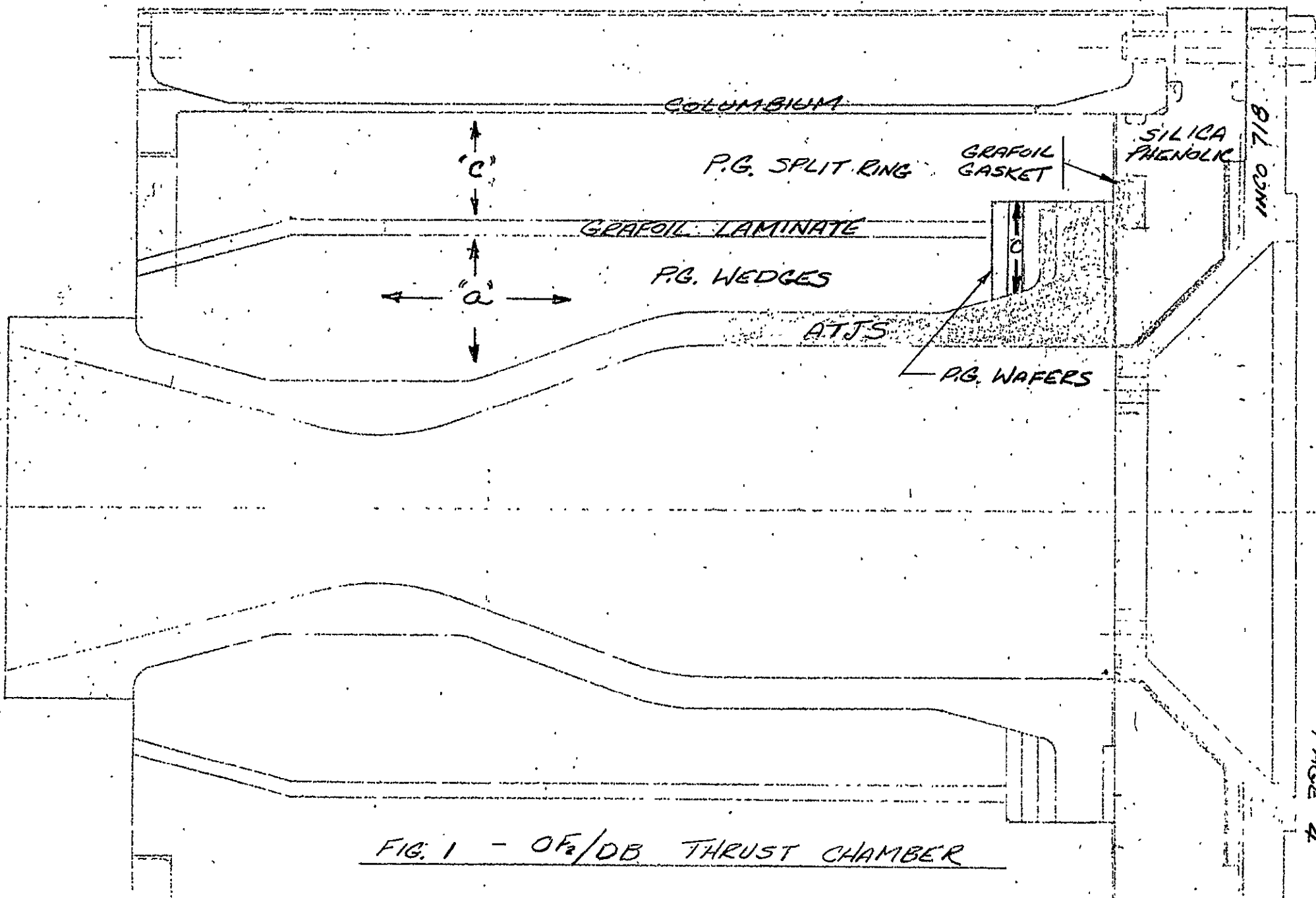


FIG. 1 - OF₂/DB THRUST CHAMBER

PREP. BY _____

CHKD. BY _____

SECURITY INFORMATION

CALCULATION
OR REPORT NO.

PAGE 5 OF 50

70

TITLE:

APPENDIX ADESIGN ANALYSIS

Thiokol CHEMICAL CORPORATION
REACTION MOTORS DIVISION
SENYVILLE, NEW JERSEY

SECURITY INFORMATION

OGILVIE PRESS INC.,
BROOKLYN 17, N. Y.
REPROVAL NO. 440H

PREP. BY C.F. NASH 10-11-68CHKD. BY G. RABE 10/31/68

SECURITY INFORMATION

CALCULATION
OR REPORT NO.PAGE 6 OF 50

TITLE:

LONGITUDINAL AVERAGE TEMPERATURES (REFER TO FIG. 2)ATJS FROM A TO B

$$\begin{array}{r}
 7991 \quad \swarrow \text{NODAL PT} \quad 5447 \quad 3823 \\
 \frac{8+9+79+15}{4} (2.23) + \frac{(10+16)}{2} 1.25 + \frac{(11+17)}{2} (.75) \\
 \quad 4216 \quad 4438 \quad 4503 \\
 + \frac{(12+18)}{2} (.75) + \frac{(13+19)}{2} (.75) + \frac{(14+20)}{2} (.75) \\
 \quad 6296 \\
 + \frac{12+18}{2} (1.12) = T_{AV} L_T
 \end{array}$$

$$T_{AV} L_T = 36,716$$

$$L_T = 7.66$$

$$T_{AV} = 4831^\circ \text{F FOR PURPOSE OF DETERMINING AXIAL GROWTH BETWEEN A \& B}$$

P.B. FROM C TO B

$$\begin{array}{r}
 5663 \quad 5441 \quad 3721 \\
 \frac{15+24}{2} (1.5) + \frac{16+25}{2} (1.25) + \frac{17+26}{2} (.75) \\
 \quad 4023 \quad 4170 \\
 + \frac{18+21+27}{3} (.75) + \frac{19+22+28}{3} (.75) + \\
 \quad 4118 \quad 6296 \\
 + \frac{20+23+29}{3} (.75) + \frac{18+12}{2} (1.12) = T_{AV} L_T = 33,432
 \end{array}$$

$$L_T = 6.87$$

$$\therefore T_{AV} = 4866^\circ \text{F}$$

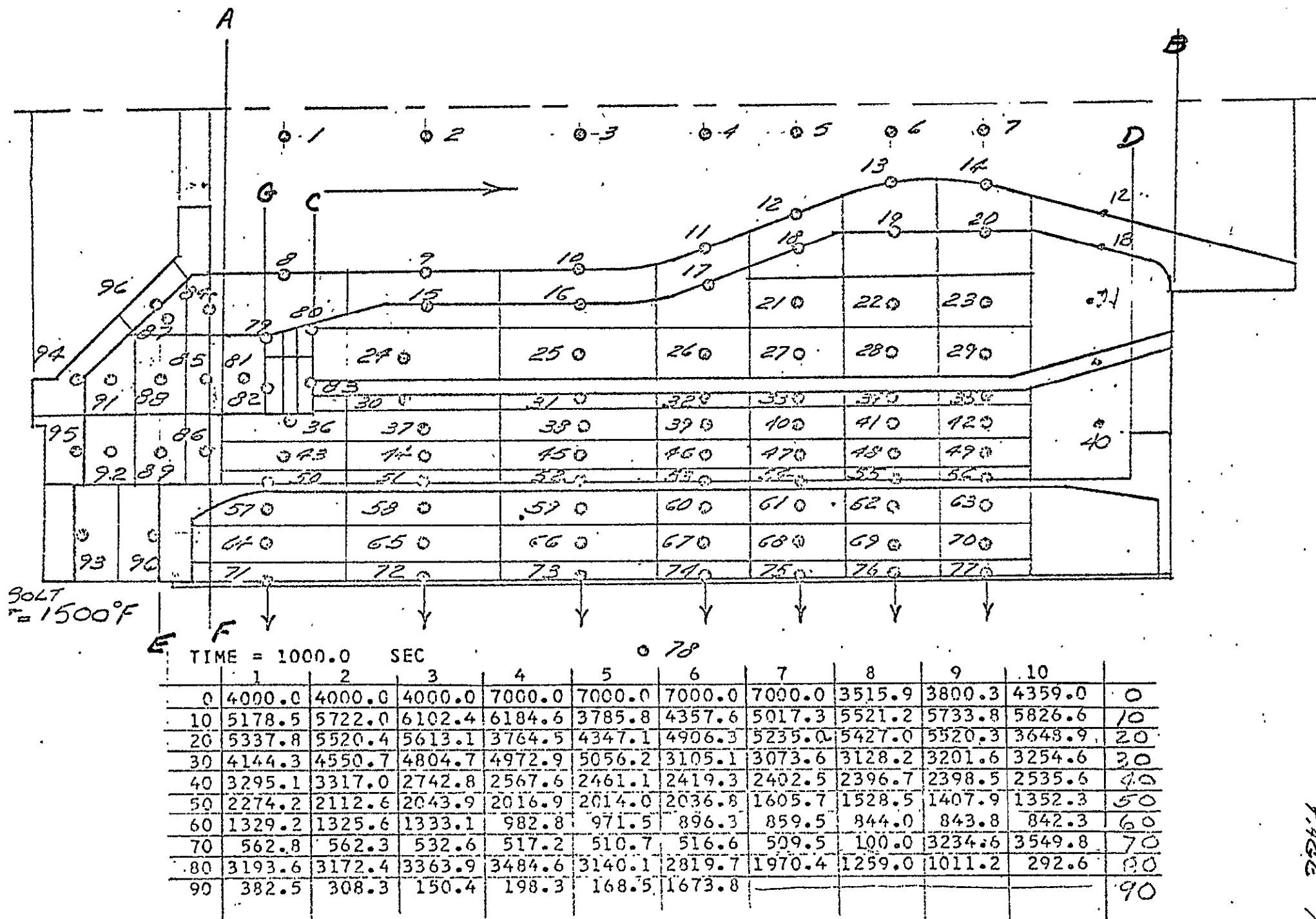


FIG. 2 - TEMPERATURE PROFILE $t = 1000 \text{ SEC.}$

PREP. BY C.F. NASH 10-16-68

CHKD. BY G. PABE 10/31/68

SECURITY INFORMATION

CALCULATION
OR REPORT NO.

