# THERMODYNAMIC AND TRANSPORT PROPERTIES OF FROZEN AND REACTING $\mathrm{pH}_{2}-\mathrm{oH}_{2}$ MIXTURES 

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#### Abstract

Application of experimental state data and spectroscopic term values shows that the thermodynamic and transport properties of reacting $\mathrm{pH}_{2}-\mathrm{oH}_{2}$ mixtures are considerably different than those of chemically frozen $\mathrm{pH}_{2}$ at temperatures below $300^{\circ} \mathrm{R}$. Such differences will be significant from the standpoint of nuclear rocket design if it turns out that para- to orthohydrogen conversion can be catalyzed by radiation in the cold dense phase. Calculated H-S data also show that radiation-induced $\mathrm{pH}_{2}-\mathrm{oH}_{2}$ equilibration at constant enthalpy can produce a temperacure drop of at least $28^{\circ} \mathrm{R}$, corresponding to an ideal shaft work loss of $15 \%$ or more for a turbine operating downstream from the point of conversion. Aside from differences in thermodynamic and transport properties, frozen $\mathrm{pH}_{2}-\mathrm{oH}_{2}$ mixtures may differ from pure $\mathrm{pH}_{2}$ on a purely hydrodynamical basis.


## Significance of Possible ParaOrthohydrogen Conversion in Nuclear Rockets

Hydrogen is generally a mixture of two distinct $\mathrm{H}_{2}$ components. A molecule of the component called "orthohydrogen" may assume quantized rotational energies that are not accessible to the component called "parahydrogen," and vice versa. The resulting disparities in energy-level populations at a given temperature imply differences in the thermodynamic and transport properties of the two types of hydrogen. Thus, for example, the enthalpies and thermal conductivities of $\mathrm{pH}_{2}-\mathrm{oH}_{2}$ mixtures differ appreciably from those of pure parahydrogen in the $36^{\circ} R-500^{\circ} \mathrm{R}$ range, not only in absolute magnitude but also in temperature
dependence. Aside from thermodynamic and transport properties, para- and orthohydrogen may differ on a purely hydrodynamical basis. The latter possibility, which has been given little attention, derives from the fact that the differences in accessible rotational energies for the two types of molecule are associated with differences in angular momenta.

The liquid hydrogen that is stored for use in nuclear rocket propulsion is usually over $99 \% \mathrm{pH}_{2}$. However, the high-temperature hydrogen gas that emerges from the nozzle of the nuclear rocket is invariably a mixture consisting of $75 \% \mathrm{oH}_{2}$ and $25 \% \mathrm{pH}_{2}$. This change in proportions results from the facts that (1) certain chemical or magnetic
reactions can convert parahydrogen to orthohydrogen when sufficient energy is available, and (2) in the presence of a suitable conversion catalyst, hydrogen tends to a $\mathrm{pH}_{2} / \mathrm{oH}_{2}$ ratio that is determined by the temperature. Catalysts which convert parahydrogen to its equilibrium proportions are available in the reactor core (in the form of H -atoms from thermal dissociation), if not elsewhere. When catalysts are present in large enough quantities that a shift in temperature is accompanied, practically instantaneously, by a shift in $\mathrm{pH}_{2}$ / $\mathrm{oH}_{2}$ ratio to a value corresponding to the new temperature, the para-orthohydrogen mixture is called "reacting" or "equilibrating." When no such catalysts are available, the $\mathrm{pH}_{2} / \mathrm{oH}_{2}$ ratio is not affected by a temperature change, and the mixture is called "frozen." In the temperature range from $60^{\circ} \mathrm{R}$ to $300^{\circ} \mathrm{R}$ the specific heats of a given nominal $\mathrm{pH}_{2} / \mathrm{OH}_{2}$ mixture differ radically according to whether the hydrogen is frozen or reacting.

