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PROGRAM FOR CALCULATION OF THERMODYNAMIC
AND TRANSPORT PROPERTIES OF COMPLEX
CHEMICAL SYSTEMS (NASA)

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**FORTRAN IV COMPUTER PROGRAM
FOR CALCULATION OF THERMODYNAMIC
AND TRANSPORT PROPERTIES OF
COMPLEX CHEMICAL SYSTEMS**

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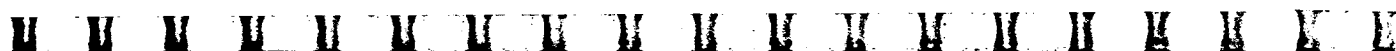
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FORTRAN IV COMPUTER PROGRAM FOR CALCULATION OF THERMODYNAMIC AND TRANSPORT PROPERTIES OF COMPLEX CHEMICAL SYSTEMS

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SUMMARY

A FORTRAN IV computer program for the calculation of the thermodynamic and transport properties of complex mixtures is described. This program (TRAN72) was developed by combining a program for the transport properties calculation with another program (CEC71), published in NASA SP-273, for the thermodynamic properties calculation.

Equations for the calculation of the transport properties are given and explained. Equations for the calculation of the thermodynamic properties can be found in NASA SP-273. Input data, included with the program, are explained.

The program has the capability of performing calculations such as (1) chemical equilibrium for assigned thermodynamic states, (2) theoretical rocket performance for both equilibrium and frozen compositions during expansion, (3) incident and reflected shock properties, and (4) Chapman-Jouguet detonation properties. Condensed species, as well as gaseous species, are considered in the thermodynamic calculations. However, only gaseous species are considered in the transport property calculations.

The program is available for external distribution. Further information on obtaining the program may be had from the authors.

INTRODUCTION

Many processes in existence today involve complex chemical mixtures, frequently at high temperatures. Some of these mixtures result from combustion processes such as occur in automobiles, aircraft, and rockets. Others occur in processing equipment in the chemical, petroleum, and natural-gas industries. Research equipment, such as shock tubes, also involves high-temperature gas mixtures.

The need frequently arises for the thermodynamic and transport properties of these mixtures, particularly for use in heat- and mass-transfer calculations. Usually, the temperatures of the gases involved are quite high, too high for the properties to be measured directly. Consequently, the properties are calculated. As a result, a number of different computer programs have been written for the property calculations. In general, most of the programs now in existence are designed to calculate either the thermodynamic properties or the transport properties, but not both. These programs are not reviewed herein. References 1 to 4 are a starting point for a review of the programs for calculating the thermodynamic properties. Some programs have also been written for calculating the transport properties (refs. 5 to 9); however, each has its limitations. Some of these programs use approximate equations (refs. 5 to 8). One is limited in the choice of the intermolecular potential energy function (ref. 7). Two programs are designed primarily for ionized gases (refs. 8 and 9).

We have developed a computer program which is designed to avoid these limitations. Rigorous equations are used in the transport calculations, and the transport cross sections are not restricted to any specific potential energy form. The program is a general one, capable of handling any chemical system. However, it does not include ionization, although it is capable of handling incipient ionization. Other important features of this program include simplicity of input, storage of all thermodynamic and transport property data on a master tape, and elimination of any need for advance knowledge of which species will be important. The program is a combination of the NASA Lewis Research Center Chemical Equilibrium Calculations Program (ref. 1) with additional routines to do the transport property calculations. The program will handle a variety of problems. It has the capability for doing calculations such as (1) chemical equilibrium for assigned thermodynamic states (T,P), (H,P), (S,P), (T,V), (U,V), or (S,V); (2) theoretical rocket performance for both equilibrium and frozen compositions during expansion; (3) incident and reflected shock properties; and (4) Chapman-Jouguet detonation properties.

The thermodynamic properties which are tabulated include pressure, temperature, density, enthalpy, entropy, molecular weight, $(\partial \ln V / \partial \ln P)_T$, $(\partial \ln V / \partial \ln T)_P$, specific heat at constant pressure, isentropic exponent, sonic velocity, and composition. The calculated transport properties are viscosity and thermal conductivity. Specific heat and thermal conductivity are calculated for both frozen and equilibrium conditions. Prandtl and Lewis numbers are included. Other properties which are characteristic of the type of problem being run are also calculated. (See the sample problems in appendix D.)

The present report does not cover the equations and numerical techniques used for the calculation of the thermodynamic properties. These are given in NASA SP-273 (ref. 1), which discusses the details of the thermodynamic calculations. The present report does give the equations used in the transport calculations, however. These are

covered in the section TRANSPORT PROPERTY EQUATIONS. Sources of the transport data are given in the section SOURCES OF TRANSPORT AND RELAXATION DATA. Symbols are defined in appendix A. Variables, indices, and constants used in the transport subroutines are given in appendix B. A listing of the entire program is shown in appendix C, and sample problems are shown in appendix D. The sample problems were selected to illustrate many of the various capabilities of the program. Flow charts of some routines are included.

COMPUTER PROGRAM

The TRAN72 computer program was written in FORTRAN IV. At the Lewis Research Center it was checked out on an IBM 7094II/7044 Direct Couple System. It has been used to generate both thermodynamic and transport properties of a number of chemical systems for internal use at Lewis.

The source program is available to other organizations. Thermodynamic and transport data are provided with the program. However, these data are updated periodically; as a result, the answers for the sample problems in appendix D may change somewhat from time to time.

Further information on obtaining the program may be had from the authors.

ASSUMPTIONS AND CAPABILITIES

The program is designed to provide both thermodynamic and transport properties for a wide range of scientific and engineering applications and for a range of independent variables. Thermodynamic data for a large number of ideal gases and condensed species are provided with the program for a temperature range of 300 to 5000 K. Transport data are provided over a wider range in many cases. See the section SOURCES OF TRANSPORT AND RELAXATION DATA for the temperature range for each interaction.

The range of applicability of the thermodynamic calculations is approximately described by the limits of applicability of the ideal-gas law. A reduced-state plot of the thermodynamic properties might give the user an idea of the limits of temperature and pressure. The lower limit for temperature in the transport calculations occurs when ternary and higher order molecular collisions become important. This also defines the upper pressure limit for the transport property calculations. The upper limit for temperature occurs when ionization becomes appreciable. However, incipient ionization can be included in the calculations. But, for increasing ionization, higher approximations are needed in the transport calculations (refs. 10 and 11). Additional comments on this may be found in the discussion of the transport property equations. The lower pressure



limit is given by the onset of the free molecular flow regime, which occurs when the mean-free-path length is of the same order of magnitude as the dimensions of the container. Under these conditions the equations for the transport properties are no longer applicable.

In the computation of the thermodynamic properties the NASA Lewis Research Center CEC71 program (ref. 1) is used. The usual equations for the conservation of mass, momentum, and energy are applied (ref. 1, eqs. (93) to (95)) and the ideal-gas law is assumed. The free energy is minimized by using a Newton-Raphson iteration technique. Composition and properties are calculated for equilibrium conditions and, for some situations, for frozen conditions (sometimes called nonreacting). The effects of chemical kinetics, or finite reaction rates, are not included. TRAN72 handles the same types of problems as does CEC71, including normal shock waves, Chapman-Jouguet detonations, rocket expansion problems, and properties at assigned thermodynamic states. The additional assumptions for each type of problem are as follows:

(1) Shock waves are of negligible thickness and normal to the direction of flow. One-dimensional flow is assumed.

(2) For Chapman-Jouguet detonations the Mach number of the wave front, based on the speed of sound in the burned gas, is unity. The assumptions mentioned previously for shock waves also apply.

(3) For rocket combustion problems, it is assumed that there is complete mixing in the chamber, adiabatic combustion at constant pressure, isentropic expansion with complete mixing, and frictionless one-dimensional flow. It is also assumed that the chamber is large enough that the velocity in the chamber is negligible.

Because of storage limitations on the IBM 7094, the maximum allowable number of species is 100 and the maximum number of elements is 10. This applies to the thermodynamic property calculations and includes gases, liquids, and solids. In doing the transport calculations, no more than 20 of the species are used. First the composition obtained from the thermodynamic calculations is searched for the 20 gaseous species with the largest concentrations. However, all gaseous species with mole fractions of less than 10^{-7} are omitted. Then this gaseous composition is normalized by summing the concentrations of these 20 species and dividing each concentration by the sum. The mole fractions obtained by this normalization procedure are the ones used in the transport property calculations.

DESCRIPTION OF PROGRAM INPUT

The procedure for operating the program is relatively simple and is almost identical to that for operating the CEC71 program (ref. 1).



The input specifies the type of problem to be run, the chemical system of interest, the mixture ratio, and the range of variables. Considerable flexibility is available in specifying the variables. For example, in a rocket combustion problem, nozzle expansion points can be specified as pressure ratios, area ratios, or a combination of both. In addition, a number of options are available, such as the following:

(1) The calculated thermodynamic and transport properties may be obtained on punched cards, as well as printed output.

(2) For rocket and shock problems, both equilibrium and frozen properties are available. In particular, for rocket expansion problems, freezing can be made to occur at the chamber, the throat, or any supersonic point in the nozzle. For this type of problem, equilibrium flow is assumed from the chamber to a previously designated station in the nozzle. After that station is reached, the composition is frozen.

(3) Input can be specified in a number of different units. For instance, pressure can be given in mm Hg, atmospheres, psia, or newtons/meter².

(4) Species may be omitted from consideration in the calculations through the use of OMIT cards. Also, certain condensed phases may be included in the initial composition through the use of INSERT cards. Otherwise, only gases are considered initially, which may lead to convergence difficulties.

(5) Thermodynamic property calculations can be obtained without including transport property calculations. If this option is used, the program is essentially the same as the CEC71 program. The opposite is not possible. Transport properties cannot be calculated without first doing the thermodynamic property calculations, since the results of the thermodynamic calculations are needed in the transport calculations.

The input data are discussed under four categories. Three of the categories are required and one is optional. The three required categories and the code names by which they are referred to herein are

(1) Library of thermodynamic and transport data for reaction products

(THERMO and TRANSPORT data library)

(2) Data pertaining to reactants (REACTANTS cards)

(3) Namelist data, which include the type of problem, required schedules, and options (NAMELISTS input)

The optional category of data is the list of chemical formulas of species which are singled out for special purposes (OMIT and INSERT cards).

Each category of data is discussed in this report. Many of the details are summarized in tables I to VI. Both input and output for 10 sample cases are given in appendix D. These cases are identified by the numbers 51, 52, 122, 123, 679, 950, 1207, 1565, 5612, and 6666. The order of the input is indicated in table II.

THERMO and TRANSPORT Data Library

A library of thermodynamic and transport data is included with each program distributed. The thermodynamic data for reaction products are in the functional form discussed in the section THERMODYNAMIC DATA. The transport data are in a tabular form. The order and format of the THERMO and TRANSPORT data are detailed in table I.

THERMO and TRANSPORT data may be read either from cards or from tape. If the data are read from cards, the program will write these data on logical tape 4. However, a permanent tape or disk containing the data may be made during any run by using the required type of control cards preceding the operating deck. When the data are read from cards, the data are preceded by a code card which has the word THERMO punched in columns 1 to 6. The sample cases in appendix D assume a permanent tape is available. Thus, the THERMO code card and the data are omitted and the input data all start with the REACTANTS cards described in the next section. When data for various species are added, removed, or changed on the tape, the whole set of THERMO and TRANSPORT data cards must be included in the input for making a new tape.

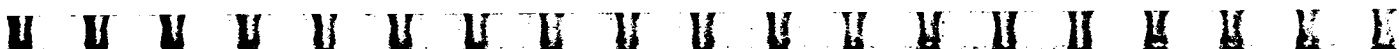
These TRANSPORT data follow immediately after the END card for the THERMO data. No general identification card is needed to indicate the beginning of the TRANSPORT data.

During a computer run, the appropriate reaction-product data consistent with each new set of REACTANTS cards will be automatically selected from the data on tape 4 and stored in core.

REACTANTS Cards

This set of cards is required for all problems. The first card in the set contains the word REACTANTS punched in card columns 1 to 9. The last card in the set is blank. In between the first and last cards may be any number of cards to a maximum of 15, one for each reactant species being considered. The cards for each reactant must give the chemical formula and the relative amount of the reactant. For some problems, enthalpy values are required. The format and contents of the cards are summarized in table III. A list of some REACTANTS cards is given in table IV.

Relative amounts of reactants. - The relative amounts of reactants may be specified in several ways. They may be specified in terms of moles, mole fraction, or mole percent (by keypunching M in card column 53) or in terms of weight, weight fraction, or weight percent (blank in column 53). For example, in appendix E, cases 679 and 1207 specify reactants in terms of moles and case 51 specifies them in terms of weight.



For these cases, the relative amounts of the reactants are completely specified by the values on the REACTANTS cards. However, there are optional variables which may be set in namelist INPT2 that indicate relative amounts of total fuel to total oxidants. (See table V and section NAMELISTS input.) For this situation, each reactant must be specified as a fuel or an oxidizer by keypunching an F or O, respectively, in column 72 of the REACTANTS card. The amounts given on the REACTANTS cards are relative to total fuel or total oxidant rather than to total reactant.

Tables V, VI, and VII describe the namelists. Referring to table V, there are four options in INPT2 for indicating relative amounts of total fuel to total oxidant. They include

- (1) Equivalence ratio, r (ERATIO is TRUE)
- (2) Oxidant-to-fuel weight ratio, O/F (OF is TRUE)
- (3) Fuel percent by weight, $\%F$ (FPCT is TRUE)
- (4) Fuel-to-air or fuel-to-oxidant weight ratio, F/A (FA is TRUE)

For each option, the values are given in the MIX array of INPT2. This feature is illustrated by cases 52, 122, 950, 5612, and 6666 in appendix D. Cases 52 and 950 show where ERATIO is TRUE (ERATIO = T), and the reactants are identified as fuel or oxidant in card column 72. Since these cases involve just one fuel and one oxidant, the amounts of each (as given in columns 46 to 52) are shown as 100. This means that the oxidizer is 100 percent of the total oxidizers and the fuel is 100 percent of the total fuels. Cases 122 and 5612 are examples which have more than one fuel. Case 122 shows that each fuel is 50 percent (by weight) of the total fuels and the one oxidizer is 100 percent of the total oxidizer.

The purpose of the previous namelist variables is to permit using one set of reactant cards with any number of values (maximum, 15) of a variable. Case 950, for example, specifies three values of equivalence ratio (ERATIO = T).

Reactant enthalpy. - Assigned enthalpy values for initial conditions are required for assigned enthalpy and pressure (HP), rocket (RKT), detonation (DETN), and shock (SHOCK) problems. An assigned internal energy is required for the assigned internal energy and volume (UV) problem. These assigned values for the total reactant are calculated automatically by the program from the enthalpies or internal energies of the individual reactants. The enthalpy values for the individual reactants are either keypunched on the REACTANTS cards or calculated from the THERMO data. The choice varies according to the type of problem as follows:

- (1) RKT, UV, and HP problems: Enthalpies or internal energies are taken from the REACTANTS cards unless zeros are punched in card columns 37 and 38. For each REACTANTS card with the "00" code, an enthalpy will be calculated for the species from the THERMO data for the temperature given in card columns 64 to 71. See MgO(s) in case 51, appendix D.

(2) SHOCK problems: Enthalpies for all the reactants are calculated from the THERMO data for the temperatures in the T schedule of namelist INPT2 (table V). If enthalpy values are punched in card columns 64 to 71 (table III), they will be ignored. It is not necessary to punch zeros in card columns 37 and 38.

(3) DETN problems: If no T schedule is given in namelist INPT2, the option for calculating reactant enthalpies is the same as for RKT, UV, and HP problems. However, if a T schedule is given in INPT2, the enthalpies will be calculated from the THERMO data for the temperatures in the T schedule, the same as for the SHOCK problem.

When the program is calculating the individual reactant enthalpy or internal energy values from the THERMO data, the following two conditions are required:

(1) The reactant must also be one of the species in the set of THERMO data. For example, $\text{NH}_3(\text{g})$ is in the set of THERMO data but $\text{NH}_3(\text{l})$ is not. Therefore, if $\text{NH}_3(\text{g})$ is used as a reactant, its enthalpy could be calculated automatically but that of $\text{NH}_3(\text{l})$ could not be.

(2) The temperature T must be in the range $T_{\text{low}}/1.2 \leq T \leq T_{\text{high}} \times 1.2$, where T_{low} to T_{high} is the temperature range of the THERMO data.

NAMELISTS Input

As indicated in table II, the NAMELISTS code card precedes the NAMELISTS input. The card has the word NAMELISTS punched in card columns 1 to 9. All problems require an INPT2 input. Rocket and shock problems each require an additional set, namely RKTINP or SHKINP. The additional set simply follows INPT2 directly.

The variables in each namelist are listed in tables II, V, VI, and VII. Table II indicates which variables are required and which are optional for the various types of problems. Tables V, VI, and VII give a brief definition of each variable. Some additional information about some of these variables follows:

Pressure units. - The program assumes the pressure in the P schedule to be in units of atmospheres unless either PSIA = T, NSQM = T, or MMHG = T.

Relative amounts of fuel (or fuels) and oxidizer (or oxidizers). - These quantities may be specified by assigning 1 to 15 values for either O/F, %F, F/A, or r. If no value is assigned for any of these options, the program assumes the relative amounts of fuel (or fuels) and oxidizer (or oxidizers) to be those specified on the REACTANTS cards. (See discussion in section REACTANTS Cards.)

Printing mole fractions of trace species. - The program normally prints only the compositions of those species with mole fractions greater than 5×10^{-6} in F-format for all problems except SHOCK. The TRACE option permits printing smaller mole fractions. If the variable TRACE is set to some positive value, mole fractions greater than or equal

to this value will be printed. When this option is used, a special E-format for mole fraction output is used automatically. A TRACE value of 1.E-38 is the lowest value allowed by the program. (See case 1565 in appendix E.)

For SHOCK problems, mole fractions of trace species are often desired. Thus, for SHOCK problems, the program will set TRACE to 5.E-9 automatically, and the E-format for output is always used. This value may be changed by using the TRACE option in INPT2 namelist input. (See case 1207 in appendix E.)

TP, HP, SP, TV, UV, or SV problems. - In these problems, from 1 to 52 values of T, and from 1 to 26 values of P or V (or RHO) may be assigned. However, only one value of entropy S0 may be assigned in INPT2 for the SP or SV problem. Only one value of enthalpy is permitted for the HP problem, and only one value of internal energy is permitted for the UV problem. However, these values of enthalpy and internal energy are not assigned in INPT2 but are calculated by the program. In a TP problem, if 52 values of T and 26 values of P are assigned in INPT2, properties will be calculated for the 1352 possible P and T combinations. Similarly, as many as 1352 combinations can be calculated for a TV problem.

DETN problem. - Calculations will be made for all combinations of initial pressure P and initial temperature T. Initial temperatures may be specified in INPT2 namelist or on the REACTANTS card.

RKT problem. - At least one chamber pressure value P is required in INPT2, although as many as 26 chamber pressures may be assigned. A complete set of calculations will be made for each chamber pressure. The RKT problem requires a second namelist for input, RKTINP, which is discussed in the next section.

RKTINP namelist (RKT problem only). - This namelist is required for RKT problems. It follows the INPT2 namelist. A list of variables and definitions is given in table VI. Even though this namelist is required, all variables are optional. If no variables are assigned, only the chamber and throat conditions will be calculated. Usually, a pressure ratio schedule (PCP), an area ratio schedule (SUBAR or SUPAR), or some combination of these schedules will be assigned.

Pressure ratio and area ratio schedules must not include values for the chamber and throat, inasmuch as these values are calculated automatically by the program. If both a pressure ratio schedule and an area ratio schedule are given in RKTINP, the pressure ratios will be calculated first. If both schedules are omitted, only chamber and throat conditions will be calculated.

The program will calculate both equilibrium and frozen performance, unless RKTINP has the logical variable FROZ set equal to FALSE (FROZ = F) or the logical variable EQL set equal to FALSE (EQL = F). If FROZ = F, only equilibrium performance will be calculated. If EQL = F, only frozen performance will be calculated.

If a frozen expansion is being calculated, it is possible to specify the freezing point by using the variable NFZ. For instance, to freeze immediately after the fifth point, set



NFZ = 5. If NFZ is not specified in the RKTINP namelist, the program assigns NFZ = 1 (freezing in the chamber). If NFZ = 1 or 2 (NFZ = 2 corresponds to the throat), 22 additional stations may be assigned in the expansion. If NFZ > 2, the program will allow only 11 additional stations. Freezing is permitted in the chamber, the throat, or any supersonic station but not at a subsonic station.

SHOCK problem. - The program requires a P and T schedule in INPT2, and a schedule of either initial velocities (U1) or Mach numbers (MACH1) in a second namelist, SHKINP (see table VII). These values of P, T, and either U1 or MACH1 all refer to the unshocked gas and must correspond one-to-one with each other. Case 1207 in appendix D is a shock problem. The pressure and temperature schedules are limited to 13 values for SHOCK problems only. This corresponds to the 13-value limit for U1 or MACH1 schedules.

REACTANTS cards must be only for gaseous reactants that are also included as reaction species in the THERMO data. This permits the program to calculate enthalpy and specific-heat values of the reactants from the THERMO data.

SHKINP namelist (SHOCK problem only). - A list of variables and definitions is given in table VII. SHKINP must include from one to 13 values of either U1 or MACH1 of the unshocked gas. The program will calculate incident shock parameters that assume both equilibrium and frozen composition unless SHKINP has the logical variable INCDEQ set equal to FALSE (INCDEQ = F) or the logical variable INCDFZ set equal to FALSE (INCDFZ = F). If INCDEQ = F, only frozen composition will be used. If INCDFZ = F, only equilibrium composition will be used. In addition, there are options for calculating reflected shock parameters. For each incident condition called for, reflected shock parameters will be calculated that assume either a frozen composition (REFLFZ = T), an equilibrium composition (REFLEQ = T), or both (REFLFZ = T, REFLEQ = T).

OMIT and INSERT Cards

As indicated in table II, OMIT and/or INSERT cards may follow the REACTANTS cards. Their inclusion is optional. They contain the names of particular species in the library of thermodynamic data for the specific purposes to be discussed. Each card contains the word OMIT (in card columns 1 to 4) or INSERT (in card columns 1 to 6) and the names of from one to four species starting in columns 16, 31, 46, and 61. The names must be exactly the same as they appear in the first 12 columns of the THERMO data cards (see table I).

OMIT cards. - Occasionally, it may be desired to specifically omit one or more species from consideration as possible species. This omission may be accomplished by means of OMIT cards containing these species names. See appendix D, cases 51 and 950.



If OMIT cards are not used, the program will consider as possible species all those species in the THERMO data which are consistent with the chemical system being considered.

INSERT cards. - These cards contain the names of condensed species only. They have been included as options for the following two reasons:

The first and more important reason for including the INSERT card option is that, in rare instances, it is impossible to obtain convergence for assigned enthalpy problems (HP or RKT) without the use of an INSERT card. This occurs because the temperature sometimes becomes extremely low (several kelvin) when only gases are considered. In these rare cases, the use of an INSERT card containing the name of the required condensed species will eliminate this kind of convergence difficulty. When this difficulty occurs, the following message is printed by the program: "LOW TEMPERATURE IMPLIES CONDENSED SPECIES SHOULD HAVE BEEN INCLUDED ON AN INSERT CARD."

The second and less important reason is for efficiency of computation. If it is known that certain condensed species will be present among the final equilibrium compositions for the first assigned point, a small amount of computer time can be saved by using an INSERT card. The inserted condensed species will then be considered by the program during the initial iterations for the first assigned point. If the INSERT card were not used, only gaseous species would be considered during the initial iterations. However, after convergence, the program would automatically insert the appropriate condensed species and reconverge. For all other assigned points the inclusion of condensed species is handled automatically by the program. Therefore, it usually is immaterial whether or not INSERT cards are used for the purpose of saving computer time.

DESCRIPTION OF PROGRAM OUTPUT

The program prints four kinds of output: input data used to do the calculations, information concerning iteration convergence, tables of results, and optional intermediate output.

Input Data

Input data have been previously described. The general procedure used in this program is to list the input as they are read in and before they are processed by the program. The purpose is to show, in as clear a way as possible, what is actually on the input cards. All problems list the following input data:

- (1) The word REACTANTS
- (2) Reactant data



(3) INSERT and/or OMIT card data

(4) The word NAMELISTS

(5) All data in namelist INPT2 given in table V (P and RHO use same storage)

Following the INPT2 data is the statement "SPECIES BEING CONSIDERED IN THIS SYSTEM." Each species in the list is preceded by some identification, such as J12/65.

The J refers to JANAF data (JANAF Thermochemical Tables, see ref. 1). The letter L refers to unpublished data calculated at the Lewis Research Center. The number refers to the month and the year the data were published or calculated (12/65 is December 1965).

For a rocket problem, the namelist RKTINP data given in table VI are listed. For a shock problem, the namelist SHKINP data given in table VII are listed.

Following the list of chemical species (or RKTINP or SHKINP data, if any) is the current value of O/F. This is followed by a listing of the enthalpies or internal energies of the total fuel and oxidant and of the total reactant. Following this is a list of the kilogram-atom per kilogram of each element in the total fuel and oxidant in the total reactant.

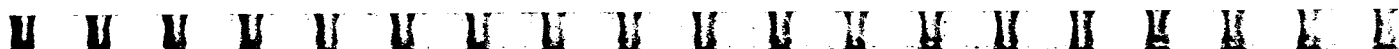
Tables of Thermodynamic Results

The final output of the program is in the form of tables that are designed to be self-explanatory. Tabulated properties include pressure P , temperature T , density ρ , enthalpy h , entropy s , molecular weight M , two partial derivatives $(\partial \ln V / \partial \ln P)_T$ and $(\partial \ln V / \partial \ln T)_P$, specific heat c_p , isentropic exponent γ_S , and velocity of sound a . (An option is available to punch these values on cards. See table V and case 123 in appendix D.) Compositions are also included and given in terms of mole fractions. In addition, rocket, shock, and detonation problems each list additional calculated properties which are pertinent to each type of problem.

Tables of Transport Results

The printed output consists of calculated results in tabular form. Punched-card output is also available as an option. With the exception of the heading at the top, the output for the transport calculations is the same for all types of problems. Viscosities, thermal conductivities, specific heats, Prandtl numbers, and Lewis numbers are calculated and listed for the same conditions as shown in the results of the thermodynamic calculations.

Both frozen and equilibrium values are shown for the thermal conductivity, specific heat, and Prandtl number. The difference between frozen and equilibrium can be described in the following way: Consider a system of reactive species initially in chemical



equilibrium. If heat is then either added or removed, the temperature and pressure will change. If the composition does not change from the initial state, the system is said to be frozen. If the composition adjusts to the equilibrium composition of the new temperature and pressure, the system is said to be in equilibrium. But, if the final composition is neither of these two conditions, the effects of chemical kinetics must be considered. As stated previously, however, the effects of chemical kinetics are not included in the program.

The specific heats shown in the transport properties table are usually identical with those shown in the thermodynamic properties table. However, differences do frequently occur for perfectly valid reasons. These are explained in the section TRANSPORT PROPERTY EQUATIONS.

At this point it is worth explaining why the calculation of the specific heat is repeated in the transport property calculations, with condensed phases omitted. The reason is that it enables the calculation of internally consistent Prandtl and Lewis numbers, numbers derived from properties which are all based on the same gaseous composition. These may be preferable for use in heat- and mass-transfer calculations.

Error Messages

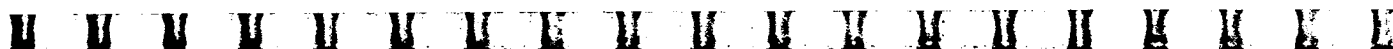
The only other printed output which can occur comes from any one of a number of programmed error messages. Most of these are in the subroutines which do the thermodynamic property calculations. These are explained in detail in reference 1. Four programmed error messages occur in the transport property subroutines. Two are in subroutine TRANSP and the other two are in subroutine INPUT. These messages are explained in the sections discussing the subroutines.

THERMODYNAMIC DATA

Thermodynamic data are included with the program. Reference 1 lists data for 62 reactants and 421 reaction species (solid, liquid, and gas phases of a species are counted as separate species).

Assigned Enthalpies

For each species, heats of formation (and, when applicable, heats of transition) were combined with sensible heats to give assigned enthalpies H_T^0 . By definition,



$$H_T^O = H_{298.15}^O + (H_T^O - H_{298.15}^O) \quad (1)$$

We have arbitrarily assumed $H_{298.15}^O = (\Delta H_f^O)_{298.15}$. Equation (1) then becomes

$$H_T^O = (\Delta H_f^O)_{298.15} + (H_T^O - H_{298.15}^O) \quad (2)$$

In general, $H_T^O \neq (\Delta H_f^O)_T$ for $T \neq 298.15$ K. For reference elements, $(\Delta H_f^O)_{298.15} = H_{298.15}^O = 0$. For the species included with the program these reference elements are Al(s), Ar(g), B(s) (beta), Be(s), Br₂(l), C(s) (graphite), Cl₂(g), Cs(s), F₂(g), Fe(s), H₂(g), He(g), K(s), Li(s), Mg(s), N₂(g), Na(s), Ne(g), O₂(g), P(s) (red, V), S(s) (rhombic), Si(s), and Xe(g).

Assigned enthalpies for reactants are given in table IV (in cal/mole as required for program input) together with some other reactant data. For cryogenic liquids, assigned enthalpies are given at their boiling points. These are usually obtained by subtracting the following quantities from the heat of formation of the gas phase at 298.15 K: sensible heat between 298.15 K and the boiling point, difference in enthalpy between ideal gas and real gas at the boiling point, and heat of vaporization at the boiling point.

Least Squares Coefficients

For each reaction species, the thermodynamic functions specific heat, enthalpy, and entropy as functions of temperature are given in the form of least squares coefficients as follows:

$$\frac{C_p^O}{R} = a_1 + a_2 T + a_3 T^2 + a_4 T^3 + a_5 T^4 \quad (3)$$

$$\frac{H_T^O}{RT} = a_1 + \frac{a_2}{2} T + \frac{a_3}{3} T^2 + \frac{a_4}{4} T^3 + \frac{a_5}{5} T^4 + \frac{a_6}{T} \quad (4)$$

$$\frac{S_T^O}{R} = a_1 \ln T + a_2 T + \frac{a_3}{2} T^2 + \frac{a_4}{3} T^3 + \frac{a_5}{4} T^4 + a_7 \quad (5)$$

Reference 12 describes a program which calculates the thermodynamic functions and fits the functions to equations of the form given in equations (3) to (5).

TRANSPORT DATA

Transport and relaxation data are provided for 59 species, and additional transport data are provided for interactions between unlike species for another 58 interactions. Sources of these data are described in the section SOURCES OF TRANSPORT AND RELAXATION DATA and in tables VIII and IX. All data are in tabular form as a function of temperature. In contrast with the thermodynamic data, the temperature range of the transport data is not the same for all interactions. The temperature ranges for the transport data are also shown in table VIII.

The temperature intervals in the table are not constant, but generally increase with increasing temperature. This was done in order to accommodate interpolation within the table. Interpolation is done by four-point Lagrange, and the number of arguments allowed per table is 20. This number was arrived at as a compromise between two considerations. First, storage space is limited (IBM 7094); and in order to allow sufficient storage for a large number of interactions, the number of intervals in each table should not be excessive. However, the interval size must be small enough such that interpolation errors are less than the uncertainty of the data within the table. Consequently, the temperature intervals tend to be closest in the vicinity of 300 K because usually the transport data are most accurately known at room temperature.

SAMPLE PROBLEMS

Ten sample problems are given to illustrate some of the features of the program. Five are rocket performance problems, RKT = T (cases 51, 122, 679, 5612, and 6666); two are combustion problems (case 123 is for combustion at constant pressure, HP = T; and case 1565 is for combustion at constant volume, UV = T); case 52 is a detonation problem, DETN = T; case 1207 is a shock problem, SHOCK = T; case 950 is an assigned temperature and pressure problem, TP = T; and case 6666 illustrates freezing in a rocket at a location other than the chamber.

It would not be practical to illustrate every possible combination of options permitted by the program. However, the sample problems were selected to illustrate many of the possible combinations and, in particular, those variations which we believe would most often be used. Included in the combinations illustrated are the following:

- (1) Specifying proportions of various reactants
 - (a) O/F: cases 122, 123, and 1565
 - (b) Equivalence ratios: cases 52 and 950
 - (c) Percent fuel by weight: cases 5612 and 6666
 - (d) Complete information on reactant cards: cases 51, 679, and 1207

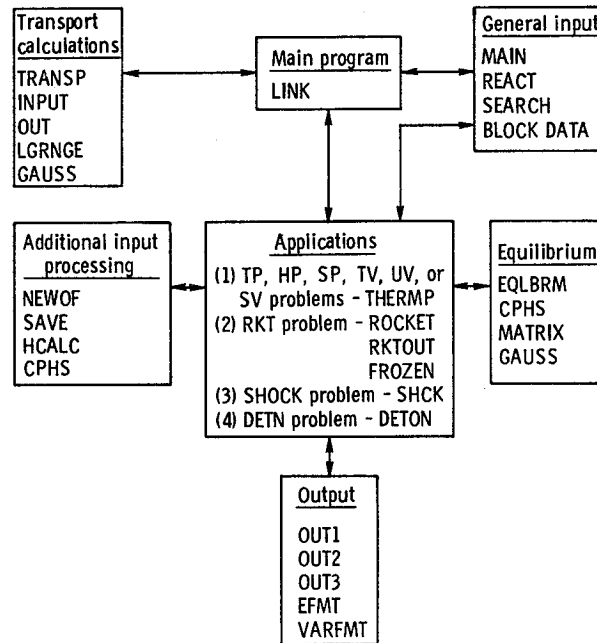
- (e) Relative weights of reactants: cases 51, 52, 122, 123, 950, 1565, 5612, and 6666
- (f) Relative moles of reactants: cases 679 and 1207
- (2) Specifying enthalpies
 - (a) On reactant cards: cases 51 (partly), 122, 123, 679, 950, 1565 (partly), 5612, and 6666
 - (b) Calculated by program: cases 51 (partly), 52, 1207, and 1565 (partly)
- (3) Pressure units
 - (a) psia: cases 51, 122, 679, 5612, and 6666
 - (b) atm: cases 52, 123, and 950
 - (c) mm Hg: case 1207
- (4) INSERT: cases 51 and 5612
- (5) OMIT: cases 51 and 950
- (6) Composition in floating-point format: case 1565
- (7) Program considers ions: case 679
- (8) Special derivatives due to two condensed phases of a species: cases 51 and 5612
- (9) Special throat interpolation: case 5612
- (10) Omit transport property calculations: case 679
- (11) Punched-card output: case 123
- (12) Freezing at supersonic station: case 6666

Some additional features of the program illustrated by the various cases are the following:

- (1) Case 51: This case shows several condensed species being automatically inserted and removed by the program. Frozen expansion is stopped at point 3 inasmuch as the exit temperature is below the melting point of 2315 K.
- (2) Case 122: This case shows that it is possible to assign a schedule of points which includes a mixture of pressure ratios, subsonic area ratios, and supersonic area ratios.

MODULAR FORM OF PROGRAM

In order to facilitate adding or deleting applications of the chemical equilibrium part of the program, the program was set up in 10 modules. These modules are concerned with overlay control, which is used on the IBM 7094 (main program), and with general input, additional input processing, four applications, equilibrium calculations, transport calculations, and output. The general flow of these modules and associated routines is given in the following schematic:



From this diagram, it is clear that, for example, the rocket application could be eliminated by omitting subroutines ROCKET, RKTOUT, and FROZEN and by omitting the statement which calls ROCKET in the main program.

LINK (MAIN PROGRAM)

LINK is the main program. Its sole function is to control the program flow between the thermodynamic and transport property calculations. The overlay structure used for the IBM 7094 is shown in figure 1. LINK and subroutine GAUSS are the only two routines in core storage at all times. (GAUSS solves a set of as many as 20 simultaneous linear equations.) Overlay is not required for machines which have sufficient storage for the entire program.

A flow chart of LINK is given in figure 2.

The number of storage locations used for each routine is shown in parentheses in figure 1. These numbers include allocations for block common, as they are introduced into storage in loading the program. That is, the number in parentheses includes a block common with the first routine in which it is used. Consequently, LINK and TRANSP have larger numbers than they would have if the common blocks had not been included.

When the program is doing thermodynamic property calculations, LINK 0 and LINK 1 are in core storage. This uses about 27 000 storage locations. When the program is doing transport property calculations, LINK 0 and LINK 2 are in core storage. This uses over 32 000 storage locations. These numbers include all the routines but not other storage needed by the computer system. This additional storage requirement will vary from

one computer installation to another. At NASA Lewis this amounts to 1548 storage locations for the system and an additional 5590 for the systems subroutines, for a total of 7138 additional storages.

DISCUSSION OF SUBROUTINES

This section describes the routines not included in reference 1 and also describes those in the CEC71 program which have been changed. Among the new routines are the subroutines needed for the transport property calculations and the main program (LINK), which links the thermodynamic calculations with the transport calculations. Subroutines which will not be discussed are those which are nearly the same as those in reference 1.

Some dimensions have been changed from the CEC71 program. In order to save storage, only 100 species and 10 elements are permitted, rather than 150 species and 15 elements, as are allowed in CEC71. Also, the number of temperatures T has been changed from 26 to 52. These dimension changes apply to any routine in which the variables appear. These changes affect the common blocks POINTS, SPECES, and MISC.

Two new common blocks, SAVED and CONTRL, have been added. SAVED is used to save information obtained from the thermodynamic calculations which is needed in the transport calculations. It is also used to save information obtained from the transport calculations which is needed later. This change also caused a slight reorganization of the variables in common blocks SPECES, MISC, and INDX. CONTRL contains additional logical variables TRNSPT, FROZN, PUNCH, and NODATA.

Flow charts are also included for aid in understanding of the program. The reader may find appendixes A and B helpful in relating symbols to the program variable names.

Subroutine MAIN

Subroutine MAIN is very similar to the main routine in the CEC71 program. A flow chart is given in figure 3. Perhaps the most noteworthy change is that it is now a subroutine. One other change is significant. That is, when thermodynamic data are being read in from cards, transport and relaxation data immediately follow the thermodynamic data. The format for the thermodynamic data is still the same as in reference 1. This change essentially involves only the insertion of 11 additional cards which are needed in order to read and write the transport and relaxation data on tape unit 4.



Subroutine SEARCH

SEARCH searches for data stored on logical tape unit 4. Thermodynamic data for all the species in the chemical system are located on tape unit 4 and saved in core storage. In addition, transport and relaxation data are also read from tape unit 4, and the data which are relevant to the chemical system are stored on logical tape unit 3 (disk storage).

Another search of the transport and relaxation data on tape unit 3 is made at the start of the transport property calculations in subroutine TRANSP. This second search is used in order to find the data involving interactions of only the important species and to save these data in core storage. This secondary search is discussed in the section Subroutine TRANSP.

Subroutine OUT1

Subroutine OUT1 is the output routine for the thermodynamic calculations. It is nearly the same as OUT1 in the CEC71 program. The only change is that punched-card output of the thermodynamic properties is now included. Only data of the standard thermodynamic properties which apply to all types of problems (rocket, shock, detonation, and assigned thermodynamic states) are punched. The additional properties, which apply only to the particular type of problem being run, are not punched.

Subroutines THERMP, ROCKET, SHCK, and DETON

These subroutines control the calculations for the same types of problems as in the CEC71 program: properties at assigned thermodynamic states, rocket combustion, normal shock waves, and Chapman-Jouguet detonations. The basic differences between the two programs are the modes of entry and return from these routines. Both standard and nonstandard entries and returns are used, in contrast with the CEC71 program, which uses only a standard entry and return. The modes of entry and return can be seen from figure 2 and the program listing (appendix C).

Another difference between the programs involves the DO loops on pressure, temperature, and O/F (P, T, OXF). The subroutines for the thermodynamic calculations and the subroutines for the transport calculations are in different core loads. So if the problem involves more than 13 points, the core load for the thermodynamic calculations has to be reloaded after each set of transport calculations is completed. However, in order to reenter the subroutines THERMP, ROCKET, SHCK, and DETON after each set of transport calculations, it would have been necessary to illegally enter inside the DO

loops. To avoid this problem, the DO loops have been eliminated and a simple, program-generated, indexing procedure on P, T, and OXF has been used.

Subroutine ROCKET has additional changes associated with the variable NFZ, the variable which specifies the freezing point for frozen flow. Since the CEC71 program permits only freezing at the chamber, the present program required some changes in order to allow freezing at the throat or at any supersonic station.

Subroutine TRANSP

Subroutine TRANSP is the main routine for the transport calculations. A flow diagram is given in figure 4. All calculations of the properties are done in this routine. The equations are given in the next section.

One other operation is carried out in this routine. Logical tape unit 3 is searched for the transport and relaxation data of the important interactions and saved in the variable TABLES. This search differs from the one in subroutine SEARCH. In SEARCH, data are saved for all interactions in the chemical system; whereas, in TRANSP, interactions involving a trace species are eliminated.

The remainder of the routine is the calculation of the properties. Calculation of the viscosity, monatomic thermal conductivity, reaction thermal conductivity, and reaction heat capacity all involve the solving of a set of simultaneous linear equations. The matrix elements for each are calculated in TRANSP, but the actual solution is obtained from subroutine GAUSS.

The solutions obtained from GAUSS are checked for accuracy for two of the properties, viscosity and reaction thermal conductivity. If the initial equations are not satisfied to a prescribed tolerance by using the solution obtained from GAUSS, an error message is printed out. (See the listing in appendix C of subroutine TRANSP for the specific information printed out in each error message.)

Subroutine INPUT

Subroutine INPUT sets up the transport and relaxation data needed for the transport property calculations done in TRANSP. It is called from TRANSP for each point. The various functions of this subroutine are outlined as follows:

(1) The EN array is searched for the most important gaseous species for the current point. These are identified and saved by storing the index of the species name in IND. A maximum of 20 species is allowed. All species of mole fractions less than 10^{-7} are omitted, as well as all condensed phases. However, all gaseous atomic elements are initially included, even if they are not among the 20 most important species, or even if

their mole fractions are less than 10^{-7} . This condition is imposed to satisfy a requirement imposed upon the A array, which is explained later in this section. If any elements have been omitted through use of an OMIT card, they are reinserted into the A array at this point. A message is printed out giving the name of the element reinserted into the A array: 'NO ELEMENT WAS FOUND IN THE LIST OF SPECIES WITH THE NAME (name of species), OR ELSE THERE IS AN ERROR IN THE A(I,K) ARRAY.'

(2) The mole fractions and molecular weights are now calculated for the new reduced composition obtained in step 1.

(3) Transport and relaxation data are initialized to zero. Then, data stored in TABLES are searched, interaction by interaction, for data pertinent to the current point. When such data are found, subroutine LGRNGE(TT) is called. LGRNGE(TT) interpolates for the temperature TT. If data are missing for a pure species, an empirical equation is used to estimate the data. If data are missing for an interaction between unlike species, data are estimated from combining rules, using the data of the pure species. The empirical equation and the combining rules are described in the next section. If data for a pure species are missing, an error message is printed out: 'NO TRANSPORT DATA WERE FOUND FOR THE SPECIES (name of species).' If the logical variable NODATA is not specified in the INPT2 namelist, the program sets NODATA = .F. and the message is printed. If NODATA = .T. is set in namelist INPT2, the message is not printed. However, no message is ever printed when data are missing for an interaction between unlike species. In either case, the program continues.

The purpose of this error message is to warn the program user when transport data for a major species are missing. When the user is certain this is not the situation, he may wish to omit the message, in order to avoid getting the message every time the program fails to find data for a minor species.

(4) The final operation of INPUT is to read the stoichiometric coefficients from the A array into the STC array and reorder them so as to express them as a set of chemical reaction equations, suitable for use in equation (25). As was mentioned earlier, all the elements in the system are initially included. This is not a necessary requirement, but was done as a matter of convenience. By including all the elements among the 20 (or less) gaseous species in the system, it is possible to use the A array to express the system in terms of a sufficient set of independent chemical equations. The number of required independent equations is given by taking the total number of species and subtracting the number of chemical elements in the system. So by choosing the set of chemical equations as the chemical reactions of formation of each species, a set of equations can be easily written directly from the stoichiometric coefficients in the A array. For instance, in the A array corresponding to the column for CH_4 , there is a 1 in the row for carbon, a 4 in the row for hydrogen, and a 0 in the rows for the remaining elements. By assigning a -1 to CH_4 , the chemical equation $\text{C} + 4\text{H} - \text{CH}_4 = 0$ is formed.



This procedure is applied to each species in the system, and the result is the initial set of equations. This initial set of equations is then reduced in order to eliminate any species or element (in this case always an element) not found among the 20 most important species in the system. This reduction is accomplished by searching through the chemical equations for an element with a mole fraction less than 10^{-7} , solving the chemical equation for that element, and then substituting the result in any other equation in which the element appears. The new set of equations is one less in number than the original set. This procedure is repeated until all the elements of mole fractions less than 10^{-7} have been eliminated from the chemical equations. The stoichiometric coefficients of this final set of equations are stored in *STC* and are used in equation (25) for calculating the reaction contribution to the heat capacity and thermal conductivity.

Subroutine OUT

The output routine, appropriately called *OUT*, handles all the output of the transport property calculations. This includes table headings, units, calculated data, spacing, and punched-card output.

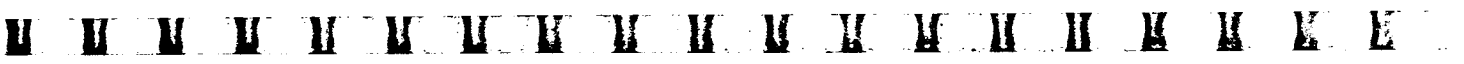
This routine was written with the capability of saving the transport data for as many as 52 points. These data are saved in *STORE*. Including the current set of 13 points, this means that as many as 65 points can be printed at one time. If the problem has more than 65 points, such as might occur for a *TP* problem, transport data will be printed out after every multiple of 65 points.

Subroutine LGRNGE(TT)

Subroutine *LGRNGE(TT)* is a four-point Lagrange interpolation routine. It is used to interpolate within the tables of transport and relaxation data at temperature *TT*.

TRANSPORT PROPERTY EQUATIONS

The rigorous theory for the transport properties of real, dilute, monatomic gases has been reviewed and studied in great detail by Chapman and Cowling (ref. 13) and Hirschfelder, Curtiss, and Bird (ref. 14). Both references 13 and 14 express the transport coefficients in terms of Sonine polynomial expansions. However, in actually solving the equations, they use different but equivalent methods. Another method originated by Maxwell and refined by Chapman is called the moment method. More recently, Grad (ref. 15) has made the expansion in the moment method more systematic, using Hermite



polynomials rather than Sonine polynomials; his method is frequently referred to as the "thirteen-moment method." An historical review of the early work in this field is given in reference 13.

The methods described in references 13 to 15 result in mathematical solutions with increasing orders of approximation to the transport coefficients. As the order of approximation increases, so does the arithmetic complexity. Fortunately, what is usually referred to as the first approximation is sufficiently accurate for nearly all practical applications. The most notable exception to this is when ionization becomes appreciable (refs. 10 and 11). This is particularly true for the thermal conductivity. The present program uses only the first approximations, and this suggests an upper limit to the range of applicability for the transport coefficient calculations. This limit is incipient ionization. When the degree of ionization is low, collisions between ionized species and neutral particles are infrequent, and collisions where both species are ionized are very infrequent. With a further increase in temperature (or decrease in pressure), ionization increases and interactions between charged particles become important. At this point the first approximation is no longer sufficient.

However, it should be reiterated that what we are referring to here are approximations to the solution of the general equation. There are other assumptions in the mathematical formulation which have been discussed in the section ASSUMPTIONS AND CAPABILITIES. These assumptions restrict the range of applicability of the general equation at high pressures and at low temperatures and pressures.

Viscosity

The viscosity of the gas mixture is calculated from the following equation (ref. 14, p. 489, eqs. (7.4-56) and (7.4-57), see also pp. 531 and 532):

$$\eta_{\text{mixture}} = \sum_{i=1}^n x_i \eta_i \quad (6)$$

where n is the number of species in the mixture, x_i is the mole fraction of species i , and η_i is found by solving the following set of simultaneous algebraic equations, which are linear in the unknown η_j :

$$\sum_{j=1}^n c_{ij} \eta_j = x_i \quad i = 1, 2, \dots, n \quad (7)$$

and the c_{ij} matrix coefficients are given by

$$c_{ii} = \frac{x_i^2}{\eta_{ii}} + \sum_{\substack{k=1 \\ k \neq i}}^n \frac{2x_i x_k}{\eta_{ik}} \frac{M_i M_k}{(M_i + M_k)^2} \left(\frac{5}{3A_{ik}^*} + \frac{M_k}{M_i} \right) \quad (7a)$$

$$c_{ij} = - \frac{2x_i x_j}{\eta_{ij}} \frac{M_i M_j}{(M_i + M_j)^2} \left(\frac{5}{3A_{ij}^*} - 1 \right) \quad i \neq j \quad (7b)$$

where

$$\eta_{ij} = \frac{5}{16N_A} \frac{\sqrt{2\pi M_i M_j RT / (M_i + M_j)}}{\pi \bar{\Omega}_{ij}^{(2,2)}} \quad (7c)$$

and

$$A_{ij}^* = \frac{\bar{\Omega}_{ij}^{(2,2)}}{\bar{\Omega}_{ij}^{(1,1)}} \quad (7d)$$

where N_A is Avogadro's number, M_i is the molecular weight of species i , R is the gas constant, T is the temperature, and $\bar{\Omega}_{ij}^{(1,1)}$ and $\bar{\Omega}_{ij}^{(2,2)}$ are cross sections. The $\bar{\Omega}_{ij}^{(1,1)}$ are the diffusion cross sections. When $j = i$, the $\bar{\Omega}_{ij}^{(2,2)}$ are viscosity cross sections, and η_{ij} simplifies to the equation for the viscosity of a pure gas $\left(5\sqrt{\pi M_i RT} / 16\pi N_A \bar{\Omega}_{ii}^{(2,2)} \right)$.

Thermal Conductivity

The thermal conductivity is usually expressed as

$$\lambda_{\text{mixture}} = \lambda_{\text{trans}} + \lambda_{\text{int}} + \lambda_{\text{reaction}} = \lambda_{\text{frozen}} + \lambda_{\text{reaction}} \quad (8)$$

An equation for the first term on the right side of equation (8) was derived by Muckenfuss and Curtiss (ref. 16) and may be written in the form

$$\lambda_{\text{trans}} = 4 \sum_{i=1}^n x_i \lambda_i \quad (9)$$

where the λ_i are found by solving the following set of simultaneous linear equations, similar to those for the viscosity:

$$\sum_{j=1}^n b_{ij} \lambda_j = x_i \quad i = 1, 2, \dots, n \quad (10)$$

and the b_{ij} matrix coefficients are given by

$$b_{ii} = \frac{4x_i^2}{\lambda_{ii}} + \sum_{\substack{k=1 \\ k \neq i}}^n \frac{2x_i x_k \left(\frac{15}{2} M_i^2 + \frac{25}{4} M_k^2 - 3B_{ik}^* M_k^2 + 4A_{ik}^* M_i M_k \right)}{(M_i + M_k)^2 A_{ik}^* \lambda_{ik}} \quad (10a)$$

$$b_{ij} = - \frac{2x_i x_j M_i M_j}{(M_i + M_j)^2 A_{ij}^* \lambda_{ij}} \left(\frac{55}{4} - 3B_{ij}^* - 4A_{ij}^* \right) \quad i \neq j \quad (10b)$$

where

$$\lambda_{ij} = \frac{75R}{64N_A} \sqrt{\frac{\pi(M_i + M_j)RT/2M_i M_j}{\bar{\Omega}_{ij}^{(2,2)}}} = \frac{15}{4} R \left(\frac{M_i + M_j}{2M_i M_j} \right) \eta_{ij} \quad (10c)$$

and

$$B_{ij}^* = \frac{5\bar{\Omega}_{ij}^{(1,2)} - 4\bar{\Omega}_{ij}^{(1,3)}}{\bar{\Omega}_{ij}^{(1,1)}} \quad (10d)$$

The $\bar{\Omega}_{ij}^{(1,2)}$ and $\bar{\Omega}_{ij}^{(1,3)}$ are cross sections similar to the $\bar{\Omega}_{ij}^{(1,1)}$ and $\bar{\Omega}_{ij}^{(2,2)}$ but are not associated with any particular transport property.

The preceding result for λ_{trans} represents the total thermal conductivity of a mixture of inert monatomic gases, species without internal structure. For polyatomic gases, Monchick, Yun, and Mason (ref. 17) and Monchick, Pereira, and Mason (ref. 18)

have extended the theory to include internal energy. Two assumptions were needed in order to obtain workable equations. The first assumption was that "complex collisions" (collisions involving more than a single quantum jump) could be ignored, and the second was that there was no correlation between internal energy states and relative velocities. With these assumptions plus suitable definitions of internal diffusion coefficients and relaxation times, they obtained a working equation for the thermal conductivity. They then simplified the equation to include only first-order correction terms and rearranged it to correctly give the thermal conductivity of the pure gas automatically. They expressed λ_{int} as

$$\lambda_{\text{int}} = (\lambda_{\text{int}})_{\text{HE}} + \Delta\lambda \quad (11)$$

where $(\lambda_{\text{int}})_{\text{HE}}$ is the Hirschfelder-Eucken approximation for the internal contribution to the thermal conductivity (ref. 19) and $\Delta\lambda$ is a correction term containing the inelastic effects between unlike species and some of the inelastic effects between like species. The Hirschfelder-Eucken approximation is given by

$$(\lambda_{\text{int}})_{\text{HE}} = \sum_{i=1}^n \left(\frac{\lambda_{\text{int},i}}{\sum_{j=1}^n \frac{D_{ij} x_j}{D_{ij} x_i}} \right) \quad (12)$$

where the D_{ij} are binary diffusion coefficients, the D_{ii} are self-diffusion coefficients, and $\lambda_{\text{int},i}$ is the internal energy contribution of species i to the thermal conductivity. The $\lambda_{\text{int},i}$ are given by (ref. 18)

$$\frac{(\lambda_{\text{int},i})M_i}{\eta_{ii}} = \left(\frac{\rho_i D_{\text{int},i}}{\eta_{ii}} \right) C_{\text{int},i} - \frac{\left(\frac{2C_{\text{int},i}}{\pi Z_i} \right) \left(\frac{5}{2} - \frac{\rho_i D_{\text{int},i}}{\eta_{ii}} \right)^2}{1 + \left(\frac{2}{\pi Z_i} \right) \left(\frac{5}{3} \frac{C_{\text{int},i}}{R} + \frac{\rho_i D_{\text{int},i}}{\eta_{ii}} \right)} \quad (13)$$

where ρ_i is the density, $C_{\text{int},i}$ the internal heat capacity, Z_i the collision number, $D_{\text{int},i}$ a quantity which is frequently referred to as the diffusion coefficient for internal energy, and the subscript i again refers to species i . For elastic collisions, $D_{\text{int},i}$ is reasonably well approximated by the self-diffusion coefficient (ref. 20). However, for

some molecules, this approximation is no longer valid. For example, polar molecules may exchange internal energy even at large separations. In particular, for the case of the exchange of rotational energy when the exchange is energetically resonant, Mason and Monchick have derived expressions for $D_{\text{int},i}$ which can be expressed as (ref. 20)

$$D_{\text{int},i} = \frac{D_{\text{ii}}}{1 + \delta_i} \quad (14)$$

They give explicit expressions for the δ_i in terms of the molecular weight, dipole moment, and moments of inertia for linear molecules and various symmetric-top molecules.

From reference 14 (p. 540),

$$\frac{\rho_i D_{\text{ii}}}{\eta_{\text{ii}}} = \frac{6}{5} A_{\text{ii}}^* \quad (15)$$

Then from equations (14) and (15),

$$\frac{\rho_i D_{\text{int},i}}{\eta_{\text{ii}}} = \frac{6}{5} \left(\frac{A_{\text{ii}}^*}{1 + \delta_i} \right) \quad (16)$$

where $\delta_i = 0$ for nonpolar molecules.

One additional modification of equation (13) should be mentioned. Only one collision number is indicated for each species in equation (13). However, there is a different collision number for each internal energy mode. If each internal energy mode is separable and a collision number identified with each mode, then one can write (ref. 18)

$$\frac{C_{\text{int},i}}{Z_i} = \sum_k \frac{C_{\text{int},ki}}{Z_{ki}} \quad (17)$$

where the subscript k runs over all internal energy modes and the subscript i refers to species i . However, in practice, the rotational energy modes are usually the only ones of importance, though the vibrational ones may become important at high temperatures.

If it is assumed that the species can be characterized by one rotational collision number and by one vibrational collision number and that $D_{\text{int},i} = D_{\text{ii}}/(1 + \delta_i)$, then from equations (13), (15), and (17) and the relationship for an ideal gas, which is

$$C_{\text{int},i} = C_{p,i} - \frac{5}{2} R \quad (18)$$

the following is obtained:

$$\frac{(\lambda_{\text{int},i})_{M_i}}{\eta_{ii}} = \frac{6}{5} A_{ii}^* \left(C_{p,i} - \frac{5}{2} R \right) - \frac{\left(\frac{C_{\text{rot},i}}{Z_{\text{rot},i}} + \frac{C_{\text{vib},i}}{Z_{\text{vib},i}} \right) \left(\frac{5}{2} - \frac{6}{5} A_{ii}^* \right)^2 R}{\frac{\pi R}{2} + \left(\frac{C_{\text{rot},i}}{Z_{\text{rot},i}} + \frac{C_{\text{vib},i}}{Z_{\text{vib},i}} \right) \left[\frac{5}{3} + \frac{6/5 A_{ii}^*}{(c_p/R) - (5/2)} \right]} \quad (19)$$

Equation (19) is written for nonpolar gases. For polar molecules, A_{ii}^* is replaced by $A_{ii}^*/(1 + \delta_i)$. To transform the denominator of equation (12), the following relationship is used (ref. 14, p. 530):

$$D_{ij} = \frac{3}{5} \left(\frac{M_i + M_j}{M_i M_j} \right) \left(\frac{RT}{P} \right) A_{ij}^* \eta_{ij} \quad (20)$$

When this equation is substituted into equation (12), the result is

$$(\lambda_{\text{int}})_{\text{HE}} = \sum_{i=1}^n \frac{\lambda_{\text{int},i}}{\sum_{j=1}^n \frac{A_{ii}^*}{A_{ij}^*} \left(\frac{2M_j}{M_i + M_j} \right) \frac{\eta_{ii} x_j}{\eta_{ij} x_i}} \quad (21)$$

The denominator contains quantities which have been previously defined. The computer program uses equation (21) with $\lambda_{\text{int},i}$ obtained from equation (19). Again, for polar molecules, A_{ii}^* is replaced by $A_{ii}^*/(1 + \delta_i)$. The program does not calculate the δ_i . It is assumed that the A_{ii}^* are provided in a form which is suitable for direct use in equations (19) and (21).

Monchick, Pereira, and Mason (ref. 18) have compared calculated results for some binary mixtures with experimental measurements in order to determine the effect of including relaxation effects. Equation (11) was used along with the internal thermal conductivity of a pure species $\lambda_{\text{int},i}$ expressed in the form

$$\lambda_{\text{int},i} = \lambda_{\text{exp},i} - \lambda_{\text{monatomic},i} = \lambda_{\text{exp},i} - \frac{15}{4} \frac{R}{M} \eta_{ii} \quad (22)$$

At the temperatures of the experimental measurements, only rotational relaxation was important. In general, satisfactory agreement was obtained between experiment and the theory of binary mixtures. Their results showed that the calculations were relatively insensitive to the inelastic collision corrections, provided that as the mole fraction of one species reached zero the calculated results were forced to agree with the experimental value of the pure gas for the other species. They concluded that for most purposes it was satisfactory to neglect inelastic effects in the mixture between different species, but that inelastic effects must be included in the calculations of the pure species. In other words, to a good approximation, $\Delta\lambda$ can be ignored in equation (11). A further consideration is that relaxation information between unlike species is almost completely lacking (ref. 18). In view of the preceding considerations the present program assumes $\Delta\lambda = 0$, and thus equation (21) is the only term contributing to equation (11).

The third and final term in equation (8) represents the contribution from chemical reaction. For a mixture of nonreacting gases (frozen mixture), this term is zero. But when chemical reactions occur, there is a contribution to the thermal conductivity. A general expression has been derived (refs. 21 and 22) for the contribution to the conductivity when local chemical equilibrium exists in a mixture of reacting gases:

$$\lambda_{\text{reaction}} = R \sum_{i=1}^{\nu} \left(\frac{\Delta H_i}{RT} \right) \lambda_{r,i} \quad (23)$$

where ν is the total number of chemical reactions and ΔH_i is the heat of reaction expressed as

$$\Delta H_i = \sum_{k=1}^n a_{ik} H_k \quad i = 1, 2, \dots, \nu \quad (24)$$

In equation (24) the a_{ik} are the stoichiometric coefficients written for the chemical reactions involving species A_k as follows

$$\sum_{k=1}^n a_{ik} A_k = 0 \quad i = 1, 2, \dots, \nu \quad (25)$$

The $\lambda_{r,i}$ are found by solving a set of simultaneous linear equations

$$\sum_{j=1}^{\nu} g_{ij} \lambda_{r,j} = \frac{\Delta H_i}{RT} \quad i = 1, 2, \dots, \nu \quad (26)$$

where the g_{ij} are given by

$$g_{ij} = \sum_{k=1}^{n-1} \sum_{l=k+1}^n \left(\frac{RT}{PD_{kl}} x_k x_l \right) \left(\frac{a_{ik}}{x_k} - \frac{a_{il}}{x_l} \right) \left(\frac{a_{jk}}{x_k} - \frac{a_{jl}}{x_l} \right) \quad (26a)$$

Rearranging equation (20) gives

$$\frac{RT}{PD_{kl}} = \frac{5M_k M_l}{3A_{kl}^* \eta_{kl} (M_k + M_l)}$$

which is the form of RT/PD_{kl} used in the program to evaluate g_{ij} in equation (26a). The sum of equations (9), (21), and (23) gives the total thermal conductivity of the gas mixture.

Specific Heat

The specific heat given in the transport properties table is calculated from the equation of reference 23

$$c_{p,eq} = c_{p,frozen} + c_{p,reaction} \quad (27)$$

where

$$c_{p,frozen} = \frac{\sum_{i=1}^n x_i C_{p,i}}{\sum_{i=1}^n x_i M_i} = \frac{1}{M} \sum_{i=1}^n x_i C_{p,i} \quad (27a)$$

and $c_{p, \text{reaction}}$ is found from an equation very similar to that for calculating $\lambda_{\text{reaction}}$ (eq. (23))

$$c_{p, \text{reaction}} = \frac{R}{M} \sum_{i=1}^{\nu} \left(\frac{\Delta H_i}{RT} \right) X_i \quad (28)$$

The X_i are found by solving the following set of linear equations:

$$\sum_{j=1}^{\nu} d_{ij} X_j = \frac{\Delta H_i}{RT} \quad i = 1, 2, \dots, \nu \quad (29)$$

where the d_{ij} are given by

$$d_{ij} = \sum_{k=1}^{n-1} \sum_{l=k+1}^n x_k x_l \left(\frac{a_{ik}}{x_k} - \frac{a_{il}}{x_l} \right) \left(\frac{a_{jk}}{x_k} - \frac{a_{jl}}{x_l} \right)$$

Equation (28) is different from, but equivalent to, that given in reference 1. It is also very similar to the equation (from refs. 21 and 22) for calculating $\lambda_{\text{reaction}}$ (eq. (23)). The only difference from equation (23) is that the (RT/PD_{kl}) term is missing in the d_{ij} coefficients. Consequently, it provides a means for checking for errors in the transport calculations, especially $\lambda_{\text{reaction}}$.

Agreement between the specific heat in the thermodynamic calculations and the specific heat in the transport calculations indicates that the transport calculations proceeded satisfactorily. However, as mentioned earlier in the section DESCRIPTION OF PROGRAM OUTPUT, differences do frequently occur for perfectly valid reasons. First, if condensed phases appear in the composition there will be some differences, because the specific heat listed in the results of the thermodynamic calculations includes condensed and gas phases, whereas the specific heat listed in the results of the transport calculations includes only the gas phase. The other reason is that sometimes not all the species appearing in the results of the thermodynamic calculations will be used in the transport calculations. This occurs because, as explained previously, only 20 gaseous species are included in the transport calculations and, among these, all the elements in the chemical system are initially included. The reason for including the elements was discussed in the section describing subroutine INPUT.

Remaining Properties

The equations for the remaining properties are summarized as follows: The frozen and equilibrium Prandtl numbers are

$$\text{Pr}_{\text{frozen}} = \frac{(c_{p, \text{frozen}})(\eta_{\text{mixture}})}{\lambda_{\text{frozen}}} \quad (30)$$

$$\text{Pr}_{\text{eq}} = \frac{(c_{p, \text{eq}})(\eta_{\text{mixture}})}{\lambda_{\text{mixture}}} \quad (31)$$

For the generalized Lewis number, as defined by Brokaw (ref. 24)

$$\text{Le} = \frac{(\lambda_{\text{reaction}})(c_{p, \text{frozen}})}{(\lambda_{\text{frozen}})(c_{p, \text{reaction}})} \quad (32)$$

A few other thermodynamic properties for the gas phase (molecular weight, enthalpy, and density) are included in the punched-card output but not in the printed output:

$$M = \sum_{i=1}^n x_i M_i \quad (33)$$

$$H = \sum_{i=1}^n x_i H_i \quad (34)$$

$$\rho = \frac{PM}{RT} \quad (35)$$

Estimation Techniques

The final subject concerns the equations used to estimate the transport cross-section data when these data are missing from the TRANSPORT data library (physical tape 4). When this occurs, empirical rules are used. For interactions involving molecules of different species, the rules suggested from the analogy to a rigid sphere (ref. 25) are

$$\bar{\Omega}_{ij}^{(2,2)} = \frac{1}{4} \left[\bar{\Omega}_{ii}^{(2,2)} + 2\sqrt{\bar{\Omega}_{ii}^{(2,2)}\bar{\Omega}_{jj}^{(2,2)}} + \bar{\Omega}_{jj}^{(2,2)} \right] \quad (36)$$

$$A_{ij}^* = \frac{1}{2} (A_{ii}^* + A_{jj}^*) \quad (37)$$

$$B_{ij}^* = \frac{1}{2} (B_{ii}^* + B_{jj}^*) \quad (38)$$

For molecules composed of hard rigid spheres the preceding equations are exact ($A_{ij}^* = B_{ij}^* = 1$).

For interactions involving molecules of the same species, an empirical relation was derived from the experimental and theoretical transport data of the pure species. This relation should not be considered as a means for providing missing data, but rather as a means for estimating cross sections of the correct order of magnitude, in order that the calculations will proceed smoothly. Problems might occur, such as division by zero, if the assigned storage locations for cross sections were allowed to remain empty. Only species for which information on transport data were available over a large temperature range were used in the analysis. These included species such as He, Ne, Ar, Kr, Xe, N, O, N₂, O₂, H₂, CO₂, and H₂O. The empirical relationship is

$$\bar{\Omega}_{ii}^{(2,2)} = \ln \left(320 \frac{M_i^4}{T^{1.4}} \right) \quad (39)$$

where $\bar{\Omega}_{ii}^{(2,2)}$ is given in the units of square angstroms. The largest errors in equation (39) occurred for species of very low molecular weight. For very high temperatures or low molecular weights, $\bar{\Omega}_{ii}^{(2,2)}$ can become negative. In order to avoid this, $\bar{\Omega}_{ii}^{(2,2)} = 1$ was arbitrarily assigned as the smallest allowable value. For all conditions where $\bar{\Omega}_{ii}^{(2,2)}$ calculated by equation (39) is less than unity, it is set equal to unity.

The A_{ii}^* and B_{ii}^* generally show only a very slight temperature dependence and usually are close to unity. Consequently, both were set equal to 1 for all temperatures. This is also consistent with equations (37) and (38) in that this approximation is exact for molecules composed of hard rigid spheres.

Also, for each species, relaxation data are needed (Z_i), and these data are often lacking. If relaxation data for the species are not found in the tape library, the program uses the Hirschfelder-Eucken approximation (ref. 19), which is equivalent to letting $Z_{rot} = Z_{vib} = \infty$ in equation (19). There is no scheme for estimating collision numbers included in the program.

SOURCES OF TRANSPORT AND RELAXATION DATA

Sources of the transport cross-section data included with the program are given in table VIII. The data are in the nature of a preliminary set of input. In order to provide data for the large number of interactions needed in a general program, data included with the program were generally obtained directly from the literature. For the most part, the data were not examined critically, and so are not necessarily the most recent or most accurate data. There is one important exception, however. This is the input for the inert gases. A considerable amount of high-temperature experimental viscosity and thermal conductivity data have become available for the inert gases in recent years. These data, as well as the earlier data, have been used to obtain the cross-section data included with the set of input. Molecular beam scattering data were used at the higher temperatures.

One method given in table VIII which should be commented upon is method 9, which applies to the CO interactions. From consideration of the electron configurations and molecular weights of N_2 and CO, it would be anticipated that the transport cross sections for interactions involving N_2 should be about the same as those for the corresponding interactions involving CO. In order to test this supposition, the viscosity data of N_2 were compared with the viscosity data of CO (refs. 26 and 27); and the binary diffusion data for N_2 -X were compared with the binary diffusion data for CO-X (ref. 28), where X is some third species. Good agreement was obtained. This suggested the possibility that if data for an interaction involving CO were unavailable, data for the corresponding interaction involving N_2 could be used. The reverse would also be true. However, since data for the N_2 interactions are considerably more extensive than those for the CO interactions, this approximation usually amounts to a method for estimating data for interactions involving CO from the corresponding interactions involving N_2 .

Although the list of interactions in table VIII is not complete, it is fairly comprehensive. An effort was made to include data for all the important species and for many of the interactions between unlike species. There are two exceptions, however. First, no data have been included for ionized species; and second, data for only a few organic molecules have been included.

Relaxation data included with the program are given in table IX. Only rotational collision numbers are included. The Hirschfelder-Eucken approximation is used for vibrational relaxation ($Z_{\text{vib}} = \infty$). Most of the collision numbers given for nonpolar or slightly polar molecules were obtained by fitting the experimental thermal conductivity data to equation (22), with $\lambda_{\text{internal}}$ given by equation (19), and letting $Z_{\text{vib}} = \infty$. All Z_{rot} were assumed to be independent of temperature. (The numbers given in table IX represent average values over the entire temperature range.) There were two reasons for doing this. One reason is that calculated values of Z_{rot} are usually quite sensitive to changes in the values of the viscosity and thermal conductivity used in the calculations.

Furthermore, since the uncertainty in the thermal conductivity is sometimes rather large, it often leads to very large uncertainties in the calculated collision number. The other reason is that at higher temperatures the absence of experimental thermal conductivity data means that Z_{rot} would have to be determined by some alternate technique. A reasonable procedure would be to extrapolate Z_{rot} to higher temperatures by means of some theoretical expression for the temperature dependence. However, investigators who have studied the temperature dependence from theoretical considerations have obtained significantly different results (refs. 29 to 31). Therefore, it seemed unwise to include temperature-dependent collision numbers without even being sure of the temperature dependence of Z_{rot} . Consequently, Z_{rot} was assumed to be a constant, and the numbers listed in table IX apply to all temperatures.

In some cases the experimental thermal conductivity data indicated a Z_{rot} less than unity. However, this seems inconsistent with the general physical notion of a collision number, and so for these cases Z_{rot} was set equal to 1.

For large collision numbers the calculated thermal conductivity is insensitive to variations in the collision number. A large range of Z_{rot} will adequately fit the experimental data. It becomes difficult, if not impossible, to determine a rotational collision number by just fitting thermal conductivity data. For a Z_{rot} of about 20 or more, there is very little difference between the thermal conductivity calculated by using Z_{rot} and that calculated from the Hirschfelder-Eucken approximation ($Z_{\text{rot}} = \infty$). Consequently, when the experimental thermal conductivity data indicated rather large collision numbers, the Hirschfelder-Eucken approximation was assumed.

For some species, viscosity data were available but thermal conductivity data were not. For these species the rotational collision numbers were estimated from the expression derived by Sather and Dahler (ref. 32) for a rough sphere surrounded by an attractive square-well potential. Their results for the rotational relaxation time τ may be expressed as

$$\tau^{-1} = \frac{16}{3} \left(\frac{\rho}{m_a} \right) \sigma^2 \left(\frac{\pi kT}{m_a} \right)^{1/2} \left[\frac{4I/m_a \sigma^2}{(1 + 4I/m_a \sigma^2)^2} \right] g(\sigma) \quad (40)$$

Considering only the low-density limit of the radial distribution function $g(\sigma)$ (ref. 14, p. 321)

$$g(\sigma) \cong \exp\left(\frac{\epsilon}{kT}\right) \quad (41)$$

and defining a collision number Z_{rot} as (ref. 18)

$$Z_{\text{rot}} = \left(\frac{4}{\pi}\right) \left(\frac{P\tau}{\eta}\right) \quad (42)$$

we can substitute into equation (40) to obtain a value for Z_{rot} . If we further assume that the viscosity η can be calculated from the equation for viscosity of rigid-sphere molecules (ref. 14)

$$\eta = \frac{5}{16} \frac{(\pi m_a kT)^{1/2}}{\pi \sigma^2} \quad (43)$$

and use the ideal-gas law, the rotational collision number is given by

$$Z_{\text{rot}}^{-1} = \frac{5\pi}{12} \left[\frac{4I/m_a \sigma^2}{(1 + 4I/m_a \sigma^2)^2} \right] \exp\left(\frac{\epsilon}{kT}\right) \quad (44)$$

Equation (44) can be used to calculate a collision number directly or to calculate a ratio of the collision numbers of two species. The advantage of calculating a ratio is that it enables one to make use of a species for which the rotational collision number is known. This was the procedure used in obtaining the collision numbers shown in table IX. Molecules treated in this way are indicated, along with the species of 'known' Z_{rot} used to make the estimate. In this report, the collision numbers obtained by fitting thermal conductivity data are considered to be the known Z_{rot} .