PAGE 8 OF 50

TITLE:

GRAFOIL FOAM FROM C TO B

$$30(1.5) + 31(1.25) + 32(.75) + 33(.75) \\ + 34(.75) + 35(.75) + \frac{(7+8)}{2}(1.12) = 31,163$$

$$L_T = 6.87$$

$$T_{AT} = 4536$$

AXIAL

FORCES BETWEEN ATJS AND INNER P.G. LINER ΔL_{ATJS}

$$\Delta T = 4831 - 70 = 4761^\circ F$$

$$L = 7.25$$

$$\Delta = 11 \times 10^{-3} \frac{IN}{IN}$$

$$\Delta L = 11 \times 10^{-3} \times 7.25 = .0797 IN$$

REF. - UNION CARBIDE
CORP.; TECH. INF.
BULLETIN # 463-201 IG

 $\Delta L_{P.G. LINER}$

$$\Delta T = 4866 - 70 = 4796^\circ F$$

$$L = 6.87$$

$$\Delta_a = .0068 \frac{IN}{IN}$$

$$\Delta L_a = .0068 \times 6.87 = .0468$$

REF. - SUPER-TEMP
CORP.
PYROLYTIC GRAPHITE

 $\Delta L_{P.G. WAFERS}$

$$\Delta T = \frac{79 + 80 + 82 + 83}{4} = 3330$$

$$L = 7.25 - 6.87 = .38$$

$$\Delta_a = .051 \frac{IN}{IN}$$

REF. - HIGH TEMP-
ERATURE MATERIALS
INC. - PG. DATA SHEET

Thiokol CHEMICAL CORPORATION
REACTION MOTORS DIVISION
CONVILLE, NEW JERSEY

SECURITY INFORMATION

OGILVIE PRESS INC.,
BROOKLYN 17, N. Y.
REPROV'EL NO. 440H

PREP. BY C.F. NASH 10-16-68CHKD. BY G. RABR 10/31/68

SECURITY INFORMATION

CALCULATION
OR REPORT NO.PAGE 9 OF 50

TITLE:

$$\Delta L_{\frac{1}{2}} = .051(.38) = .0194 \text{ in.}$$

$$\therefore \text{ATJS } \Delta L = .0797 \text{ in.}$$

$$\text{P.G. LINER + WAFERS} = .0468 + .0194 = .0662 \text{ in.}$$

$\therefore$ NO INTERFERENCE & NO FORCES

GASKET COMPRESSION

AVERAGE TEMP OF OUTER P.G. FROM C TO D

$$\begin{aligned} & \frac{842}{4} \frac{30+36+43+50}{4} (.28) + \frac{3614}{4} \frac{30+37+44+51}{4} (1.25) + \frac{3702}{4} \frac{31+38+45+52}{4} (1.25) \\ & + \frac{2291}{4} \frac{32+39+46+53}{4} (.75) + \frac{2340}{4} \frac{33+40+47+54}{4} (.75) \\ & + \frac{2377}{4} \frac{34+41+48+55}{4} (.75) + \frac{2402}{4} \frac{35+42+49+56}{4} (.75) \\ & + \frac{2604}{4} \frac{40}{4} (.8) = 20172 \end{aligned}$$

$$L_T = 6.58 \quad \therefore T_{AV} = 3066^\circ \text{F}$$

AVERAGE TEMP OF COLUMBINUM FROM E TO D

$$\begin{aligned} & 50(1.5) + 51(1.25) + 52(1.25) + 53(.75) + 54(.77) \\ & + 55(.77) + 56(1.51) = 17000 \\ & L_T = 7.8 \quad T_{AV} = 2180^\circ \text{F} \end{aligned}$$

PREP. BY C. F. NASH 10-17-68

CHKD. BY G. L. ABLE 10/31/68

SECURITY INFORMATION

CALCULATION
OR REPORT NO.

PAGE 10 OF 50

TITLE:

AVERAGE T OF PG. WAFERS = 3330°F

AVERAGE T OF SILICA PHENOLIC FROM E TO F

$$\frac{84+87+85+88+86+89}{6} = 2281^{\circ}\text{F}$$

AVERAGE T OF ATJS FLANGE = 81 = 3194°F

GAP AT GASKET:

$$-(l_{CO} + \Delta l_{CO})_{PG} - (l_{CG} + \Delta l_{CG})_{\text{WAFERS}} - (l_{AG} + \Delta l_{AG})_{\text{ATJS}} \\ - (l_{EF} + \Delta l_{EF})_{\text{SILICA PHENOLIC}} + (l_{ED} + \Delta l_{ED})_{\text{COLUMBIUM}} = G$$

$$l_{CO} + l_{CG} + l_{GA} + l_{EA} = l_{ED}$$

$$\text{OR } -(\Delta l_{CO})_{PG} - (\Delta l_{CG})_{\text{WAFERS}} - (\Delta l_{AG})_{\text{ATJS}} \\ - (\Delta l_{EF})_{SP} + (\Delta l_{ED})_{\text{COL.}} = G$$

$$(\Delta l_{CO})_{PG}$$

$$\Delta T = 3066 - 70 = 2996^{\circ}\text{F}$$

$$L = 6.44$$

$$\Delta_{\text{REF}} = .002 \frac{\text{IN}}{\text{IN}}$$

{ REF - HIGH TEMPERATURE
MATERIAL INC. -
PG. DATA SHEET

$$\therefore (\Delta l_{CO})_{PG} = .002(6.44) = .01288$$

Thiokol CHEMICAL CORPORATION
REACTION MOTORS DIVISION
SCHULLE, NEW JERSEY

SECURITY INFORMATION

OGILVIE PRESS INC.,
BROOKLYN 17, N. Y.
REPROVAL NO. 440H

PREP. BY C.F. NASH 10-17-68CHKD. BY G. LARBE 10/31/68

SECURITY INFORMATION

CALCULATION
OR REPORT NO.PAGE 11 OF 50

TITLE:

$$(\Delta L_{CG})_{NAFEEs} = .0194 \text{ in. (TOP OF p.9)}$$

$$(\Delta L_{AG})_{ATJS}$$

$$\Delta T = 3194 - 70 = 3124^{\circ}\text{F}$$

$$L = .58$$

$$\alpha = 6 \times 10^{-3} \text{ IN/IN}$$

REF - UNION CARBIDE
CORP - TECHNICAL
INFORMATION
BULLETIN No. 463-2016

$$\therefore (\Delta L_{AG})_{ATJS} = 6 \times 10^{-3} \times .58 = .00348 \text{ in.}$$

$$(\Delta L_{EF})_{SP}$$

$$\Delta T = 2281 - 70 = 2211^{\circ}\text{F}$$

$$L = .4$$

$$\alpha = 3 \times 10^{-6}$$

REF - POLYMERIC
CHEMICALS INC.
DATA SHEET
FM-5067

$$\therefore (\Delta L_{EF})_{SP} = .4(3)10^{-6}(2211) = .00265$$

$$(\Delta L_{ED})_{COL}$$

$$\Delta T = 2180 - 70 = 2110^{\circ}\text{F}$$

$$L = 7.80$$

$$\alpha = 4.5 \times 10^{-6}$$

WAN CHANG ALBANY
C-103 DATA

$$\therefore (\Delta L_{ED})_{COL} = 7.8(2110)(4.5 \times 10^{-6}) = .07406$$

$$\begin{aligned} \text{GAP} &= -(0.1288 + .0194 + .00348 + .00265) + .07406 \\ &= +.0356 \end{aligned}$$

PREP. BY C.F. NASH 10-17-68

CHKD. BY G. ROBE 10/21/68

SECURITY INFORMATION

CALCULATION
OR REPORT NO.

PAGE 12 OF 50

TITLE:

RADIAL THERMAL GROWTHS (THROAT SECTION)

CHECK PLANE OF NODAL PTS. 14 & 77

ATJS AV. TEMP = 6185

$$\begin{array}{r} 5827 \\ 2 \overline{) 12012} \\ 6006^\circ\text{F} \end{array}$$

$\Delta T = 5936$

$R_0 = 1$

$t = .42$

$\Delta = .018 \frac{\text{IN}}{\text{IN}}$

EXTRAPOLATED

$\Delta R = .018(1) = .018 \text{ IN.}$

REF. UNION CARBIDE CORP.
TECH INFO BUL 463-201 IG

INNER P.G.

AV. TEMP = 5827

$$\begin{array}{r} 5613 \\ 5520 \end{array}$$

$$\begin{array}{r} 3 \overline{) 16960} \\ 5653 \end{array}$$

$\Delta T = 5583^\circ\text{F}$

$t = 1.15$

$\Delta_{2''} = .008 \frac{\text{IN}}{\text{IN}}$

EXTRAPOLATED

REF. SUPER-TEMP CORP.

$\Delta t = .008(1.15) = .0092 \text{ IN.}$

OUTER P.G.

AV. TEMP = 5056

$$\begin{array}{r} 3317 \\ 2399 \end{array}$$

$$\begin{array}{r} 2037 \end{array}$$

$$\begin{array}{r} 4 \overline{) 12809} \\ 3202^\circ\text{F} \end{array}$$

PREP. BY C.F. NASH 10-18-68
 CHED. BY G. RABE 10/31/68

SECURITY INFORMATION

CALCULATION
OR REPORT NO.

PAGE 13 OF 50

TITLE:

$$t = .85$$

$$\Delta_c = .050 \text{ IN}$$

REF. - HIGH TEMPERATURE MATERIALS INC.
P.G. DATA SHEET

$$\Delta t = .85(.05) = .0425 \text{ IN.}$$

COLUMBIUM

$$T = 2037^\circ \text{F}$$

$$\Delta T = 1967^\circ \text{F}$$

$$\alpha = 4.5 \times 10^{-6} \frac{\text{IN}}{\text{IN}/^\circ \text{F}}$$

REF. WAN CHANG
ALBANY
C-103

$$R = 3.18$$

$$\Delta R = 3.18 \times 4.5 \times 10^{-6} \times 1967 = .028$$

ASSUMING NO ELASTIC DEFLECTIONS, THE GRAFILL
FOAM IS CRUSHED

$$.018 + .0092 + .0425 - .028 = \underline{\underline{.0417 \text{ IN}}}$$

SELECTION OF A LOW DENSITY FOAM WILL
LIMIT THE COMPRESSIVE PRESSURES TO LESS
THAN 100#/IN²

Thiokol CHEMICAL CORPORATION
REACTION MOTORS DIVISION
OHIOVILLE, NEW JERSEY

SECURITY INFORMATION

OGILVIE PRESS INC.,
BROOKLYN 17, N. Y.
REPROVAL NO. 440H

TITLE:

ATJS THERMAL STRESS

REF. ROARK 3rd ED. p. 338, CASE 16.

OUTER SURFACE

$$S_t = \frac{\Delta T \alpha E}{2(1-\mu) \ln \frac{c}{b}} \left(1 - \frac{2b^2}{c^2 - b^2} \ln \frac{c}{b} \right) \text{ TENSION}$$

INNER SURFACE

$$S_t = \frac{\Delta T \alpha E}{2(1-\mu) \ln \frac{c}{b}} \left(1 - \frac{2c^2}{c^2 - b^2} \ln \frac{c}{b} \right) \text{ COMP}$$

b = INNER RADIUS

c = OUTER RADIUS

EXAMINE NODAL PTS. 14/20

TIME	ΔT	AV. T
30	1495	2531
60	1309	3219
90	1154	3691
120	1032	
150	936	
180		
210		
240		
270		
1000	357	

THE MAXIMUM THERMAL
GRADIENT OCCURS
AT t = 30 SEC.