In nuclear rocket design, a question arises as to what type of hydrogen should be assumed to exist in the relatively cold regions between the propellant tank and the core inlet. If the hydrogen is chemically frozen throughout this region, then it obviously remains in almost pure $\mathrm{pH}_{2}$ form, and thermodynamic and heat transfer calculations can be based on parahydrogen properties. If, on the other hand, the flowing hydrogen is catalysed by radiation or by paramagnetic surfaces, then the hydrogen may be chemically reacting over at least part of the region below the reactor core, and pure parahydrogen properties may not apply. From the standpoint of an overall design study, the effect of catalytic conversion is not limited to the values of thermodynamic and transport properties of hydrogen at a prescribed temperature and pressure. The sudden equilibration of hydrogen due to catalysis at a certain point in the flow-path can reduce the temperature by as much as $40^{\circ} \mathrm{R}$, through a thermochemical process that is analogous to the cooling of paramagnetic salts in a decreasing magnetic field. Such "conver-sion-cooling" can reduce the available energy for a turbine operation or alter the dimensions of various orifices for an optimum design.

Whether hydrogen conversion in the subcore region is of design significance depends on three questions. These are: (1) does an effective mechanism for conversion actually exist in relatively cold hydrogen
subject to irradiation and possible encounters with paramagnetic sites, and how much conversion can it produce? (2) What are the quantitative thermodynamic and transport properties of frozen and reacting $\mathrm{pH}_{2} / \mathrm{oH}_{2}$ mixtures? (3) What is the overall effect of conversion on a specific design? In regard to the first question, it will only be noted that data obtained during practical tests indicate that relatively cold parahydrogen can be converted by radiation, and that reasonable chemical models have been advanced to explain this effect. The third question is in the province of rocket designers. The results given here pertain only to the second question, viz., information on the basic properties of $\mathrm{pH}_{2}-\mathrm{oH}_{2}$ mixtures.

## Equilibrium Orthohydrogen Fraction

The equilibrium orthohydrogen fraction at a given temperature is independent of pressure, at least for pressures in the range of nuclear rocket application and lower. For temperatures below $500^{\circ} \mathrm{K}\left(900{ }^{\circ} \mathrm{R}\right)$ the equilibrium orthohydrogen fraction, $\omega_{e}$, is given to an accuracy of $0.01 \%$ by
$\omega_{e}=\sum_{j=1}^{7}$ (odd) $g_{j} e^{-\theta_{j} / T} / \sum_{j=0}^{8} g_{j} e^{-\theta_{j} / T}$
where $j$ is the number of a rotational level. Even and odd values of j correspond to $\mathrm{pH}_{2}$ and $\mathrm{oH}_{2}$ rotational levels, respectively. The parameter $\theta_{j}$ represents the molecular rotational energy of a particular level divided by Boltzmann's constant. Using the spectroscopic term values cited in the definitive work of Woolley, et al. at NBS (Ref. 1), it is found that a suitable approximation is

$$
\begin{align*}
\theta_{j}\left({ }^{\mathrm{O}} \mathrm{~K}\right)= & 85.3757 \mathrm{j}(\mathrm{j}+1)-0.065769 \mathrm{j}^{2}(\mathrm{j}+1)^{2} \\
& +0.0000712 \mathrm{j}^{3}(\mathrm{j}+1)^{3} \tag{2}
\end{align*}
$$

for values of $j$ less than or equal to 8. This prescription ignores the role of vibrational excitation, which is negligible below $500^{\circ} \mathrm{K}$. The parameter $\mathrm{g}_{j}$ in Equation (1) is a statistical weight given by
$g_{j}=3(2 j+1), j$ odd
$=(2 j+1), j$ even
At temperatures above $T=500^{\circ} \mathrm{K}$, the equilibrium orthohydrogen fraction is $\omega_{e}=$ 0.750 .

Evaluation of Equation (1) yields the dependence of equilibrium orthohydrogen fraction on temperature shown in Figure 1. It is seen that the temperature range over which $\omega_{\mathrm{e}}$ varies significantly is $30^{\circ} \mathrm{K}$ to $220^{\circ} \mathrm{K}$, or $54^{\circ} \mathrm{R}$ to $396^{\circ} \mathrm{R}$.