The equation is temperature dependent. However, since temperature dependences are not given for the species of 'known' Z_{rot} , they are not given for the calculated ones either. The temperature actually used in each calculation was an average temperature. This average temperature was found by taking the average of the temperature range used in determining the Z_{rot} of the reference species ('known' Z_{rot}).

Collision numbers for the polar gases were taken from Zeleznik and Svehla (ref. 29). These are theoretical values of Z_{rot} based on a classical calculation of rotational relaxation times. The calculated values of Z_{rot} do have a temperature dependence. These are shown in table IX.

CONCLUDING REMARKS

The program described in this report is complete as it is presented herein. However, changes may occur from time to time as the authors become aware of improved techniques for doing the calculations. Though these changes may not be published, an outside organization requesting the program automatically receives the latest version.

Improved calculational results may also be obtained with the addition of new thermodynamic and transport data or with the updating of data already included in the program. This can be done by the program user if he has data to be added or changed, or he can send for the authors' updated version of the data.

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APPENDIX A

SYMBOLS

A_e/A_t	ratio of nozzle exit area to throat area, dimensionless
A_k	chemical formula of species k, dimensionless
A_{ij}^*	$\bar{\Omega}_{ij}(2,2)/\bar{\Omega}_{ij}(1,1)$, dimensionless
a	sonic velocity, m/sec
a_{ik}	stoichiometric coefficient for species k in reaction i, dimensionless
B_{ij}^*	$[5\bar{\Omega}_{ij}(1,2) - 4\bar{\Omega}_{ij}(1,3)]/\bar{\Omega}_{ij}(1,1)$, dimensionless
b_{ij}	matrix coefficient in eq. (10), (m)(sec)(K)/J
C_F	coefficient of thrust, dimensionless
C_p	heat capacity at constant pressure, J/(kg-mole)(K)
c_{ij}	matrix coefficient in eq. (7), (m)(sec)/kg
c_p	specific heat at constant pressure, J/(kg)(K)
c^*	characteristic velocity, m/sec
D_{ij}	binary diffusion coefficient, m^2/sec
d_{ij}	matrix coefficient in eq. (29), dimensionless
F/A	fuel-to-air weight (or mass) ratio or fuel-to-oxidant weight (or mass) ratio, dimensionless
% F	percent of total fuel in total reactant by weight (or mass), dimensionless
g_{ij}	matrix coefficient in eq. (26), (m)(sec)/kg-mole
$g(\sigma)$	radial distribution function evaluated at σ , dimensionless
H	enthalpy, J/kg-mole
H_0^0	standard-state enthalpy at 0 K, J/kg-mole
ΔH	heat of reaction, J/kg-mole
$(\Delta H_f^0)_T$	heat of formation at temperature T, J/kg-mole
h	enthalpy, J/kg
I	moment of inertia, (kg)(m^2)
I_{sp}	specific impulse with exit and ambient pressure equal, (N)(sec)/(kg)
I_{vac}	vacuum specific impulse, (N)(sec)/(kg)

k	Boltzmann's constant per molecule, 1.380622×10^{-23} J/K
Le	Lewis number (defined by eq. (32)), dimensionless
M	molecular weight, kg/kg-mole
m_a	molecular mass, kg
N_A	Avogadro's number, 6.022169×10^{26} molecules/kg-mole
n	number of gaseous species included in transport calculations, dimensionless
O/F	oxidant-to-fuel weight (or mass) ratio, dimensionless
P	pressure, N/m ²
P_c/P	ratio of combustion pressure to exit pressure, dimensionless
Pr	Prandtl number ($c_p \eta / \lambda$), dimensionless
R	gas constant, 8314.3 J/(kg-mole)(K) or 1.987165 cal/(g-mole)(K)
r	equivalence ratio, dimensionless
S	entropy, J/(kg-mole)(K)
S_0^0	standard-state entropy at 0 K, J/(kg-mole)(K)
s	entropy, J/(kg)(K)
T	temperature, K
U	internal energy, J/kg-mole
u_1	velocity of unshocked gas relative to incident shock front, m/sec
u_2	velocity of incident-shocked gas relative to incident shock front, m/sec
V	volume, m ³
v_2	actual velocity of incident-shocked gases in fixed coordinates, m/sec
X_i	unknown in eq. (28), dimensionless
x_i	mole fraction of species i, dimensionless
Z_i	collision number of species i, dimensionless
γ	isentropic exponent ($\partial \ln P / \partial \ln \rho$) _S , dimensionless
δ	correction term in eq. (14) for resonant exchange of rotational energy, dimensionless
ϵ	depth of potential energy well, J
η	viscosity, kg/(m)(sec)
η_i	unknown in eq. (6), kg/(m)(sec)

η_{i}	viscosity of species i , kg/(m)(sec)
η_{ij}	defined quantity (see eq. (7c)), kg/(m)(sec)
λ	thermal conductivity, J/(m)(sec)(K)
λ_j	unknown in eq. (9), J/(m)(sec)(K)
λ_{ij}	defined quantity (see eq. (10c)), J/(m)(sec)(K)
$\lambda_{r,i}$	unknown in eq. (23), kg-mole/(m)(sec)
$\Delta\lambda$	correction term involving relaxation effects, J/(m)(sec)(K)
ν	number of chemical reactions, dimensionless
$\pi\bar{\Omega}(l, s)$	collision cross section (equivalent to $\pi\sigma^2\Omega(2,2)^*$ of ref. 14), m^2
ρ	density, kg/m^3
σ	molecular diameter in eq. (40), m
τ	rotational relaxation time, sec

Subscripts:

eq	equilibrium
exp	experimentally measured value
frozen	chemically frozen (nonreacting)
HE	Hirschfelder -Eucken
i, j, k, l	index for species or reaction number
int	pertaining to internal energy modes
mixture	for the mixture
monatomic	translational energy contribution for a single species
P	at constant pressure
reaction	chemical reaction contribution
rot	rotational
S	at constant entropy
T	at constant temperature
trans	translational
vib	vibrational

Superscript:

o	standard state
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APPENDIX B

VARIABLES, INDICES, AND CONSTANTS USED IN TRANSPORT SUBROUTINES

FORTRAN symbol	Dimension	Common label ^a	Transport subroutines used ^b	Description and comments ^c
A	10,100	SPECES	INPUT	Stoichiometric coefficient A(i,j) of element i in species j
ANS	15	TRANS	TRANSP OUT	Output results (each ANS equivalenced to a particular property)
ANSR	3	INTERP	INPUT LGRNGE	Answer vector from Lagrange interpolation
ASTAR	20,20	TRANS	TRANSP INPUT	$\bar{\omega}_{ij}^{(2,2)}/\bar{\omega}_{ij}^{(1,1)}, A_{ij}^*$
ATOM	3,101	MISC	INPUT	For atom j ATOM(1,j) = atomic symbol ATOM(2,j) = atomic weight ATOM(3,j) = atomic valence
AVGDRO	1	DATA STATEMENT	TRANSP	Avgadro's Number (without the exponent 10 ²⁶)
BIGEN	1	-----	INPUT	Test number in finding largest EN
BOLTZ	1	DATA STATEMENT	TRANSP	Boltzmann's Constant (without the exponent 10 ⁻²³)
BSTAR	20,20	TRANS	TRANSP INPUT	$(5\bar{\omega}_{ij}^{(1,2)} - 4\bar{\omega}_{ij}^{(1,3)})/\bar{\omega}_{ij}^{(1,1)}, B_{ij}^*$
CHECK	20	DIMENSION STATEMENT	TRANSP	Check of results from GAUSS solution, double precision
COEFF	1	-----	INPUT	Stoichiometric coefficient of species to be eliminated (in the reaction to be eliminated)
CONST	1	-----	TRANSP	Coefficient in $n_{ij}, 5/16(10^{54}k/\pi N_A)^{1/2}$
CPEQ	1	EQUIVALENCE STATEMENT	TRANSP	Equilibrium specific heat of mixture, $c_{p,eq}$
CPFROZ	1	EQUIVALENCE STATEMENT	TRANSP	Frozen specific heat of mixture, $c_{p,frozen}$
CPREAC	1	EQUIVALENCE STATEMENT	TRANSP	Reaction specific heat of mixture, $c_{p,reaction}$
CPRR	20	TRANS	TRANSP	Dimensionless heat capacity, C_p/R
CVIBR	20	TRANS	TRANSP INPUT	Vibrational heat capacity, C_{vib}
DELH	17	DIMENSION STATEMENT	TRANSP	Heat of reaction, $\Delta H/RT$
DENSTY	1	EQUIVALENCE STATEMENT	TRANSP	Gas density of mixture used in transport calculations, ρ
EN	100,13	SPECES	INPUT	EN(i,j) - kg-moles of species i per kg of mixture for point j
ENTLPY	1	EQUIVALENCE STATEMENT	TRANSP OUT	Enthalpy, H
ENTRPY	1	-----	OUT	Entropy, S
ETA	20,20	DIMENSION STATEMENT	TRANSP	Quantity defined in equation (7), η_{ij}

^aCommon block is specified. If it is not in a common block, the type of statement is indicated. If it is in neither, a dash is shown.

^bIn most cases only the transport subroutines are listed. However, in some cases, it was useful to list the other routines in order to describe the application.

^cFORTTRAN IV convention is followed unless otherwise indicated. If the variable is real, integer, logical, or double precision, it is so indicated.

NOT REPRODUCIBLE

FORTTRAN symbol	Dimension	Common label	Transport subroutines used	Description and comments
EQCON	1	EQUIVALENCE STATEMENT	TRANSP	Equilibrium thermal conductivity of mixture, λ_{mixture}
EQRAT	1	MISC	OUT	Equivalence ratio
FIRSTP	1	SAVED	OUT	First pressure, P
FIRSTV	1	SAVED	OUT	First volume, V
FPC	1	-----	OUT	Fuel percent, $1/(1 + OF)$
FROZN	1	CONTRL	TRANSP INPUT OUT	Point is frozen if FROZN = T, logical variable
FRZCON	1	EQUIVALENCE STATEMENT	TRANSP	Frozen thermal conductivity of mixture, λ_{frozen}
G	20,21	DOUBLE	TRANSP GAUSS	Matrix coefficients, double precision
GMAT	20,21	DIMENSION STATEMENT	TRANSP	Set equal to G, used for checking results from GAUSS, double precision
HRRT	20	TRANS	TRANSP	Dimensionless enthalpy, H/RT
IATOM	3,101	DIMENSION STATEMENT EQUIVALENCE STATEMENT	INPUT	Equivalenced to ATOM, used to identify elements in calculating molecular weights
IMAT	1	INDX	TRANSP	Number of equations in GAUSS solution
IND	20	SAVED	TRANSP INPUT	Index to identify species used in transport calculations
INTCON	1	EQUIVALENCE STATEMENT	TRANSP	Internal thermal conductivity of mixture, $\lambda_{\text{internal}}$, real variable
INTRNL	1	-----	OUT	Internal energy of first point, U, real variable
ISV	1	INDX	TRANSP OUT	Used as test in controlling transport output ISV \neq 0: more thermodynamic calculations to follow ISV = 0: end of thermodynamic calculations of problem
ITT	1	-----	OUT	Current temperature expressed as integer
IUSE	100	SPECES	SEARCH INPUT	Used as test to see if species is condensed
LEWIS	1	EQUIVALENCE STATEMENT	TRANSP OUT	Lewis number, Le, real variable
LLL	1	SAVED	OUT	Index to control spacing interval in transport output
LLMT	10	MISC	INPUT	Alphameric symbols for elements
LM	1	SAVED	OUT	Index of current point being processed in transport output
MAXNM	1	DATA STATEMENT	INPUT	Maximum number of species allowed
MAXNP	1	SAVED	TRANSP INPUT OUT	Index used in controlling transport output
MONCON	1	EQUIVALENCE STATEMENT	TRANSP	Translational thermal conductivity of mixture, λ_{trans} , real variable



FORTTRAN symbol	Dimension	Common label	Transport subroutines used	Description and comments
N	1	TRANS	TRANSP INPUT OUT	Index of current point
ND	1	DATA STATEMENT	SEARCH TRANSP INPUT	Indicates end of transport data
NFZ	1	PERF	INPUT OUT	Index of freezing point
NLM	1	INDX	INPUT	Number of elements in the system
NM	1	SAVED	TRANSP INPUT	Number of species in transport calculations, n
NODATA	1	CONTRL	INPUT	If NODATA = T, message is printed out whenever cross section data are not found in the library - applies only to data for a pure species, logical variable
NPT	1	INDX	TRANSP	Number of points in current set
NR	1	TRANS	TRANSP INPUT	Number of chemical reactions, v
NS	1	INDX	SEARCH TRANSP INPUT	Number of species in the thermodynamic calculations
NSP	1	-----	INPUT	Special index used to change A array to add an element which has been omitted through use of an OMIT card
NTAB	100	TRANS	TRANSP INPUT	} Code to specify type of data used in transport calculations: = 0 if relaxation data = 1 if transport cross sections
NTB	1	-----	SEARCH TRANSP INPUT	
NTP	1	-----	SEARCH TRANSP INPUT LGRNGE	} Number of entries in table of transport or relaxation data (data stored in TABLES)
NTT	100	TRANS	TRANSP INPUT	
OF	1	MISC	OUT	Oxidant-to-fuel weight ratio
OMEGA	20,20	TRANS	TRANSP INPUT	Viscosity cross section, $\bar{\omega}^{(2,2)}$
PI	1	DATA STATEMENT	TRANSP	π , 3.14159265
PP	1	MISC	TRANSP OUT	Pressure of current point
PPP	13	POINTS	TRANSP OUT	Pressure schedule for output
PREQ	1	EQUIVALENCE STATEMENT	TRANSP	Equilibrium Prandtl number of mixture, Pr_{eq}
PRFROZ	1	EQUIVALENCE STATEMENT	TRANSP	Frozen Prandtl number of mixture, Pr_{frozen}
PUNCH	1	CONTRL	OUT	If PUNCH = T output is included on punched cards, logical variable
R	1	MISC	TRANSP OUT	Universal gas constant, 1.987165 cal/(g-mole)(K) or 8.31430 J/(kg-mole)(K)

FORTTRAN symbol	Dimension	Common label	Transport subroutines used	Description and comments
REACON	1	EQUIVALENCE STATEMENT	TRANSP	Reaction thermal conductivity of mixture, $\lambda_{\text{reaction}}$
RELXTN	20	TRANS	TRANSP	Temporary storage used in calculating $\lambda_{\text{internal}}$ } Number of rotational degrees of freedom
ROTM	20	TRANS	TRANSP INPUT	
ROTN	1	-----	SEARCH TRANSP	
ROTNM	80	TRANS	TRANSP INPUT	
RPVT	1	DATA STATEMENT	TRANSP	Universal gas constant, $82.0562 \text{ (cm}^3\text{)(atm)/(g-mole)/(K)}$
SPECE	2,3	DIMENSION STATEMENT	SEARCH	Alphameric identification of current interaction, integer variable
		TRANS	TRANSP	
SPECIE	100,2,3	TRANS	TRANSP INPUT	Alphameric identification of interaction which is put in core storage with TABLES, integer variable
STC	17,20	TRANS	TRANSP INPUT	Table of stoichiometric coefficients, a_{ik}
STCF	17,20	TRANS	INPUT	Intermediate storage of stoichiometric coefficients
STCOEF	20	TRANS	INPUT	Result of dividing stoichiometric coefficients of each species (in the reaction to be eliminated) by COEFF
STORE	52,16	SAVED	OUT	Temporary storage of transport calculations, while thermodynamic calculations are continued
SUB	100,3	SPECES	SEARCH TRANSP INPUT	Alphameric name of species included in thermodynamic calculations, integer variable
TABLES	100,20,3	TRANS	TRANSP INPUT	} Tables of cross sections and relaxation data
TABLS	20,3	DIMENSION STATEMENT	SEARCH	
TEM	100,20	TRANS	TRANSP INPUT	Temperature schedule for TABLES
TEMPR	20	DIMENSION STATEMENT	SEARCH	Temperature schedule for TABLS
TESTEN	1	-----	INPUT	Smallest EN allowed in transport calculations
TRNSPT	1	CONTRL	LINK	If TRNSPT = F transport calculations are omitted, logical variable
TT	1	MISC	TRANSP INPUT OUT LGRNGE	Temperature of current point
TTT	13	POINTS	TRANSP	Temperature schedule for output
VISC	1	EQUIVALENCE STATEMENT	TRANSP	Viscosity of mixture, η_{mixture}
WM	13	POINTS	INPUT	Molecular weight of the mixture in thermodynamic calculations
WMOL	20	SAVED	TRANSP INPUT	Molecular weight of pure species, M_i
WTMOL	1	EQUIVALENCE STATEMENT	TRANSP	Molecular weight of the mixture in transport calculations, M

FORTTRAN symbol	Dimension	Common label	Transport subroutines used	Description and comments
X	20	DOUBLE	TRANSP GAUSS	Answer region for matrix solution, double precision
XS	20	SAVED	TRANSP INPUT	Mole fraction of species used in transport calculations
XSKL	20,20	DIMENSION STATEMENT	TRANSP	$(XS(k) \cdot XS(l))^{-1}$
Y	20,3	INTERP	INPUT LGRNGE	Table in subroutine LGRNGE interpolation
Z	20	INTERP	INPUT LGRNGE	Argument in subroutine LGRNGE interpolation
ZROT	20	TRANS	TRANSP INPUT	Rotational collision number, Z_{rot}
ZVIB	20	TRANS	TRANSP INPUT	Vibrational collision number, Z_{vib}

APPENDIX C

PROGRAM LISTING

C	MAIN PROGRAM	LINK	1
C		LINK	2
C	LINKS SUBROUTINES FOR THERMODYNAMIC AND TRANSPORT CALCULATIONS FOR LINK	LINK	3
C		LINK	4
C	DOUBLE PRECISION G,X	LINK	5
C		LINK	6
C	REAL MIX(15)	LINK	7
C	INTEGER SPECE	LINK	8
C	INTEGER DATA, OMIT, INSERT, REAC, BLANK, THRM, END, SUB	LINK	9
C		LINK	10
C	LOGICAL SHOCK, MMHG, UV, IC, DETN, SIUNIT, EUNITS, NSQM	LINK	11
C	LOGICAL HP, SP, TP, NEWR, IONS, MOLES, FROZ, EQL, PSIA, RKT, VOL, TV, SV	LINK	12
C	LOGICAL FA, OF, ERATIO, FPCT, OTTO	LINK	13
C	LOGICAL TRNSPT, FROZN, PUNCH, NCDATA	LINK	14
C		LINK	15
C	COMMON /POINTS/HSUM(13), SSUM(13), CPR(13), DLVTP(13), DLVPT(13),	LINK	16
C	1 GAMMAS(13), P(26), T(52), V(26), PPP(13), WM(13), SONVEL(13), TTT(13),	LINK	17
C	2 VLM(13), TCTN(13)	LINK	18
C	COMMON /SPECES/COEF(2,7,100), S(100), HO(100), DELN(100), DUMMY(100),	LINK	19
C	1 EN(100,13), ENLN(100), A(10,100), SUB(100,3), IUSE(100), TEMP(50,2)	LINK	20
C	COMMON /MISC/ENN, SUMN, TT, SO, ATOM(3,101), LLMT(10), BO(10), BOP(10,2),	LINK	21
C	1 TM, TLOW, TMID, THIGH, PP, CPSUM, OF, EQRT, FPCT, R, RR, HSUBO, AM(2),	LINK	22
C	2 HPP(2), RH(2), VMIN(2), VPLS(2), WP(2), DATA(22), NAME(15,5),	LINK	23
C	3 ANUM(15,5), PECWT(15), ENTH(15), FAZ(15), RTEMP(15), FOX(15), DENS(15),	LINK	24
C	4 RHOP, RMW(15), TLN, CR, OXF(15), ENNL, TRACE, LLMTS(10), SBOP(10,2)	LINK	25
C	COMMON /DOUBLE/ G(20,21), X(20)	LINK	26
C	COMMON /INDX/IDERUG, CONVG, TP, HP, SP, ISV, NPP, MOLES, NP, NT, NPT, NLM,	LINK	27
C	1 NS, KMAT, IMAT, IQ1, IOF, NOF, NOMIT, IP, NEWR, NSUB, NSUP, RKT, DETN, SHOCK,	LINK	28
C	2 ICNS, NC, NSERT, JSOL, JLIQ, KASE, NREAC, IC, JS1, VOL, IT, CALCH, NLS, LOGV,	LINK	29
C	3 ISUP, ISUB, ITNUM, ITM, INCDFZ, INCDEQ, CPRF, IPP, SEQL, PCPLT	LINK	30
C	COMMON /PERF/PCP(22), VMOC(13), SPIM(13), VACI(13), SUBAR(13),	LINK	31
C	1 SUPAR(13), APP(13), AEAT(13), CSTR, EQL, FROZ, SSO, AREA, AWT, NFZ,	LINK	32
C	2 APPL, ARATIO, ELN	LINK	33
C	COMMON /SAVED/SLN(100), IQSAVE, ENSAVE, ENLSAV, LSAVE, JSOLS, JLIQS,	LINK	34
C	1 LLL, LM, MAXNP, STORE(52,16), XS(20), WMOL(20), IND(20), NM,	LINK	35
C	2 FIRSTP, FIRSTV	LINK	36
C	COMMON /CONTRL/TRNSPT, FROZN, PUNCH, NODATA	LINK	37
C		LINK	38
C		LINK	39
C	LM = 0	LINK	40
C	MAXNP = 0	LINK	41
C	NEWR = .FALSE.	LINK	42
C	NLS = 0	LINK	43
C	1 CALL MAIN	LINK	44
C	2 IF(NPT.EQ.0) GO TO 1	LINK	45
C	IF(.NOT.RKT.AND..NOT.SHOCK) GO TO 7	LINK	46
C	IF(.NOT.EQL) FROZN = .TRUE.	LINK	47
C	IF(EQL) FROZN = .FALSE.	LINK	48
C	7 IF(.NOT.TRNSPT) GO TO 8	LINK	49
C	CALL TRANSP	LINK	50
C	8 IF(.NOT.RKT) GO TO 3	LINK	51
C	CALL ROCKT1 (\$1)	LINK	52
C	GO TO 2	LINK	53
C	3 IF(.NOT.DETN) GO TO 4	LINK	54
C	CALL DETON1 (\$1)	LINK	55
C	GO TO 2	LINK	56

4	IF(.NOT.SHOCK) GC TO 5	LINK	57
	CALL SHCK1 (\$1)	LINK	58
	GO TO 2	LINK	59
5	CONTINUE	LINK	60
	CALL THERM1 (\$1)	LINK	61
	GO TO 2	LINK	62
	END	LINK	63

C	SUBROUTINE GAUSS	GAUS	1
C		GAUS	2
C	SOLVE ANY LINEAR SET OF UP TO 20 EQUATIONS	GAUS	3
C	NUMBER OF EQUATIONS = IMAT	GAUS	4
C		GAUS	5
C	DOUBLE PRECISION G,X,COEFX(20),SUM,Z	GAUS	6
C		GAUS	7
	COMMON/DOUBLE/G(20,21),X(20)	GAUS	8
	COMMON /INDX/IDEBUG,CONVG,TP,HP,SP,ISV,NPP,MOLES,NP,NT,NPT,NLM,	GAUS	9
	1 NS,KMAT,IMAT,IQ1,IOF,NOF,NOMIT,IP,NEWR,NSUB,NSUP,RKT,DETN,SHOCK,	GAUS	10
	2 ICNS,NC,NSERT,JSOL,JLIQ,KASE,NREAC,IC,JS1,VOL,IT,CALCH,NLS,LOGV,	GAUS	11
	3 ISUP,ISUB,ITNUM,ITM,INCDFZ,INCDEQ,CPRF,IPP,SEQL,PCPLT	GAUS	12
C		GAUS	13
C	DATA BIGNO/1.E+38/	GAUS	14
C		GAUS	15
C	BEGIN ELIMINATION OF NNTH VARIABLE	GAUS	16
C		GAUS	17
	IUSE1 = IMAT+1	GAUS	18
6	DO 45 NN=1,IMAT	GAUS	19
	IF(NN-IMAT) 8,83,8	GAUS	20
83	IF(G(NN,NN)) 31,23,31	GAUS	21
C		GAUS	22
C	SEARCH FOR MAXIMUM COEFFICIENT IN EACH ROW	GAUS	23
C		GAUS	24
8	DO 18 I=NN,IMAT	GAUS	25
	COEFX(I) = BIGNO	GAUS	26
	IF(G(I,NN).EQ.0.) GC TO 18	GAUS	27
	COEFX(I) = 0.	GAUS	28
	DO 10 J=NN,IUSE1	GAUS	29
	SUM = G(I,J)	GAUS	30
	IF(SUM.LT.0.) SUM=-SUM	GAUS	31
	IF(J.NE.NN) GO TO 9	GAUS	32
	Z = SUM	GAUS	33
	GO TO 1C	GAUS	34
9	IF(SUM.GT.COEFX(I)) COEFX(I)=SUM	GAUS	35
1C	CONTINUE	GAUS	36
	COEFX(I) = COEFX(I)/Z	GAUS	37
1E	CONTINUE	GAUS	38
C		GAUS	39
C	LOCATE ROW WITH SMALLEST MAXIMUM COEFFICIENT	GAUS	40
C		GAUS	41
	TEMP = BIGNO	GAUS	42
	I=0	GAUS	43
2C	DO 22 J=NN,IMAT	GAUS	44
	IF (COEFX(J)-TEMP) 87,22,22	GAUS	45
87	TEMP=COEFX(J)	GAUS	46
	I=J	GAUS	47
22	CONTINUE	GAUS	48
	IF(I) 28,23,28	GAUS	49



C		GAUS	50
C	INDEX I LOCATES EQUATION TO BE USED FOR ELIMINATING THE NTH	GAUS	51
C	VARIABLE FROM THE REMAINING EQUATIONS	GAUS	52
C		GAUS	53
C	INTERCHANGE EQUATIONS I AND NN	GAUS	54
C		GAUS	55
	28 IF(NN-I) 29,31,29	GAUS	56
	29 DO 30 J=NN,IUSE1	GAUS	57
	Z=G(I,J)	GAUS	58
	G(I,J)=G(NN,J)	GAUS	59
	G(NN,J)=Z	GAUS	60
	30 CONTINUE	GAUS	61
C		GAUS	62
C	DIVIDE NTH ROW BY NTH DIAGONAL ELEMENT AND ELIMINATE THE NTH	GAUS	63
C	VARIABLE FROM THE REMAINING EQUATIONS	GAUS	64
C		GAUS	65
	31 K = NN + 1	GAUS	66
	DO 36 J = K, IUSE1	GAUS	67
	IF(G(NN,NN).EQ.0.) GO TO 23	GAUS	68
	G(NN,J) = G(NN,J) / G(NN,NN)	GAUS	69
	36 CONTINUE	GAUS	70
	IF(K-IUSE1) 88,45,88	GAUS	71
	88 DO 44 I=K,IMAT	GAUS	72
	40 DO 44 J = K,IUSE1	GAUS	73
	G(I,J) = G(I,J) - G(I,NN)*G(NN,J)	GAUS	74
	44 CONTINUE	GAUS	75
	45 CONTINUE	GAUS	76
C		GAUS	77
C	BACKSOLVE FOR THE VARIABLES	GAUS	78
C		GAUS	79
	K = IMAT	GAUS	80
	47 J = K + 1	GAUS	81
	X(K) = 0.000	GAUS	82
	SUM = 0.0	GAUS	83
	IF(IMAT-J) 51,48,48	GAUS	84
	48 DO 50 I=J,IMAT	GAUS	85
	SUM = SUM + G(K,I)* X(I)	GAUS	86
	50 CONTINUE	GAUS	87
	51 X(K) = G(K,IUSE1) - SUM	GAUS	88
	K = K - 1	GAUS	89
	IF(K) 47,151,47	GAUS	90
	23 IMAT = IMAT-1	GAUS	91
	151 RETURN	GAUS	92
	END	GAUS	93
C	SUBROUTINE MAIN	MAIN	1
C		MAIN	2
C	MAIN PROGRAM FOR THERMODYNAMIC CALCULATIONS	MAIN	3
C		MAIN	4
	DOUBLE PRECISION G,X	MAIN	5
C		MAIN	6
C	THE FOLLOWING DOUBLE PRECISION TYPE STATEMENTS ARE REQUIRED FOR	MAIN	7
C	IBM 360 MACHINES ONLY	MAIN	8
C		MAIN	9
C	DOUBLE PRECISION HSUM,SSUM,CPR,DLVTP,DLVPT,GAMMAS	MAIN	10
C	DOUBLE PRECISION COEF,S,EN,ENLN,HO,DELN	MAIN	11



C	REAL MIX(15)	MAIN 12
	INTEGER SPECE	MAIN 13
	INTEGER DATA, OMIT, ENSERT, REAC, BLANK, THRM, END, SUB	MAIN 14
	LOGICAL SHOCK, MMHG, UV, IC, DETN, SIUNIT, EUNITS, NSQM, CALCH	MAIN 15
	LOGICAL HP, SP, TP, NEWR, IONS, MOLES, FROZ, EQL, PSIA, RKT, VOL, TV, SV	MAIN 16
	LOGICAL FA, OF, ERATIO, FPCT, OTTO	MAIN 17
	LOGICAL. TRNSPT, FROZN, PUNCH, NCDATA	MAIN 18
C		MAIN 19
	DIMENSION OMIT(3,3), NCD(4), ENSERT(3,3), RHO(26), LVP(2), VM(2),	MAIN 20
	1 VL(26), DAT(22)	MAIN 21
	DIMENSION SPECE(2,3), TEMPR(2C), TABLS(20,3)	MAIN 22
C		MAIN 23
	COMMON SPECE, TEMPR, TABLS	MAIN 24
C		MAIN 25
	COMMON /POINTS/HSUM(13), SSUM(13), CPR(13), DLVTP(13), DLVPT(13),	MAIN 26
	1 GAMMAS(13), P(26), T(52), V(13), PPP(13), WM(13), SONVEL(13), TTT(13),	MAIN 27
	2 VLM(13), TOTN(13)	MAIN 28
	COMMON /SPECES/COEF(2,7,100), S(100), HO(100), DELN(100), DUMMY(100),	MAIN 29
	1 EN(100,13), ENLN(100), A(10,100), SUB(100,3), IUSE(100), TEMP(50,2)	MAIN 30
	COMMON /MISC/ENN, SUMN, TT, SO, ATOM(3,101), LLMT(10), BO(10), BOP(10,2),	MAIN 31
	1 TM, TLOW, TMID, THIGH, PP, CPSUM, OF, EQRAT, FPCT, R, RR, HSUBO, AM(2),	MAIN 32
	2 HPP(2), RH(2), VMIN(2), VPLS(2), WP(2), DATA(22), NAME(15,5),	MAIN 33
	3 ANUM(15,5), PECWT(15), ENTH(15), FAZ(15), RTEMP(15), FCX(15), DENS(15),	MAIN 34
	4 RHOP, RMH(15), TLN, CR, OXF(15), ENNL, TRACE, LLMTS(10), SBOP(10,2)	MAIN 35
	COMMON /DOUBLE/ G(20,21), X(20)	MAIN 36
	COMMON /INCX/IDEBUG, CONVG, TP, HP, SP, ISV, NPP, MOLES, NP, NT, NPT, NLM,	MAIN 37
	1 NS, KMAT, IMAT, IQ1, IOF, NOF, NOMIT, IP, NEWR, NSUB, NSUP, RKT, DETN, SHOCK,	MAIN 38
	2 IONS, NC, NSERT, JSOL, JLIQ, KASE, NREAC, IC, JS1, VOL, IT, CALCH, NLS, LOGV,	MAIN 39
	3 ISUP, ISUB, ITNUM, ITM, INCDFZ, INCDEQ, CPRF, IPP, SEQL, PCPLT	MAIN 40
	COMMON /PERF/PCP(22), VMOC(13), SPIM(13), VACI(13), SUBAR(13),	MAIN 41
	1 SUPAR(13), APP(13), AEAT(13), CSTR, EQL, FROZ, SSO, AREA, AWT, NFZ,	MAIN 42
	2 APPL, ARATIO, ELN	MAIN 43
	COMMON /CONTRL/TRNSPT, FROZN, PUNCH, NCDATA	MAIN 44
C		MAIN 45
	EQUIVALENC (OMIT, ENLN), (ENSERT, DELN), (OXF, MIX),	MAIN 46
	1 (OF, CXFL), (RHO, P, VL), (SO, SO), (OTTO, CPCVFR), (DATA, DAT)	MAIN 47
C		MAIN 48
	DATA MIT/4FOMIT/, BLANK/1H /, PSIA/4HPSIA/, REAC/4HREAC/, IZ/2HOO/,	MAIN 49
	1 NMLT/4HNAME/, IE/1HE/, INSERT/4HINSE/, THRM/4HTHER/, END/3HEND/,	MAIN 50
	2 GAS/1HG/, ND/4HLAST/	MAIN 51
C		MAIN 52
	NAMELIST/INPT2/KASE, T, P, PSIA, MMHG, NSQM, V, RHO, ERATIO, OF, FPCT, FA,	MAIN 53
	1MIX, TP, HP, SP, TV, UV, SV, RKT, SHOCK, DETN, OTTO, CR, SO, SO, IONS, IDEBUG,	MAIN 54
	2TRACE, SIUNIT, EUNITS, TRNSPT, FROZN, PUNCH, NCDATA	MAIN 55
C		MAIN 56
	NEWR = .FALSE.	MAIN 57
C		MAIN 58
	1 WRITE(6,400)	MAIN 59
	400 FORMAT(1F1)	MAIN 60
	RR = 8314.3	MAIN 61
	R = RR/4184.	MAIN 62
	203 READ (5,204) (DATA(I), I=1,15)	MAIN 63
	204 FORMAT(5(3A4,3X))	MAIN 64
	WRITE (6,2045)(DATA(I), I=1,15)	MAIN 65
	2045 FORMAT(1X,5(3A4,3X))	MAIN 66
	IF(DATA(1).EQ.THRM) GO TO 90	MAIN 67
	IF(DATA(1).EQ.REAC) GO TO 11	MAIN 68
	IF (DATA(1).EQ.MIT) GO TO 205	MAIN 69
	IF (DATA(1).EQ.INSERT) GO TO 180	MAIN 70
	IF(DATA(1).EQ.NMLT) GO TO 210	MAIN 71
	IF(DATA(1).EQ.BLANK) GO TO 203	MAIN 72
	1023 WRITE(6,1024)	MAIN 73
	1024 FORMAT(40H0ERROR IN ABOVE CARD. CONTENTS IGNORED.)	MAIN 74
	GO TO 203	MAIN 75
		MAIN 76

11	NSERT = 0	MAIN 77
	MOLES = .FALSE.	MAIN 78
	CALL REACT	MAIN 79
	IF(NLM.EQ.0) WRITE(6,52)	MAIN 80
52	FORMAT(24HCERROR IN REACTANT CARDS)	MAIN 81
	CALCH = .FALSE.	MAIN 82
	DC 755 N=1,NREAC	MAIN 83
	IF(NAME(N,5).EQ.IZ) CALCH=.TRUE.	MAIN 84
755	CONTINUE	MAIN 85
	GO TO 202	MAIN 86
C		MAIN 87
C	READ THERMO AND TRANSPORT DATA FROM CARDS AND STORE ON TAPE 4	MAIN 88
C		MAIN 89
90	NEWR = .TRUE.	MAIN 90
	REWIND 4	MAIN 91
	READ(5,5) TLOW, TMID, THIGH	MAIN 92
5	FORMAT (3F10.3)	MAIN 93
	WRITE (4,5) TLOW, TMID, THIGH	MAIN 94
97	READ (5,10)(DAT(I), I=1,16), NCD(1)	MAIN 95
10	FORMAT(3A4,6X,2A3,4(A2,F3.0),A1,2F10.3,I15)	MAIN 96
	IF(DATA(1).EQ.BLANK) DATA(1)=END	MAIN 97
	WRITE (4,10)(DAT(I), I=1,16)	MAIN 98
	IF(DATA(1).NE.END) GO TO 18	MAIN 99
	GO TO 13	MAIN 100
18	READ(5,20)(DAT(I), I=1,5), NCD(2), (DAT(J), J=6,10), NCD(3), (DAT(K),	MAIN 101
	1K=11,14), NCD(4)	MAIN 102
20	FORMAT(5E15.8,15/5E15.8,15/4E15.8,I20)	MAIN 103
	WRITE (4,21)(DAT(I), I=1,14)	MAIN 104
21	FORMAT(5E15.8/5E15.8/4E15.8)	MAIN 105
	DO 25 I=1,4	MAIN 106
	IF(NCD(I).EQ.I) GO TO 25	MAIN 107
	WRITE(6,22) (DATA(J), J=1,3)	MAIN 108
22	FORMAT(28HCERROR IN ORDER OF CARDS FOR ,3A4)	MAIN 109
25	CONTINUE	MAIN 110
	GO TO 97	MAIN 111
C		MAIN 112
C	TRANSPORT DATA CARDS	MAIN 113
C		MAIN 114
13	READ(5,14) ((SPECE(I,L), L=1,3), I=1,2), NTP, NTB, ROTN	MAIN 115
14	FORMAT(2(3A4,6X),2I5,F24.1)	MAIN 116
	WRITE(4) ((SPECE(I,L), L=1,3), I=1,2), NTP, NTB, ROTN	MAIN 117
	IF(SPECE(1,1).EQ.ND) GO TO 203	MAIN 118
	READ(5,15)(TEMPR(I), (TABLS(I,L), L=1,3), I=1, NTP)	MAIN 119
	WRITE(4) (TEMPR(I), (TABLS(I,L), L=1,3), I=1, NTP)	MAIN 120
15	FORMAT(4F10.4)	MAIN 121
	GO TO 13	MAIN 122
C		MAIN 123
C		MAIN 124
C	CHECK INSERT CARDS	MAIN 125
C		MAIN 126
180	DO 185 I=4,15,3	MAIN 127
	IF (DATA(I).EQ.BLANK) GO TO 185	MAIN 128
	NSERT = NSERT+1	MAIN 129
	ENSERT(1,NSERT) = DATA(I)	MAIN 130
	ENSERT(2,NSERT) = DATA(I+1)	MAIN 131
	ENSERT(3,NSERT) = DATA(I+2)	MAIN 132
185	CONTINUE	MAIN 133
	GO TO 202	MAIN 134
C		MAIN 135
C	CHECK OMIT CARDS	MAIN 136
C		MAIN 137
205	DC 208 I=4,15,3	MAIN 138
	IF(DATA(I).EQ.BLANK) GO TO 208	MAIN 139
	NOMIT = NOMIT+1	MAIN 140
	OMIT(1,NOMIT) = DATA(I)	MAIN 141

	OMIT(2,NCMIT) = DATA(I+1)	MAIN 142
	OMIT(3,NCMIT) = DATA(I+2)	MAIN 143
208	CONTINUE	MAIN 144
	NEW= .TRUE.	MAIN 145
	REWIND 4	MAIN 146
	GO TO 203	MAIN 147
C		MAIN 148
C	BEGIN NAMELIST INPT2	MAIN 149
C		MAIN 150
210	DO 299 I=1,26	MAIN 151
	P(I)= 0.	MAIN 152
	V(I) = 0.	MAIN 153
299	CONTINUE	MAIN 154
	DO 306 I=1,52	MAIN 155
	T(I)=C.	MAIN 156
306	CONTINUE	MAIN 157
	TRACE = C.	MAIN 158
	S0 = C.	MAIN 159
	V1 = C.	MAIN 160
	V2 = C.	MAIN 161
	CR = C.	MAIN 162
	RHCP = 0.	MAIN 163
	KASE= 0	MAIN 164
	TP = .FALSE.	MAIN 165
	HP=.FALSE.	MAIN 166
	SP=.FALSE.	MAIN 167
	TV = .FALSE.	MAIN 168
	UV = .FALSE.	MAIN 169
	SV = .FALSE.	MAIN 170
	OTTO = .FALSE.	MAIN 171
	RKT = .FALSE.	MAIN 172
	SHOCK = .FALSE.	MAIN 173
	DETN = .FALSE.	MAIN 174
	VOL = .FALSE.	MAIN 175
	MMHG = .FALSE.	MAIN 176
	PSIA = .FALSE.	MAIN 177
	NSQM = .FALSE.	MAIN 178
	SIUNIT = .FALSE.	MAIN 179
	EUNITS = .FALSE.	MAIN 180
	IONS = .FALSE.	MAIN 181
	IDEBUG = 0	MAIN 182
	FA= .FALSE.	MAIN 183
	OF= .FALSE.	MAIN 184
	ERATIO = .FALSE.	MAIN 185
	FPCT= .FALSE.	MAIN 186
	TRNSPT = .TRUE.	MAIN 187
	FROZN = .FALSE.	MAIN 188
	PUNCH = .FALSE.	MAIN 189
	NCDATA= .FALSE.	MAIN 190
	DO 303 I=1,15	MAIN 191
	MIX(I) = 0.	MAIN 192
303	CONTINUE	MAIN 193
	NT = 1	MAIN 194
	EQL = .TRUE.	MAIN 195
	READ(5,INPT2)	MAIN 196
	WRITE(6,INPT2)	MAIN 197
	IF(.NOT.CETN.AND..NOT.SHOCK) GO TO 1303	MAIN 198
	DO 1300 N=1,NREAC	MAIN 199
	IF(FAZ(N).NE.GAS) GO TO 1301	MAIN 200
1300	CONTINUE	MAIN 201
	GO TO 1303	MAIN 202
1301	WRITE(6,1302)	MAIN 203
1302	FORMAT(60HCONDENSED REACTANTS NOT PERMITTED IN DETN OR SHOCK PROB	MAIN 204
	1LEMS)	MAIN 205
	GO TO 1	MAIN 206

1303	IF(.NCT.TV.AND..NOT.CV.AND..NOT.SV) GO TO 304	MAIN 207
	VCL = .TRUE.	MAIN 208
	DO 1304 I=1,26	MAIN 209
	IF(RHO(I).NE.0.) VL(I) = 1./RHO(I)	MAIN 210
	IF(V(I).NE.0.) VL(I)=V(I)	MAIN 211
	IF(VL(I).EQ.0.) GO TO 1305	MAIN 212
	NP = I	MAIN 213
1304	CONTINUE	MAIN 214
1305	TP = TV	MAIN 215
	HP = UV	MAIN 216
	SP = SV	MAIN 217
	GO TO 322	MAIN 218
304	DO 305 I=1,26	MAIN 219
	IF(P(I).EQ.0.) GO TO 322	MAIN 220
	NP = I	MAIN 221
	IF(MMHG) P(NP) = P(NP)/760.	MAIN 222
	IF(PSIA) P(NP)=P(NP)/14.696C06	MAIN 223
	IF(NSQM) P(NP)=P(NP)/101325.	MAIN 224
305	CONTINUE	MAIN 225
322	DO 307 IT = 1,52	MAIN 226
	IF(T(IT).EQ.0.) GO TO 722	MAIN 227
	NT = IT	MAIN 228
307	CONTINUE	MAIN 229
722	DO 625 IST=1,15	MAIN 230
	IF(MIX(IST).NE.0.) GO TO 323	MAIN 231
	IF(IST.NE.1) GO TO 745	MAIN 232
	WRITE(6,724)	MAIN 233
724	FORMAT(48HONO INPT2 VALUE GIVEN FOR OF, EQRAT, FA, OR FPCT)	MAIN 234
	IF(WP(2).NE.0.) OXFL = WP(1)/WP(2)	MAIN 235
	GO TO 332	MAIN 236
323	OXFL = MIX(IST)	MAIN 237
	IF(FA) OXFL =1./MIX(IST)	MAIN 238
	IF(FPCT) OXFL =(100.-MIX(IST))/MIX(IST)	MAIN 239
	IF(.NOT.ERATIO) GO TO 333	MAIN 240
	EQRAT = MIX(IST)	MAIN 241
	IF(EQRAT.EQ.1.) EQRAT = 1.0C00045	MAIN 242
	OXFL = (-EQRAT*VMIN(2)-VPLS(2))/(VPLS(1)+EQRAT*VMIN(1))	MAIN 243
333	OXF(IST) = OXFL	MAIN 244
	NCF = IST	MAIN 245
625	CONTINUE	MAIN 246
745	IF(.NOT.ICNS) GO TO 746	MAIN 247
	IF(LLMT(NLM).EQ.IE) GO TO 746	MAIN 248
	NLM = NLM+1	MAIN 249
	IF(LLMT(NLM).NE.IE) NEWR=.TRUE.	MAIN 250
	REWIND 4	MAIN 251
	LLMT(NLM) = IE	MAIN 252
	BOP(NLM,1) = 0.	MAIN 253
	BOP(NLM,2) = 0.	MAIN 254
	GO TO 748	MAIN 255
746	IF(LLMT(NLM).NE.IE) GO TO 748	MAIN 256
	DO 747 J=1,NS	MAIN 257
	IF(A(NLM,J).NE.0.) IUSE(J)=-10000	MAIN 258
747	CONTINUE	MAIN 259
	NLM = NLM-1	MAIN 260
748	IF(NEWR) CALL SEARCH	MAIN 261
	IF(NS.EQ.0) GO TO 1	MAIN 262
C		MAIN 263
C	INITIAL ESTIMATES	MAIN 264
C		MAIN 265
	SO = SO/R	MAIN 266
	ENN = .1	MAIN 267
	ENNL = -2.3025851	MAIN 268
	SUMN = ENN	MAIN 269
	XI = NS - NC	MAIN 270



XI = ENN/XI	MAIN 271
XLN = ALOG(XI)	MAIN 272
DO 432 J=1,NS	MAIN 273
IF(IUSE(J).GT.0) IUSE(J)=-IUSE(J)	MAIN 274
IF(IUSE(J).EQ.-10000.AND.IONS) IUSE(J) = 0	MAIN 275
EN(J,1) = 0.	MAIN 276
ENLN(J) = 0.	MAIN 277
IF (IUSE(J).NE.0) GO TO 432	MAIN 278
EN(J,1) = XI	MAIN 279
ENLN(J) = XLN	MAIN 280
432 CONTINUE	MAIN 281
IQ1 = NLM+1	MAIN 282
IF (INC.EQ.0.OR.NSERT.EQ.0). GO TO 790	MAIN 283
DO 302 I=1,NSERT	MAIN 284
INC = 0	MAIN 285
DO 301 J=1,NS	MAIN 286
IF(IUSE(J).EQ.0) GO TO 301	MAIN 287
INC = INC+1	MAIN 288
IF(SUB(J,1).NE.ENSERT(1,I)) GO TO 301	MAIN 289
IF(SUB(J,2).NE.ENSERT(2,I)) GO TO 301	MAIN 290
IF(SUB(J,3).NE.ENSERT(3,I)) GO TO 301	MAIN 291
IF(T(1).EQ.0.) GO TO 295	MAIN 292
IF(T(1).LT.TEMP(INC,1).OR.T(1).GT.TEMP(INC,2)) GO TO 301	MAIN 293
295 IQ1 = IQ1+1	MAIN 294
IUSE(J) = -IUSE(J)	MAIN 295
GO TO 302	MAIN 296
301 CCNTINUE	MAIN 297
302 CCNTINUE	MAIN 298
NSERT = 0	MAIN 299
790 CONTINUE	MAIN 300
IF(.NCT.TP.AND..NOT.FP.AND..NOT.SP) GO TO 791	MAIN 301
CALL THERMP	MAIN 302
GO TO 800	MAIN 303
791 CONTINUE	MAIN 304
IF(DETN) CALL DETON	MAIN 305
IF(RKT) CALL ROCKET	MAIN 306
IF(SHOCK) CALL SHCK	MAIN 307
800 RETURN	MAIN 308
END	MAIN 309

C	SUBROUTINE REACT	REAC 1
C		REAC 2
C	LOGICAL HP,SP,TP,CONVG,NEWR,IONS,MOLES,EQL,FROZ,VOL	REAC 3
C		REAC 4
C	DIMENSION ANAME(15,5),V(10)	REAC 5
C		REAC 6
C	COMMON /MISC/ENN,SUMN,TT,SO,ATOM(3,101),LLMT(10),BC(10),BOP(10,2),	REAC 7
1	TM,TLOW,TMID,THIGH,PP,CPSUM,OF,EQRAT,FPCT,R,RR,HSUBO,AM(2),	REAC 8
2	HPP(2),RH(2),VMIN(2),VPLS(2),WP(2),DATA(22),NAME(15,5),	REAC 9
3	ANUM(15,5),PECWT(15),ENTH(15),FAZ(15),RTEMP(15),FCX(15),DENS(15),	REAC 10
4	RPOP,RMW(15);TLN,CR,OXF(15),ENNL,TRACE,LLMTS(10),SBOP(10,2)	REAC 11
	CCOMMON /INDX/IDEBUG,CONVG,TP,HP,SP,ISV,NPP,MOLES,NP,NT,NPT,NLM,	REAC 12
1	NS,KMAT,IMAT;IQ1,IOF,NOF,NOMIT,IP,NEWR,NSUB,NSUP,RKT,DETN,SHOCK,	REAC 13
2	IONS,NC,NSERT,JSOL,JLIQ,KASE,NREAC,IC,JS1,VOL,IT,CALCH,NLS,LOGV,	REAC 14
3	ISUP,ISUB,ITNUM,ITM,INCDFZ,INCDEQ,CPRF,IPP,SEQ,PCPLT	REAC 15
C		REAC 16
C	EQUIVALENCE (NAME,ANAME),(NLM,L),(BLANK,LANK)	REAC 17



C		REAC 18
	DATA MOL/1HM/,OX/1HO/,LANK/1H /,IZERO/2H00/,ZERO/1H0/	REAC 19
C		REAC 20
	DO 10 K=1,2	REAC 21
	WP(K)=0.	REAC 22
	HPP(K)=0.	REAC 23
	RP(K)=0.	REAC 24
	VPLS(K)=0.	REAC 25
	VMIN(K)=0.	REAC 26
	AM(K)=0.	REAC 27
	DC 8 J=1,10	REAC 28
	LLMT(J)=0	REAC 29
	BOP(J,K)=0.	REAC 30
	8 CONTINUE	REAC 31
	10 CONTINUE	REAC 32
	NFUEL = 0	REAC 33
	N=1	REAC 34
	L=1	REAC 35
C		REAC 36
C	READ AND WRITE REACTANT CARDS	REAC 37
C		REAC 38
	20 READ(5,21)(NAME(N,I),ANUM(N,I),I=1,5),PECWT(N),MOLE,ENTH(N),	REAC 39
	1 FAZ(N),RTEMP(N),FOX(N),DENS(N)	REAC 40
	21 FORMAT(5(A2,F7.5),F7.5,A1,F9.5,A1,F8.5,A1,F8.5)	REAC 41
	IF(NAME(N,1).EQ.LANK) GO TO 200	REAC 42
	IF(L.EQ.0)GO TO 20	REAC 43
	WRITE (6,31)(NAME(N,I),ANUM(N,I),I=1,5),PECWT(N),MOLE,ENTH(N),	REAC 44
	1 FAZ(N),RTEMP(N),FOX(N),DENS(N)	REAC 45
	31 FORMAT(1X,5(A2,1X,F7.4,2X),F8.4,2X,A1,F11.2,2X,A1,2X,F8.3,2X,	REAC 46
	1 A1,3X,F8.5)	REAC 47
	35 IF(MOLE.EQ.MOL) MOLES=.TRUE.	REAC 48
C		REAC 49
C	IF OXIDANT, K=1	REAC 50
C	IF FUEL, K=2	REAC 51
C		REAC 52
	IF(FOX(N).EQ.ZERO) FOX(N)=OX	REAC 53
	K = 1	REAC 54
	IF(FOX(N).EQ.OX) GO TO 37	REAC 55
	K = 2	REAC 56
	NFUEL = NFUEL+1	REAC 57
	37 DO 38 J=1,15	REAC 58
	DATA(J) = 0.	REAC 59
	38 CONTINUE	REAC 60
	RM=0.	REAC 61
C		REAC 62
C	STORE ATOMIC SYMBOLS IN LLMT ARRAY.	REAC 63
C	CALCULATE MOLECULAR WEIGHT.	REAC 64
C	TEMPORARILY STORE ATOMIC VALENCE IN V.	REAC 65
C		REAC 66
	DO 100 JJ=1,5	REAC 67
	IF(ANUM(N,JJ).EQ.0.)GO TO 101	REAC 68
	IF(ANAME(N,JJ).EQ.ZERO) ANAME(N,JJ)=OX	REAC 69
	DO 41 J=1,10	REAC 70
	NJ = J	REAC 71
	IF(LLMT(J).EQ.0) GO TO 45	REAC 72
	IF(NAME(N,JJ).EQ.LLMT(J))GO TO 46	REAC 73
	41 CONTINUE	REAC 74
	45 L = NJ	REAC 75
	LLMT(J)=NAME(N,JJ)	REAC 76
	46 DC 48 KK=1,101	REAC 77
	IF(ATOM(1,KK).EQ.ANAME(N,JJ))GO TO 50	REAC 78
	48 CONTINUE	REAC 79
	L=0	REAC 80
	GO TO 20	REAC 81
	50 RM=RM+ANUM(N,JJ)*ATOM(2,KK)	REAC 82

	V(J)=ATOM(3,KK)	REAC 83
	DATA(J)=ANUM(N,JJ)	REAC 84
100	CONTINUE	REAC 85
C		REAC 86
C	ADD CONTRIBUTIONS TO WP(K), HPP(K), AM(K), BOP(I,K) AND RH(K).	REAC 87
C		REAC 88
101	PCWT=PECWT(N)	REAC 89
	IF(MOLES) PCWT=PCWT*RM	REAC 90
	WP(K)=WP(K) + PCWT	REAC 91
	EM = ENTH(N)	REAC 92
	IF(NAME(N,5).NE.IZERO)HPP(K)=HPP(K)+EM*PCWT/(RM*R)	REAC 93
	AM(K)=AM(K)+PCWT/RM	REAC 94
	DC 110 J=1,L	REAC 95
	BOP(J,K)=DATA(J)*PCWT/RM +BOP(J,K)	REAC 96
110	CONTINUE	REAC 97
	IF(DENS(N).NE.O.)GO TO 115	REAC 98
	GO TO 117	REAC 99
115	RH(K)=RH(K)+PCWT/DENS(N)	REAC 100
117	RMW(N) = RM	REAC 101
	N = N+1	REAC 102
	IF(N.NE.16) GO TO 20	REAC 103
200	NREAC =N-1	REAC 104
	IF(NFUEL.GT.O) GO TO 210	REAC 105
C		REAC 106
C	100 PERCENT OXIDANT, CALL REACTANTS FUEL	REAC 107
C		REAC 108
	DO 205 N=1,NREAC	REAC 109
	FOX(N) = BLANK	REAC 110
205	CONTINUE	REAC 111
	RH(2) = RH(1)	REAC 112
	RH(1) = 0.	REAC 113
	WP(2) = WP(1)	REAC 114
	WP(1) = 0.	REAC 115
	HPP(2) = HPP(1)	REAC 116
	AM(2) = AM(1)	REAC 117
	AM(1) = 0.	REAC 118
	DC 208 J=1,L	REAC 119
	BOP(J,2) = BOP(J,1)	REAC 120
208	CONTINUE	REAC 121
210	IF(L.EQ.C) GO TO 1000	REAC 122
C		REAC 123
C	NORMALIZE HPP(K),AM(K),BOP(I,K), AND PECWT(N).	REAC 124
C	CALCULATE RH(K), V+(K), AND V-(K)	REAC 125
C		REAC 126
	DC 220 K=1,2	REAC 127
	IF(WP(K).EQ.O.)GO TO 220	REAC 128
	HPP(K)=HPP(K)/WP(K)	REAC 129
	AM(K) = WP(K)/AM(K)	REAC 130
	IF(RH(K).NE.O.)RH(K)=WP(K)/RH(K)	REAC 131
	DC 215 J=1,L	REAC 132
	BOP(J,K)=BOP(J,K)/WP(K)	REAC 133
	IF(V(J).LT.O.)VMIN(K)= VMIN(K)+BOP(J,K)*V(J)	REAC 134
	IF(V(J).GT.O.)VPLS(K)=VPLS(K)+BOP(J,K)*V(J)	REAC 135
215	CONTINUE	REAC 136
	IF(MOLES) GO TO 220	REAC 137
	DC 218 N=1,NREAC	REAC 138
	IF(FCX(N).EQ.OX.AND.K.EQ.2) GO TO 218	REAC 139
	IF(FCX(N).NE.OX.AND.K.EQ.1) GO TO 218	REAC 140
	PECWT(N) = PECWT(N)/WP(K)	REAC 141
218	CONTINUE	REAC 142
220	CONTINUE	REAC 143
	NEWR=.TRUE.	REAC 144
C		REAC 145
C	ARE ELEMENTS SAME AS FOR LAST SET OF REACTANTS, IF SC, NEWR=.FALSE.	REAC 146

IF(NLM.NE.NLS) GO TO 226	REAC 147
IF(NOMIT.NE.0) GO TO 226	REAC 148
DC 224 I=1,NLS	REAC 149
DO 222 J=1,NLM	REAC 150
IF(LLMT(J).NE.LLMTS(I)) GO TO 222	REAC 151
SBOP(I,1) = BOP(J,1)	REAC 152
SBCP(I,2) = BOP(J,2)	REAC 153
GO TO 224	REAC 154
222 CCNTINUE	REAC 155
GO TO 226	REAC 156
224 CCNTINUE	REAC 157
NEWB = .FALSE.	REAC 158
DC 225 I=1,NLM	REAC 159
LLMT(I) = LLMTS(I)	REAC 160
BOP(I,1) = SBOP(I,1)	REAC 161
BOP(I,2) = SBOP(I,2)	REAC 162
225 CCNTINUE	REAC 163
GO TO 229	REAC 164
C	REAC 165
C	REAC 166
226 NLS = NLM	REAC 167
NOMIT = 0	REAC 168
REWIND 4	REAC 169
DC 228 I=1,NLM	REAC 170
LLMTS(I) = LLMT(I)	REAC 171
228 CCNTINUE	REAC 172
229 DO 230 N=1,NREAC	REAC 173
IF (DENS(N).NE.0.) GO TO 230	REAC 174
RH(2) = 0.	REAC 175
RH (1) = 0.	REAC 176
GO TO 1000	REAC 177
230 CCNTINUE	REAC 178
1000 RETURN	REAC 179
END.	REAC 180
	REAC 181

C	SUBROUTINE SEARCH	SRCH 1
C		SRCH 2
C	SEARCH TAPE FOR THERMO DATA AND TRANSPORT CROSS SECTIONS OF SPECIES	SRCH 3
C	TO BE CONSIDERED	SRCH 4
C		SRCH 5
C	THE FOLLOWING DOUBLE PRECISION TYPE STATEMENTS ARE REQUIRED FOR	SRCH 6
C	IBM 360 MACHINES ONLY	SRCH 7
C		SRCH 8
C	DOUBLE PRECISION COEF,S,EN,ENLN,HO,DELN	SRCH 9
C		SRCH 10
C	INTEGER SUB,OMIT,END,TOOBIG	SRCH 11
C	INTEGER SPECE	SRCH 12
C		SRCH 13
C	LOGICAL NEWB,OTTO,TRNSPT	SRCH 14
C		SRCH 15
C	DIMENSION DATE(2,3),MT(4),R(4),OMIT(3,3),NAM(3),TOOBIG(3,50)	SRCH 16
C	DIMENSION SPECE(2,3),TEMPR(20),TABLS(20,3)	SRCH 17
C		SRCH 18
C	COMMON SPECE , TEMPR , TABLS	SRCH 19
C	COMMON /SPECES/COEF(2,7,100),S(100),HO(100),DELN(100),DUMMY(100),	SRCH 20
C	EN(100,13),ENLN(100),A(10,100),SUB(100,3),IUSE(100),TEMP(50,2)	SRCH 21
C	COMMON /MISC/ENN,SUMN,TT,SO,ATOM(3,101),LLMT(10),RO(10),BOP(10,2),	SRCH 22



1	JM,TLOW,TMID,THIGH,PP,CPSUM,OF,EQRAT,FPCT,R,RR,HSUBO,AM(2),	SRCH	23
2	HPP(2),RH(2),VMIN(2),VPLS(2),WP(2),DATA(22),NAME(15,5),	SRCH	24
3	ANUM(15,5),PECWT(15),ENTH(15),FAZ(15),RTEMP(15),FOX(15),DENS(15),	SRCH	25
4	RHOP,RMW(15),TLN,CR,OXF(15),ENNL,TRACE,LLMTS(10),SBOP(10,2)	SRCH	26
	CCMMCN /INCX/IDEBUG,CONVG,TP,HP,SP,ISV,NPP,MOLES,NP,NT,NPT,NLM,	SRCH	27
1	NS,KMAT,IMAT,IQ1,IOF,NOF,NOMIT,IP,NEWR,NSUB,NSUP,RKT,DETN,SHOCK,	SRCH	28
2	IONS,NC,NSERT,JSOL,JLIQ,KASE,NREAC,IC,JS1,VOL,IT,CALCH,NLS,LOGV,	SRCH	29
3	ISUP,ISUB,ITNUM,ITM,INCFZ,INCDEQ,CPRF,IPP,SEQL,PCPLT	SRCH	30
		SRCH	31
C	EQUIVALENCE (DATE,EN),(OMIT,ENLN),(ENDD,END),(TOORIG,ENLN)	SRCH	32
C		SRCH	33
	DATA GAS/1HG/,END/3HEND/,ND/4HLAST/	SRCH	34
C		SRCH	35
C		SRCH	36
C	SEARCH FOR THERMO DATA	SRCH	37
C		SRCH	38
	I2B = 0	SRCH	39
	NC = C	SRCH	40
	IX = 0	SRCH	41
C		SRCH	42
C	CHECK DIMENSION FOR NUMBER OF SPECIES, CLEAR A(I,J)	SRCH	43
C		SRCH	44
	SUB(1,1) = END	SRCH	45
	DO 3 I=1,1000	SRCH	46
	IF(A(1,I).EQ.ENDD) GO TO 4	SRCH	47
	DO 3 J=1,NLM	SRCH	48
	A(J,I) = 0.	SRCH	49
	3 CONTINUE	SRCH	50
	4 MAXNS = I-1	SRCH	51
C		SRCH	52
C	READ TEMPERATURE RANGES FOR COEFFICIENTS OF GASEOUS SPECIES.	SRCH	53
C		SRCH	54
	READ(4,5) TLOW,TMID,THIGH	SRCH	55
	5 FCRMT (3F10.3)	SRCH	56
	NS = 1	SRCH	57
C		SRCH	58
C	BEGIN LCCP FOR READING SPECIES DATA FROM TAPE.	SRCH	59
C		SRCH	60
	7 READ (4,10) (NAM(I),I=1,3),DATE(1,NS)-DATE(2,NS),(MT(J),B(J),	SRCH	61
	1 J=1,4),FHAZ,T1,T2	SRCH	62
	10 FORMAT(3A4,6X,2A3,4(A2,F3.0),A1,2F10.3)	SRCH	63
	IF(NAM(1).EQ.END) GO TO 171	SRCH	64
	READ (4,20) ((COEF(I,J,NS),J=1,7),I=1,2)	SRCH	65
	20 FORMAT (5E15.8)	SRCH	66
	IF(NCMIT.EQ.0) GO TO 810	SRCH	67
	DO 805 I=1,NOMIT	SRCH	68
	DO 804 J=1,3	SRCH	69
	IF(OMIT(J,I).NE.NAM(J)) GO TO 805	SRCH	70
804	CONTINUE	SRCH	71
	GO TO 7	SRCH	72
805	CONTINUE	SRCH	73
810	DO 820 K=1,4	SRCH	74
	IF(B(K).EQ.0.) GO TO 825	SRCH	75
	DO 168 I=1,NLM	SRCH	76
	IF(LLMT(I).EQ.MT(K)) GO TO 820	SRCH	77
168	CONTINUE	SRCH	78
	IF(NS.GT.MAXNS) GO TO 7	SRCH	79
	DO 819 J=1,NLM	SRCH	80
819	A(J,NS) = 0.	SRCH	81
	GO TO 7	SRCH	82
820	IF(NS.LE.MAXNS) A(I,NS) = B(K)	SRCH	83
825	IF(NS.LE.MAXNS) GO TO 828	SRCH	84
	I2B = I2B+1	SRCH	85
	DO 826 I=1,3	SRCH	86

826	TOOBIG(I,I2B) = NAM(I)	SRCH	87
	GO TO 7	SRCH	88
828	DO 829 I=1,3	SRCH	89
829	SUB(NS,I) = NAM(I)	SRCH	90
	IUSE(NS) = 0	SRCH	91
	IF(PHAZ.EQ.GAS) GO TO 170	SRCH	92
C		SRCH	93
C	CONDENSED SPECIES	SRCH	94
C		SRCH	95
	NC= NC+1	SRCH	96
	TEMP(NC,1)= T1	SRCH	97
	TEMP(NC,2)= T2	SRCH	98
	IX= IX+1	SRCH	99
	IF(NS.EQ.1.OR.IUSE(NS-1).EQ.0) GO TO 145	SRCH	100
	DO 830 I=1,NLM	SRCH	101
	IF(A(I,NS).NE.A(I,NS-1)) GO TO 145	SRCH	102
830	CONTINUE	SRCH	103
	IX= IX-1	SRCH	104
145	IUSE(NS)= -IX	SRCH	105
170	NS= NS+1	SRCH	106
	GO TO 7	SRCH	107
C		SRCH	108
C	END CARD HAS BEEN READ.	SRCH	109
C		SRCH	110
171	NS= NS-1	SRCH	111
	NEWB= .FALSE.	SRCH	112
	WRITE(6,172)	SRCH	113
172	FORMAT(42HC SPECIES BEING CONSIDERED IN THIS SYSTEM)	SRCH	114
	DO 174 I=1,NS,5	SRCH	115
	I5= I+4	SRCH	116
	IF(NS.LT.I5) I5=NS	SRCH	117
174	WRITE (6,176)(DATE(1,J),DATE(2,J),SUB(J,1),SUB(J,2),SUB(J,3),	SRCH	118
	1 J=I,I5)	SRCH	119
176	FORMAT(5(5X,2A3,2X,3A4))	SRCH	120
	IF(I2B.GT.0) GO TO 870	SRCH	121
	GO TO 16	SRCH	122
870	WRITE(6,871) I2B	SRCH	123
871	FORMAT(35HC INSUFFICIENT STORAGE FOR FOLLOWING,I3,8H SPECIES)	SRCH	124
	WRITE(6,880)(TOOBIG(1,J),TOOBIG(2,J),TOOBIG(3,J),J=1,I2B)	SRCH	125
880	FORMAT(8(3X,3A4))	SRCH	126
	NS = 0	SRCH	127
C		SRCH	128
C	SEARCH FOR TRANSPORT CROSS SECTIONS	SRCH	129
C		SRCH	130
16	NK = 1	SRCH	131
13	READ(4) ((SPECE(I,L),L=1,3),I=1,2),NTP,NTB,ROTN	SRCH	132
	IF(SPECE(1,1).EQ.ND) GO TO 21	SRCH	133
	K=1	SRCH	134
	DO 25 J=1,NS	SRCH	135
	DO 24 I=1,3	SRCH	136
24	IF(SPECE(K,I).NE.SUB(J,I)) GO TO 25	SRCH	137
	GO TO 6	SRCH	138
25	CONTINUE	SRCH	139
	GO TO 13	SRCH	140
6	K=2	SRCH	141
	DO 8 JJ=1,NS	SRCH	142
	DO 27 II=1,3	SRCH	143
27	IF(SPECE(K,II).NE.SUB(JJ,II)) GO TO 8	SRCH	144
	GO TO 21	SRCH	145
8	CONTINUE	SRCH	146
	GO TO 13	SRCH	147
21	WRITE(3) ((SPECE(I,L),L=1,3),I=1,2),NTP,NTB,ROTN	SRCH	148
	IF(SPECE(1,1).EQ.ND) GO TO 17	SRCH	149
	READ(4) (TEMPR(I),(TABLS(I,L),L=1,3),I=1,NTP)	SRCH	150
	WRITE(3) (TEMPR(I),(TABLS(I,L),L=1,3),I=1,NTP)	SRCH	151

NK=NK+1
 GO TO 13
 17 CONTINUE
 REWIND 3
 RETURN
 END

SRCH 152
 SRCH 153
 SRCH 154
 SRCH 155
 SRCH 156
 SRCH 157

C	SUBROUTINE HCALC	HCAL	1
C		HCAL	2
C	CALCULATE PROPERTIES FOR TOTAL REACTANT USING THERMO DATA FOR	HCAL	3
C	ONE OR MORE REACTANTS.	HCAL	4
C		HCAL	5
C	THE FOLLOWING DOUBLE PRECISION TYPE STATEMENTS ARE REQUIRED FOR	HCAL	6
C	IBM 360 MACHINES ONLY	HCAL	7
C		HCAL	8
C	DOUBLE PRECISION HSUM,SSUM,CPR,DLVTP,DLVPT,GAMMAS	HCAL	9
C	DOUBLE PRECISION COEF,S,EN,ENLN,HO,DELN	HCAL	10
C		HCAL	11
C	LOGICAL MOLES,VOL,SHOCK,CALCH	HCAL	12
C	CALCULATE ENTHALPY FOR PROPELLANT USING COEFFICIENTS	HCAL	13
C	DIMENSION NUM(15,5)	HCAL	14
C		HCAL	15
C	COMMON /POINTS/HSUM(13),SSUM(13),CPR(13),DLVTP(13),DLVPT(13),	HCAL	16
C	1 GAMMAS(13),P(26),T(52),V(13),PPP(13),WM(13),SONVEL(13),TTT(13),	HCAL	17
C	2 VLM(13),TOTN(13)	HCAL	18
C	CCMMCN /SPECES/COEF(2,7,100),S(100),HO(100),DELN(100),DUMMY(100),	HCAL	19
C	1 EN(100,13),ENLN(100),A(10,100),SUB(100,3),IUSE(100),TEMP(50,2)	HCAL	20
C	CCMMCN /MISC/ENN,SUM,TT,SO,ATOM(3,101),LLMT(10),BO(10),ROP(10,2),	HCAL	21
C	1 TM,TLOW,TMID,THIGH,PP,CPSUM,OF,EQRAT,FPCT,R,RR,HSUBD,AM(2),	HCAL	22
C	2 HPP(2),RH(2),VMIN(2),VPLS(2),WP(2),DATA(22),NAME(15,5),	HCAL	23
C	3 ANUM(15,5),PECWT(15),ENTH(15),FAZ(15),RTEMP(15),FCX(15),DENS(15),	HCAL	24
C	4 RHOP,RMW(15),TLN,CR,OXF(15),ENNL,TRACE,LLMTS(10),SBOP(10,2)	HCAL	25
C	CCMMCN /INDX/IDEBU,CONVG,TP,HP,SP,ISV,NPP,MOLES,NP,NT,NPT,NLM,	HCAL	26
C	1 NS,KMAT,IMAT,IQ1,IOF,NOF,NOMIT,IP,NEW,NSUB,NSUP,RKT,DETN,SHOCK,	HCAL	27
C	2 IONS,NC,NSERT,JSOL,JLIQ,KASE,NREAC,IC,JS1,VOL,IT,CALCH,NLS,LOGV,	HCAL	28
C	3 ISUP,ISUB,ITNUM,ITM,INCDFZ,INCDEQ,CPRF,IPP,SEQL,PCPLT	HCAL	29
C		HCAL	30
C	EQUIVALENCE (ANUM,NUM),(L,NLM),(J,JS1)	HCAL	31
C	EQUIVALENCE (AM1,DATA(20)),(CPR1,DATA(21))	HCAL	32
C		HCAL	33
C	DATA AG/1HG/, IZERO/2H0J/, OX/1HO/, BLK/1H /	HCAL	34
C		HCAL	35
C	TSAVE = TT	HCAL	36
C		HCAL	37
C	CALCULATE MOLECULAR WEIGHT OF TOTAL REACTANT, AM1.	HCAL	38
C		HCAL	39
C	IF (AM(1).NE.0.0 .AND. AM(2).NE.0.0) GO TO4	HCAL	40
C	AM1= AM(2)	HCAL	41
C	IF (AM(2).EQ.0.0) AM1= AM(1)	HCAL	42
C	GC TO 9	HCAL	43
C	4 AM1=(OF*1.)*AM(1)*AM(2)/(AM(1)+OF*AM(2))	HCAL	44
C	9 TM = 0.	HCAL	45
C	IF (PP.GT.0.) TM = ALOG(PP*AM1)	HCAL	46
C	SSUM(NPT) = 0.	HCAL	47
C	HPP(1) = 0.	HCAL	48
C	HPP(2) = 0.	HCAL	49
C	HSUBD = 0.	HCAL	50