PREP. BY C.F. NASH 10-21-68
CHKD. BY G. ROBE 10/31/68

SECURITY INFORMATION

CALCULATION
OR REPORT NO

PAGE 15 OF 50

RE

TITLE:

$$\begin{aligned} C &= 1.0 & E &= 2.2 \times 10^6 @ 2500^\circ F \\ b &= .58 & \alpha &= \frac{(7.0 - 4.5) 10^{-3}}{1000} = 2.5 \times 10^{-6} \frac{\text{IN}}{\text{IN/OF}} @ 2500^\circ F \\ \mu &= .12 \text{ (RMD MATERIAL SECTION)} \end{aligned}$$

OUTER SURFACE

$$\begin{aligned} S_t &= \frac{1495 (2.5) (2.2)}{2 \ln \frac{1}{.58} (.88)} \left(1 - \frac{2 \times .58^2}{1^2 - .58^2} \ln \frac{1}{.58} \right) \\ &= 3840 \text{ psi} \end{aligned}$$

INNER SURFACE

$$\begin{aligned} S_t &= \frac{1495 (2.5) (2.2)}{2 \ln \frac{1}{.58} (.88)} \left(1 - \frac{2}{1 - .58^2} \ln \frac{1}{.58} \right) \\ &= -5510 \text{ psi} \end{aligned}$$

OK

$$\begin{aligned} F_{cu} @ 2500^\circ F &= -13,000 \text{ psi} \\ F_{tu} @ 2500^\circ F &= 6800 \text{ psi} \end{aligned} \left\{ \begin{array}{l} \text{REF-UNION CARBIDE} \\ \text{CORP., TECH. INF.} \\ \text{BULLETIN \# 463-201} \end{array} \right.$$

PREP. BY C.F. NASH 10-21-68
 CHKD. BY G. LARBE 10/31/68

SECURITY INFORMATION

CALCULATION
OR REPORT NO.

PAGE 16 OF 50

TITLE:

THICKNESS OF COLUMBIUM SHELL

LIMIT THE AXIAL GROWTH OF THE SHELL
TO .005 IN. (FOR SEALING PURPOSES)

$$\text{AXIAL GASKET FORCE} = 330 (\pi) (3.64^2 - 2.22^2) = 2120^{\#}$$

(DESIRED GASKET PRESSURE @ $t = 1000$)
 ASSUMING NO ALLEVIATION.

$$\text{GAS AXIAL FORCE} = 100 \pi (3.13)^2 = 3080^{\#}$$

ASSUMING SMALL
LEAK FAST GASKET

$$\text{LET SHELL } T = 2500^{\circ}\text{F} \left(\begin{array}{l} \text{CONSV. - CALCS. SHOW} \\ 2274^{\circ}\text{F MAX LOCALLY} \end{array} \right)$$

$$\text{TIME} = 16.7 \text{ MIN.}$$

$$\text{MAX. \% ELONGATION ALLOWED} = \frac{.005 \times 100}{6.55} = .0763\%$$

CREEP DATA FOR .0763% NOT AVAILABLE

CHECK ELASTIC GROWTH FOR 5000 psi STRESS
 $E = 6.3 \times 10^6$ @ 2500°F (REF. - WAN CHANG) LEVEL

$$E = \frac{5000}{6.3 \times 10^6} = .000795 \frac{\text{IN}}{\text{IN}}$$

$S = 6.55 \times .000795$
 $S_{\text{AXIAL}} = .0052 \text{ IN}$

∴ @ 5000 psi STRESS, THE ELASTIC GROWTH
ALONE IS OVER THE DESIGN VALUE.

ESTIMATE ALLOWABLE ^{AXIAL} STRESS = 2500 psi
AND FIND t

$$t = \frac{(3080 + 2120)}{2500 (2) \pi (3.17)} = .105$$

PREP. BY C. F. NASH 10-21-68CHKD. BY G. Kase 10/21/68

SECURITY INFORMATION

CALCULATION
OR REPORT NO.PAGE 17 OF 50

TITLE:

ACTUALLY, THE FORWARD END OF THE COLUMBIUM IS THE ONLY SECTION AT 2500°F AT $\frac{750}{60} = 12.5$ MIN. THAT SECTION IS AT 2000°F.

∴ SAY THAT 2 IN. OF THE COLUMBIUM IS AT 2500°F FOR $16.7 - 12.5 = 4.2$ MIN. THE REST OF THE COLUMBIUM IS AT 2000°F, AND REFERRING TO THE WAH CHANG CATALOG, THERE IS NO CREEP AT 2000°F FOR STRESSES OF <15,000 psi @ 1 hr.

CONSIDER USING TWO IDENTICAL GASKETS.

LIMIT THE TOTAL GROWTH TO .010

FROM WAH CHANG THE ALLOWABLE STRESS FOR .5% CREEP FOR 5.7 MIN @ 2500°F IS 7000 psi.

LET $f = 5000$ psi AND CALCULATE THE GROWTH.

$$\Delta_{2500^\circ\text{F}} = \frac{5000}{6.3 \times 10^6} \times 2 = .0016$$

$$\Delta_{2000^\circ\text{F}} = \frac{5000}{12.3 \times 10^6} \times 4.55 = .0018$$

$$\Delta_{\text{CREEP}} = \underset{\substack{\text{WAH CHANG} \\ \text{FROM CATALOG} \\ \uparrow \\ 2500^\circ\text{F} \\ 5000 \text{ psi} \quad 5.4 \text{ MIN.}}}{2} \times .002 = .004$$

.0074 IN TOTAL

$$t = \frac{.105}{2} = .0525 \text{ IN.}$$

PREP. BY C. F. NASH 10-22-68CHKD. BY G. PAGE 10/31/68

SECURITY INFORMATION

CALCULATION
OR REPORT NO.PAGE 18 : 50

TITLE:

THE BOLT DEFLECTION MUST BE ADDED TO THE
.0074 IN.

BOLT $T = 1500^{\circ}\text{F}$

DETERMINE THERMAL GROWTH :

MATERIAL CB-74 (752)

REF. AEROSPACE
STRUCTURAL
METAL HDBK
VOL IIA

$$\alpha = 4.1 \times 10^{-6} \frac{\text{IN}}{\text{IN/}^{\circ}\text{F}} @ 1500^{\circ}\text{F}$$

$$L = .35 \text{ (SMALL SUBASSEMBLY BOLTS)}$$

$$\Delta L = .35(4.1)(10^{-6})(1500) = .00215 \text{ IN}$$

THE ADJACENT SILICA PHENOLIC IS AT LOW
TEMP AND $\therefore$ THERMAL EXPANSION CAN BE
IGNORED.

DETERMINE INITIAL BOLT LOADS TO COMPRESS
A 900 psi GASKET (R.T.)

$$F_{\text{AXIAL}} = 900 \pi (2.64^2 - 2.22^2) = 5770 \#$$

~ COMPRESSIVE Δ IN SILICA PHENOLIC IS

$$\Delta = \frac{PL}{AE} = \frac{7261 \times .62}{\pi \left(\frac{3.9^2 - 3.2^2}{4} \right) 2.3 \times 10^6} = .0001 \text{ IN}$$

NEGLIGIBLE

PREP. BY C.I.F. NASH 10-22-68

CHKD. BY G. RABE 10/31/68

SECURITY INFORMATION

CALCULATION
OR REPORT NO.

PAGE 19 OF 50

TITLE:

REFER BACK TO PAGE 11 AND REDUCE
GROWTH ASSUMING NO GASKET LEAK.

AXIAL GASKET FORCE = 2120# @ 330psi

GAS AXIAL FORCE = $100\pi(2.43)^2 = 1855\#$

↑
CENTER OF
GASKET

TOTAL AXIAL FORCE = 3975#

LET $t_{\text{SHELL}} = .060$ MIN.

AS BEFORE LET 2 IN OF SHELL BE AT 2500°F
" 4.55 IN " " " 2000°F

$$f_t = \frac{3975}{2\pi(3.17)(.06)} = 3330 \text{ psi}$$

SHELL

$$\Delta_{2500} = \frac{3330}{6.3 \times 10^6} \times 2 = .00106 \text{ IN.}$$

$$\Delta_{2000} = \frac{3330}{12.3 \times 10^6} \times 4.55 = .00123 \text{ IN.}$$

$$\Delta_{\text{CREEP}} = 2 \times .0015 = .003 \text{ IN.}$$

↑
EST.

.005 IN TOTAL - SHELL

BOLT (12 1/4 IN) CB 752

$$\Delta_{\text{THERMAL}} = .00215 \text{ IN. (FROM PAGE 18)}$$

$$\Delta_{\text{STRESS}} = \frac{3975 \times .35}{12 \pi \left(\frac{1}{4}\right)^2 \times 12 \times 10^6} = .0002$$

↑
ESTIMATED
@ 1500°F

SMALL SUB-
ASSEMBLY
BOLTS

PREP. BY C.F. NASH 10-22-68

CHKD. BY G. PABE 10/31/68

SECURITY INFORMATION

CALCULATION
OR REPORT NO.

PAGE 20 OF 50

TITLE:

TOTAL DEFLECTION AT GASKET IN THE
DIRECTION OF LOOSENESS

$$\begin{array}{r}
 .0011 \\
 .0012 \\
 .0030 \\
 .0022 \\
 .0002 \\
 \hline
 .0077 \\
 + .0356 \text{ FROM PAGE 6} \\
 \hline
 .0433 \text{ IN}
 \end{array}$$

CHECK OUT P.G. COMPRESSION

$$\Delta = \frac{4100 \times 6.44}{\pi(3.12^2 - 2.25^2) 3 \times 10^6} = .0006 \text{ IN. OK}$$

∴ ADEQUATE PROVISION WILL HAVE TO BE PROVIDED
IN THE GASKET DESIGN FOR A .045 IN BACKOFF.

DESIGN WANTS TO MAKE SMALL SUBASSEMBLY,
BOLTS FROM STAINLESS. ∴ LONG COLUMBIUM
BOLTS ARE GOING TO CARRY THE LOAD AT
TEMPERATURE. THE NEW DEFLECTION AT THE
GASKET TOWARDS LOOSENESS IS

$$.00215 \times \frac{1}{.35} = .00614$$

BOLT LENGTH
↑
P. 18

$$\begin{array}{r}
 .0450 \\
 - .0022 \\
 \hline
 .0428 \\
 + .0061 \\
 \hline
 .0489
 \end{array}$$

NEW BACKOFF = .049 IN

Thiokol CHEMICAL CORPORATION
REACTION MOTORS DIVISION
SENVILLE NEW JERSEY

SECURITY INFORMATION

OGILVIE PRESS INC.,
BROOKLYN 17, N. Y.
REPROVAL NO. 440H

PREP. BY C. F. NASH 10-22-68
 CHKD. BY G. PAGE 10/31/68

SECURITY INFORMATION

CALCULATION
OR REPORT NO.