## Calculation of Enthalpy and Entropy

The calculation of enthalpies and entropies is obviated by expressing the results as ideal gas values, augmented by "realgas" terms that arise from intermolecular reactions. The latter are obtained from an equation of state, which is usually written in the form of a temperature and density dependent for the compressibility factor $Z=\mathrm{pv} / \mathrm{RT}$. In obtaining the present results it has been assumed that the equation of state

$$
\begin{equation*}
Z=Z(T, \rho) \tag{4}
\end{equation*}
$$

is the same for either para- or orthohydrogen. The state equation used is that given by Wooley et al. for normal hydrogen ( $75 \%$ ortho). This state equation, which was based on rather old normal hydrogen data, has been compared with data reported more recently by Michels et al. (Ref. 2). Typical comparisons are shown in Figure 2. An analysis of the difference between the old and new data, which is taken as a measure of the present uncertainty in the state equation for normal hydrogen, shows that the corresponding uncertainties in enthalpy and energy of normal hydrogen are respectively only about $1 \mathrm{Btu} / 1 \mathrm{~b}$ and 0.002 $\mathrm{Btu} / 1 \mathrm{~b}{ }^{\mathrm{O}} \mathrm{R}$. Furthermore, recent data by Hermans et al. (Ref. 3), on the difference between the second virial coefficients of para- and normal hydrogen, indicate that the use of a normal hydrogen state equation on $\mathrm{pH}_{2}-\mathrm{oH}_{2}$ mixtures will not lead to an error greater than that corresponding to the present uncertainty in the normalhydrogen state data.

The real-gas enthalpies and entropies of a number of mixtures have been calculated using tabular data given by Woolley et al. to obtain the integrals involving $Z$. Ideal-gas values of the enthalpy and entropy for both frozen and reacting $\mathrm{pH}_{2}-\mathrm{OH}_{2}$ mixtures have been obtained from the $\theta_{j}$ and $g_{j}$ defined in Equations (2) and (3).



The enthalpies of frozen $\mathrm{pH}_{2}$, frozen $\mathrm{oH}_{2}$ and equilibrating hydrogen at 0 and 800 psi are shown in Figure 3. The corresponding specific heats, obtained by differentiation of $H$ with respect to temperature, are shown in Figure 4. It is seen that $\mathrm{EH}_{2}$ behaves as a mixture with an intermediate specific heat only above $100^{\circ} \mathrm{K}$; at lower temperatures the specific heat of reacting hydrogen is appreciably higher than that of either frozen component. By contrast, the specific heat of a frozen mixture is obtained by simply calculating the average of the frozen $\mathrm{pH}_{2}$ and $\mathrm{oH}_{2}$ values, weighted by their respective concentrations in the mixture.


## Transport Properties

The viscosity of a $\mathrm{pH}_{2}-\mathrm{OH}_{2}$ mixture is determined by transport of momentum alone, and is therefore independent of the $\mathrm{pH}_{2}-$ $\mathrm{oH}_{2}$ composition insofar as $\mathrm{pH}_{2}$ and $\mathrm{OH}_{2}$ conform to the same equation of state. On the other hand, the thermal conductivity of an ideal-gas mixture of para- and orthohydrogen is related to the viscosity, $\eta$, by Eucken's relation

$$
\begin{equation*}
\mathrm{K}_{\mathrm{o}}=(9 \gamma-5) \mathrm{C}_{\mathrm{v}}^{0} \eta /(4 \mathrm{M}) \tag{5}
\end{equation*}
$$

where $C^{\circ}$ is the specific heat of the ideal gas, $\gamma$ is the ratio of specific heats, and $M$ is the molecular weight. The realgas thermal conductivity K is related to $\mathrm{K}_{\mathrm{o}}$ by the following Enskog relation:

$$
\begin{equation*}
\mathrm{K} / \mathrm{K}_{\mathrm{o}}=1+0.575 \mathrm{E}+0.5017 \mathrm{E}^{2}-0.204 \mathrm{E}^{3} \tag{6}
\end{equation*}
$$

where $E$ is given by

$$
\begin{equation*}
E=Z-1+T\left(\frac{\partial Z}{\partial T}\right)_{\rho} \tag{7}
\end{equation*}
$$

Figure 5 shows the thermal conductivity for $\mathrm{pH}_{2}, \mathrm{OH}_{2}$ and a reacting mixture at 0 psi and 800 psi . As in the case of specific heat, the thermal conductivity depends strongly on whether a given mixture is frozen or reacting.