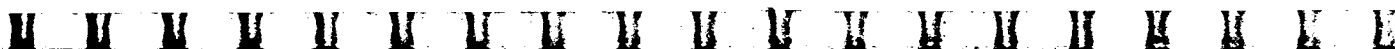
	CPR1 = 0.	HCAL 51
	ANN = (1.+CF)	HCAL 52
C		HCAL 53
C	LOCP ON REACTANTS.	HCAL 54
C	IF OXIDANT, K=1	HCAL 55
C	IF FUEL, K=2	HCAL 56
C		HCAL 57
	DO 900 N=1,NREAC	HCAL 58
	K=2	HCAL 59
	IF(FOX(N).EQ.OX)K=1	HCAL 60
	IF(NAME(N,5).NE.IZERO) GO TO 90	HCAL 61
	IF(.NOT.CALCH.AND.TT.NE.0.) GO TO 15	HCAL 62
	TT = RTEMP(N)	HCAL 63
C		HCAL 64
C	IS TT IN RANGE	HCAL 65
C		HCAL 66
	15 IF(SHOCK) GO TO 10	HCAL 67
	IF(TT.LT.(TLOW/1.2).OR.TT.GT.(THIGH*1.2)) GO TO 75	HCAL 68
	16 J = NUM(N,5)	HCAL 69
	IF (J.NE.0) GO TO 90	HCAL 70
	DO 10 J=1,L	HCAL 71
	DATA(J)=0.	HCAL 72
	10 CONTINUE	HCAL 73
C		HCAL 74
C	TEMPORARILY STORE STOICHIOMETRIC COEFFICIENTS IN DATA ARRAY.	HCAL 75
C		HCAL 76
	DO 40 I=1,4	HCAL 77
	IF(ANUM(N,I).EQ.0.)GO TO 50	HCAL 78
	DO 20 J=1,L	HCAL 79
	IF(LLMT(J).EQ.NAME(N,I)) GO TO 30	HCAL 80
	20 CONTINUE	HCAL 81
	30 DATA(J)=ANUM(N,I)	HCAL 82
	40 CONTINUE	HCAL 83
	50 IS=0	HCAL 84
C		HCAL 85
C	SEARCH FOR REACTANT IN THERMC SPECIES. STORE INDEX IN NUM(N,5).	HCAL 86
C		HCAL 87
	DO 70 J=1,NS	HCAL 88
	IF(IUSE(J).EQ.0)GO TO 55	HCAL 89
	IS = IS+1	HCAL 90
	IF(FAZ(N).EQ.AG)GO TO 70	HCAL 91
	IF(TT.GT.TEMP(IS,2).AND.TEMP(IS,2).NE.THIGH) GO TO 70	HCAL 92
	IF(TT.LT.TEMP(IS,1).AND.TEMP(IS,1).NE.TLOW) GO TO 70	HCAL 93
	GO TO 56	HCAL 94
	55 IF(FAZ(N).NE.AG.AND.FAZ(N).NE.BLK) GO TO 70	HCAL 95
	56 DO 60 I=1,L	HCAL 96
	IF(A(I,J).NE.DATA(I)) GO TO 70	HCAL 97
	60 CONTINUE	HCAL 98
	NUM(N,5) = J	HCAL 99
	GO TO 90	HCAL 100
	70 CONTINUE	HCAL 101
	GO TO 80	HCAL 102
C		HCAL 103
C	CALCULATE EN FOR REACTANT AND CALL CPHS TO CALCULATE PROPERTIES.	HCAL 104
C		HCAL 105
	90 IF (MOLES) ENJ = PECWT(N)/WP(K)	HCAL 106
	IF (.NOT.MOLES) ENJ = PECWT(N)/RMW(N)	HCAL 107
	BNJ = ENJ/ANN	HCAL 108
	IF(K.EQ.1) ENJ = ENJ*OF	HCAL 109
	IF(NAME(N,5).NE.IZERO)GO TO 500	HCAL 110
	NSS = NS	HCAL 111
	NS = J	HCAL 112
	TLN = ALOG(TT)	HCAL 113
	IF(.NOT.CALCH) EN(J,NPT) = ENJ	HCAL 114
	CALL CPHS	HCAL 115



NS = NSS	HCAL 116
IF (HO(J).GT.-.01 .AND. HO(J).LT..01) HO(J) = 0.	HCAL 117
RTEMP(N) = TT	HCAL 118
IF(VOL) HO(J)=HO(J)-1.	HCAL 119
ENTH(N) = HO(J)*R*TT	HCAL 120
C	HCAL 121
C	HCAL 122
C	HCAL 123
ADD CONTRIBUTION TO CP, H, AND S OF TOTAL REACTANT.	HCAL 124
CPR1 = CPR1 + CPSUM	HCAL 125
SSUM(NPT) = SSUM(NPT) + ENJ * (S(J)-ALOG(ENJ)-TM)	HCAL 126
500 ER = ENTH(N)*ENJ/R	HCAL 127
HSUBO = HSUBO+ER	HCAL 128
HPP(K) = HPP(K)+ER	HCAL 129
900 CONTINUE	HCAL 130
IF(TSAVE.NE.0.) TT=TSAVE	HCAL 131
GO TO 1000	HCAL 132
75 WRITE(6,76)	HCAL 133
76 FORMAT(50HOREACTANT TEMPERATURE OUT OF RANGE OF THERMO DATA)	HCAL 134
TT = 0.	HCAL 135
GO TO 1000	HCAL 136
80 WRITE(6,85) N	HCAL 137
85 FORMAT(9HOREACTANT,I2,22H IS NOT IN THERMO DATA)	HCAL 138
TT = 0.	HCAL 139
1000 RETURN	HCAL 140
END	

C	SUBRCUTINE SAVE	SAVE 1
C		SAVE 2
C	SAVES OR USES COMPOSITIONS FROM PREVIOUS POINT AS INITIAL ESTIMATES	SAVE 3
C		SAVE 4
C		SAVE 5
C	THE FOLLOWING DOUBLE PRECISION TYPE STATEMENTS ARE REQUIRED FOR	SAVE 6
C	IBM 360 MACHINES ONLY	SAVE 7
C		SAVE 8
C	DOUBLE PRECISION COEF,S,EN,ENLN,HO,DELN	SAVE 9
C		SAVE 10
C	LOGICAL VOL,CALCH,IONS,SHOCK	SAVE 11
C		SAVE 12
C	COMMON /SPECES/COEF(2,7,100),S(100),HO(100),DELN(100),DUMMY(100),	SAVE 13
C	1 EN(100,13),ENLN(100),A(10,100),SUB(100,3),IUSE(100),TEMP(50,2)	SAVE 14
C	COMMON /MISC/ENN,SUMN,TT,SO,ATOM(3,101),LLMT(10),BC(10),BOP(10,2),	SAVE 15
C	1 TM,TLOW,TMID,THIGH,PP,CPSUM,OF,EQRAT,FPCT,R,RR,HSUBO,AM(2),	SAVE 16
C	2 HPP(2),RH(2),VMIN(2),VPLS(2),WP(2),DATA(22),NAME(15,5),	SAVE 17
C	3 ANUM(15,5),PECWT(15),ENTH(15),FAZ(15),RTEMP(15),FOX(15),DENS(15),	SAVE 18
C	4 RHOP,RMW(15),TLN,CR,OXF(15),ENNL,TRACE,LLMTS(10),SBOP(10,2)	SAVE 19
C	COMMON /INDX/IDEBUG,CONVG,TP,HP,SP,ISV,NPP,MOLES,NP,NT,NPT,NLM,	SAVE 20
C	1 NS,KMAT,IMAT,IQ1,IOF,NOF,NOMIT,IP,NEWR,NSUB,NSUP,RKT,DETN,SHOCK,	SAVE 21
C	2 IONS,NC,NSERT,JSOL,JLIQ,KASE,NREAC,IC,JS1,VOL,IT,CALCH,NLS,LOGV,	SAVE 22
C	3 ISUP,ISUB,ITNUM,ITM,INCDFZ,INCDEQ,CPRF,IPP,SEQ,PCPLT	SAVE 23
C	COMMON /SAVED/SLN(100),IQSAVE,ENSAVE,ENLSAV,LSAVE,JSOLS,JLIQS,	SAVE 24
C	1 LLL,LM,MAXNP,STORE(52,16),XS(20),WMOL(20),IND(20),NM,	SAVE 25
C	2 FIRSPT,FIRSTV	SAVE 26
C		SAVE 27
C	DATA IE/1HE/	SAVE 28
C		SAVE 29
C	IF(ISV)100,10,200	SAVE 30

C		SAVE	31
C	NEXT POINT FIRST T IN SCHEDULE, USE PREVIOUS COMPOSITICNS FOR THIS T	SAVE	32
C		SAVE	33
	10 IQ1 = IQSAVE	SAVE	34
	JSOL = JSOLS	SAVE	35
	JLIQ = JLIQS	SAVE	36
	ENN = ENSAVE	SAVE	37
	ENNL = ENLSAV	SAVE	38
	LL1 = NLM	SAVE	39
	DO 50 J = 1,NS	SAVE	40
	IF(.NOT.IONS) GO TO 15	SAVE	41
	IF(LLMT(NLM).EQ.LSAVE) GO TO 15	SAVE	42
	IF(LLMT(NLM).EQ.IE) GO TO 13	SAVE	43
	IF(IUSE(J).NE.-10000) GO TO 15	SAVE	44
	IUSE(J) = 0	SAVE	45
	LL1 = NLM+1	SAVE	46
	GO TO 20	SAVE	47
	12 IF(SLN(J).NE.0..CR.IUSE(J).NE.0) GO TO 15	SAVE	48
	LL1 = NLM-1	SAVE	49
	IUSE(J) = -10000	SAVE	50
	GO TO 50	SAVE	51
	15 IF (IUSE(J).EQ.0) GO TO 20	SAVE	52
	EN (J,NPT) = SLN(J)	SAVE	53
	IF(IUSE(J).GT.0) IUSE(J) = -IUSE(J)	SAVE	54
	IF (EN(J,NPT).NE.0.)IUSE(J) = -IUSE(J)	SAVE	55
	GO TO 50	SAVE	56
	20 EN(J,NPT) = 0.	SAVE	57
	ENLN(J) = SLN(J)	SAVE	58
	IF ((ENLN(J)-ENNL + 18.5).LE.0.) GO TO 50	SAVE	59
	EN(J,NPT) = 2.718281828459**ENLN(J)	SAVE	60
	50 CONTINUE	SAVE	61
	NLM = LL1	SAVE	62
	GO TO 1000	SAVE	63
C		SAVE	64
C	FIRST T--SAVE COMPOSITICNS FOR FUTURE POINTS WITH THIS T	SAVE	65
C		SAVE	66
	100 ISV = -ISV	SAVE	67
	JSOLS = JSOL	SAVE	68
	JLIQS = JLIQ	SAVE	69
	IQSAVE = IQ1	SAVE	70
	ENSAVE = ENN	SAVE	71
	ENLSAV = ENNL	SAVE	72
	LSAVE = LLMT(NLM)	SAVE	73
	DO 150 J = 1,NS	SAVE	74
	SLN(J) = ENLN(J)	SAVE	75
	IF(IUSE(J).NE.0) SLN(J)=EN(J,ISV)	SAVE	76
	150 CONTINUE	SAVE	77
C		SAVE	78
C	USE COMPOSITICNS FROM PREVIOUS POINT	SAVE	79
C		SAVE	80
	200 DO 300 J = 1,NS	SAVE	81
	EN(J,NPT) = EN(J,ISV)	SAVE	82
	300 CONTINUE	SAVE	83
	1000 RETURN	SAVE	84
C		SAVE	85
C	CALCULATE NEW VALUES OF BO AND HSUBO FOR NEW OF RATIC	SAVE	86
C		SAVE	87
	ENTRY NEWOF	SAVE	88
C		SAVE	89
C		SAVE	90
	WRITE(6,730) OF	SAVE	91
	730 FORMAT(6HOF = ,F10.6)	SAVE	92
	EQRAT = 0.	SAVE	93
	SUM = OF + 1.	SAVE	94
	V1 = (OF*VPLS(1)+VPLS(2))/SUM	SAVE	95



V2 = (OF*VPMIN(1)+VMIN(2))/SUM	SAVE 96
IF(V2.NE.0.) EQRAT=ARS(V1/V2)	SAVE 97
IF (RH(1) .NE. 0. .AND. RH(2) .NE. 0.) GO TO 744	SAVE 98
RHCP = RF(2)	SAVE 99
IF (RHCP .EQ. 0.) RHCP = RH(1)	SAVE 100
GO TO 745	SAVE 101
744 RHCP = (OF+1.)*RH(1)*RH(2)/(RH(1)+OF*RH(2))	SAVE 102
745 DO 747 I=1,NLM	SAVE 103
BC(I) = (OF*BOP(I,1)+BOP(I,2))/SUM	SAVE 104
747 CONTINUE	SAVE 105
NPT = 1	SAVE 106
IF(.NOT.CALCH) GO TO 750	SAVE 107
CALL HCALC	SAVE 108
IF(TT.EQ.0.) RETURN	SAVE 109
CALCH = .FALSE.	SAVE 110
IF(OF.NE.0.) HPP(1)=SUM*HPP(1)/OF	SAVE 111
HPP(2) = SUM*HPP(2)	SAVE 112
GO TO 760	SAVE 113
750 HSUBC= (OF*HPP(1) + HPP(2))/SUM	SAVE 114
760 IC = 0	SAVE 115
JSOL = 0	SAVE 116
JLIQ = 0	SAVE 117
WRITE (6,770)	SAVE 118
770 FORMAT(1H ,25X,14HEFFECTIVE FUEL,10X,17HEFFECTIVE CXIDANT,12X,7HMI	SAVE 119
XTURE)	SAVE 120
IF(VOL) WRITE(6,772)	SAVE 121
IF(.NOT.VOL) WRITE(6,774)	SAVE 122
772 FORMAT(16H INTERNAL ENERGY,14X,6HHPP(2),19X,6HHPP(1),19X,5HHSUBO)	SAVE 123
774 FORMAT(9H ENTHALPY,21X,6HHPP(2),19X,6HHPP(1),19X,5HHSUBO)	SAVE 124
WRITE(6,776) HPP(2),HPP(1),HSUBO	SAVE 125
776 FORMAT(19H (KG-MOL)(DEG K)/KG,E21.8,2E25.8)	SAVE 126
WRITE(6,778)	SAVE 127
778 FORMAT(12HCKG-ATOMS/KG,17X,8HBOP(I,2),17X,8HBOP(I,1),18X,5HBO(I))	SAVE 128
780 FORMAT(8X,A2,5X,3E25.8)	SAVE 129
WRITE(6,780) (LLMT(I),BOP(I,2),BOP(I,1),BO(I),I=1,NLM)	SAVE 130
RETURN	SAVE 131
END	SAVE 132

C	SUBROUTINE EQLBRM	EQLM 1
C	ROUTINE TO CALCULATE EQUILIBRIUM COMPOSITION AND PROPERTIES	EQLM 2
C		EQLM 3
C	DOUBLE PRECISION X,G,SUM	EQLM 4
C		EQLM 5
C	THE FOLLOWING DOUBLE PRECISION TYPE STATEMENTS ARE REQUIRED FOR	EQLM 6
C	IBM 360 MACHINES ONLY	EQLM 7
C		EQLM 8
C	DOUBLE PRECISION HSUM,SSUM,CPR,DLVTP,DLVPT,GAMMAS	EQLM 9
C	DOUBLE PRECISION COEF,S,EN,ENLN,HO,DELN	EQLM 10
C	DOUBLE PRECISION ENL,PROW,DLNT,AA	EQLM 11
C		EQLM 12
C	LOGICAL HP,SP,TP,CONVG,IONS,SINGC,LOGV,ISING,IC,VOL,SHOCK,RITE	EQLM 13
C		EQLM 14
C	COMMON /POINTS/HSUM(13),SSUM(13),CPR(13),DLVTP(13),DLVPT(13)	EQLM 15
	1 GAMMAS(13),P(26),T(52),V(13),PPP(13),WM(13),SONVEL(13),TTT(13),	EQLM 16
	2 VLM(13),TCTN(13)	EQLM 17
	COMMON /SPECES/COEF(2,7,100),S(100),HO(100),DELN(100),DUMMY(100),	EQLM 18
	1 EN(100,13),ENLN(100),A(10,100),SUB(100,3),IUSE(100),TEMP(50,2)	EQLM 19
	COMMON /MISC/ENN,SUMN,TT,SO,ATOM(3,101),LLMT(10),BO(10),BOP(10,2),EQLM	20

	1 TM,TLOW,TMID,THIGH,PP,CPSUM,OF,EQRAT,FPCT,R,RR,HSUBO,AM(2),	EQLM	21
	2 PPP(2),RH(2),VMIN(2),VPLS(2),WPI(2),DATA(22),NAME(15,5),	EQLM	22
	3 ANUM(15,5),PECWT(15),ENTH(15),FAZ(15),RTEMP(15),FOX(15),DENS(15),	EQLM	23
	4 RHOP,RMW(15),TLN,CR,OXF(15),ENNL,TRACE,LLMTS(10),SBOP(10,2)	EQLM	24
	COMMON /DOUBLE/ G(20,21), X(20)	EQLM	25
	COMMON /INDX/ IDEBUG,CONVG,TP,HP,SP,ISV,NPP,MOLES,NP,NT,NPT,NLM,	EQLM	26
	1 NS,KMAT,IMAT,IQ1,IOF,NOF,NOMIT,IP,NEW,NSUB,NSUP,RKT,DETN,SHOCK,	EQLM	27
	2 IONS,NC,NSERT,JSOL,JLIQ,KASE,NREAC,IC,JS1,VOL,IT,CALCH,NLS,LOGV,	EQLM	28
	3 ISUP,ISUB,ITNUM,ITM,INCDFZ,INCDEQ,CPRF,IPP,SEQ,PCPLT	EQLM	29
C	EQUIVALENCE (NLM,L)	EQLM	30
C		EQLM	31
C	DATA IE/IHE/,SMALNO/1.E-6/,SMNOL/-13.815511/,ITN/35/	EQLM	32
		EQLM	33
		EQLM	34
	E = 2.718281828459	EQLM	35
	SINGC = .FALSE.	EQLM	36
	ENL = ENNL	EQLM	37
	RITE = .FALSE.	EQLM	38
	IF(IDEBUG.GT.0.AND.NPT.GE.IDEBUG) RITE=.TRUE.	EQLM	39
	SIZE = 18.420681	EQLM	40
	ISING = .FALSE.	EQLM	41
	LOGV = .FALSE.	EQLM	42
	IF(.NOT.VOL) GO TO 6	EQLM	43
	RV = RR/101.325	EQLM	44
	PP = RV*ENN*TT/VLM(NPT)	EQLM	45
6	JLN = ALOG(TT)	EQLM	46
	CONVG = .FALSE.	EQLM	47
	ITNUMB = ITN	EQLM	48
	JS1 = 1	EQLM	49
	CALL CPHS	EQLM	50
	ITM = ALOG(PP/ENN)	EQLM	51
C		EQLM	52
	IF (.NOT.ICNS.OR.IE.EQ.LLMT(L)) GO TO 33	EQLM	53
	L = L+1	EQLM	54
	IQ1 = IQ1+1	EQLM	55
	DO 499 J = 1,NS	EQLM	56
	IF (A(L,J) .EQ.0.) GO TO 499	EQLM	57
	EN(J,NPT) = 1.E-8	EQLM	58
	ENLN(J) = -SIZE	EQLM	59
	IUSE(J) = C	EQLM	60
499	CONTINUE	EQLM	61
33	IF(NPT.EQ.1.AND..NOT.SHOCK) WRITE(6,244)(LLMT(I),I=1,L)	EQLM	62
244	FORMAT (4HOPT ,14(5X,A4))	EQLM	63
C		EQLM	64
C	BEGIN ITERATION	EQLM	65
C		EQLM	66
43	IF (.NOT.CONVG) GO TO 62	EQLM	67
	SUMN = ENN	EQLM	68
	IF(JSCL.EQ.0) GO TO 62	EQLM	69
	ENSC = EN(JSOL,NPT)	EQLM	70
	EN(JSOL,NPT) = EN(JSOL,NPT)+EN(JLIQ,NPT)	EQLM	71
	IUSE(JLIQ) = -IUSE(JLIQ)	EQLM	72
	IQ1 = IQ1-1	EQLM	73
	DLVTP(NPT) = 0.	EQLM	74
	CPR(NPT) = 0.	EQLM	75
	GAMMAS(NPT) = 0.	EQLM	76
	LOGV = .TRUE.	EQLM	77
62	CALL MATRIX	EQLM	78
	NUMB = ITN-ITNUMB+1	EQLM	79
	IQ2 = IQ1 + 1	EQLM	80
	IF(CONVG) IMAT=IMAT-1	EQLM	81
	IF(.NOT.RITE) GO TO 72	EQLM	82
	IF(.NOT.CONVG) GO TO 88	EQLM	83
	IF(.NOT.LOGV) WRITE(6,81).	EQLM	84



81	FCRMT(15HCT DERIV MATRIX)	EQLM 85
	IF(LOGV) WRITE(6,82)	EQLM 86
82	FCRMT(15HCP DERIV MATRIX)	EQLM 87
	GC TO 89	EQLM 88
88	WRITE(6,772) NUMB	EQLM 89
772	FCRMT(11H0ITERATION ,I3,6X,7HMATRIX //)	EQLM 90
89	DC 911 I=1,IMAT	EQLM 91
911	WRITE (6,73) (G(I,K),K=1,KMAT)	EQLM 92
72	ITST = IMAT	EQLM 93
	CALL GAUSS	EQLM 94
	IF(ITST.NE.IMAT) GO TO 774	EQLM 95
	IF(.NCT.RITE) GO TO 773	EQLM 96
	WRITE (6,373)(LLMT(I),I=1,L)	EQLM 97
373	FORMAT (7H0PI ,9(A4,10X))	EQLM 98
	WRITE (6,73)(X(I),I=1,IMAT)	EQLM 99
73	FCRMT (9E14.6)	EQLM 100
773	IF(.NOT.CONVG) GO TO 85	EQLM 101
	IF(.NOT.LOGV) GO TO 174	EQLM 102
	GO TO 171	EQLM 103
C		EQLM 104
C	TEMPERATURE DERIVATIVES--CONVG=T, LOGV=F	EQLM 105
C		EQLM 106
174	DLVTP(NPT) = 1.-X(IQ1)	EQLM 107
	CPR(NPT) = G(IQ2,IQ2)	EQLM 108
	DC 176 J=1,IQ1	EQLM 109
	CPR(NPT) = CPR(NPT)-G(IQ2,J)*X(J)	EQLM 110
176	CONTINUE	EQLM 111
C		EQLM 112
C	PRESSURE DERIVATIVE--CONVG=T, LOGV=T	EQLM 113
C		EQLM 114
	LOGV = .TRUE.	EQLM 115
	GO TO 62	EQLM 116
C		EQLM 117
C	SINGULAR MATRIX	EQLM 118
C		EQLM 119
774	IF(.NOT.CONVG) GO TO 775	EQLM 120
	WRITE(6,172)	EQLM 121
172	FCRMT(2EH0DERIVATIVE MATRIX SINGULAR)	EQLM 122
	GC TO 1171	EQLM 123
775	IF(.NOT.(P.OR.NPT.NE.1.OR.NC.EQ.0.OR.TT.GT.100.)) GO TO 871	EQLM 124
	WRITE(6,E74)	EQLM 125
874	FORMAT(96H0LOW TEMPERATURE IMPLIES CONDENSED SPECIES SHOULD HAVE	EQLM 126
	1BEEN INCLUDED ON AN INSERT CARD, RESTART)	EQLM 127
	GO TO 873	EQLM 128
871	WRITE(6,74)	EQLM 129
74	FCRMT(1EH0SINGULAR MATRIX)	EQLM 130
	IF(SINGC) GO TO 873	EQLM 131
	DC 970 JJ = 1,NS	EQLM 132
	IF(IUSE(JJ).NE.0) GO TO 970	EQLM 133
	IF(EN(JJ,NPT).NE.0.) GO TO 970	EQLM 134
	EN(JJ,NPT) = SMALNO	EQLM 135
	ENLN(JJ) = SMNOL	EQLM 136
970	CONTINUE	EQLM 137
	IF(ISING) GO TO 870	EQLM 138
	ISING = .TRUE.	EQLM 139
	WRITE (6,776)	EQLM 140
776	FORMAT (8H0RESTART)	EQLM 141
	GC TO 62	EQLM 142
C		EQLM 143
C	TEST FOR SINGULARITY TO CONDENSED SPECIES.	EQLM 144
C		EQLM 145
870	NCCND = IQ1-NLM-1	EQLM 146
	IF(NCCND.LT.2.OR.SIZEG.EQ.0.) GO TO 873	EQLM 148
	DC 872 J=1,NS	EQLM 149
	IF(IUSE(J).LE.0) GO TO 872	EQLM 150

	IF(J.EQ.JDELG) GO TO 872	EQLM 151
	DO 671 I=1,NLM	EQLM 152
	IF(A(I,J).EQ.A(I,JDELG)) GO TO 671	EQLM 153
	IF(A(I,J).EQ.0..CR.A(I,JDELG).EQ.0.) GO TO 872	EQLM 154
671	CONTINUE	EQLM 155
	SINCC = .TRUE.	EQLM 156
	IQ1 = IQ1-1	EQLM 157
	EN(J,NPT) = 0.	EQLM 158
	IUSE(J) = -IUSE(J)	EQLM 159
872	CONTINUE	EQLM 160
	IF(SINCC) GO TO 40	EQLM 161
	GO TO 872	EQLM 162
C		EQLM 163
C	OBTAIN CORRECTIONS TO THE ESTIMATES	EQLM 164
C		EQLM 165
85	ITNUMB= ITNUMB-1	EQLM 166
	KK = L + 1	EQLM 167
	IF(VOL) X(IQ2)=X(IQ1)	EQLM 168
	IF(TP) X(IQ2)=0.	EQLM 169
	DLNT= X(IQ2)	EQLM 170
	SUM = X(IQ1)	EQLM 171
	IF(.NOT.VOL) GO TO 97	EQLM 172
	X(IQ1) = 0.	EQLM 173
	SUM = -DLNT	EQLM 174
97	DO 101 J=1,NS	EQLM 175
	IF (IUSE(J)) 101,98,100	EQLM 176
98	DELN(J) = HO(J)*DLNT-HO(J)+S(J)-ENLN(J)-TM+SUM	EQLM 177
	DO 99 K=1,L	EQLM 178
	DELN(J)= DELN(J)+A(K,J)*X(K).	EQLM 179
99	CONTINUE	EQLM 180
	GO TO 101	EQLM 181
100	DELN(J) = X(KK)	EQLM 182
	KK = KK + 1	EQLM 183
101	CONTINUE	EQLM 184
C		EQLM 185
C	CALCULATE CONTROL FACTOR,AMBDA	EQLM 186
C		EQLM 187
	AMBDA= 1.	EQLM 188
	AMBDA1= 1.	EQLM 189
	SUM = X(IQ1)	EQLM 190
	IF(SUM.LT.0.) SUM=-SUM	EQLM 191
	IF(DLNT.GT.SUM) SUM=DLNT	EQLM 192
	IF(-DLNT.GT.SUM) SUM=-DLNT	EQLM 193
	DO 917 J=1,NS	EQLM 194
	IF (IUSE(J).NE.0) GO TO 917	EQLM 195
	IF((EN(J,NPT).GT.0.).AND.DELN(J).GT.SUM) SUM = DELN(J)	EQLM 196
	IF((EN(J,NPT).NE.0.) .OR. DELN(J).LE.0.) GO TO 917	EQLM 197
	SUM1 = (-9.212-ENLN(J)+ ENL)/(DELN(J)-X(IQ1))	EQLM 198
	IF(SUM1.LT.0.) SUM1=-SUM1	EQLM 199
	IF (SUM1.LT.AMBDA1) AMBDA1 = SUM1	EQLM 200
917	CONTINUE	EQLM 201
	IF(SUM.GT.2.)AMBDA=2./SUM	EQLM 202
	IF (AMBDA1.LT.AMBDA) AMBDA = AMBDA1	EQLM 203
	IF(.NOT.RITE) GO TO 111	EQLM 204
C		EQLM 205
C	INTERMEDIATE OUTPUT	EQLM 206
C		EQLM 207
	WRITE(6,923) TT,ENN, ENL,PP, TM,AMBDA	EQLM 208
923	FORMAT (3H0T=,E15.8,6H ENN=,E15.8,7H ENNL=E15.8,5H PP=,E15.8,	EQLM 209
	1 9H LN P/N=E15.8,8H AMBDA=E15.8)	EQLM 210
	IF(VOL) WRITE(6,1924) VLM(NPT)	EQLM 211
1924	FORMAT(8+ VOLUME=,E15.8,4HCC/G)	EQLM 212
	WRITE (6,924)	EQLM 213
924	FORMAT(1H0,18X,2HNJ,12X,5HLN NJ,8X,9HDEL LN NJ,9X,6HHOJ/RT,9X,5HSO	EQLM 214
	1J/R,10X,7H-GOJ/RT,8X,6H-GJ/RT)	EQLM 215

DC 926 J=1,NS	EQLM 216
GNEG1 = S(J)-HO(J)	EQLM 217
GNEG2 = GNEG1	EQLM 218
IF (IUSE(J).EQ.0) GNEG2=GNEG2-ENLN(J)-TM	EQLM 219
WRITE (6,925) SUB(J,1),SUB(J,2),	EQLM 220
1SUB(J,3),EN(J,NPT),ENLN(J),DELN(J),HO(J),S(J),GNEG1,GNEG2	EQLM 221
925 FORMAT (1X,3A4,7E15.6)	EQLM 222
926 CONTINUE	EQLM 223
WRITE (6,110)	EQLM 224
110 FORMAT(1H0)	EQLM 225
C	EQLM 226
C APPLY CORRECTIONS TO ESTIMATES	EQLM 227
C	EQLM 228
111 SUM = 0.	EQLM 229
DO 113 J=1,NS	EQLM 230
IF (IUSE(J)) 113,112,114	EQLM 231
112 ENLN(J)=ENLN(J)+AMBDA*DELN(J)	EQLM 232
EN(J,NPT) = 0.	EQLM 233
IF((ENLN(J)- ENL+SIZE).LE.0.) GO TO 113	EQLM 234
EN(J,NPT) = E**ENLN(J)	EQLM 235
SUM = SUM*EN(J,NPT)	EQLM 236
GO TO 113	EQLM 237
114 EN(J,NPT) = EN(J,NPT) + AMBDA * DELN(J)	EQLM 238
113 CONTINUE	EQLM 239
SUMN = SUM	EQLM 240
IF (TP) GO TO 115	EQLM 241
TLN= TLN+AMBDA*DLNT	EQLM 242
TT = EXP(TLN)	EQLM 243
JS1 = 1	EQLM 244
CALL CPHS	EQLM 245
115 IF(VOL) GO TO 2115	EQLM 246
ENL = ENL+AMBDA*X(IQ1)	EQLM 247
ENN = E**ENL	EQLM 248
GO TO 1115	EQLM 249
2115 ENN = SUMN	EQLM 250
ENL = ALOG(ENN)	EQLM 251
PP = RV*TT*ENN/VLM(NPT)	EQLM 252
1115 TM = ALOG(PP/ENN)	EQLM 253
IF (LLMT(L).NE.IE) GC TO 116	EQLM 254
C	EQLM 255
C CHECK ON REMOVING IONS	EQLM 256
C	EQLM 257
DO 1116 J = 1,NS	EQLM 258
IF (A(L,J).EQ.0.) GO TO 1116	EQLM 259
IF (EN(J,NPT).GT.0.) GO TO 116	EQLM 260
1116 CONTINUE	EQLM 261
DO 1118 J=1,NS	EQLM 262
IF(A(L,J).NE.0.) IUSE(J) = -10000	EQLM 263
1118 CONTINUE	EQLM 264
L = L-1	EQLM 265
IQ1 = IQ1-1	EQLM 266
GC TO 43	EQLM 267
C	EQLM 268
C TEST FOR CONVERGENCE	EQLM 269
C	EQLM 270
116 IF (ITNUMB.EQ.0) GO TO 14	EQLM 271
IF (AMBDA.LT.1.) GO TO 43	EQLM 272
SUM = (ENN-SUMN)/ENN	EQLM 273
IF (SUM.LT.0.) SUM = -SUM	EQLM 274
IF (SUM.GT.0.5E-5) GO TO 43	EQLM 275
DC 130 J=1,NS	EQLM 276
IF (IUSE(J).LT.0) GO TO 130	EQLM 277
AA= DELN(J)/SUMN	EQLM 278
IF(AA.LT.0.) AA=-AA	EQLM 279

	IF (IUSE(J).EQ.0) AA = AA*EN(J,NPT)	EQLM 280
	IF(AA.GT.0.5E-5) GO TO 43	EQLM 281
130	CONTINUE	EQLM 282
C		EQLM 283
C	CALCULATE ENTROPY, CHECK ON DELTA S FOR SP PROBLEMS	EQLM 284
C		EQLM 285
	TCTN(NPT) = 0.	EQLM 286
	SSUM(NPT) = 0.	EQLM 287
	DO 183 J=1,NS	EQLM 288
	IF(IUSE(J).LT.0) GO TO 183	EQLM 289
	TCTN(NPT) = TCTN(NPT) + EN(J,NPT)	EQLM 290
	SS = S(J)	EQLM 291
	IF(IUSE(J).EQ.0) SS=SS-ENLN(J)-TM	EQLM 292
	SSUM(NPT) = SSUM(NPT)+SS*EN(J,NPT)	EQLM 293
183	CONTINUE	EQLM 294
	IF(.NOT.SP.OR.NPT.EQ.1) GO TO 13	EQLM 295
	SS = SSUM(NPT) -S0	EQLM 296
	IF(SS.LT.(-0.00005).OR.SS.GT.0.00005) GO TO 43	EQLM 297
	IF(RITE) WRITE(6,1183) SS	EQLM 298
1183	FORMAT(12HDELTA S/R =,E15.8)	EQLM 299
C		EQLM 300
	13 CCNVC= .TRUE.	EQLM 301
	GC TO 160	EQLM 302
	14 WRITE(6,973) ITN,NPT	EQLM 303
973	FORMAT(1FL,I2,69H ITERATIONS DID NOT SATISFY CONVERGENCE REQUIREME	EQLM 304
	INTS FOR THE POINT I5)	EQLM 305
	IF (.NOT.HP.OR.NPT.NE.1.OR.NC.EQ.0.OR.TT.GT.100.) GO TO 873	EQLM 306
	WRITE(6,E74)	EQLM 307
	GC TO 873	EQLM 308
C		EQLM 309
C	CONVERGENCE TESTS ARE SATISFIED, TEST CONDENSED SPECIES.	EQLM 310
C		EQLM 311
160	IF(NC.EQ.0) GO TO 143	EQLM 312
	DO 146 J=1,NS	EQLM 313
	IF(EN(J,NPT).GE.0.) GO TO 146	EQLM 314
	IF (J.NE.JSOL .AND. J .NE.JLIQ) GO TO 147	EQLM 315
	JSQL = 0	EQLM 316
	JLIQ = 0	EQLM 317
147	IQ1 = IQ1 - 1	EQLM 318
	EN(J,NPT) = 0.	EQLM 319
	GO TO 166	EQLM 320
146	CCONTINUE	EQLM 321
	SIZEG = 0.	EQLM 322
	INC = 0	EQLM 323
	DO 170 J = 1,NS	EQLM 324
	IF (IUSE(J).EQ.0 .OR. IUSE(J).EQ.-10000) GO TO 170	EQLM 325
	INC = INC + 1	EQLM 326
	IF(RITE) WRITE(6,144)(SUB(J,I),I=1,3),TEMP(INC,1),TEMP(INC,2),IUSE	EQLM 327
	1E(J),EN(J,NPT)	EQLM 328
144	FORMAT (1H0,3A4,2F10.3,3X,5HIUSE=,I4,E15.7)	EQLM 329
	IF(EN(J,NPT).GT.0.) GO TO 169	EQLM 330
	KG = 1	EQLM 331
	IF(IUSE(J).EQ.-IUSE(J+1)) GO TO 154	EQLM 332
	IF(J.EQ.1.OR.IUSE(J).NE.-IUSE(J-1)) GO TO 153	EQLM 333
	KG = -1	EQLM 334
154	JKG = J + KG	EQLM 335
	TMELT = TEMP(INC,1)	EQLM 336
	IMP = INC + KG	EQLM 337
	IF(TMELT.EQ.TEMP(IMP,2)) GO TO 158	EQLM 338
	TMELT = TEMP(IMP,2)	EQLM 339
	IF (TMELT.EQ.TEMP(IMP,1)) GO TO 157	EQLM 340
	WRITE (6,156)	EQLM 341
156	FORMAT (50H03 PHASES OF A CONDENSED SPECIES ARE OUT OF ORDER)	EQLM 342
	GC TO 873	EQLM 343

C	JTH SPECIES A SOLID (EN=0), (J+KG)TH SPECIES A LIQUID (EN IS +)	EQLM 344
C		EQLM 345
	157 IF(TT.GT.TMELT) GO TO 169	EQLM 346
	IF (TP.AND.TT.EQ.TMELT) GO TO 169	EQLM 347
	IF (TP) GO TO 1165	EQLM 348
	IF (TT.LE.TMELT-150.) GO TO 1165	EQLM 349
	JSOL = J	EQLM 350
	JLIQ = JKG	EQLM 351
	GO TO 159	EQLM 352
C		EQLM 353
C	JTH SPECIES A LIQUID(EN=0), (J+KG)TH SPECIES A SOLID (EN IS +)	EQLM 354
C		EQLM 355
	158 IF (TT.LT.TMELT) GO TO 169	EQLM 356
	IF (TP.AND.TT.EQ.TMELT) GO TO 169	EQLM 357
	IF (TP) GO TO 1165	EQLM 358
	IF (TT.GE.TMELT+150.) GO TO 1165	EQLM 359
	JSOL = JKG	EQLM 360
	JLIQ = J	EQLM 361
	159 TLN = ALCG (TMELT)	EQLM 362
	TT = TMELT	EQLM 363
	EN(JKG,NPT) = .5 * EN(JKG,NPT)	EQLM 364
	EN(J,NPT) = EN(JKG,NPT)	EQLM 365
	GC TO 165	EQLM 366
C		EQLM 367
C	WRONG PHASE INCLUDED FOR T INTERVAL, SWITCH EN	EQLM 368
C		EQLM 369
	1185 EN(J,NPT) = EN (JKG, NPT)	EQLM 370
	IUSE(J) = -IUSE(J)	EQLM 371
	IUSE (JKG) = -IUSE(JKG)	EQLM 372
	EN(JKG,NPT)= 0.	EQLM 373
	GO TO 40	EQLM 374
	153 IF (TT.LT.TEMP(INC,1) .AND.TEMP(INC,1).NE.TLOW) GO TO 169	EQLM 375
	IF (TT.GT.TEMP(INC,2)) GO TO 169	EQLM 376
C		EQLM 377
	SUM = 0.	EQLM 378
	DO 167 I = 1,L	EQLM 379
	SUM = SUM + A(I,J)*X(I)	EQLM 380
	167 CONTINUE	EQLM 381
	DELG = HC(J)-S(J)-SUM	EQLM 382
	IF(RITE) WRITE(6,168)DELG,SIZEG	EQLM 383
	168 FORMAT (18H GO-SUM(AIJ*PII) =E15.7,10X,17HMAX NEG DELTA G =,E15.7)	EQLM 384
	IF(DELG.GE.SIZEG .OR. DELG.GE.0.) GO TO 169	EQLM 385
	SIZEG = CELG	EQLM 386
	JDELG = J	EQLM 387
	169 IF(INC.EQ.NC) GO TO 1160	EQLM 388
	170 CONTINUE	EQLM 389
	1160 IF (SIZEG.EQ.0.) GO TO 143	EQLM 390
	J = JDELG	EQLM 391
	165 IQ1 = IQ1 + 1	EQLM 392
	166 IUSE(J) = - IUSE(J)	EQLM 393
	40 CONVG = .FALSE.	EQLM 394
	JS1 = 1	EQLM 395
	CALL CPHS	EQLM 396
	143 TN = NUME	EQLM 397
	IF(.NOT.SHOCK) WRITE(6,771)NPT,(X(IL),IL=1,L),TN	EQLM 398
	771 FORMAT (I3,14F9.3)	EQLM 399
	JS1 = 1	EQLM 400
	IF(TP.AND.CONVG) CALL CPHS	EQLM 401
	ITNUMB = ITN	EQLM 402
	GO TO 43	EQLM 403
C		EQLM 404
C	CALCULATE EQUILIBRIUM PROPERTIES	EQLM 405
C		EQLM 406
		EQLM 407

C		EQLM 408
1171	DLVPT(NPT) = -1.	EQLM 409
	DLVTP(NPT) = 1.	EQLM 410
	CPR(NPT) = CPSUM	EQLM 411
	GO TO 199	EQLM 412
171	DLVPT(NPT) = -1. + X(IQ1)	EQLM 413
	IF(JLIQ.EQ.0) GO TO 199	EQLM 414
	EN(JSOL,NPT) = ENSOL	EQLM 415
	IUSE(JLIQ) = -IUSE(JLIQ)	EQLM 416
	HSUM(NPT) = HSUM(NPT)+EN(JLIQ,NPT)*(HO(JLIQ)-HO(JSOL))	EQLM 417
	IQ1 = IQ1+1	EQLM 418
	GAMMAS(NPT) = -1./DLVPT(NPT)	EQLM 419
	GO TO 186	EQLM 420
199	GAMMAS(NPT) = -1./(DLVPT(NPT)+(DLVTP(NPT)**2)*ENN/CPR(NPT))	EQLM 421
186	TT(NPT) = TT	EQLM 422
	ENNL = ENL	EQLM 423
	PPP(NPT) = PP	EQLM 424
	VLM(NPT) = RR*ENN*TT/(101.325*PP)	EQLM 425
	HSUM(NPT) = HSUM(NPT)*TT	EQLM 426
	WM(NPT) = 1./ENN	EQLM 427
	IF(TRACE.EQ.0.) GO TO 200	EQLM 428
	DC 1200 J=1,NS	EQLM 429
	IF(IUSE(J).NE.0) GO TO 1200	EQLM 430
	IF(ENLN(J).GT.-87.) EN(J,NPT)=DEXP(ENLN(J))	EQLM 431
1200	CONTINUE	EQLM 432
200	IF(.NOT.RITE) GO TO 863	EQLM 433
	WRITE(6,201) NPT,PP,TT,HSUM(NPT),SSUM(NPT),WM(NPT),CPR(NPT),	EQLM 434
	1 DLVPT(NPT),DLVTP(NPT),GAMMAS(NPT),VLM(NPT)	EQLM 435
201	FORMAT (7HOPOINT=I3,3X,2HP=E13.6,3X,2HT=E13.6,3X,4HH/R=E13.6,3X,4HEQ	EQLM 436
	1S/R=E13.6/73X,3HMW=E13.6,3X,5HCP/R=E13.6,3X,6HDLVPT=E13.6,3X,6HDLVE	EQLM 437
	2TP=E13.6,3X,9HGAMMA(S)=E13.6,3X,2HV=,E13.6)	EQLM 438
863	IF(TT.GE.TLOW.AND.TT.LE.THIGH.OR.SHOCK) GO TO 1000	EQLM 439
	WRITE(6,306) TT,NPT	EQLM 440
306	FORMAT(17HOTHE TEMPERATURE=E12.4,26H IS OUT OF RANGE. FOR POINT,I5)	EQLM 441
	IF(TT.GE.TLOW/1.5.AND.TT.LE.THIGH*1.25) GO TO 1000	EQLM 442
	NPT = NPT+1	EQLM 443
		EQLM 444
C		EQLM 445
C	ERROR, SET TT=0	EQLM 446
C		EQLM 447
	873 TT=0.	EQLM 448
	NPT = NPT-1	EQLM 449
1000	RETURN	EQLM 450
	END	EQLM 450

C	SUBROUTINE CPHS	CPHS 1
C	CALCULATES THERMODYNAMIC PROPERTIES FOR INDIVIDUAL SPECIES	CPHS 2
C		CPHS 3
C	THE FOLLOWING DOUBLE PRECISION TYPE STATEMENTS ARE REQUIRED FOR	CPHS 4
C	IBM 360 MACHINES ONLY	CPHS 5
C		CPHS 6
C	DOUBLE PRECISION COEF,S,EN,ENLN,HO,DELN	CPHS 7
C		CPHS 8
C		CPHS 9
	COMMON /SPECES/COEF(2,7,100),S(100),HO(100),DELN(100),DUMMY(100),	CPHS 10
1	EN(100,13),ENLN(100),A(10,100),SUB(100,3),IUSE(100),TEMP(50,2)	CPHS 11
	COMMON /MISC/ENN,SUMN,TT,SO,ATOM(3,101),LLMT(10),BO(10),BOP(10,2),	CPHS 12
1	TM,TLOW,TMID,THIGH,PP,CPSUM,OF,EQRAT,FPCT,R,RR,HSUBO,AM(2),	CPHS 13
2	HPP(2),RH(2),VMIN(2),VPLS(2),WP(2),DATA(22),NAME(15,5),	CPHS 14
3	ANUH(15,5),PECWT(15),ENTH(15),FAZ(15),RTEMP(15),FOX(15),DENS(15),	CPHS 15
4	RHOP,RMW(15),TLN,CR,DXF(15),ENNL,TRACE,LLMTS(10),SBOP(10,2)	CPHS 16
	COMMON /INCX/IDEBUG,CONVG,TP,HP,SP,ISV,NPP,MOLES,NP,NT,NPT,NLM.	CPHS 17



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1 NS,KMAT,IMAT,IQ1,IOF,NOF,NOMIT,IP,NEW,NSUB,NSUP,RKT,DETN,SHOCK, CPHS 18
2 ICNS,NC,NSERT,JSOL,JLIQ,KASE,NREAC,IC,JS1,VOL,IT,CALCH,NLS,LOGV, CPHS 19
3 ISUP,ISUB,ITNUM,ITM,INCDFZ,INCDEQ,CPRF,IPP,SEQL,PCPLT CPHS 20
C EQUIVALENCE (J,JS1) CPHS 21
C CPHS 22
K = 1 CPHS 23
IF(TT.LE.TMID) K = 2 CPHS 24
KK = C CPHS 25
CPSUM=0. CPHS 26
90 IF(CCEF(K,1,J).NE.0.)GO TO 97 CPHS 27
IF (IUSE(J).LT.0) GO TO 100 CPHS 28
C CPHS 29
C IF COEFFICIENTS ARE ZERO; USE OTHER TEMPERATURE INTERVAL CPHS 30
C CPHS 31
C CPHS 32
KK = K CPHS 33
K = 1 CPHS 34
IF (KK.EQ.1) K = 2 CPHS 35
97 S(J) = (((COEF(K,5,J)/4.)*TT+ COEF(K,4,J)/3.)*TT+ COEF(K,3,J)/ CPHS 36
1 2.)* TT+(COEF(K,2,J))*TT+ COEF(K,1,J)*TLN + COEF(K,7,J) CPHS 37
HC(J) = (((COEF(K,5,J)/5.)*TT+ COEF(K,4,J)/4.)*TT+ COEF(K,3,J)/ CPHS 38
1 3.)* TT+(COEF(K,2,J)/2.)*TT+ COEF(K,1,J) + COEF(K,6,J)/TT CPHS 39
CPSUM= CPSUM+(((COEF(K,5,J))*TT+ COEF(K,4,J))*TT+ COEF(K,3,J))*TT CPHS 40
1 + COEF(K,2,J))*TT+ COEF(K,1,J))*EN(J,NPT) CPHS 41
IF (KK.EQ.0) GO TO 100 CPHS 42
K = KK CPHS 43
KK = 0 CPHS 44
100 IF(J.EQ.NS) GO TO 200 CPHS 45
J=J+1 CPHS 46
GO TO 90 CPHS 47
200 RETURN CPHS 48
END CPHS 49

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C SUBROUTINE MATRIX MATX 1
C MATX 2
C MATX 3
DOUBLE PRECISION G,X MATX 4
LOGICAL FP,SP,TP,IDEBUG,CONVG,NEW, VOL,UV,SV,TV,LOGV MATX 5
C MATX 6
C THE FOLLOWING DOUBLE PRECISION TYPE STATEMENTS ARE REQUIRED FOR MATX 7
C IBM 360 MACHINES ONLY MATX 8
C MATX 9
C DOUBLE PRECISION HSUM,SSUM,CPR,DLVTP,DLVPT,GAMMAS MATX 10
C DOUBLE PRECISION COEF,S,EN,ENLN,HO,DELN MATX 11
C DOUBLE PRECISION H,F,SS,TERM1,TERM,SSS MATX 12
C MATX 13
COMMON /POINTS/HSUM(13),SSUM(13),CPR(13),DLVTP(13),DLVPT(13), MATX 14
1 GAMMAS(13),P(26),T(52),V(13),PPP(13),WM(13),SONVEL(13),TTT(13), MATX 15
2 VLM(13),TOTN(13) MATX 16
COMMON /SPECES/COEF(2,7,100),S(100),HO(100),DELN(100),DUMMY(100), MATX 17
1 EN(100,13),ENLN(100),A(10,100),SUB(100,3),IUSE(100),TEMP(50,2) MATX 18
COMMON /MISC/ENN,SUMN,TT,SO,ATOM(3,101),LLMT(10),BO(10),BOP(10,2), MATX 19
1 TM,TLOW,TMID,THIGH,PP,CPSUM,OF,EQRAT,FPCT,R,RR,HSUBO,AM(2), MATX 20
2 HPP(2),RH(2),VMIN(2),VPLS(2),WP(2),DATA(22),NAME(15,5), MATX 21
3 ANUM(15,5),PECWT(15),ENTH(15),FAZ(15),RTEMP(15),FOX(15),DENS(15), MATX 22
4 RHOP,RMW(15),TLN,CR,OXF(15),ENNL,TRACE,LLMTS(10),SBOP(10,2) MATX 23
COMMON /DOUBLE/ G(20,21), X(20) MATX 24
COMMON /INDX/IDEBUG,CONVG,TP,HP,SP,ISV,NPP,MOLES,NP,NT,NPT,NLM, MATX 25

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1	NS,KMAT,IMAT,IQ1,IOF,NOF,NOMIT,IP,NEW,NSUB,NSUP,RKT,DETN,SHOCK,	MATX	26
2	IONS,NC,NSERT,JSOL,JLIQ,KASE,NREAC,IC,JSI,VOL,IT,CALCH,NLS,LOGV,	MATX	27
3	ISUP,ISUB,ITNUM,ITM,INCOFZ,INCDEQ,CPRF,IPP,SEQL,PCPLT	MATX	28
C		MATX	29
	EQUIVALENCE (NLM,L),(TP,TV),(SV,SP),(UV,HP)	MATX	30
C		MATX	31
	IQ2 = IQ1 + 1	MATX	32
	IQ3 = IQ2 + 1	MATX	33
	KMAT = IQ3	MATX	34
	(F(.NOT.CONVG.AND.TP) KMAT = IQ2	MATX	35
	IMAT = KMAT - 1	MATX	36
C		MATX	37
C	CLEAR MATRIX STORAGES TO ZERO	MATX	38
C		MATX	39
	DO 211 I=1,IMAT	MATX	40
	DO 211 K=1,KMAT	MATX	41
	G(I,K)= 0.CDO	MATX	42
211	CONTINUE	MATX	43
	SSS = 0.	MATX	44
	HSUM(NPT) = 0.	MATX	45
C		MATX	46
C	BEGIN SET UP OF ITERATION MATRIX	MATX	47
C		MATX	48
	KK = L	MATX	49
	DO 65 J=1,NS	MATX	50
	IF(IUSE(J).LT.0) GO TO 65	MATX	51
	H=HO(J)*EN(J,NPT)	MATX	52
	IF(IUSE(J).GT.0) GO TO 70	MATX	53
	F = (HO(J)-S(J)+ENLN(J)*TM)*EN(J,NPT)	MATX	54
	SS = H-F	MATX	55
	TERM1 = H	MATX	56
	IF (KMAT .EQ. IQ2) TERM1 = F	MATX	57
	DO 55 I = 1, L	MATX	58
C		MATX	59
C	CALCULATE THE ELEMENTS R(I,K)	MATX	60
C		MATX	61
	IF (A(I,J) .EQ. 0.) GO TO 55	MATX	62
	TERM= A(I,J)*EN(J,NPT)	MATX	63
	DO 15 K=I, L	MATX	64
	G(I,K)= G(I,K) + A(K,J)*TERM	MATX	65
15	CONTINUE	MATX	66
C		MATX	67
	G(I,IQ1)=G(I,IQ1)+TERM	MATX	68
	G(I,IQ2)=G(I,IQ2)+A(I,J)*TERM1	MATX	69
	IF (CONVG .OR. TP) GO TO 55	MATX	70
	G(I,IQ3)= G(I,IQ3)+A(I,J)*F	MATX	71
	IF (SP) G(IQ2,I) = G(IQ2,I) + A(I,J)*SS	MATX	72
55	CCNTINUE	MATX	73
	IF (KMAT .EQ. IQ2) GO TO 64	MATX	74
	IF(CONVG.OR.HP) GO TO 59	MATX	75
	G(IQ2,IQ1) = G(IQ2,IQ1) + SS	MATX	76
	G(IQ2,IQ2)=G(IQ2,IQ2)+HO(J)*SS	MATX	77
	G(IQ2,IQ3) = G(IQ2,IQ3)+(S(J) - ENLN(J)-TM)*F	MATX	78
	GO TO 62	MATX	79
59	G(IQ2,IQ2)=G(IQ2,IQ2)+HO(J)*H	MATX	80
	IF (CONVG) GO TO 64	MATX	81
	G(IQ2,IQ3)=G(IQ2,IQ3)+HO(J)*F	MATX	82
62	G(IQ1,IQ2)=G(IQ1,IQ2)+F	MATX	83
64	G(IQ1,IQ2)=G(IQ1,IQ2)+TERM1	MATX	84
	GO TO 65	MATX	85
C		MATX	86
C	CONDENSED SPECIES	MATX	87
C		MATX	88
	70 KK = KK + 1	MATX	89
	DO 75 I = 1,L	MATX	90



	G(I, KK) = A(I, J)	MATX 91
	G(I, KMAT) = C(I, KMAT) - A(I, J)*EN(J, NPT)	MATX 92
75	CONTINUE	MATX 93
	G(KK, IQ2) = HO(J)	MATX 94
	G(KK, KMAT) = HO(J) - S(J)	MATX 95
	HSUM(NPT) = HSUM(NPT) + H	MATX 96
	IF(.NOT.SP) GO TO 65	MATX 97
	SSS = SSS + S(J)*EN(J, NPT)	MATX 98
	G(IQ2, KK) = S(J)	MATX 99
85	CONTINUE	MATX 100
	SSS = SSS + G(IQ2, IQ1)	MATX 101
	HSUM(NPT) = HSUM(NPT) + G(IQ1, IQ2)	MATX 102
	G(IQ1, IQ1) = SUMN - ENN	MATX 103
C		MATX 104
C	REFLECT SYMMETRIC PORTIONS OF THE MATRIX	MATX 105
C		MATX 106
	ISYM = IQ1	MATX 107
	IF(HP.OR.CONVG) ISYM=IQ2	MATX 108
	DO 102 I=1, ISYM	MATX 109
	DO 102 J=I, ISYM	MATX 110
	G(J, I)=G(I, J)	MATX 111
102	CONTINUE	MATX 112
C		MATX 113
C	COMPLETE THE RIGHT HAND SIDE	MATX 114
C		MATX 115
	IF(.NOT.CONVG) GO TO 140	MATX 116
	IF(.NOT.LOGV) GO TO 175	MATX 117
C		MATX 118
C	LOGV = .TRUE.-- SET UP MATRIX TO SOLVE FOR DLVPT	MATX 119
C		MATX 120
	G(IQ1, IQ2) = ENN	MATX 121
	IQ = IQ1 - 1	MATX 122
	DO 135 I = 1, IQ	MATX 123
	G(I, IQ2) = G(I, IQ1)	MATX 124
135	CONTINUE	MATX 125
	GO TO 175	MATX 126
140	DO 145 I=1, L	MATX 127
	X(1)=BO(I)-G(I, IQ1)	MATX 128
	G(I, KMAT) = G(I, KMAT)+X(1)	MATX 129
145	CONTINUE	MATX 130
	G(IQ1, KMAT) = G(IQ1, KMAT)+ENN-SUMN	MATX 131
C		MATX 132
C	COMPLETE ENERGY ROW AND TEMPERATURE COLUMN	MATX 133
C		MATX 134
	IF (KMAT .EQ. IQ2) GO TO 185	MATX 135
	IF (SP)ENERGY = SO+ENN-SUMN - SSS	MATX 136
	IF(HP)ENERGY=HSUBO/TT - HSUM(NPT)	MATX 137
	G(IQ2, IQ3)=G(IQ2, IQ3)+ ENERGY	MATX 138
175	G(IQ2, IQ2)= G(IQ2, IQ2)+CPSUM	MATX 139
185	IF(.NOT.VOL.OR.CONVG) GO TO 1000	MATX 140
C		MATX 141
C	CONSTANT VOLUME MATRIX	MATX 142
C		MATX 143
	IQ = IQ1-1	MATX 144
	IF(KMAT.EQ.IQ2) GO TO 230	MATX 145
	DO 220 I=1, IQ	MATX 146
	G(IQ1, I) = G(IQ2, I)-G(IQ1, I)	MATX 147
	G(I, IQ1) = G(I, IQ2)-G(I, IQ1)	MATX 148
	G(I, IQ2) = G(I, IQ3)	MATX 149
220	CONTINUE	MATX 150
	G(IQ1, IQ1) = G(IQ2, IQ2)-G(IQ1, IQ2)-G(IQ2, IQ1)	MATX 151
	G(IQ1, IQ2) = G(IQ2, IQ3)-G(IQ1, IQ3)	MATX 152
	IF (UV) G(IQ1, IQ2) = G(IQ1, IQ2) + ENN	MATX 153
	GO TO 260	MATX 154

230 DO 240 I=1,IQ	MATX 155
G(I,IQ1) = G(I,IQ2)	MATX 156
240 CONTINUE	MATX 157
260 KMAT = IMAT	MATX 158
IMAT = IMAT-1	MATX 159
1000 RETURN	MATX 160
END	MATX 161

C		OUTP	1
C	SUBROUTINE OUT1	OUTP	2
C	DOUBLE PRECISION G,X	OUTP	3
C		OUTP	4
C	THE FOLLOWING DOUBLE PRECISION TYPE STATEMENTS ARE REQUIRED FOR	OUTP	5
C	IBM 360 MACHINES ONLY	OUTP	6
C		OUTP	7
C	DOUBLE PRECISION HSUM,SSUM,CPR,DLVTP,DLVPT,GAMMAS	OUTP	8
C	DOUBLE PRECISION COEF,S,EN,ENLN,HO,DELN	OUTP	9
C		OUTP	10
C	LOGICAL EQL,FROZ,TP,HP,SP,HPSP,TPSP,MOLES,VOL,PUNCH,RKT	OUTP	11
C		OUTP	12
C	DIMENSION NV(13),Z(10,3),HEAD(15),YX(5),YN(5),FSB(3),FRHO(3)	OUTP	13
C	DIMENSION DENSTY(13),ENTLPY(13),ENTRPY(13),SPHEAT(13)	OUTP	14
C		OUTP	15
C	COMMON /POINTS/HSUM(13),SSUM(13),CPR(13),DLVTP(13),DLVPT(13),	OUTP	16
C	1 GAMMAS(13),P(26),T(52),V(13),PPP(13),WM(13),SONVEL(13),TTT(13),	OUTP	17
C	2 VLM(13),TOTN(13)	OUTP	18
C	COMMON /SPECES/COEF(2,7,100),S(100),HO(100),DELN(100),DUMMY(100),	OUTP	19
C	1 EN(100,13),ENLN(100),A(10,100),SUB(100,3),IUSE(100),TEMP(50,2)	OUTP	20
C	COMMON /MISC/ENN,SUMN,TT,SO,ATOM(3,101),LLMT(10),BO(10),BOP(10,2),	OUTP	21
C	1 TM,TLOW,TMID,THIGH,PP,CPSUM,OF,EQRAT,FPCT,R,RR,HSUBO,AM(2),	OUTP	22
C	2 HPP(2),RH(2),VMIN(2),VPLS(2),WP(2),DATA(22),NAME(15,5),	OUTP	23
C	3 ANUM(15,5),PECWT(15),ENTH(15),FAZ(15),RTEMP(15),FOX(15),DENS(15),	OUTP	24
C	4 RHOP,RMW(15),TLN,CR,OXF(15),ENNL,TRACE,LLMTS(10),SBOP(10,2)	OUTP	25
C	COMMON /DOUBLE/ G(20,21), X(20)	OUTP	26
C	COMMON /INCX/IDEBUG,CONVG,TP,HP,SP,ISV,NPP,MOLES,NP,NT,NPT,NLM,	OUTP	27
C	1 NS,KMAT,IMAT,IQ1,IOF,NOF,NOMIT,IP,NEW,NSUB,NSUP,RKT,DET,SHOCK,	OUTP	28
C	2 ICNS,NC,INSERT,JSOL,JLIQ,KASE,NREAC,IC,JS1,VOL,IT,CALCH,NLS,LOGV,	OUTP	29
C	3 ISUP,ISUB,ITNUM,ITM,INCOFZ,INCDEQ,CPRF,IPP,SEQ,PCPLT	OUTP	30
C	COMMON /PERF/PCP(22),VMOC(13),SPIM(13),VACI(13),SUBAR(13),	OUTP	31
C	1 SUPAR(13),APP(13),AEAT(13),CSTR,EQL,FROZ,SSO,AREA,AWT,NFZ,	OUTP	32
C	2 APPL,ARATIO,ELN	OUTP	33
C	COMMON /SAVED/SLN(100),IQSAVE,ENSAVE,ENLSAV,LSAVE,JSOLS,JLIQS,	OUTP	34
C	1 LLL,LM,MAXNP,STORE(52,16),XS(20),WMOL(20),IND(20),NM,	OUTP	35
C	2 FIRSTP,FIRSTV	OUTP	36
C	COMMON /OUP/FMT(30),FP(4),FT(4),FH(4),FS(4),FM(4),FV(4),FD(4),	OUTP	37
C	1 FC(4),FG(4),FB,FMT13,F1,F2,F3,F4,F5,FL(4),FMT19,FA1,FA2,	OUTP	38
C	2 FR1,FC1,FN(4),FR(4),FA(4),FI(4),FMT9X,F0	OUTP	39
C	COMMON /CONTRL/TRNSPT,FROZN,PUNCH,NODATA	OUTP	40
C		OUTP	41
C	EQUIVALENCE (V,NV),(Z,HO),(IB,FB)	OUTP	42
C		OUTP	43
C	HEAD=(1H ,2A4,5(A2,F8.5,3X),5X,F7.5,F13.3,4X,A1,F10.2,F9.4)	OUTP	44
C		OUTP	45
C	DATA HEAD/4H(1H ,4H,2A4,2H,5,4H(A2,,4HF8.5 ,4H,3X),2H,5 ,2HX,	OUTP	46
C	1 ,4HF7.5 ,4H,F13 ,4H.3,4 ,4HX,A1 ,4H,F10 ,4H.2,F ,4H9.4)/	OUTP	47
C	DATA FUEL/4HFUEL/,OXID/4HOXID/,ANT/3HANT/,CX/1HO/,IZ/2H00/,	OUTP	48
C	1 YN/2H,1, 2H,2, 2H,3, 2H,4, 2H,5 /,F75/4HF7.5/.	OUTP	49



	2 YX/3H,57,3H,44,3H,31,3H,18,2H,5 /,F73/4HF7.3/	OUTP 50
	DATA FRHO/4HRHO,,4H G/C,1HC/	OUTP 51
C	IF(KASE.NE.0) WRITE (6,3) KASE	OUTP 52
	2 FCRMAT (9H CASE NO. ,I8)	OUTP 53
	IF(.NOT.MOLES) WRITE(6,5)	OUTP 54
	5 FCRMAT (77X,46HWT FRACTION ENERGY STATE TEMP DENSITY/	OUTP 55
	1 10X,16HCHEMICAL FORMULA,51X,21H(SEE NOTE) CAL/MOL,10X,5HDEG K,	OUTP 56
	2 4X,4HG/CC)	OUTP 57
	IF(MOLES) WRITE(6,6)	OUTP 58
	6 FCRMAT (79X,5HMOLES,7X, 33H ENERGY STATE TEMP DENSITY/	OUTP 59
	1 10X,16HCHEMICAL FORMULA,66X,7H CAL/MOL,10X,13HDEG K G/CC)	OUTP 60
	DO 15 N=1,NREAC	OUTP 61
	IF(FOX(N).NE.OX)GO TO 10	OUTP 62
	HD1 = OXID	OUTP 63
	HD2 = ANT	OUTP 64
	GO TO 11	OUTP 65
10	HD1 = FUEL	OUTP 66
	HD2 = FB	OUTP 67
11	DO 13 J=1,5	OUTP 68
	IF(NAME(N,J).EQ.IZ.OR.NAME(N,J).EQ.IB) GO TO 14	OUTP 69
13	CONTINUE	OUTP 70
	J=6	OUTP 71
14	J=J-1	OUTP 72
	HEAD(3)=YN(J)	OUTP 73
	HEAD(7)=YX(J)	OUTP 74
	HEAD(9) = F75	OUTP 75
	IF(PECWT(N).GE.10.) HEAD(9)=F73	OUTP 76
	WRITE(6,HEAD) HD1,HD2,(NAME(N,J),ANUM(N,JJ),JJ=1,J),PECWT(N),	OUTP 77
	1 ENTH(N), FAZ(N),RTEMP(N),DENS(N)	OUTP 78
15	CONTINUE	OUTP 79
	FPC = 100./(1.+OF)	OUTP 80
	WRITE(6,20) OF,FPC,EQRAT,RHOP	OUTP 81
20	FORMAT (1H0,15X, 4HO/F=, F8.4,4X,13HPERCENT FUEL=,F8.4,4X,	OUTP 82
	1 19HEQUIVALENCE RATIO= ,F7.4,4X,17HREACTANT DENSITY=,F8.4//)	OUTP 83
	AGV = 9.80665	OUTP 84
		OUTP 85
C	RETURN	OUTP 86
		OUTP 87
C	ENTRY OUT2	OUTP 88
	FMT(4) = FMT(6)	OUTP 89
		OUTP 90
C	PRESSURE	OUTP 91
C		OUTP 92
C	50 IF(R.LT.10.) GO TO 60	OUTP 93
	CALL EFMT(NPT,FP,PPP)	OUTP 94
	GO TO 64	OUTP 95
	60 CALL VARFMT (PPP,NPT)	OUTP 96
	WRITE (6,FMT) (FP(I),I=1,4),(PPP(J),J=1,NPT)	OUTP 97
		OUTP 98
C	TEMPERATURE	OUTP 99
C		OUTP 100
C	64 DO 65 I=1,NPT	OUTP 101
	NV(I)= TIT(I)+.5	OUTP 102
	65 CONTINUE	OUTP 103
	FMT(4)= FMT13	OUTP 104
	FMT(5)= FMTI9	OUTP 105
	WRITE (6,FMT) (FT(I),I=1,4),(NV(J),J=1,NPT)	OUTP 106
		OUTP 107
C	DENSITY	OUTP 108
C		OUTP 109
C	DO 70 I=1,NPT	OUTP 110
	IF(VLM(I).NE.0.) V(I)=1./VLM(I)	OUTP 111
	DENSTY(I) = V(I)	OUTP 112
		OUTP 113

70	CONTINUE		OUTP 114
	CALL EFMT(NPT,FRHO,V)		OUTP 115
C			OUTP 116
C	ENTHALPY		OUTP 117
C			OUTP 118
	DO 75 I=1,NPT		OUTP 119
	V(I) = HSUM(I) * R		OUTP 120
	ENTLPHY(I) = V(I)		OUTP 121
75	CONTINUE		OUTP 122
	FMT(5)= FB		OUTP 123
	IF(R.LT.10.) GO TO 76		OUTP 124
	CALL EFMT(NPT,FH,V)		OUTP 125
	FMT(7) = F1		OUTP 126
	GO TO 77		OUTP 127
76	FMT(7) = F1		OUTP 128
	WRITE (6,FMT) (FH(I),I=1,4),(V(J),J=1,NPT)		OUTP 129
C			OUTP 130
C	ENTROPY		OUTP 131
C			OUTP 132
	FMT(7)=F4		OUTP 133
77	DO 78 I=1,NPT		OUTP 134
	V(I) = SSUM(I) * R		OUTP 135
	ENTRPY(I) = V(I)		OUTP 136
78	CONTINUE		OUTP 137
	WRITE (6,FMT) (FS(I),I=1,4),(V(J),J=1,NPT)		OUTP 138
	WRITE (6,80)		OUTP 139
80	FORMAT (1H)		OUTP 140
C			OUTP 141
C	MOLECULAR WEIGHT		OUTP 142
C			OUTP 143
	FMT(7)= F3		OUTP 144
	WRITE (6,FMT) (FM(I),I=1,4),(WM(J),J=1,NPT)		OUTP 145
C			OUTP 146
C	(DLV/DLP)T		OUTP 147
C			OUTP 148
	FMT(7)=F5		OUTP 149
	IF(EQL) WRITE(6,FMT) (FV(I),I=1,4),(DLVPT(J),J=1,NPT)		OUTP 150
C			OUTP 151
C	(DLV/DLT)P		OUTP 152
C			OUTP 153
	FMT(7)= F4		OUTP 154
	IF(EQL) WRITE(6,FMT) (FD(I),I=1,4),(DLVTP(J),J=1,NPT)		OUTP 155
C			OUTP 156
C	HEAT CAPACITY		OUTP 157
C			OUTP 158
	IF(R.GT.10.) FMT(7)=F1		OUTP 159
	DO 85 I=1,NPT		OUTP 160
	V(I) = CPR(I) * R		OUTP 161
	SPHEAT(I) = V(I)		OUTP 162
85	CONTINUE		OUTP 163
	WRITE(6,FMT) (FC(I),I=1,4),(V(J),J=1,NPT)		OUTP 164
C			OUTP 165
C	GAMMA(S)		OUTP 166
C			OUTP 167
	FMT(7) = F4		OUTP 168
	WRITE(6,FMT) (FG(I),I=1,4),(GAMMAS(J),J=1,NPT)		OUTP 169
C			OUTP 170
C	SONIC VELOCITY		OUTP 171
C			OUTP 172
	FMT(7)= F1		OUTP 173
	DO 95 I = 1,NPT		OUTP 174
	SONVEL(I) = (RR*GAMMAS(I)*TTT(I)/WM(I))**.5		OUTP 175
95	CONTINUE		OUTP 176
	WRITE(6,FMT) (FL(I),I=1,4),(SONVEL(J),J=1,NPT)		OUTP 177

C		OUTP 178
C	PUNCHED CARDS	OUTP 179
C		OUTP 180
	IF(.NOT.PUNCH) GO TO 4	OUTP 181
	DO 1 I=1,NPT	OUTP 182
	IF(RKT.AND.ISV.EQ.O.AND.MAXNP.GT.O.AND.(I.EQ.1.OR.I.EQ.2)) GO TO 1	OUTP 183
	PUNCH 2, TTT(I),PPP(I),DENSTY(I),ENTLPY(I),ENTRPY(I),WM(I),	OUTP 184
	1 DLVPT(I),CLVTP(I),V(I),GAMMAS(I),SONVEL(I),FPC	OUTP 185
	2 FORMAT (F8.2,2(3X,E10.5),F11.2,F11.4,F11.5/2F11.6,F11.5,F11.6,	OUTP 186
	1 F10.2,2X,F8.4)	OUTP 187
	1 CONTINUE	OUTP 188
C		OUTP 189
	4 RETURN	OUTP 190
C		OUTP 191
	ENTRY OUT3	OUTP 192
C		OUTP 193
	TRA = 5.E-6	OUTP 194
	IF(TRACE.NE.O.) TRA= TRACE	OUTP 195
	IF(.NOT.EQL) GO TO 331	OUTP 196
C		OUTP 197
C	MOLE FRACTIONS - EQUILIBRIUM	OUTP 198
C		OUTP 199
	WRITE (6,80)	OUTP 200
	FMT(7)= F5	OUTP 201
	WRITE(6,310)	OUTP 202
310	FORMAT(15HMOLE FRACTIONS //)	OUTP 203
	DO 330 K=1,NS	OUTP 204
	DO 315 I=1,NPT	OUTP 205
	V(I) = EN(K,I)/TOTN(I)	OUTP 206
315	CONTINUE	OUTP 207
	DO 316 I=1,NPT	OUTP 208
	IF(TRACE.EQ.O.) GO TO 317	OUTP 209
	IF(V(I).GE.TRACE) GO TO 325	OUTP 210
317	IF(V(I).GE.(5.E-6)) GO TO 320	OUTP 211
316	CONTINUE	OUTP 212
	GO TO 330	OUTP 213
320	WRITE (6,FMT) SUB(K,1),SUB(K,2),SUB(K,3),FB,(V(I),I=1,NPT)	OUTP 214
	GO TO 330	OUTP 215
325	FSB(1) = SUB(K,1)	OUTP 216
	FSB(2) = SUB(K,2)	OUTP 217
	FSB(3) = SUB(K,3)	OUTP 218
	CALL EFMT(NPT,FSB,V)	OUTP 219
330	CCONTINUE	OUTP 220
331	WRITE(6,335) TRA	OUTP 221
335	FORMAT(82H0ADDITIONAL PRODUCTS WHICH WERE CONSIDERED BUT WHOSE MOLE	OUTP 222
	FRACITNS WERE LESS THAN ,E12.5,28H FOR ALL ASSIGNED CONDITIONS/OUTP	OUTP 223
	2//)	OUTP 224
	LINE= 0	OUTP 225
	NN = 1	OUTP 226
	IF(EQL) NN=NPT	OUTP 227
	DO 350 K=1,NS	OUTP 228
	DO 340 I=1,NN	OUTP 229
	IF ((EN(K,I)/TOTN(I)).GE.TRA) GO TO 343	OUTP 230
340	CONTINUE	OUTP 231
	LINE= LINE+1	OUTP 232
	Z(LINE,1)= SUB(K,1)	OUTP 233
	Z(LINE,2)= SUB(K,2)	OUTP 234
	Z(LINE,3)= SUB(K,3)	OUTP 235
343	IF ((LINE.NE.10) .AND. K.NE.NS) GO TO 350	OUTP 236
	IF (LINE.EQ.O) GO TO 1000	OUTP 237
	WRITE(6,245) (Z(LN,1),Z(LN,2),Z(LN,3),LN=1,LINE)	OUTP 238
345	FORMAT (10(1X,3A4))	OUTP 239
	LINE= 0	OUTP 240
350	CONTINUE	OUTP 241
	IF(.NCT.MOLES) WRITE(6,360)	OUTP 242

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360 FORMAT(7EHNOTE. WEIGHT FRACTION OF FUEL IN TOTAL FUELS AND OF OXIOUTP 243
      2DANT IN TOTAL OXIDANTS )      OUTP 244
1000 RETURN      OUTP 245
      ENC      OUTP 246