PAGE 21 OF 50

TITLE:

BOLT ANALYSIS

LONG COLUMBIUM BOLTS

12 $\frac{1}{4}$ IN. BOLTS $A_t = .0362 \text{ IN}^2$

GASKET PRESSURE @ 1000 SEC = 330 psi

ASSUME A PRESSURE LEAK PASS THE GASKET JUST PRIOR TO 1000 SEC.

$$\begin{aligned} \text{TOTAL AXIAL FORCE} &= 100\pi(3.3)^2 + 330\pi(2.64^2 - 2.22^2) \\ &= 3421^{\#} + 2120^{\#} = 5540^{\#} \end{aligned}$$

$$\text{FORCE/BOLT} = \frac{5540}{12} = 461^{\#}$$

$$f_t = \frac{461}{.0362} = 12,700 \text{ psi}$$

BOLTS CB-74 (752)

ASSUME THREADS ARE AT 2000°F @ 999+ SEC.

FROM VOI-SHAN MANUFACTURING CO. FASTENER CATALOG $F_{tm} = 52,000 \text{ psi @ } 2000^{\circ}\text{F}$

FROM AEROSPACE METALS HANDBOOK

$$\left. \begin{aligned} F_{tm} &= 36,000 \text{ psi} \\ F_{ty} &= 28,000 \text{ psi} \end{aligned} \right\} @ 2000^{\circ}\text{F}$$

$$\text{M.S. ON YIELD} = \frac{28000}{12700} - 1 = \underline{1.2}$$

Thiokol CHEMICAL CORPORATION
REACTION MOTORS DIVISION
DENVER, NEW JERSEY

SECURITY INFORMATION

OGILVIE PRESS INC.,
BROOKLYN 17, N. Y.
REPROVAL NO. 440H

PREP. BY C.F. NASH 11-5-68CALCULATION
OR REPORT NO.

CHKD. BY _____

SECURITY INFORMATION

PAGE 22 OF 50

TITLE:

REANALYZE BOLTS FOR NEW GRAFOIL GASKET

$$\text{BOLT LOAD @ R.T.} = \frac{13805}{12} = 1150 \# \quad (\text{PAGE 28})$$

$$\text{BOLT LOAD @ } 2000^{\circ}\text{F} = \frac{5540 + 4602}{12} = 845 \# \quad (\text{PAGE 29})$$

$$\text{@ R.T. } f_z = \frac{1150}{.0362} = 31,768 \text{ psi}$$

FROM AEROSPACE STRUCTURAL METALS HANDBOOK
 $P_{ALL} = 2500 \#$ FOR A $\frac{1}{4}$ -20^{COATED} BOLT WHICH HAS
 A SMALLER STRESS AREA THAN THE $\frac{1}{4}$ -28.
 $\therefore \text{M.S.} = \frac{2500}{1150} - 1 = 1.2$ ON ULT.

@ 2000°F

$$f_z = \frac{845}{.0362} = 23,343 \text{ psi}$$

$$F_{ty} = 28,000 \text{ psi}$$

$$\text{M.S.}_y = \frac{28,000}{23,343} = \underline{.20} \text{ ON YIELD}$$

ALSO FROM THE SAME SOURCE AS ABOVE

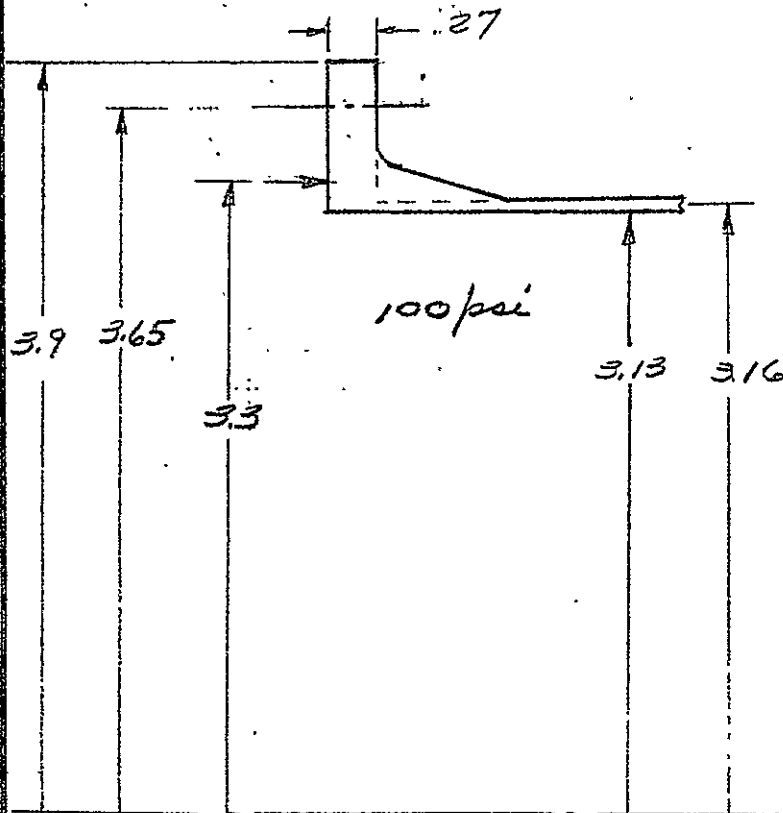
$$P_{ALL} = 1500 \# \text{ @ } 2000^{\circ}\text{F}$$

$$\therefore \text{M.S.}_u = \frac{1500}{845} - 1 = \underline{.77} \text{ ON ULT.}$$

PREP. BY: C.F. NASH 10-23-68	SECURITY INFORMATION	RE
CHKD. BY: G. PAGE 10/31/68		CALCULATION OR REPORT NO.
		PAGE 23 OF 50

TITLE:

FWD. FLANGE ANALYSIS



ASSUME GASKET LEAK
GASKET $p = 330/\text{psi.}$
(@ TEMP)

$$d-c = \frac{3.65}{-3.16} = .49$$

$$R(d-c) = \frac{5540(.49)}{2\pi(3.16)} = 137$$

$$\beta = \frac{1.285}{\sqrt{.06 \times 3.16}} = 2.95$$

$$K = \frac{.455}{(2.95)(3.16)} \left(\frac{.27}{.06} \right)^3 \ln \frac{3.9}{3.13} = .992$$

$$M_0 = \frac{137}{1 + \frac{2.95 \times .27}{2} + .992} = 57.3$$

$$P_0 = 2.95(57.3) = 169$$

$$f_{c \text{ FLANGE}} = \frac{-6(57.3)(.992)}{(.27)^2(.223)} - \frac{(169 - 100 \times .27)(3.5)^2}{3.13(.27)(3.9 - 3.13)}$$

$$= -21,000 \text{ psi} - 2680 \text{ psi} = -23680 \text{ psi}$$

$$N.G. F_{ty} = 8000 \text{ psi @ } 2500^\circ \text{F}$$

Thiokol CHEMICAL CORPORATION
REACTION MOTORS DIVISION
SENVILLE, NEW JERSEY

SECURITY INFORMATION

OGILVIE PRESS INC.,
BROOKLYN 17, N. Y.
REPROVAL NO. 440H

PREP. BY C.E. NASH 10-23-68

CHKD. BY G. FARE 11/31/68

SECURITY INFORMATION

CALCULATION
OR REPORT NO.

PAGE 24 OF 50

TITLE:

LET $h = .4$

$$K = .992 \left(\frac{.4}{.27} \right)^3 = 3.23$$

$$M_o = \frac{137}{1 + \frac{2.95(.4)}{2} + 3.23} = 27.8$$

$$P_o = 2.95(27.8) = 82.3$$

$$f_{c \text{ MOMENT}} = \frac{-6(27.8)(3.23)}{(.4)^2(.223)} = -15100 \text{ psi}$$

MOVE BOLTS IN. TO 3.57R, LET $h = .4$

$$R(d-c) = \frac{5540(3.57 - 3.16)}{2\pi(3.16)} = 115$$

$$B = 2.95 \quad K = 3.23$$

$$M_o = 27.8 \frac{115}{13.7} = 23.3$$

$$P_o = 2.95(23.3) = 68.8$$

$$f_{cM} = \frac{-6(23.3)(3.23)}{(.4)^2(.223)} = -12700 \text{ psi}$$

Thiokol CHEMICAL CORPORATION
REACTION MOTORS DIVISION
SENVILLE, NEW JERSEY

SECURITY INFORMATION

OGILVIE PRESS INC.,
BROOKLYN 17, N. Y.
REPROVAL NO. 440H

PREP. BY <u>G. F. NASH 10-23-68</u>	SECURITY INFORMATION	CALCULATION OR REPORT NO.
CHKD. BY <u>G. RABRE 10/31/68</u>		PAGE <u>25</u> OF <u>50</u>

RE

P 0

TITLE:

HEAT TRANSFER SECTION ESTIMATES THE
IFLANGE TEMPERATURE TO BE 2000°F RATHER
THAN 2500°F BASED ON CONSERVATIVE CALCULATIONS.

$$\begin{aligned} @ 2000^\circ\text{F} \quad F_{tu} &= 25,000 \text{ psi} \\ F_{ty} &= 18,000 \text{ psi} \end{aligned} \left. \begin{array}{l} \text{MIN.} \\ \text{GUAR.} \end{array} \right\} \text{(REF. - WAH CHANG ALBANY)}$$

LETTING $k = .4$ AND BOLT RADIUS = 3.57

$$f_c = -12,700 - \frac{(68.8 - 100 \times .40)(3.5)^2}{3.13(.4)(3.9 - 3.13)}$$

$$f_c = -12,700 - 366 = -13,066 \text{ psi}$$

$$M.S. = \frac{18000}{13066} - 1 = .38 \text{ ON YIELD}$$

SHELL STRESS WILL BE TAKEN CARE OF
BY TAPER, AT THE WALL,

$$f = \frac{6(23.3)}{(.24)^2} + \frac{5.540}{2\pi(3.25)(.24)} = 2430 + 1130 = 3560 \text{ psi}$$

OK

Thiokol CHEMICAL CORPORATION
REACTION MOTORS DIVISION
CINCINNATI, NEW JERSEY

SECURITY INFORMATION

OGILVIE PRESS INC.,
BROOKLYN 17, N. Y.
REPROVAL NO. 440H

PREP. BY C.P. NASH 10-31-68

CHKD. BY G. PAGE 10/31/68

SECURITY INFORMATION

CALCULATION
OR REPORT NO.