## Cooling Due to Conversion

If a chemically frozen parahydrogen gas is suddenly exposed to a conversion-catalyst such as radiation or a paramagnetic surface, the resulting equilibration to a $\mathrm{pH}_{2}-\mathrm{oH}_{2}$ mixture is an irreversible process. Hence, the reaction cannot be isentropic even if it happens to be adiabatic. In general, the enthalpy change due to a differential conversion process is
$\mathrm{dH}=\mathrm{TdS}+\mathrm{Vdp}+\mu_{1} \mathrm{dx}_{1}+\mu_{2} \mathrm{dx}_{2}$
where $\mathrm{x}_{1}$ and $\mathrm{x}_{2}$ are the $\mathrm{pH}_{2}$ and $\mathrm{oH}_{2}$ mole fractions, respective $1 y$, and where $\mu_{1}$ and $\mu_{2}$ are the chemical potentials. In the case where no heat enters or leaves the system and the pressure is kept at a constant value, Equation (8) simplifies to

$$
\begin{equation*}
\operatorname{TdS}=\left(\mu_{1}-\mu_{2}\right) \mathrm{dx}_{2} \tag{9}
\end{equation*}
$$

This increase in entropy is accompanied by a decrease in temperature, which can, for example, subsequently reduce the amount of available energy from a turbine operating between two prescribed pressures. The possible effect of such cooling is seen from the approximate $H-S$ chart shown in Figure 6, which has been constructed from Figure 3 and calculated entropy data. When parahydrogen at $297^{\circ} \mathrm{R}$ is converted to $60 \% \mathrm{oH}_{2}$ at constant enthalpy and constant pressure, the temperature decreases from $297^{\circ} \mathrm{R}$ to $269^{\circ} \mathrm{R}$. If conversion had not occurred, the energy available to a turbine operating between 975 psi and 675 psi would be $111 \mathrm{Btu} / 1 \mathrm{~b}$. However, it is seen that $60 \%$ conversion would reduce the available energy to $98 \mathrm{Btu} / \mathrm{lb}$. The magnitudes of such losses depend upon the inlet enthalpy and, of course, the amount of conversion that is assumed. Figure 7 shows the percent loss in ideal energy for an assumed conversion of $60 \%$ as a function of inlet enthalpy.

## Possible Hydrodynamic Differences Between $\mathrm{pH}_{2}$ and $\mathrm{oH}_{2}$

The difference between the thermodynamic and transport properties of parahydrogen and those of orthohydrogen are completely specified by the rotational energy leve1s accessible to each, at least insofar as the two modifications conform to the same equation of state. However, from the hydrodynamical standpoint, another type of difference might be worth exploring.

Parahydrogen molecules may take intrinsic angular momenta of $0,2 \mathrm{~h}, 4 \mathrm{~K}$, etc.; whereas orthohydrogen molecules may take intrinsic angular momenta of $\hbar, 3 k, 5 k$, etc. At temperatures below $180^{\circ} \mathrm{R}$, over $97 \%$ of all parahydrogen molecules are in a state of zero angular momentum. For practical purposes one may say that, at these temperatures, parahydrogen is a fluid composed of molecules with no intrinsic angular momentum, whereas orthohydrogen is a fluid whose molecules have an intrinsic angular momentum of $\hbar$. Hence, on a rigorous hydrodynamical basis (Ref. 4), the equations for energy and momentum conservation, which are sufficient to describe the behavior of a parahydrogen fluid, must be augmented by an equation of angular momentum in the case of orthohydrogen. In the language of transport theory, collisions between orthohydrogen molecules involve an extra summational invarient. It is therefore conceivable that the details
of such phenomena as the transition from laminar to turbulent flow might differ in the two types of fluids, independently of any effects associated with thermodynamic and transport properties.



## References

1. Woolley, H. W., Scott, R. B., and Brickwedde, F. G., NBS Research Paper RP1932, Volume 41, November 1948, pp. 379-475.
2. Michels, A., et al., Physica 25, 1959, pp. 25-42.
3. Hermans, L. J. F., et al., Physica 31, 1965, pp. 1567-1574.
4. Chapman, S., and Cowling, T. G., The Mathematical Theory of Non-Uniform Gases (Cambridge), 1953, p. 202.