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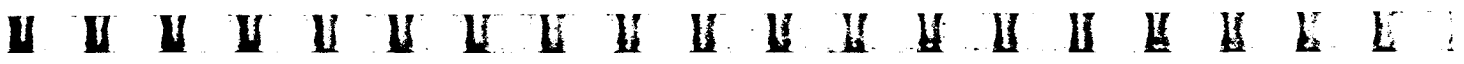
C      SUBROUTINE VARFMT(V,NPT)      VRFT  1
C      DIMENSION V(13)      VRFT  2
C      COMMON/OUPT/FMT(30),FP(4),FT(4),FH(4),FS(4),FM(4),FV(4),FD(4),
1 FC(4),FG(4),FB,FMT13,F1,F2,F3,F4,F5,FL(4),FMTI9,FA1,FA2,
2 FR1,FC1,FN(4),FR(4),FA(4),FI(4),FMT9X,F0      VRFT  3
C      DC 45 I=1,NPT      VRFT  4
      K= 2*I+3      VRFT  5
      FMT(K) = F4      VRFT  6
      IF (V(I).GE.10.) FMT(K) = F3      VRFT  7
      IF (V(I).GE.100.) FMT(K) = F2      VRFT  8
      IF (V(I).GE.10000.) FMT(K) = F1      VRFT  9
      IF (V(I).GE.1000000.) FMT(K) = F0      VRFT 10
45 CONTINUE      VRFT 11
      RETURN      VRFT 12
      END      VRFT 13

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C      SUBROUTINE EFMT(NPT,AA,V)      EFMT  1
C      DIMENSION AA(3), V(13), W(13), NE(13), FRMT(7)      EFMT  2
C      COMMON/OUPT/FMT(30),FP(4),FT(4),FH(4),FS(4),FM(4),FV(4),FD(4),
1 FC(4),FG(4),FB,FMT13,F1,F2,F3,F4,F5,FL(4),FMTI9,FA1,FA2,
2 FR1,FC1,FN(4),FR(4),FA(4),FI(4),FMT9X,F0      EFMT  3
C      DATA FRMT/3H(1H,4H,3A4,4H,11X,4H,13(,4HF7.4,4H,I2),1H)/,F63/4HF6.3
1/,FI3/4H,I3)/,F74/4HF7.4/,FI2/4H,I2)/,F11X/4H,11X/,F2X/3H,2X/      EFMT  4
C      FRMT(5) = F74      EFMT  5
      FRMT(6) = FI2      EFMT  6
      J1 = 1      EFMT  7
      FRMT(3) = F2X      EFMT  8
      IF(FMT(4).NE.FMT9X) GO TO 130      EFMT  9
      J1 = 2      EFMT 10
      FRMT(3) = F11X      EFMT 11
130 DC 145 I=J1,NPT      EFMT 12
      IF(V(I).NE.0.) GO TO 140      EFMT 13
      W(I) = 0.      EFMT 14
      NE(I) = 0.      EFMT 15
      GO TO 145      EFMT 16
140 EE = ALOG10(ABS(V(I)))      EFMT 17
      NE(I) = EE      EFMT 18
      FE = NF(I)      EFMT 19

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IF(EE.LE.0..AND.FE.NE.EE) NE(I)=NE(I)-1	EFMT 27
IF(IABS(NE(I)).LT.10) GO TO 144	EFMT 28
FRMT(5) = F63	EFMT 29
FRMT(6) = F13	EFMT 30
144 W(I) = V(I)/10.**NE(I)	EFMT 31
145 CCNTINUE	EFMT 32
WRITE(6,FRMT) (AA(I),I=1,3),(W(J), NE(J),J=J1,NPT)	EFMT 33
1000 RETURN	EFMT 34
END	EFMT 35

C	SUBROUTINE THERMP (*)	THRP 1
C		THRP 2
C	THE FOLLOWING DOUBLE PRECISION TYPE STATEMENTS ARE REQUIRED FOR	THRP 3
C	IBM 360 MACHINES ONLY	THRP 4
C		THRP 5
C	DOUBLE PRECISION HSUM,SSUM,CPR,DLVTP,DLVPT,GAMMAS	THRP 6
C	DOUBLE PRECISION COEF,S,EN,ENLN,HO,DELN	THRP 7
C		THRP 8
C	LOGICAL HP,SP,TP,UV,SV,NEW, IONS,MOLES,FROZ,EQL,PSIA,RKT,VOL,TV,	THRP 9
C	1 CALCH	THRP 10
C		THRP 11
C	DIMENSION VL(26)	THRP 12
C		THRP 13
C	COMMON /POINTS/HSUM(13),SSUM(13),CPR(13),DLVTP(13),DLVPT(13),	THRP 14
C	1 GAMMAS(13),P(26),T(52),V(13),PPP(13),WM(13),SONVFL(13),TTT(13),	THRP 15
C	2 VLM(13),TOTN(13)	THRP 16
C	COMMON /SPECES/COEF(2,7,100),S(100),HO(100),DELN(100),DUMMY(100),	THRP 17
C	1 EN(100,13),ENLN(100),A(10,100),SUB(100,3),IUSE(100),TEMP(50,2)	THRP 18
C	COMMON /MISC/ENN,SUMN,TT,SO,ATOM(3,101),LLMT(10),BO(10),BOP(10,2),	THRP 19
C	1 TM,TLOW,TMID,THIGH,PP,CPSUM,OF,EQRAT,FPCT,R,RR,HSUBO,AM(2),	THRP 20
C	2 HPP(2),RH(2),VMIN(2),VPLS(2),WP(2),DATA(22),NAME(15,5),	THRP 21
C	3 ANUM(15,5),PECWT(15),ENTH(15),FAZ(15),RTEMP(15),FOX(15),DENS(15),	THRP 22
C	4 RHOP,RMW(15),TLN,CR,OXF(15),ENNL,TRACE,LLMTS(10),SBCP(10,2)	THRP 23
C	COMMON /INDX/IDERUG,CONVG,TP,HP,SP,ISV,NPP,MOLES,NP,NT,NPT,NLM,	THRP 24
C	1 NS,KMAT,IMAT,IQ1,IOF,NOF,NOMIT,IP,NEW,NSUB,NSUP,RKT,DET,SHOCK,	THRP 25
C	2 IONS,NC,NSERT,JSOL,JLIQ,KASE,NREAC,IC,JS1,VOL,IT,CALCH,NLS,LOGV,	THRP 26
C	3 ISUP,ISUB,ITNUM,ITM,INCDFZ,INCDEQ,CPRF,IPP,SEQ,PCPLT	THRP 27
C	COMMON /DUPT/FMT(30),FP(4),FT(4),FH(4),FS(4),FM(4),FV(4),FD(4),	THRP 28
C	1 FC(4),FG(4),FB,FMT13,F1,F2,F3,F4,F5,FL(4),FMTI9,FA1,FA2,	THRP 29
C	2 FR1,FC1,FN(4),FR(4),FA(4),FI(4),FMT9X,FC	THRP 30
C		THRP 31
C	EQUIVALENCE (K,ISV),(VL,P),(UV,HP),(TP,TV),(SP,SV)	THRP 32
C		THRP 33
C	DATA FUU/4+U, C/	THRP 34
C		THRP 35
C	IF(T(1).EQ.0.) T(1) = 3800.	THRP 36
C		THRP 37
C	IOF = 0	THRP 38
C	95 IOF = IOF+1	THRP 39
C	OF = OXF(IOF)	THRP 40
C	CALL NEWCF	THRP 41
C	IF(TT.EQ.0..AND.CALCH) RETURN 1	THRP 42
C		THRP 43
C	SET ASSIGNED P OR VOLUME	THRP 44
C		THRP 45
C	IP = 0	THRP 46
C	903 IP = IP + 1	THRP 47



	PP = P(IF)	THRP 48
	VLM(NPT) = VL(IP)	THRP 49
C		THRP 50
C	SET ASSIGNED T	THRP 51
	IT = 0	THRP 52
902	IT = IT + 1	THRP 53
	TT = T(IT)	THRP 54
	CALL EQLPRM	THRP 55
	IF(TT.NE.0.) GO TO 800	THRP 56
	IF(NPT.EC.0) GO TO 1000	THRP 57
800	K = 0	THRP 58
	IF(IP.EQ.NP.AND.IT.EQ.NT.OR.TT.EQ.0.) GO TO 860	THRP 59
	K = NPT	THRP 60
	IF(NPT.NE.13) GO TO 870	THRP 61
860	IF(.NOT.HP) WRITE(6,5)	THRP 62
	5 FORMAT(1H1,41X,48HTHERMODYNAMIC EQUILIBRIUM PROPERTIES AT ASSIGNED	THRP 63
	1)	THRP 64
	IF(HP) WRITE(6,6)	THRP 65
	6 FORMAT(1H1,36X,59HTHERMODYNAMIC EQUILIBRIUM COMBUSTION PROPERTIES	THRP 66
	1AT ASSIGNED)	THRP 67
	IF(.NOT.VOL) GO TO 861	THRP 68
	IF(UV) WRITE(6,10)	THRP 69
10	FORMAT(1H0,62X,7H VOLUME /)	THRP 70
	IF(TV) WRITE(6,11)	THRP 71
11	FORMAT(1H0,54X,22HTEMPERATURE AND VOLUME/)	THRP 72
	IF(SV) WRITE(6,12)	THRP 73
12	FORMAT(1H0,56X,18HENTROPY AND VOLUME/)	THRP 74
	GO TO 862	THRP 75
861	IF(HP) WRITE(6,20)	THRP 76
20	FORMAT(1H0,62X,10H PRESSURES /)	THRP 77
	IF(TP) WRITE(6,21)	THRP 78
21	FORMAT(1H0,53X,24HTEMPERATURE AND PRESSURE/)	THRP 79
	IF(SP) WRITE(6,22)	THRP 80
22	FORMAT(1H0,55X,20HENTROPY AND PRESSURE/)	THRP 81
862	CALL OUT1	THRP 82
	WRITE (6,863)	THRP 83
863	FORMAT (25HOTHERMODYNAMIC PROPERTIES//)	THRP 84
	IF(.NOT.VOL) GO TO 864	THRP 85
	FMT(4) = FMT(6)	THRP 86
	IF(.NOT.UV) GO TO 864	THRP 87
	DO 63 I=1,NPT	THRP 88
	FMT(2*I+3) = F2	THRP 89
	V(I) = HSUBO*R	THRP 90
63	CONTINUE	THRP 91
	WRITE(6,FMT) FUU,FH(2),FB,FB,(V(I),I=1,NPT)	THRP 92
864	CALL OUT2	THRP 93
	CALL OUT3	THRP 94
C		THRP 95
	RETURN	THRP 96
C		THRP 97
	ENTRY THERM1	THRP 98
C		THRP 99
		THRP 100
865	IF(K.EQ.0 .AND. IOF.EQ.NO) GO TO 1000	THRP 101
	IF(IDEBUG.GT.13) IDEBUG=IDEBUG-13	THRP 102
	WRITE(6,868)	THRP 103
868	FORMAT(1H1)	THRP 104
	IF(NT.EQ.1.AND.NP.EQ.1) GO TO 95	THRP 105
	NPT = 0	THRP 106
870	NPT = NPT + 1	THRP 107
	IF(.NOT.TP.AND.TT.NE.0.) T(1)=TT	THRP 108
	IF(IP.EQ.1.AND.IT.EQ.1) ISV=-ISV	THRP 109
	IF(NT.EQ.1) GO TO 871	THRP 110
	IF(IT.EQ.NT.OR.TT.EQ.0.) ISV=0	THRP 111
871	CALL SAVE	THRP 112
	IF(IT.LT.NT) GO TO 902	THRP 113

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IF(IP.LT.NP) GO TO 903
GO TO 95
1000 RETURN 1
END

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THRP 114
THRP 115
THRP 116
THRP 117

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C          SUBROUTINE ROCKET (*)                ROCK  1
C          ROCKE. PERFORMANCE                  ROCK  2
C          DOUBLE PRECISION USQ,ASQ            ROCK  3
C          DOUBLE PRECISION HSUM,SSUM,CPR,DLVTP,DLVPT,GAMMAS  ROCK  4
C          DOUBLE PRECISION COEF,S,EN,EMLN,HO,DELN  ROCK  5
C          LOGICAL HP,SP,TP,THI,FROZ,EQL,AREA,SEQL,CALCH  ROCK  6
C          COMMON /POINTS/HSUM(13),SSUM(13),CPR(13),DLVTP(13),DLVPT(13),  ROCK  7
C          1 GAMMAS(13),P(26),T(52),V(13),PPP(13),WP(13),SONVEL(13),TTT(13),  ROCK  8
C          2 VLM(13),TCTN(13)                   ROCK  9
C          COMMON /SPECES/COEF(2,7,100),S(100),HO(100),DELN(100),DUMMY(100),  ROCK 10
C          1 EN(100,13),FNLN(100),A(10,100),SUB(100,3),IUSE(100),TEMP(50,2)  ROCK 11
C          COMMON /MISC/ENN,SUMN,TT,SO,ATOM(3,101),LLMT(10),BC(10),BOP(10,2),  ROCK 12
C          1 TM,TLOW,TMID,THIGH,PP,CPSUM,OF,EQRAT,FPCT,R,RR,HSUBO,AM(2),  ROCK 13
C          2 HPP(2),RH(2),VMIN(2),VPLS(2),WP(2),DATA(22),NAME(15,5),  ROCK 14
C          3 ANUM(15,5),PECWT(15),ENTH(15),FAZ(15),RTEMP(15),FOX(15),DENS(15),  ROCK 15
C          4 RHOP,RMW(15),TLN,CR,DXF(15),ENNL,TRACE,LLMTS(10),SBOP(10,2)  ROCK 16
C          COMMON /INCX/IDEBUG,CONVG,TP,HP,SP,ISV,NPP,MOLES,NP,NT,NPT,NLM,  ROCK 17
C          1 NS,KMAT,IMAT,IQ1,IOF,NOF,NOMIT,IP,NEWR,NSUB,NSUP,RKT,DETN,SHOCK,  ROCK 18
C          2 IONS,NC,NSERT,JSOL,JLIQ,KASE,NREAC,IC,JS1,VOL,IT,CALCH,NLS,LOGV,  ROCK 19
C          3 ISUP,ISUB,ITNUM,ITM,INCOFZ,INCDEQ,CPRF,IPP,SEQL,PCPLT  ROCK 20
C          COMMON /PERF/PCP(22),VMOC(13),SPIM(13),VACI(13),SUPAR(13),  ROCK 21
C          1 SUPAR(13),APP(13),AEAT(13),CSTR,EQL,FROZ,SSO,AREA,AWT,NFZ,  ROCK 22
C          2 APPL,ARATIO,ELN  ROCK 23
C          ROCK 24
C          ROCK 25
C          ROCK 26
C          ROCK 27
C          ROCK 28
C          ROCK 29
C          ROCK 30
C          ROCK 31
C          ROCK 32
C          ROCK 33
C          ROCK 34
C          ROCK 35
C          ROCK 36
C          ROCK 37
C          ROCK 38
C          ROCK 39
C          ROCK 40
C          ROCK 41
C          ROCK 42
C          ROCK 43
C          ROCK 44
C          ROCK 45
C          ROCK 46
C          ROCK 47
C          ROCK 48
C          ROCK 49
C          ROCK 50
C          ROCK 51
C          ROCK 52
C          ROCK 53

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DO 320 I=1,13	ROCK 54
IF(SUBAR(I).NE.0.) NSUB=NSUB+1	ROCK 55
IF(SUPAR(I).NE.0.) NSUP=NSUP+1	ROCK 56
320 CCNTINUE	ROCK 57
WRITE (6,RKTINP)	ROCK 58
SEQL = EGL	ROCK 59
IOF = 0	ROCK 60
TT = 3800.	ROCK 61
C	ROCK 62
C LOOP FOR EACH O/F	ROCK 63
C	ROCK 64
321 IT = 1	ROCK 65
IOF = IOF + 1	ROCK 66
OF = OXF(IOF)	ROCK 67
CALL NEWOF	ROCK 68
IF(CALCH.AND.TT.EQ.0.) RETURN 1	ROCK 69
IF(T(1).EQ.0.) GO TO 322	ROCK 70
TT = T(1)	ROCK 71
C	ROCK 72
C LOOP FOR CHAMBER PRESSURES	ROCK 73
C	ROCK 74
322 IP = 0	ROCK 75
998 IP = IP + 1	ROCK 76
ITNUM = 0	ROCK 77
AREA = .FALSE.	ROCK 78
IF(T(1).EQ.0.) HP=.TRUE.	ROCK 79
IF(T(1).NE.0.) TP=.TRUE.	ROCK 80
SP = .FALSE.	ROCK 81
EQL = .TRUE.	ROCK 82
ISUB = 1	ROCK 83
ISUP = 1	ROCK 84
PP = P(IP)	ROCK 85
IPP = 1	ROCK 86
ITROT = 3	ROCK 87
ISUPSV = 1	ROCK 88
C	ROCK 89
C LOOP FOR PRESSURE RATIOS	ROCK 90
C	ROCK 91
331 IF(EQL) GO TO 332	ROCK 92
CALL FROZEN	ROCK 93
GO TO 1332	ROCK 94
332 CALL EQLERM	ROCK 95
IF(NPT.NE.NFZ) GO TO 1332	ROCK 96
CPRF = CPSUM	ROCK 97
IF(NFZ.NE.2) EQL = SEQL	ROCK 98
C	ROCK 99
C TT = 0 IF NO CONVERGENCE	ROCK 100
C	ROCK 101
1332 IF(TT.NE.0.) GO TO 333	ROCK 102
IF(NPT.LT.1) GO TO 1000	ROCK 103
GO TO 900	ROCK 104
333 IF(IPP.GT.1) GO TO 195	ROCK 105
C	ROCK 106
C COMBUSTION CHAMBER	ROCK 107
C	ROCK 108
TP = .FALSE.	ROCK 109
HP = .FALSE.	ROCK 110
SP = .TRUE.	ROCK 111
SO = SSUM(1)	ROCK 112
334 TMELT=0.	ROCK 113
ITROT= 3	ROCK 114
THI = .FALSE.	ROCK 115
APP(2)=((GAMMAS(1)+1.)/2.)*(GAMMAS(1)/(GAMMAS(1)-1.))	ROCK 116
PP = PPP(1)/APP(2)	ROCK 117
TT = 2.*TT/(GAMMAS(1)+1.)	ROCK 118



	ISV = 1	ROCK 119
	GO TO 87C	ROCK 120
195	USQ = 2.*(HSUM(1)-HSUM(NPT)) * RR	ROCK 121
	IF (IPP.CT.2) GO TO 900	ROCK 122
C		ROCK 123
C	THROAT	ROCK 124
C		ROCK 125
190	IF(.NOT.THI) GO TO 191	ROCK 126
	GAMMAS(2) = 0.	ROCK 127
	GO TO 899	ROCK 128
191	ASQ = GAMMAS(2)*TT*ENN*RR	ROCK 129
	IF(EQL) WRITE(6,194) APP(2),TT	ROCK 130
194	FORMAT (7H PC/PT= , F9.6, 6H T = , F9.2)	ROCK 131
	IF(IDEBUG.EQ.1.OR.IDEBUG.EQ.2) WRITE(6,923)USQ,ASC	ROCK 132
923	FORMAT(5HOURS=,E15.8,5X,4HASQ=,E15.8)	ROCK 133
	DH = (USQ-ASQ)/ASQ	ROCK 134
	IF(DH.LT.0.) DH=-DH	ROCK 135
	IF(DH.LE.0.4E-4.OR.ITROT.EQ.0) GO TO 899	ROCK 136
	IF(JSOL.NE.0) GO TO 925	ROCK 137
	IF(TMELT.EQ.0.) GO TO 192	ROCK 138
	DLT = ALOG(TMELT/TT)	ROCK 139
	DD = DLT*CPR(2)/(ENN*DLVTP(2))	ROCK 140
	PP = EXP(DD)	ROCK 141
	APP(2) = P(IP)/PP	ROCK 142
	THI = .TRUE.	ROCK 143
	GO TO 331	ROCK 144
925	TMELT = TT	ROCK 145
192	APP(2) = APP(2)/(1.+(USQ-ASQ)/(ENN*TT*RR*(GAMMAS(2)+1.)))	ROCK 146
193	PP = P(IP)/APP(2)	ROCK 147
	ITROT = ITROT-1	ROCK 148
	GO TO 331	ROCK 149
899	AWT = ENN*TT/(PP*USQ**.5)	ROCK 150
	PCPLT = ALCG(APP(2))	ROCK 151
	IF(NFZ.EC.2) EQL = SEQL	ROCK 152
900	ISV = C	ROCK 153
	AEAT(NPT) = ENN*TTT(NPT)/(PP*USQ**.5*AWT)	ROCK 154
	IF(TT.EQ.0.) GO TO 860	ROCK 155
	IF(AREA) GO TO 800	ROCK 156
	IF(IPP.LT.NPP) GO TO 859	ROCK 157
788	IF(NSUB.LE.0.AND.NSUP.EQ.0) GO TO 860	ROCK 158
	AREA = .TRUE.	ROCK 159
C		ROCK 160
C	PCP ESTIMATES FOR AREA RATIOS	ROCK 161
C		ROCK 162
800	IF(ITNUM.NE.0) GO TO 810	ROCK 163
	DLNP = 1.	ROCK 164
	ITNUM = 1	ROCK 165
	ARATIO = SUBAR(ISUB)	ROCK 166
	IF(NSUB.LE.0) ARATIO=SUPAR(ISUP)	ROCK 167
	IF(EQL.OR.NFZ.LT.3) GO TO 798	ROCK 168
	IF(ARATIO.GT.AEAT(NFZ)) GO TO 798	ROCK 169
	WRITE(6,884)	ROCK 170
	GO TO 834	ROCK 171
798	ELN = ALCG(ARATIO)	ROCK 172
	IF(NSUB.LE.0) GO TO 799	ROCK 173
	APPL = PCPLT/(SUBAR(ISUB)+(10.587*ELN**2+9.454)*ELN)	ROCK 174
	IF(ARATIO.LT.1.09) APPL=.9*APPL	ROCK 175
	IF(ARATIO.GT.10.) APPL=APPL/ARATIO	ROCK 176
	GO TO 859	ROCK 177
799	IF(NFZ.EQ.IPP) ISUPSV = ISUP	ROCK 178
	IF(SUPAR(ISUP).LT.2.) GO TO 805	ROCK 179
	IF(ISUP.GT.1.AND.SUPAR(ISUP-1).GE.2.) GO TO 802	ROCK 180
	APPL = GAMMAS(2)+ELN*1.4	ROCK 181
	GO TO 859	ROCK 182
805	APPL = SQRT(ELN*(1.535+3.294*ELN))+PCPLT	ROCK 183
	GO TO 859	ROCK 184



C		ROCK 185
C	TEST FOR CONVERGENCE ON AREA RATIO.	ROCK 186
C		ROCK 187
	810 CHECK = .00004	ROCK 188
	IF(IDEBUG.LE.0.OR.NPT.LT.IDEBUG) GO TO 809	ROCK 189
	WRITE(6,1811)ITNUM,ARATIO,AEAT(NPT),APP(NPT),DLNP	ROCK 190
1811	FORMAT (6H0ITER=,I2,5X,15HASSIGNED AE/AT=,F15.8,5X,6HAE/AT=,F15.8,	ROCK 191
	15X,5HPC/F=,F15.8,5X,13HDELTA LN PCP=,F15.8)	ROCK 192
809	IF(ABS(AEAT(NPT)- ARATIO) /ARATIO .LE.CHECK) GO TO 830	ROCK 193
	DELTAE = (AEAT(NPT)-ARATIO)/ARATIO	ROCK 194
	IF(ABS(DLNP).LT..00004) GO TO 830	ROCK 195
	AEATL= ALOG(AEAT(NPT))	ROCK 196
811	ITNUM = ITNUM+1	ROCK 197
	IF(ITNUM.GT.10) GO TO 840	ROCK 198
C		ROCK 199
C	IMPROVED PCP ESTIMATES	ROCK 200
C		ROCK 201
	ASQ = GAMMAS(NPT)*ENN*RR*TT	ROCK 202
	DLNPE = GAMMAS(NPT)*USQ/(USQ-ASQ)	ROCK 203
802	DLNP = DLNPE*ELN-DLNPE*AEATL	ROCK 204
	APPL = APPL+DLNP	ROCK 205
	IF(ITNUM.EQ.1) GO TO 859	ROCK 206
	APP(NPT) = EXP(APPL)	ROCK 207
	PP = P(IF)/APP(NPT)	ROCK 208
	GO TO 331	ROCK 209
C		ROCK 210
830	ITNUM = 0	ROCK 211
	AEAT(NPT) = ARATIO	ROCK 212
	IF(NSUB.LE.0) GO TO 834	ROCK 213
	ISUB = ISUB+1	ROCK 214
	IF(ISUB.LE.NSUB) GO TO 800	ROCK 215
	ISUB = 1	ROCK 216
	NSUB = -NSUB	ROCK 217
	IF(ISUP.LE.NSUP) GO TO 800	ROCK 218
	GO TO 835	ROCK 219
834	ISUP = ISUP+1	ROCK 220
	ITNUM = C	ROCK 221
	IF(ISUP.LE.NSUP) GO TO 800	ROCK 222
	ISUP = ISUPSV	ROCK 223
835	AREA = .FALSE.	ROCK 224
	GO TO 860	ROCK 225
840	WRITE(6,841) ARATIO	ROCK 226
841	FORMAT(34HODID NOT CONVERGE FOR AREA RATIO =,F10.5)	ROCK 227
	GO TO 830	ROCK 228
C		ROCK 229
C	TEST FOR OUTPUT -- END OF PCP,SUBAR,AND SUPAR SCHEDULES OR NPT=13.	ROCK 230
C		ROCK 231
859	ISV = NPT	ROCK 232
	IF(NPT.NE.13) GO TO 870	ROCK 233
860	IF(EQL) GO TO 861	ROCK 234
	IF(NFZ.GT.1) GO TO 861	ROCK 235
	CPR(NFZ) = CPRF	ROCK 236
	GAMMAS(NFZ) = CPRF/(CPRF-1./WM(NFZ))	ROCK 237
C		ROCK 238
861	CALL RKTOUT	ROCK 239
C		ROCK 240
C	IF (TT.EQ.0.) ISV = 0	ROCK 241
C		ROCK 242
C	RETURN	ROCK 243
C		ROCK 244
C	ENTRY ROCKT1	ROCK 245
C		ROCK 246
	DLNP = 1.	ROCK 247
	IF(.NOT.EQL.AND.TT.EQ.0.) WRITE(6,862)	ROCK 248



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862 FORMAT(105H0CALCULATIONS WERE STOPPED BECAUSE NEXT POINT IS MORE TROCK 249
      1HAN 50 DEG BELOW TEMP RANGE OF A CONDENSED SPECIES) ROCK 250
      IF (ISV.EQ.0) GO TO 990 ROCK 251
      IF (IDEBUG.GT.13) IDEBUG = IDEBUG-13 ROCK 252
      IF (EQL) WRITE(6,865) ROCK 253
865 FORMAT(1H1) ROCK 254
      NPT = 2 ROCK 255
C ROCK 256
C SET INDICES AND ESTIMATES FOR NEXT POINT. ROCK 257
C ROCK 258
870 NPT = NPT + 1 ROCK 259
      IF (.NOT.EQL.AND.(ISV.NE.1.OR.SEQL)) GO TO 880 ROCK 260
      IF (ISV.EQ.1) ISV = -1 ROCK 261
      CALL SAVE ROCK 262
880 IPP = IPP+1 ROCK 263
      IF (NPT.EC.2) GO TO 331 ROCK 264
      IF (AREA) GO TO 885 ROCK 265
      APP(NPT) = PCP(IPP-2) ROCK 266
      IF (EQL) GO TO 886 ROCK 267
      IF (APP(NPT).GE.APP(NFZ)) GO TO 886 ROCK 268
      WRITE(6,884) ROCK 269
884 FORMAT(//,1X,114HSUPERSONIC PRESSURE RATIOS MUST BE IN ASCENDING OROCK 270
      1RDER POINTS OUT OF ORDER WERE OMITTED FROM FROZEN CALCULATIONS) ROCK 271
      GO TO 880 ROCK 272
885 APP(NPT) = EXP(APPL) ROCK 273
886 PP = P(IP)/APP(NPT) ROCK 274
      GO TO 331 ROCK 275
C ROCK 276
C END OF PCP, SUBAR, AND SUPAR SCHEDULES. ROCK 277
C ROCK 278
990 IF (NSUB.LT.0) NSUB=-NSUB ROCK 279
      IF (.NOT.FROZ.OR..NOT.EQL) GO TO 997 ROCK 280
C ROCK 281
C SET UP FOR FROZEN. ROCK 282
C ROCK 283
      EQL = .FALSE. ROCK 284
      CALL SAVE ROCK 285
      IT = TTT(NFZ) ROCK 286
      IPP = NFZ ROCK 287
      IF (NFZ.EC.NPT) GO TO 860 ROCK 288
      NPT = NFZ ROCK 289
      ENN = 1./WM(NFZ) ROCK 290
      IF (NFZ.EC.1) GO TO 334 ROCK 291
      NSUB = -NSUB ROCK 292
      IF (APP(NFZ).GE.APP(2)) GO TO 994 ROCK 293
      WRITE(6,993) ROCK 294
993 FORMAT (//,28X,77HFREEZING IS NOT ALLOWED AT A SUBSONIC POINT, FROROCK 295
      IZEN CALCULATIONS WERE OMITTED) ROCK 296
      GO TO 997 ROCK 297
994 IF (NFZ.LT.NPP) GO TO 870 ROCK 298
      GO TO 78E ROCK 299
997 NPT = 1 ROCK 300
C ROCK 301
C ARE THERE MORE ASSIGNED, ROCK 302
C 1) CHAMBER PRESSURES(IP = NP) ROCK 303
C 2) CHAMBER TEMPERATURES(IT = NT) ROCK 304
C 3) O/F VALUES(IOF = NOF) ROCK 305
C ROCK 306
      IF (IP.EQ.NP.AND.IT.EQ.NT.AND.IOF.EQ.NOF) GO TO 1000 ROCK 307
      WRITE(6,865) ROCK 308
      IF (SEQL) CALL SAVE ROCK 309
      IT = TTT(1) ROCK 310
      IF (IP.LT.NP) GO TO 998 ROCK 311
      IF (IT.GE.NT) GO TO 999 ROCK 312
      IT = IT+1 ROCK 313

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TT = T(IT)
GO TO 322
999 IF (IOF.GE.NOF) GO TO 1000
GO TO 321
1000 RETURN 1
END

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ROCK 314
ROCK 315
ROCK 316
ROCK 317
ROCK 318
ROCK 319

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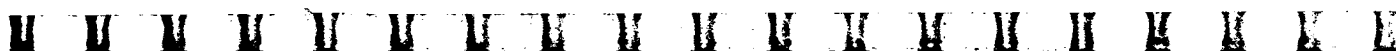
C
C SUBROUTINE RKTOUT ROUT 1
C
C ROCKET PERFORMANCE PARAMETERS ROUT 2
C ROUT 3
C THE FOLLOWING DOUBLE PRECISION TYPE STATEMENTS ARE REQUIRED FOR ROUT 4
C IBM 360 MACHINES ONLY ROUT 5
C ROUT 6
C ROUT 7
C DOUBLE PRECISION HSUM,SSUM,CPR,DLVTP,DLVPT,GAMMAS ROUT 8
C DOUBLE PRECISION COEF,S,EN,ENLN,HO,DELN ROUT 9
C ROUT 10
C LOGICAL EQL,FROZ,TP,HP,SP,SHOCK,AREA ROUT 11
C ROUT 12
C DIMENSION NV(13),Z(10,4) ROUT 13
C ROUT 14
C COMMON /FOINTS/HSUM(13),SSUM(13),CPR(13),DLVTP(13),DLVPT(13), ROUT 15
1 GAMMAS(13),P(26),T(52),V(13),PPP(13),WM(13),SONVEL(13),TTT(13), ROUT 16
2 VLM(13),TOTN(13) ROUT 17
COMMON /SPECES/COEF(2,7,100),S(100),HO(100),DELN(100),DUMMY(100), ROUT 18
1 EN(100,13),ENLN(100),A(10,100),SUB(100,3),IUSE(100),TEMP(50,2) ROUT 19
COMMON /MISC/ENN,SUMN,TT,SO,ATOM(3,101),LLMT(10),BO(10),BOP(10,2), ROUT 20
1 TM,TLOW,TMID,THIGH,PP,CPSUM,OF,EQRAT,FPCT,R,RR,HSUBO,AM(2), ROUT 21
2 HPP(2),RH(2),VMIN(2),VPLS(2),WP(2),DATA(22),NAME(15,5), ROUT 22
3 ANUM(15,5),PECWT(15),ENTH(15),FAZ(15),RTEMP(15),FCX(15),DENS(15), ROUT 23
4 RHOP,RMW(15),TLN,CR,OXF(15),ENNL,TRACE,LLMTS(10),SBOP(10,2) ROUT 24
COMMON /INDX/IDEBUG,CONVG,TP,HP,SP,ISV,NPP,MOLES,NP,NT,NPT,NLM, ROUT 25
1 NS,KMAT,IMAT,IQ1,IOF,NOF,NOMIT,IP,NEWR,NSUB,NSUP,RKT,DETN,SHOCK, ROUT 26
2 IONS,NC,NSERT,JSOL,JLIQ,KASE,NREAC,IC,JS1,VOL,IT,CALCH,NLS,LOGV, ROUT 27
3 ISUP,ISLB,ITNUM,ITM,INCDFZ,INCDEQ,CPRF,IPP,SEQ,PCPLT ROUT 28
COMMON /PERF/PCP(22),VMOC(13),SPIM(13),VACI(13),SUBAR(13), ROUT 29
1 SUPAR(12),APP(13),AEAT(13),CSTR,EQL,FROZ,SSO,AREA,AWT,NFZ, ROUT 30
2 APPL,ARATIO,ELN ROUT 31
COMMON /DUPT/FMT(30),FP(4),FT(4),FH(4),FS(4),FM(4),FV(4),FD(4), ROUT 32
1 FC(4),FG(4),FB,FMT13,F1,F2,F3,F4,F5,FL(4),FMTI9,FA1,FA2, ROUT 33
2 FR1,FC1,FN(4),FR(4),FA(4),FI(4),FMT9X,F0 ROUT 34
C ROUT 35
C EQUIVALENCE (V,NV),(Z,HO) ROUT 36
C ROUT 37
C DATA EXIT/4HEXIT/ ROUT 38
C ROUT 39
C IF(.NOT.EQL) GO TO 636 ROUT 40
WRITE(6,37) ROUT 41
37 FORMAT(1H1/24X,84HTHEORETICAL ROCKET PERFORMANCE ASSUMING EQUILIBR ROUT 42
1IUM COMPOSITION DURING EXPANSION ROUT 43
GO TO 39 ROUT 44
636 WRITE(6,38) ROUT 45
38 FORMAT(1H1,26X,78HTHEORETICAL ROCKET PERFORMANCE ASSUMING FROZEN CROUT 46
1OMPOSITION DURING EXPANSION ROUT 47
IF(NFZ.GT.1) WRITE(6,637)NFZ ROUT 48
637 FORMAT(5EX,11HAFTER POINT,I2) ROUT 49
39 IF(TTT(1).EQ.T(IT)) WRITE(6,737) ROUT 50

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737	FORMAT (52X,28H) AT AN ASSIGNED TEMPERATURE	ROUT	51
	TEM = PPP(1)*14.696006	ROUT	52
	WRITE (6,40) TEM	ROUT	53
40	FORMAT(5H)OPC = ,F8.1,5H PSIA)	ROUT	54
	CALL OUT1	ROUT	55
	NEX = NPT - 2	ROUT	56
	DO 862 I = 1,NEX	ROUT	57
862	V(I) = EXIT	ROUT	58
	WRITE(6,48) (V(I),I=1,NEX)	ROUT	59
48	FORMAT(1H0,16X,16H)CHAMBER THROAT ,11(5X,A4))	ROUT	60
C		ROUT	61
C	PRESSURE RATIOS	ROUT	62
C		ROUT	63
	FMT(4) = FMT(6)	ROUT	64
	CALL VARFMT (APP,NPT)	ROUT	65
	WRITE (6,FMT) FR1,FB,FB,FB,(APP(J),J=1,NPT)	ROUT	66
	CALL OUT2	ROUT	67
C		ROUT	68
	AGV = 9.80665	ROUT	69
	DO 202 K=2,NPT	ROUT	70
	SPIM(K) = (2.*RR*(HSUM(1)-HSUM(K))**.5/AGV	ROUT	71
C		ROUT	72
C	AW (A/W) IN UNITS OF SEC/ATM	ROUT	73
C		ROUT	74
	AW = RR*TTT(K)/(PPP(K)*WM(K)*SPIM(K)*AGV**2)	ROUT	75
	IF(K.NE.2)GO TO 200	ROUT	76
	CSTR = 32.174*PPP(1)*AW	ROUT	77
	AEAT(2) = 1.	ROUT	78
200	VACI(K)=SPIM(K)+PPP(K)*AW	ROUT	79
	IF (SONVEL(K).NE.0.) VMOC(K)=SPIM(K)*AGV/SONVEL(K)	ROUT	80
	NV(K)= CSTR + .5	ROUT	81
202	CONTINUE	ROUT	82
C		ROUT	83
C	MACH NUMBER	ROUT	84
C		ROUT	85
	VMOC(1)=0.	ROUT	86
	IF(GAMMAS(2).EQ.0.) VMOC(2)=0.	ROUT	87
	FMT(7) = F3	ROUT	88
	WRITE(6,FMT) (FN(I),I=1,4),(VMOC(J),J=1,NPT)	ROUT	89
	WRITE (6,208)	ROUT	90
208	FORMAT (1H)	ROUT	91
C		ROUT	92
C	AREA RATIO	ROUT	93
C		ROUT	94
	FMT(4) = FMT9X	ROUT	95
	CALL VARFMT (AEAT,NPT)	ROUT	96
	FMT(5) = FB	ROUT	97
	WRITE(6,FMT) FA1,FA2,FB,FB,(AEAT(J),J=2,NPT)	ROUT	98
C		ROUT	99
C	C*	ROUT	100
C		ROUT	101
	FMT(5) = FMT13	ROUT	102
	FMT(6) = FMTI9	ROUT	103
	FMT(7) = FB	ROUT	104
	WRITE(6,FMT) (FR(I),I=1,4),(NV(J),J=2,NPT)	ROUT	105
C		ROUT	106
C	CF - THRUST COEFFICIENT	ROUT	107
C		ROUT	108
	FMT(6) = FMT(8)	ROUT	109
	FMT(7) = F3	ROUT	110
	DO 212 I=2,NPT	ROUT	111
212	V(I)=32.174*SPIM(I)/CSTR	ROUT	112
	WRITE(6,FMT) FC1,FB,FB,FB,(V(J),J=2,NPT)	ROUT	113
C		ROUT	114
C	VACUUM IMPULSE	ROUT	115

C	FMT(5) = FMT13	ROUT 116
	FMT(7) = F1	ROUT 117
	WRITE(6,FMT) (FA(I),I=1,4),(VACI(J),J=2,NPT)	ROUT 118
C		ROUT 119
C	SPECIFIC IMPULSE	ROUT 120
C		ROUT 121
C	WRITE(6,FMT) (FI(I),I=1,4),(SPIM(J),J=2,NPT)	ROUT 122
	WRITE(6,208)	ROUT 123
	FMT(4) = FB	ROUT 124
	FMT(5) = FMT13	ROUT 125
	FMT(7) = F5	ROUT 126
	IF(EQL) GO TO 312	ROUT 127
	WRITE(6,310)	ROUT 128
310	FORMAT(15HOMOLE FRACTIONS //)	ROUT 129
C		ROUT 130
C	MOLE FRACTIONS - FROZEN	ROUT 131
C		ROUT 132
C		ROUT 133
	TRA = 5.E-6	ROUT 134
	IF(TRACE.NE.0.) TRA=TRACE	ROUT 135
	LINE = 0	ROUT 136
	DC 430 K =1,NS	ROUT 137
	V(LINE+1) = EN(K,NFZ)/TOTN(NFZ)	ROUT 138
	IF(V(LINE+1).LT.TRA) GO TO 424	ROUT 139
	LINE = LINE+1	ROUT 140
	Z(LINE,1) = SUB(K,1)	ROUT 141
	Z(LINE,2) = SUB(K,2)	ROUT 142
	Z(LINE,3) = SUB(K,3)	ROUT 143
	Z(LINE,4) = V(LINE)	ROUT 144
424	IF (LINE.NE.4.AND.K.NE.NS) GO TO 430	ROUT 145
	IF (LINE.EQ.0) GO TO 312	ROUT 146
	WRITE(6,426) (Z(LN,1),Z(LN,2),Z(LN,3),Z(LN,4),LN=1,LINE)	ROUT 147
426	FORMAT (1H ,4(3A4,F9.5,7X))	ROUT 148
	LINE = 0	ROUT 149
430	CONTINUE	ROUT 150
312	CALL OUT3	ROUT 151
1000	RETURN	ROUT 152
	ENC	ROUT 153

C	SUBROUTINE FROZEN	FROZ 1
C		FROZ 2
C	(FROZEN COMPOSITION EXPANSION ONLY)	FROZ 3
C		FROZ 4
C	THE FOLLOWING DOUBLE PRECISION TYPE STATEMENTS ARE REQUIRED FOR	FROZ 5
C	IBM 360 MACHINES ONLY	FROZ 6
C		FROZ 7
C	DOUBLE PRECISION HSUM,SSUM,CPR,DLVTP,DLVPT,GAMMAS	FROZ 8
C	DOUBLE PRECISION COEF,S,EN,ENLN,H0,DELN	FROZ 9
C	DOUBLE PRECISION SUMS,SUMH,SS	FROZ 10
C		FROZ 11
C	LOGICAL EQL,FROZ,CONVG,SP,HP,VOL	FROZ 12
C		FROZ 13
	COMMON /POINTS/HSUM(13),SSUM(13),CPR(13),DLVTP(13),DLVPT(13),	FROZ 14
	1 GAMMAS(13),P(26),T(52),V(13),PPP(13),WM(13),SONVEL(13),TTT(13),	FROZ 15
	2 VLM(13),TOTN(13)	FROZ 16
	COMMON /SPECES/COEF(2,7,00),S(100),H0(100),DELN(100),DUMMY(100).	FROZ 17
	1 EN(100,13),ENLN(100),A(0,100),SUB(100,3),IUSE(100),TEMP(50,2)	FROZ 18



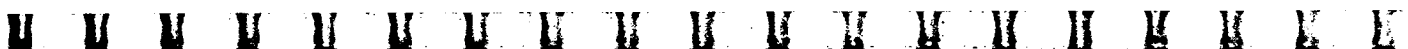
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COMMON /MISC/ENN,SUMN,TT,SO,ATOM(3,101),LLMT(10),BO(10),BOP(10,2),FROZ 19
1 TM,TLOW,TMID,THIGH,PP,CPSUM,OF,EQRAT,FPCT,R,RR,HSUBO,AM(2), FROZ 20
2 HPP(2),RH(2),VMIN(2),VPLS(2),WP(2),DATA(22),NAME(15,5), FROZ 21
3 ANUM(15,5),PECWT(15),ENTH(15),FAZ(15),RTEMP(15),FOX(15),DENS(15),FROZ 22
4 RHOP,RMW(15),TLN,CR,OXF(15),ENNL,TRACE,LLMTS(10),SBOP(10,2) FROZ 23
COMMON /INDX/IDEBUG,CONVG,TP,HP,SP,ISV,NPP,MOLES,NP,NT,NPT,NLM, FROZ 24
1 NS,KMAT,IMAT,IQ1,IQF,NOF,NOMIT,IP,NEWNR,NSUB,NSUP,RKT,DETN,SHOCK, FROZ 25
2 ICNS,NC,NSERT,JSOL,JLIQ,KASE,NREAC,IC,JS1,VOL,IT,CALCH,NLS,LOGV, FROZ 26
3 ISUP,ISUB,ITNUM,ITM,INCDFZ,INCDEQ,CPRF,IPP,SEQ,PCPLT FROZ 27
COMMON /PERF/PCP(22),VMOC(13),SPIM(13),VACI(13),SUBAR(13), FROZ 28
1 SUPAR(13),APP(13),AEAT(13),CSTR,EQL,FROZ,SSO,AREA,AWT,NFZ, FROZ 29
2 APPL,ARATIO,ELN FROZ 30
COMMON /DUPT/FMT(30),FP(4),FT(4),FH(4),FS(4),FM(4),FV(4),FD(4), FROZ 31
1 FC(4),FG(4),FB,FMT13,F1,F2,F3,F4,F5,FL(4),FMTI9,FA1,FA2, FROZ 32
2 FR1,FC1,FN(4),FR(4),FA(4),FI(4),FMT9X,F0 FROZ 33
C
CONVG = .FALSE. FROZ 35
TLN = ALOG(TT) FROZ 36
DO 51 ITER=1,8 FROZ 37
SUMS = 0. FROZ 38
SUMH = 0. FROZ 39
JS1 = ITM FROZ 40
NNN = NPT FROZ 41
NPT = NFZ FROZ 42
CALL CPHS FROZ 43
CC = CPSUM FROZ 44
55 NPT = NNN FROZ 45
DO 60 J=ITM,NS FROZ 46
IF (EN(J,NFZ).EQ.0.) GO TO 60 FROZ 47
PMN = PP*WM(NFZ)*EN(J,NFZ) FROZ 48
SS = S(J) FROZ 49
IF(IUSE(J).EQ.0) SS=SS-ALOG(PMN) FROZ 50
SUMS = SUMS+SS*EN(J,NFZ) FROZ 51
IF (CONVG) SUMH=SUMH+HO(J)*EN(J,NFZ) FROZ 52
60 CONTINUE FROZ 53
IF (CONVG) GO TO 81 FROZ 54
DLNT=(SUMS-SO)/CC FROZ 55
TLN=TLN-DLNT FROZ 56
IF(DLNT.LT.0.) DLNT=-DLNT FROZ 57
IF(DLNT.LT.0.5E-4) CONVG=.TRUE. FROZ 58
TT = EXP(TLN) FROZ 59
51 CONTINUE FROZ 60
WRITE(6,70) FROZ 61
70 FORMAT(40H0FROZEN DID NOT CONVERGE IN 8 ITERATIONS) FROZ 62
GO TO 903 FROZ 63
81 TTT(NPT)= TT FROZ 64
SSUM(NPT)= SUMS FROZ 65
HSUM(NPT)= TT*SUMH FROZ 66
GAMMAS(NPT)= CPSUM/(CPSUM-1./WM(NFZ)) FROZ 67
VLM(NPT) = RR*TT/(WM(NFZ)*101.325*PP) FROZ 68
WM(NPT) = WM(NFZ) FROZ 69
C
DLVPT(NPT) = -1. FROZ 71
DLVTP(NPT) = 1. FROZ 72
TOTN(NPT) = TOTN(NFZ) FROZ 73
PPP(NPT) = PP FROZ 74
CPR(NPT) = CPSUM FROZ 75
IF (TT.LT.(TLOW-150.))GO TO 903 FROZ 76
IF(NC.EQ.0) GO TO 1000 FROZ 77
INC = 0 FROZ 78
DO 901 I=ITM,NS FROZ 79
IF(IUSE(I).EQ.0.OR.IUSE(I).EQ.-10000) GO TO 901 FROZ 80
INC = INC+1 FROZ 81
IF (EN(I,NFZ).EQ.0.) GO TO 901 FROZ 82
IF(TT.LT.(TEMP(INC,1)-50.).OR.TT.GT.(TEMP(INC,2)+50.))GO TO 903 FROZ 83

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901	CONTINUE	FROZ	84
	GO TO 1000	FROZ	85
903	TT=0.	FROZ	86
	NPT= NPT-1	FROZ	87
1000	RETURN	FROZ	88
	END	FROZ	89

C	SUBROUTINE SHCK (*)	SHCK	1
C		SHCK	2
	DOUBLE PRECISION G,X,GG	SHCK	3
C		SHCK	4
C	THE FOLLOWING DOUBLE PRECISION TYPE STATEMENTS ARE REQUIRED FOR	SHCK	5
C	IBM 360 MACHINES ONLY	SHCK	6
C		SHCK	7
C	DOUBLE PRECISION HSUM,SSUM,CPR,DLVTP,DLVPT,GAMMAS	SHCK	8
C	DOUBLE PRECISION COEF,S,EN,ENLN,HO,DELN	SHCK	9
C		SHCK	10
	REAL MACH1,M1,MACH2,M2,M12,M5,M25,MACHO ,MU12RT,M2M1	SHCK	11
	LOGICAL INCDEQ,INCDFZ,REFLEQ,REFLFZ,TP,FROZ,EQL,SECL,MOLES,	SHCK	12
	1 SHOCK,SREFL,REFL,CALCH	SHCK	13
C		SHCK	14
	DIMENSION NUM(15,5),FV2(4),FLV(4),W(10)	SHCK	15
	DIMENSION M2M1(13),T2T1(13),U1U2(13),RRHO(13),SG(78),U5(13)	SHCK	16
	DIMENSION U1(13),MACH1(13),UTWO(13),Z(10,3),U2STAR(13)	SHCK	17
C		SHCK	18
	COMMON /POINTS/HSUM(13),SSUM(13),CPR(13),DLVTP(13),DLVPT(13),	SHCK	19
	1 GAMMAS(13),P(26),T(52),V(13),PPP(13),WM(13),SONVEL(13),TTT(13),	SHCK	20
	2 VLM(13),TOTN(13)	SHCK	21
	COMMON /SPECES/COEF(2,7,100),S(100),HO(100),DELN(100),DUMMY(100),	SHCK	22
	1 EN(100,13),ENLN(100),A(10,100),SUB(100,3),IUSE(100),TEMP(50,2)	SHCK	23
	COMMON /MISC/ENN,SUMN,TT,SO,ATOM(3,101),LLMT(10),RO(10),BOP(10,2),	SHCK	24
	1 TM,TLOW,TMID,THIGH,PP,CPSUM,OF,EQRAT,FPCT,R,RR,HSUBO,AM(2),	SHCK	25
	2 HPP(2),RH(2),VMIN(2),VPLS(2),WP(2),DATA(22),NAME(15,5),	SHCK	26
	3 ANUM(15,5),PECWT(15),ENTH(15),FAZ(15),RTEMP(15),FOX(15),DENS(15),	SHCK	27
	4 RHOP,RMW(15),TLN,CR,DXF(15),ENNL,TRACE,LLMTS(10),SBOP(10,2)	SHCK	28
	COMMON /DOUBLE/ G(20,21),X(20)	SHCK	29
	COMMON /INDX/IDEBUG,CONVG,TP,HP,SP,ISV,NPP,MOLES,NP,NT,NPT,NLM,	SHCK	30
	1 NS,KMAT,IMAT,IQ1,IOF,NOF,NOMIT,IP,NEWR,NSUB,NSUP,RKT,DETN,SHOCK,	SHCK	31
	2 IONS,NC,NSERT,JSOL,JLIQ,KASE,NREAC,IC,JS1,VOL,IT,CALCH,NLS,LOGV,	SHCK	32
	3 ISUP,ISUB,ITNUM,ITM,INCDFZ,INCDEQ,CPRF,IPP,SEQ,PCPLT	SHCK	33
	COMMON /PERF/PCP(22),VMOC(13),SPIM(13),VACI(13),SUBAR(13);	SHCK	34
	1 SUPAR(13),APP(13),AEAT(13),CSTR,EQL,FROZ,SSO,AREA,AWT,NFZ,	SHCK	35
	2 APPL,ARATIO,ELN	SHCK	36
	COMMON /DUPT/FMT(30),FP(4),FT(4),FH(4),FS(4),FM(4),FV(4),FD(4),	SHCK	37
	1 FC(4),FG(4),FB,FMT13,F1,F2,F3,F4,F5,FL(4),FMTI9,FA1,FA2,	SHCK	38
	2 FR1,FC1,FN(4),FR(4),FA(4),FI(4),FMT9X,F0	SHCK	39
C		SHCK	40
	EQUIVALENCE(M2M1,AEAT),(T2T1,SPIM),(U1U2,VACI,U2STAR),(U1,SUBAR)	SHCK	41
	EQUIVALENCE(SG,G(4,3)),(APP,RRHO),(Z,HO),(ANUM,NUM),(U5,UTWO)	SHCK	42
	1,(GG,X(4)),(MACH1,SUPAR),(M1,DATA(20)),(CPR1,DATA(21))	SHCK	43
	EQUIVALENCE(REFL,ISUP),(NSK,ISUB)	SHCK	44
C		SHCK	45
	NAMelist /SHKINP/U1,MACH1,GAMMA1,INCDEQ,REFLEQ,INCDFZ,REFLFZ,A1	SHCK	46
	DATA ONE/IH1/, FPP/4HP2/P/, FTT/4HT2/T/	SHCK	47
	2 FU1/3HU1/, FMM/4HM2/M/, FRA/4HRHO2/, FRB/4H/RHO/	SHCK	48
	3 FMA/4HMACH/, FMB/4H NO./, IZERO/2HO0/,FU2/3HU2,/	SHCK	49
	DATA TWO/IH2/, FP5/4HP5/P/, FT5/4HT5/T/	SHCK	50
	2 FU5/3FU5,/, FM5/4HM5/M/,FR5/4HRHO5/	SHCK	51



	DATA FV2/4HV2(U,4H1-U2,4H)M/S,2HEC/	SHCK 52
	1 , FUV/4HU5+V, 4H2,M/,3HSEC,1H /	SHCK 53
C	NFZ = 1	SHCK 54
	CALCH = .FALSE.	SHCK 55
	IF(TRACE.EQ.0.) TRACE=5.E-9	SHCK 56
	IOF = 0	SHCK 57
	TP=.TRUE.	SHCK 58
	CPR1 = 0.	SHCK 59
	DO 10 I=1,13	SHCK 60
	MACH1(I)=0.	SHCK 61
	U1(I)=0.	SHCK 62
10	CONTINUE	SHCK 63
	GAMMA1 = 0.	SHCK 64
	INCDEQ = .TRUE.	SHCK 65
	INCDFZ = .TRUE.	SHCK 66
	REFLEQ = .FALSE.	SHCK 67
	REFLFZ = .FALSE.	SHCK 68
	DO 18 N = 1,NREAC	SHCK 69
	NAME(N,5) = IZERO	SHCK 70
18	CONTINUE	SHCK 71
	SREFL = .FALSE.	SHCK 72
	READ (5,SHKINP)	SHCK 73
	WRITE(6,SHKINP)	SHCK 74
	IF(REFLEQ.OR.REFLFZ) SREFL=.TRUE.	SHCK 75
	SEQL = INCDEQ	SHCK 76
	IF(T(1).EQ.0.) T(1)=RTEMP(1)	SHCK 77
	DO 20 I = 1,13	SHCK 78
	IF (MACH1(I).EQ.0.0.AND.U1(I).EQ.0.0) GO TO 21	SHCK 79
	NSK = I	SHCK 80
20	CONTINUE	SHCK 81
21	IOF = IOF+1	SHCK 82
	OF = OXF(IOF)	SHCK 83
	CALL NEWOF	SHCK 84
C		SHCK 85
	INCDEQ = SEQL	SHCK 86
17	REFL = .FALSE.	SHCK 87
	IT2 = 2	SHCK 88
	IT1 = 1	SHCK 89
	PP = P(1)	SHCK 90
	TT = T(1)	SHCK 91
C		SHCK 92
C	FROZEN	SHCK 93
C		SHCK 94
117	DO 118 N = 1,NSK	SHCK 95
	DLVTP(N) = 1.	SHCK 96
	DLVPT(N) = -1.	SHCK 97
	DO 118 J = 1,NS	SHCK 98
	EN(J,N) = 0.0	SHCK 99
118	CONTINUE	SHCK 100
C		SHCK 101
19	DO 35 NPT=1,NSK	SHCK 102
	PPP(NPT) = P(NPT)	SHCK 103
	TTT(NPT) = T(NPT)	SHCK 104
	IF(NPT.EQ.1) GO TO 14	SHCK 105
	IF(PPP(NPT).EQ.0.) PPP(NPT)=PPP(NPT-1)	SHCK 106
	IF(TTT(NPT).EQ.0.) TTT(NPT)=TTT(NPT-1)	SHCK 107
	SSUM(NPT) = SSUM(NPT-1)	SHCK 108
	HSUM(NPT) = HSUM(NPT-1)	SHCK 109
	IF(TTT(NPT).EQ.TT.AND.PPP(NPT).EQ.PP) GO TO 15	SHCK 110
14	PP = PPP(NPT)	SHCK 111
	TT = TTT(NPT)	SHCK 112
	IF(TT.GE.TLOW/1.5) GO TO 814	SHCK 113
	WRITE(6,1152)	SHCK 114
	GO TO 1000	SHCK 115
		SHCK 116

814	CALL HCALC	SHCK 117
	HSUM(NPT) = HSUBC	SHCK 118
15	IF(CPR1.NE.0.) GAMMA1=CPR1/(CPR1-1./M1)	SHCK 119
	A1 = [RR*GAMMA1*TT/M1]**.5	SHCK 120
31	IF(U1(NPT).EQ.0.) U1(NPT)=A1*MACH1(NPT)	SHCK 121
	IF (MACH1(NPT).EQ.0.) MACH1(NPT) = U1(NPT)/A1	SHCK 122
	WM(NPT) = M1	SHCK 123
	CPR(NPT) = CPR1	SHCK 124
	GAMMAS(NPT) = GAMMA1	SHCK 125
	VLM(NPT) = RR*TT/(M1*101.325*PP)	SHCK 126
35	CONTINUE	SHCK 127
C		SHCK 128
C	OUTPUT--1ST CONDITION	SHCK 129
C		SHCK 130
	WRITE (6,861)	SHCK 131
861	FORMAT(1H1,48X,30HSHCK WAVE PARAMETERS ASSUMING)	SHCK 132
	IF(.NOT.INCDEQ) GO TO 44	SHCK 133
	WRITE (6,862)	SHCK 134
862	FORMAT (1H ,35X,55HEQUILIBRIUM COMPOSITION FOR INCIDENT SHOCKED COND	SHCK 135
	ITIONS //)	SHCK 136
	GO TO 45	SHCK 137
44	WRITE (6,863)	SHCK 138
863	FORMAT (1H ,37X,50HFROZEN COMPOSITION FOR INCIDENT SHOCKED CONDITI	SHCK 139
	ONS//)	SHCK 140
45	EQL = .FALSE.	SHCK 141
	CALL OUT1	SHCK 142
	WRITE(6,46)	SHCK 143
46	FORMAT (16H INITIAL GAS (1))	SHCK 144
	FMT(4)=FMT13	SHCK 145
	FMT(5)=FB	SHCK 146
	FMT(7)=F4	SHCK 147
	WRITE (6,FMT) FMA,FMB,FB,FB,(MACH1(J),J=1,NPT)	SHCK 148
	FMT(7) = F2	SHCK 149
	WRITE (6,FMT) FU1,FL(3),FL(4),FB,(U1(J),J=1,NPT)	SHCK 150
	CALL OUT2	SHCK 151
C		SHCK 152
C	BEGIN CALCULATIONS FOR 2ND CCNDITION	SHCK 153
C		SHCK 154
	IF(INCDEQ) EQL=.TRUE.	SHCK 155
47	NPT = 1	SHCK 156
48	GAMMA1 = GAMMAS(NPT)	SHCK 157
	UU = U1(NPT)	SHCK 158
	M1 = WM(NPT)	SHCK 159
	P1 = PPP(NPT)	SHCK 160
	T1 = TTT(NPT)	SHCK 161
	HS = HSUM(NPT)	SHCK 162
	IF(REFL) UU=U1U2(NPT)	SHCK 163
	MU12RT = M1*UU**2/(RR*T1)	SHCK 164
	IF(REFL) GO TO 59	SHCK 165
	P21 = (2.*GAMMA1*MACH1(NPT)**2-GAMMA1+1.)/(GAMMA1+1.)	SHCK 166
	T21 = P21*(2./MACH1(NPT)**2+GAMMA1-1.)/(GAMMA1+1.)	SHCK 167
	IF((T1*T21).GT.2000..AND. EQL) T21 = .7*T21 + 600./T1	SHCK 168
	GO TO 61	SHCK 169
		SHCK 170
C		SHCK 171
C	REFLECTED--SUBSCRIPTS 2=1, 5=2, P52=P21	SHCK 172
C		SHCK 173
59	T21 = 2.	SHCK 174
	B2 = (-1.-MU12RT-T21)/2.	SHCK 175
	P21 = -B2*SQRT(B2**2-T21)	SHCK 176
61	P21L=ALOG(P21)	SHCK 177
	T21L=ALOG(T21)	SHCK 178
	DO 100 ITR=1,8	SHCK 179
	IF(IDEBUG.GT.0.AND.NPT.GE.IDEBUG) WRITE(6,152) ITR,IT2,IT1,T21,	SHCK 180
	1IT2,IT1,P21	

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152 FORMAT(10H0ITR NO.= ,I1,7X,1HT,I1,2H/T,I1,2H =,F9.4,7X,1HP,I1,2H/PSHCK 181
1,I1,2H =,F9.4 ) SHCK 182
IT=T21*T1 SHCK 183
PP=P21*P1 SHCK 184
IF (.NOT.EQL) GO TO 40 SHCK 185
CALL EQLBRM SHCK 186
IF(TT.EQ.0.) GO TO 430 SHCK 187
GO TO 50 SHCK 188
C SHCK 189
C FROZEN SHCK 190
C SHCK 191
40 TLN = ALOG (TT) SHCK 192
IF(.NOT.INCDEQ) GO TO 88 SHCK 193
JS1 = 1 SHCK 194
CALL CPHS SHCK 195
CPR(NPT) = CPSUM SHCK 196
HSUM(NPT) = 0. SHCK 197
DO 84 J= 1,NS SHCK 198
IF(IUSE(J).EQ.0) HSUM(NPT)=HSUM(NPT)+HO(J)*EN(J,NPT) SHCK 199
84 CONTINUE SHCK 200
HSUM(NPT) = HSUM(NPT)*TT SHCK 201
GO TO 50 SHCK 202
88 CALL FCALC SHCK 203
IF(TT.EQ.0.) GO TO 150 SHCK 204
HSUM(NPT) = HSUBG SHCK 205
CPR(NPT) = CPR1 SHCK 206
C SHCK 207
50 RHO12 = M1*T21/(WM(NPT)*P21) SHCK 208
GG=RFC12*MU12RT SHCK 209
RHO52 = 1./RHO12 SHCK 210
IF(REFL) GG=-MU12RT*RHO52/(RHO52-1.):**2 SHCK 211
G(1,1)=-GG*DLVPT(NPT)-P21 SHCK 212
G(1,2)=-GG*DLVTP(NPT) SHCK 213
G(1,3)=P21-1.+GG-MU12RT SHCK 214
IF(REFL) G(1,3) = P21-1.+GG*(RHO52-1.) SHCK 215
GG = GG*T1/M1 SHCK 216
IF(.NOT.REFL) GG=GG*RHO12 SHCK 217
G(2,1)=-GG*DLVPT(NPT)+TT*(DLVTP(NPT)-1.)/WM(NPT) SHCK 218
G(2,2)=-GG*DLVTP(NPT)-TT*CPR(NPT) SHCK 219
GG = 1.-RHO12**2 SHCK 220
IF(REFL) GG=(RHO52+1.)/(RHO52-1.) SHCK 221
G(2,3)=HSUM(NPT)-HS-UU**2*GG/(2.*RR) SHCK 222
X(3)=G(1,1)*G(2,2)-G(1,2)*G(2,1) SHCK 223
X(1)=(G(1,3)*G(2,2)-G(2,3)*G(1,2))/X(3) SHCK 224
X(2)=(G(1,1)*G(2,3)-G(2,1)*G(1,3))/X(3) SHCK 225
C SHCK 226
AX = X(1) SHCK 227
AXX = X(2) SHCK 228
IF(AX.LT.0.) AX = -AX SHCK 229
IF (AXX.LT.0.) AXX = -AXX SHCK 230
IF (AXX.GT.AX) AX = AXX SHCK 231
IF(AX.LT..00005) GO TO 150 SHCK 232
AX = AX/.4C54652 SHCK 233
IF(AX.LE.1.) GO TO 75 SHCK 234
X(1) = X(1)/AX SHCK 235
X(2) = X(2)/AX SHCK 236
75 P21L=P21L*AX(1) SHCK 237
T21L=T21L*AX(2) SHCK 238
P21=EXP(P21L) SHCK 239
T21=EXP(T21L) SHCK 240
100 CONTINUE SHCK 241
WRITE(6,125) U1(NPT) SHCK 242
125 FORMAT(25HODID NOT CONVERGE FOR U1=,F8.2,56H ANSWERS PROBABLY NO SHCK 243
IT RELIABLE, SOLUTION MAY NOT EXIST) SHCK 244

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150	RRHO(NPT) = RHO52	SHCK 245
	M2M1(NPT) = WM(NPT)/M1	SHCK 246
	PCP(NPT) = P21	SHCK 247
	T2T1(NPT) = T21	SHCK 248
	UTWO(NPT) = UU*RHO12	SHCK 249
	U1U2(NPT) = UU-UTWO(NPT)	SHCK 250
	IF(TT.GE.TLOW/1.5.AND.TT.LE.THIGH*1.25) GO TO 153	SHCK 251
	WRITE(6,1152)	SHCK 252
1152	FORMAT(47H)OTEMPERATURE IS OUT OF RANGE OF THE THERMO DATA)	SHCK 253
153	IF(.NOT.REFL) GO TO 154	SHCK 254
	U5(NPT) = UU/(RHO52-1.)	SHCK 255
	U2STAR(NPT) = U5(NPT)+UU	SHCK 256
154	IF(EQL) GO TO 431	SHCK 257
C		SHCK 258
C	FROZEN	SHCK 259
C		SHCK 260
161	PPP(NPT) = PP	SHCK 261
	TTT(NPT) = TT	SHCK 262
	GAMMAS(NPT) = CPR(NPT)/(CPR(NPT)-1./M1)	SHCK 263
	VLM(NPT) = RR*TT/(M1*101.325*PP)	SHCK 264
	IF(.NOT.INCDEQ) GO TO 431	SHCK 265
	SSUM(NPT) = 0.	SHCK 266
	DO 166 J=1,NS	SHCK 267
	PMN = PP*M1*EN(J,NPT)	SHCK 268
	IF(IUSE(J).EQ.0) SSUM(NPT)=SSUM(NPT)+EN(J,NPT)*(S(J)-ALOG(PMN))	SHCK 269
166	CONTINUE	SHCK 270
C		SHCK 271
	GO TO 431	SHCK 272
430	IF(NPT.LT.1) GO TO 1000	SHCK 273
	NSK = NPT	SHCK 274
C		SHCK 275
431	ISV = 0	SHCK 276
	IF(NPT.LT.NSK) ISV=NPT	SHCK 277
	IF(NPT.EQ.1) ISV=-1	SHCK 278
	NPT = NPT+1	SHCK 279
	IF(EQL) CALL SAVE	SHCK 280
	IF(NPT.LE.NSK) GO TO 48	SHCK 281
	NPT = NSK	SHCK 282
C		SHCK 283
C	OUTPUT--2ND CONDITION	SHCK 284
C		SHCK 285
	WRITE(6,156)	SHCK 286
156	FORMAT(1H)	SHCK 287
	IF(REFL) GO TO 56	SHCK 288
	IF(.NOT.EQL) WRITE(6,57)	SHCK 289
57	FORMAT(34H)OSHOCKED GAS (2)--INCIDENT--FROZEN)	SHCK 290
	IF(EQL) WRITE(6,157)	SHCK 291
157	FORMAT(39H)OSHOCKED GAS (2)--INCIDENT--EQUILIBRIUM)	SHCK 292
	DO 55 I=1,4	SHCK 293
55	W(I) = FV2(I)	SHCK 294
	W(5) = FPP	SHCK 295
	W(6) = ONE	SHCK 296
	W(7) = FIT	SHCK 297
	W(8) = FMM	SHCK 298
	W(9) = FRA	SHCK 299
	W(10) = FU2	SHCK 300
	GO TO 700	SHCK 301
56	IF(.NOT.EQL) WRITE(6,58)	SHCK 302
	IF(EQL) WRITE(6,690)	SHCK 303
58	FORMAT(35H)OSHOCKED GAS (5)--REFLECTED--FROZEN)	SHCK 304
690	FORMAT(40H)OSHOCKED GAS (5)--REFLECTED--EQUILIBRIUM)	SHCK 305
	DO 65 I=1,4	SHCK 306
65	W(I) = FUV(I)	SHCK 307
	W(5) = FP5	SHCK 308
	W(6) = TWO	SHCK 309



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W(7) = FT5
W(8) = FM5
W(9) = FR5
W(10) = FU5
700 FMT(7) = F2
WRITE (6,FMT)W(10),FL(3),FL(4),FB,(UTWO(J),J=1,NPT)
CALL OUT2
WRITE(6,156)
FMT(7)=F2
WRITE(6,FMT)W(5),W(6),FB,FB,(PCP(J),J=1,NPT)
WRITE(6,FMT)W(7),W(6),FB,FB,(T2T1(J),J=1,NPT)
FMT(7)=F4
WRITE(6,FMT)W(8),W(6),FB,FB,(M2M1(J),J=1,NPT)
WRITE(6,FMT)W(9),FRB,W(6),FB,(RRHO(J),J=1,NPT)
FMT(7) = F2
WRITE(6,FMT) (W(I),I=1,4),(U1U2(J),J=1,NPT)
IF(.NOT.EQL) GO TO 850
CALL OUT3
GO TO 865

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SHCK 310
SHCK 311
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C
C WRITE FROZEN MOLE FRACTIONS
C

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850 FMT(7) = F5
IF(.NOT.INCDEQ) GO TO 852
EQL = .TRUE.
CALL OUT3
EQL = .FALSE.
GO TO 865
852 WRITE(6,854)
854 FORMAT (15#OMOLE FRACTIONS //)
DO 856 N = 1, NREAC
J = NUM(N,5)
DO 855 I = 1,NPT
V(I) = EN(J,I)*M1
855 CONTINUE
WRITE (6,FMT) SUB (J,1),SUB(J,2),FB,FB,(V(I),I = 1,NPT)
856 CONTINUE

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C
865 RETURN
C

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ENTRY SHCK1

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C
I
IF(.NOT.SREFL) GO TO 948
IF(.NOT.REFL) GO TO 935
IF(EQL.OR..NOT.REFLEQ) GO TO 948
GO TO 940
935 REFL = .TRUE.
IT2 = 5
IT1 = 2
EQL = .TRUE.
IF(.NOT.REFLFZ) GO TO 47
EQL = .FALSE.
IF(.NOT.REFLEQ) GO TO 47
J = 0
DO 936 I=1,NPT
J = J+1
SG(J) = U1U2(I)
J = J+1
SG(J) = WM(I)
J = J+1
SG(J) = PPP(I)
J = J+1
SG(J) = TTT(I)
J = J+1
SG(J) = HSUM(I)

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J = J+1	SHCK 375
SG(J) = GAMMAS(I)	SHCK 376
936 CONTINUE	SHCK 377
GO TO 47	SHCK 378
940 J = 1	SHCK 379
DO 946 I=1,NPT	SHCK 380
U1U2(I) = SG(J)	SHCK 381
WM(I) = SG(J+1)	SHCK 382
PPP(I) = SG(J+2)	SHCK 383
TTT(I) = SG(J+3)	SHCK 384
HSUM(I) = SG(J+4)	SHCK 385
GAMMAS(I) = SG(J+5)	SHCK 386
946 J = J+6	SHCK 387
EQL = .TRUE.	SHCK 388
GO TO 47	SHCK 389
948 IF(.NOT.INCDEQ.OR..NOT.INCDFZ) GO TO 950	SHCK 390
INCDEQ = .FALSE.	SHCK 391
EQL = .FALSE.	SHCK 392
GO TO 17	SHCK 393
950 IF(IOF.LT.NOF) GO TO 21	SHCK 394
TP = .FALSE.	SHCK 395
DO 999 N=1,NREAC	SHCK 396
RTEMP(N) = T(1)	SHCK 397
999 CONTINUE	SHCK 398
1000 RETURN 1	SHCK 399
END	SHCK 400

C	SUBROUTINE DETON (*)	DETN 1
C		DETN 2
C	CHAPMAN-JOUQUET DETONATIONS	DETN 3
C		DETN 4
C	THE FOLLOWING DOUBLE PRECISION TYPE STATEMENTS ARE REQUIRED FOR	DETN 5
C	IBM 360 MACHINES ONLY	DETN 6
C		DETN 7
C	DOUBLE PRECISION HSUM,SSUM,CPR,DLVTP,DLVPT,GAMMAS	DETN 8
C	DOUBLE PRECISION COEF,S,EN,ENLN,HO,DELN	DETN 9
C		DETN 10
C	LOGICAL HP,SP,TP,EQL,TSCHED	DETN 11
C		DETN 12
C	DIMENSION GM(13),CP(13),H1(13),PUB(13),TUB(13),GM1(13),RRHO(13)	DETN 13
C		DETN 14
C	COMMON /POINTS/HSUM(13),SSUM(13),CPR(13),DLVTP(13),DLVPT(13),	DETN 15
	1 GAMMAS(13),P(26),T(52),V(13),PPP(13),WM(13),SONVEL(13),TTT(13),	DETN 16
	2 VLM(13),TCTN(13)	DETN 17
	COMMON /SPECES/COEF(2,7,100),S(100),HO(100),DELN(100),DUMMY(100),	DETN 18
	1 EN(100,13),ENLN(100),A(10,100),SUB(100,3),IUSE(100),TEMP(50,2)	DETN 19
	COMMON /MISC/ENN,SUMN,TT,SO,ATOM(3,101),LLMT(10),PO(10),BOP(10,2),	DETN 20
	1 TM,TLOW,TMID,THIGH,PP,CPSUM,OF,EQRAT,FPCT,R,RR,HSUBO,AM(2),	DETN 21
	2 HPP(2),RH(2),VMIN(2),VPLS(2),WP(2),DATA(22),NAME(15,5),	DETN 22
	3 ANUM(15,5),PECWT(15),ENTH(15),FAZ(15),RTEMP(15),FCX(15),DENS(15),	DETN 23
	4 RHOP,RMW(15),TLN,CR,OXF(15),ENNL,TRACE,LLMTS(10),SBOP(10,2)	DETN 24
	COMMON /INDX/IDEBUG,CONVG,TP,HP,SP,ISV,NPP,MOLES,NP,NT,NPT,NLM,	DETN 25
	1 NS,KMAT,IMAT,IQ1,IOF,NOF,NOMIT,IP,NEWNR,NSUB,NSUP,RKT,DETN,SHOCK,	DETN 26
	2 IONS,NC,NSERT,JSOL,JLIQ,KASE,NREAC,IC,JS1,VOL,IT,CALCH,NLS,LOGV,	DETN 27
	3 ISUP,ISUB,ITNUM,ITM,INCDFZ,INCDEQ,CPRF,IPP,SEQL,PCPLT	DETN 28
	COMMON /PERF/PCP(22),VMOC(13),SPIM(13),VACI(13),SUBAR(13),	DETN 29
	1 SUPAR(13),APP(13),AEAT(13),CSTR,EQL,FROZ,SSO,AREA,AWT,NFZ,	DETN 30
	2 APPL,ARATIO,ELN	DETN 31