PAGE 26 OF 50

TITLE:

FWD. FLANGE ANALYSIS - 900 psi GASKET
PRESSURE AND
100 psi LEAK

$$R(d-c) = \frac{115 \times (3421 + 2120 \times \frac{900}{330})}{5540} = 191$$

$$M_o = 23.3 \times \frac{191}{115} = 38.7$$

$$f_{CM} = -12700 \times \frac{38.7}{23.3} = -21094 \text{ psi}$$

$$f_c = \frac{-(2.95 \times 38.7 - 100 \times .4)(3.5)^2}{3.13(.4)(3.9 - 3.13)} = -942$$

$$f_{c \text{ RING}} = -22036 \text{ psi}$$

SHELL

$$f = \frac{6(38.7)}{(.24)^2} + \frac{9203}{2\pi(3.25)(.24)} = 4031 + 1878$$

$$f = 5909 \text{ psi}$$

OK $F_{ey} = 40 \text{ ksi}$ } @ R.T. REF. WAI-CHANG ALBANY
 $F_{em} = 58 \text{ ksi}$

PREP. BY C.F. NASH 10-29-68CHKD. BY G. RABIE 11/31/68

SECURITY INFORMATION

CALCULATION
OR REPORT NO.PAGE 27 OF 50

RE:

TITLE:

FWD. FLANGE ANALYSIS - PROOF PRESSURE

$$h = .4 \quad t = .06$$

$$P = \pi (3.13)^2 (250) = 7694$$

$$P' = \pi (3.3^2 - 3.13^2) 250 = \frac{859}{8553}$$

$$G = .10 (8553) = 855$$

$$R(d-c) = \frac{(\overset{3770}{7694})(.49) + (\overset{374}{859}) \left(\frac{2 \times 3.65 - 3.13 - 3.3}{2} \right) + (\overset{399}{855})(3.65 - 3.3)}{2\pi (3.16)}$$

$$R(d-c) = 224$$

$$\beta = 2.95$$

$$K = 3.23$$

$$M_0 = \frac{224}{1 + \frac{2.95 \times .4}{2} + 3.23} = 46.5$$

$$P_0 = 2.95 (46.5) = 137$$

$$f_{cm} = \frac{-6 (46.5) (3.23)}{(.4)^2 (.223)} - \frac{(137 - 250 \times .4) (3.5)^2}{3.13 (.4) (3.9 - 3.13)}$$
$$= -25257 - 470 = -25727 \text{ psi}$$

SHELL STRESS

$$f = \frac{6 (46.5)}{(.24)^2} + \frac{250 \times 3.16}{2 (.24)} = 4844 + 1646 = 6490 \text{ psi}$$

$$\text{OK } F_{cy} = 40 \text{ ksi} \quad F_{cm} = 58 \text{ ksi} \quad @ \text{ R.T.}$$

Thiokol CHEMICAL CORPORATION
REACTION MOTORS DIVISION
SENVILLE, NEW JERSEY

SECURITY INFORMATION

OGILVIE PRESS INC.,
BROOKLYN 17, N. Y.
REPROVAL NO. 440H

PREP. BY C. F. NASH 11-5-68

RE

CHKD. BY

SECURITY INFORMATION

CALCULATION
OR REPORT NO.

PAGE 28 OF 50

TITLE:

REDESIGNED FLANGE GASKET

1. CHECK BOTH GRAFOIL GASKETS AT 900 psi WITH A LEAK OF 100 psi TO THE OUTSIDE GASKET.

(REF. p 26)

$$P = 9203^{\#}$$

$$P_g = 900\pi(3.38^2 - 3.13^2) = 4602$$

$$P_b = 13805^{\#}$$

$$R(d-c) = \frac{9203(3.57-3.16) + 4602 \left[\frac{2(3.57) - 3.13 - 3.38}{2} \right]}{2\pi(3.16)} = 263$$

$$\beta = 2.95$$

$$h = .42 \quad f = 3.87$$

$$K = \frac{.455}{2.95(3.16)} \left(\frac{.42}{.06} \right)^3 \ln \frac{3.87}{3.13} = 3.6$$

Michael CHEMICAL CORPORATION
REACTION MOTORS DIVISION
MOIVILLE, NEW JERSEY

SECURITY INFORMATION

OGILVIE PRESS INC.,
BROOKLYN 17, N. Y.
REPROVED NO. 4404

PREP. BY C. F. NASH 11-3-68

CALCULATION
OR REPORT NO.

CHKD. BY

SECURITY INFORMATION

PAGE 29 OF 50

TITLE:

$$M_0 = \frac{263}{1 + \frac{2.95(.42) + 3.6}{2}} = 50.4$$

$$P_0 = 2.95(50.4) = 149$$

$$f_{RING} = \frac{-6(50.4)(3.6)}{(.42)^2(.215)} - \frac{(149 - 100 \times .42)(3.5)^2}{3.13(.42)(3.87 - 3.13)}$$

$$= -28,704 - 1347 = -30,051 \text{ psi}$$

OK FOR BEGINNING
OF RUN, I.R. R.T.

ANALYZE HOT CONDITION WITH OUTER GASKET
PRESSURE = 900 #/IN² (DESIRED BY DESIGN DEPT)
INNER GASKET $p = 330 \text{ #/IN}^2$, 100 psi LEAK TO
OUTER GASKET.

$$\text{LET } h = .5$$

$$P = 5540$$

$$P' = 4602$$

$$R(d-c) = \frac{5540(3.57 - 3.16) + 1450}{2\pi(3.16)} = 187$$

$$K = \frac{.455}{2.95(3.16)} \left(\frac{.5}{.06} \right)^3 (.215) = 6.08$$

$$M_0 = \frac{187}{1 + \frac{2.95 \times .5}{2} + 6.08} = 24$$

PREP. BY C.F. NASH 11-5-68

CHKD. BY _____

SECURITY INFORMATION

CALCULATION
OR REPORT NO.PAGE 30 OF 50

TITLE:

$$f_{RING} = \frac{-6(24)(6.08)}{(.5)^2(.215)} - \frac{(24 \times 2.95 - 100 \times .5)(3.5)^2}{3.13(.5)(3.87 - 3.13)}$$

$$= -16288 - 220 = -16,508$$

@ 2000°F $F_{ty} = 18 \text{ ksi}$

$F_{tu} = 25 \text{ ksi}$

OK
3

PREP. BY C. L. NASH 10-24-69

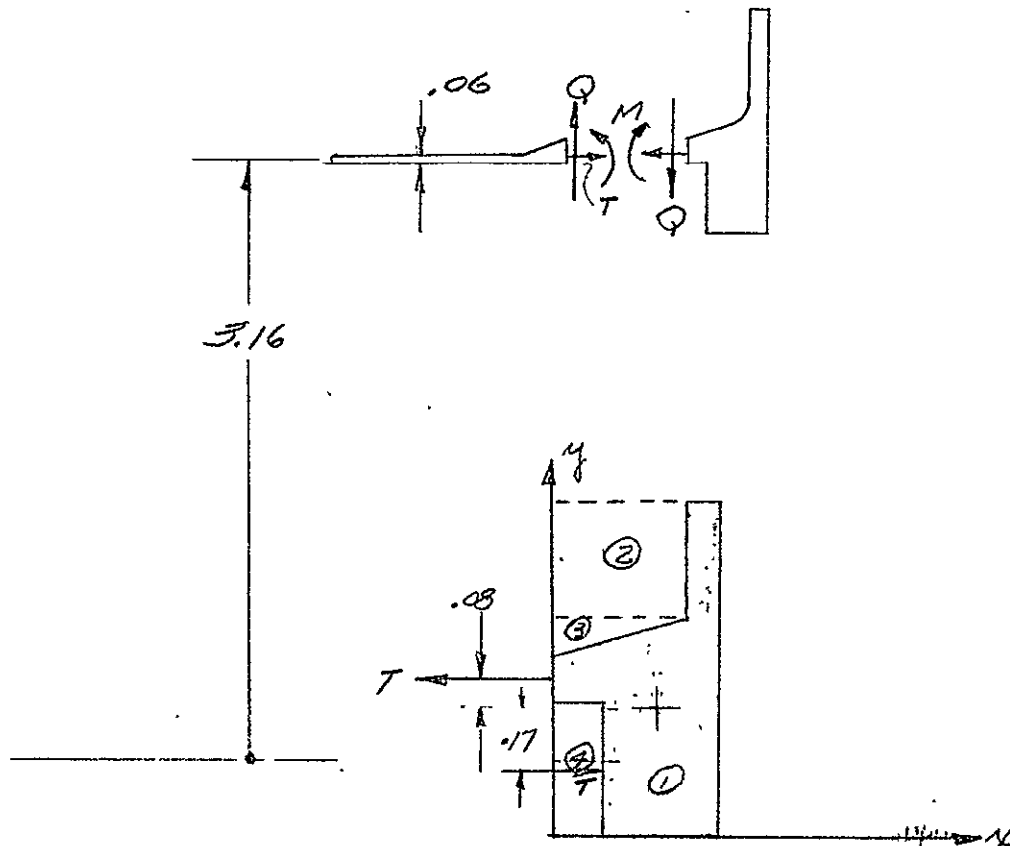
CHKD. BY G. PABE 10/24/69

SECURITY INFORMATION

CALCULATION
OR REPORT NO.

PAGE 31 OF 50

TITLE:

AFT FLANGE ANALYSIS

BODY	A	X	Y	AX	A.Y ²	AY	I _o
①	.43 x .87 = .374	.215	.435	.08041	.01729	.16269	$\frac{.43^3 \times .87}{12} = .00576$
②	.35 x .3 = .105	.175	.72	.01838	-.00322	-.0756	$\frac{.35^3 \times .3}{12} = -.00107$
③	$\frac{.35}{2} \times .1 = .018$	.117	.54	-.00210	-.00025	-.00972	$\frac{.35^3 \times .1}{12} = -.00012$
④	.13 x .35 = .046	.065	.175	-.00299	-.00019	-.00805	$\frac{.36}{12} \times .35 = -.00006$
	.205			.05694	.01363	.06932	.00451

$$I_{yy} = .00451 + .01363 = .01814$$

$$I_{cg} = .01814 - .205(.2778)^2 = .0023$$

$$\bar{x} = \frac{.05694}{.205} = .2778$$

$$\bar{y} = \frac{.06932}{.205} = .3381$$

Michael CHEMICAL CORPORATION
REACTION MOTORS DIVISION
DENVER, NEW JERSEY

SECURITY INFORMATION

OGILVIE PRESS INC.,
BROOKLYN 17, N. Y.
REPROVAL NO. 440H

PREP. BY C.F. NASH 10-24-68CHKD. BY G. RABE 11/31/68

SECURITY INFORMATION

CALCULATION
OR REPORT NOPAGE 32 OF 50

TITLE:

SHELL:

AXIAL LOAD T

$$\text{DUE TO PRESSURE} = \pi(3.3)^2(100) = 3421$$

(ASSUMES GASKET LEAK)

$$\text{DUE TO NEW GASKET} = 330\pi(2.65^2 - 2.22^2) = 2171$$

DESIGN

$$T = \frac{5592}{2\pi 3.16} = 282$$

$$\beta = \frac{1.285}{\sqrt{3.16(.06)}} = 2.95$$

$$\frac{D}{E} = \frac{.06^3}{10.92} = 19.78 \times 10^{-6}$$

$$\frac{E}{2D\beta^2} = \frac{10^6}{2(19.78)(2.95)^2} = 2905$$

$$\frac{E}{D\beta} = \frac{10^6}{19.78 \times 2.95} = 17138$$

$$\frac{E}{2D\beta^3} = 985$$

$$EW_p = - \left[\frac{100(3.16)}{.06} - \frac{.3(282)}{.06} \right] (3.16) = -12187$$

$$EQ = 2905Q + 17138M$$

$$EW = -12187 - 985Q - 2905M$$

PREP. BY C.F. NASH 10-24-63

CHKD. BY G. LARRE 10/31/68

SECURITY INFORMATION

CALCULATION
OR REPORT NO.