	CCMMCN /DUPT/FMT(30),FP(4),FT(4),FH(4),FS(4),FM(4),FV(4),FD(4),	DETN	32
	1 FC(4),FG(4),FB,FMT13,F1,F2,F3,F4,F5,FL(4),FMT19,FA1,FA2,	DETN	33
	2 FR1,FC1,FN(4),FR(4),FA(4),FI(4),FMT9X,F0	DETN	34
C		DETN	35
	EQUIVALENCE(CP,DATA),(GM,SPIM),(H1,VAC1),(PUB,SUBAR),(TUR,SUPAR)	DETN	36
	EQUIVALENCE(GM1,AEAT),(K,ISV)	DETN	37
	EQUIVALENCE(AM1,DATA(20)),(CPR1,DATA(21))	DETN	38
C		DETN	39
	DATA FT1/4FT1,D/, FP1/4HP1,A/, FH1/4HH1,C/, FM1/4HM1,M/	DETN	40
	1 , FG1/4HA1 /, FPP/4HP/P1/, FTT/4TT/T1/	DETN	41
	2 ; FUD/4HDET /, FMM/4HM/M1/, FRA/4HRHO//, FRB/4HRH01/	DETN	42
	3 ; FMA/4FMACH/, FMB/4H NO./, IZERO/2HOC/	DETN	43
C		DETN	44
	IOF = 0	DETN	45
C		DETN	46
C	IF NO T SCHEDULE, SET TSCHED=.FALSE. AND USE T FROM FIRST REACTANT	DETN	47
C		DETN	48
	TSCHED = .TRUE.	DETN	49
	IF(T(1).NE.0.) GO TO 3	DETN	50
	T(1) = RTEMP(1)	DETN	51
	TSCHED = .FALSE.	DETN	52
	GO TO 7	DETN	53
	3 DO 4 N=1,NREAC	DETN	54
	NAME(N,5) = IZERO	DETN	55
	4 CCNTINUE	DETN	56
	7 TT = T(1)	DETN	57
	IOF = IOF+1	DETN	58
	OF = OXF(IOF)	DETN	59
	CALL NEWOF	DETN	60
	WRITE (6,11)	DETN	61
	11 FORMAT(33H1DETONATION VELOCITY CALCULATIONS)	DETN	62
C		DETN	63
C	BEGIN T LOOP.	DETN	64
C		DETN	65
	IT = 0	DETN	66
901	IT = IT + 1	DETN	67
	T1= T(IT)	DETN	68
	TT = T1	DETN	69
	IF(.NOT.TSCHED) GO TO 20	DETN	70
	CALL HCALC	DETN	71
	IF(TT.EQ.0.) RETURN 1	DETN	72
	20 IF(IDEBUG.NE.0) CALL OUT1	DETN	73
C		DETN	74
C	BEGIN P LCCP.	DETN	75
C		DETN	76
	IP = 0	DETN	77
903	IP = IP + 1	DETN	78
	P1= P(IP)	DETN	79
	H1(NPT) = FSUBO*R	DETN	80
	TUB(NPT)=T1	DETN	81
	PUB(NPT)=P1	DETN	82
	CP(NPT) = CPR1*R	DETN	83
	ITR= 0	DETN	84
	TT= 3800.	DETN	85
	PP1= 15.	DETN	86
	PP= PP1*P1	DETN	87
C		DETN	88
C	CALCULATE ENTHALPY FOR INITIAL ESTIMATE OF T2(TT AFTER EQLBRM)	DETN	89
C		DETN	90
	HSUBC = H1(NPT)/R + .75*T1*PP1/AM1	DETN	91
	TP = .FALSE.	DETN	92
	HP= .TRUE.	DETN	93
	CALL EQLBRM	DETN	94
	HSUBO = H1(NPT)/R	DETN	95
	HP= .FALSE.	DETN	96




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IF(TT.EQ.0.) GO TO 902
GAM= GAMMAS(NPT)
TT1= TT/T1
II= 0
TEM=TT1-.75*PP1/(CPR(NPT)*AM1)
AMM=WM(NPT)/AM1
WRITE(6,190)TT
190 FORMAT(8H0T EST.=,F8.2/I1X,4HP/P1,17X,4HT/T1)
WRITE(6,203) II,PP1,TT1
C
C
C LOOP FOR IMPROVING T2/T1 AND P2/P1 INITIAL ESTIMATE.
C
200 DO 202 II=1,3
ALFA=AMM/TT1
PP1= (1.+GAM)*(1.+(1.-4.*GAM*ALFA/(1.+GAM)**2)**.5)/(2.*GAM*ALFA)
RK=PP1*ALFA
TT1= TEM+.5*PP1*GAM*(RK*RK-1.)/(AM1*CPR(NPT)*RK)
IF(IDEBUG.GT.0.AND.NPT.GE.IDEBUG) WRITE(6,203) II,PP1,TT1
203 FCRMAT (I5,2E20.8)
202 CCNTINUE
TP= .TRUE.
TT= T1*TT1
RR1 = PP1*AMM/TT1
C
C
C BEGIN MAIN ITERATION LOOP.
C
205 ITR= ITR+1
PP= P1*PP1
CALL EQLBRM
IF (NPT.EQ.0) GO TO 1000
IF (TT.EQ.0.) GO TO 860
GAM= GAMMAS(NPT)
AMM= WM(NPT)/AM1
RR1= PP1*AMM/TT1
A11= 1./PP1 + GAM*RR1*DLVPT(NPT)
A12= GAM*RR1*DLVTP(NPT)
A21= .5*GAM*(RR1**2-1.-DLVPT(NPT)*(1.+RR1**2))+DLVTP(NPT)-1.
A22=-.5*GAM*DLVTP(NPT)*(RR1**2+1.)-WM(NPT)*CPR(NPT)
B1= 1./PP1-1.+GAM*(RR1-1.)
B2= WM(NPT)*(HSUM(NPT)-H1(NPT)/R)/TT-.5*GAM*(RR1*RR1-1.)
D = A11*A22-A12*A21
X1 = (A22*B1-A12*B2)/D
X2 = (A11*B2-A21*B1)/D
ALAM= 1.
TEM = X1
IF(TEM.LT.0.) TEM = -TEM
IF(X2.GT.TEM) TEM=X2
IF (-X2.GT.TEM) TEM = -X2
IF(TEM.GT.0.4054652) ALAM=.4054652/TEM
PP1= PP1*EXP(X1*ALAM)
TT1= TT1*EXP(X2*ALAM)
TT = T1*TT1
UD = RR1*(RR*GAM*TT/WM(NPT))**.5
IF(IDEBUG.GT.0.AND.NPT.GE.IDEBUG) WRITE(6,30)ITR,PP1,TT1,RR1,X1,
1X2
30 FORMAT(7H0ITER =,I2,5X,6HP/P1 =,E15.8,5X,6HT/T1 =,E15.8,5X,10HRHO/
1RHO1 =,E15.8/7X,13HDEL LN P/P1 =,E15.8,5X,13HDEL LN T/T1 =,E15.8)
C
C
C CONVERGENCE TEST
C
IF(ITR.LT.8.AND.TEM.GT.0.5E-04) GO TO 205
IF(ITR.LT.8) GO TO 35
WRITE(6,34)
34 FCRMAT(53H0CONSERVATION EQNS WERE NOT SATISFIED IN 8 ITERATIONS)
NPT = NPT-1

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DETN 97
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DETN 160
DETN 161

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TT = 0.	DETN 162
GO TO 150	DETN 163
35 RRHO(NPT)=RR1	DETN 164
IF (CP(NPT).EQ.0.) GO TO 40	DETN 165
GM1(NPT) = CP(NPT) / (CP(NPT)-R/AM1)	DETN 166
VMOC(NPT) = UD/(RR*GM1(NPT)*T1/AM1)**.5	DETN 167
GO TO 150	DETN 168
40 GM1(NPT) = 0.	DETN 169
VMOC(NPT) = 0.	DETN 170
150 K = 0	DETN 171
IF (IP.EQ.NP.AND.IT.EQ.NT.OR.TT.EQ.0.) GO TO 860	DETN 172
K = NPT	DETN 173
IF (NPT.NE.13) GO TO 870	DETN 174
C	DETN 175
C OUTPUT	DETN 176
C	DETN 177
860 WRITE (6,5)	DETN 178
5 FORMAT(1H1,42X,46HDETONATION PROPERTIES OF AN IDEAL REACTING GAS)	DETN 179
CALL OUT1	DETN 180
WRITE(6,46)	DETN 181
46 FORMAT(13H UNBURNED GAS//)	DETN 182
FMT(4)=FMT13	DETN 183
FMT(5)=F5	DETN 184
FMT(7)=F4	DETN 185
WRITE(6,FMT) FP1,FP(2),FB,FB,(PUB(J),J=1,NPT)	DETN 186
FMT(7)=F2	DETN 187
WRITE(6,FMT) FT1,FT(2),FB,FB,(TUB(J),J=1,NPT)	DETN 188
WRITE(6,FMT) FH1,FH(2),FB,FB,(H1(J),J=1,NPT)	DETN 189
DO 56 I=1,NPT	DETN 190
V(I)=AM1	DETN 191
SONVEL(I) = (RR*GM1(I)*TUB(I)/AM1)**.5	DETN 192
56 CONTINUE	DETN 193
FMT(7)=F3	DETN 194
WRITE(6,FMT) FM1,FM(2),FM(3),FB,(V(J),J=1,NPT)	DETN 195
FMT(7)=F4	DETN 196
IF(.NOT.TSCHED) GO TO 57	DETN 197
WRITE(6,FMT) FG(1),FG1,FB,FB,(GM1(J),J=1,NPT)	DETN 198
FMT(7)=F1	DETN 199
WRITE(6,FMT) (FL(I),I=1,4),(SONVEL(J),J=1,NPT)	DETN 200
57 WRITE(6,58)	DETN 201
58 FORMAT(11HCBURNED GAS//)	DETN 202
FMT(4)=FMT(6)	DETN 203
CALL OUT2	DETN 204
WRITE(6,68)	DETN 205
88 FORMAT(22HODETONATION PARAMETERS //)	DETN 206
FMT(7)=F2	DETN 207
DO 70 I=1,NPT	DETN 208
V(I)= PPP(I)/PUB(I)	DETN 209
PCP(I)=TTT(I)/TUB(I)	DETN 210
SONVEL(I)=SONVEL(I)*RRHO(I)	DETN 211
70 CONTINUE	DETN 212
WRITE(6,FMT) FPP,FB,FB,FB,(V(J),J=1,NPT)	DETN 213
WRITE(6,FMT) FTT,FB,FB,FB,(PCP(J),J=1,NPT)	DETN 214
DO 73 I=1,NPT	DETN 215
V(I)=WM(I)/AM1	DETN 216
73 CONTINUE	DETN 217
FMT(7)=F4	DETN 218
WRITE(6,FMT) FMM,FB,FB,FB,(V(J),J=1,NPT)	DETN 219
WRITE(6,FMT) FRA,FRE,FB,FB,(RRHO(J),J=1,NPT)	DETN 220
IF(TSCHED) WRITE(6,FMT) FMA,FMB,FB,FB,(VMOC(J),J=1,NPT)	DETN 221
FMT(7)=F1	DETN 222
WRITE(6,FMT) FUD,FL(2),FL(3),FL(4),(SONVEL(J),J=1,NPT)	DETN 223
EQL=.TRUE.	DETN 224
CALL OUT3	DETN 225
C	DETN 226
C END OUTPUT.	DETN 227

C		RETURN	DETN 228
C		ENTRY DETON1	DETN 229
C			DETN 230
	865	IF(K.EQ.0.AND.IOF.EQ.NOF) GC TO 1000	DETN 231
		IF (NP.EQ.1 .AND. NT.EQ.1) GO TO 7	DETN 232
		IDEBUG = IDEBUG-13	DETN 233
		WRITE(6,868)	DETN 234
	868	FORMAT(1F1)	DETN 235
		NPT = 0	DETN 236
	870	NPT = NPT + 1	DETN 237
		IF(ISV.EQ.1) ISV=-1	DETN 238
		CALL SAVE	DETN 239
		IF(IP.LT.NP) GO TO 903	DETN 240
	902	IF(IT.LT.NT) GO TO 901	DETN 241
		IF(IOF.GE.NOF) GO TO 1000	DETN 242
		IDEBUG = IDEBUG+13	DETN 243
		GO TO 7	DETN 244
	1000	TP = .FALSE.	DETN 245
		RETURN 1	DETN 246
		END	DETN 247
			DETN 248
			DETN 249

C		BLOCK DATA	BLOK 1
C			BLOK 2
C		DIMENSION ATEM(3,50)	BLOK 3
C			BLOK 4
		COMMON /MISC/ENN,SUMN,TT,SO,ATOM(3,101),LLMT(10),BO(10),BOP(10,2),	BLOK 5
	1	TM,TLOW,TMID,THIGH,PP,CPSUM,OF,EQRAT,FPCT,R,RR,HSUB0,AM(2),	BLOK 6
	2	HPP(2),RH(2),VMIN(2),VPLS(2),WP(2),DATA(22),NAME(15,5),	BLOK 7
	3	ANUM(15,5),PECWT(15),ENTH(15),FAZ(15),RTEMP(15),FOX(15),DENS(15),	BLOK 8
	4	RHOP,RMW(15),TLN,CR,OXF(15),ENNL,TRACE,LLMTS(10),SBOP(10,2)	BLOK 9
		COMMON /OUP/T/FMT(30),FP(4),FT(4),FH(4),FS(4),FM(4),FV(4),FD(4),	BLOK 10
	1	FC(4),FG(4),FB,FMT13,F1,F2,F3,F4,F5,FL(4),FMTI9,FA1,FA2,	BLOK 11
	2	FR1,FC1,FN(4),FR(4),FA(4),FI(4),FMT9X,FO	BLOK 12
C			BLOK 13
C		EQUIVALENCE (ATOM(1,52),ATEM)	BLOK 14
C			BLOK 15
C		ATOMIC SYMBOLS, WEIGHTS, AND VALENCES	BLOK 16
C			BLOK 17
		DATA ATOM/ 2HE ,5.48597E-4,-1.,	BLOK 18
	A	2HH , 1.00797 , 1., 2HHE, 4.0026, 0., 2HLI, 6.939 , 1.,	BLOK 19
	B	2HBE, 9.0122 , 2., 2HB , 10.811 , 3., 2HC , 12.01115, 4.,	BLOK 20
	C	2HN , 14.0067 , 0., 2HO , 15.9994,-2., 2HF , 18.9984 , -1.,	BLOK 21
	D	2HNE, 20.183 , 0., 2HNA, 22.9898, 1., 2HMG, 24.312 , 2.,	BLOK 22
	E	2HAL, 26.9815 , 3., 2HSI, 28.086 , 4., 2HP , 30.9738 , 5.,	BLOK 23
	F	2HS , 32.064 , 4., 2HCL, 35.453 , -1., 2HAR, 39.948 , 0.,	BLOK 24
	G	2HK , 39.102 , 1., 2HCA, 40.080 , 2., 2HSC, 44.956 , 3.,	BLOK 25
	H	2HTI, 47.900 , 4., 2HV , 50.942 , 5., 2HCR, 51.996 , 3.,	BLOK 26
	I	2HMN, 54.9380 , 2., 2HFE, 55.847 , 3., 2HCO, 58.9332 , 2.,	BLOK 27
	J	2HNI, 58.710 , 2., 2HCU, 63.540 , 2., 2HZN, 65.370 , 2.,	BLOK 28
	K	2HGA, 69.720 , 3., 2HGE, 72.590 , 4., 2HAS, 74.9216 , 3.,	BLOK 29
	L	2HSE, 78.960 , 4., 2HBR, 79.909 , -1., 2HKR, 83.800 , 0.,	BLOK 30
	M	2HRB, 85.47 , 1., 2HSR, 87.620 , 2., 2HY , 88.905 , 3.,	BLOK 31
	N	2HZR, 91.220 , 4., 2HNR, 92.906 , 5., 2HMO, 95.94 , 6.,	BLOK 32
	O	2HTC, 99.000 , 7., 2HRU,101.070 , 3., 2HRH,102.905 , 3.,	BLOK 33
	P	2HPD,106.400 , 2., 2HAG,107.870 , 1., 2HCD,112.400 , 2.,	BLOK 34
	Q	2HIN,114.820 , 3., 2HSN,118.690 , 4., 2HSP,121.750 , 3.,	BLOK 35



	DATA ATEM/					BLOK	36
R	2HTE,127.600	, 4.,	2HI,126.9044,-1.,	2HXE,131.300	, 0.,	BLOK	37
S	2HCS,132.905	, 1.,	2HBA,137.340, 2.,	2HLA,138.910	, 3.,	BLOK	38
T	2HCE,140.120	, 3.,	2HPR,140.907, 3.,	2HND,144.240	, 3.,	BLOK	39
U	2HPM,145.000	, 3.,	2HSM,150.350, 3.,	2HEU,151.960	, 3.,	BLOK	40
V	2HGD,157.250	, 3.,	2HTB,158.924, 3.,	2HDY,162.500	, 3.,	BLOK	41
W	2HHO,164.930	, 3.,	2HER,167.260, 3.,	2HTM,168.934	, 3.,	BLOK	42
X	2HYB,173.040	, 3.,	2HLU,174.997, 3.,	2HHF,178.490	, 4.,	BLOK	43
Y	2HTA,180.948	, 5.,	2HW,183.850, 6.,	2HRE,186.200	, 7.,	BLOK	44
Z	2HOS,190.200	, 4.,	2HIR,192.200, 4.,	2HPT,195.090	, 4.,	BLOK	45
A	2HAU,196.967	, 3.,	2HHG,200.590, 2.,	2HTL,204.370	, 1.,	BLOK	46
B	2HPB,207.190	, 2.,	2HBI,208.980, 3.,	2HPO,210.000	, 2.,	BLOK	47
C	2HAT,210.000	, 0.,	2HRN,222.000, 0.,	2HFR,223.000	, 1.,	BLOK	48
D	2HRA,226.000	, 2.,	2HAC,227.000, 3.,	2HTH,232.038	, 4.,	BLOK	49
E	2HPA,231.000	, 5.,	2HU,238.030, 6.,	2HNP,237.000	, 5.,	BLOK	50
F	2HPU,242.000	, 4.,	2HAM,243.000, 3.,	2HCM,247.000	, 3.,	BLOK	51
G	2HBK,249.000	, 3.,	2HCF,251.000, 3.,	2HES,254.000	, 0.,	BLOK	52
H	2HD,2.014102, 1./					BLOK	53

C
C
C INFORMATION USED IN VARIABLE OUTPUT FORMAT BLOK 54
BLOK 55
BLOK 56

DATA FMT/3H(1H,4H,3A4,4H,A2,,3HF9.,2H0,,3HF9.,2H0,,3HF9.,2H0,,3HF9BLOK 57
1.,2H0,,3HF9.,2H0,,3HF9.,2H0,,3HF9.,2H0,,3HF9.,2H0,,3HF9.,2H0,,3HF9BLOK 58
2.,2H0,,3HF9.,2H0,,3HF9.,2H0,,3HF9.,1H0,1H)/,FB,F0,F1,F2,F3,F4,F5/BLOK 59
31H,2H0,,2H1,,2H2,,2H3,,2H4,,2H5,/,FMT13/2H13/,FMT9X/3H9X,/,FMTI9BLOK 60
4/3H19,/, BLOK 61
DATA FP/4HP, A,4HTM,2H,1H / BLOK 62
1,FT/4HT, D,4HEG K,4H,2H /,FH/4HH, C,4HAL/G,2H,1H / BLOK 63
2,FS/4HS, C,4HAL/(,4HG)(K,2H) /,FM/4HM, M,4HOL W,2HT,1H / BLOK 64
3,FV/4H(DLV,4H/DLF,4H)T,2H /,FD/4H(DLV,4H/DLT,2H)P,1H / BLOK 65
4,FC/4HCP,4HCAL/,4H(G)(,2HK)/,FG/4HGAMM,4HA(S,2H),1H / BLOK 66
5,FL/4HSON,4HVEL,,4HM/SE,2HC / BLOK 67
BLOK 68

C
C
C INFORMATION USED IN PERFORMANCE OUTPUT BLOK 69
BLOK 70

DATA FR1/4HPC/P/, FC1/2HCF/, FN/4HMACH,4H NUM,4HBER,1H / BLOK 71
1,FR/4HCSTA,4HR, F,4HT/SE,2HC /,FI/4HISP,,4H LB-,4HSEC/,2HLB/ BLOK 72
2,FA/4HIVAC,4H, LB-,4HSEC/,2HLB /,FA1/4HAE/A/,FA2/1HT/ BLOK 73
END BLOK 74

C
C SUBROUTINE TRANSP TRAN 1
C TRAN 2
C CALCULATES GAS TRANSPORT PROPERTIES TRAN 3
C TRAN 4
C MAXIMUM = 20 MOLECULES AND 17 REACTIONS TRAN 5
C NUMBER OF MOLECULES = NM TRAN 6
C NUMBER OF CHEMICAL REACTIONS = NR TRAN 7
C IF PUNCHED CARDS WANTED, PUNCH = TRUE TRAN 8
C ARRAY OF STOICHIOMETRIC COEFFICIENTS = STC TRAN 9
C NUMBER OF ROTATIONAL MODES = ROTM TRAN 10
C ROTATIONAL COLLISION NUMBER = ZROT TRAN 11
C VIBRATIONAL COLLISION NUMBER = ZVIB TRAN 12
C VIBRATIONAL HEAT CAPACITY = CVIBR TRAN 13
C MAXIMUM = 120 TABLES OF 20 TEMPERATURES EACH TRAN 14
C IF CROSS SECTION DATA NTAB = 1, IF RELAXATION DATA NTAB = 2 TRAN 15
C VISCOSITY=ANS(1), MONATOMIC CONDUCTIVITY=ANS(2), TRAN 16
C INTERNAL CONDUCTIVITY=ANS(3), FROZEN CONDUCTIVITY=ANS(4), TRAN 17
C REACTION CONDUCTIVITY=ANS(5), EQUILIBRIUM CONDUCTIVITY=ANS(6), TRAN 18

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C      FROZEN CP=ANS(7), EQUILIBRIUM CP=ANS(8),          TRAN 19
C      FROZEN PRANDTL NUMBER=ANS(9), EQUILIBRIUM PRANDTL NUMBER=ANS(10), TRAN 20
C      LEWIS NUMBER=ANS(11), MOLECULAR WEIGHT=ANS(12), DENSITY=ANS(13), TRAN 21
C      REACTION CP=ANS(14), ENTHALPY=ANS(15)             TRAN 22
C                                                       TRAN 23
      DOUBLE PRECISION G,X,GMAT,CHECK,SUM1,SUM2          TRAN 24
      INTEGER SUB,SPECIE,SPECE                           TRAN 25
      REAL MONCON,INTCON,LEWIS                           TRAN 26
      LOGICAL TRNSPT,FROZN,PUNCH,NODATA                  TRAN 27
C                                                       TRAN 28
      COMMON /POINTS/HSUM(13),SSUM(13),CPR(13),DLVTP(13),DLVPT(13), TRAN 29
1     GAMMAS(13),P(26),T(52),V(13),PPP(13),WM(13),SONVEL(13),TTT(13), TRAN 30
2     VLM(13),TOTN(13)                                   TRAN 31
      COMMON /SPECES/COEF(2,7,100),S(100),HO(100),DELN(100),DUMMY(100), TRAN 32
1     EN(100,13),ENLN(100),A(10,100),SUB(100,3),IUSE(100),TEMP(50,2) TRAN 33
      COMMON /MISC/ENN,SUMN,TT,SO,ATOM(3,101),LLMT(10),PO(10),ROP(10,2), TRAN 34
1     TM,TLOW,TMID,THIGH,PP,CPSUM,OF,EQRAT,FPCT,R,RR,HSUBO,AM(2),   TRAN 35
2     HPP(2),RH(2),VMIN(2),VPLS(2),WP(2),DATA(22),NAME(15,5),      TRAN 36
3     ANUM(15,5),PECWT(15),ENTH(15),FAZ(15),RTEMP(15),FCX(15),DENS(15), TRAN 37
4     RHOP,RMW(15),TLN,CR,OXF(15),ENNL,TRACE,LLMTS(10),SBOP(10,2)  TRAN 38
      COMMON /DOUBLE/ G(20,21), X(20)                    TRAN 39
      COMMON /INDX/IDEBUG,CONVG,TP,HP,SP,ISV,NPP,MOLES,NP,NT,NPT,NLM, TRAN 40
1     NS,KMAT,IMAT,IQ1,IOF,NOF,NOMIT,IP,NEWR,NSUB,NSUP,RKT,DETN,SHOCK, TRAN 41
2     IONS,NC,NSERT,JSOL,JLIQ,KASE,NREAC,IC,JS1,VOL,IT,CALCH,NLS,LOGV, TRAN 42
3     ISUP,ISUB,ITNUM,ITM,INCDZF,INCDEQ,CPRF,IPP,SEQ,PCPLT         TRAN 43
      COMMON /PERF/PCP(22),VMOC(13),SPIM(13),VACI(13),SUBAR(13),    TRAN 44
1     SUPAR(13),APP(13),AEAT(13),CSTR,EQL,FROZ,SSO,AREA,AWT,NFZ,   TRAN 45
2     APPL,ARATIO,ELN                                             TRAN 46
      COMMON /SAVED/SLN(100),IQSAVE,ENSAVE,ENLSAV,LSAVE,JSOLS,JLIQS, TRAN 47
1     LLL,LM,MAXNP,STORE(52,16),XS(20),WMOL(20),IND(20),NM,       TRAN 48
2     FIRSTP,FIRSTV                                              TRAN 49
      COMMON /TRANS/ TEM(100,20),TABLES(100,20,3),SPECIE(100,2,3), TRAN 50
1     OMEGA(20,20),ASTAR(20,20),BSTAR(20,20),CPRR(20),           TRAN 51
2     HRRT(20),ZROT(20),ZVIB(20),CVIBR(20),ROTM(20),RELXTN(20),   TRAN 52
3     ROTNM(80),STCF(17,20),STC(17,20),STCOEF(20),ANS(15),      TRAN 53
4     SPECE(2,3),NTT(100),NTAB(100),NR,N                       TRAN 54
      COMMON /INTERP/ Z(20),Y(20,3),NTP,ANSR(3)          TRAN 55
      COMMON /CONTRL/TRNSPT,FROZN,PUNCH,NODATA           TRAN 56
C                                                       TRAN 57
      DIMENSION ETA(20,20),DELH(17),CHECK(20)           TRAN 58
      DIMENSION GMAT(20,21),RTPD(20,20),STXS(20,20),XSKL(20,20)  TRAN 59
C                                                       TRAN 60
      EQUIVALENCE (ANS(1),VISC ), (ANS(2),MONCON), (ANS(3),INTCON) TRAN 61
      EQUIVALENCE (ANS(4),FRZCON), (ANS(5),REACON), (ANS(6),EQCON) TRAN 62
      EQUIVALENCE (ANS(7),CPFROZ), (ANS(8),CPEQ ), (ANS(9),PRFROZ) TRAN 63
      EQUIVALENCE (ANS(10),PREQ ), (ANS(11),LEWIS ), (ANS(12),WTMOL ) TRAN 64
      EQUIVALENCE (ANS(13),DENSTY), (ANS(14),CPREAC), (ANS(15),ENTLPY) TRAN 65
      EQUIVALENCE (EQL,EQLB) , (S,ETA) , (RTPD,OMEGA)       TRAN 66
      EQUIVALENCE (STXS,BSTAR) , (XSKL,ETA)                TRAN 67
C                                                       TRAN 68
      DATA PI/3.14159265/,AVGDRO/6.022169/,BOLTZ/1.380622/     TRAN 69
      DATA RPVT/82.0562/                                       TRAN 70
      DATA ND/4HLAST/                                          TRAN 71
C                                                       TRAN 72
      NAMELIST /MATRX/GMAT                                     TRAN 73
C                                                       TRAN 74
C      READ TRANSPORT AND RELAXATION DATA FROM TAPE 3         TRAN 75
C      SEARCH FOR AND STORE INTERACTIONS TO BE CONSIDERED     TRAN 76
C                                                       TRAN 77
      NK=1                                                     TRAN 78
13 REAC(3) ((SPECE(I,L),L=1,3),I=1,2),NTP,NTB,ROTN         TRAN 79
      IF(SPECE(1,1).EQ.ND) GO TO 10                           TRAN 80
      K=1                                                       TRAN 81
      DO 5 J=1,NS                                             TRAN 82
      DO 1 N=1,NPT                                           TRAN 83
      TESTEN=(1.E-7)/WM(N)                                     TRAN 84

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1	IF(EN(J,N).GT.TESTEN) GO TO 2	TRAN 85
	GO TO 5	TRAN 86
2	DO 4 I=1,3	TRAN 87
4	IF(SPECE(K,I).NE.SUB(J,I)) GO TO 5	TRAN 88
	GO TO 6	TRAN 89
5	CONTINUE	TRAN 90
	READ(3) (TEM(NK,I),(TABLES(NK,I,L),L=1,3),I=1,NTP)	TRAN 91
	GO TO 13	TRAN 92
6	K=2	TRAN 93
	DO 8 JJ=1,NS	TRAN 94
	DO 7 II=1,3	TRAN 95
7	IF(SPECE(K,II).NE.SUB(JJ,II)) GO TO 8	TRAN 96
	IF(EN(JJ,N).GT.TESTEN) GO TO 10	TRAN 97
8	CONTINUE	TRAN 98
	READ(3) (TEM(NK,I),(TABLES(NK,I,L),L=1,3),I=1,NTP)	TRAN 99
	GO TO 13	TRAN 100
10	DO 12 L=1,3	TRAN 101
	DO 12 I=1,2	TRAN 102
12	SPECIE(NK,I,L)=SPECE(I,L)	TRAN 103
	IF(SPECIE(NK,1,1).EQ.ND) GO TO 17	TRAN 104
	NTT(NK)=NTP	TRAN 105
	NTAB(NK)=NTR	TRAN 106
	ROTNM(NK)=ROTN	TRAN 107
	READ(3) (TEM(NK,I),(TABLES(NK,I,L),L=1,3),I=1,NTP)	TRAN 108
	NK=NK+1	TRAN 109
	IF(NK.GT.100) GO TO 19	TRAN 110
	GO TO 13	TRAN 111
19	WRITE(6,18)	TRAN 112
18	FORMAT(1F0,40X,5CTABLES OF TRANSPORT AND RELAXATION DATA ARE FILL	TRAN 113
	1ED)	TRAN 114
17	REWIND 3	TRAN 115
C		TRAN 116
C	START TRANSPORT CALCULATIONS	TRAN 117
C		TRAN 118
22	DO 3 N=1,NPT	TRAN 119
	IF(ISV.EQ.0.AND.MAXNP.GT.12) CALL OUT	TRAN 120
	IF(MAXNP.GT.51) CALL OUT	TRAN 121
	TT=TTT(N)	TRAN 122
	PP=PPP(N)	TRAN 123
C		TRAN 124
C	CALL INPUT	TRAN 125
		TRAN 126
	K=1	TRAN 127
	IF(TT.LE.TMID) K=2	TRAN 128
	DO 26 I=1,NM	TRAN 129
	J=IND(I)	TRAN 130
	CPRR(I)=(((COEF(K,5,J)*TT+COEF(K,4,J))*TT+COEF(K,3,J))*TT+	TRAN 131
	1 COEF(K,2,J))*TT+COEF(K,1,J)	TRAN 132
	HRRT(I) = (((COEF(K,5,J)/5.)*TT+COEF(K,4,J)/4.)*TT+COEF(K,3,J)/	TRAN 133
	1 3.)*TT+COEF(K,2,J)/2.)*TT+COEF(K,1,J)+COEF(K,6,J)/TT	TRAN 134
26	CONTINUE	TRAN 135
C		TRAN 136
C	CALCULATE VISCOSITY AND MONATOMIC THERMAL CONDUCTIVITY	TRAN 137
C		TRAN 138
	CONST = (5./16.)*SQRT(1.0E5*BOLTZ/(PI*AVGDRO))	TRAN 139
	DO 24 I=1,15	TRAN 140
24	ANS(I)=0.0	TRAN 141
	DO 25 I=1,NM	TRAN 142
	DO 25 J=1,NM	TRAN 143
	ETA(I,J)= CONST*SQRT(2.0*WMOL(I)*WMOL(J)*TT/(WMOL(I)+WMOL(J)))/	TRAN 144
	1 OMEGA(I,J)	TRAN 145
25	ETA(J,I)=ETA(I,J)	TRAN 146
	DO 27 I=1,NM	TRAN 147
	DO 27 J=1,NM	TRAN 148
	IF(I-J) 29,28,29	TRAN 149



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28 SUM=0.0 TRAN 150
   DO 30 K=1,NM TRAN 151
   IF(K-I) 31,30,31 TRAN 152
31 SUM=2.0*XS(I)*XS(K)*WMOL(I)*WMOL(K)*((5./3.)/ASTAR(I,K)+WMOL(K)/ TRAN 153
   1 WMOL(I))/(ETA(I,K)*(WMOL(I)+WMOL(K))**2)+SUM TRAN 154
30 CONTINUE TRAN 155
   G(I,J)=XS(I)**2/ETA(I,I)+SUM TRAN 156
   GO TO 27 TRAN 157
29 G(I,J)=-2.0*XS(I)*XS(J)*WMOL(I)*WMOL(J)*((5./3.)/ASTAR(I,J)-1.0)/ TRAN 158
   1 (ETA(I,J)*(WMOL(I)+WMOL(J))**2) TRAN 159
   G(J,I)=G(I,J) TRAN 160
27 CONTINUE TRAN 161
   K=NM+1 TRAN 162
   DO 32 I=1,NM TRAN 163
32 G(I,K)=XS(I) TRAN 164
   IMAT=NM TRAN 165
   DO 33 I=1,NM TRAN 166
   DO 33 J=1,K TRAN 167
33 GMAT(I,J)=G(I,J) TRAN 168
   CALL GAUSS TRAN 169
   DO 34 I=1,NM TRAN 170
   CHECK(I)=0.0 TRAN 171
   DO 35 J=1,NM TRAN 172
35 CHECK(I)=CHECK(I)+X(J)*GMAT(I,J) TRAN 173
   IF(ABS((CHECK(I)-XS(I))/XS(I))-0.0001) 34,36,36 TRAN 174
36 WRITE(6,37) NM,I,CHECK(I),XS(I) TRAN 175
37 FORMAT(1H1,31X,48HERROR IN GAUSS SOLUTION IN CALCULATING VISCOSITY TRAN 176
   1//3X,10HTHERE ARE 12,45H EQUATIONS AND THERE IS AN ERROR IN EQUAT TRAN 177
   2ICN 12,26H THE CALCULATED ANSWER IS F10.7,12H INSTEAD OF F10.7 TRAN 178
   3//50X,19HTHE MATRIX ARRAY IS/) TRAN 179
   WRITE(6,MATRX) TRAN 180
34 CCNTINUE TRAN 181
   DO 39 I=1,NM TRAN 182
39 VISC=VISC+XS(I)*X(I) TRAN 183
C TRAN 184
   DO 40 I=1,NM TRAN 185
   DO 40 J=1,NM TRAN 186
   IF(I-J) 42,41,42 TRAN 187
41 SUM=0.0 TRAN 188
   DO 43 K=1,NM TRAN 189
   IF(K-I) 44,43,44 TRAN 190
44 SUM=16.0*XS(I)*XS(K)*((7.5*WMOL(I)**2+6.25*WMOL(K)**2-3.0* TRAN 191
   1 WMOL(K)**2*BSTAR(I,K)+4.0*WMOL(I)*WMOL(K)*ASTAR(I,K)*WMOL(I)* TRAN 192
   2 WMOL(K))/(15.0*R*(WMOL(I)+WMOL(K))**3*ASTAR(I,K)*ETA(I,K))+SUM TRAN 193
43 CCNTINUE TRAN 194
   G(I,J)=16.0*XS(I)**2*WMOL(I)/(15.0*R*ETA(I,I))+SUM TRAN 195
   GO TO 40 TRAN 196
42 G(I,J)=-16.0*XS(I)*XS(J)*WMOL(I)**2*WMOL(J)**2*(13.75-3.0* TRAN 197
   1 BSTAR(I,J)-4.0*ASTAR(I,J))/(15.0*R*(WMOL(I)+WMOL(J))**3 TRAN 198
   2 *ASTAR(I,J)*ETA(I,J)) TRAN 199
   G(J,I)=G(I,J) TRAN 200
40 CONTINUE TRAN 201
   K=NM+1 TRAN 202
   DO 45 I=1,NM TRAN 203
45 G(I,K)=XS(I) TRAN 204
   CALL GAUSS TRAN 205
   DO 47 I=1,NM TRAN 206
47 MONCON=MONCON+4.0*XS(I)*X(I) TRAN 207
C TRAN 208
C CALCULATE INTERNAL THERMAL CCNDUCTIVITY TRAN 209
C TRAN 210
   DO 104 I=1,NM TRAN 211
   IF(CVIBR(I).EQ.0.0) CVIBR(I) = CPRR(I)-(2.5+0.5*ROTM(I)) TRAN 212
   RELXTN(I)=0.0 TRAN 213
   IF(ZROT(I).NE.0.) RELXTN(I)=0.5*ROTM(I)/ZROT(I) TRAN 214
   IF(ZVIB(I).NE.0.) RELXTN(I)=RELXTN(I)+CVIBR(I)/ZVIB(I) TRAN 215

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104	CCONTINUE	TRAN 216
	DC 53 I=1,NM	TRAN 217
	IF(CPRR(I).EQ.2.5) GO TO 53	TRAN 218
	SUM=0.0	TRAN 219
	DO 54 K=1,NM	TRAN 220
	IF(K-I) 55,54,55	TRAN 221
55	SUM=SUM+ASTAR(I,I)*ETA(I,I)*XS(K)*2.0*WMOL(K)/(ASTAR(I,K)*	TRAN 222
	1 ETA(I,K)*XS(I)*(WMOL(I)+WMOL(K)))	TRAN 223
54	CONTINUE	TRAN 224
	INTCON=INTCON+(1.2*ASTAR(I,I)*(CPRR(I)-2.5)-RELXTN(I)*	TRAN 225
	1 (2.5-1.2*ASTAR(I,I))**2/(0.5*PI+RELXTN(I)*(5.0/3.0+1.2*	TRAN 226
	2 ASTAR(I,I)/(CPRR(I)-2.5))) *R*ETA(I,I)/WMOL(I)/(1.0+SUM)	TRAN 227
53	CONTINUE	TRAN 228
	IF(NR.EQ.C) GO TO 91	TRAN 229
	IF(FRCZN) GO TO 91	TRAN 230
C		TRAN 231
E	CALCULATE REACTION HEAT CAPACITY AND THERMAL CONDUCTIVITY	TRAN 232
C		TRAN 233
	L=1+NR	TRAN 234
	SUM1=0.0	TRAN 235
	SUM2=0.0	TRAN 236
	DO 65 I=1,NR	TRAN 237
	DELH(I)=0.0	TRAN 238
	DO 66 K=1,NM	TRAN 239
66	DELH(I)=STC(I,K)*HRRT(K)+DELH(I)	TRAN 240
65	G(I,L)=DELH(I)	TRAN 241
	JJ=NM-1	TRAN 242
	DO 99 K=1,JJ	TRAN 243
	LL=K+1	TRAN 244
	DO 99 L=LL,NM	TRAN 245
	RTPD(K,L) = WMOL(K)*WMOL(L)/	TRAN 246
	1 (ASTAR(K,L)*ETA(K,L)*(WMOL(K)+WMOL(L)))	TRAN 247
	XSKL(K,L) = 1.0/(XS(K)*XS(L))	TRAN 248
	XSKL(L,K) = XSKL(K,L)	TRAN 249
99	RTPD(L,K) = RTPD(K,L)	TRAN 250
	DO 98 I=1,17	TRAN 251
	DO 98 J=1,20	TRAN 252
98	IF (ABS(STC(I,J)) > T.1.0E-6) STC(I,J) = 0.0	TRAN 253
	DO 67 I=1,NR	TRAN 254
	DO 67 J=1,NR	TRAN 255
	DO 68 K=1,JJ	TRAN 256
	LL=K+1	TRAN 257
	DO 68 L=LL,NM	TRAN 258
	STXS(K,L) = 0.0	TRAN 259
	IF ((STC(I,K).EQ.0.0).AND.(STC(I,L).EQ.0.0)) GO TO 68	TRAN 260
	IF ((STC(J,K).EQ.0.0).AND.(STC(J,L).EQ.0.0)) GO TO 68	TRAN 261
	STXS(K,L) = XSKL(K,L)*	TRAN 262
	1 (XS(L)*STC(I,K)-XS(K)*STC(I,L))*	TRAN 263
	2 (XS(L)*STC(J,K)-XS(K)*STC(J,L))	TRAN 264
	SUM1 = SUM1+STXS(K,L)	TRAN 265
	SUM2 = SUM2+RTPD(K,L)*STXS(K,L)	TRAN 266
68	CONTINUE	TRAN 267
	GMAT(I,J) = SUM2	TRAN 268
	SUM2=0.0	TRAN 269
	GMAT(J,I) = GMAT(I,J)	TRAN 270
	G(I,J) = SUM1	TRAN 271
	SUM1=C.0	TRAN 272
67	G(J,I)=G(I,J)	TRAN 273
	IMAT=NR	TRAN 274
	CALL GAUSS	TRAN 275
	DO 101 I=1,NR	TRAN 276
101	CPREAC=CPREAC+R*DELH(I)*X(I)	TRAN 277
C		TRAN 278
	L=1+NR	TRAN 279
	DO 57 I=1,NR	TRAN 280


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57 G(I,L)=DELH(I)
   JJ=NM-1
   DO 59 I=1,NR
   DO 59 J=I,NR
   G(I,J) = GMAT(I,J)
59 G(J,I)=G(I,J)
   CALL GAUSS
   DO 70 I=1,NR
   CHECK(I)=0.0
   DO 71 J=1,NR
71 CHECK(I)=CHECK(I)+X(J)*GMAT(I,J)
   IF(ABS((CHECK(I)-DELH(I))/DELH(I))-0.010) 70,72,72
72 WRITE(6,73) NR,I,CHECK(I),DELH(I)
73 FORMAT(1F1,31X,68HERROR IN GAUSS SOLUTION IN CALCULATING REACTION
   1THERMAL CONDUCTIVITY//3X,10HTHERE ARE 12,45H EQUATIONS AND THERE I
   2S AN ERROR IN EQUATION 12,26H THE CALCULATED ANSWER IS F10.7,
   312H INSTEAD OF F10.7//50X,19HTHE MATRIX ARRAY IS/)
   WRITE(6,MATRX)
70 CONTINUE
   DO 75 I=1,NR
75 REACON=REACON+R*DELH(I)*X(I)
   REACON = (3./5.)*REACON
C
C   CALCULATE OTHER ANSWERS
C
91 FRZCON=MONCON+INTCON
   EQCON=FRZCON+REACON
   DO 102 I=1,NM
   CPFROZ=CPFROZ+XS(I)*CPRR(I)
   ENTLPY=ENTLPY+XS(I)*HRRT(I)
102 WTMCL=WTMOL+XS(I)*WMCL(I)
   CPFROZ=CPFROZ*R/WTMOL
   CPREAC=CPREAC/WTMOL
   CPEQ=CPREAC+CPFROZ
   ENTLPY=R*TT*ENTLPY/WTMOL
   PRFROZ=VISC*CPFROZ/FRZCON
   PREQ=VISC*CPEQ/EQCON
   PREQ=VISC*CPEQ/EQCON
   DENSTY=(WTMOL*PP)/(RPVT*TT)
   IF(FRCZN.OR.NR.EQ.0) GO TO 105
   LEWIS=(REACON*CPFROZ)/(FRZCON*CPREAC)
105 CONTINUE
C
C   CALL OUT
C
3 CONTINUE
   RETURN
   END

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TRAN 281
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TRAN 326
TRAN 327
TRAN 328

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C
C   SUBROUTINE INPUT
C
C   BRINGS IN AND SORTS OUT INPUT FOR TRANSPORT CALCULATIONS
C
   DOUBLE PRECISION G,X
   INTEGER SUB,SPECIE,SPECE
   REAL MONCON,INTCON,LEWIS
   LOGICAL TRNSPT,FROZN,PUNCH,NODATA
INPT 1
INPT 2
INPT 3
INPT 4
INPT 5
INPT 6
INPT 7
INPT 8

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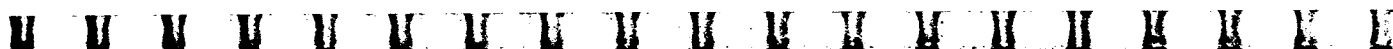
C		INPT	9
	COMMON /POINTS/HSUM(13),SSUM(13),CPR(13),DLVTP(13),CLVPT(13),	INPT	10
	1 GAMMAS(13),P(26),T(52),V(13),PPP(13),WM(13),SONVEL(13),TTT(13),	INPT	11
	2 VLM(13),TOTN(13)	INPT	12
	COMMON /SPECES/COEF(2,7,100),S(100),HO(100),DELN(100),DUMMY(100),	INPT	13
	1 EN(100,13),ENLN(100),A(10,100),SUB(100,3),IUSE(100),TEMP(50,2)	INPT	14
	COMMON /MISC/ENN,SUMN,TT,SO,ATOM(3,101),LLMT(10),BO(10),BOP(10,2),	INPT	15
	1 TM,TLOW,TMID,THIGH,PP,CPSUM,OF,EQRAT,FPCT,R,RR,HSUBO,AM(2),	INPT	16
	2 HPP(2),RH(2),VMIN(2),VPLS(2),WP(2),DATA(22),NAME(15,5),	INPT	17
	3 ANUM(15,5),PECWT(15),ENTH(15),FAZ(15),RTEMP(15),FCX(15),DENS(15),	INPT	18
	4 RHOP,RMW(15),TLN,CR,OXF(15),ENNL,TRACE,LLMTS(10),SBOP(10,2)	INPT	19
	COMMON /DOUBLE/ G(20,21), X(20)	INPT	20
	COMMON /INDX/IDEBUG,CONVG,TP,HP,SP,ISV,NPP,MOLES,NP,NT,NPT,NLM,	INPT	21
	1 NS,KMAT,IMAT,IQ1,IOF,NOF,NOMIT,IP,NEWNR,NSUB,NSUP,RKT,DETN,SHOCK,	INPT	22
	2 IONS,NC,NSERT,JSOL,JLIQ,KASE,NREAC,IC,JS1,VOL,IT,CALCH,NLS,LOGV,	INPT	23
	3 ISUP,ISUB,ITNUM,ITM,INCFZ,INCDEQ,CPRF,IPP,SEQ,PCPLT	INPT	24
	COMMON /PERF/PCP(22),VMOC(13),SPIM(13),VACI(13),SUBAR(13),	INPT	25
	1 SUPAR(13),APP(13),AEAT(13),CSTR,EQL,FROZ,SSO,AREA,AWT,NFZ,	INPT	26
	2 APPL,ARATIO,ELN	INPT	27
	COMMON /SAVED/SLN(100),IQSAVE,ENSAVE,ENLSAV,LSAVE,JSOLS,JLIQS,	INPT	28
	1 LLL,LM,MAXNP,STORE(52,16),XS(20),WMOL(20),IND(20),NM,	INPT	29
	2 FIRSTP,FIRSTV	INPT	30
	COMMON /TRANS/ TEM(100,20),TABLES(100,20,3),SPECIE(100,2,3),	INPT	31
	1 OMEGA(20,20),ASTAR(20,20),BSTAR(20,20),CPRR(20),	INPT	32
	2 HRRT(20),ZROT(20),ZVIB(20),CVIBR(20),ROTM(20),RELXTN(20),	INPT	33
	3 ROTNM(80),STCF(17,20),STC(17,20),STCOEF(20),ANS(15),	INPT	34
	4 SPECE(2,3),NTT(100),NTAB(100),NR,N	INPT	35
	COMMON /INTERP/ Z(20),Y(20,3),NTP,ANSR(3)	INPT	36
	COMMON /CONTRL/TRNSPT,FROZN,PUNCH,NODATA	INPT	37
C		INPT	38
	DIMENSION IATOM(3,101)	INPT	39
C		INPT	40
	EQUIVALENCE (ATOM,IATOM)	INPT	41
	EQUIVALENCE (ANS(1),VISC), (ANS(2),MONCON), (ANS(3),INTCON)	INPT	42
	EQUIVALENCE (ANS(4),FRZCON), (ANS(5),REACON), (ANS(6),EQCON)	INPT	43
	EQUIVALENCE (ANS(7),CPFROZ), (ANS(8),CPEQ), (ANS(9),PRFROZ)	INPT	44
	EQUIVALENCE (ANS(10),PREQ), (ANS(11),LEWIS), (ANS(12),WTMOL)	INPT	45
	EQUIVALENCE (ANS(13),DENSTY), (ANS(14),CPREAC), (ANS(15),ENTLPY)	INPT	46
C		INPT	47
	DATA MAXNM/20/,ND/4HLAST/,NBLANK/1H /	INPT	48
C		INPT	49
C		INPT	50
C	PICK OUT ELEMENTS	INPT	51
C		INPT	52
	IF(FROZN.AND.N.GT.NFZ) GO TO 92	INPT	53
	IF(FROZN.AND.MAXNP.GT.12) GO TO 92	INPT	54
	NSP=NS	INPT	55
	DO 1 J=1,NLM	INPT	56
	DO 2 I=1,NS	INPT	57
	IF(LLMT(J).NE.SUB(I,1)) GO TO 2	INPT	58
	SUMA=0.0	INPT	59
	DO 60 K=1,NLM	INPT	60
80	SUMA=SUMA+A(K,I)	INPT	61
	IF(SUMA.NE.1.) GO TO 2	INPT	62
	IND(J)=I	INPT	63
	GO TO 1	INPT	64
	2 CONTINUE	INPT	65
	WRITE(6,61) LLMT(J)	INPT	66
81	FORMAT(1H0,15X,58HNO ELEMENT WAS FOUND IN THE LIST OF SPECIES WITHIN	INPT	67
	1 THE NAME A3,45HOR ELSE THERE IS AN ERROR IN THE A(I,K) ARRAY)	INPT	68
	NSP=NSP+1	INPT	69
	IND(J) = NSP	INPT	70
	EN(NSP,N) = 0.0	INPT	71
	DO 3 K=1,NLM	INPT	72
3	A(K,NSP) = 0.0	INPT	73
	A(J,NSP) = 1.0	INPT	74

	SUB(NSP,1) = LLMT(J)	INPT 75
	SUB(NSP,2) = NBLANK	INPT 76
	SUB(NSP,3) = NBLANK	INPT 77
	1 CONTINUE	INPT 78
C		INPT 79
C	PICK OUT IMPORTANT SPECIES	INPT 80
C		INPT 81
	NM=NLM	INPT 82
	DO 4 I=1,NLM	INPT 83
	J=IND(I)	INPT 84
	EN(J,N)=-EN(J,N)	INPT 85
	4 CONTINUE	INPT 86
	TESTEN=(1.E-7)/WM(N)	INPT 87
	5 BIGEN=(1.E-7)/WM(N)	INPT 88
	DO 6 J=1,NSP	INPT 89
	IF(IUSE(J).NE.0) GO TO 6	INPT 90
	IF(EN(J,N).LT.BIGEN) GO TO 6	INPT 91
	BIGEN=EN(J,N)	INPT 92
	6 CONTINUE	INPT 93
	IF(BIGEN.EQ.TESTEN) GO TO 7	INPT 94
	DO 59 J=1,NSP	INPT 95
	IF (BIGEN.NE.EN(J,N)) GO TO 59	INPT 96
	EN(J,N)=-EN(J,N)	INPT 97
	NM=N+1	INPT 98
	IND(NM)=J	INPT 99
	59 CONTINUE	INPT 100
	IF(NM.LT.MAXNM) GO TO 5	INPT 101
	7 DO 8 I=1,NM	INPT 102
	J=IND(I)	INPT 103
	EN(J,N)=-EN(J,N)	INPT 104
	8 CONTINUE	INPT 105
C		INPT 106
C	CALCULATE MOLE FRACTIONS FROM THE EN(J,N)	INPT 107
C		INPT 108
	TOTAL=0.0	INPT 109
	DO 10 I=1,NM	INPT 110
	J=IND(I)	INPT 111
	XS(I)=EN(J,N)	INPT 112
	TOTAL=EN(J,N)+TOTAL	INPT 113
	10 CONTINUE	INPT 114
	DO 11 I=1,NM	INPT 115
	XS(I)=XS(I)/TOTAL	INPT 116
	DO 31 I=1,NM	INPT 117
	31 IF(XS(I).LT.1.E-10) XS(I)=1.E-10	INPT 118
C		INPT 119
C	CALCULATE MOLECULAR WEIGHTS	INPT 120
C		INPT 121
	DO 12 I=1,NM	INPT 122
	WMOL(I)=0.0	INPT 123
	12 CONTINUE	INPT 124
	DO 32 I=1,NLM	INPT 125
	DO 33 K=1,101	INPT 126
	IF(LLMT(I).EQ.IATOM(1;K)) GO TO 34	INPT 127
	33 CONTINUE	INPT 128
	34 DO 35 J=1,NM	INPT 129
	L=IND(J)	INPT 130
	WMOL(J)=WMOL(J)+ATOM(2,K)*A(I,L)	INPT 131
	35 CONTINUE	INPT 132
	32 CONTINUE	INPT 133
	92 CONTINUE	INPT 134
C		INPT 135
C	FIND TRANSPORT AND RELAXATION DATA FOR IMPORTANT INTERACTIONS	INPT 136
C		INPT 137
	DO 9 I=1,NM	INPT 138
	ZROT(I) = 0.0	INPT 139

B



ROTM(I) = 0.0	INPT 140
ZVIB(I) = 0.0	INPT 141
CVIBR(I) = 0.0	INPT 142
DO 9 J=1,NM	INPT 143
OMEGA(I,J)=0.0	INPT 144
9 CONTINUE	INPT 145
NK=0	INPT 146
18 NK=NK+1	INPT 147
IF(SPECIE(NK,1,1).EQ.ND) GO TO 22	INPT 148
K=1	INPT 149
14 DO 16 L=1,NM	INPT 150
J=IND(L)	INPT 151
DO 15 I=1,3	INPT 152
IF(SPECIE(NK,K,I).NE.SUB(J,I)) GO TO 16	INPT 153
15 CONTINUE	INPT 154
IF(K.EQ.2) GO TO 20	INPT 155
M=L	INPT 156
GO TO 17	INPT 157
16 CONTINUE	INPT 158
GO TO 18	INPT 159
17 JJ=J	INPT 160
DO 19 I=1,3	INPT 161
IF(SPECIE(NK,2,I).NE.SUB(J,I)) GO TO 24	INPT 162
19 CONTINUE	INPT 163
GO TO 20	INPT 164
24 K=2	INPT 165
GO TO 14	INPT 166
20 NTP=NTT(NK)	INPT 167
DO 39 I=1,NTP	INPT 168
Z(I)=TEM(NK,I)	INPT 169
DO 39 J=1,3	INPT 170
Y(I,J)=TABLES(NK,I,J)	INPT 171
39 CONTINUE	INPT 172
CALL LGRNGE(TT)	INPT 173
IF(NTAB(NK).EQ.1) GO TO 21	INPT 174
ROTM(M)=ROTNM(NK)	INPT 175
ZRCT(M)=ANSR(1)	INPT 176
ZVIB(M)=ANSR(2)	INPT 177
CVIBR(M)=ANSR(3)	INPT 178
GO TO 18	INPT 179
21 CONTINUE	INPT 180
OMEGA(L,M)=ANSR(1)	INPT 181
ASTAR(L,M)=ANSR(2)	INPT 182
BSTAR(L,M)=ANSR(3)	INPT 183
IF(J.EQ.JJ) GO TO 18	INPT 184
OMEGA(M,L)=OMEGA(L,M)	INPT 185
ASTAR(M,L)=ASTAR(L,M)	INPT 186
BSTAR(M,L)=BSTAR(L,M)	INPT 187
GO TO 18	INPT 188
C	INPT 189
C MAKE ESTIMATES FOR MISSING DATA	INPT 190
C	INPT 191
22 DO 27 I=1,NM	INPT 192
IF(OMEGA(I,I).NE.0.) GO TO 27	INPT 193
K=IND(I)	INPT 194
IF(XS(I).LT.5.0E-6) GO TO 36	INPT 195
IF(NODATA) GO TO 36	INPT 196
WRITE(6,28) (SUB(K,L),L=1,3)	INPT 197
28 FORMAT(1H0,40X,45HNO TRANSPORT DATA WERE FOUND FOR THE SPECIES 3A4	INPT 198
1).	INPT 199
36 CONTINUE	INPT 200
OMEGA(I,I) = ALOG (320.*WMOL(I)**4/TT**1.4)	INPT 201
IF (OMEGA(I,I).LT.1.) OMEGA(I,I) = 1.	INPT 202
ASTAR(I,I)=1.0	INPT 203
BSTAR(I,I)=1.0	INPT 204



27	CONTINUE	INPT 205
	NMM=NM-1	INPT 206
	DO 23 I=1,NMM	INPT 207
	K=I+1	INPT 208
	DO 23 J=K,NM	INPT 209
	IF(OMEGA(I,J).NE.0.) GO TO 26	INPT 210
	OMEGA(I,J)=(OMEGA(I,I)+OMEGA(J,J)+2.*SQRT(OMEGA(I,I)*OMEGA(J,J))	INPT 211
	/4.0	INPT 212
	ASTAR(I,J)=(ASTAR(I,I)+ASTAR(J,J))/2.	INPT 213
	BSTAR(I,J)=(BSTAR(I,I)+BSTAR(J,J))/2.	INPT 214
26	OMEGA(J,I)=OMEGA(I,J)	INPT 215
	ASTAR(J,I)=ASTAR(I,J)	INPT 216
	BSTAR(J,I)=BSTAR(I,J)	INPT 217
23	CONTINUE	INPT 218
	IF(FROZN) GO TO 96	INPT 219
C		INPT 220
C	REWRITE REACTIONS TO ELIMINATE TRACE SPECIES	INPT 221
C		INPT 222
	LL=NLM+1	INPT 223
	NR=NM-NLM	INPT 224
	IF(NR.EQ.0) GO TO 96	INPT 225
	DO 30 K=1,17	INPT 226
	DO 30 L=1,20	INPT 227
30	STC(K,L)=0.0	INPT 228
	K=1	INPT 229
	DO 62 I=LL,NM	INPT 230
	STC(K,I)=-1.0	INPT 231
	J=IND(I)	INPT 232
	DO 63 L=1,NLM	INPT 233
63	STC(K,L)=A(L,J)	INPT 234
	K=K+1	INPT 235
62	CONTINUE	INPT 236
	I=1	INPT 237
	NN=I	INPT 238
81	IF(XS(I).LT.1.0E-07) GO TO 97	INPT 239
98	I=I+1	INPT 240
	NN=I	INPT 241
	IF(I-NM) 81,81,96	INPT 242
97	L=1	INPT 243
	J=1	INPT 244
80	IF(ABS(STC(J,I)).GT.1.0E-06) GO TO 95	INPT 245
	DO 79 K=1,NM	INPT 246
79	STCF(L,K)=STC(J,K)	INPT 247
	L=L+1	INPT 248
	IF(J.GE.NR) GO TO 98	INPT 249
	J=J+1	INPT 250
	GO TO 80	INPT 251
95	COEFF=STC(J,I)	INPT 252
	DO 90 K=1,NM	INPT 253
90	STCOEF(K)=STC(J,K)/COEFF	INPT 254
	GO TO 77	INPT 255
84	J=J+1	INPT 256
	IF(ABS(STC(J,I)).LT.1.0E-06) GO TO 89	INPT 257
	COEFF=STC(J,I)	INPT 258
	DO 87 K=1,NM	INPT 259
87	STC(J,K)=(STC(J,K)/COEFF)-STCOEF(K)	INPT 260
89	DO 85 K=1,NM	INPT 261
85	STCF(L,K)=STC(J,K)	INPT 262
	L=L+1	INPT 263
77	IF(J.LT.NR) GO TO 84	INPT 264
	DO 82 I=1,NM	INPT 265
	DO 82 J=1,NR	INPT 266
82	STC(J,I)=STCF(J,I)	INPT 267
	I=NN	INPT 268
	NR=L-1	INPT 269
	GO TO 98	INPT 270



96 CONTINUE
RETURN
END

INPT 271
INPT 272
INPT 273

```
C      SUBROUTINE OUT                                OUT    1
C
C      SETS UP AND WRITES OUTPUT FOR TRANSPORT PROPERTIES OUT    2
C
C      DOUBLE PRECISION G,X                          OUT    3
C      INTEGER SUB,SPECIE,SPECE                      OUT    4
C      REAL MONCON,INTCON,LEWIS,INTRNL              OUT    5
C      LOGICAL TRNSPT,FROZN,PUNCH,NODATA            OUT    6
C      LOGICAL TP,HP,SP,DETN,SHOCK,RKT,EQL,VOL      OUT    7
C
C      COMMON /POINTS/HSUM(13),SSUM(13),CPR(13),DLVTP(13),DLVPT(13), OUT    8
1 GAMMAS(13),P(26),T(52),V(13),PPP(13),WM(13),SONVEL(13),TTT(13), OUT    9
2 VLM(13),TOTN(13)                                  OUT   10
C      COMMON /SPECES/COEF(2,7,100),S(100),HO(100),DELN(100),DUMMY(100), OUT  11
1 EN(100,13),ENLN(100),A(10,100),SUB(100,3),IUSE(100),TEMP(50,2) OUT  12
C      COMMON /MISC/ENN,SUMN,TT,SO,ATOM(3,101),LLMT(10),BC(10),BOP(10,2), OUT  13
1 TM,TLOW,TMID,THIGH,PP,CPSUM,DF,EQRAT,FPCT,R,RR,HSUBO,AM(2), OUT  14
2 HPP(2),RH(2),VMIN(2),VPLS(2),WP(2),DATA(22),NAME(15,5), OUT  15
3 ANUM(15,5),PECWT(15),ENTH(15),FAZ(15),RTEMP(15),FOX(15),DENS(15), OUT  16
4 RHOP,RMW(15),TLN,CR,OXF(15),ENNL,TRACE,LLMTS(10),SBOP(10,2) OUT  17
C      COMMON /DOUBLE/ G(20,21), X(20)              OUT  18
C      COMMON /INDX/IDEBUG,CONVG,TP,HP,SP,ISV,NPP,MOLES,NP,NT,NPT,NLM, OUT  19
1 NS,KMAT,IMAT,IQ1,IOF,NOF,NOMIT,IP,NEWR,NSUB,NSUP,RKT,DETN,SHOCK, OUT  20
2 IONS,NC,NSERT,JSOL,JLIQ,KASE,NREAC,IC,JS1,VOL,IT,CALCH,NLS,LOGV, OUT  21
3 ISUP,ISUB,ITNUM,ITM,INCDZF,INCDEQ,CPRF,IPP,SEQ,PCPLT OUT  22
C      COMMON /PERF/PCP(22),VMOC(13),SPIM(13),VACI(13),SUPAR(13), OUT  23
1 SUPAR(13),APP(13),AEAT(13),CSTR,EQL,FROZ,SSO,AREA,AWT,NFZ, OUT  24
2 APPL,ARATIO,ELN OUT  25
C      COMMON /SAVED/SLN(100),IQSAVE,ENSAVE,ENLSAV,LSAVE,JSOLS,JLIQS, OUT  26
1 LLL,LM,MAXNP,STORE(52,16),XSI(20),WMOL(20),IND(20),NM, OUT  27
2 FIRSTP,FIRSTV OUT  28
C      COMMON /TRANS/ TEM(100,20),TABLES(100,20,3),SPECIE(100,2,3), OUT  29
1 OMEGA(20,20),ASTAR(20,20),BSTAR(20,20),CPRR(20), OUT  30
2 HRRT(20),ZROT(20),ZVIB(20),CVIBR(20),ROTM(20),RELXTN(20), OUT  31
3 ROTNM(80),STCF(17,20),STC(17,20),STCOEF(20),ANS(15), OUT  32
4 SPECE(2,3),NTT(100),NTAB(100),NR,N OUT  33
C      COMMON /INTERP/ Z(20),Y(20,3),NTP,ANSR(3) OUT  34
C      COMMON /CONTRL/TRNSPT,FROZN,PUNCH,NODATA OUT  35
C
C      EQUIVALENCE (ANS(1),VISC ), (ANS(2),MONCON), (ANS(3),INTCON) OUT  36
C      EQUIVALENCE (ANS(4),FRZCON), (ANS(5),REACON), (ANS(6),EQCON ) OUT  37
C      EQUIVALENCE (ANS(7),CPFROZ), (ANS(8),CPEQ ), (ANS(9),PRFROZ) OUT  38
C      EQUIVALENCE (ANS(10),PREQ ), (ANS(11),LEWIS ), (ANS(12),WTMOL ) OUT  39
C      EQUIVALENCE (ANS(13),DENSTY), (ANS(14),CPREAC), (ANS(15),ENTLPY) OUT  40
C
C      ENTLPY = HSUBO*R OUT  41
C      ENTRPY = SO*R OUT  42
C      FPC = 100./(1.+OF) OUT  43
C      IF(N.NE.1) GO TO 134 OUT  44
C      IF(ISV.EQ.0.AND.MAXNP.GT.12) GO TO 134 OUT  45
C      IF(MAXNP.GT.51.OR.(LM.GT.52.AND.LM.LT.66)) GO TO 134 OUT  46
C      LM=1 OUT  47
C      IF(MAXNP.LT.1) MAXNP=0 OUT  48
C
C      OUT  49
C      OUT  50
C      OUT  51
C      OUT  52
C      OUT  53
C      OUT  54
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134	CONTINUE	OUT	55
	ITT= TT + 0.5	OUT	56
	IF(MAXNP.GT.51.OR.LM.GT.52) GO TO 127	OUT	57
	IF(ISV.NE.0) GO TO 123	OUT	58
	IF(MAXNP.GT.12) GO TO 127	OUT	59
	GO TO 124	OUT	60
C		OUT	61
C	STORE DATA	OUT	62
C		OUT	63
123	IF(MAXNP.EQ.0) FIRSTP = PP	OUT	64
	IF(MAXNP.EQ.0) FIRSTV = VLM(1)	OUT	65
	STORE(MAXNP+1,1)=TT	OUT	66
	DO 128 J=1,15	OUT	67
128	STORE(MAXNP+1,J+1)=ANS(J)	OUT	68
	MAXNP=MAXNP+1	OUT	69
	GO TO 132	OUT	70
127	IF(LM.GT.MAXNP) MAXNP=0	OUT	71
	IF(LM.GT.MAXNP) GO TO 104	OUT	72
129	LM=1	OUT	73
132	IF(LM.GT.MAXNP) GO TO 137	OUT	74
	ITT=STORE(LM,1)*0.5	OUT	75
	TT=STORE(LM,1)	OUT	76
	DO 131 K=1,15	OUT	77
131	ANS(K)=STORE(LM,K+1)	OUT	78
	IF(LM.GT.1) GO TO 104	OUT	79
124	IF(N.NE.1) GO TO 104	OUT	80
	IF(ISV.EQ.0.AND.LM.NE.1) GO TO 104	OUT	81
C		OUT	82
C	WRITE HEADING FOR DATA	OUT	83
C		OUT	84
	WRITE(6,1)	OUT	85
1	FORMAT(1H1)	OUT	86
	IF(MAXNP.LT.13) FIRSTP = PP	OUT	87
	IF(MAXNP.LT.13) FIRSTV = VLM(1)	OUT	88
	IF(DETN) GO TO 6	OUT	89
	IF(SHOCK) GO TO 7	OUT	90
	IF(RKT) GO TO 8	OUT	91
	IF(VOL) GO TO 3	OUT	92
	IF(TP) GO TO 2	OUT	93
	IF(HP) GO TO 4	OUT	94
	IF(SP) GO TO 5	OUT	95
3	IF(TP) WRITE(6,16)	OUT	96
16	FORMAT(1H0,38X,55HTRANSPORT PROPERTIES AT ASSIGNED TEMPERATURE AND	OUT	97
	1 VOLUME/)	OUT	98
	IF(TP) WRITE(6,20) OF,FPC,EQRAT,FIRSTV	OUT	99
20	FORMAT(1H0,12X,4H0/F=,F8.4,4X,13HPERCENT FUEL=,F8.4,4X,	OUT	100
	1 19HEQUIVALENCE RATIO= ,F7.4,4X,13HFIRST VOLUME=F8.2,	OUT	101
	2 1X,4HCC/G///)	OUT	102
	IF(TP) GO TO 155	OUT	103
	IF(SP) WRITE(6,17)	OUT	104
17	FORMAT(1H0,41X,51HTRANSPORT PROPERTIES AT ASSIGNED ENTROPY AND VOL	OUT	105
	UME/)	OUT	106
	IF(SP) GO TO 14	OUT	107
	WRITE(6,141)	OUT	108
141	FORMAT(1H0,46X,39HTRANSPORT PROPERTIES AT ASSIGNED VOLUME/)	OUT	109
	INTRNL = ENTLPY	OUT	110
	WRITE(6,15) OF,FPC,EQRAT,INTRNL	OUT	111
15	FORMAT(1H0,11X,4H0/F=,F8.4,4X,13HPERCENT FUEL=,F8.4,4X,	OUT	112
	1 19HEQUIVALENCE RATIO= ,F7.4,4X,16HINTERNAL ENERGY=F8.2,	OUT	113
	2 6H CAL/G ///)	OUT	114
	GO TO 155	OUT	115
	2 WRITE(6,140)	OUT	116
140	FORMAT(1H0,37X,57HTRANSPORT PROPERTIES AT ASSIGNED TEMPERATURE AND	OUT	117
	1 PRESSURE/)	OUT	118
	13 WRITE(6,147) OF,FPC,EQRAT,FIRSTP	OUT	119



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147 FORMAT (1H0,12X, 4H0/F=, F8.4,4X,13HPERCENT FUEL=,F8.4,4X, OUT 120
1 19HEQUIVALENCE RATIO= ,F7.4,4X,15HFIRST PRESSURE=F8.3, OUT 121
2 1X,3HATM///) OUT 122
GO TO 155 OUT 123
4 WRITE(6,142) OUT 124
142 FORMAT(1F0,44X,42HTRANSPORT PROPERTIES AT ASSIGNED PRESSURES/) OUT 125
WRITE(6,149) OF,FPC,EQRAT,ENTLTY OUT 126
149 FORMAT (1H0,15X, 4H0/F=, F8.4,4X,13HPERCENT FUEL=,F8.4,4X, OUT 127
1 19HEQUIVALENCE RATIO= ,F7.4,4X,9HENTHALPY=F8.1,6H CAL/G///) OUT 128
GO TO 155 OUT 129
5 WRITE(6,143) OUT 130
143 FORMAT(1F0,39X,53HTRANSPORT PROPERTIES AT ASSIGNED ENTROPY AND PREOUT 131
1SSURE/) OUT 132
14 WRITE(6,150) OF,FPC,EQRAT,ENTRPT OUT 133
150 FORMAT (1H0,15X, 4H0/F=, F8.4,4X,13HPERCENT FUEL=,F8.4,4X, OUT 134
1 19HEQUIVALENCE RATIO= ,F7.4,4X,8HENTROPY=F8.4,11H CAL/(G)(K)///)OUT 135
GO TO 155 OUT 136
6 WRITE(6,144) OUT 137
144 FORMAT(1F0,45X,41HTRANSPORT PROPERTIES OF THE DETCNATED GAS/) OUT 138
WRITE(6,151) OF,FPC,EQRAT,FIRSTP OUT 139
151 FORMAT (1H0,16X, 4H0/F=, F8.4,4X,13HPERCENT FUEL=,F8.4,4X, OUT 140
1 19HEQUIVALENCE RATIO= ,F7.4,4X,26HFIRST DETONATION PRESSURE= OUT 141
2 F8.3,1X,3HATM///) OUT 142
GO TO 155 OUT 143
7 IF (FROZN) GO TO 9 OUT 144
WRITE(6,154) OUT 145
154 FORMAT(1H0,27X,72HTRANSPORT PROPERTIES OF THE SHOCKED GAS ASSUMINGOUT 146
1 EQUILIBRIUM COMPOSITION/) OUT 147
GO TO 10 OUT 148
9 WRITE(6,157) OUT 149
157 FORMAT(1H0,27X,67HTRANSPORT PROPERTIES OF THE SHOCKED GAS ASSUMINGOUT 150
1 FROZEN COMPOSITION/) OUT 151
10 WRITE(6,152) OF,FPC,EQRAT,PPP(1) OUT 152
152 FORMAT (1H0,10X, 4H0/F=, F8.4,4X,13HPERCENT FUEL=,F8.4,4X, OUT 153
1 19HEQUIVALENCE RATIO= ,F7.4,4X,21HFIRST SHOCK PRESSURE=F9.4, OUT 154
2 1X,3HATM///) OUT 155
GO TO 155 OUT 156
8 IF (FROZN) GO TO 11 OUT 157
WRITE(6,156) OUT 158
156 FORMAT(1H0,21X,88HTRANSPORT PROPERTIES OF ROCKET EXHAUST ASSUMING OUT 159
1EQUILIBRIUM COMPOSITION DURING EXPANSION/) OUT 160
GO TO 12 OUT 161
11 WRITE(6,158) OUT 162
158 FORMAT(1H0,24X,83HTRANSPORT PROPERTIES OF ROCKET EXHAUST ASSUMING OUT 163
1FROZEN COMPOSITICN DURING EXPANSION/) OUT 164
IF(.NOT.EQL.AND.NFZ.NE.1) WRITE(6,159).NFZ OUT 165
159 FORMAT(56X,18HFROZEN AFTER POINT, 12 /) OUT 166
12 WRITE(6,153) OF,FPC,EQRAT,PPP(1) OUT 167
153 FORMAT (1H0,15X, 4H0/F=, F8.4,4X,13HPERCENT FUEL=,F8.4,4X, OUT 168
1 19HEQUIVALENCE RATIO= ,F7.4,4X,17HCHAMBER PRESSURE=F8.3, OUT 169
2 1X,3HATM///) OUT 170
155 CONTINUE OUT 171
IF(.NOT.FROZN) GO TO 105 OUT 172
WRITE(6,106) OUT 173
106 FORMAT (32X,4HTEMP,3X,9HVISCOSITY,2X,9HMONATOMIC,2X,8HINTERNAL,4X,OUT 174
16HFROZEN,6X,2HCP,8X,7HPRANDTL/52X,4HCOND,7X,4HCOND,7X,4HCOND,9X, OUT 175
24HFROZ,5X,4HFROZ//31X,5HDEG K,5X,5HPOISE,5X,27H----- CAL/(CM)(SEC)OUT 176
1(K) ----,5X,10HCAL/(G)(K)///) OUT 177
WRITE(6,107) ITT,(ANS(I),I=1,4),ANS(7),ANS(9) OUT 178
107 FORMAT(30X,I6,F9.0,5HX10-6,F6.0,5HX10-6,F6.0,5HX10-6,F6.0,5HX10-6,OUT 179
1F8.4,F10.4) OUT 180
GO TO 108 OUT 181
105 WRITE(6,109) OUT 182
109 FORMAT (2X,4HTEMP,3X,9HVISCOSITY,2X,9HMONATOMIC,2X,8HINTERNAL,4X, OUT 183
16HFROZEN,5X,8HREACTION,3X,11HEQUILIBRIUM,3X,2HCP,9X,2HCP,7X, OUT 184
27HPRANDTL,3X,7HPRANDTL,4X,5HLEWIS/22X,4HCOND,7X,4HCOND,7X,4HCOND, OUT 185

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	38X,4HCOND,8X,4HCOND,9X,4HFROZ,7X,2HEQ,6X,4HFROZ,7X,2HEQ,6X,	OUT	186
	46HNUMBER//1X,5HDEG K,5X,5HPOISE,5X,	OUT	187
	554H----- CAL/(CM)(SEC)(K) -----,7X,	OUT	188
	610HCAL/(G)(K),7X,25H ---- DIMENSIONLESS ----//)	OUT	189
C		OUT	190
C	WRITE DATA	OUT	191
C		OUT	192
	IF(LEWIS.EQ.0.) GO TO 135	OUT	193
	WRITE(6,110) ITT,(ANS(I),I=1,11)	OUT	194
110	FORMAT(16,F9.0,5HX10-6,F6.0,5HX10-6,F6.0,5HX10-6,F6.0,5HX10-6,	OUT	195
	1F7.0,5HX10-6,F7.0,5HX10-6,F8.4,4F10.4)	OUT	196
	GO TO 108	OUT	197
135	WRITE(6,136) ITT,(ANS(I),I=1,10)	OUT	198
136	FORMAT(16,F9.0,5HX10-6,F6.0,5HX10-6,F6.0,5HX10-6,F6.0,5HX10-6,	OUT	199
	1F7.0,5HX10-6,F7.0,5HX10-6,F8.4,3F10.4)	OUT	200
	GO TO 108	OUT	201
104	IF(.NOT.RKT) GO TO 200	OUT	202
	IF(LM.EQ.14.OR.LM.EQ.15) GO TO 201	OUT	203
	IF(RKT.AND.(LM.EQ.27.OR.LM.EQ.28)) GO TO 137	OUT	204
	IF(RKT.AND.(LM.EQ.40.OR.LM.EQ.41)) GO TO 137	OUT	205
	IF(RKT.AND.(LM.EQ.53.OR.LM.EQ.54)) GO TO 137	OUT	206
	GO TO 200	OUT	207
201	LLL=LLL+1	OUT	208
	GO TO 108	OUT	209
200	IF(LM-LLL) 112,111,112	OUT	210
111	WRITE(6,113)	OUT	211
113	FORMAT(1H0)	OUT	212
	LLL=LLL+5	OUT	213
112	IF(.NOT.FROZN) GO TO 115	OUT	214
	WRITE(6,116) ITT,(ANS(I),I=1,4),ANS(7),ANS(9)	OUT	215
116	FORMAT(30X,I6,F9.0,3F11.0,F13.4,F10.4)	OUT	216
	GO TO 108	OUT	217
115	IF(LEWIS.EQ.0.) GO TO 118	OUT	218
	WRITE(6,117) ITT,(ANS(I),I=1,11)	OUT	219
117	FORMAT(I6,F9.0,3F11.0,2F12.0,F13.4,4F10.4)	OUT	220
	GO TO 108	OUT	221
118	WRITE(6,119) ITT,(ANS(I),I=1,10)	OUT	222
119	FORMAT(I6,F9.0,3F11.0,2F12.0,F13.4,3F10.4)	OUT	223
108	LM=LM+1	OUT	224
	IF(MAXNP.GT.0) GO TO 132	OUT	225
133	CONTINUE	OUT	226
C		OUT	227
C	PUNCHED CARDS	OUT	228
C		OUT	229
	IF(.NOT.PUNCH) GO TO 137	OUT	230
	IF(RKT.AND.(LM.EQ.15.OR.LM.EQ.16)) GO TO 137	OUT	231
	IF(RKT.AND.(LM.EQ.28.OR.LM.EQ.29)) GO TO 137	OUT	232
	IF(RKT.AND.(LM.EQ.41.OR.LM.EQ.42)) GO TO 137	OUT	233
	IF(RKT.AND.(LM.EQ.54.OR.LM.EQ.55)) GO TO 137	OUT	234
	PUNCH 121, TT, PP, (ANS(I),I=1,13),FPC	OUT	235
121	FORMAT (F8.2,3X,E10.5,4F9.2,2F11.2/F9.5,F10.5,3F9.5,F11.5,3X,	OUT	236
	1 E10.5,2X,F8.4)	OUT	237
137	CONTINUE	OUT	238
C		OUT	239
	RETURN	OUT	240
	END	OUT	241



C	SUBROUTINE LGRNGE(ITT)	LGRN	1
C	COMMON /INTERP/ Z(20),Y(20,3),NTP,ANSR(3)	LGRN	2
C	DIMENSION A(10)	LGRN	3
C	EQUIVALENCE (XX,A(1)),(X0,A(2)),(X1,A(3)),(X2,A(4)),(X3,A(5)),	LGRN	4
C	1(Y0,A(6)),(Y1,A(7)),(Y2,A(8)),(Y3,A(9))	LGRN	5
C	IF(ITT-Z(2))10,10,11	LGRN	6
	10 MX=1	LGRN	7
	GO TO 51	LGRN	8
	11 IF(ITT-Z(NTP-1)) 12,12,13	LGRN	9
	13 MX=NTP-3	LGRN	10
	GO TO 51	LGRN	11
	12 K=NTP-1	LGRN	12
	DO 14 JA=2,K	LGRN	13
	IF(ITT-Z(JA))15,15,14	LGRN	14
	15 MX=JA-2	LGRN	15
	GO TO 51	LGRN	16
	14 CONTINUE	LGRN	17
	51 XX=ALOG(ITT+1.0)	LGRN	18
	DO 23 I=1,4	LGRN	19
	MXI=MX+I-1	LGRN	20
	23 A(I+1)=ALOG(Z(MXI)+1.0)	LGRN	21
	B1=((XX-X1)*(XX-X2)*(XX-X3))/(X0-X1)/(X0-X2)/(X0-X3)	LGRN	22
	B2=((XX-X0)*(XX-X2)*(XX-X3))/(X1-X0)/(X1-X2)/(X1-X3)	LGRN	23
	B3=((XX-X0)*(XX-X1)*(XX-X3))/(X2-X0)/(X2-X1)/(X2-X3)	LGRN	24
	B4=((XX-X0)*(XX-X1)*(XX-X2))/(X3-X0)/(X3-X1)/(X3-X2)	LGRN	25
	DO 8 J=1,3	LGRN	26
	DO 3 I=1,4	LGRN	27
	MXI=MX+I-1	LGRN	28
	3 A(I+5)=ALOG(Y(MXI,J)+1.0)	LGRN	29
	ANSWR=B1*Y0+B2*Y1+B3*Y2+B4*Y3	LGRN	30
	8 ANSR(J)=EXP(ANSWR)-1.0	LGRN	31
	RETURN	LGRN	32
	END	LGRN	33
		LGRN	34
		LGRN	35
		LGRN	36
		LGRN	37



APPENDIX D

SAMPLE PROBLEMS - INPUT AND OUTPUT

Case 51 - Input

```

REACTANTS
N 1.      H 4.      CL1.      C 4.      72.06      -70690.      S298.15      O
C 1.      H 1.86955C .0312565 .008415      18.58      -2999.082L798.15      F
AL1.
MG1.      C 1.      00      9.00C      0.0      S298.15      F
H 2.      G 1.      .16      -68317.4      L298.15      F

OMIT      ALH      AL20      AL202
OMIT      C2      C3      CCL
OMIT      CH      CH2      CH4      CN
OMIT      COCL2      CS2      CLCN      CL20
OMIT      C1O2      MGS      N2O      NS
OMIT      SCL      SCL2      S2CL2      SOCL
OMIT      SOCL2      SO2CL2      SO3
INSERT      AL203(L)
NAMELISTS
$INPT2 KASE=51, RKT=1, PSIA=F, P=500, NODATA=T
$RKTINP PCP=2.5,2.75,3,3.25,3.5,4,10,34.02285, 100,1000,10000
    
```

Case 51 - Output

```

REACTANTS
N 1.0000 H 4.0000 CL 1.0000 O 4.0000 -0.      72.0600      -70690.00      S 298.150      O -0.
C 1.0000 H 1.8696 O 0.0313 S 0.0084 -0.      18.5800      -2999.08      L 298.150      F -0.
AL 1.0000 -0.      -0.      -0.      -0.      9.0000      0.      S 298.150      F -0.
MG 1.0000 D 1.0000 -0.      -0.      00 -0.      0.2000      -0.      S 298.150      F -0.
H 2.0000 O 1.0000 -0.      -0.      -0.      0.1600      -68317.40      L 298.150      F -0.