PAGE 33 OF 50

TITLE:

RING:

$$M_N = .25(382) + .28Q - M$$

$$Q_N = Q$$

$$EQ = \frac{M_N R^2}{I} = \frac{M_N (3.08)^2}{.0023} = 4125 M_N$$

$$EQ = 290,813 + 1155Q - 4125M$$

$$EW_c = \frac{Q(3.08)^2}{.205} = 46Q$$

$$\begin{aligned} EW_L &= 4.6Q + .2778(290,813 + 1155Q - 4125M) \\ &= 4.6Q + 80788 + 321Q - 1146M \\ &= 367Q - 1146M + 80,788 \end{aligned}$$

EQUATING RING TO SHELL

$$2905Q + 17138M - 1155Q + 4125M - 290813 = 0$$

$$1750Q + 21263M - 290813 = 0$$

$$-12187 - 985Q - 2905M - 367Q + 1146M - 80,788 = 0$$

$$-1352Q - 1759M - 92975 = 0$$

$$-1750Q - 2277M - 120,345 = 0$$

$$0 \quad 18986M = 411158$$

$$M = 21.66 \frac{\text{IN} \cdot \text{IN}}{\text{IN}}$$

Thiokol CHEMICAL CORPORATION
REACTION MOTORS DIVISION
GENEVILLE, NEW JERSEY

SECURITY INFORMATION

OGILVIE PRESS INC.,
BROOKLYN 17, N. Y.
REPROVAL NO. 440H

PREP. BY C.F. NASH 10-24-68

CHKD. BY G. PABE 10/21/68

SECURITY INFORMATION

CALCULATION
OR REPORT NO.

PAGE 34 OF 50

TITLE:

$$1750 Q = 290813 - 21263(21.66)$$

$$Q = -97 \text{ #/in.}$$

$$EW_L = 367(-97) - 1146(21.66) + 80788$$

$$EW_L = 20,367$$

$$\begin{aligned} EWR &= 46(-97) - .15(290813) - .15(1155)(-97) \\ &\quad + .15(4125)(21.66) \\ &= -17876 \end{aligned}$$

RING

$$\text{MAX STRESS } f = \frac{-20367}{3.08} = -6613 \text{ psi}$$

SHELL

$$\text{MAX STRESS } f = \frac{6(21.66)}{(.10)^2} + \frac{282}{.10} = 15,816 \text{ psi}$$

↑ THICKNESS AT GUT

$$\text{TEMP} = 2000^\circ \text{F}$$

$$F_{ty} = 18,000 \text{ psi}$$

$$F_{tm} = 25,000 \text{ psi}$$

$$M.S. = \frac{18000}{15816} - 1 = .14 \text{ ON YIELD}$$

INCREASE TAPERED SECTION TO GET MORE MARGIN.

Thickol. CHEMICAL CORPORATION
REACTION MOTORS DIVISION
DENVER, NEW JERSEY

SECURITY INFORMATION

OGILVIE PRESS INC.,
BROOKLYN 17, N. Y.
REPROVAL NO. 440H

PREP. BY: C.F. NASH

CHKD. BY: G. RABE 10/31/68

SECURITY INFORMATION

CALCULATION
OR REPORT NO.

PAGE 35 OF 50

TITLE:

CHECK CONDITION WHERE THE GASKET PRESSURE
IS 900 psi (BEGINNING OF RUN)

$$\begin{aligned} \text{TOTAL AXIAL FORCE} &= 900\pi(2.65^2 - 2.22^2) + 3421 \\ &= 5920 + 3421 = 9341 \# \end{aligned}$$

$$T = \frac{9341}{2\pi(3.16)} = 470 \#/\text{IN}$$

SHELL:

$$EQ = 2905Q + 17138M$$

$$EW_p = -\left[100(3.16) - .3(470)\right] \frac{3.16}{.06} = -9217$$

$$EW = -9217 - 985Q - 2905M$$

RING:

$$EQ = 484,000 + 1155Q - 4125M$$

$$EW_L = 367Q - 1146M + 134800$$

$$367Q - 1146M + 134800 + 9217 + 985Q + 2905M = 0$$

$$1352Q + 1759M + 144017 = 0$$

$$2905Q + 17138M - 484000 - 1155Q + 4125M = 0$$

$$1750Q + 21263M - 484000 = 0$$

$$-14668M = -517942$$

$$M = 35.31$$

$$1352Q = -144017 - 1759(35.31)$$

$$Q = -152.5$$

PREP. BY C.F. NASH 10-24-68
CHKD. BY G. RABE 10/31/68

SECURITY INFORMATION

RE
CALCULATION
OR REPORT NO.

PAGE 36 OF 50

TITLE:

RING STRESS:

$$E\sigma_L = 367(-152.5) - 1146(35.31) + 134800 \\ = 42700$$

$$f = -\frac{42700}{3.08} = -13864 \text{ psi}$$

SHELL STRESS:

$$f = \frac{6(35.31)}{(1)^2} + \frac{470}{.1} = 25886 \text{ psi}$$

OK $F_{61} = 40,000 \text{ psi}$ @ RT (TIME WHEN
 $F_{61} = 58,000 \text{ psi}$ $P_6 = 900 \text{ psi}$)

PREP. BY <u>G. KARE</u> <u>10/31/68</u>	SECURITY INFORMATION	CALCULATION OR REPORT NO.
CHKD. BY <u>C. NASH</u> <u>10-31-68</u>		PAGE <u>37</u> OF <u>50</u>

RE

PC

TITLE:

AFT FLANGE

FOR PROOF PRESSURE = 260 #/in²

SHELL

$$E_{WP} = - \frac{.85 (260)(3.16)^2}{.06} = -36780$$

$$E_{\Theta} = 17138 M + 2905 Q$$

$$E.W = -2905 M - 985 Q - 36780$$

RING

$$M_N = \frac{250 (3.16) (.25)}{2} + .28 Q - M$$

$$E_{\Theta_L} = 4125 M_N$$

$$= -4125 M + 1155 Q + 407344$$

$$E.W_L = -1146 M + 367 Q + .2778 (407344)$$

$$= -1146 M + 367 Q + 113160$$

EQUATING RING TO SHELL

$$\textcircled{1} \quad 21263 M + 1750 Q - 407344 = 0$$

$$\textcircled{2} \quad -1759 M - 1352 Q - 149940 = 0$$

$$\textcircled{2} \quad \frac{1750}{1352} - 2277 M - 1750 Q - 194079 = 0$$

Thiokol CHEMICAL CORPORATION
REACTION MOTORS DIVISION
CENYILLE, NEW JERSEY

SECURITY INFORMATION

OGILVIE PRESS INC.,
BROOKLYN 17, N. Y.
REPROVAL NO. 440H

PREP. BY <u>G. KARE 10/31/68</u> CHKD. BY <u>C. NASH 10-31-68</u>	SECURITY INFORMATION	RE CALCULATION OR REPORT NO. PAGE <u>38</u> OF <u>50</u>
TITLE: $18986 M = 601423$ $M = 31.68 \text{ IN} - \# / \text{IN}$ $Q = \frac{149940 + 1759(31.68)}{-1352} = -152 \text{ \# / IN}$ $E_{WL} = 21071$ RING STRESS $f_{\text{MAX}} = \frac{-21071}{3.08} = -6841 \text{ \# / IN}^2$ SHELL STRESS $f_{\text{MAX}} = \frac{6(31.68)}{(.1)^2} + \frac{260(3.16)}{(2)(.01)}$ $= 19010 + 4108 = 23118 \text{ \# / IN}^2$ $M.S._y = \frac{40000}{23118} - 1 = \underline{+.73}$		

PREP. BY C. F. NASH 10-25-68

CHKD. BY G. RABE 10/21/68

SECURITY INFORMATION

CALCULATION
OR REPORT NO.

PAGE 39 OF 50

TITLE:

RADIAL THERMAL GROWTH IN THE PLANE
OF THE ATJS FLANGE

$$\text{ATJS: } T = \frac{8 + 79 + 81}{3} = 3315$$

$$R_o = 2.45$$

REF. UNION CARBIDE
CORP., TECH INF
BUL. No. 463-201 IG

$$\Delta = 7.8 \times 10^{-3} \frac{\text{IN}}{\text{IN}} \text{ FOR } R_o \text{ (ACROSS GRAIN)}$$

$$\Delta R = 7.8 \times 10^{-3} \times 2.45 = .019$$

P.B. OUTER LINER:

$$T = \frac{36 + 43 + 50}{3} = 2795$$

$$t = .7$$

$$\Delta \epsilon'' = 40 \times 10^{-3} \text{ IN/IN}$$

REF. - HIGH TEMPERATURE
MATERIALS INC.
P.B. DATA SHEET

$$\Delta t = .7 \times 40 \times 10^{-3} = .028 \text{ IN.}$$

COLUMBIUM:

REF. - WAN
CHANG
ALBANY

$$T = 2000^\circ \text{F (HEAT TRANSFERS EST. OF ACTUAL T)}$$

$$\alpha = 4.0 \times 10^{-6} \text{ IN/IN/}^\circ \text{F} \quad R = 3.13$$

$$\Delta R = 3.13 (4 \times 10^{-6}) (2000) = .025$$

$$\therefore \text{RADIAL INTERFERENCE} = .019 + .028 - .025 = .022 \text{ IN.}$$

PREP. BY C.F. NASH 10-28-68CHKD. BY G. LABBE 10/31/69

SECURITY INFORMATION

CALCULATION
OR REPORT NO.

PAGE 40 OF 50

TITLE:

CIRCUMFERENTIAL GROWTH OF P.G.

INNER P.G. IN PLANE OF NOZZLE

$$\text{INNER CIRC.} = 2\pi(1) = 6.28$$

$$T = 5827^{\circ}\text{F}$$

$$\Delta_{\frac{1}{2}}'' = .09 \quad \text{REF. HIGH TEMPERATURE MATL INC.}$$

$$\Delta C = 6.28 \times .09 = .565$$

$$\text{OUTER CIRC.} = 2\pi(2.15) = 13.51$$

$$T = 5520^{\circ}\text{F}$$

$$\Delta_{\frac{1}{2}}'' = .085$$

$$\Delta C = 13.51(.085) = 1.15$$

CIRCUMFERENTIAL
GRAFOIL
FILLER SHEETS
MUST DEFLECT
THESE AMOUNTS
TO ALLOW FOR
CIRCUMFERENTIAL
GROWTH.