OMIT      ALH      AL20      AL202
OMIT      C2      C3      CCL
OMIT      CH      CH2      CH4      CN
OMIT      COCL2      CS2      CLCN      CL20
OMIT      C1O2      MGS      N2O      NS
OMIT      SCL      SCL2      S2CL2      SOCL
OMIT      SOCL2      SO2CL2      SO3
INSERT      AL203(L)
NAMELISTS
$INPT2
KASE =          51,
I      =      0.      ,      0.      ,      0.      ,      0.      ,      0.      ,      0.      ,      0.      ,
0.      ,      0.      ,      0.      ,      0.      ,      0.      ,      0.      ,      0.      ,
0.      ,      0.      ,      0.      ,      0.      ,      0.      ,      0.      ,      0.      ,
0.      ,      0.      ,      0.      ,      0.      ,      0.      ,      0.      ,      0.      ,
0.      ,      0.      ,      0.      ,      0.      ,      0.      ,      0.      ,      0.      ,
0.      ,      0.      ,      0.      ,      0.      ,      0.      ,      0.      ,      0.      ,
P      =      5.0000000E+02,      0.      ,      0.      ,      0.      ,      0.      ,      0.      ,      0.      ,
0.      ,      0.      ,      0.      ,      0.      ,      0.      ,      0.      ,      0.      ,
0.      ,      0.      ,      0.      ,      0.      ,      0.      ,      0.      ,      0.      ,
0.      ,      0.      ,      0.      ,      0.      ,      0.      ,      0.      ,      0.      ,
PSIA =      T, MMHG =      F, NSQM =      F,
V      =      0.      ,      0.      ,      0.      ,      0.      ,      0.      ,      0.      ,      0.      ,
0.      ,      0.      ,      0.      ,      0.      ,      0.      ,      0.      ,      0.      ,
0.      ,      0.      ,      0.      ,      0.      ,      0.      ,      0.      ,      0.      ,
RHD =      5.0000000E+02,      0.      ,      0.      ,      0.      ,      0.      ,      0.      ,      0.      ,
0.      ,      0.      ,      0.      ,      0.      ,      0.      ,      0.      ,      0.      ,
0.      ,      0.      ,      0.      ,      0.      ,      0.      ,      0.      ,      0.      ,
0.      ,      0.      ,      0.      ,      0.      ,      0.      ,      0.      ,      0.      ,
ERATIU=      F, OF =      F, FPCT =      F, FA =      F,
MIX =      0.      ,      0.      ,      0.      ,      0.      ,      0.      ,      0.      ,      0.      ,
0.      ,      0.      ,      0.      ,      0.      ,      0.      ,      0.      ,      0.      ,
0.      ,      0.      ,      0.      ,      0.      ,      0.      ,      0.      ,      0.      ,
TP =      F, HP =      F, SP =      F, TV =      F, UV =      F, SV =      F,
RKT =      T, SHOCK =      F, DEIN =      F, OTTO =      F, CR =      0.      ,      SO =      0.      ,      SO =      0.      ,
IONS =      F, IDEBUG=      0, TRACE =      0.      ,      SIUNIT=      F, EUNITS=      F,
TRNSPI=      T, FRUZN =      F, PUNCH=      F, NODATA=      T,
$ END
NO INPT2 VALUE GIVEN FOR OF, ERAT, FA, OR FPCT
    
```



SPECIES BEING CONSIDERED IN THIS SYSTEM

J12/65 AL(S)	J12/65 AL(L)	J12/65 AL	J 6/70 ALCL	J 9/64 ALCL2
J 6/70 ALCL3(S)	J 6/70 ALCL3(L)	J 6/70 ALCL3	J12/62 ALN(S)	J 3/61 ALN
J 6/70 ALD	J 9/64 ALQCL	J12/67 ALOH	J12/68 ALD2	J12/68 ALD2H
J 6/70 AL2CL6	J 3/64 AL2O3(S)	J 3/64 AL2O3(L)	J 3/61 C(S)	J 3/61 C
J12/68 CCL2	J 6/70 CCL3	J 3/61 CH2O	J 6/69 CH3	J 6/66 CNN
J12/70 CM2	J 9/65 CO	J12/65 COCL	J 3/61 COS	J 9/65 CO2
J12/62 CS	J12/68 C2CL2	J 3/67 C2H	J 3/61 C2H2	J 9/65 C2H4
L 5/72 C2H6	J 3/67 C2N	J 3/61 C2V2	J 9/66 C2O	J 6/68 C3O2
J12/69 C4	J12/69 C5	J 3/61 CL	J 6/61 CLO	J 9/65 CL2
J 9/65 H	J 3/64 HALD	J 9/64 HCL	L12/69 HCN	J12/70 HCO
J12/70 HNCO	J 3/63 HNO	J 3/64 H2O	J 3/61 H2	L11/65 H2O(S)
L11/65 H2O(L)	J 3/61 H2O	L 2/69 H2O2	J12/65 H2S	J 9/62 H2S(S)
J 9/62 HGL(L)	J 9/62 HG	J 3/66 HGCL	J12/65 HGCL2(S)	J12/65 HGCL2(L)
J12/69 HGCL2	J12/66 MGH	J 3/64 MGN	J12/65 MGO(S)	J12/65 MGO(L)
J12/65 MGD	J 6/67 MGOH	J 6/67 MGO2H2	J12/71 MGS(S)	J 3/61 N
J12/70 NCO	J12/71 NH	J12/65 NH2	J 9/65 NH3	J 6/63 NO
J12/65 NOCL	J 9/64 NO2	J12/65 NO2CL	J12/64 NO3	J 9/65 N2
J12/65 N2H4	J 9/64 N2O4	J12/70 N3	J 6/62 O	J12/70 OH
J 9/65 O2	J 6/61 O3	J12/65 S(S)	J12/65 S(L)	J 6/71 S
J 6/67 SH	J 6/61 SN	J 6/71 SO	J 6/61 SO2	J12/65 S2

\$RKTIIP

eQL = T, FROZ = T,

SUBAR =	0.	0.	0.	0.	0.	0.	0.	0.
	0.	0.	0.	0.	0.	0.	0.	0.
	0.	0.	0.	0.	0.	0.	0.	0.
SUPAR =	0.	0.	0.	0.	0.	0.	0.	0.
	0.	0.	0.	0.	0.	0.	0.	0.
	0.	0.	0.	0.	0.	0.	0.	0.
PCP =	2.5000000E+00,	2.7500000E+00,	3.0000000E+00,	3.2500000E+00,	3.5000000E+00,	4.0000000E+00,		
	1.0000000E+01,	3.4022853E+01,	1.0000000E+02,	1.0000000E+03,	1.0000000E+04,	0.	0.	0.
	0.	0.	0.	0.	0.	0.	0.	0.
	0.	0.	0.	0.	0.	0.	0.	0.

NFZ = 1.

\$ END

OF = 2.579098

ENTHALPY	EFFECTIVE FUEL	EFFECTIVE OXIDANT	MIXTURE
(KG-MOL)(DEG K)/KG	HPP(2)	HPP(1)	HSUBO
	-3.92203147E+02	-0.30277923E+03	-0.24394427E+03
KG-ATOMS/KG	BOP(I,2)	BOP(I,1)	BO(I)
N	0.	0.85114220E-02	0.61333306E-02
H	0.85409148E-01	0.34045688E-01	0.48396638E-01
CL	0.	0.85114220E-02	0.61333306E-02
O	0.19127246E-02	0.34045688E-01	0.25067738E-01
C	0.45344284E-01	0.	0.12669193E-01
S	0.38157215E-03	0.	0.10661126E-03
AL	0.11938507E-01	0.	0.33356188E-02
MG	0.17757250E-03	0.	0.49613757E-04

PT	N	H	CL	O	C	S	AL	MG	
1	-13.569	-9.334	-20.870	-19.843	-11.590	-17.222	-19.688	-21.832	12.000
2	-13.684	-9.154	-21.372	-20.772	-11.369	-16.985	-21.017	-22.434	3.000
PC/PT= 1.769526	T = 2483.75								
2	-13.685	-9.155	-21.376	-20.779	-11.367	-16.983	-21.028	-22.439	2.000
PC/PT= 1.777143	T = 2481.97								
3	-13.751	-9.225	-21.709	-21.419	-11.185	-16.859	-21.952	-22.866	3.000
4	-13.769	-9.244	-21.806	-21.609	-11.127	-16.827	-22.228	-22.934	3.000
4	-13.779	-9.254	-21.789	-21.545	-11.179	-16.842	-22.136	-22.951	3.000
5	-13.823	-9.297	-21.833	-21.545	-11.266	-16.854	-22.136	-22.952	3.000
6	-13.863	-9.337	-21.873	-21.546	-11.346	-16.866	-22.135	-22.953	2.000
7	-13.903	-9.374	-21.910	-21.546	-11.420	-16.878	-22.135	-22.953	2.000
7	-13.888	-9.363	-21.931	-21.624	-11.356	-16.858	-22.271	-23.006	2.000
8	-13.913	-9.390	-22.070	-21.900	-11.271	-16.813	-22.745	-23.193	3.000
9	-14.086	-9.571	-23.143	-24.101	-10.505	-16.605	-26.548	-24.720	4.000
10	-14.323	-9.814	-24.931	-28.000	-8.957	-16.582	-33.289	-27.498	4.000
10	-14.324	-9.815	-24.924	-27.990	-8.963	-16.581	-33.267	-27.788	3.000
11	-14.555	-10.040	-26.870	-32.455	-7.060	-16.744	-40.922	-33.493	4.000
12	-15.152	-10.583	-32.489	-45.990	-0.912	-17.604	-63.504	-50.483	5.000
12	-15.163	-10.598	-32.338	-45.514	-1.232	-17.568	-62.828	-49.968	3.000
13	-16.122	-11.577	-35.546	-51.136	-1.072	-17.937	-74.386	-58.615	5.000

THEORETICAL ROCKET PERFORMANCE ASSUMING EQUILIBRIUM COMPOSITION DURING EXPANSION

PC = 500.0 PSIA
CASE NO. 31

CHEMICAL FORMULA				WT FRACTION (SEE NOTE)	ENERGY CAL/MOL	STATE	TEMP DEG K	DENSITY G/CC
OXIDANT N	1.00000	H	4.00000	CL	1.00000	O	4.00000	
FUEL C	1.00000	H	1.86955	O	0.03126	S	0.00841	
FUEL AL	1.00000							
FUEL MG	1.00000	O	1.00000					
FUEL H	2.00000	O	1.00000					

O/F = 2.5791 PERCENT FUEL = 27.9400 EQUIVALENC RATIO = 1.9479 REACTANT DENSITY = 0.

CHAMBER	THRUAT	EXIT	EXIT	EXIT	EXIT	EXIT	EXIT	EXIT	EXIT	EXIT	EXIT	EXIT	EXIT	EXIT
PC/P	1.0000	1.7771	2.5000	2.7500	3.0000	3.2500	3.5000	4.0000	10.000	34.023	100.00	1000.00	10000.0	
P, ATM	34.023	19.145	13.609	12.372	11.341	10.469	9.7208	8.5057	3.4023	1.0000	0.3402	0.0340	0.0034	0.0034
T, DEG K	2727	2482	2341	2315	2315	2315	2299	2246	1900	1504	1222	800	688	
RHO, G/CC	3.5172-3	2.1804-3	1.6450-3	1.5123-3	1.3862-3	1.2795-3	1.1963-3	1.0720-3	5.0741-4	1.8841-4	7.8929-5	1.2086-5	1.4933-6	
H, CAL/G	-484.8	-613.2	-683.7	-702.6	-719.8	-735.7	-750.4	-776.3	-938.5	-1115.9	-1241.0	-1435.5	-1576.9	
S, CAL/(G)(K)	2.5272	2.5272	2.5272	2.5272	2.5272	2.5272	2.5272	2.5272	2.5272	2.5272	2.5272	2.5272	2.5272	

MOLE FRACTIONS

ALCL	0.00019	0.00004	0.00002	0.00001	0.00001	0.00001	0.00001	0.00001	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000
ALCL2	0.00049	0.00018	0.00009	0.00008	0.00008	0.00008	0.00007	0.00005	0.00005	0.00000	0.00000	0.00000	0.00000	0.00000
ALCL3	0.00006	0.00004	0.00002	0.00002	0.00002	0.00002	0.00002	0.00002	0.00002	0.00000	0.00000	0.00000	0.00000	0.00000
ALCL4	0.00008	0.00002	0.00001	0.00001	0.00001	0.00001	0.00001	0.00001	0.00001	0.00000	0.00000	0.00000	0.00000	0.00000
ALOH	0.00001	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000
ALOH2	0.00002	0.00001	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000
AL2O3(S)	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000
AL2O3(L)	0.03674	0.03710	0.03721	0.03718	0.03718	0.03718	0.03718	0.03718	0.03718	0.03718	0.03718	0.03718	0.03718	0.03718
C(S)	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000
CO	0.26412	0.26332	0.26249	0.26220	0.26229	0.26227	0.26215	0.26172	0.25750	0.24736	0.23225	0.17345	0.07536	0.00000
CO2	0.00005	0.00005	0.00006	0.00006	0.00006	0.00006	0.00006	0.00006	0.00006	0.00006	0.00005	0.00003	0.00002	0.00000
C2O2	0.01814	0.01957	0.02065	0.02087	0.02086	0.02086	0.02100	0.02150	0.02600	0.03613	0.05103	0.10718	0.14921	0.00000
CS	0.00001	0.00001	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000
CL	0.00171	0.00087	0.00054	0.00050	0.00052	0.00054	0.00052	0.00042	0.00008	0.00000	0.00000	0.00000	0.00000	0.00000
H	0.00597	0.00295	0.00180	0.00166	0.00173	0.00180	0.00172	0.00139	0.00024	0.00001	0.00000	0.00000	0.00000	0.00000
HCL	0.13146	0.13342	0.13410	0.13419	0.13416	0.13413	0.13418	0.13437	0.13497	0.13560	0.13702	0.13716	0.13716	0.13716
HCN	0.00001	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000
HCO	0.00001	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000
H2	0.32172	0.37472	0.32632	0.32661	0.32659	0.32657	0.32675	0.32739	0.33228	0.34234	0.35701	0.41045	0.39641	0.39641
H2O	0.14672	0.14552	0.14458	0.14438	0.14435	0.14433	0.14419	0.14374	0.13949	0.12910	0.11331	0.05974	0.07377	0.07377
H2S	0.00140	0.00166	0.00181	0.00183	0.00181	0.00178	0.00179	0.00185	0.00216	0.00231	0.00233	0.00235	0.00237	0.00237
MG	0.00052	0.00001	0.00000	0.00000	0.00000	0.00001	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000
MGCL	0.00003	0.00001	0.00001	0.00001	0.00001	0.00001	0.00001	0.00001	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000
MGCL2	0.00102	0.00107	0.00109	0.00109	0.00109	0.00109	0.00109	0.00109	0.00111	0.00083	0.00007	0.00000	0.00000	0.00000
MG(O)	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000
MG(OH)	0.00003	0.00001	0.00001	0.00001	0.00001	0.00001	0.00001	0.00001	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000
MG(OH2)	0.00001	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000
NH3	0.00001	0.00001	0.00001	0.00001	0.00001	0.00001	0.00001	0.00001	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000
NO	0.00003	0.00001	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000
N2	0.06831	0.06848	0.06854	0.06855	0.06855	0.06854	0.06855	0.06857	0.06863	0.06863	0.06863	0.06863	0.06863	0.06863
O	0.00001	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000
OH	0.00071	0.00027	0.00013	0.00012	0.00012	0.00013	0.00012	0.00009	0.00001	0.00000	0.00000	0.00000	0.00000	0.00000
S	0.00009	0.00005	0.00003	0.00003	0.00003	0.00003	0.00003	0.00003	0.00003	0.00003	0.00003	0.00003	0.00003	0.00003
SH	0.00035	0.00041	0.00033	0.00031	0.00032	0.00033	0.00033	0.00029	0.00010	0.00001	0.00000	0.00000	0.00000	0.00000
SO	0.00016	0.00010	0.00007	0.00006	0.00007	0.00007	0.00007	0.00006	0.00001	0.00000	0.00000	0.00000	0.00000	0.00000
SO2	0.00007	0.00005	0.00004	0.00004	0.00004	0.00004	0.00004	0.00004	0.00004	0.00004	0.00004	0.00004	0.00004	0.00004
S2	0.00003	0.00003	0.00003	0.00003	0.00003	0.00003	0.00003	0.00003	0.00002	0.00000	0.00000	0.00000	0.00000	0.00000

ADDITIONAL PRODUCTS WHICH WERE CONSIDERED BUT WHUSE MOLE FRACTIONS WERE LESS THAN 0.50000E-05 FOR ALL ASSIGNED CONDITIONS

AL(S)	AL(L)	AL	ALCL3(S)	ALCL3(L)	ALN(S)	ALN	ALO	ALO2	AL2CL6
C	CCL2	CCL3	CH2O	CH3	CNN	CN2	COCL	C2LL2	C2H
C2H2	C2H4	C2H6	C2N	C2N2	C2O	C3O2	C4	C5	CLO
CL2	HALO	HNGO	HNO	H2O	H2O(S)	H2O(L)	H2O2	HG(S)	HG(L)
MGCL2(S)	MGCL2(L)	MGN	MGN	MG(O)	MG(O)	MGS(S)	M	NCU	NH
NH2	NOCL	NO2	NO2CL	NO3	N2H4	N2O4	N3	O2	O3
S(S)	S(L)	SN							

NOTE. WEIGHT FRACTION OF FUEL IN TOTAL FULLS AND OF OXIDANT IN TOTAL OXIDANTS

TRANSPORT PROPERTIES OF ROCKET EXHAUST ASSUMING EQUILIBRIUM COMPOSITION DURING EXPANSION

O/F= 2.5791 PERCENT FUEL= 27.9400 EQUIVALENCE RATIO= 1.9479 CHAMBER PRESSURE= 34.023 ATM

TEMP DEG K	VISCOACITY POISE	MONATOMIC COND	INTERNAL COND	FROZEN COND	REACTION COND	EQUILIBRIUM COND	CP FROZ	CP EQ	PRANDTL FKOZ	PRANDTL EQ	LEWIS NUMBER
		CAL/(CM)(SEC)(K)				CAL/(G)(K)		---- DIMENSIONLESS ----			
2727	778.X10-6	414.X10-6	380.X10-6	795.X10-6	377.X10-6	1171.X10-6	0.4965	0.5992	0.4859	0.3978	2.2923
2482	725.	385.	344.	729.	208.	977.	0.4903	0.5528	0.4880	0.4282	2.2369
2341	695.	369.	322.	691.	137.	828.	0.4862	0.5303	0.4892	0.4456	2.1757
2315	690.	366.	318.	684.	128.	812.	0.4854	0.5272	0.4893	0.4480	2.1613
2315	690.	366.	318.	684.	133.	818.	0.4854	0.5290	0.4893	0.4464	2.1651
2315	690.	366.	318.	685.	138.	823.	0.4854	0.5307	0.4893	0.4449	2.1686
2299	687.	364.	316.	680.	134.	814.	0.4849	0.5290	0.4894	0.4462	2.1601
2246	675.	358.	308.	666.	111.	777.	0.4832	0.5213	0.4898	0.4527	2.1205
1900	599.	319.	254.	573.	27.	601.	0.4704	0.4851	0.4912	0.4836	1.5213
1504	507.	274.	194.	468.	11.	479.	0.4522	0.4677	0.4896	0.4949	0.6759
1222	437.	241.	152.	393.	18.	411.	0.4370	0.4682	0.4855	0.4974	0.6391
800	322.	190.	100.	290.	44.	344.	0.4133	0.5094	0.4585	0.4906	0.6528
688	287.	174.	90.	264.	56.	320.	0.4084	0.5450	0.4444	0.4893	0.6339

THEORETICAL ROCKET PERFORMANCE ASSUMING FROZEN COMPOSITION DURING EXPANSION

PC = 500.0 PSIA
CASE NO. 51

CHEMICAL FORMULA	WT FRACTION (SEE NOTE)	ENERGY CAL/MOL	STATE	TEMP DEG K	DENSITY G/CC
OXIDANT N 1.00000	1.00000	-70690.000	S	298.15	-0.
FUEL C 1.00000	0.66500	-2999.082	L	298.15	-0.
FUEL AL 1.00000	0.32212	0.	S	298.15	-0.
FUEL MG 1.00000	0.00716	-143690.881	S	298.15	-0.
FUEL H 2.00000	0.00573	-68317.400	L	298.15	-0.

O/F= 2.5791 PERCENT FUEL= 27.9400 EQUIVALENCE RATIO= 1.9479 REACTANT DENSITY= 0.

	CHAMBER	THROAT	EXIT
PC/P	1.0000	1.7885	2.5000
P, ATM	34.023	19.023	13.609
T, DEG K	2727	2451	2303
RHO, G/CC	3.5172-3	2.1887-3	1.6664-3
H, CAL/G	-484.8	-613.9	-682.3
S, CAL/(G)(K)	2.5272	2.5272	2.5272
M, MOL WT	23.135	23.135	23.135
CP, CAL/(G)(K)	0.4697	0.4636	0.4599
GAMMA (S)	1.2238	1.2274	1.2296
SON VEL, M/SEC	1095.2	1039.7	1008.7
MACH NUMBER	0.	1.000	1.275
AE/AT	1.0000	1.1683	
CSTAR, FT/SEC		4970	4970
CF		0.686	0.849
IVAC, LB-SEC/LB		192.4	196.7
ISP, LB-SFC/LB		106.0	131.1

MOLE FRACTIONS

ALCL	0.00019	ALCL2	0.00049	ALCL3	0.00006	ALOCCL	0.00008
ALOH	0.00001	ALOH	0.00002	AL2O3(L)	0.03674	CO	0.26412
COS	0.00005	CO2	0.01814	CS	0.00001	CL	0.00171
H	0.00597	HCL	0.13146	HEN	0.00001	HCO	0.00001
H2	0.32172	H2O	0.14672	H2S	0.00140	MG	0.00002
MGCL	0.00003	MGCL2	0.00102	MGDH	0.00003	MGO2H2	0.00001
NH3	0.00001	NO	0.00003	N2	0.06831	O	0.00001
OH	0.00071	S	0.00009	SH	0.00055	SO	0.00016
SO2	0.00007	S2	0.00003				

ADDITIONAL PRODUCTS WHICH WERE CONSIDERED BUT WHOSE MOLE FRACTIONS WERE LESS THAN 0.50000E-05 FOR ALL ASSIGNED CONDITIONS

AL(S)	AL(L)	AL	ALCL3(S)	ALCL3(L)	ALN(S)	ALN	ALO	ALO2	AL2CL6
AL2O3(S)	C(S)	C	CCL2	CCL3	CH2(S)	CH3	CNN	CN2	COCL
C2CL2	C2H	C2H2	C2H4	C2H6	C2N	C2N2	C2O	C3O2	C4
C5	CLD	CL2	HALO	HNCO	HNO	H2O	H2O(S)	H2O(L)	H2O2
MG(S)	MG(L)	MGCL2(S)	MGCL2(L)	MGN	MGN	MG(S)	MG(L)	MG	MGS(S)
N	NCO	NH	NH2	NOCL	NO2	NO2CL	NO3	N2H4	N2O4
N3	O2	O3	S(S)	S(L)	SN				

NOTE. WEIGHT FRACTION OF FUEL IN TOTAL FUELS AND OF OXIDANT IN TOTAL OXIDANTS

TRANSPORT PROPERTIES OF ROCKET EXHAUST ASSUMING FROZEN COMPOSITION DURING EXPANSION

O/F= 2.5791 PERCENT FUEL= 27.9400 EQUIVALENCE RATIO= 1.9479 CHAMBER PRESSURE= 34.023 ATM

TEMP DEG K	VISCOACITY POISE	MONATOMIC COND	INTERNAL COND	FROZEN COND	CP FROZ	PRANDTL FRGZ
		CAL/(CM)(SEC)(K)			CAL/(G)(K)	
2727	778.X10-6	414.X10-6	380.X10-6	795.X10-6	0.4965	0.4859
2451	720.	384.	338.	722.	0.4893	0.4878
2303	688.	367.	315.	682.	0.4848	0.4891

Case 52 - Input

```

REACTANTS
H 2.      00      100.  0.      G298.15 F
O 2.      00      100.0 0.0     G298.15 0

NAMELISTS
$INPT2 KASE=52,DETN=1,ERATIO=T,MIX=1,T=298.15,500,P=1
  
```

Case 52 - Output

```

REACTANTS
H 2.0000  -0.      -0.      -0.      00 -0.      100.0000      0.  G  298.150  F -0.
O 2.0000  -0.      -0.      -0.      00 -0.      100.0000      0.  G  298.150  0  -0.

NAMELISTS
$INPT2
KASE = 52,
I = 2.9815000E+02, 5.0000000E+02, 0., 0., 0., 0., 0., 0., 0., 0.,
    0., 0., 0., 0., 0., 0., 0., 0., 0., 0.,
    0., 0., 0., 0., 0., 0., 0., 0., 0.,
    0., 0., 0., 0., 0., 0., 0., 0., 0.,
    0., 0., 0., 0., 0., 0., 0., 0., 0.,
    0., 0., 0., 0., 0., 0., 0., 0., 0.,
P = 1.0000000E+00, 0., 0., 0., 0., 0., 0., 0., 0., 0.,
    0., 0., 0., 0., 0., 0., 0., 0., 0.,
    0., 0., 0., 0., 0., 0., 0., 0., 0.,
    0., 0., 0., 0., 0., 0., 0., 0., 0.,
P SIA = F, MMHG = F, NSQM = F,
V = 0., 0., 0., 0., 0., 0., 0., 0., 0., 0.,
    0., 0., 0., 0., 0., 0., 0., 0., 0.,
RHO = 1.0000000E+00, 0., 0., 0., 0., 0., 0., 0., 0., 0.,
      0., 0., 0., 0., 0., 0., 0., 0., 0.,
      0., 0., 0., 0., 0., 0., 0., 0., 0.,
      0., 0., 0., 0., 0., 0., 0., 0., 0.,
ERATIO= T, OF = F, GPCT = F, FA = F,
MIX = 1.0000000E+00, 0., 0., 0., 0., 0., 0., 0., 0., 0.,
      0., 0., 0., 0., 0., 0., 0., 0., 0.,
      0., 0., 0., 0., 0., 0., 0., 0., 0.,
TP = F, HP = F, SP = F, TV = F, UV = F, SV = F,
RKT = F, SMUCK = F, DETN = T, OTTO = F, CR = 0., SO = 0., SO = 0.,
IDNS = F, IDEBUG= 0, TRACE = 0., SIUNIT= F, EUNITS= F,
TRANSPT= T, FROZN = F, PUNCH = F, NODATA= F,
$ END

SPECIES BEING CONSIDERED IN THIS SYSTEM
J 9/65 H J 3/64 HD2 J 3/61 H2 L11/65 H2O(S) L11/65 H2O(L)
J 3/61 H2O L 2/69 H2O J 6/62 O J12/70 OH J 9/65 O2
J 6/61 O3

OF = 7.936411
ENTHALPY EFFECTIVE FULL EFFECTIVE OXIDANT MIXTURE
(KG-MOL)(DES K)/KG HPP(2) HPP(1) HSUBO
0. 0. 0. 0.

KG-ATOMS/KG HOP(I,2) BOP(I,1) BO(I)
H 0.99209300E+00 0. 0.11101694E+00
O 0. 0.62502343E-01 0.55508222E-01

DETONATION VELOCITY CALCULATIONS
PT H O
1 -10.312 -15.661 8.000
T EST.= 3611.38
      P/P1 T/T1
      0 0.15000000E+02 0.12112625E+02

PT H O
1 -10.228 -15.582 3.000
PT H O
1 -10.224 -15.583 3.000
PT H O
1 -10.274 -15.583 2.000
2 -10.377 -15.692 6.000

T EST.= 3729.78
      P/P1 T/T1
      0 0.15000000E+02 0.74575531E+01
2 -10.434 -15.790 3.000
2 -10.441 -15.789 3.000
2 -10.441 -15.788 2.000
  
```

DEFONATION PROPERTIES OF AN IDEAL REACTING GAS

CASE NO. 52

	CHEMICAL FORMULA	WT FRACTION (SEE NOTE)	ENERGY CAL/MOL	STATE	TEMP DEG K	DENSITY G/CC
FUEL	H 2.00000	1.00000	1405.408	G	500.00	-0.
OXIDANT	O 2.00000	1.00000	1455.140	G	500.00	-0.

O/F= 7.9364 PERCENT FUEL= 11.1902 EQUIVALENCE RATIO= 1.0000 REACTANT DENSITY= 0.

UNBURNED GAS

P1, ATM	1.0000	1.0000
T1, DEG K	298.15	500.00
H1, CAL/G	0.	118.40
M1, MOL WT	12.010	12.010
GAMMA1	1.4015	1.3856
SON VEL, M/SEC	537.8	692.5

BURNED GAS

P2, ATM	18.844	10.998
T2, DEG K	3683	3607
RHO2, G/CC	9.0261-4	5.2888-4
H2, CAL/G	679.5	760.9
S2, CAL/(G)(K)	4.1589	4.2558
M2, MOL WT	14.474	14.235
(DLV/DLP)F	-1.08305	-1.08990
(DLV/DLT)P	2.3791	2.5176
CP2, CAL/(G)(K)	3.9365	4.3702
GAMMA (S)	1.1291	1.1268
SON VEL, M/SEC	1545.5	1540.9

DEFONATION PARAMETERS

P/P1	18.844	10.998
T/T1	12.352	7.215
M/M1	1.2052	1.1852
RHO/RHO1	1.8386	1.8067
MACH NO.	5.2833	4.0199
DET VEL, M/SEC	2841.5	2783.9

MOLE FRACTIONS

H	0.08139	0.09230
H02	0.00011	0.00009
H2	0.16475	0.16935
H2O	0.53045	0.50628
H2O2	0.00002	0.00002
O	0.03886	0.04365
OH	0.13496	0.13663
O2	0.04945	0.05169

ADDITIONAL PRODUCTS WHICH WERE CONSIDERED BUT WHOSE MOLE FRACTIONS WERE LESS THAN 0.50000E-05 FOR ALL ASSIGNED CONDITIONS

H2O(S) H2O(L) O3

NOTE. WEIGHT FRACTION OF FUEL IN TOTAL FUELS AND OF OXIDANT IN TOTAL OXIDANTS

NO TRANSPORT DATA WAS FOUND FOR THE SPECIES H02

NO TRANSPORT DATA WAS FOUND FOR THE SPECIES H2O2

TRANSPORT PROPERTIES OF THE DEFONATED GAS

O/F= 7.9364 PERCENT FUEL= 11.1902 EQUIVALENCE RATIO= 1.0000 FIRST DEFONATION PRESSURE= 18.844 ATM

TEMP DEG K	VISCOSITY POISE	MONATOMIC COND	INTERNAL COND	FROZEN COND CAL/(CM)(SEC)(K)	REACTION COND	EQUILIBRIUM COND	CP FROZ CAL/(G)(K)	CP EQ	PRANDTL FROZ DIMENSIONLESS	PRANDTL EQ	LEWIS NUMBER
3683	1112.X10-6	707.X10-6	719.X10-6	1426.X10-6	8068.X10-6	9494.X10-6	0.7662	3.9365	0.5979	0.4613	1.3677
3607	1091.	717.	697.	1414.	9051.	10465.	0.7649	4.3702	0.5900	0.4554	1.3582

NO TRANSPORT DATA WAS FOUND FOR THE SPECIES H02

NO TRANSPORT DATA WAS FOUND FOR THE SPECIES H2O2

Case 122 - Input

```

REACTANTS
N 2.      H 8.      C 2.      50.      12734.8  L298.15  F .7861
N 2.      H 4.      50.      12050.    L298.15  F 1.0036
F 2.      100.     -3098.   L 85.02   0 1.505

NAMLISTS
$INPT2 KASE=122,P=1000,PSIA=T,OF=T,MIX=2.5, KKT=T, NODATA=T      $
$RKTINP PCP=10,68.0457, SUBAR=10,5,3,2,1.5,1.1,1.01,1.001,
SUPAR=1.0005,1.05,1.1,1.5,1.8,2,5,10,100,200,500,1000          $
    
```

Case 122 - Output

```

REACTANTS
N 2.0000 H 8.0000 C 2.0000 -0. -0. 50.0000 12734.80 L 298.150 F 0.78610
N 2.0000 H 4.0000 -0. -0. -0. 50.0000 12050.00 L 298.150 F 1.00360
F 2.0000 -0. -0. -0. -0. 100.0000 -3098.00 L 85.020 0 1.50500
NAMLISTS
$INPT2
KASE = 122,
T = 0. 0. 0. 0. 0. 0. 0. 0. 0. 0.
0. 0. 0. 0. 0. 0. 0. 0. 0. 0.
0. 0. 0. 0. 0. 0. 0. 0. 0. 0.
0. 0. 0. 0. 0. 0. 0. 0. 0. 0.
0. 0. 0. 0. 0. 0. 0. 0. 0. 0.
0. 0. 0. 0. 0. 0. 0. 0. 0. 0.
0. 0. 0. 0. 0. 0. 0. 0. 0. 0.
0. 0. 0. 0. 0. 0. 0. 0. 0. 0.
P = 1.0000000E+03, 0. 0. 0. 0. 0. 0. 0. 0. 0.
0. 0. 0. 0. 0. 0. 0. 0. 0. 0.
0. 0. 0. 0. 0. 0. 0. 0. 0. 0.
0. 0. 0. 0. 0. 0. 0. 0. 0. 0.
PSIA = T, MMHG = F, NSQM = F,
V = 0. 0. 0. 0. 0. 0. 0. 0. 0. 0.
0. 0. 0. 0. 0. 0. 0. 0. 0. 0.
0. 0. 0. 0. 0. 0. 0. 0. 0. 0.
KHO = 1.0000000E+03, 0. 0. 0. 0. 0. 0. 0. 0. 0. 0.
0. 0. 0. 0. 0. 0. 0. 0. 0. 0.
0. 0. 0. 0. 0. 0. 0. 0. 0. 0.
0. 0. 0. 0. 0. 0. 0. 0. 0. 0.
0. 0. 0. 0. 0. 0. 0. 0. 0. 0.
ERATIO= F, OF = T, FPCT = F, FA = F,
MIX = 2.5000000E+00, 0 0. 0. 0. 0. 0. 0. 0. 0. 0.
0. C 0. 0. 0. 0. 0. 0. 0. 0. 0. 0.
0. 0. 0. 0. 0. 0. 0. 0. 0. 0.
TP = F, HP = F, SP = F, TV = F, UV = F, SV = F,
RKT = T, SHUCK = F, DETN = F, DITO = F, CR = 0. , SO = 0. , SO = 0.
IONS = F, IDEBUG= 0, TRACE = 0. , SIUNIT= F, EUNITS= F,
TRANSP= T, FROZN = F, PUNCH = F, NODATA= T,
$ END
SPECIES BEING CONSIDERED IN THIS SYSTEM
J 3/61 C(S) J 3/61 C J 6/70 CF J 6/70 CF2 J 6/69 CF3
J 6/69 CF4 J12/67 CH J 6/69 CH2 J 6/69 CH3 J 3/61 CH4
J 6/69 CN J 6/66 CNN J12/70 CN2 J12/69 C2 J12/67 C2F2
J 6/69 C2F4 J 3/67 C2H J12/67 C2HF J 3/61 C2H2 J 9/65 C2H4
L 5/72 C2H6 J 3/67 C2N J 3/61 C2N2 J12/69 C3 J12/69 C4
J12/69 C5 J 9/65 F J 6/69 FCN J12/60 F2 J 9/65 H
L12/69 HCN J12/68 HF J 3/61 H2 J 3/61 N J 6/65 NF
J 3/64 NF2 J 6/69 NF3 J12/71 NH J12/65 NH2 J 9/65 NH3
J 9/65 N2 J12/65 N2H4 J12/70 N3
    
```



\$RKTIIP

EQL = T, FRUZ = T,

SUBAK = 1.0000000E+01, 5.0000000E+00, 3.0000000E+00, 2.0000000E+00, 1.5000000E+00, 1.1000000E+00,
1.0100000E+00, 1.0010000E+00, 0., 0., 0., 0.

SUPAR = 1.0005000E+00, 1.0500000E+00, 1.1000000E+00, 1.5000000E+00, 1.8000000E+00, 2.0000000E+00,
5.0000000E+00, 1.0000000E+01, 1.0000000E+02, 2.0000000E+02, 5.0000000E+02, 1.0000000E+03,

PCP = 1.0000000E+01, 6.8045700E+01, 0., 0., 0., 0.,
0., 0., 0., 0.,
0., 0., 0., 0.,
0., 0., 0., 0.

NFZ = 1,

\$ END

OF = 2.500000

ENTHALPY (KG-MOL) (DEG K)/KG EFFECTIVE FUEL HPP(2) EFFECTIVE OXIDANT HPP(1) MIXTURE HSUBO
0.14793078E+03 -0.41029893E+02 0.12958869E+02

KG-ATOMS/KG BOP(1,2) BOP(1,1) BD(1)

N 0.47844928E-01 0. 0.13669979E-01
H 3.12896802E+00 0. 0.36848007E-01
C 0.16639085E-01 0. 0.47540242E-02
F 0. 0.52636011E-01 0.37597151E-01

PT	N	H	C	F	
1	-13.886	-11.179	-5.953	-19.837	10.000
2	-14.031	-11.466	-5.420	-20.308	4.000
PC/PT= 1.750480 T = 4188.90					
2	-14.030	-11.466	-5.421	-20.307	2.000
PC/PT= 1.749150 T = 4189.27					
3	-14.468	-12.543	-3.483	-21.918	5.000
3	-14.513	-12.456	-4.065	-21.827	4.000
4	-15.066	-13.383	-3.603	-23.502	5.000
5	-13.762	-11.329	-4.452	-20.028	7.000
5	-13.887	-11.181	-5.950	-19.840	5.000
5	-13.887	-11.180	-5.951	-19.838	2.000
5	-13.887	-11.180	-5.951	-19.838	2.000
5	-13.887	-11.180	-5.951	-19.838	1.000
5	-13.887	-11.180	-5.951	-19.838	1.000
6	-13.889	-11.184	-5.945	-19.844	2.000
6	-13.888	-11.184	-5.945	-19.844	2.000
6	-13.888	-11.184	-5.945	-19.844	1.000
7	-13.892	-11.190	-5.934	-19.854	2.000
7	-13.892	-11.191	-5.931	-19.856	2.000
7	-13.892	-11.191	-5.931	-19.856	2.000
8	-13.898	-11.202	-5.910	-19.875	2.000
8	-13.901	-11.207	-5.901	-19.883	2.000
8	-13.901	-11.208	-5.900	-19.884	2.000
8	-13.901	-11.208	-5.900	-19.884	1.000
9	-13.910	-11.225	-5.866	-19.913	2.000
9	-13.914	-11.234	-5.851	-19.928	2.000
9	-13.915	-11.235	-5.849	-19.929	2.000
9	-13.915	-11.235	-5.849	-19.929	1.000
10	-13.958	-11.319	-5.692	-20.069	3.000
10	-13.959	-11.321	-5.689	-20.071	2.000
10	-13.959	-11.321	-5.689	-20.071	1.000
11	-14.004	-11.411	-5.571	-20.219	3.000
11	-14.003	-11.411	-5.572	-20.218	2.000
12	-14.015	-11.433	-5.480	-20.255	3.000
12	-14.020	-11.444	-5.461	-20.272	2.000
12	-14.021	-11.447	-5.455	-20.277	2.000
12	-14.021	-11.447	-5.455	-20.277	2.000
13	-14.037	-11.481	-5.394	-20.331	3.000
13	-14.037	-11.479	-5.396	-20.329	2.000



THEORETICAL ROCKET PERFORMANCE ASSUMING EQUILIBRIUM COMPOSITION DURING EXPANSION

PC = 1000.0 PSIA
CASE NO. 122

CHEMICAL FORMULA
FUEL N 2.00000 H 8.00000 C 2.00000
FUEL N 2.00000 H 4.00000
OXIDANT F 2.00000

WT FRACTION (SEE NOTE) ENERGY STATE TEMP DENSITY
CAL/MOL DEG K G/CC
0.50000 12734.800 L 298.15 0.7861
0.50000 12050.000 L 298.15 1.0036
1.00000 -3098.000 L 85.07 1.5050

O/F = 2.5000 PERCENT FUEL = 24.5714 EQUIVALENCE RATIO = 1.4859 REACTANT DENSITY = 1.2521

	CHAMBER	THROAT	EXIT	EXIT	EXIT	EXIT	EXIT	EXIT	EXIT	EXIT	EXIT	EXIT	EXIT	EXIT
PC/P	1.0000	1.7491	10.000	68.046	1.0021	1.0084	1.0241	1.0586	1.1181	1.3245	1.5759	1.6895	1.7946	
P, ATM	68.046	38.902	6.8046	1.3000	67.956	67.480	65.442	64.279	60.858	51.376	43.178	40.275	37.916	
T, DEG K	4464	4189	3502	2902	4463	4460	4452	4435	4408	4324	4239	4206	4177	
RHO, G/CC	3.8190E-3	2.3626E-3	5.1436E-4	9.4214E-5	3.8123E-3	3.7917E-3	3.7416E-3	3.6369E-3	3.4701E-3	3.0004E-3	2.5841E-3	2.4341E-3	2.3111E-3	
H, CAL/G	25.8	-206.2	-825.1	-1381.0	24.9	22.2	15.5	1.3	-22.1	-93.1	-164.3	-192.4	-216.4	
S, CAL/(G)(K)	2.7398	2.7398	2.7398	2.7398	2.7398	2.7398	2.7398	2.7398	2.7398	2.7398	2.7398	2.7398	2.7398	
M, MOL WT	20.558	20.877	21.727	22.433	20.559	20.563	20.572	20.591	20.623	20.721	20.819	20.858	20.891	
(DLV/DLPI)	-1.03593	-1.02942	-1.02251	-1.00455	-1.03590	-1.03583	-1.03564	-1.03524	-1.03458	-1.03255	-1.03052	-1.02971	-1.02902	
(ULV/ULT)P	1.5692	1.4890	1.5681	1.1157	1.5689	1.5681	1.5659	1.5613	1.5537	1.5296	1.5044	1.4941	1.4852	
CP, CAL/(G)(K)	1.3378	1.2425	1.9125	0.7232	1.3375	1.3365	1.3341	1.3289	1.3202	1.2922	1.2616	1.2489	1.2377	
GAMMA (S)	1.1655	1.1615	1.1051	1.1736	1.1655	1.1655	1.1654	1.1652	1.1650	1.1643	1.1637	1.1636	1.1635	
SON VEL, M/SEC	1493.6	1393.3	1217.1	1123.5	1450.4	1449.7	1448.0	1444.6	1438.8	1421.3	1403.6	1396.7	1390.7	
MACH NUMBER	0.	1.000	2.197	3.054	0.059	0.120	0.203	0.313	0.440	0.702	0.899	0.967	1.024	
AE/AT		1.0000	2.3984	10.183	10.000	5.0000	3.0000	2.0000	1.5000	1.1000	1.0100	1.0010	1.0005	
CSTAR, FT/SEC		6872	5872	6872	6872	6872	6872	6872	6872	6872	6872	6872	6872	
CF		0.665	1.274	1.638	0.041	0.083	0.140	0.216	0.302	0.476	0.602	0.645	0.680	
IVAC, LB-SEC/LR		264.2	323.3	361.8	2145.4	1077.1	655.5	449.7	351.0	279.1	265.5	264.3	264.2	
ISP, LB-SEC/LR		142.1	272.1	349.9	8.8	17.7	29.9	46.1	64.5	101.7	128.6	137.8	145.2	

MOLE FRACTIONS

C(S)	0.	0.	0.03126	0.08883	0.	0.	0.	0.	0.	0.	0.	0.	0.
C	0.00253	0.00183	0.00046	0.00002	0.00253	0.00252	0.00250	0.00246	0.00238	0.00217	0.00195	0.00187	0.00180
CF	0.01983	0.01805	0.00969	0.00142	0.01982	0.01980	0.01976	0.01966	0.01949	0.01896	0.01840	0.01817	0.01796
CF2	0.00593	0.00636	0.00601	0.00253	0.00593	0.00594	0.00595	0.00597	0.00601	0.00613	0.00627	0.00633	0.00639
CF3	0.00004	0.00004	0.00003	0.00001	0.00004	0.00004	0.00004	0.00004	0.00004	0.00004	0.00004	0.00004	0.00004
CH	0.00024	0.00015	0.00002	0.00000	0.00024	0.00024	0.00024	0.00023	0.00022	0.00019	0.00016	0.00015	0.00014
CH2	0.00001	0.00001	0.00000	0.	0.00001	0.00001	0.00001	0.00001	0.00001	0.00001	0.00001	0.00001	0.00001
CH3	0.01306	0.01186	0.00640	0.00080	0.01306	0.01305	0.01301	0.01295	0.01284	0.01248	0.01210	0.01194	0.01180
LN2	0.00001	0.00000	0.00000	0.00000	0.00001	0.00001	0.00001	0.00001	0.00001	0.00001	0.00000	0.00000	0.00000
C2	0.00132	0.00115	0.00039	0.00001	0.00132	0.00132	0.00131	0.00129	0.00124	0.00119	0.00116	0.00116	0.00114
C2F2	0.00002	0.00002	0.00001	0.00000	0.00002	0.00002	0.00002	0.00002	0.00002	0.00002	0.00002	0.00002	0.00002
C2H	0.00899	0.00970	0.00657	0.00027	0.00899	0.00900	0.00902	0.00907	0.00914	0.00937	0.00958	0.00966	0.00973
C2HF	0.00041	0.00045	0.00031	0.00032	0.00041	0.00042	0.00042	0.00042	0.00042	0.00044	0.00044	0.00045	0.00045
C2H2	0.00148	0.00161	0.00109	0.00004	0.00149	0.00149	0.00149	0.00150	0.00151	0.00155	0.00159	0.00160	0.00162
C2N	0.00035	0.00051	0.00387	0.00020	0.00035	0.00036	0.00037	0.00039	0.00043	0.00054	0.00055	0.00059	0.00057
C2N2	0.00046	0.00057	0.00064	0.00007	0.00046	0.00046	0.00047	0.00048	0.00048	0.00051	0.00055	0.00056	0.00057
C3	0.00179	0.00253	0.00301	0.00008	0.00179	0.00180	0.00181	0.00185	0.00192	0.00213	0.00237	0.00248	0.00257
C4	0.00001	0.00002	0.00002	0.00000	0.00001	0.00001	0.00001	0.00001	0.00001	0.00001	0.00001	0.00001	0.00002
C5	0.00001	0.00001	0.00004	0.00000	0.00001	0.00001	0.00001	0.00001	0.00001	0.00001	0.00001	0.00001	0.00001
F	0.08241	0.06744	0.03443	0.01527	0.08236	0.08218	0.08176	0.08084	0.07935	0.07476	0.07016	0.06834	0.06678
FCN	0.00159	0.00158	0.00118	0.00031	0.00159	0.00159	0.00159	0.00159	0.00159	0.00158	0.00158	0.00158	0.00158
F2	0.00001	0.00000	0.00000	0.00000	0.00001	0.00001	0.00001	0.00001	0.00001	0.00001	0.00000	0.00000	0.00000
H	0.04706	0.03678	0.01447	0.00308	0.04702	0.04689	0.04659	0.04593	0.04485	0.04155	0.03823	0.03693	0.03581
HCN	0.01297	0.01322	0.01003	0.00176	0.01297	0.01298	0.01299	0.01300	0.01303	0.01311	0.01319	0.01321	0.01323
HF	0.65661	0.68449	0.73343	0.74638	0.65672	0.65704	0.65784	0.65953	0.66232	0.67085	0.67943	0.68282	0.68573
H2	0.01410	0.01087	0.00422	0.00079	0.01408	0.01404	0.01395	0.01375	0.01343	0.01243	0.01145	0.01106	0.01073
N	0.00034	0.00019	0.00003	0.00000	0.00034	0.00034	0.00033	0.00032	0.00031	0.00026	0.00022	0.00020	0.00019
NF	0.00001	0.00001	0.00000	0.00000	0.00001	0.00001	0.00001	0.00001	0.00001	0.00001	0.00001	0.00001	0.00001
NH	0.00002	0.00001	0.00000	0.00000	0.00002	0.00002	0.00002	0.00002	0.00002	0.00001	0.00001	0.00001	0.00001
N2	0.12337	0.12583	0.13244	0.13810	0.12338	0.12341	0.12347	0.12362	0.12366	0.12461	0.12537	0.12568	0.12594

ADDITIONAL PRODUCTS WHICH WERE CONSIDERED BUT WHOSE MOLE FRACTIONS WERE LESS THAN 0.50000E-05 FOR ALL ASSIGNED CONDITIONS

	CH3	CH4	CNN	C2F4	C2H4	C2H6	NF2	NF3	NH2
CF4									
NH3	N2H4	N3							

NOTE. WEIGHT FRACTION OF FUEL IN TOTAL FUELS AND OF OXIDANT IN TOTAL OXIDANTS

3	-14.104	-11.622	-5.136	-20.556	3.000
3	-14.104	-11.621	-5.139	-20.553	2.000
4	-14.138	-11.697	-5.001	-20.672	3.000
5	-14.306	-12.093	-4.291	-21.270	4.000
5	-14.297	-12.071	-4.331	-21.237	3.000
5	-14.297	-12.071	-4.331	-21.236	1.000
6	-14.392	-12.323	-3.880	-21.604	3.000
6	-14.411	-12.288	-4.123	-21.567	3.000
6	-14.380	-12.238	-4.140	-21.490	3.000
6	-14.380	-12.238	-4.140	-21.489	2.000
7	-14.458	-12.365	-4.097	-21.687	3.000
7	-14.430	-12.318	-4.113	-21.615	3.000
7	-14.430	-12.318	-4.113	-21.615	2.000
8	-14.840	-13.108	-3.842	-22.744	5.000
8	-14.818	-13.055	-3.860	-22.677	3.000
8	-14.818	-13.055	-3.860	-22.677	1.000
9	-15.061	-13.859	-3.610	-23.485	4.000
9	-15.061	-13.855	-3.611	-23.482	2.000
10	-15.575	-18.484	-2.366	-28.630	9.000
10	-15.583	-18.553	-2.339	-28.855	7.000
11	-15.726	-19.815	-1.909	-33.294	3.000
11	-15.717	-19.735	-1.933	-32.997	1.000
12	-15.912	-21.559	-1.477	-40.206	2.000
12	-15.923	-21.664	-1.456	-40.645	1.000
13	-16.176	-23.640	-1.141	-49.285	2.000
13	-16.113	-23.512	-1.157	-48.706	1.000

THEORETICAL ROCKET PERFORMANCE ASSUMING EQUILIBRIUM COMPOSITION DURING EXPANSION

PC = 1000.0 PSIA
CASE NO. 122

CHEMICAL FORMULA				WT FRACTION	ENERGY	STATE	TEMP	DENSITY	
FUEL	N	H	C	(SEE NOTE)	CAL/MOL		DEG K	G/CC	
FUEL	N	2.00000	H	8.00000	0.50000	12734.800	L	298.15	0.7861
FUEL	N	2.00000	H	4.00000	0.50000	12050.000	L	298.15	1.0036
OXIDANT	F	2.00000			1.00000	-3098.000	L	85.02	1.5050

O/F = 2.5000 PERCENT FUEL = 28.5714 EQUIVALENCE RATIO = 1.4859 REACTANT DENSITY = 1.2521

PC/P	CHAMBER	THROAT	EXIT	EXIT	EXIT	EXIT	EXIT	EXIT	EXIT	EXIT	EXIT	EXIT	EXIT
P, ATM	68.046	38.902	29.263	25.566	13.710	10.265	8.8021	2.5347	1.0242	0.0470	0.0183	0.0052	0.0020
T, DEG K	4464	4189	4055	3992	3709	3608	3569	3224	2911	1625	1301	955	748
RHO, G/CC	3.8190-3	2.3626-3	1.8497-3	1.6469-3	9.6438-4	7.4680-4	6.4949-4	2.1203-4	9.6152-5	8.0299-6	3.8999-6	1.5169-6	7.4686-7
H, CAL/G	25.8	-206.2	-317.5	-368.8	-593.1	-690.8	-741.7	-1126.4	-1374.8	-1982.6	-2102.7	-2225.1	-2295.6
S, CAL/(G)(K)	2.7398	2.7398	2.7398	2.7398	2.7398	2.7398	2.7398	2.7398	2.7398	2.7398	2.7398	2.7398	2.7398
M, MOL WT	20.558	20.877	21.031	21.102	21.410	21.541	21.609	22.131	22.427	22.793	22.794	22.794	22.795
(DLV/DLPT)	-1.03593	-1.02932	-1.02614	-1.02468	-1.01853	-1.02754	-1.02563	-1.01183	-1.00469	-1.00004	-1.00000	-1.00000	-1.00000
(DLV/DLTP)	1.5692	1.4890	1.4465	1.4262	1.3332	1.6866	1.6420	1.3053	1.1195	1.0014	1.0000	1.0000	1.0000
CP, CAL/(G)(K)	1.3378	1.2425	1.1874	1.1600	1.0258	2.2124	2.1000	1.2323	0.7338	0.3809	0.3626	0.3448	0.3352
GAMMA (S)	1.1655	1.1635	1.1633	1.1634	1.1659	1.1002	1.1019	1.1265	1.1719	1.2978	1.3166	1.3384	1.3515
SDN VEL, M/SEC	1450.6	1393.3	1365.6	1352.7	1295.9	1257.8	1230.1	1168.2	1124.6	877.1	790.5	682.8	607.2
MACH NUMBER	0.	1.000	1.241	1.343	1.756	1.978	2.060	2.658	3.044	4.674	5.339	6.356	7.259
AE/AT	1.0000	1.0500	1.1000	1.5000	1.8000	2.0000	5.0000	10.000	100.00	200.00	500.00	1000.00	1000.00
CSTAR, FT/SEC	6872	6872	6872	6872	6872	6872	6872	6872	6872	6872	6872	6872	6872
CF	0.665	0.809	0.867	1.086	1.169	1.210	1.482	1.634	1.957	2.015	2.072	2.104	2.104
IVAC, LB-SEC/LB	264.2	259.3	273.6	296.6	307.7	313.7	356.4	381.2	432.8	441.8	450.7	455.7	455.7
ISP, LB-SEC/LB	142.1	172.8	185.3	232.0	249.7	258.4	316.6	349.1	418.0	430.3	442.6	449.4	449.4

MOLE FRACTIONS

C(S)	O.	O.	O.	O.	O.	0.00883	0.01766	0.07021	0.08855	0.09425	0.09428	0.09428	0.09428
C	0.00253	0.00183	0.00151	0.00137	0.00081	0.00364	0.00057	0.00014	0.00002	0.	0.	0.	0.
CF	0.01983	0.01805	0.01706	0.01657	0.01414	0.01247	0.01139	0.00442	0.00148	0.00000	0.	0.	0.
CF2	0.00593	0.00636	0.00665	0.00680	0.00772	0.00742	0.00686	0.00361	0.00253	0.00006	0.00000	0.	0.
CF3	0.00004	0.00004	0.00004	0.00004	0.00004	0.00004	0.00004	0.00001	0.00001	0.00000	0.00000	0.	0.
CF4	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00382	0.00387	0.00387	0.00387
CH	0.00024	0.00015	0.00011	0.00009	0.00004	0.00003	0.00003	0.00000	0.00000	0.	0.	0.	0.
CH2	0.00001	0.00001	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.	0.	0.	0.
CN	0.01306	0.01186	0.01117	0.01083	0.00910	0.00896	0.00743	0.00295	0.00084	0.	0.	0.	0.
CN2	0.00001	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.	0.	0.	0.
C2	0.00132	0.00115	0.00105	0.00100	0.00076	0.00061	0.00052	0.00009	0.00001	0.	0.	0.	0.
C2F2	0.00002	0.00002	0.00002	0.00002	0.00002	0.00002	0.00002	0.00000	0.00000	0.	0.	0.	0.
C2H	0.00089	0.00070	0.00098	0.01009	0.01013	0.00923	0.00815	0.00204	0.00029	0.	0.	0.	0.
C2HF	0.00041	0.00045	0.00047	0.00048	0.00052	0.00047	0.00040	0.00010	0.00002	0.	0.	0.	0.
C2H2	0.00148	0.00161	0.00167	0.00170	0.00179	0.00160	0.00139	0.00033	0.00005	0.	0.	0.	0.
C2N	0.00535	0.00571	0.00587	0.00594	0.00551	0.00486	0.00424	0.00027	0.	0.	0.	0.	0.
C2N2	0.00046	0.00057	0.00064	0.00067	0.00089	0.00086	0.00077	0.00025	0.00008	0.	0.	0.	0.
C3	0.00179	0.00253	0.00300	0.00324	0.00457	0.00439	0.00384	0.00082	0.00009	0.	0.	0.	0.
C4	0.00001	0.00002	0.00002	0.00002	0.00003	0.00003	0.00002	0.00000	0.00000	0.	0.	0.	0.
C5	0.00001	0.00001	0.00002	0.00003	0.00006	0.00006	0.00005	0.00001	0.00000	0.	0.	0.	0.
F	0.06241	0.06744	0.06621	0.06688	0.06436	0.06391	0.06248	0.01549	0.00003	0.00000	0.	0.	0.
FEN	0.00159	0.00158	0.00158	0.00158	0.00160	0.00149	0.00136	0.00062	0.00031	0.00000	0.	0.	0.
F2	0.00001	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.	0.	0.	0.
H	0.04706	0.03628	0.03112	0.02877	0.01888	0.01629	0.01564	0.00889	0.00321	0.00000	0.	0.	0.
HCN	0.01247	0.01372	0.01329	0.01331	0.01324	0.01233	0.01145	0.00524	0.00143	0.00000	0.	0.	0.
HF	0.65661	0.68449	0.69794	0.70412	0.73071	0.73527	0.73436	0.73644	0.74610	0.76072	0.76074	0.76074	0.76074
H2	0.01410	0.01087	0.00935	0.00866	0.00579	0.00495	0.00468	0.00242	0.00082	0.00000	0.	0.	0.
N	0.00034	0.00019	0.00014	0.00012	0.00005	0.00004	0.00004	0.00001	0.00000	0.	0.	0.	0.
NF	0.00001	0.00001	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.	0.	0.	0.
NH	0.00002	0.00001	0.00001	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.	0.	0.	0.
NH2	0.12337	0.12583	0.12708	0.12767	0.13030	0.13135	0.13175	0.13535	0.13803	0.14111	0.14111	0.14111	0.14111

ADDITIONAL PRODUCTS WHICH WERE CONSIDERED BUT WHOSE MOLE FRACTIONS WERE LESS THAN 0.50000E-05 FOR ALL ASSIGNED CONDITIONS

CH3	CH4	CN	C2F4	C2H4	C2H6	NF2	NF3	NH2	NH3
N2H4	N3								

NOTE: WEIGHT FRACTION OF FUEL IN TOTAL FUELS AND OF OXIDANT IN TOTAL OXIDANTS

TRANSPORT PROPERTIES OF ROCKET EXHAUST ASSUMING EQUILIBRIUM COMPOSITION DURING EXPANSION

O/F = 2.5000 PERCENT FUEL = 28.5714 EQUIVALENCE RATIO = 1.4859 CHAMBER PRESSURE = 68.046 ATM

TEMP DEG K	VISCOSITY POISE	MONATOMIC COND	INTERNAL COND	FROZEN COND	REACTION COND	EQUILIBRIUM COND	CP FROZ	CP EQ	PRANDTL FROZ	PRANDTL EQ	LEWIS NUMBER
		CAL/(CM)(SEC)(K)				CAL/(G)(K)		DIMENSIONLESS			
4464	1431.X10-6	580.X10-6	354.X10-6	935.X10-6	2979.X10-6	3914.X10-6	0.4281	1.3369	0.6556	0.4889	1.5016
4189	1373.	536.	338.	874.	2606.	3480.	0.4251	1.2416	0.6676	0.4889	1.5020
3502	1219.	445.	288.	733.	1558.	2292.	0.4162	0.9554	0.6918	0.5082	1.6400
2902	1072.	382.	233.	615.	819.	1235.	0.4057	0.6440	0.7065	0.5590	1.7130
4463	1431.	580.	354.	934.	2978.	3912.	0.4281	1.3365	0.6556	0.4889	1.5018
4460	1430.	579.	354.	934.	2974.	3908.	0.4280	1.3356	0.6557	0.4889	1.5024
4452	1429.	578.	354.	932.	2964.	3896.	0.4279	1.3332	0.6561	0.4889	1.5038
4435	1425.	575.	353.	928.	2944.	3872.	0.4278	1.3280	0.6568	0.4889	1.5068
4408	1419.	571.	351.	922.	2909.	3831.	0.4275	1.3193	0.6580	0.4889	1.5118
4324	1402.	558.	346.	904.	2798.	3701.	0.4266	1.2913	0.6617	0.4890	1.5272
4239	1384.	544.	341.	885.	2679.	3564.	0.4256	1.2607	0.6654	0.4894	1.5428
4206	1377.	539.	339.	878.	2631.	3509.	0.4253	1.2480	0.6669	0.4897	1.5490
4177	1370.	534.	337.	872.	2588.	3460.	0.4249	1.2368	0.6681	0.4899	1.5543
4055	1344.	516.	329.	845.	2399.	3244.	0.4236	1.1865	0.6735	0.4914	1.5762
3992	1330.	506.	325.	832.	2297.	3129.	0.4228	1.1590	0.6762	0.4926	1.5869
3709	1265.	465.	306.	772.	1806.	2577.	0.4193	1.0244	0.6877	0.5029	1.6221
3603	1242.	454.	298.	752.	1661.	2413.	0.4179	0.9848	0.6905	0.5071	1.6283
3569	1234.	451.	294.	745.	1626.	2372.	0.4173	0.9751	0.6909	0.5073	1.6326
3224	1154.	418.	263.	681.	1162.	1862.	0.4116	0.8306	0.6978	0.5203	1.6733
2911	1074.	383.	234.	617.	634.	1251.	0.4058	0.6492	0.7062	0.5572	1.7133
1625	679.	238.	103.	340.	3.	343.	0.3706	0.3740	0.7386	0.7395	0.8626
1301	561.	196.	66.	264.	0.	264.	0.3570	0.3571	0.7577	0.7577	0.8896
955	424.	148.	35.	183.	0.	183.	0.3403	0.3403	0.7910	0.7910	
748	336.	117.	19.	136.	0.	136.	0.3324	0.3324	0.8214	0.8214	

THEORETICAL ROCKET PERFORMANCE ASSUMING FROZEN COMPOSITION DURING EXPANSION

PC = 1000.0 PSIA
CASE NO. 122

	CHEMICAL FORMULA	WT FRACTION (SEE NOTE)	ENERGY CAL/MOL	STATE	TEMP DEG K	DENSITY G/CC
FUEL	N 2.00000 H 8.00000 C 2.00000	0.50000	12734.800	L	298.15	0.7861
FUEL	N 2.00000 H 4.00000	0.50000	12050.000	L	298.15	1.0036
OXIDANT	F 2.00000	1.00000	-3098.000	L	85.07	1.5050

O/F = 2.5000 PERCENT FUEL = 28.5714 EQUIVALENCE RATIO = 1.4859 REACTANT DENSITY = 1.2921

	CHAMBER	THROAT	EXIT	EXIT	EXIT	EXIT	EXIT	EXIT	EXIT	EXIT	EXIT	EXIT	EXIT
PC/P	1.0000	1.8302	13.000	68.046	1.0022	1.0091	1.0261	1.0634	1.1280	1.3545	1.6348	1.7619	1.8817
P, ATM	68.046	37.178	6.8046	1.0000	67.894	67.435	65.317	63.991	60.323	50.238	41.623	38.620	36.162
T, DEG K	4464	4891	2621	1635	4462	4455	4438	4402	4344	4168	3993	3925	3867
MOL WT	3.8190-3	2.3936-3	6.5049-4	1.5322-4	3.8124-3	3.7924-3	3.7437-3	3.6418-3	3.4790-3	3.0201-3	2.6116-3	2.4649-3	2.3430-3
W, CAL/G	25.8	-218.0	-746.3	-1134.6	24.8	21.9	14.7	-0.5	-25.5	-100.8	-175.0	-203.6	-228.4
S, CAL/(G)(K)	2.7498	2.7398	2.7398	2.7398	2.7398	2.7398	2.7398	2.7398	2.7398	2.7398	2.7398	2.7398	2.7398
M, MOL WT	20.558	20.558	20.558	20.558	20.558	20.558	20.558	20.558	20.558	20.558	20.558	20.558	20.558
CP, CAL/(G)(K)	0.4281	0.4233	0.4061	0.3734	0.4280	0.4280	0.4278	0.4276	0.4271	0.4257	0.4242	0.4236	0.4230
GAMMA (S)	1.2917	1.2960	1.3124	1.3419	1.2917	1.2918	1.2919	1.2921	1.2925	1.2938	1.2951	1.2957	1.2962
SUN VELOCITY/SEC	1527.1	1478.2	1179.4	942.0	1526.7	1525.6	1522.8	1516.8	1506.9	1476.7	1446.2	1434.2	1423.8
MACH NUMBER	0.	1.000	2.155	3.309	0.059	0.118	0.200	0.309	0.435	0.697	0.896	0.966	1.024
AE/AT	1.0000	2.0675	7.1598	10.000	5.0000	3.0003	2.0000	1.5000	1.1000	1.0100	1.0010	1.0010	1.0005
CSTAR, FT/SEC	6617	6617	6617	6617	6617	6617	6617	6617	6617	6617	6617	6617	6617
CF	0.708	1.260	1.945	0.044	0.089	0.151	0.233	0.325	0.510	0.643	0.687	0.723	
IVAC, LB-SEC/LB	258.0	301.7	339.4	2061.0	1037.5	632.4	434.7	340.3	272.0	259.2	258.1	258.1	
ISP, LB-SEC/LB	145.6	259.2	317.8	9.1	18.4	31.0	47.9	66.8	104.9	132.2	141.3	148.7	

MOLE FRACTIONS

C	0.00253	CF	0.01983	CF2	0.00593	CF3	0.00004
CH	0.00024	CH2	0.00001	CH	0.01306	CN2	0.00001
C2	0.00132	C2F2	0.00002	C2H	0.00899	C2HF	0.00041
C2H2	0.00148	C2N	0.00535	C2N2	0.00046	C3	0.00179
C4	0.00001	C5	0.00001	F	0.08241	FCN	0.00159
F2	0.00001	H	0.04706	HCN	0.01297	HF	0.65661
H2	0.01410	N	0.00034	NF	0.00001	NH	0.00002
N2	0.12337						

ADDITIONAL PRODUCTS WHICH WERE CONSIDERED BUT WHOSE MOLE FRACTIONS WERE LESS THAN 0.50000E-05 FOR ALL ASSIGNED CONDITIONS

C(S)	CF4	CH3	CH4	CNN	C2F4	C2H4	C2H6	NF2	NF3
NH2		NH3	N2H4	N3					

NOTE: WEIGHT FRACTION OF FUEL IN TOTAL FUELS AND OF OXIDANT IN TOTAL OXIDANTS

THEORETICAL ROCKET PERFORMANCE ASSUMING FROZEN COMPOSITION DURING EXPANSION

PC = 1000.0 PSIA
CASE NO. 122

CHEMICAL FORMULA			WT FRACTION (SEE NOTE)	ENERGY CAL/MOL	STATE	TEMP DEG K	DENSITY G/CC
FUEL	N 2.00000	H 8.00000	0.50000	12734.800	L	298.15	1.7861
FUEL	N 2.00000	H 4.00000	0.50000	12050.000	L	298.15	1.0036
OXIDANT	F 2.00000		1.00000	-3098.000	L	85.02	1.5050

O/F= 2.5000 PERCENT FUEL= 78.5714 EQUIVALENCE RATIO= 1.4859 REACTANT DENSITY= 1.2521

	CHAMBER	THROAT	EXIT	LXIT	EXIT	EXIT	EXIT	EXIT	EXIT	EXIT	EXIT	EXIT	EXIT
PC/P	1.0000	1.8302	2.4922	2.8860	5.6056	7.8973	9.4581	39.876	111.17	3103.65	8387.46	31073.1	83508.0
P, ATM	68.346	37.178	27.303	23.578	11.968	8.6163	7.1944	1.7064	0.6121	0.0219	0.0081	0.0022	0.0008
T, DEG K	4464	3891	3626	3505	2995	2772	2656	1871	1441	577	433	297	222
RHO, G/CC	3.8190-3	2.3936-3	1.8866-3	1.6851-3	1.0013-3	7.7882-4	6.7870-4	2.2849-4	1.0641-4	9.5246-6	4.6894-6	1.8494-6	9.1778-7
H, CAL/G	25.8	-718.0	-330.1	-380.7	-593.3	-68.8	-732.1	-1044.2	-1207.5	-1513.6	-1561.8	-1607.5	-1632.1
S, CAL/(G)(K)	2.7398	2.7398	2.7398	2.7398	2.7398	2.7398	2.7398	2.7398	2.7398	2.7398	2.7398	2.7398	2.7398
M, MOL WT	20.558	20.558	20.558	20.558	20.558	20.558	20.558	20.558	20.558	20.558	20.558	20.558	20.558
CP, CAL/(G)(K)	0.4281	0.4233	0.4207	0.4194	0.4126	0.4089	0.4067	0.3872	0.3721	0.3382	0.3351	0.3327	0.3313
GAMMA (S)	1.2917	1.2960	1.2983	1.2995	1.3059	1.3096	1.3117	1.3327	1.3509	1.4003	1.4054	1.4096	1.4119
SUN VEL, M/SEC	1527.1	1428.2	1379.8	1357.3	1257.6	1211.6	1187.0	1004.2	887.4	571.5	496.3	411.2	356.4
MACH NUMBER	0.	1.000	1.251	1.359	1.810	2.013	2.122	2.980	3.620	6.280	7.343	8.990	10.451
AE/AT		1.0000	1.0500	1.1000	1.5000	1.8000	2.0000	5.0000	10.000	100.00	200.00	500.00	1000.00
CSTAR, FT/SEC		6617	6617	6617	6617	6617	6617	6617	6617	6617	6617	6617	6617
CF		0.708	0.856	0.914	1.128	1.209	1.249	1.484	1.593	1.779	1.807	1.833	1.847
IVAC, LB-SEC/LB		250.0	262.6	266.4	286.1	295.5	300.3	330.9	346.1	372.6	376.6	380.3	382.3
ISP, LB-SEC/LB		145.6	176.0	188.1	232.1	248.7	256.8	305.1	327.6	366.0	371.7	377.0	379.8

MOLE FRACTIONS

C	0.00253	CF	0.01983	CF2	0.00593	CF3	0.00004
CH	0.00024	CH2	0.00001	CH	0.01306	CN2	0.00001
C2	0.00132	C2F2	0.00002	C2H	0.00899	C2HF	0.00041
C2H2	0.00148	C2N	0.00535	C2N2	0.00046	C3	0.00179
C4	0.00001	C5	0.00031	F	0.08241	FCN	0.00159
F2	0.03001	H	0.04706	HCN	0.01297	HF	0.65661
H2	0.01410	N	0.00034	NF	0.00001	NH	0.00002
N2	0.12337						

ADDITIONAL PRODUCTS WHICH WERE CONSIDERED BUT WHOSE MOLE FRACTIONS WERE LESS THAN 0.50000E-05 FOR ALL ASSIGNED CONDITIONS

C(S)	CF4	CH3	CH4	CNN	C2F4	C2H4	C2H6	NF2	NF3
NH2	NH3	N2H4	N3						

NOTE. WEIGHT FRACTION OF FUEL IN TOTAL FUELS AND OF OXIDANT IN TOTAL OXIDANTS

TRANSPORT PROPERTIES OF ROCKET EXHAUST ASSUMING FROZEN COMPOSITION DURING EXPANSION

O/F= 2.5000 PERCENT FUEL= 78.5714 EQUIVALENCE RATIO= 1.4859 CHAMBER PRESSURE= 68.346 ATM

TEMP DEG K	VISCOUSITY POISE	MONATOMIC COND	INTERVAL COND	FROZEN COND	CP FROZ	PRANDTL FROZ
		-----	CAL/(CM)(SEC)(K)	----	CAL/(G)(K)	
4464	1431.X10-6	580.X10-6	354.X10-6	935.X10-6	0.4281	0.6556
3891	1295.	524.	309.	833.	0.4233	0.6579
2621	965.	388.	199.	587.	0.4051	0.6674
1635	666.	265.	103.	368.	0.3794	0.6870
4462	1431.	580.	354.	934.	0.4281	0.6556
4455	1429.	579.	354.	933.	0.4280	0.6556
4438	1425.	578.	352.	930.	0.4279	0.6557
4402	1417.	574.	350.	924.	0.4276	0.6558
4344	1403.	569.	345.	914.	0.4271	0.6560
4168	1362.	551.	331.	883.	0.4257	0.6567
3993	1320.	534.	317.	852.	0.4242	0.6574
3425	1303.	527.	312.	839.	0.4236	0.6577
3887	1289.	521.	307.	829.	0.4231	0.6580
3626	1230.	497.	288.	785.	0.4207	0.6591
3505	1199.	485.	278.	762.	0.4194	0.6598
2995	1067.	430.	233.	663.	0.4127	0.6638
2772	1007.	405.	213.	618.	0.4089	0.6658
2656	974.	392.	202.	594.	0.4068	0.6670
1871	743.	297.	126.	423.	0.3872	0.6802
1441	601.	239.	83.	322.	0.3721	0.6946
577	264.	102.	13.	115.	0.3382	0.7741
433	200.	77.	0.	83.	0.3351	0.8325
297	137.	53.	2.	55.	0.3327	0.8360
222	103.	39.	0.	40.	0.3314	0.8539

Case 123 - Input

```

REACTANTS
N 2.      H 4.      50.      12050.  L298.15  F 1.0036
N 2.      H 8.      50.      12734.8 L298.15  F .7861
F 2.      C 2.      100.     -3098.  L 85.02  O 1.505
    
```

```

NAMELIST
$INPT2 KASE=123, HP=T,OF=T,MIX=2.5,P=100,10,1, PUNCH=T, NODATA=T $
    
```

Case 123 - Output

```

REACTANTS
N 2.0000 H 4.0000 -0.      -0.      -0.      50.0000 12050.00 L 298.150 F 1.00360
N 2.0000 H 8.0000 C 2.0000 -0.      -0.      -0.      50.0000 12734.80 L 298.150 F 0.78610
F 2.0000 -0.      -0.      -0.      -0.      100.0000 -3098.00 L 85.020 O 1.50500
NAMELIST
    
```

\$INPT2

KASE = 123,

```

T = 0.      , 0.      , 0.      , 0.      , 0.      , 0.      , 0.      , 0.      , 0.      ,
    0.      , 0.      , 0.      , 0.      , 0.      , 0.      , 0.      , 0.      , 0.      ,
    0.      , 0.      , 0.      , 0.      , 0.      , 0.      , 0.      , 0.      , 0.      ,
    0.      , 0.      , 0.      , 0.      , 0.      , 0.      , 0.      , 0.      , 0.      ,
    0.      , 0.      , 0.      , 0.      , 0.      , 0.      , 0.      , 0.      , 0.      ,
    0.      , 0.      , 0.      , 0.      , 0.      , 0.      , 0.      , 0.      , 0.      ,
    0.      , 0.      , 0.      , 0.      , 0.      , 0.      , 0.      , 0.      , 0.      ,
    
```

```

P = 1.0000000E+02, 1.0000000E+01, 1.0000000E+00, 0.      , 0.      , 0.      , 0.      ,
    0.      , 0.      , 0.      , 0.      , 0.      , 0.      , 0.      , 0.      , 0.      ,
    0.      , 0.      , 0.      , 0.      , 0.      , 0.      , 0.      , 0.      , 0.      ,
    0.      , 0.      , 0.      , 0.      , 0.      , 0.      , 0.      , 0.      , 0.      ,
    
```

PSIA = F, MMHG = F, NSQM = F,

```

V = 0.      , 0.      , 0.      , 0.      , 0.      , 0.      , 0.      , 0.      ,
    0.      , 0.      , 0.      , 0.      , 0.      , 0.      , 0.      , 0.      ,
    
```

```

RHD = 1.0000000E+02, 1.0000000E+01, 1.0000000E+00, 0.      , 0.      , 0.      , 0.      ,
    0.      , 0.      , 0.      , 0.      , 0.      , 0.      , 0.      , 0.      , 0.      ,
    0.      , 0.      , 0.      , 0.      , 0.      , 0.      , 0.      , 0.      , 0.      ,
    0.      , 0.      , 0.      , 0.      , 0.      , 0.      , 0.      , 0.      , 0.      ,
    
```

CRATIO= F, DF = T, FPCT = F, FA = F,

```

MIX = 2.5000000E+00, 0.      , 0.      , 0.      , 0.      , 0.      , 0.      ,
    0.      , 0.      , 0.      , 0.      , 0.      , 0.      , 0.      , 0.      ,
    0.      , 0.      , 0.      , 0.      , 0.      , 0.      , 0.      , 0.      ,
    
```

TP = F, HP = T, SP = F, TV = F, UV = F, SV = F,

RKT = F, SHUCK = F, DETN = F, DTTD = F, CR = 0., SO = 0., SO = 0.

IDNS = F, IDEBUG= 0, TRACE = 0., SIUNIT= F, EUNITS= F,

TRNSPT= T, FROZN = F, PUNCH = T, NODATA= T,

\$ END

UF = 2.500000

ENTHALPY (KG-MOL)(DEG K)/KG	EFFECTIVE FUEL HPP(2)	EFFECTIVE OXIDANT HPP(1)	MIXTURE HSUR0
0.14793078E+03	-0.41029893E+02	0.12958869E+02	
KG-ATOMS/KG	BOP(1,2)	BOP(1,1)	B0(1)
N	0.47844928E-01	0.	0.13669979E-01
H	0.12896802E+00	0.	0.36848007E-01
C	0.16639085E-01	0.	0.47540242E-02
F	0.	0.52636011E-01	0.37597151E-01

PT	N	H	C	F	
1	-13.724	-11.002	-6.011	-19.566	10.000
2	-14.692	-12.080	-5.639	-21.205	4.000
3	-15.657	-13.207	-5.224	-22.881	4.000

THEMODYNAMIC EQUILIBRIUM COMBUSTION PROPERTIES AT ASSIGNED

CASE NO. 123

PRESSURES

CHEMICAL FORMULA				WT FRACTION	ENERGY	STATE	TFMP	DENSITY
FUEL	N	H	C	(SEE NOTE)	CAL/MOL		DEG K	G/CC
FUEL	N	2.00000	H 4.00000	0.50000	12050.000	L	298.15	1.0036
FUEL	N	2.00000	H 8.00000	0.50000	12734.800	L	298.15	0.7861
OXIDANT	F	2.00000		1.00000	-3098.000	L	85.02	1.5050

O/F= 2.5000 PERCENT FUEL= 28.5714 EQUIVALENCE RATIO= 1.4859 REACTANT DENSITY= 1.2521

THERMODYNAMIC PROPERTIES

P, ATM	100.00	10.000	1.0000
T, DEG K	45.	4118	3733
RHD, G/CC	5.5516-3	5.9440-4	6.3939-5
H, CAL/G	25.8	25.8	25.8
S, CAL/(G)(K)	2.7027	2.9274	3.1582
M, MOL WT	20.658	20.086	19.586
(DLV/DLP)T	-1.03428	-1.04434	-1.05388
(DLV/DLP)P	1.5332	1.7670	2.0318
CP, CAL/(G)(K)	1.2639	1.7797	2.4735
GAMMA (S)	1.1691	1.1484	1.1305
SUN VEL, M/SEC	1460.7	1399.2	1338.5

MOLE FRACTIONS

C	0.00228	0.00386	0.00538
CF	0.01984	0.01889	0.01659
CF2	0.00670	0.00325	0.00162
CF3	0.00306	0.00001	0.00000
CH	0.00326	0.00017	0.00009
CH2	0.00301	0.00000	0.00000
CH3	0.00001	0.00000	0.00000
CN	0.01270	0.01433	0.01474
CN2	0.00301	0.00000	0.00000
C2	0.00122	0.00177	0.00213
C2F2	0.00002	0.00001	0.00000
C2H	0.00882	0.00931	0.00876
C2HF	0.00348	0.00020	0.00008
C2H2	0.00163	0.00091	0.00047
C2N	0.00536	0.00501	0.00425
C2N2	0.00051	0.00028	0.00015
C3	0.00158	0.00309	0.00529
C4	0.00001	0.00001	0.00002
C5	0.00001	0.00001	0.00001
F	0.07885	0.09876	0.11566
FCN	0.00177	0.00091	0.00047
F2	0.00001	0.00003	0.00000
H	0.04346	0.06588	0.08820
HCN	0.01370	0.00969	0.00655
HF	0.66208	0.62986	0.60034
H2	0.31454	0.01159	0.00837
N	0.00035	0.00030	0.00022
NF	0.00002	0.00000	0.00000
NH	0.00002	0.00001	0.00000
N2	0.12372	0.12188	0.12061

ADDITIONAL PRODUCTS WHICH WERE CONSIDERED BUT WHOSE MOLE FRACTIONS WERE LESS THAN 0.50000E-05 FOR ALL ASSIGNED CONDITIONS

C(S)	CF4	CH4	CNV	C2F4	C2H4	C2H6	NF2	NF3	NH2
NH3	N2H4	N3							

NOTE. WEIGHT FRACTION OF FUEL IN TOTAL FUELS AND OF OXIDANT IN TOTAL OXIDANTS

TRANSPORT PROPERTIES AT ASSIGNED PRESSURES

O/F= 2.5000 PERCENT FUEL= 28.5714 EQUIVALENCE RATIO= 1.4859 ENTHALPY= 25.8 CAL/G

TEMP	VISCOSITY	MONATOMIC	INTERNAL	FROZEN	REACTION	EQUILIBRIUM	CP	CP	PRANDTL	PRANDTL	LEWIS
DEG K	POISE	COND	COND	COND	COND	COND	FROZ	EQ	FROZ	EQ	NUMBER
									---- DIMENSIONLESS ----		
4535	1448.X10-6	581.X10-6	363.X10-6	944.X10-6	2772.X10-6	3716.X10-6	0.4285	1.2628	0.6577	0.4922	1.5088
4118	1346.	573.	316.	889.	4068.	4957.	0.4258	1.7791	0.6447	0.4830	1.4402
3733	1247.	561.	273.	835.	5434.	6269.	0.4231	2.4729	0.6320	0.4919	1.3439

Case 679 - Input

```

REACTANTS
LI 1.
F 2.
      1.  MO.  S298.15  F
      .5556 M-3098.  L 85.02  O 1.505

NAMELISTS
$INPT2 KASE=679,      RKT=T,P=1000,PSIA=T,IONS=T,TRNSPT=F      $
$RKTINP PCP=3,10,30,68.0457, 100,1000,3000,30000,300000      $
    
```

Case 679 - Output

```

REACTANTS
LI 1.0000  -0.  -0.  -0.  -0.  1.0000 M  0.  S  298.150  F  -0.
F 2.0000  -0.  -0.  -0.  -0.  0.5556 M  -3098.00  L  85.020  O  1.50500
NAMELISTS

$INPT2
KASE = 679,

T = 0. 0. 0. 0. 0. 0. 0. 0. 0. 0.
  0. 0. 0. 0. 0. 0. 0. 0. 0. 0.
  0. 0. 0. 0. 0. 0. 0. 0. 0. 0.
  0. 0. 0. 0. 0. 0. 0. 0. 0. 0.
  0. 0. 0. 0. 0. 0. 0. 0. 0. 0.
  0. 0. 0. 0. 0. 0. 0. 0. 0. 0.
  0. 0. 0. 0. 0. 0. 0. 0. 0. 0.

P = 1.0000000E+03, 0. 0. 0. 0. 0. 0. 0. 0. 0. 0.
  0. 0. 0. 0. 0. 0. 0. 0. 0. 0.
  0. 0. 0. 0. 0. 0. 0. 0. 0. 0.
  0. 0. 0. 0. 0. 0. 0. 0. 0. 0.

PSIA = T, MMHG = F, NSQM = F,
V = 0. 0. 0. 0. 0. 0. 0. 0. 0. 0.
  0. 0. 0. 0. 0. 0. 0. 0. 0. 0.
  0. 0. 0. 0. 0. 0. 0. 0. 0. 0.

RHO = 1.0000000E+03, 0. 0. 0. 0. 0. 0. 0. 0. 0. 0.
  0. 0. 0. 0. 0. 0. 0. 0. 0. 0.
  0. 0. 0. 0. 0. 0. 0. 0. 0. 0.
  0. 0. 0. 0. 0. 0. 0. 0. 0. 0.

ERATIO= F, OF = F, FPCT = F, FA = F,
MIX = 0. 0. 0. 0. 0. 0. 0. 0. 0. 0.
      0. 0. 0. 0. 0. 0. 0. 0. 0. 0.

TP = F, HP = F, SP = F, TV = F, UV = F, SV = F,
RKT = T, SHUCK = F, DETN = F, DTTD = F, CR = 0., SO = 0., SO = 0.
IONS = T, IDEBUG= 0, TRACE = 0., SIUNIT= F, EUNITS= F,
TRNSPT= F, FRUZN = F, PUNCH = F, NODATA= F,

$ END

NO INPT2 VALUE GIVEN FOR OF, EQRAT, FA, OR FPCT

SPECIES BEING CONSIDERED IN THIS SYSTEM
L02/67 E J 9/65 F J12/71 F- J12/60 F2 J 6/62 LI(S)
J 6/62 LI(L) J 6/62 LI J 3/65 LI+ J12/68 LIF(S) J12/68 LIF(L)
J12/68 LIF J12/68 LIF2- J 6/62 LI2 J12/68 LI2F2 J12/68 LI3F3
    
```



SRKTINP

EQL = T, FRDZ = T,

SUBAR = 0.0, 0.0, 0.0, 0.0, 0.0, 0.0, 0.0, 0.0, 0.0, 0.0

SUPAR = 0.0, 0.0, 0.0, 0.0, 0.0, 0.0, 0.0, 0.0, 0.0, 0.0

PCP = 3.000000E+00, 1.000000E+01, 3.000000E+01, 6.804570E+01, 1.000000E+02, 1.000000E+03, 3.000000E+03, 3.000000E+04, 3.000000E+05, 0.0, 0.0, 0.0, 0.0

NFZ = 1,

\$ END

OF = 3.042372

ENTHALPY (KG-MOL)(DEG K)/KG, EFFECTIVE FUEL HPP(2), EFFECTIVE OXIDANT HPP(1), MIXTURE HSUBO

KG-ATOMS/KG, LI, F, E, BOP(I,2), BOP(I,1), BOP(I)

PT 1 -16.252 -19.930 -9.124 9.000

THE TEMPERATURE= 0.5691E+04 IS OUT OF RANGE FOR POINT 1

THE TEMPERATURE= 0.5340E+04 IS OUT OF RANGE FOR POINT 2

THE TEMPERATURE= 0.5341E+04 IS OUT OF RANGE FOR POINT 2

THE TEMPERATURE= 0.5036E+04 IS OUT OF RANGE FOR POINT 3

THEORETICAL ROCKET PERFORMANCE ASSUMING EQUILIBRIUM COMPOSITION DURING EXPANSION

PC = 1000.0 PSIA, CASE NO. 679

CHEMICAL FORMULA, MOLES, ENERGY CAL/MOL, STATE, TEMP DEG K, DENSITY G/CC

O/F= 3.0424 PERCENT FUEL= 24.7379 EQUIVALENCE RATIO= 0.8999 REACTANT DENSITY= 0.

Table with columns: PC/P, P, ATM, T, DEG K, RHO, G/CC, S, CAL/(G)(K), M, MOL WT, (DLV/DLP)F, (DLV/DLT)F, CP, CAL/(G)(K), GAMMA (S), SON VEL, M/SEC, MACH NUMBER, AE/AT, CSTAR, FT/SEC, CF, IVAC, LB-SEC/LB, ISP, LB-SEC/LB. Rows show various performance parameters across different points.

MOLE FRACTIONS

E	0.00294	0.00237	0.00188	0.00096	0.00036	0.00009	0.00003	0.	0.	0.	0.	0.
F	0.21151	0.19574	0.18087	0.14865	0.12245	0.10760	0.10329	0.10154	0.10446	0.11258	0.12105	
F-	0.00464	0.00364	0.00284	0.00148	0.00067	0.00028	0.00015	0.00000	0.	0.00000	0.	
F2	0.00002	0.00001	0.00001	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	
LI	0.12106	0.10422	0.08820	0.05320	0.02455	0.00824	0.00347	0.00000	0.	0.	0.	
LI+	0.00758	0.00601	0.00471	0.00243	0.00104	0.00038	0.00019	0.00000	0.	0.	0.	
LIF	0.65089	0.68690	0.72056	0.79259	0.85030	0.88273	0.89207	0.88385	0.85238	0.76605	0.67705	
LI2	0.00028	0.00014	0.00007	0.00001	0.00000	0.00000	0.00000	0.	0.	0.	0.	
LI2F2	0.00109	0.00096	0.00085	0.00068	0.00062	0.00068	0.00081	0.01449	0.04246	0.11762	0.19413	
LI3F3	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00011	0.00071	0.00374	0.00777	

ADDITIONAL PRODUCTS WHICH WERE CONSIDERED BUT WHOSE MOLE FRACTIONS WERE LESS THAN 0.50000E-05 FOR ALL ASSIGNED CONDITIONS

LI(S) LI(L) LIF(S) LIF(L) LIF2-

THEORETICAL ROCKET PERFORMANCE ASSUMING FROZEN COMPOSITION DURING EXPANSION

PC = 1000.0 PSIA
CASE NO. 679

CHEMICAL FORMULA
FUEL LI 1.00000
OXIDANT F 2.00000

MOLES ENERGY STATE TEMP DENSITY
CAL/MOL DEG K G/CC
1.00000 0 S 298.15 -0.
0.55560 -3098.000 L 85.02 1.5050

O/F= 3.0424 PERCENT FUEL= 24.7379 EQUIVALENCE RATIO= 0.8999 REACTANT DENSITY= 0.

	CHAMBER	THROAT	EXIT	EXIT	EXIT	EXIT	EXIT	EXIT	EXIT	EXIT	EXIT	EXIT
PC/P	1.0000	1.8444	3.0000	10.000	30.000	68.046	100.00	1000.00	3000.00	30000.0	300000.0	300000.0
P, ATM	68.046	36.893	22.682	6.8046	2.2682	1.0000	0.6805	0.0680	0.0227	0.0023	0.0002	0.0002
T, DEG K	5691	4915	4366	3235	2448	1984	1796	984	734	388	195	195
RHO, G/CC	3.1975-3	2.0071-3	1.3892-3	5.6249-4	2.4781-4	1.3480-4	1.0131-4	1.8501-5	8.2670-6	1.5643-6	3.1113-7	3.1113-7
H, CAL/G	-61.4	-354.9	-559.1	-970.7	-1251.7	-1415.4	-1481.3	-1762.9	-1847.8	-1961.3	-2020.0	-2020.0
S, CAL/(G)(K)	2.7095	2.7095	2.7095	2.7095	2.7095	2.7095	2.7095	2.7095	2.7095	2.7095	2.7095	2.7095
M, MOL WT	21.943	21.943	21.943	21.943	21.943	21.943	21.943	21.943	21.943	21.943	21.943	21.943
CP, CAL/(G)(K)	0.3823	0.3746	0.3690	0.3594	0.3544	0.3516	0.3503	0.3421	0.3365	0.3159	0.2915	0.2915
GAMMA (S)	1.3104	1.3188	1.3253	1.3369	1.3432	1.3470	1.3487	1.3600	1.3683	1.4019	1.4508	1.4508
SON VEL, M/SEC	1681.0	1567.3	1480.7	1280.1	1116.1	1006.2	958.1	711.9	616.7	453.8	327.4	327.4
MACH NUMBER	0.	1.000	1.378	2.155	2.828	3.345	3.598	5.300	6.269	8.786	12.367	12.367
AE/AT		1.0000	1.1095	2.0273	4.0221	6.9325	9.0081	45.060	98.405	504.34	2497.35	2497.35
CSTAR, FT/SEC		7191	7191	7191	7191	7191	7191	7191	7191	7191	7191	7191
CF		0.715	0.931	1.259	1.440	1.536	1.573	1.722	1.764	1.819	1.847	1.847
IVAC, LB-SEC/LB		281.0	290.8	326.6	351.8	366.0	371.6	394.9	401.6	410.3	414.7	414.7
ISP, LB-SEC/LB		159.8	208.1	281.3	321.8	343.2	351.5	384.8	394.3	406.6	412.8	412.8

MOLE FRACTIONS

E	0.00294	F	0.21151	F-	0.00464	F2	0.00002
LI	0.12106	LI+	0.00758	LIF	0.65089	LI2	0.00028
LI2F2	0.00109						

ADDITIONAL PRODUCTS WHICH WERE CONSIDERED BUT WHOSE MOLE FRACTIONS WERE LESS THAN 0.50000E-05 FOR ALL ASSIGNED CONDITIONS

LI(S) LI(L) LIF(S) LIF(L) LIF2- LI3F3

Case 950 - Input

```

REACTANTS
H 2-
N 1.561760 .419590AR.009324C .000300      100.   0.   G298.15 F
N 1.561760 .419590AR.009324C .000300      100.  -28.2  G298.15 O

OMIT          C2H4          C3O2          H2O(S)        C(S)
OMIT          C2N2          H2O(L)        C2G           C2H2
OMIT          H02           H2O2          C2G           C2H2
OMIT          NH2           CH2           CH            NH3
OMIT          C2N           CH3           NO2           CH4
OMIT          HCN          C2H           C3            N2O
OMIT          N2C          C2            CN            HCO
OMIT          N2H4          N2O4          CN2           CN2
NAMELISTS
$INPT2 TP=T,P=.1,.01,ERATIO=T,MIX=1.5,1.2, T=3000,2000,KASE=950
  
```

Case 950 - Output

```

REACTANTS
H 2.0000      -0.      -0.      -0.      -0.      100.0000      0.   G   298.150  F  -0.
N 1.5618 D   0.4196 AR  0.0093 C   0.0003  -0.      100.0000      -28.20 G   298.150  O  -0.
OMIT          C2H4          C3O2          H2O(S)        C(S)
OMIT          C2N2          H2O(L)        C2G           C2H2
OMIT          H02           H2O2          C2G           C2H2
OMIT          NH2           CH2           CH            NH3
OMIT          C2N           CH3           NO2           CH4
OMIT          HCN          C2H           C3            N2O
OMIT          N2C          C2            CN            HCO
OMIT          N2H4          N2O4          CN2           CN2
NAMELISTS
  
```

\$INPT2

KASE = 950,

```

T = 3.0000000E+03, 2.0000000E+03, 0.      , 0.      , 0.      , 0.      , 0.      ,
0.      , 0.      , 0.      , 0.      , 0.      , 0.      , 0.      ,
0.      , 0.      , 0.      , 0.      , 0.      , 0.      , 0.      ,
0.      , 0.      , 0.      , 0.      , 0.      , 0.      , 0.      ,
0.      , 0.      , 0.      , 0.      , 0.      , 0.      , 0.      ,
0.      , 0.      , 0.      , 0.      , 0.      , 0.      , 0.      ,
0.      , 0.      , 0.      , 0.      , 0.      , 0.      , 0.      ,
0.      , 0.      , 0.      , 0.      , 0.      , 0.      , 0.      ,
  
```

```

P = 1.0000000E-01, 1.0000000E-02, 0.      , 0.      , 0.      , 0.      , 0.      ,
0.      , 0.      , 0.      , 0.      , 0.      , 0.      , 0.      ,
0.      , 0.      , 0.      , 0.      , 0.      , 0.      , 0.      ,
0.      , 0.      , 0.      , 0.      , 0.      , 0.      , 0.      ,
  
```

PSIA = F, MMHG = F, NSQM = F,

```

V = 0.      , 0.      , 0.      , 0.      , 0.      , 0.      , 0.      ,
0.      , 0.      , 0.      , 0.      , 0.      , 0.      , 0.      ,
0.      , 0.      , 0.      , 0.      , 0.      , 0.      , 0.      ,
  
```

```

RHD = 1.0000000E-01, 1.0000000E-02, 0.      , 0.      , 0.      , 0.      , 0.      ,
0.      , 0.      , 0.      , 0.      , 0.      , 0.      , 0.      ,
0.      , 0.      , 0.      , 0.      , 0.      , 0.      , 0.      ,
0.      , 0.      , 0.      , 0.      , 0.      , 0.      , 0.      ,
0.      , 0.      , 0.      , 0.      , 0.      , 0.      , 0.      ,
  
```

ERATIO= T, OF = F, FPCT = F, FA = F,

```

MIX = 1.5000000E+00, 1.0000000E+00, 2.0000000E+00, 0.      , 0.      , 0.      ,
0.      , 0.      , 0.      , 0.      , 0.      , 0.      , 0.      ,
0.      , 0.      , 0.      , 0.      , 0.      , 0.      , 0.      ,
  
```

TP = T, HP = F, SP = F, TV = F, UV = F, SV = F,

RKT = F, SHOCK = F, DETN = F, OTTD = F, CR = 0., SO = 0., SO = 0.,

IONS = F, IDEBUG= 0, TRACE = 0., SIUNIT= F, EUNITS= F,

TRNSPT= T, FROZN = F, PUNCH = F, NODATA= F,

\$ END

```

SPECIES BEING CONSIDERED IN THIS SYSTEM
L 5/66 AR      J 3/61 C           J 6/66 CNH          J 9/65 CO
J 9/65 CO2     L 5/72 C2H6          J12/69 C4          J 9/65 H
J12/70 H2CO   J 3/63 HNO          J 3/61 H2          J 3/61 N
J12/70 NCO    J12/71 NH          J 6/63 NO          J12/64 NO3        J 9/65 N2
J12/70 N3     J 6/62 O            J12/70 OH          J 9/65 O2          J 6/61 O3
  
```

DF = 22.849901

ENTHALPY (KG-MOL)(DEG K)/KG	EFFECTIVE FUEL HPP(2)	EFFECTIVE OXIDANT HPP(1)	MIXTURE HSUBO
0.	-0.48994914E+00	0.	-0.46940611E+00
KG-ATOMS/KG	BOP(I,2)	BOP(I,1)	BOP(I)
H	0.99209300E+00	0.	0.41597364E-01
N	0.	0.53920039E-01	0.51659231E-01
O	0.	0.14486419E-01	0.13879019E-01
AR	0.	0.32191274E-03	0.30841529E-03
C	0.	0.10357553E-04	0.99232720E-05

```

PT   H        N        O        AR        C
1   -12.567   -15.738   -18.416   -29.654   -26.227   17.000
2   -11.844   -14.915   -21.829   -28.570   -23.639    7.000
3   -14.101   -17.003   -19.689   -32.185   -27.408    5.000
4   -13.002   -16.067   -21.821   -30.875   -25.954    8.000
  
```

THERMODYNAMIC EQUILIBRIUM PROPERTIES AT ASSIGNED

CASE NO. 950
 TEMPERATURE AND PRESSURE
 CHEMICAL FORMULA
 FUEL H 2.00000
 OXIDANT N 1.56176 O 0.41959 AR 0.00932 C 0.00030
 WT FRACTION (SEE NOTE) 1.00000
 ENERGY CAL/MDL 0.
 STATE G
 TEMP DEG K 298.15
 DENSITY G/CC -0.
 D/F= 22.8499 PERCENT FUEL= 4.1929 EQUIVALENCE RATIO= 1.5000 REACTANT DENSITY= 0.

THERMODYNAMIC PROPERTIES

P, ATM 0.1000 0.1000 0.0100 0.0100
 T, DEG K 3000 2000 3000 2000
 RHO, G/CC 7.1132-6 1.2964-5 5.6618-7 1.2930-6
 H, CAL/G 1551.2 -117.7 3222.6 -103.6
 S, CAL/(G)(K) 3.6980 3.0712 4.5486 3.2936
 M, MDL WT 17.510 21.275 13.937 21.220
 (DLV/DLP)T -1.08647 -1.00060 -1.08691 -1.00193
 (DLV/DLT)P 2.6852 1.0172 2.6389 1.0556
 CP, CAL/(G)(K) 4.2389 0.4965 4.9243 0.6014
 GAMMA (S) 1.1193 1.2408 1.1296 1.2071
 SON VEL, M/SEC 1262.7 984.8 1421.8 972.6

MOLE FRACTIONS

AR 0.00540 0.00656 0.00430 0.00654
 CO 0.00016 0.00015 0.00013 0.00015
 CO2 0.00002 0.00006 0.00000 0.00007
 H 0.18282 0.00196 0.39418 0.00616
 H2 0.13549 0.14675 0.06299 0.14483
 H2O 0.11209 0.29458 0.01459 0.29282
 N 0.00003 0. 0.00008 0.
 NO 0.00971 0.00003 0.00767 0.00009
 N2 0.44742 0.54952 0.35612 0.54805
 O 0.04229 0.00000 0.11840 0.00004
 OH 0.05041 0.00039 0.03043 0.00122
 O2 0.01417 0.00000 0.01110 0.00003

ADDITIONAL PRODUCTS WHICH WERE CONSIDERED BUT WHOSE MOLE FRACTIONS WERE LESS THAN 0.50000E-05 FOR ALL ASSIGNED CONDITIONS

C CH2O CNN C2H6 C4 C5 H2CO HNO NCO NH
 NO3 N3 O3

NOTE. WEIGHT FRACTION OF FUEL IN TOTAL FUELS AND OF OXIDANT IN TOTAL OXIDANTS

TRANSPORT PROPERTIES AT ASSIGNED TEMPERATURE AND PRESSURE

D/F= 22.8499 PERCENT FUEL= 4.1929 EQUIVALENCE RATIO= 1.5000 FIRST PRESSURE= 0.100 ATM

TEMP	VISCOSITY	MONATOMIC COND	INTERNAL COND	FROZEN COND	REACTION COND	EQUILIBRIUM COND	CP FROZ	CP EQ	PRANDTL FROZ	PRANDTL EQ	LEWIS NUMBER
DEG K	POISE	CAL/(CM)(SEC)(K)			CAL/(G)(K)		CAL/(G)(K)		DIMENSIONLESS		
3000	839.X10-6	563.X10-6	285.X10-6	848.X10-6	10172.X10-6	11020.X10-6	0.4838	4.2389	0.4789	0.3227	1.5462
2000	640.	255.	227.	482.	151.	633.	0.4499	0.4965	0.5971	0.5021	3.0156
3000	808.	829.	173.	1003.	10027.	11029.	0.4968	4.9243	0.4003	0.3608	1.1220
2000	640.	258.	226.	484.	475.	959.	0.4501	0.6014	0.5951	0.4014	2.9182

UF = 34.291058

ENTHALPY (KG-MOL)(DEG K)/KG	EFFECTIVE FUEL HPP(2)	EFFECTIVE OXIDANT HPP(1)	MIXTURE HSUB0
	0.	-0.48994914E+00	-0.47606605E+00
KG-ATOMS/KG	BOP(1,2)	BOP(1,1)	BO(1)
H	0.99209300E+00	0.	0.28111739E-01
N	0.	0.53920039E-01	0.52392171E-01
O	0.	0.14486419E-01	0.14075934E-01
AR	0.	0.32191274E-03	0.31279108E-03
C	0.	0.10357553E-04	0.10064063E-04

PT	H	N	O	AR	C	
1	-12.809	-15.669	-18.085	-29.513	-26.456	5.000
2	-13.412	-14.836	-18.557	-28.413	-28.927	7.000
3	-14.309	-16.920	-19.494	-32.017	-27.442	5.000
4	-14.200	-15.991	-19.315	-30.721	-29.806	8.000

THERMODYNAMIC EQUILIBRIUM PROPERTIES AT ASSIGNED

TEMPERATURE AND PRESSURE

CASE NO. 950
 CHEMICAL FORMULA
 FUEL H 2.00000
 OXIDANT N 1.56176 O 0.41959 AR 0.00932 C 0.00030
 WT FRACTION (SEE NOTE) \ CAL/MOL
 1.00000 0. G 298.15 -0.
 1.00000 -28.200 G 298.15 -0.
 D/F= 34.2911 PERCENT FUEL= 2.8336 EQUIVALENCE RATIO= 1.0000 REACTANT DENSITY= 0.

THERMODYNAMIC PROPERTIES

P, ATM 0.1000 0.1000 0.0100 0.0100
 T, DEG K 3000 2000 3000 2000
 RHD, G/CC 8.0798-6 1.4956-5 6.6021-7 1.4877-6
 H, CAL/G 1372.4 -193.6 2659.6 -166.6
 S, CAL/(G)(K) 3.3290 2.7344 4.0132 2.9347
 H, MOL WT 19.890 24.545 16.252 24.415
 (DLV/DLP)T -1.07939 -1.00143 -1.07450 -1.00352
 (DLV/DLP)P 2.5496 1.0454 2.4081 1.1093
 CP, CAL/(G)(K) 3.4784 0.5174 3.7121 0.6795
 GAMMA (S) 1.1202 1.2042 1.1319 1.1681
 SON VEL,M/SEC 1185.3 903.2 1318.0 891.9

MOLE FRACTIONS

AR 0.00622 0.00768 0.00508 0.00764
 CO 0.00017 0.00002 0.00016 0.00004
 CO2 0.00003 0.00023 0.00001 0.00021
 H 0.14373 0.00041 0.32026 0.00186
 H2 0.08374 0.00638 0.04158 0.01318
 H2O 0.09639 0.33736 0.01170 0.32680
 N 0.00003 0. 0.00009 0.
 NO 0.01448 0.00077 0.01013 0.00114
 N2 0.51378 0.64260 0.42063 0.63900
 O 0.05885 0.00010 0.14391 0.00048
 OH 0.05514 0.00212 0.03004 0.00453
 O2 0.02743 0.00233 0.01640 0.00513

ADDITIONAL PRODUCTS WHICH WERE CONSIDERED BUT WHOSE MOLE FRACTIONS WERE LESS THAN 0.50000E-05 FOR ALL ASSIGNED CONDITIONS

C CH2O CNN C2H6 C4 C5 HNCO HNO NCO NH
 NO3 N3 O3

NOTE. WEIGHT FRACTION OF FUEL IN TOTAL FUELS AND OF OXIDANT IN TOTAL OXIDANTS

TRANSPORT PROPERTIES AT ASSIGNED TEMPERATURE AND PRESSURE

D/F= 34.2911 PERCENT FUEL= 2.8336 EQUIVALENCE RATIO= 1.0000 FIRST PRESSURE= 0.100 ATM

TEMP DEG K	VISCOSITY POISE	MUNATOMIC COND	INTERNAL COND	FROZEN COND	REACTION COND	EQUILIBRIUM COND	CP FROZ	CP EQ	PRANDTL FROZ	PRANDTL EQ	LEWIS NUMBER
3000	855.X10-6	467.X10-6	240.X10-6	707.X10-6	8287.X10-6	8995.X10-6	0.4271	3.4784	0.5164	0.3307	1.6400
2000	661.	206.	186.	391.	194.	585.	0.3988	0.5174	0.6739	0.5849	1.6634
3000	830.	682.	157.	838.	7227.	8065.	0.4369	3.7121	0.4326	0.3820	1.1502
2000	660.	208.	186.	394.	507.	901.	0.3990	0.6795	0.6686	0.4980	1.8302

DF = 17.133338

ENTHALPY (KG-MOL)(DEG K)/KG	EFFECTIVE FUEL HPP(2)	EFFECTIVE OXIDANT HPP(1)	MIXTURE HSUBO
0.	0.	-0.48994914E+00	-0.46292989E+00
KG-ATOMS/KG	BOP(1,2)	BOP(1,1)	B0(1)
H	0.99209300E+00	0.	0.54710996E-01
N	0.	0.53920039E-01	0.50946508E-01
O	0.	0.14486419E-01	0.13687535E-01
AR	0.	0.32191274E-03	0.30416020E-03
C	0.	0.10357553E-04	0.97863643E-05

PT	H	N	O	AR	C
1	-12.415	-15.802	-18.700	-29.785	-26.048
2	-11.566	-14.986	-22.522	-28.708	-22.917
3	-13.976	-17.075	-19.854	-32.329	-27.382
4	-12.723	-16.137	-22.515	-31.014	-25.231

THERMODYNAMIC EQUILIBRIUM PROPERTIES AT ASSIGNED

TEMPERATURE AND PRESSURE

CASE NO. 950

CHEMICAL FORMULA				WT FRACTION	ENERGY	STATE	TEMP	DENSITY
FUEL	H	2.00000		(SEE NOTE)	CAL/MOL		DEG K	G/CC
OXIDANT	N	1.56176	O 0.41959 AR 0.00932 C 0.00030	1.00000	0.	G	298.15	-0.
				1.00000	-28.200	G	298.15	-0.

O/F= 17.1333 PERCENT FUEL= 5.5147 EQUIVALENCE RATIO= 2.0000 REACTANT DENSITY= 0.

THERMODYNAMIC PROPERTIES

P, ATM	0.1000	0.1000	0.0100	0.0100
T, DEG K	3000	2000	3000	2000
RHO, G/CC	6.3311-6	1.1450-5	4.9731-7	1.1414-6
H, CAL/G	1774.4	-27.3	3769.9	-8.9
S, CAL/(G)(K)	4.0682	3.3911	5.3648	3.6441
M, MOL WT	15.585	18.790	12.242	18.732
(DLV/DLP)F	-1.08791	-1.00072	-1.03487	-1.00226
(DLV/DLTP)	2.7067	1.0201	2.7866	1.0636
CP, CAL/(G)(K)	4.7915	0.5595	6.0360	0.6904
GAMMA (S)	1.1199	1.2437	1.1286	1.2071
SON VFL,M/SEC	1338.8	1049.1	1516.4	1035.1

MOLE FRACTIONS

AR	0.00474	0.00572	0.00372	0.00570
CO	0.00014	0.00015	0.00012	0.00015
CO2	0.00001	0.00003	0.00000	0.00003
H	0.21280	0.00259	0.44687	0.00813
H2	0.18358	0.25589	0.08095	0.25266
H2O	0.11428	0.25670	0.01589	0.25530
N	0.00003	0.	0.00008	0.
NO	0.00685	0.00001	0.00605	0.00004
N2	0.39356	0.47864	0.30878	0.47715
O	0.03183	0.00000	0.10033	0.00002
OH	0.04415	0.00026	0.02923	0.00081
O2	0.00802	0.00000	0.00797	0.00001

ADDITIONAL PRODUCTS WHICH WERE CONSIDERED BUT WHOSE MOLE FRACTIONS WERE LESS THAN 0.50000E-05 FOR ALL ASSIGNED CONDITIONS

C	CH2O	CNN	C2H6	C4	C5	HNCO	HNO	NCO	NH
NO3	N3	O3							

NOTE. WEIGHT FRACTION OF FUEL IN TOTAL FUELS AND OF OXIDANT IN TOTAL OXIDANTS

TRANSPORT PROPERTIES AT ASSIGNED TEMPERATURE AND PRESSURE

O/F= 17.1333 PERCENT FUEL= 5.5147 EQUIVALENCE RATIO= 2.0000 FIRST PRESSURE= 0.100 ATM

TEMP DEG K	VISCOSITY POISE	MONATOMIC COND	INTERNAL COND	FROZEN COND	REACTION COND	EQUILIBRIUM COND	CP	CP	PRANDTL FROZ	PRANDTL EQ	LEWIS NUMBER
							FROZ	EQ			
							CAL/(G)(K)		---- DIMENSIONLESS ----		
3000	820.X10-6	653.X10-6	325.X10-6	978.X10-6	11644.X10-6	12622.X10-6	0.5393	4.7915	0.4524	0.3114	1.5103
2000	621.	302.	263.	565.	204.	769.	0.4996	0.5595	0.5484	0.4516	3.0043
3000	787.	954.	189.	1143.	12426.	13569.	0.5550	6.0360	0.3822	0.3502	1.1004
2000	621.	306.	262.	568.	638.	1206.	0.4999	0.6904	0.5463	0.3552	2.9504



Case 1207 - Input

```

REACTANTS
H 2.          00      0.050 M      G 300.00
O 2.          00      0.050 M      G 300.00
AR1.         00      0.900 M      G 300.00
  
```

```

NAMELISTS
$INPT2 KASE=1207,P=10,20,MMHG=T, SHOCK=T
$SHKINP U1=1000,1100,1200,1250,1300,1350,1400,1450,1500, INCDEQ=T,INCDZF=T $
  
```

Case 1207 - Output

```

REACTANTS
H 2.0000      -0.      -0.      -0.      00 -0.      0.0500 M      -0.      G 300.000      -0.
O 2.0000      -0.      -0.      -0.      00 -0.      0.0500 M      -0.      G 300.000      -0.
AR 1.0000     -0.      -0.      -0.      00 -0.      0.9000 M      -0.      G 300.000      -0.
NAMELISTS
  
```

\$INPT2

KASE = 1207,

```

T = 0.      , 0.      , 0.      , 0.      , 0.      , 0.      , 0.      , 0.      ,
    0.      , 0.      , 0.      , 0.      , 0.      , 0.      , 0.      , 0.      ,
    0.      , 0.      , 0.      , 0.      , 0.      , 0.      , 0.      , 0.      ,
    0.      , 0.      , 0.      , 0.      , 0.      , 0.      , 0.      , 0.      ,
    0.      , 0.      , 0.      , 0.      , 0.      , 0.      , 0.      , 0.      ,
    0.      , 0.      , 0.      , 0.      , 0.      , 0.      , 0.      , 0.      ,
    0.      , 0.      , 0.      , 0.      , 0.      , 0.      , 0.      , 0.      ,
  
```

```

P = 1.0000000E+01, 2.0000000E+01, 0.      , 0.      , 0.      , 0.      , 0.      , 0.      ,
    0.      , 0.      , 0.      , 0.      , 0.      , 0.      , 0.      , 0.      ,
    0.      , 0.      , 0.      , 0.      , 0.      , 0.      , 0.      , 0.      ,
    0.      , 0.      , 0.      , 0.      , 0.      , 0.      , 0.      , 0.      ,
  
```

PSIA = F, MMHG = T, NSQM = F,

```

V = 0.      , 0.      , 0.      , 0.      , 0.      , 0.      , 0.      , 0.      ,
    0.      , 0.      , 0.      , 0.      , 0.      , 0.      , 0.      , 0.      ,
    0.      , 0.      , 0.      , 0.      , 0.      , 0.      , 0.      , 0.      ,
  
```

```

RHO = 1.0000000E+01, 2.0000000E+01, 0.      , 0.      , 0.      , 0.      , 0.      , 0.      ,
    0.      , 0.      , 0.      , 0.      , 0.      , 0.      , 0.      , 0.      ,
    0.      , 0.      , 0.      , 0.      , 0.      , 0.      , 0.      , 0.      ,
    0.      , 0.      , 0.      , 0.      , 0.      , 0.      , 0.      , 0.      ,
  
```

EKRATIO= F, DF = F, FPCT = F, FA = F,

```

MIX = 0.      , 0.      , 0.      , 0.      , 0.      , 0.      , 0.      , 0.      ,
    0.      , 0.      , 0.      , 0.      , 0.      , 0.      , 0.      , 0.      ,
    0.      , 0.      , 0.      , 0.      , 0.      , 0.      , 0.      , 0.      ,
  
```

TP = F, HP = F, SP = F, TV = F, UV = F, SV = F,

RKT = F, SHOCK = T, DETN = F, DTTU = F, CR = 0. , SO = 0. , SO = 0. ,

IONS = F, IDEBUG= 0, TRACE = 0. , SIUNIT= F, EUNITS= F,

TRANSPT= T, FRUZN = F, PUNCH = F, NODATA= F,

\$ END

NO INPT2 VALUE GIVEN FOR DF, EQRAT, FA, OR FPCT

SPECIES BEING CONSIDERED IN THIS SYSTEM

```

L 5/66 AR      J 9/65 H      J 3/64 H02      J 3/61 H2      L11/65 H2O(S)
L11/65 H2O(L)  J 3/61 H2U      L 2/69 H2O2      J 6/62 O      J12/70 OH
J 9/65 O2      J 6/61 O3
  
```

\$SHKINP

```

U1 = 1.0000000E+03, 1.1000000E+03, 1.2000000E+03, 1.2500000E+03, 1.3000000E+03, 1.3500000E+03,
    1.4000000E+03, 1.4500000E+03, 1.5000000E+03, 0.      , 0.      , 0.      ,
  
```

```

MACH1 = 0.      , 0.      , 0.      , 0.      , 0.      , 0.      , 0.      , 0.      ,
    0.      , 0.      , 0.      , 0.      , 0.      , 0.      , 0.      , 0.      ,
    0.      , 0.      , 0.      , 0.      , 0.      , 0.      , 0.      , 0.      ,
  
```

GAMMA1= 0. , INCDEQ= T, REFLDQ= F, INCDZF= T, REFLFZ= F, A1 = 1.0000000E+00,

\$ END

UF = 0.

ENTHALPY (KGMOL)(DEG K)/KG	EFFECTIVE FUEL HPP(2)	EFFECTIVE OXIDANT HPP(1)	MIXTURE HSUBO
KG-ATOMS/KG	BOP(1,2)	BOP(1,1)	B0(1)
H	0.26557648E-02	0.	0.26557648E-02
O	0.26557648E-02	0.	0.26557648E-02
AR	0.23901883E-01	0.	0.23901883E-01

SHOCK WAVE PARAMETERS ASSUMING
EQUILIBRIUM COMPOSITION FOR INCIDENT SHOCKED CONDITIONS

CASE NO. 1207

CHEMICAL FORMULA		MOLES		ENERGY	STATE	TEMP	DENSITY
FUEL	H 2.00000	0.05000	13.478	G	300.00	-0.	
FUEL	O 2.00000	0.05000	12.892	G	300.00	-0.	
FUEL	AR 1.00000	0.90000	9.191	G	300.00	-0.	

O/F= 0. PERCENT FUEL=100.0000 EQUIVALENCE RATIO= 0.5000 REACTANT DENSITY= 0.

INITIAL GAS (1)	3.0480	3.3528	3.6576	3.8100	3.9624	4.1148	4.2672	4.4196	4.5720
MACH NO.	1000.00	1100.00	1200.00	1250.00	1300.00	1350.00	1400.00	1450.00	1500.00
U1, M/SEC	0.0132	0.0263	0.0263	0.0263	0.0263	0.0263	0.0263	0.0263	0.0263
P, ATM	300	300	300	300	300	300	300	300	300
T, DEG K	2.0126-5	4.0253-5	4.0253-5	4.0253-5	4.0253-5	4.0253-5	4.0253-5	4.0253-5	4.0253-5
RHO, G/CC	0.3	0.3	0.3	0.3	0.3	0.3	0.3	0.3	0.3
H, CAL/G	1.2406	1.2041	1.2041	1.2041	1.2041	1.2041	1.2041	1.2041	1.2041
S, CAL/(G)(K)	37.654	37.654	37.654	37.654	37.654	37.654	37.654	37.654	37.654
M, MOL WT	0.1372	0.1372	0.1372	0.1372	0.1372	0.1372	0.1372	0.1372	0.1372
CP, CAL/(G)(K)	1.6249	1.6249	1.6249	1.6249	1.6249	1.6249	1.6249	1.6249	1.6249
GAMMA (S)	328.1	328.1	328.1	328.1	328.1	328.1	328.1	328.1	328.1
SON VEL, M/SEC									

UID NOT CONVERGE FOR U1= 1000.00 ANSWERS PROBABLY NOT RELIABLE, SOLUTION MAY NOT EXIST

SHOCKED GAS (2)--INCIDENT--EQUILIBRIUM	575.88	667.74	576.55	560.68	549.47	540.62	532.79	525.22	517.53
U2, M/SEC	3.1145	0.2152	0.3235	0.3686	0.4139	0.4604	0.5086	0.5590	0.6118
P, ATM	1542	1527	1817	1933	2044	2153	2259	2361	2457
T, DEG K	3.4949-5	6.6310-5	8.3781-5	8.9742-5	9.5234-5	1.0052-4	1.0577-4	1.1113-4	1.1667-4
RHO, G/CC	93.6	91.6	132.6	149.4	166.1	183.1	200.6	218.6	237.1
H, CAL/G	1.3281	1.2943	1.2979	1.3001	1.3026	1.3052	1.3080	1.3109	1.3139
S, CAL/(G)(K)	38.619	38.619	38.614	38.608	38.597	38.580	38.552	38.510	38.453
M, MOL WT	-1.00001	-1.00000	-1.00005	-1.00010	-1.00021	-1.00041	-1.00073	-1.00123	-1.00193
(DLV/DLP) F	1.0003	1.0002	1.0018	1.0037	1.0070	1.0124	1.0208	1.0330	1.0493
(DLV/DLT) P	0.1404	0.1401	0.1442	0.1477	0.1530	0.1611	0.1726	0.1882	0.2078
CP, CAL/(G)(K)	1.5792	1.5807	1.5582	1.5410	1.5173	1.4865	1.4501	1.4111	1.3733
GAMMA (S)	724.0	721.0	780.8	800.8	817.4	830.6	840.6	848.1	854.2
SON VEL, M/SEC	5.915	8.178	12.294	14.008	15.729	17.495	19.328	21.243	23.247
P2/P1	4.428	5.092	6.057	6.442	6.815	7.178	7.531	7.870	8.191
T2/T1	1.0256	1.0256	1.0255	1.0253	1.0251	1.0246	1.0238	1.0227	1.0212
M2/M1	1.7365	1.6473	2.0814	2.2294	2.3659	2.4971	2.6277	2.7607	2.8984
RHO2/RHO1	424.12	432.26	623.45	689.32	750.53	809.38	857.21	924.78	982.47
V2(U1-U2)M/SEC									

MOLE FRACTIONS

AR	9.2406-1	9.2306-1	9.2294-1	9.2280-1	9.2255-1	9.2213-1	9.2146-1	9.2047-1	9.1910-1
H	1.4775-7	7.1348-8	4.3013-6	1.5667-5	4.7584-5	1.2521-4	2.9107-4	6.0405-4	1.1305-3
H2	9.8099-9	1.0366-8	6.7804-8	1.2217-7	2.0224-7	3.1325-7	4.5774-7	6.3422-7	8.3714-7
H2	3.0708-6	1.8670-6	3.5421-5	8.9393-5	1.9761-4	3.9339-4	7.1392-4	1.1893-3	1.8303-3
H2O	5.1238-2	5.1249-2	5.1028-2	5.0786-2	5.0385-2	4.9758-2	4.8834-2	4.7553-2	4.5891-2
H2O2	7.212-10	9.131-10	4.464 -9	7.362 -9	1.131 -8	1.642 -8	2.267 -8	2.984 -8	3.758 -8
J	3.3010-6	2.0013-6	3.9835-5	1.0712-4	2.2910-4	4.6321-4	8.5589-4	1.4579-3	2.3083-3
OH	7.8598-5	5.9618-5	4.1738-4	7.6735-4	1.2423-3	2.0296-3	2.9976-3	4.1846-3	5.5478-3
O2	2.5621-2	2.5626-2	2.5532-2	2.5439-2	2.5299-2	2.5103-2	2.4848-2	2.4539-2	2.4187-2

ADDITIONAL PRODUCTS WHICH WERE CONSIDERED BUT WHOSE MOLE FRACTIONS WERE LESS THAN 0.50000E-08 FOR ALL ASSIGNED CONDITIONS

H2O(S) H2O(L) O3

TRANSPORT PROPERTIES OF THE SHOCKED GAS ASSUMING EQUILIBRIUM COMPOSITION

O/F= 0. PERCENT FUEL=100.0000 EQUIVALENCE RATIO= 0.5000 FIRST SHOCK PRESSURE= 0.1145 ATM

TEMP	VISCOSITY	MONATOMIC COND	INTERNAL COND	FROZEN COND	REACTION COND	EQUILIBRIUM COND	CP FROZ	CP EQ	PRANDTL FROZ	PRANDTL EQ	LEWIS NUMBER
DEG K	POISE	CAL/(CM)(SEC)(K)						CAL/(G)(K)		DIMENSIONLESS	
1542	723.X10-6	140.X10-6	13.X10-6	153.X10-6	1.X10-6	154.X10-6	0.1396	0.1404	0.6600	0.6581	1.5041
1527	719.	139.	13.	152.	1.	153.	0.1395	0.1401	0.6602	0.6590	1.4339
1817	807.	156.	16.	173.	8.	181.	0.1405	0.1442	0.6570	0.6436	1.8061
1933	842.	163.	18.	181.	18.	198.	0.1408	0.1477	0.6558	0.6268	1.9897
2044	874.	169.	19.	188.	35.	223.	0.1411	0.1530	0.6545	0.5992	2.1791
2153	906.	176.	20.	196.	65.	261.	0.1413	0.1611	0.6530	0.5995	2.3617
2259	936.	182.	21.	203.	113.	316.	0.1416	0.1726	0.6512	0.5112	2.5206
2361	965.	188.	22.	211.	182.	393.	0.1418	0.1882	0.6488	0.4620	2.6397
2457	992.	195.	23.	218.	274.	492.	0.1420	0.2078	0.6456	0.4187	2.7101

SHOCK WAVE PARAMETERS ASSUMING
FROZEN COMPOSITION FOR INCIDENT SHOCKED CONDITIONS

CASE NO. 1207

CHEMICAL FORMULA		MOLES	ENERGY	STATE	TEMP	DENSITY
			CAL/MOL		DEG K	G/CC
FUEL	H 2.00000	0.05000	13.478	G	300.00	-0.
FUEL	O 2.00000	0.05000	12.892	G	300.00	-0.
FUEL	AR 1.00000	0.90000	9.191	G	300.00	-0.

D/F= 0. PERCENT FUEL=100.0000 EQUIVALENC RATIO= 0.5000 REACTANT DENSITY= 0.

INITIAL GAS (1)

MACH NO.	3.0480	3.3528	3.6576	3.8100	3.9624	4.1148	4.2672	4.4196	4.5720
U1, M/SEC	1000.00	1100.00	1200.00	1250.00	1300.00	1350.00	1400.00	1450.00	1500.00
P, ATM	0.0132	0.0263	0.0263	0.0263	0.0263	0.0263	0.0263	0.0263	0.0263
T, DEG K	300	300	300	300	300	300	300	300	300
RHO, G/CC	2.0126-5	4.0253-5	4.0253-5	4.0253-5	4.0253-5	4.0253-5	4.0253-5	4.0253-5	4.0253-5
H, CAL/G	0.3	0.3	0.3	0.3	0.3	0.3	0.3	0.3	0.3
S, CAL/(G)(K)	1.2406	1.2041	1.2041	1.2041	1.2041	1.2041	1.2041	1.2041	1.2041
M, MOL WT	37.654	37.654	37.654	37.654	37.654	37.654	37.654	37.654	37.654
CP, CAL/(G)(K)	0.1372	0.1372	0.1372	0.1372	0.1372	0.1372	0.1372	0.1372	0.1372
GAMMA (S)	1.6249	1.6249	1.6249	1.6249	1.6249	1.6249	1.6249	1.6249	1.6249
SON VEL, M/SEC	328.1	328.1	328.1	328.1	328.1	328.1	328.1	328.1	328.1

SHOCKED GAS (2)--INCIDENT--FROZEN

U2, M/SEC	317.25	332.77	349.41	358.06	366.89	375.88	385.00	394.24	403.59
P, ATM	0.1488	0.3616	0.4318	0.4692	0.5082	0.5487	0.5908	0.6345	0.6797
T, DEG K	1076	1247	1433	1532	1635	1742	1852	1967	2085
RHO, G/CC	6.3440-5	1.3306-4	1.3824-4	1.4052-4	1.4263-4	1.4457-4	1.4637-4	1.4805-4	1.4961-4
H, CAL/G	107.7	131.5	157.7	171.7	186.1	201.2	216.8	232.9	249.7
S, CAL/(G)(K)	1.2892	1.2629	1.2731	1.2781	1.2830	1.2879	1.2927	1.2974	1.3020
M, MOL WT	37.654	37.654	37.654	37.654	37.654	37.654	37.654	37.654	37.654
CP, CAL/(G)(K)	0.1396	0.1400	0.1404	0.1407	0.1409	0.1411	0.1413	0.1415	0.1418
GAMMA (S)	1.6079	1.6050	1.6020	1.6005	1.5990	1.5975	1.5960	1.5945	1.5930
SON VEL, M/SEC	618.1	664.8	712.1	735.9	759.8	783.8	807.9	832.1	856.3

P2/P1	11.307	13.741	16.409	17.831	19.312	20.852	22.451	24.110	25.827
T2/T1	3.587	4.157	4.778	5.108	5.450	5.806	6.174	6.555	6.949
M2/M1	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000
RHO2/RHO1	3.1521	3.3056	3.4343	3.4910	3.5433	3.5916	3.6364	3.6779	3.7167
V2(U1-U2)M/SEC	682.75	767.23	850.59	891.94	933.11	974.12	1015.00	1055.76	1096.41

MOLE FRACTIONS

H2	0.05000	0.05000	0.05000	0.05000	0.05000	0.05000	0.05000	0.05000	0.05000
O2	0.05000	0.05000	0.05000	0.05000	0.05000	0.05000	0.05000	0.05000	0.05000
AR	0.90000	0.90000	0.90000	0.90000	0.90000	0.90000	0.90000	0.90000	0.90000

TRANSPORT PROPERTIES OF THE SHOCKED GAS ASSUMING FROZEN COMPOSITION

D/F= 0. PERCENT FUEL=100.0000 EQUIVALENC RATIO= 0.5000 FIRST SHOCK PRESSURE= 0.1488 ATM

TEMP	VISCOSITY	MONATOMIC	INTERNAL	FROZEN	CP	PRANDTL
DEG K	POISE	COND	COND	COND	FROZ	FROZ
		----	----	----	----	----
		CAL/(CM)(SEC)(K)	CAL/(CM)(SEC)(K)	CAL/(G)(K)		
1076	570.X10-6	125.X10-6	14.X10-6	140.X10-6	0.1396	0.5706
1247	630.	139.	17.	155.	0.1400	0.5673
1433	691.	152.	20.	172.	0.1404	0.5661
1532	722.	159.	21.	181.	0.1407	0.5625
1635	754.	166.	23.	189.	0.1409	0.5608
1742	786.	174.	25.	198.	0.1411	0.5591
1852	819.	181.	27.	208.	0.1413	0.5574
1967	852.	188.	29.	217.	0.1415	0.5558
2085	886.	196.	31.	227.	0.1418	0.5542

Case 1565 - Input

```

REACTANTS
N 2.          00      .75524      G647.95  0
O 2.          00      .23144      G647.95  0
AR1.         00      .01286      G647.95  0
C 1.         0 2.      .00046      G647.95  0
C 7.         H 8.      .4          2867.   L 298.15  F
C 8.         H 18.     .6          -59740. L 298.15  F
    
```

```

NAMELISTS
$INPT2 KASE=1565, UV=1,V=300,225.24, OF=T,MIX=17,TRACE=1.E-15 $
    
```

Case 1565 - Output

```

REACTANTS
N 2.0000      -0.      -0.      -0.      00 -0.      0.7552      -0.   G   647.950  0  -0.
O 2.0000      -0.      -0.      -0.      00 -0.      0.2314      -0.   C   647.950  0  -0.
AR 1.0000      -0.      -0.      -0.      00 -0.      0.0129      -0.   C   647.950  0  -0.
C 1.0000  O 2.0000      -0.      -0.      -0.      00 -0.      0.0005      -0.   C   647.950  0  -0.
C 7.0000  H 8.0000      -0.      -0.      -0.      -0.      0.4000      2867.00  L 298.150  F  -0.
C 8.0000  H 18.0000      -0.      -0.      -0.      -0.      0.6000      -59740.00 L 298.150  F  -0.
NAMELISTS
    
```

\$INPT2

KASE = 1565,

```

T = 0.      , 0.      , 0.      , 0.      , 0.      , 0.      , 0.      , 0.      ,
    0.      , 0.      , 0.      , 0.      , 0.      , 0.      , 0.      , 0.      ,
    0.      , 0.      , 0.      , 0.      , 0.      , 0.      , 0.      , 0.      ,
    0.      , 0.      , 0.      , 0.      , 0.      , 0.      , 0.      , 0.      ,
    0.      , 0.      , 0.      , 0.      , 0.      , 0.      , 0.      , 0.      ,
    0.      , 0.      , 0.      , 0.      , 0.      , 0.      , 0.      , 0.      ,
    0.      , 0.      , 0.      , 0.      , 0.      , 0.      , 0.      , 0.      ,
    
```

```

P = 0.      , 0.      , 0.      , 0.      , 0.      , 0.      , 0.      , 0.      ,
    0.      , 0.      , 0.      , 0.      , 0.      , 0.      , 0.      , 0.      ,
    0.      , 0.      , 0.      , 0.      , 0.      , 0.      , 0.      , 0.      ,
    0.      , 0.      , 0.      , 0.      , 0.      , 0.      , 0.      , 0.      ,
    
```

```

PSIA = F, MMHG = F, NSQM = F,
V = 3.0000000E+02, 2.2524000E+02, 0.      , 0.      , 0.      , 0.      ,
    0.      , 0.      , 0.      , 0.      , 0.      , 0.      ,
    
```

```

RHO = 0.      , 0.      , 0.      , 0.      , 0.      , 0.      , 0.      , 0.      ,
    0.      , 0.      , 0.      , 0.      , 0.      , 0.      , 0.      , 0.      ,
    0.      , 0.      , 0.      , 0.      , 0.      , 0.      , 0.      , 0.      ,
    0.      , 0.      , 0.      , 0.      , 0.      , 0.      , 0.      , 0.      ,
    
```

```

ERATIO= F, OF = T, FPCT = F, FA = F,
MIX = 1.7000000E+01, 0.      , 0.      , 0.      , 0.      , 0.      , 0.      , 0.      ,
    0.      , 0.      , 0.      , 0.      , 0.      , 0.      , 0.      , 0.      ,
    
```

```

TP = F, HP = F, SP = F, TV = F, UV = T, SV = F,
RKT = F, SHOCK = F, DETN = F, DTTO = F, CR = 0.      , SO = 0.      , SO = 0.      ,
    
```

```

IONS = F, IDEBUG= 0, TRACE = 1.0000000E-15, SIUNIT= F, EUNITS= F,
TRANSP= T, FROZN = F, PUNCH = F, NODATA= F,
    
```

\$ END

SPECIES BEING CONSIDERED IN THIS SYSTEM

L 5/66 AR	J 3/61 C(S)	J 3/61 C	J12/67 CH	J 6/69 CH2
J 3/61 CH2O	J 6/69 CH3	J 3/61 CH4	J 6/69 CN	J 6/66 CNN
J12/70 CN2	J 9/65 CO	J 9/65 CO2	J12/69 C2	J 3/67 C2H
J 3/61 C2H2	J 9/65 C2H4	L 5/72 C2H6	J 3/67 C2N	J 3/61 C2N2
J 9/66 C2O	J12/69 C3	J 6/68 C3O2	J12/69 C4	J12/69 C5
J 9/65 H	L12/69 HCN	J12/70 HCO	J12/70 HNC0	J 3/63 HNO
J 3/64 H02	J 3/61 H2	L11/65 H2O(S)	L11/65 H2O(L)	J 3/61 H2O
L 2/69 H2O2	J 3/61 H	J12/70 NCO	J12/71 NH	J12/65 NH2
J 9/65 NH3	J 6/63 N0	J 9/64 N02	J12/64 N03	J 9/65 N2
J12/65 N2H4	J12/64 N2U	J 9/64 N2O4	J12/70 N3	J 6/62 O
J12/70 OH	J 9/65 U2	J 6/61 O3		

OF = 17.000000

INTERNAL ENERGY (KG-MOL)(DEG K)/KG	EFFECTIVE FUEL HPP(2) -0.15164043E+33	EFFECTIVE OXIDANT HPP(1) 0.20365920E+02	MIXTURE HSURO 0.10810011E+02
KG-ATOMS/KG	BOP(I,2)	BOP(I,1)	B0(I)
N	0.	0.53919910E-01	0.50924358E-01
O	0.	0.14486447E-01	0.13681644E-01
AR	0.	0.32191849E-03	0.30403413E-03
C	0.72407449E-01	0.10452182E-04	0.40325075E-02
H	0.12927296E+00	0.	0.71818314E-02

```

PT      N      O      AR      C      H
1 -12.574 -15.095 -23.385 -19.796 -11.805 14.000
2 -12.385 -14.965 -23.104 -19.710 -11.711 3.000
    