OUTER P.G. IN PLANE OF NOZZLE

$$\text{INNER CIRC.} = 2\pi(2.28) = 14.326$$

$$T = 5056^{\circ}\text{F}$$

$$\Delta_{\frac{1}{2}}'' = .007 \quad \left\{ \begin{array}{l} \text{REF. SUPER-} \\ \text{TEMP CORP.} \end{array} \right.$$

$$\Delta C = 14.326(.007) = .10$$

$$\text{OUTER CIRC.} = 2\pi(3.12) = 19.60$$

$$T = 2037$$

$$\Delta_{\frac{1}{2}}'' = .0018 \quad \left\{ \begin{array}{l} \text{REF. SUPER-} \\ \text{TEMP CORP.} \end{array} \right.$$

$$\Delta C = 19.60 \times .0018 = .035$$

PREP. BY G. LABE 10/23/68

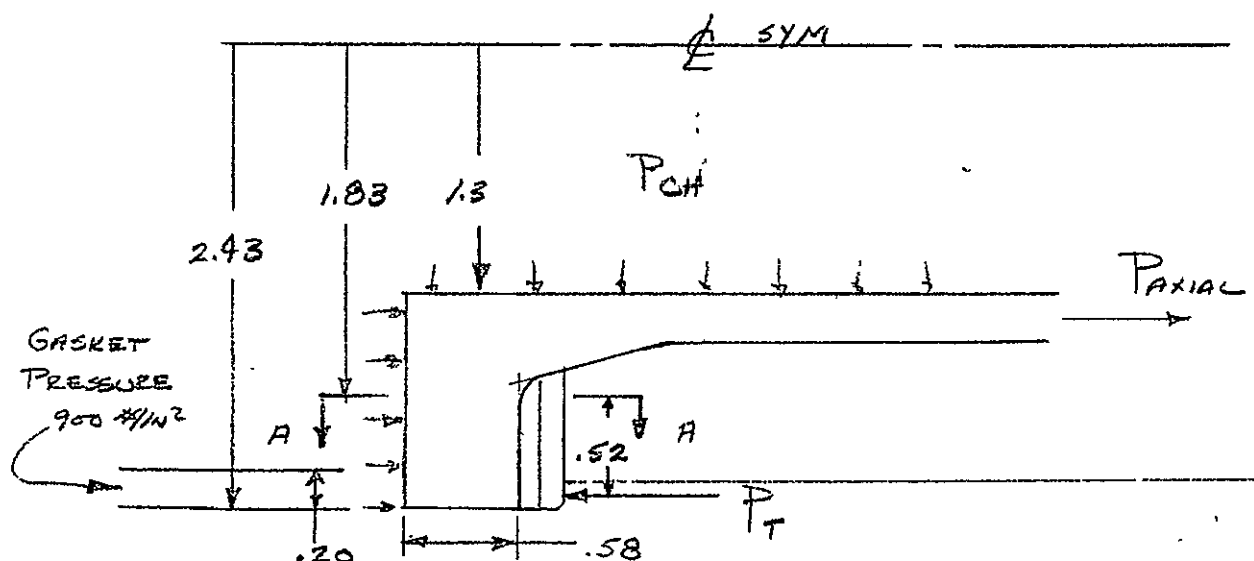
CHKD. BY C. NASH 10-31-68

SECURITY INFORMATION

**CALCULATION
OF REPORT NO.**

PAGE 41 OF 50

TITLE:



$$T_{\text{THRUST}} (\text{SEA LEVEL}) = 125 \#$$

$$F_{CH} = 100 \text{ #/in}^2$$

$$P_{\text{AXIAL}} = \pi (1.3)^2 (100) - 125 = 531 - 125 = 406 *$$

AT START $P_{CH} = 200 \text{ #/in.}^2$

$$P_{AXIAL} = 812 \text{ 呎}$$

$$P_T = 812 + (200)\pi\left(\frac{3.23^2}{2.23} - 1.3^2\right) + (900)\pi\left(\frac{1.93^2}{2.43} - 2.23^2\right)$$

$$= 812 + 2060 + 2630 = 5502 *$$

Nichol. CHEMICAL CORPORATION
REACTION MOTORS DIVISION
CONVILLE, NEW JERSEY

SECURITY INFORMATION

OGILVIE PRESS INC.,
BROOKLYN 17, N. Y.
REPROVAL NO. 440H

PREP. BY G. LARBE 10/23/68
 CHKD. BY C. NASH 10-31-68

SECURITY INFORMATION

CALCULATION
OR REPORT NO.

PAGE 42 OF 50

TITLE:

SECTION A-H

$$M_{A-H} = \frac{5502(.52)}{2\pi(1.83)} - \frac{2630(.5)}{2\pi(1.83)} - \frac{200(.4)^2}{2}$$

$$= 249 - 115 - 16 = 118 \text{ IN-#/IN}$$

$$f_{b_{A-H}} = \frac{6(118)}{(.58)^2} = 2105 \text{ #/IN}^2$$

FLANGE ANALYSIS

DIMENSIONS (IN.)

$$P = 812 \text{ #}$$

$$b = 1.3$$

$$h = .58$$

$$P' = 2060 \text{ #}$$

$$C = 1.42$$

$$t = .25$$

$$G = 2630 \text{ #}$$

$$d = 2.35$$

$$a = \frac{2.43 + 1.3}{2}$$

$$e = 2.33$$

$$= 1.86$$

$$f = 2.43$$

$$R(d-e) = \frac{812 \left(\overset{.93}{2.35 - 1.42} \right) + 2060 \left(\overset{.535}{\frac{4.7 - 1.3 - 2.33}{2}} \right) + 2630 \left(\overset{.02}{2.35 - 2.33} \right)}{2\pi(1.42)}$$

$$= \frac{755 + 1100 + 52.6}{8.93} = \frac{1907.6}{8.93} = 214 \text{ IN-#/IN}$$

$$\beta = \frac{1.285}{\sqrt{1.42(.25)}} = 2.16$$

$$K = \frac{.455}{(2.16)(1.42)} \left(\frac{.58}{.25} \right)^3 \ln \frac{2.43}{1.3}$$

$$= .1485 (12.5) (.625) = .116$$

PREP. BY G. KABE 10/23/68
CHKD. BY C. NASH 10-31-68

SECURITY INFORMATION

RE
CALCULATION
OR REPORT NO.

PAGE 43 OF 50

TITLE:

FLANGE ANALYSIS (CONT.)

$$M_0 = \frac{214}{1 + \frac{2.16(.58)}{2} + 1.16} = \frac{214}{2.785} = 76.7 \text{ IN-}\frac{\text{#}}{\text{IN}}$$

$$f_t \text{ WALL} = \frac{6(76.7)}{(.45)^2} + \frac{812}{2\pi(1.42).45}$$

$$= 2280 + 202 = 2482 \text{ #/IN}^2$$

$$f_c \text{ FLANGE} = -\frac{6(76.7)1.16}{(.58)^2(.625)} - \frac{[2.16(76.7) - 200(.58)](1.86)^2}{1.3(.58)(2.43-1.3)}$$

$$= -2540 - 203 = -2743 \text{ #/IN}^2$$

$$M.S. \text{ BENDING} = \frac{5000}{2482} - 1 = +1.01$$

$$M.S. \text{ COMPRESSION} = \frac{12000}{2743} - 1 = +3.37$$

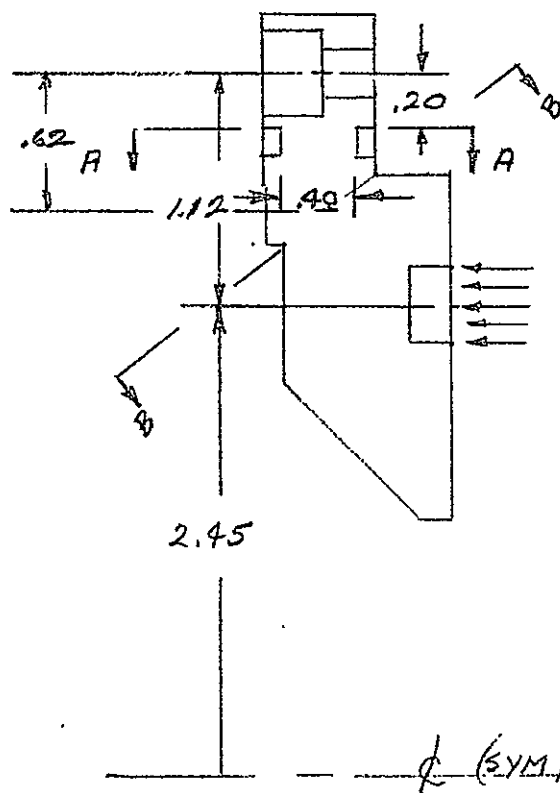
PREP. BY: G. RABE 10/24/68CHKD. BY: C. NASH 10-31-68

SECURITY INFORMATION

CALCULATION
OR REPORT NO.PAGE 44 OF 50

TITLE:

INSULATOR BLOCK DURING INSTALLATION

BOLT HEAD
DIAMETER900 #/in²

MATERIAL - SILICA PHEUSUC

 $F_{LU} = 14000 \text{ #/in}^2 @ \text{R.T.}$ REF. POLYMERIC
CHEM.
FM-5067

$$M_{RING} = 900 (.4) 2\pi (2.45) (1.12) = 6207 \text{ IN-}\cancel{\text{#}}$$

$$\frac{I}{c} = \frac{.112}{.150} = .224 \quad (\text{REF. NEXT PAGE})$$

$$f_b = \frac{6207 \cancel{\text{REF}}}{2\pi \cancel{\text{REF}} (.224)} = 4410 \text{ #/in}^2$$

$$MS. = \frac{14000}{4410} - 1 = + 2.17$$

{ REF - POLYMERIC CHEMICALS INC.
DATA SHEET FM-5067

Thiokol CHEMICAL CORPORATION
REACTION MOTORS DIVISION
DENVER, NEW JERSEY

SECURITY INFORMATION

OGILVIE PRESS INC.,
BROOKLYN 17, N. Y.
REPROVAL NO. 440H

PREP. BY G. KARR 10/21/68
CHKD. BY C. NASH 10-31-68

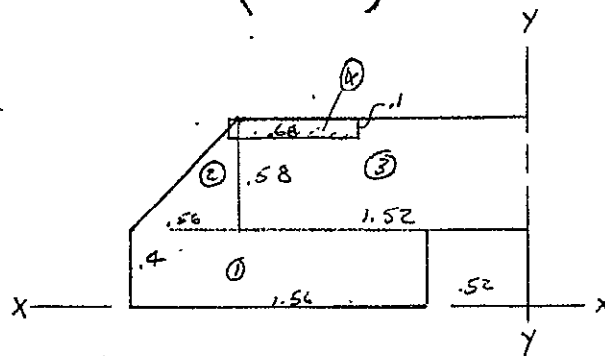
SECURITY INFORMATION.

CALCULATION
OR REPORT NO.

PAGE 45 OF 50

TITLE:

INSULATOR BLOCK (CONT.)



ITEM	A	x	y	Ax	Ay	Ay ²	I _{ax}
1	$(.4)(.56) = .624$	1.30	.2	.811	.1248	.02496	$\frac{1.56(.4)^3}{12} = .00832$
2	$\frac{.58(.56)}{2} = .1624$	.76	.59	.123	.0958	.05653	$\frac{.56(.58)^3}{36} = .00304$
3	$.58(1.52) = .8816$	1.71	.69	1.508	.6083	.41973	$\frac{1.52(.58)^3}{12} = .02471$
4	$.4(.68) = .068$	1.22	.93	-.083	-.0632	-.05881	$-\frac{.68(.1)^3}{12} = -.00006$
Σ	1.60			2.359	.7657	.44241	.003601

$$\bar{X} = \frac{2.359}{1.6} = 1.474 \text{ in.} \quad \bar{Y} = \frac{.7657}{1.6} = .4786 \text{ in.}$$

$$I_{xx} = .03601 + .44241 - .4786(.7657) = .112 \text{ in.}^4$$

BOLT STRESS

$$P = \frac{6207}{1.12(12)} = 461 \text{ *}$$

$$f_t = \frac{461}{.0362} = 12800 \text{ #/in}^2 \text{ NOT CRITICAL}$$

PREP. BY <u>G. KARE</u> <u>10/24/68</u>	SECURITY INFORMATION	CALCULATION OR REPORT NO.
CHKD. BY <u>C. NASH</u> <u>10-31-68</u>		PAGE <u>46</u> OF <u>50</u>

TITLE:

INSULATOR BLOCK (CONT.)

SECTION A-A

$$f_{b A-A} = \frac{(461)(.20)(6)}{2 \frac{(63)}{.21} (.4)^2} = 2744 \text{ #/in}^2$$

$$M.S. = \frac{17000}{2744} - 1 = + \underline{4.10}$$

$$f_s = \frac{461(12)}{2\pi(3.2)(.4)} = 688 \text{ #/in}^2$$

O.K.

SECTION B-B

$$f_{b B-B} = \frac{461(12)(.22)6}{2\pi(2.95)(.6)^2} = \pm 3084 \text{ #/in}^2$$

$$f_{c B-B} = \frac{461(12)\sqrt{.7^2 - .4^2}}{2\pi(2.95)(.6)(.6)} = -371 \text{ #/in}^2$$

$$M.S. = \frac{14000}{3084 + 371} - 1 = + \underline{3.05}$$

PREP. BY G. KABE 10/25/68
 CHKD. BY C. NASH 10-31-68

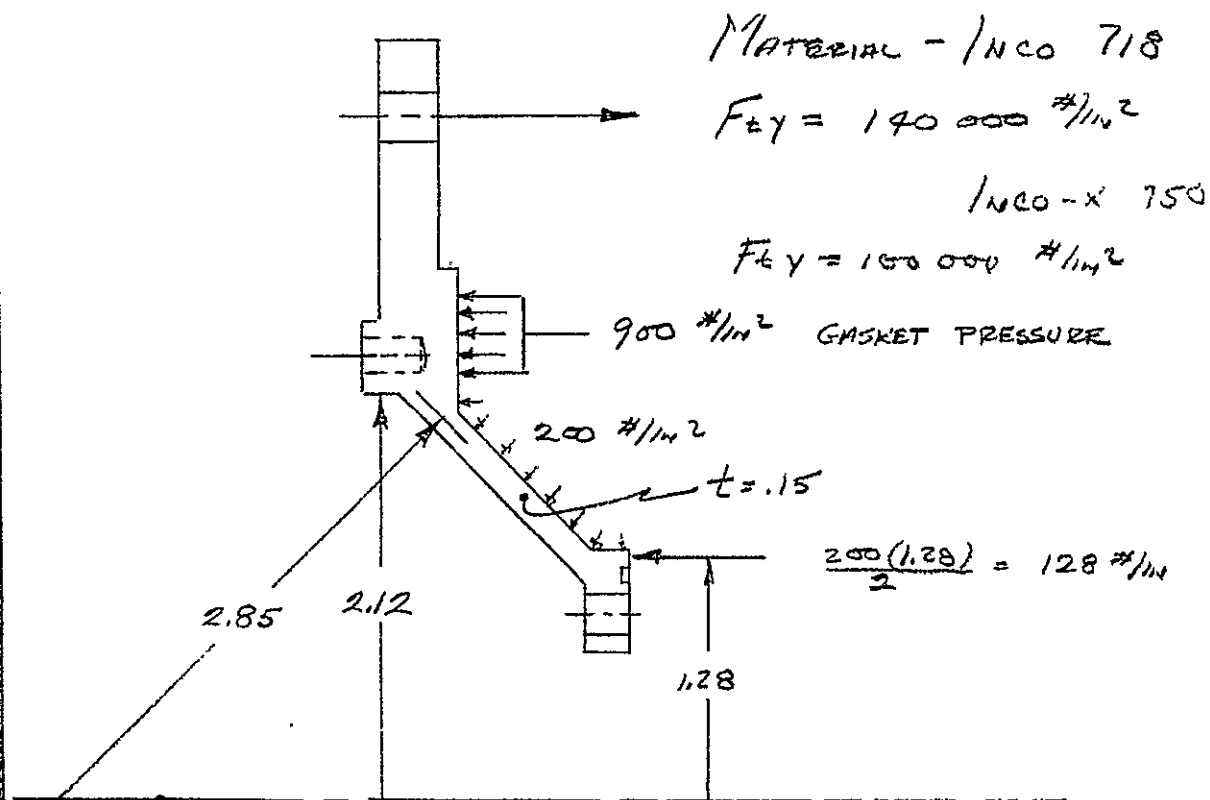
SECURITY INFORMATION

CALCULATION
OR REPORT NO.

PAGE 47 OF 50

TITLE:

INJECTOR PLATE



CONE

$$S_2 = \frac{200(2.85)}{.15} = 3800 \text{ #/in}^2 \text{ NOT CRIT.}$$

PREP. BY G. FARE 10/25/68
CHKD. BY C. NASH 10-31-68

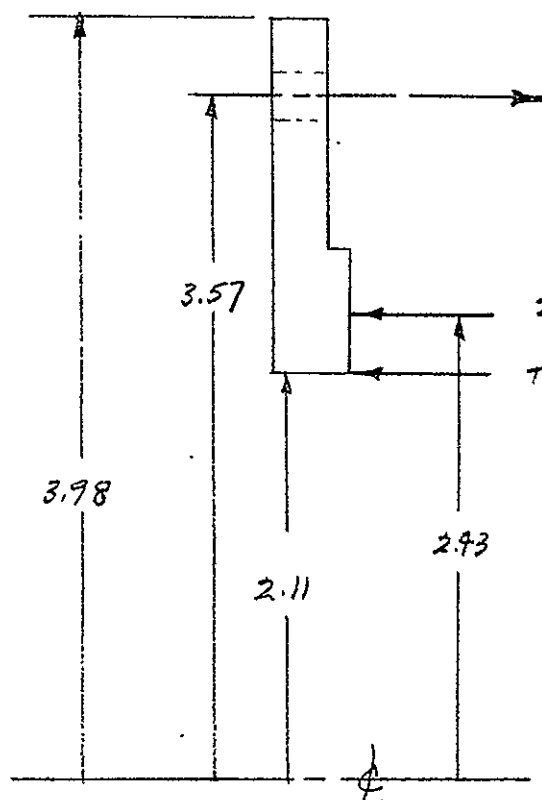
SECURITY INFORMATION

CALCULATION
OR REPORT NO.

PAGE 48 OF 50

TITLE:

INJECTOR PLATE (CONT.)



$$2\pi (2.43) 900 (.4) = 5490 *$$

$$\pi (2.11)^2 (200) = 2800 *$$

FOR LOAD AT INNER EDGE

$$S_t = \frac{3 (2800)}{2\pi (3.33) (.4)^2} \left[\frac{2(3.98)^2 (4.33)}{3.98^2 - 2.11^2} \cdot \frac{.525}{2.11} + 2.33 \left(\frac{3.57^2 - 2.11^2}{3.98^2 - 2.11^2} \right) \right]$$

$$= 2500 (6.38 + 1.70) = 20200 */in^2$$

FOR THE GASKET LOAD

$$S_t = \frac{3 (5490)}{2\pi (3.33) (.4)^2} \left[\frac{2(3.98)^2 (4.33)}{11.38} \cdot \frac{.386}{2.43} + \frac{2.33 (3.57^2 - 2.43^2)}{11.38} \right]$$

$$= 4920 (4.65 + 1.40) = 29800 */in^2$$

Thiokol CHEMICAL CORPORATION
REACTION MOTORS DIVISION
GENEVILLE, NEW JERSEY

SECURITY INFORMATION

OGILVIE PRESS INC.,
BROOKLYN 17, N. Y.
REPROVAL NO. 440H

RE

PC

PREP. BY <u>G. KARE</u> <u>10/25/68</u>	SECURITY INFORMATION	CALCULATION OR REPORT NO.
CNKD. BY <u>C. NASH</u> <u>10-31-68</u>		PAGE <u>49</u> OF <u>50</u>

TITLE:

INJECTOR PLATE (CONT.)

$$S_{t \text{ TOTAL}} = 20200 + 29800 = 50000 \text{ #/IN}^2$$

$$M.S. = \frac{100000}{50000} - 1 = \underline{+ 1.00}$$

PREP. BY G. KARE 10/31/68
CHKD. BY C. NASH 10-31-68

SECURITY INFORMATION

CALCULATION
OR REPORT NO.

PAGE 50 OF 50

TITLE:

PROOF PRESSURE

ASSUME PRESSURE ACTS ON
Cb WALL DUE TO GASKET
LEAK

$$P_{\text{PROOF}} = 100 (1.15) \frac{F_{ty \text{ RTI}}}{F_{ty \text{ 2500 } ^\circ\text{F}}}$$

$$P_{\text{PROOF}} = \frac{115 (40,000)}{18,000} = 255 \text{ #/in}^2$$

USE $P_{\text{PROOF}} = 250 - 260 \text{ #/in}^2$

~~Trichlor~~ CHEMICAL CORPORATION
REACTION MOTORS DIVISION
DOXVILLE, NEW JERSEY

SECURITY INFORMATION

OGILVIE PRESS INC.,
BROOKLYN 17, N. Y.
REPROVAL NO. 440H