```



Thermodynamic Equilibrium Combustion Properties at Assigned Volume

CASE NO. 1565

VOLUME

CHEMICAL FORMULA	WT FRACTION (SEE NOTE)	ENERGY KCAL/MOL	STATE	TEMP DEG K	DENSITY G/CC
OXIDANT N 2.00000	0.75524	1134.555	G	647.95	-0.
OXIDANT O 2.00000	0.23144	1292.515	G	647.95	-0.
OXIDANT AR 1.00000	0.01286	450.192	G	647.95	-0.
OXIDANT C 1.00000 U 2.00000	0.00046	-91701.919	G	647.95	-0.
FUEL C 7.00000 H 8.00000	0.40000	2867.000	L	298.15	-0.
FUEL C 8.00000 H 18.00000	0.60000	-59740.000	L	298.15	-0.

O/F= 17.0000 PERCENT FUEL= 5.5556 EQUIVALENCE RATIO= 0.8519 REACTANT DENSITY= 0.

Thermodynamic Properties

U, CAL/G	21.48	21.48
P, ATM	25.578	34.181
T, DEG K	2693	3427.04
RHO, G/CC	3.3333-3	4.4397-3
H, CAL/G	207.3	207.9
S, CAL/(G)(K)	2.0960	2.0762
M, MOL WT	28.800	28.820
(DLV/DLP)T	-1.00380	-1.00353
(DLV/DLP)P	1.0946	1.0876
CP, CAL/(G)(K)	0.5164	0.5040
GAMMA (S)	1.1852	1.1881
SON VEL, M/SEC	960.0	962.7

Mole Fractions

AR	8.7562-3	8.7623-3
C	6.404-15	5.993-15
CH	1.158-15	1.172-15
CH2O	2.843-10	3.212-10
CH3	3.222-15	3.679-15
CN	7.571-12	7.784-12
CN2	2.283-15	2.739-15
CO	1.1627-2	1.0745-2
CO2	1.0451-1	1.0547-1
C2O	1.155-15	1.262-15
H	4.4450-4	3.8337-4
HCN	3.005-10	3.241-10
HCO	1.4378-8	1.5108-8
HNCO	2.6951-9	3.1952-9
HNO	1.0667-6	1.1919-6
HO2	6.3652-6	6.9525-6
H2	1.6653-3	1.5251-3
H2O	9.8202-2	9.8591-2
H2O2	9.1393-7	1.0745-6
N	2.5831-7	2.4367-7
NCO	3.186-10	3.581-10
NH	1.8630-8	1.9082-8
NH2	3.2741-8	3.5684-8
NH3	1.3017-8	1.5106-8
NO	1.1523-2	1.1624-2
NO2	1.4118-5	1.6171-5
NO3	8.310-11	1.102-10
N2	7.2754-1	7.2800-1
N2O	2.8154-6	3.2851-6
N3	3.821-11	4.774-11
O	1.1500-3	1.0335-3
OH	6.0493-3	6.354-3
O2	2.7908-2	2.7480-2
O3	1.1540-8	1.3380-8

ADDITIONAL PRODUCTS WHICH WERE CONSIDERED BUT WHOSE MOLE FRACTIONS WERE LESS THAN 0.10000E-14 FOR ALL ASSIGNED CONDITIONS

C(S)	CH2	CH4	CN4	C2	C2H	C2H2	C2H4	C2+6	C2N
C2N2	C3	C3O2	C4	C5	H2O(S)	H2O(L)	N2H4	N2C4	

NOTE. WEIGHT FRACTION OF FUEL IN TOTAL FUELS AND OF OXIDANT IN TOTAL OXIDANTS

NO TRANSPORT DATA WAS FOUND FOR THE SPECIES HO2

Transport Properties at Assigned Volume

O/F= 17.0000 PERCENT FUEL= 5.5556 EQUIVALENCE RATIO= 0.8519 INTERNAL ENERGY= 21.48 CAL/G

TEMP	VISCOSITY	MUNATOMIC COND	INTERNAL COND	FROZEN COND	REACTION COND	EQUILIBRIUM COND	CP FROZ	CP EQ	PRANDTL FROZ	PRANDTL EQ	LEWIS NUMBER
DEG K	POISE	CAL/(CM)(SEC)(K)				CAL/(G)(K)		DIMENSIONLESS			
2693	818.X10-6	215.X10-6	189.X10-6	404.X10-6	270.X10-6	674.X10-6	0.3413	0.5164	0.6913	0.6265	1.3049
2704	821.	215.	190.	405.	250.	655.	0.3414	0.5040	0.6915	0.6317	1.2930

NO TRANSPORT DATA WAS FOUND FOR THE SPECIES HO2

Case 5612 - Input

```

REACTANTS
N 2.      H 4.      80.    12050.  L298.15  F 1.0036
BE1.     20.      0.0     5298.15  F 1.85
H 2.     D 2.     100.   -44880.  L298.15  O 1.407

INSERT   BE0(L)
NAMELISTS
$INPT2  KASE=5612,FPCT=T, MIX=67, P=1000,500,PSIA=T, RKT=T, NODATA=T $
$RKTINP PCP=3,10,30,300, FROZ=F $
    
```

Case 5612 - Output

```

REACTANTS
N 2.0000 H 4.0000 -0. -0. -0. 80.0000 12050.00 L 298.150 F 1.00360
BE 1.0000 -0. -0. -0. -0. 20.0000 0. S 298.150 F 1.85000
H 2.0000 O 2.0000 -0. -0. -0. 100.0000 -44880.00 L 298.150 O 1.40700

INSERT   BE0(L)
NAMELISTS
$INPT2
KASE = 5612,
T = 0. , 0. , 0. , 0. , 0. , 0. , 0. , 0. , 0. ,
  0. , 0. , 0. , 0. , 0. , 0. , 0. , 0. , 0. ,
  0. , 0. , 0. , 0. , 0. , 0. , 0. , 0. , 0. ,
  0. , 0. , 0. , 0. , 0. , 0. , 0. , 0. , 0. ,
  0. , 0. , 0. , 0. , 0. , 0. , 0. , 0. , 0. ,
  0. , 0. , 0. , 0. , 0. , 0. , 0. , 0. , 0. ,
P = 1.0000000E+03, 5.0000000E+02, 0. , 0. , 0. , 0. , 0. , 0. ,
  0. , 0. , 0. , 0. , 0. , 0. , 0. , 0. , 0. ,
  0. , 0. , 0. , 0. , 0. , 0. , 0. , 0. , 0. ,
  0. , 0. , 0. , 0. , 0. , 0. , 0. , 0. , 0. ,
PSIA = T, MMHG = F, NSQM = F,
V = 0. , 0. , 0. , 0. , 0. , 0. , 0. , 0. , 0. ,
  0. , 0. , 0. , 0. , 0. , 0. , 0. , 0. , 0. ,
RHO = 1.0000000E+03, 5.0000000E+02, 0. , 0. , 0. , 0. , 0. , 0. ,
  0. , 0. , 0. , 0. , 0. , 0. , 0. , 0. , 0. ,
  0. , 0. , 0. , 0. , 0. , 0. , 0. , 0. , 0. ,
ERATIO= F, OF = F, FPCT = T, FA = F,
MIX = 6.7000000E+01, 0. , 0. , 0. , 0. , 0. , 0. , 0. ,
  0. , 0. , 0. , 0. , 0. , 0. , 0. , 0. ,
TP = F, HP = F, SP = F, IV = F, UV = F, SV = F,
RKT = T, SHOCK = F, DETN = F, OTTO = F, CR = 0. , SO = 0. , SO = 0. ,
IONS = F, IDEBUG= 0, TRACE = 0. , SIUNIT= F, EUNITS= F,
TRNSPT= T, FROZ= F, PUNCH = F, NODATA= T,
$ END

SPECIES BEING CONSIDERED IN THIS SYSTEM
J 9/61 BE(S) J 9/61 BE(L) J 9/61 BE J 3/63 BEH J 6/63 BEN
J 6/71 BE0(S) J 6/71 BE0(S) J 6/71 BE0(L) J 9/63 BE0 J 9/63 BE0H
J 3/67 BE02H2 J 9/63 BE20 J 9/63 BE202 J 9/63 BE303 J 9/63 BE404
J 9/65 H J 3/63 HNO J 3/64 H02 J 3/61 H2 L11/65 H20(S)
L11/65 H20(L) J 3/61 H20 L 2/69 H202 J 3/61 N J12/71 NH
J12/65 NH2 J 9/65 NH3 J 6/63 NO J 9/64 N02 J12/64 N03
J 9/65 N2 J12/65 N2H4 J12/64 N20 J 9/64 N204 J12/70 N3
J 6/62 O J12/70 OH J 9/65 O2 J 6/61 O3

$RKTINP
EQL = T, FROZ = F,
SUBAR = 0. , 0. , 0. , 0. , 0. , 0. , 0. , 0. ,
  0. , 0. , 0. , 0. , 0. , 0. , 0. , 0. ,
SUPAR = 0. , 0. , 0. , 0. , 0. , 0. , 0. , 0. ,
  0. , 0. , 0. , 0. , 0. , 0. , 0. , 0. ,
    
```

PCP = 3.000000E+00, 1.000000E+01, 3.000000E+01, 3.000000E+02, 0. , 0. ,
 0. , 0. , 0. , 0. , 0. , 0. ,
 0. , 0. , 0. , 0. , 0. , 0. ,
 0. , 0. , 0. , 0. , 0. , 0. ,

NFZ = 1,
 \$ END

OF = 0.492537
 ENTHALPY EFFECTIVE FUEL EFFECTIVE OXIDANT MIXTURE
 (KG-MOL)(DEG K)/KG HPP(2) HPP(1) HSUBO
 0.15138364E+03 -0.66397491E+03 -0.11768468E+03
 KG-ATOMS/KG BOP(I,2) BOP(I,1) B0(I)
 N 0.49929349E-01 0. 0.33452664E-01
 H 0.99858698E-01 0.58798038E-01 0.86308680E-01
 BE 0.22192139E-01 0. 0.14868733E-01
 O 0. 0.58798038E-01 0.19403352E-01

PT N H BE O
 1 -12.759 -8.578 -13.145 -20.218 11.000
 2 -12.897 -8.719 -13.764 -20.839 3.000
 PC/PT= 1.748578 T = 2844.77
 2 -12.897 -8.720 -13.766 -20.841 2.000
 PC/PT= 1.751558 T = 2844.13
 3 -13.027 -8.855 -14.461 -21.526 3.000
 3 -13.084 -8.910 -14.166 -21.236 3.000
 4 -13.688 -9.517 -14.169 -21.233 3.000
 4 -13.476 -9.311 -15.668 -22.379 4.000
 5 -13.730 -9.579 -18.318 -24.378 4.000
 5 -13.752 -9.600 -18.141 -24.210 3.000
 6 -14.276 -10.158 -26.901 -30.508 4.000

THEORETICAL RCKET PERFORMANCE ASSUMING EQUILIBRIUM COMPOSITION DURING EXPANSION

PC = 1000.0 PSIA
 CASE NO. 5612

CHEMICAL FORMULA WT FRACTION ENERGY STATE TEMP DENSITY
 FUEL N 2.00000 H 4.00000 (SEE NOTE) CAL/MOL DEG K G/CC
 FUEL BE 1.00000 0.80000 12050.000 L 298.15 1.0036
 OXIDANT H 2.00000 D 2.00000 0.20000 0. S 298.15 1.8500
 1.00000 -44880.000 L 298.15 1.4070
 O/F= 0.4925 PERCENT FUEL= 67.0000 EQUIVALENCE RATIO= 2.9904 REACTANT DENSITY= 1.1890

	CHAMBER	THROAT	EXIT	EXIT	EXIT	EXIT
PC/P	1.0000	1.7516	3.0000	10.000	30.000	300.00
P, ATM	68.046	38.849	22.682	6.8046	2.2682	0.2268
T, DEG K	3068	2844	2721	2423	2071	1402
RHO, G/CC	4.4700-3	2.7624-3	1.6878-3	5.7008-4	2.2271-4	3.2936-5
H, CAL/G	-233.9	-432.6	-610.0	-987.1	-1282.2	-1753.7
S, CAL/(G)(K)	3.4110	3.4110	3.4110	3.4110	3.4110	3.4110
M, MOL WT	16.536	16.595	16.612	16.654	16.688	16.700
(DLV/DLP)I	-1.00511	-1.00378	-1.00273	-1.00141	-1.00036	-1.00001
(DLV/DLT)P	1.0924	1.0633	0.	1.0317	1.0093	1.0001
CP, CAL/(G)(K)	0.9894	0.9257	0.	0.8341	0.7515	0.6703
GAMMA (S)	1.1625	1.1668	0.9973	1.1777	1.1920	1.2159
SUN VEL,M/SEC	1339.1	1289.4	1165.3	1193.5	1109.1	921.1
MACH NUMBER	0.	1.000	1.522	2.104	2.671	3.872
AE/AT		1.0000	1.1895	2.4888	5.4000	30.326
CSTAR, FT/SEC		6351	6351	6351	6351	6351
CF		0.666	0.417	1.297	1.530	1.842
I VAC, LB-SEC/LB		244.2	259.2	305.1	337.6	383.6
I SP, LB-SEC/LB		131.5	180.9	256.0	302.0	363.6

MULE FRACTIONS

BE	0.00003	0.00001	0.00000	0.00000	0.	0.
BEH	0.00001	0.00000	0.00000	0.00000	0.	0.
BE0(S)	0.	0.	0.	0.	0.19872	0.19891
BE0(S)	0.	0.	0.07071	0.19809	0.	0.
BE0(L)	0.19539	0.19660	0.12632	0.	0.	0.
BE0H	0.00032	0.00013	0.00008	0.00001	0.00000	0.
BE02H2	0.00207	0.00149	0.00120	0.00047	0.00010	0.00000
H	0.01490	0.00974	0.00821	0.00433	0.00111	0.00001
H2	0.50639	0.51002	0.51105	0.51362	0.51586	0.51665
H2O	0.05765	0.05863	0.05902	0.05999	0.06052	0.06066
NH2	0.00002	0.00001	0.00001	0.00000	0.00000	0.
NH3	0.00010	0.00006	0.00004	0.00007	0.00001	0.00000
NO	0.00004	0.00002	0.00001	0.00000	0.00000	0.
N2	0.22247	0.22295	0.22307	0.22337	0.22366	0.22376
O	0.00001	0.00000	0.00000	0.00000	0.00000	0.
OH	0.00060	0.00033	0.00025	0.00009	0.00001	0.00000

ADDITIONAL PRODUCTS WHICH WERE CONSIDERED BUT WHOSE MOLE FRACTIONS WERE LESS THAN 0.50000E-05 FOR ALL ASSIGNED CONDITIONS

BE(S)	BE(L)	BEH	BEJ	BEZ0	BE202	BE303	BE404	HNO	HD2
H2O(S)	H2O(L)	H2O2	N	NH	NO2	NO3	N2H4	N2O	N2O4
N3	O2	O3							

NOTE. WEIGHT FRACTION OF FUEL IN TOTAL FUELS AND OF OXIDANT IN TOTAL OXIDANTS

TRANSPORT PROPERTIES OF ROCKET EXHAUST ASSUMING EQUILIBRIUM COMPOSITION DURING EXPANSION

O/F= 0.4925 PERCENT FUEL= 67.0000 EQUIVALENCE RATIO= 2.9904 CHAMBER PRESSURE= 68.046 ATM

TEMP	VISCOSITY	MONATOMIC COND	INTERNAL COND	FROZEN COND	REACTION COND	EQUILIBRIUM COND	CP FROZ	CP EQ	PRANDTL FROZ	PRANDTL EQ	LEWIS NUMBER
DEG K	POISE	CAL/(CM)(SEC)(K)				CAL/(G)(K)		DIMENSIONLESS			
3068	688.X10-6	766.X10-6	673.X10-6	1439.X10-6	1165.X10-6	2603.X10-6	0.8782	1.1951	0.4200	0.3159	2.2428
2844	651.	718.	620.	1338.	823.	2161.	0.8691	1.1033	0.4224	0.3321	2.2818
2721	630.	694.	590.	1284.	727.	2010.	0.8634	1.0763	0.4236	0.3371	2.2963
2423	579.	634.	516.	1150.	433.	1583.	0.8478	0.9850	0.4266	0.3601	2.3260
2071	518.	564.	428.	993.	131.	1123.	0.8251	0.8716	0.4304	0.4018	2.3350
1402	397.	434.	266.	700.	1.	702.	0.7677	0.7683	0.4348	0.4344	2.2061

THEORETICAL ROCKET PERFORMANCE ASSUMING EQUILIBRIUM COMPOSITION DURING EXPANSION

PC = 500.0 PSIA
CASE NO. 5612

CHEMICAL FORMULA	WT FRACTION (SEE NOTE)	ENERGY CAL/MOL	STATE	TEMP DEG K	DENSITY G/CC
FUEL N 2.00000 H 4.00000	0.80000	12050.000	L	298.15	1.0036
FUEL BE 1.00000	0.20000	0.	S	298.15	1.8500
OXIDANT H 2.00000 O 2.00000	1.00000	-44880.000	L	298.15	1.4070

O/F= 0.4925 PERCENT FUEL= 67.0000 EQUIVALENCE RATIO= 2.9904 REACTANT DENSITY= 1.1890

	CHAMBER	THROAT	EXIT	EXIT	EXIT	EXIT
PC/P	1.0000	1.7492	3.0000	10.000	30.000	300.00
P, ATM	34.023	19.451	11.341	3.4023	1.1341	0.1134
T, DEG K	3041	2827	2721	2416	2071	1404
RHO, G/CC	2.2475-3	1.3882-3	8.4200-4	2.8556-4	1.1133-4	1.6445-5
M, CAL/G	-233.9	-431.1	-608.9	-985.4	-1280.4	-1752.3
S, CAL/(G)(K)	3.4945	3.4945	3.4945	3.4945	3.4945	3.4945
M, MOL WT	16.485	16.559	16.575	16.637	16.683	16.700
(DLV/DLP)T	-1.00656	-1.00430	-1.00380	-1.00191	-1.00050	-1.00001
(DLV/DL)P	1.1213	1.0846	0.	1.0435	1.0131	1.0001
CP, CAL/(G)(K)	1.0570	0.9780	0.	0.8663	0.7636	0.6707
GAMMA (S)	1.1585	1.1679	0.9962	1.1740	1.1899	1.2158
SON VEL,M/SEC	1333.0	1284.9	1166.0	1190.5	1108.3	921.7
MACH NUMBER	0.	1.000	1.519	2.107	2.670	3.867
AE/AT		1.0000	1.1958	2.4908	5.4142	30.428
CSTAR, FT/SEC		6341	6341	6341	6341	6341
CF		0.665	0.917	1.298	1.531	1.844
IVAC, LB-SEC/LB		243.7	759.2	304.8	337.3	383.5
ISP, LB-SEC/LB		131.0	180.6	255.7	301.8	363.5

MOLE FRACTIONS

BE	0.00005	0.00001	0.00001	0.00000	0.00000	0.
BEH	0.00001	0.00000	0.00000	0.00000	0.	0.
BE0(S)	0.	0.	0.	0.	0.19868	0.19891
BE0(L)	0.	0.	0.08351	0.19793	0.	0.
BE0(H)	0.19488	0.19626	0.11314	0.	0.	0.
BE0H	0.00040	0.00016	0.00011	0.00002	0.00000	0.
BE0ZH2	0.00198	0.00144	0.00120	0.00046	0.00010	0.00000
H	0.01942	0.01297	0.01159	0.00592	0.00156	0.00001
H2	0.50298	0.50760	0.50853	0.51242	0.51552	0.51665
H2O	0.05742	0.05846	0.05882	0.05992	0.06050	0.06066
NH2	0.00002	0.00001	0.00000	0.00000	0.00000	0.
NH3	0.00005	0.00003	0.00002	0.00001	0.00000	0.00000
NO	0.00006	0.00003	0.00002	0.00001	0.00000	0.
N2	0.22194	0.22258	0.22269	0.22319	0.22361	0.22376
O	0.00002	0.00001	0.00001	0.00000	0.00000	0.
OH	0.00076	0.00043	0.00035	0.00013	0.00002	0.00000

ADDITIONAL PRODUCTS WHICH WERE CONSIDERED BUT WHOSE MOLE FRACTIONS WERE LESS THAN 0.50000E-05 FOR ALL ASSIGNED CONDITIONS

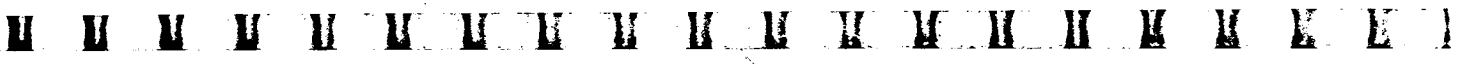
RE(S)	RE(L)	BEH	BE3	BE2D	BE2D2	BE3D3	BE4D4	HN0	HO2
H2O(S)	H2O(L)	H2O2	N	NH	N02	N03	N2H4	N2O	N2O4
N3	O2	O3							

NOTE. WEIGHT FRACTION OF FUEL IN TOTAL FUELS AND OF OXIDANT IN TOTAL OXIDANTS

TRANSPORT PROPERTIES OF ROCKET EXHAUST ASSUMING EQUILIBRIUM COMPOSITION DURING EXPANSION

D/F= 0.4925 PERCENT FUEL= 67.0000 EQUIVALENCE RATIO= 2.9904 CHAMBER PRESSURE= 34.023 ATM

TEMP	VISCOSITY	MONAIDMIC	INTERNAL	FROZEN	REACTION	EQUILIBRIUM	CP	CP	PRANDTL	PRANDTL	LEWIS
DEG K	POISE	COND	COND	COND	COND	COND	FROZ	EQ	FROZ	EQ	NUMBER
		CAL/(CM)(SEC)(K)					CAL/(G)(K)		---- DIMENSIONLESS ----		
3041	534.X10-6	768.X10-6	663.X10-6	1432.X10-6	1529.X10-6	2961.X10-6	0.8773	1.2974	0.4193	0.2999	2.2294
2827	648.	720.	814.	1334.	1101.	2436.	0.8685	1.1841	0.4219	0.3151	2.2717
2721	630.	698.	588.	1287.	1024.	2311.	0.8636	1.1646	0.4229	0.3175	2.2842
2416	578.	634.	514.	1148.	593.	1742.	0.8476	1.0363	0.4263	0.3437	2.3208
2071	518.	565.	428.	993.	185.	1178.	0.8251	0.8908	0.4303	0.3918	2.3341
1404	397.	434.	267.	701.	2.	703.	0.7679	0.7688	0.4348	0.4342	2.2476



Case 6666 - Input

```

REACTANTS
H 2.          100.  -2154.  L 20.27  F .0709
O 2.          100.  -3102.  L 90.18  O 1.149
  
```

```

NAMELIST
$INPT2 KASE=6666, P=3000, PSIA=T, FPCT=T, MIX=20, RKT=T
$RKTINP SUPAR=1.5,2.5,4., PCP=2.5,3,4,10,30, SUBAR=2,3,10, NFZ=4, $
  
```

Case 6666 - Output

```

REACTANTS
H 2.0000    -0.    -0.    -0.    -0.    100.0000    -2154.00  L 20.270  F 0.07090
O 2.0000    -0.    -0.    -0.    -0.    100.0000    -3102.00  L 90.180  O 1.14900
NAMELIST
$INPT2
KASE =          6666,
T = 0.          , 0.          , 0.          , 0.          , 0.          , 0.          , 0.          , 0.          ,
  0.          , 0.          , 0.          , 0.          , 0.          , 0.          , 0.          , 0.          ,
  0.          , 0.          , 0.          , 0.          , 0.          , 0.          , 0.          , 0.          ,
  0.          , 0.          , 0.          , 0.          , 0.          , 0.          , 0.          , 0.          ,
  0.          , 0.          , 0.          , 0.          , 0.          , 0.          , 0.          , 0.          ,
  0.          , 0.          , 0.          , 0.          , 0.          , 0.          , 0.          , 0.          ,
  0.          , 0.          , 0.          , 0.          , 0.          , 0.          , 0.          , 0.          ,
P = 3.0000000E+03, 0.          , 0.          , 0.          , 0.          , 0.          , 0.          , 0.          ,
  0.          , 0.          , 0.          , 0.          , 0.          , 0.          , 0.          , 0.          ,
  0.          , 0.          , 0.          , 0.          , 0.          , 0.          , 0.          , 0.          ,
  0.          , 0.          , 0.          , 0.          , 0.          , 0.          , 0.          , 0.          ,
PSIA =  T, MMHG =  F, NSQM =  F,
V = 0.          , 0.          , 0.          , 0.          , 0.          , 0.          , 0.          , 0.          ,
  0.          , 0.          , 0.          , 0.          , 0.          , 0.          , 0.          , 0.          ,
  0.          , 0.          , 0.          , 0.          , 0.          , 0.          , 0.          , 0.          ,
RHD = 3.0000000E+03, 0.          , 0.          , 0.          , 0.          , 0.          , 0.          , 0.          ,
  0.          , 0.          , 0.          , 0.          , 0.          , 0.          , 0.          , 0.          ,
  0.          , 0.          , 0.          , 0.          , 0.          , 0.          , 0.          , 0.          ,
  0.          , 0.          , 0.          , 0.          , 0.          , 0.          , 0.          , 0.          ,
ERATIO= F, OF =  F, FPCT =  T, FA =  F,
MIX = 2.0000000E+01, 0.          , 0.          , 0.          , 0.          , 0.          , 0.          , 0.          ,
  0.          , 0.          , 0.          , 0.          , 0.          , 0.          , 0.          , 0.          ,
  0.          , 0.          , 0.          , 0.          , 0.          , 0.          , 0.          , 0.          ,
IP =  F, HP =  F, SP =  F, TV =  F, UV =  F, SV =  F,
RKT =  T, SHUCK =  F, DETN =  F, DTTO =  F, CR = 0.          , 50 = 0.          , 50 = 0.          ,
IONS =  F, IUEBUG= 0, TRACE = 0.          , SIUNIT=  F, EUNITS=  F,
TRNSPI=  T, FROZN =  F, PUNCH =  F, NODATA=  F,
$ END
SPECIES BEING CONSIDERED IN THIS SYSTEM
  J 9/65  H          J 3/64  H02          J 3/61  H2          L11/65  H2O(S)          L11/65  H2O(L)
  J 3/61  H2O          L 2/69  H2O2          J 6/62  O          J12/70  OH          J 9/65  O2
  J 6/61  O3
$RKTINP
EQL =  T, FROZ =  T,
SUBAR = 2.0000000E+00, 3.0000000E+00, 1.0000000E+01, 0.          , 0.          , 0.          ,
  0.          , 0.          , 0.          , 0.          , 0.          , 0.          ,
  0.          , 0.          , 0.          , 0.          , 0.          , 0.          ,
SUPAR = 1.5000000E+00, 2.5000000E+00, 4.0000000E+00, 0.          , 0.          , 0.          ,
  0.          , 0.          , 0.          , 0.          , 0.          , 0.          ,
  0.          , 0.          , 0.          , 0.          , 0.          , 0.          ,
PCP = 2.5000000E+00, 3.0000000E+00, 4.0000000E+00, 1.0000000E+01, 3.0000000E+01, 0.          ,
  0.          , 0.          , 0.          , 0.          , 0.          , 0.          ,
  0.          , 0.          , 0.          , 0.          , 0.          , 0.          ,
  0.          , 0.          , 0.          , 0.          , 0.          , 0.          ,
NFZ =          4,
$ END
  
```



OF = 4.000000

ENTHALPY (KG-MUL)(DEG K)/KG	EFFECTIVE FUEL HPP(2) -0.53769263E+03	EFFECTIVE OXIDANT HPP(1) -0.48783627E+02	MIXTURE HSUBO -0.14656543E+03
KG-ATOMS/KG	BOP(1,2) H 0.99209300E+00 O 0.	BOP(1,1) C 0.62502343E-01	BO(1) 0.19841859E+00 0.50001875E-01

PT H U

1	-8.106	-18.242	9.000
2	-8.224	-19.064	3.000
PC/PT= 1.770715	T = 2719.66		
2	-8.225	-19.070	2.000
PC/PT= 1.777559	T = 2717.89		
2	-8.225	-19.070	1.000
PC/PT= 1.77525	T = 2717.86		
3	-8.293	-19.634	3.000
4	-8.329	-19.961	3.000
5	-8.386	-20.513	3.000
6	-8.563	-22.618	3.000
7	-8.774	-25.980	3.000
8	-8.116	-18.305	8.000
8	-8.118	-18.318	2.000
8	-8.118	-18.320	2.000
8	-8.118	-18.320	1.000
9	-8.110	-18.270	2.000
9	-8.111	-18.274	2.000
9	-8.111	-18.275	1.000
10	-8.106	-18.247	2.000
10	-8.106	-18.244	2.000
10	-8.106	-18.245	1.000
10	-8.106	-18.245	1.000
10	-8.106	-18.245	1.000
11	-8.438	-21.072	4.000
11	-8.439	-21.083	2.000
12	-8.599	-23.125	3.000
12	-8.601	-23.148	1.000
13	-8.742	-25.405	3.000
13	-8.736	-25.300	1.000

THEORETICAL ROCKET PERFORMANCE ASSUMING EQUILIBRIUM COMPOSITION DURING EXPANSION

PC = 3000.0 PSIA
CASE NO. 6666

CHEMICAL FORMULA	WT FRACTION (SEE NOTE)	ENERGY CAL/MOL	STATE	TEMP DEG K	DENSITY G/CC
FUEL H 2.00000	1.00000	-2154.000	L	20.27	0.0709
OXIDANT O 2.00000	1.00000	-3102.000	L	90.18	1.1490

O/F = 4.0000 PERCENT FUEL = 20.0000 EQUIVALENCE RATIO = 1.9841 REACTANT DENSITY = 0.2843

	CHAMBER	THROAT	EXIT	EXIT	EXIT	EXIT	EXIT	EXIT	EXIT	EXIT	EXIT	EXIT	EXIT
PC/P	1.0000	1.7776	2.5000	3.0000	4.0000	10.000	30.000	1.0601	1.0247	1.0021	5.2560	12.183	24.655
P, ATM	204.14	114.84	81.655	68.046	51.034	20.414	6.8046	192.56	199.21	203.71	38.839	16.756	8.2797
T, DEG K	2988	2718	2563	2482	2357	1984	1593	2960	2977	2987	2241	1909	1658
RHO, G/CC	8.3498-3	5.1773-3	3.9076-3	3.3640-3	2.6581-3	1.2639-3	5.2480-4	7.9531-3	8.1813-3	8.3351-3	2.1276-3	1.0781-3	6.1339-4
H, CAL/G	-291.2	-615.9	-793.8	-884.6	-1021.9	-1413.5	-1799.7	-325.6	-305.7	-292.5	-1145.7	-1489.2	-1736.8
S, CAL/(G)(K)	4.9111	4.9111	4.9111	4.9111	4.9111	4.9111	4.9111	4.9111	4.9111	4.9111	4.9111	4.9111	4.9111
M, MOL WT	10.029	10.054	10.064	10.068	10.072	10.078	10.080	10.032	10.031	10.029	10.075	10.079	10.080
(DLV/DLP)T	-1.00251	-1.00126	-1.00078	-1.00059	-1.00037	-1.00006	-1.00000	-1.00236	-1.00245	-1.00251	-1.00023	-1.00004	-1.00001
(DLV/DL)T	1.0495	1.0270	1.0176	1.0138	1.0090	1.0017	1.0001	1.0468	1.0484	1.0494	1.0058	1.0011	1.0002
CP, CAL/(G)(K)	1.2974	1.1978	1.1491	1.1263	1.0945	1.0199	0.9569	1.2864	1.2928	1.2970	1.0686	1.0074	0.9674
GAMMA (S)	1.1986	1.2088	1.2153	1.2188	1.2242	1.2406	1.2595	1.1996	1.1990	1.1987	1.2293	1.2440	1.2561
SDN VEL, M/SEC	1723.1	1648.3	1634.1	1580.5	1543.2	1424.9	1286.4	1715.5	1719.9	1722.9	1507.9	1399.6	1310.7
MACH NUMBER	0.	1.000	1.278	1.410	1.602	2.151	2.762	0.313	0.202	0.060	1.773	2.262	2.654
AE/AT		1.0000	1.0650	1.1385	1.2984	2.2034	4.5769	2.0000	3.0000	10.000	1.5000	2.5000	4.0000
CSTAR, FT/SEC		7952	7952	7952	7952	7952	7952	7952	7952	7952	7952	7952	7952
CF		0.680	0.846	0.919	1.020	1.264	1.466	0.221	0.143	0.042	1.103	1.306	1.435
IVAC, LB-SEC/LB		307.1	314.4	321.0	332.4	366.9	400.0	521.0	759.0	2466.9	343.2	373.6	394.8
TSP, LB-SEC/LB		168.1	209.1	227.2	252.1	312.5	362.3	54.7	35.5	10.5	272.7	322.5	354.7

MOLE FRACTIONS

H	0.00743	0.00396	0.00255	0.00197	0.00126	0.00023	0.00001	0.00701	0.00725	0.00741	0.00080	0.00015	0.00002
H2	0.49109	0.49340	0.49424	0.49463	0.49511	0.49583	0.49599	0.49135	0.49120	0.49110	0.49543	0.49589	0.49598
H2O	0.49895	0.50168	0.50264	0.50300	0.50341	0.50392	0.50400	0.49930	0.49910	0.49896	0.50365	0.50395	0.50400
O	0.00002	0.00001	0.00000	0.00000	0.00000	0.	0.	0.00002	0.00002	0.00002	0.00000	0.	0.
OH	0.00249	0.00105	0.00057	0.00040	0.00022	0.00002	0.00000	0.00230	0.00241	0.00248	0.00012	0.00001	0.00000
O2	0.00001	0.00000	0.00000	0.00000	0.00000	0.	0.	0.00001	0.00001	0.00001	0.00000	0.	0.

ADDITIONAL PRODUCTS WHICH WERE CONSIDERED BUT WHOSE MOLE FRACTIONS WERE LESS THAN 0.50000E-05 FOR ALL ASSIGNED CONDITIONS

H2O2 H2O(L) H2O2 O3

NOTE. WEIGHT FRACTION OF FUEL IN TOTAL FUELS AND OF OXIDANT IN TOTAL OXIDANTS

TRANSPORT PROPERTIES OF ROCKET EXHAUST ASSUMING EQUILIBRIUM COMPOSITION DURING EXPANSION

O/F= 4.0000 PERCENT FUEL= 20.0000 EQUIVALENCE RATIO= 1.9841 CHAMBER PRESSURE= 204.137 ATM

TEMP DEG K	VISCOSITY POISE	MONATOMIC COND	INTERNAL COND	FROZEN COND	REACTION COND	EQUILIBRIUM COND	CP FROZ	CP EQ	PRANDTL FROZ	PRANDTL EQ	LEWIS NUMBER
		CAL/(CM)(SEC)(K)				CAL/(G)(K)		DIMENSIONLESS			
2988	854.X10-6	790.X10-6	892.X10-6	1682.X10-6	542.X10-6	2274.X10-6	1.1019	1.2974	0.5596	0.4982	1.8171
2718	795.	734.	803.	1537.	311.	1848.	1.0826	1.1978	0.5605	0.5158	1.9025
2563	761.	702.	751.	1453.	210.	1662.	1.0700	1.1491	0.5607	0.5262	1.9517
2482	743.	685.	723.	1408.	166.	1574.	1.0629	1.1263	0.5607	0.5314	1.9773
2357	714.	660.	679.	1339.	111.	1450.	1.0511	1.0945	0.5606	0.5389	2.0162
1984	624.	582.	546.	1128.	23.	1152.	1.0102	1.0199	0.5590	0.5530	2.1195
1593	524.	498.	409.	907.	2.	909.	0.9561	0.9569	0.5525	0.5520	2.1732
2960	848.	784.	883.	1667.	515.	2182.	1.1001	1.2864	0.5597	0.4999	1.8258
2977	852.	787.	888.	1675.	531.	2206.	1.1012	1.2928	0.5596	0.4990	1.8207
2987	854.	790.	892.	1681.	541.	2222.	1.1019	1.2970	0.5596	0.4983	1.8174
2241	687.	536.	638.	1274.	73.	1347.	1.0394	1.0686	0.5604	0.5448	2.0512
1909	605.	566.	520.	1086.	15.	1102.	1.0008	1.0074	0.5581	0.5540	2.1350
1658	542.	513.	432.	944.	3.	947.	0.9660	0.9674	0.5540	0.5531	2.1696

THEORETICAL ROCKET PERFORMANCE ASSUMING FROZEN COMPOSITION DURING EXPANSION AFTER POINT 4

PC = 3000.0 PSIA
CASE NO. 6666

CHEMICAL FORMULA
FUEL H 2.00000
OXIDANT O 2.00000

WT FRACTION (SEE NOTE)
ENERGY CAL/MOL
STATE
TEMP DEG K
DENSITY G/CC

O/F= 4.0000 PERCENT FUEL= 20.0000 EQUIVALENCE RATIO= 1.9841 REACTANT DENSITY= 0.2841

	CHAMBER	THROT	EXIT	EXIT	EXIT	EXIT	EXIT	EXIT	EXIT	EXIT
PC/P	1.0000	1.7776	2.5000	3.0000	4.0000	10.000	30.000	5.2795	12.257	24.810
P, ATM	204.14	114.84	81.655	68.046	51.034	20.414	6.8046	38.666	16.655	8.2280
T, DEG K	2988	2718	2563	2482	2352	1973	1582	2232	1896	1645
RHO, G/CC	8.3498-3	5.1773-3	3.9076-3	3.3540-3	2.6622-3	1.2693-3	5.2765-4	2.1256-3	1.0778-3	6.1357-4
H, CAL/G	-291.2	-615.9	-793.8	-884.6	-1021.8	-1412.1	-1796.5	-1147.3	-1489.8	-1736.0
S, CAL/(G)(K)	4.9111	4.9111	4.9111	4.9111	4.9111	4.9111	4.9111	4.9111	4.9111	4.9111
M, MDL WT	10.029	10.054	10.064	10.068	10.068	10.068	10.068	10.068	10.068	10.068
CP, CAL/(G)(K)	1.2974	1.1978	1.1491	1.1263	1.0507	1.0090	0.9547	1.0385	0.9993	0.9643
GAMMA (S)	1.1986	1.2088	1.2153	1.2188	1.2313	1.2432	1.2606	1.2347	1.2461	1.2573
SON VEL, M/SEC	1723.1	1648.3	1604.1	1580.5	1546.5	1423.3	1283.4	1508.5	1396.8	1307.1
MACH NUMBER	0.	1.000	1.278	1.410	1.599	2.152	2.765	1.774	2.267	2.660
AE/AT	1.0000	1.0650	1.1385	1.2965	2.1953	4.5571	1.5000	2.5000	4.0000	
CSTAR, FT/SEC	7952	7952	7952	7952	7952	7952	7952	7952	7952	
CF	0.680	0.846	0.919	1.020	1.264	1.464	1.104	1.307	1.434	
IVAC, LB-SEC/LB	307.1	314.4	321.0	332.2	366.6	399.4	343.1	373.4	394.4	
ISP, LB-SEC/LB	168.1	209.1	227.2	252.1	312.3	361.9	272.9	322.9	354.6	

MOLE FRACTIONS

H 0.00197 H2 0.49463 H2O 0.50300 OH 0.00040

ADDITIONAL PRODUCTS WHICH WERE CONSIDERED BUT WHOSE MOLE FRACTIONS WERE LESS THAN 0.50000E-05 FOR ALL ASSIGNED CONDITIONS

H2O H2O(S) H2O(L) H2O2 O3

NOTE. WEIGHT FRACTION OF FUEL IN TOTAL FUELS AND OF OXIDANT IN TOTAL OXIDANTS

TRANSPORT PROPERTIES OF ROCKET EXHAUST ASSUMING FROZEN COMPOSITION DURING EXPANSION FROZEN AFTER POINT 4

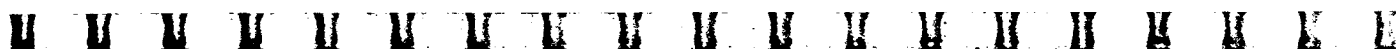
O/F= 4.0000 PERCENT FUEL= 20.0000 EQUIVALENCE RATIO= 1.9841 CHAMBER PRESSURE= 204.137 ATM

TEMP DEG K	VISCOSITY POISE	MONATOMIC COND	INTERNAL COND	FROZEN COND	CP FROZ	PRANDTL FROZ
		CAL/(CM)(SEC)(K)			CAL/(G)(K)	
2988	854.X10-6	790.X10-6	892.X10-6	1682.X10-6	1.1019	0.5596
2718	796.	734.	803.	1537.	1.0826	0.5605
2563	761.	702.	751.	1453.	1.0700	0.5607
2482	743.	685.	723.	1408.	1.0629	0.5607
2352	713.	659.	677.	1336.	1.0507	0.5605
1973	622.	581.	542.	1123.	1.0090	0.5585
1582	521.	497.	405.	902.	0.9547	0.5519
2232	684.	635.	634.	1269.	1.0385	0.5601
1896	602.	565.	515.	1080.	0.9993	0.5576
1645	538.	511.	427.	938.	0.9543	0.5533

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TABLE I. - FORMAT OF THERMODYNAMIC AND TRANSPORT DATA

(a) THERMO (thermodynamic) data

Card order	Content	Format	Card column
1	THERMO	3A4	1 to 6
2	Temperature ranges for two sets of coefficients: lowest T, common T, and highest T	3F10.3	1 to 30
3	Species name Date Atomic symbols and formula Phase of species (S, L, or G for solid, liquid, or gas, respectively) Temperature range Integer 1	3A4 2A3 4(A2, F3.0) A1 2F10.3 I15	1 to 12 19 to 24 25 to 44 45 46 to 65 80
4	Coefficients a_i ($i = 1$ to 5) in equations (3) to (5) (for upper temperature interval) Integer 2	5(E15.8) I5	1 to 75 80
5	Coefficients in equations (3) to (5) (a_6 and a_7 for upper temperature interval and a_1 , a_2 , and a_3 for lower) Integer 3	5(E15.8) I5	1 to 75 80
6	Coefficients in equations (3) to (5) (a_4 , a_5 , a_6 , and a_7 for lower temperature interval) Integer 4	4(E15.8) I20	1 to 60 80
(a)	Repeat cards numbered 1 to 4 in card column 80 for each species		
Final card	END (indicates end of thermodynamic data)	3A4	1 to 3

^aGaseous species and condensed species with only one condensed phase can be in any order. However, the sets for two or more condensed phases of the same species must be adjacent. If there are more than two condensed phases of a species, their sets must be either in increasing or decreasing order according to their temperature intervals.

TABLE I. - Concluded. FORMAT OF THERMODYNAMIC AND TRANSPORT DATA

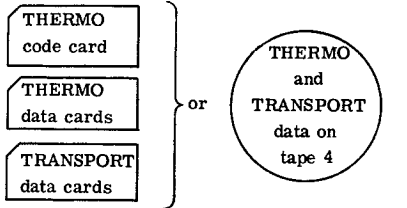
(b) TRANSPORT data

Card type	Content ^a	Format	Card column
1	Identification of interaction: chemical formula of species 1, chemical formula of species 2, number of temperatures in table (NTP), code to indicate type of data (1 for transport and 2 for relaxation), and number of rotational degrees of freedom	2(3A4, 6X), 2I5, F24.1	1 to 70
^b 2	Tables of data: either transport data (temperature, viscosity cross section, A*, and B*) or relaxation data (temperature, rotational collision number, vibrational collision number, and dimensionless vibrational heat capacity (C _{vib} /R))	4F10.4	1 to 40
3	End card to indicate end of transport data; LAST written in card columns 1 to 4	A4	1 to 4

^aIdentification of interaction is done by giving chemical formula of particular species involved, whether they are the same or different. They may be specified in either order, inasmuch as the program assumes interaction A-B to be same as B-A. The number of rotational degrees of freedom is meaningful only for data of a pure species (interaction of the type A-A). The temperature schedule is arbitrary, provided the number of temperatures is not more than the maximum of 20. In addition, the data should be ordered in either an increasing or decreasing function of temperature, in order that interpolation within the table be meaningful. As a matter of input convenience, the Hirschfelder-Eucken approximation is denoted by setting the collision number equal to 0.0. If the vibrational heat capacity is not specified (C_{vib}/R = 0), the program will calculate a value assuming that the electronic heat capacity is zero and that the rotational heat capacity is classical. For polar molecules A* should be corrected for resonant exchange of internal energy. See the main-text section TRANSPORT PROPERTY EQUATIONS for an explanation.

^bThere are NTP cards of type 2. They are followed by a card of either type 1 or type 3.

TABLE II. - PROGRAM INPUT



- REACTANTS code card
- REACTANTS cards
- OMIT card(s) (optional)
- INSERT card(s) (optional)
- NAMELISTS code card

\$INPT2

Optional variables:
 KASE
 MIX (1 to 15)
 OF, FPCT, FA, or ERATIO
 IONS
 IDEBUG
 TRACE
 TRNSPT
 NODATA
 PUNCH
 FROZN
 (additional namelist input is given in table on the right)

Problem	Namelist	Variables	
		Required	Optional
Assigned temperature and pressure (TP)	INPT2	TP = .TRUE. T(1 to 52); P(1 to 26)	NSQM, PSIA, or MMHG
Assigned enthalpy and pressure (HP)	INPT2	HP = .TRUE. P(1 to 26)	NSQM, PSIA, or MMHG
Assigned entropy and pressure (SP)	INPT2	SP = .TRUE. S0(1); P(1 to 26)	NSQM, PSIA, or MMHG
Assigned temperature and volume or density (TV)	INPT2	TV = .TRUE. T(1 to 52); V(1 to 26) or RHO(1 to 26)	
Assigned internal energy and volume or density (UV)	INPT2	UV = .TRUE. V(1 to 26) or RHO(1 to 26)	
Assigned entropy and volume or density (SV)	INPT2	SV = .TRUE. V(1 to 26) or RHO(1 to 26); S0(1)	
Detonation (DETN)	INPT2	DETN = .TRUE. P(1 to 26) (initial gas)	T(1 to 52)(initial gas); NSQM, PSIA, or MMHG
Shock (SHOCK)	INPT2	SHOCK = .TRUE. P(1 to 13) (initial T(1 to 13) gas)	NSQM, PSIA, or MMHG
	SHKINP	UI(1 to 13) or MACH1 (1 to 13)	INCDEQ = .FALSE. or INCDFZ = .FALSE.
Rocket (RKT)	INPT2	RKT = .TRUE. P(1 to 26) (chamber pressures)	T(1 to 52) (chamber); NSQM, PSIA, or MMHG
	RKTINP		EQL = .FALSE. or FROZ = .FALSE. NFZ PCP(1 to 22) SUPAR(1 to 13) SUBAR(1 to 13)

TABLE III. - REACTANTS CARDS

Card order	Content	Format	Card column
First	REACTANTS	3A4	1 to 9
Any	One card for each reactant species (maximum, 15). Each card contains		
	(1) Atomic symbols and formula numbers (maximum, five sets) ^a	5(A2, F7.5)	1 to 45
	(2) Relative weight ^b or number of moles	F7.5	46 to 52
	(3) Blank if (2) is relative weight, or M if (2) is number of moles	A1	53
	(4) Enthalpy or internal energy ^a , cal/mole	F9.5	54 to 62
	(5) State: S, L, or G for solid, liquid, or gas, respectively	A1	63
	(6) Temperature associated with enthalpy in (4)	F8.5	64 to 71
	(7) F if fuel, or O if oxidant	A1	72
	(8) Density in g/cm ³ (optional)	F8.5	73 to 80
Last	Blank		

^aProgram will calculate the enthalpy or internal energy (4) for species in the THERMO data at the temperature (6) if zeros are punched in card columns 37 and 38.

^bRelative weight of fuel in total fuels or oxidant in total oxidants. All reactants must be given either all in relative weights or all in number of moles. This number must never be zero.



TABLE IV. - LIST OF REACTANTS CARDS FOR SOME OXIDANTS AND FUELS

Chemical	Chemical formula (card columns 1 to 45)	Percent (cc 46-52)	Assigned enthalpy, cal/mole (cc 54-62)	(a)	Temper- ature, K (cc 64-71)	(b)	Density, g/cm ³ (cc 73-80)
Acetonitrile	C 2. H 3. N 1.	100.	12800.	L	298.15	F	.7857
Acetylene	C 2. H 2.	100.	49270.	L	192.60	F	.610
Air ^c	N 1.56176O .41959 AR.0009324O .000300	100.	-28.2	G	298.15	O	
Aluminum	AL1.	100.	0.	S	298.15	F	2.702
Ammonia(g)	N 1. H 3.	100.	-10970	G	298.15	F	
Ammonia(l)	N 1. H 3.	100.	-17090	L	239.72	F	.676
Ammonium perchlorate	N 1. H 4. CL1. O 4.	100.	-70690	S	298.15	F	1.95
Aniline	C 6. H 7. N 1.	100.	7100.	L	298.15	F	1.02173
Argon	AR1.	100.	0.0	G	298.15	F	
Benzene	C 6. H 6.	100.	11718.	L	298.15	F	.8737
Beryllium	BE1.	100.	0.0	S	298.15	F	1.85
Butane	C 4. H 10.	100.	-36080.	L	272.65	F	.6012
1-butene	C 4. H 8.	100.	-5800	L	266.9	F	.6263
Chlorine(g)	CL2.	100.	0.	G	298.15	O	
Chlorine(l)	CL2.	100.	-5391.	L	239.09	O	1.56
Chlorine trifluoride(g)	CL1. F 3.	100.	-39000.	G	298.15	O	
Chlorine trifluoride(l)	CL1. F 3.	100.	-45680.	L	284.55	O	1.8517
Cyanogen(g)	C 2. N 2.	100.	73840.	G	298.15	F	
Cyanogen(l)	C 2. N 2.	100.	67655.	L	252.01	F	.9537
Diborane	B 2. H 6.	100.	4970.	L	180.59	F	.4371
Ethane	C 2. H 6.	100.	-25008.	L	184.52	F	.5464
Ethyl alcohol	C 2. H 6. O 1.	100.	-66370.	L	298.15	F	.7893
Ethylene	C 2. H 4	100.	8100.	L	169.44	F	.5688
Ethylene oxide	C 2. H 4. O 1.	100.	-18840.	L	283.72	F	.8824
Ethylene polymer ^d	C 1. H 2.	100.	-6100.	S	298.15	F	.935
Fluorine(g)	F 2.	100.	0.	G	298.15	O	
Fluorine(l)	F 2.	100.	-3098.	L	85.02	O	1.505
Graphite	C 1.	100.	0.	S	298.15	F	2.25
Helium	HE1.	100.	0.	G	298.15	F	
Heptane	C 7. H 16.	100.	-53630.	L	298.15	F	.67951
Hydrazine	N 2. H 4.	100.	12100.	L	298.15	F	1.0036

^aPhase: S, solid; L, liquid; G, gas.

^bFuel, F; oxidant, O.

^cBased on the following molar percents: N₂ = 78.0881, O₂ = 20.9495, Ar = 0.9324, CO₂ = 0.0300.

^dEstimate based on paraffin hydrocarbon series.

TABLE IV. - Concluded. LIST OF REACTANTS CARDS FOR SOME OXIDANTS AND FUELS

Chemical	Chemical formula (card columns 1 to 45)	Percent (cc 46-52)	Assigned enthalpy, cal/mole (cc 54-62)	(a)	Temper- ature, K (cc 64-71)	(b)	Density, g/cm ³ (cc 73-80)
Hydrogen(g)	H 2.	100.	0.	G	298.15	F	
Hydrogen(l)	H 2.	100.	-2154.	L	20.27	F	.0709
Hydrogen peroxide	H 2. O 2.	100.	-44880.	L	298.15	O	1.407
IRFNA ^e	H 1.57216N 1.62945O 4.69505F .02499	100.	-64860.	L	298.15	O	1.48
JP-5, ASTMA ^f	C 1. H 1.9185	100.	-5300.	L	298.15	F	.807
JP-4, RP-1 ^g	C 1. H 1.9423	100.	-5430.	L	298.15	F	.773
Lithium(l)	LI1.	100.	1714.1	L	453.69	F	.512
Lithium(s)	LI1.	100.	0.	S	298.15	F	.534
Lithium perchlorate	LI1. CL1. O 4.	100.	-90880.	S	298.15	O	2.43
Methane(g)	C 1. H 4.	100.	-17895.	G	298.15	F	
Methane(l)	C 1. H 4.	100.	-21390.	L	111.66	F	.4239
Methyl alcohol	C 1. H 4. O 1.	100.	-57040.	L	298.15	F	.78659
Monomethyl hydrazine	C 1. H 6. N 2.	100.	12900.	L	298.15	F	.874
Nitric acid	H 1. N 1. O 3.	100.	-41460.	L	298.15	O	1.5027
Nitrogen(g)	N 2.	100.	0.0	G	298.15	F	
Nitrogen(l)	N 2.	100.	-2939.	L	77.35	F	.808
Nitrogen tetroxide	N 2. O 4.	100.	-4680.	L	298.15	O	1.431
Nitrogen trifluoride	N 1. F 3.	100.	-34100.	L	144.14	O	1.531
Nitromethane	C 1. H 3. N 1. O 2.	100.	-27030.	L	298.15	F	1.1371
Octane	C 8. H 18.	100.	-59740.	L	298.15	F	.69849
Oxygen(g)	O 2.	100.	0.0	G	298.15	O	
Oxygen(l)	O 2.	100.	-3102.	L	90.18	O	1.149
Oxygen difluoride	O 1. F 2.	100.	1869.	L	127.88	O	1.521
Ozone(g)	O 3.	100.	34100.	G	298.15	O	
Ozone(l)	O 3.	100.	30310.	L	162.64	O	1.449
Pentaborane	B 5. H 9.	100.	7740.	L	298.15	F	.6183
Perchloryl fluoride	CL1. O 3. F 1.	100.	-11350.	L	226.48	O	1.392
Propane	C 3. H 8.	100.	-30372.	L	231.08	F	.5808
n-propyl nitrate	C 3. H 7. N 1. O 3.	100.	-51270.	L	298.15	F	1.0538
Toluene	C 7. H 8.	100.	2867.	L	298.15	F	.86230
Unsymmetrical dimethylhydrazine	C 2. H 8. N 2.	100.	11900.	L	298.15	F	.783

^aPhase: S, solid; L, liquid; G, gas.

^bFuel, F; oxidant, O.

^eInhibited red fuming nitric acid based on following weight percents: HNO₃(l) = 83.5, N₂O₄(l) = 14, H₂O(l) = 2, HF(g) = 0.5.

^fTypical jet fuel having following properties: H/C weight ratio = 0.161, heat of combustion = 18 600 Btu/lb.

^gTypical jet fuel having following properties: H/C weight ratio = 0.163, heat of combustion = 18 640 Btu/lb.

TABLE V. - VARIABLES IN INPT2 NAMELIST

Variable	Dimension	Type	Common label	Value before read	Definition and comments
KASE	1	I	INDX	0	Optional assigned number associated with case
P	26	R	POINTS	0	Assigned pressures: chamber pressures for rocket problems; values in atm unless PSIA, NSQM, or MMHG = T (see below)
NSQM	1	L	-----	FALSE	Values in P array in N/m^2 ^b
PSIA	1	L	-----	FALSE	Values in P array in psia units ^b
MMHG	1	L	-----	FALSE	Values in P array in mm Hg units ^b
V	26	R	POINTS	0	Volume, cm^3/g
RHO	26	R	POINTS ^a (P)	0	Density, g/cm^3
T	26	R	POINTS	0	Assigned temperature, K
MIX	15	R	MISC ^a (OXF)	0	Values of equivalence ratios if ERATIO = T; oxidant-to-fuel weight ratio if OF = T; percent fuel by weight if FPCT = T; and fuel-to-air weight ratio if FA = T
ERATIO	1	L	MISC	FALSE	Equivalence ratios given in MIX ^b
OF	1	L	MISC	FALSE	Oxidant-to-fuel weight ratios given in MIX ^b
FPCT	1	L	MISC	FALSE	Percent fuel by weight given in MIX ^b
FA	1	L	-----	FALSE	Fuel-to-air weight ratios given in MIX ^b
TRACE	1	R	MISC	0 (5. E-9 for SHOCK problem)	Option to print mole fractions \geq TRACE in special E-format
IONS	1	L	INDX	FALSE	Consider ionic species ^b
IDEBUG	1	I	INDX	0	Print intermediate output for all points indexed \geq integer value
TP	1	L	INDX	FALSE	Assigned temperature and pressure problem ^b
HP	1	L	INDX	FALSE	Assigned enthalpy and pressure problem ^b
SP	1	L	INDX	FALSE	Assigned entropy (S0) and pressure problem ^b
S0	1	R	MISC	0	Assigned entropy, cal/(g)(K)
TV	1	L	INDX	FALSE	Assigned temperature and volume (or density) problem ^b
UV	1	L	INDX	FALSE	Assigned internal energy and volume (or density) problem ^b
SV	1	L	INDX	FALSE	Assigned entropy (S0) and volume (or density) problem ^b
RKT	1	L	-----	FALSE	Rocket problem ^b
DETN	1	L	-----	FALSE	Detonation problem ^b
SHOCK	1	L	INDX	FALSE	Shock problem ^b
TRNSPT	1	L	CONTRL	TRUE	Transport properties included with the calculations ^b
PUNCH	1	L	CONTRL	FALSE	Punched cards of calculations included with output ^b
NODATA	1	L	CONTRL	FALSE	Message concerning missing transport data not printed ^b
FROZN	1	L	CONTRL	FALSE	Frozen transport properties calculated for the current point ^b

^aEquivalenced to variable given in parentheses.

^bIf variable is set to be TRUE.

TABLE VI. - VARIABLES IN RKTINP NAMELIST^a

Variable	Dimension	Type	Common label	Value before read	Definition and comments
EQL	1	L	PERF	TRUE	Calculate rocket performance assuming equilibrium composition during expansion ^b
FROZ	1	L	PERF	TRUE	Calculate rocket performance assuming frozen composition during expansion ^b
NFZ	1	I	PERF	1	Freezing point; must be ≤ 13
PCP	26	R	PERF	0	Ratio of chamber pressure to exit pressure; list should not include values for the chamber and throat; storage allows for 22 values
SUBAR	13	R	PERF	0	Subsonic area ratios
SUPAR	13	R	PERF	0	Supersonic area ratios

^aRequired for rocket problems only.

^bSet variable to be FALSE if these calculations are not desired.

TABLE VII. - VARIABLES IN SHKINP NAMELIST^a

Variable	Dimension	Type	Value before read	Definition and comments
INCDEQ	1	L	TRUE	Calculate incident shock parameters assuming equilibrium compositions ^b
INCDFZ	1	L	TRUE	Calculate incident shock parameters assuming frozen compositions ^b
REFLEQ	1	L	FALSE	Calculate reflected shock parameters assuming equilibrium composition ^c
REFLFZ	1	L	FALSE	Calculate reflected shock parameters assuming composition frozen at incident composition ^c
U1	13	R	0	Shock velocity in m/sec (not required if values of Mach1 are listed)
MACH1	13	R	0	Ratio of shock velocity to the velocity of sound in the unshocked gas (not required if values of U1 are listed)

^aRequired for shock problems only.

^bSet variable to be FALSE if these calculations are not desired.

^cIf variable is set to be TRUE.

TABLE VIII. - SOURCES OF TRANSPORT DATA

Interaction	Temperature range of data included with program, K	Method (a)	Interaction	Temperature range of data included with program, K	Method (a)	Interaction	Temperature range of data included with program, K	Method (a)
Ar-Ar	200 to 5000	21	CO ₂ -SF ₆	200 to 5000	12	K-K	1000 to 10 000	18
Ar-CO	200 to 8000	9	CS ₂ -CS ₂	↓	1	Kr-Kr	200 to 5000	10
Ar-CO ₂	200 to 8000	11	C ₂ H ₂ -C ₂ H ₂	↓	↓	Kr-Xe	200 to 5000	14
Ar-H ₂	200 to 5000	12	C ₂ H ₄ -C ₂ H ₄	↓	↓	Li-Li	1500 to 10 000	18
Ar-He	200 to 5000	15	C ₂ H ₆ -C ₂ H ₆	↓	↓	N-N	1000 to 10 000	4
Ar-Kr	200 to 5000	14	C ₂ N ₂ -C ₂ N ₂	↓	↓	N-NO	1000 to 8000	11
Ar-N	1000 to 8000	11	C ₆ H ₆ -C ₆ H ₆	↓	↓	N-N ₂	1000 to 10 000	4
Ar-NO	200 to 8000	↓	Cl ₂ -Cl ₂	↓	↓	N-O	1000 to 10 000	4
Ar-N ₂	200 to 8000	↓	Cs-Cs	1000 to 10 000	18	ND ₃ -ND ₃	200 to 5000	2
Ar-O	1000 to 8000	↓	DCI-DCI	200 to 5000	3	NH ₃ -NH ₃	↓	2
Ar-O ₂	200 to 8000	↓	DF-DF	200 to 5000	2	NO-NO	↓	1
Ar-SF ₆	200 to 5000	12	D ₂ O-D ₂ O	300 to 5000	2	NO-NO ₂	↓	8
Ar-Xe	↓	15	F ₂ -F ₂	200 to 5000	1	NO-O	1000 to 10 000	4
BCl ₃ -BCl ₃	↓	1	H-H	1000 to 10 000	5	NO-N ₂ O ₄	200 to 2000	8
BF ₃ -BF ₃	↓	1	H-H ₂	1000 to 10 000	5	NO ₂ -NO ₂	200 to 5000	↓
Br ₂ -Br ₂	↓	1	H-He	2000 to 10 000	19	NO ₂ -O ₂	200 to 5000	↓
C-O	1000 to 10 000	22	H-Li	1000 to 10 000	6	NO ₂ -N ₂ O ₄	200 to 2000	↓
CCl ₄ -CCl ₄	200 to 5000	1	H-O	1000 to 10 000	6	N ₂ -N ₂	200 to 10 000	4
CF ₄ -CF ₄	↓	1	HBr-HBr	200 to 5000	2	N ₂ -O	1000 to 10 000	4
CHCl ₃ -CHCl ₃	↓	3	HCN-HCN	↓	2	N ₂ -O ₂	200 to 10 000	4
CH ₃ Cl-CH ₃ Cl	↓	3	HCl-HCl	↓	3	N ₂ -SF ₆	200 to 5000	12
CH ₃ OH-CH ₃ OH	↓	3	HF-HF	↓	2	N ₂ O-N ₂ O	200 to 5000	1
CH ₄ -CH ₄	↓	1	HI-HI	↓	1	N ₂ O ₄ -N ₂ O ₄	200 to 2000	8
CH ₄ -O ₂	↓	17	H ₂ -H ₂	200 to 10 000	5	N ₂ O ₄ -O ₂	200 to 2000	8
CO-CO	200 to 10 000	9	H ₂ -H ₂ O	300 to 5000	7	Na-Na	1000 to 10 000	18
CO-CO ₂	200 to 8000	↓	H ₂ -He	2000 to 10 000	20	Ne-Ne	200 to 5000	10
CO-H ₂	200 to 5000	↓	H ₂ -N ₂	200 to 5000	13	O-O	1000 to 10 000	4
CO-He	200 to 5000	↓	H ₂ -OH	500 to 5000	7	O-O ₂	1000 to 10 000	4

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CO-N	1000 to 10 000		H ₂ -O ₂	200 to 5000	7	OH-OH	500 to 5000	7
CO-N ₂	200 to 10 000		H ₂ -SF ₆	200 to 5000	12	OH-O ₂	500 to 5000	7
CO-O	1000 to 10 000		H ₂ O-H ₂ O	300 to 5000	2	O ₂ -O ₂	200 to 10 000	4
CO-O ₂	200 to 10 000		H ₂ O-O ₂	300 to 5000	7	Rb-Rb	1000 to 10 000	18
CO-SF ₆	200 to 5000	12	H ₂ S-H ₂ S	200 to 5000	2	SF ₆ -SF ₆	200 to 5000	1
COS-COS	200 to 5000	1	He-He		10	SO ₂ -SO ₂		2
CO ₂ -CO ₂	200 to 8000	11	He-Kr		14	SiF ₄ -SiF ₄		1
CO ₂ -H ₂	200 to 5000	13	He-N ₂		16	SiH ₄ -SiH ₄		1
CO ₂ -NO	200 to 8000	11	He-SF ₆		12	UF ₆ -UF ₆		1
CO ₂ -N ₂	200 to 8000		He-Xe		15	Xe-Xe		10
CO ₂ -O	1000 to 8000		I ₂ -I ₂		1			
CO ₂ -O ₂	200 to 8000							

^aMethods used to obtain transport data:

1. Lennard-Jones (12-6) potential. Parameters were taken from reference 33.
2. Stockmayer (12-6-3) potential. Parameters were obtained from reference 29. Equations for resonant correction were obtained from reference 20.
3. Same as previous method, except that parameters were obtained from reference 34.
4. Reference 35. Data were extended to lower temperatures in some cases by using the potential energy parameters of reference 35.
5. Reference 36. Data were extended to lower temperatures for H₂-H₂ by using the potential energy parameters of reference 36.
6. Reference 37.
7. Reference 25. Data were extended to lower temperatures in some cases by using the potential energy parameters of reference 25.
8. Lennard-Jones (12-6) potential. Parameters were obtained from reference 38.
9. Cross-section data for interactions of the type CO-X were assumed to be the same as those for interactions of the type N₂-X.
10. Data were obtained directly from the available transport property measurements. The cross sections were selected in order to adequately reproduce both the viscosity and thermal conductivity data. At higher temperatures the cross-section data were smoothed into the results obtained from molecular beam scattering measurements (ref. 39).
11. Reference 40. Data were extended to lower temperatures in some cases by using the potential energy parameters of reference 40.
12. Exponential-6 potential. Parameters were taken from reference 28.
13. Lennard-Jones (12-6) potential. Parameters were taken from reference 41.
14. Lennard-Jones (12-6) potential. Parameters were taken from reference 42.
15. Lennard-Jones (12-6) potential. Parameters were taken from reference 43.
16. Exponential-6 potential. Parameters were taken from reference 28. Experimental diffusion data (ref. 44) and molecular beam scattering measurements (ref. 45) were used.
17. Exponential-6 potential. Parameters were taken from reference 46.
18. Reference 47.
19. Reference 48.
20. Reference 49.
21. Reference 50. Method 10 was used at higher temperatures.
22. Reference 51.

TABLE IX. - ROTATIONAL COLLISION NUMBERS

Molecule	Z_{rot}^a	Source ^b
Ar	-----	Atom with no rotational energy modes
BCl ₃	1	Obtained by fitting thermal conductivity data
BF ₃	1	
Br ₂	2	
CCl ₄	1	
CF ₄	1	
CHCl ₃	908 to 26 581	Reference 29 ^b
CH ₃ Cl	20 to 406	Reference 29 ^b
CH ₃ OH	19 to 401	Reference 29 ^b
CH ₄	8	Obtained by fitting thermal conductivity data
CO	2	
COS	HE	
CO ₂	3	
CS ₂	HE	
C ₂ H ₂	1	
C ₂ H ₄	3	
C ₂ H ₆	HE	
C ₂ N ₂	2	Equation (44) using $Z_{rot}(N_2)$ as a reference
C ₆ H ₆	HE	Obtained by fitting thermal conductivity data
Cs	-----	Atom with no rotational energy modes
Cl ₂	1	Obtained by fitting thermal conductivity data
DCl	46 to 1084	Reference 29 ^b
DF	4.3 to 22	Reference 29 ^b
D ₂ O	13 to 37	Reference 29 ^b
F ₂	3	Obtained by fitting thermal conductivity data
H	-----	Atom with no rotational energy modes
HBr	485 to 6099	Reference 29 ^b
HCN	2.8 to 10.5	
HCl	61 to 1349	
HF	5.7 to 27	
HI	HE	Equation (44) using $Z_{rot}(I_2)$ as a reference

^aHE refers to Hirschfelder-Eucken approximation.

^bCalculations of theoretical collision numbers were extended to cover the temperature range shown in table VIII.

TABLE IX. - Concluded. ROTATIONAL COLLISION NUMBERS

Molecule	Z_{rot}^a	Source ^b
H ₂	12	Obtained by fitting thermal conductivity data
H ₂ O	15 to 40	Reference 29 ^b
H ₂ S	168 to 3393	Reference 29 ^b
He	-----	Atom with no rotational energy modes
I ₂	1	Obtained by fitting thermal conductivity data
K	-----	Atom with no rotational energy modes
Kr	-----	
Li	-----	
N	-----	
ND ₃	12 to 193	Reference 29 ^b
NH ₃	16 to 235	Reference 29 ^b
NO	2	Obtained by fitting thermal conductivity data
NO ₂	3	
N ₂	8	
N ₂ O	3	
N ₂ O ₄	1	Equation (44) using $Z_{rot}(NO_2)$ as a reference
Na	-----	Atom with no rotational energy modes
Ne	-----	Atom with no rotational energy modes
O	-----	Atom with no rotational energy modes
OH	8	Estimated
O ₂	8	Obtained by fitting thermal conductivity data
Rb	-----	Atom with no rotational energy modes
SF ₆	1	Obtained by fitting thermal conductivity data
SO ₂	28 to 657	Reference 29 ^b
SiF ₄	1	Obtained by fitting thermal conductivity data
SiH ₄	9	Equation (44) using $Z_{rot}(CH_4)$ as a reference
UF ₆	2	Equation (44) using $Z_{rot}(SF_6)$ as a reference
Xe	-----	Atom with no rotational energy modes

^aHE refers to Hirschfelder-Eucken approximation.

^bCalculations of theoretical collision numbers were extended to cover the temperature range shown in table VIII.

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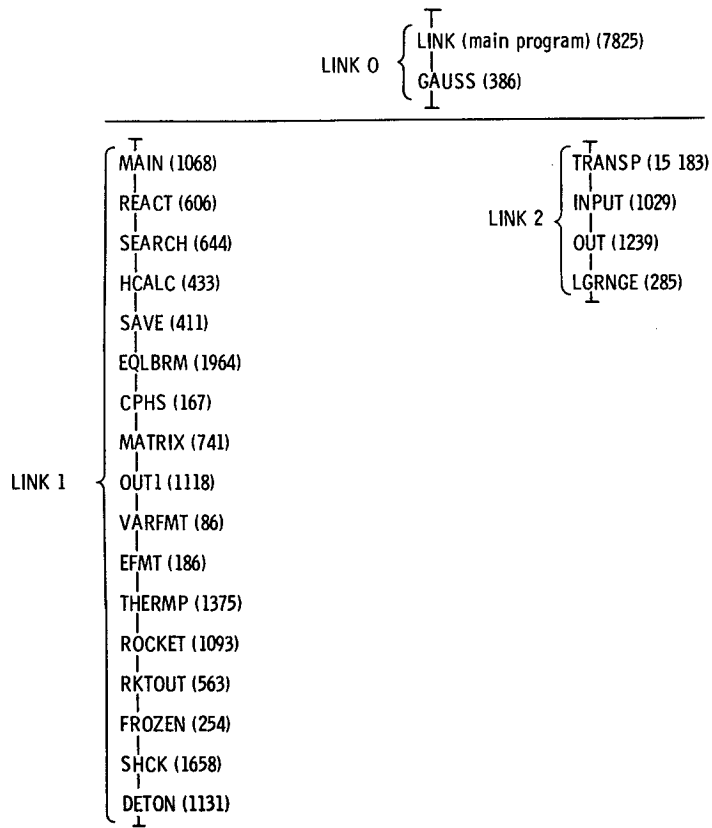


Figure 1. - Overlay structure of TRAN72 computer program for IBM 7094.

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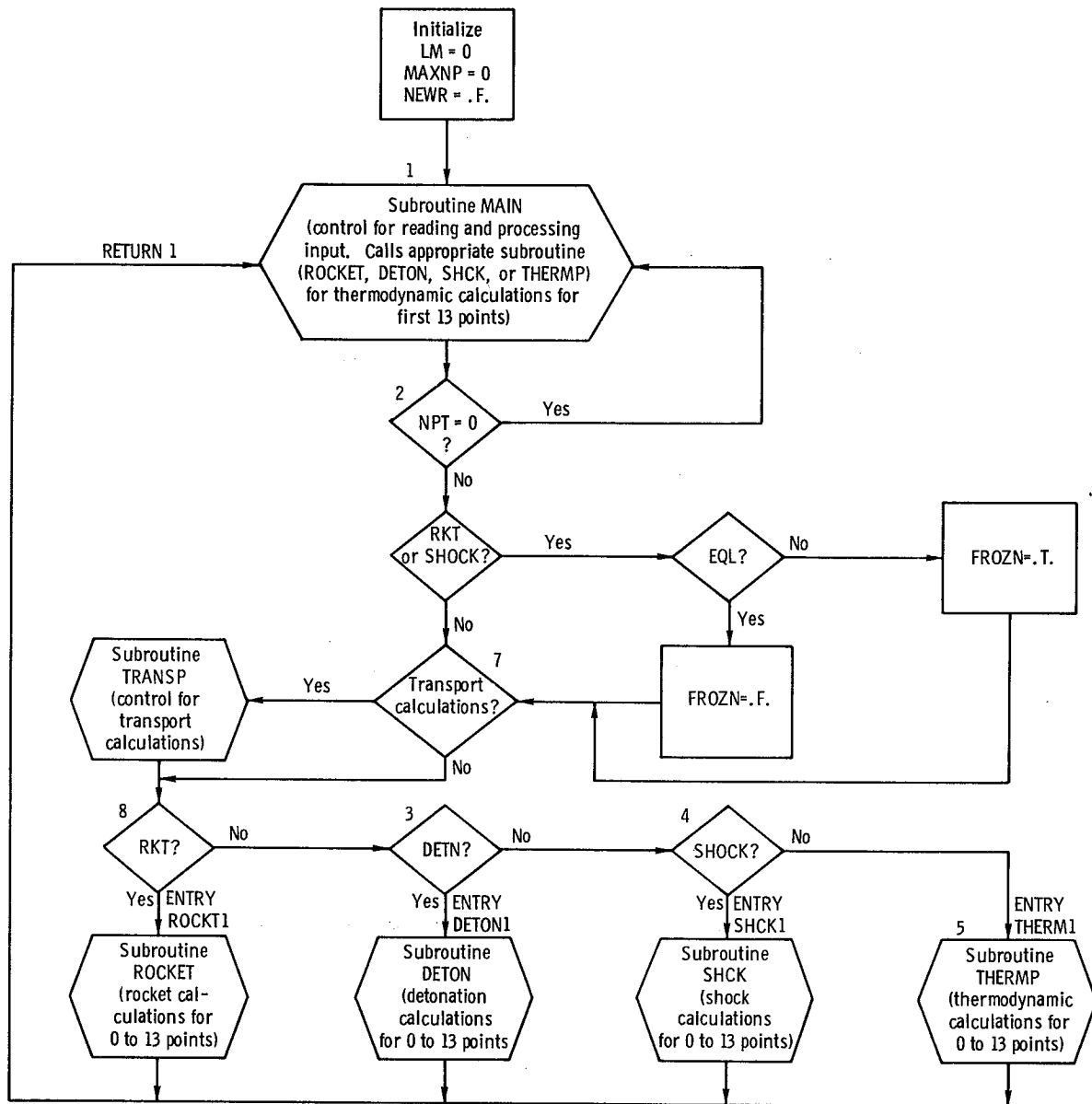


Figure 2. - Main program LINK.



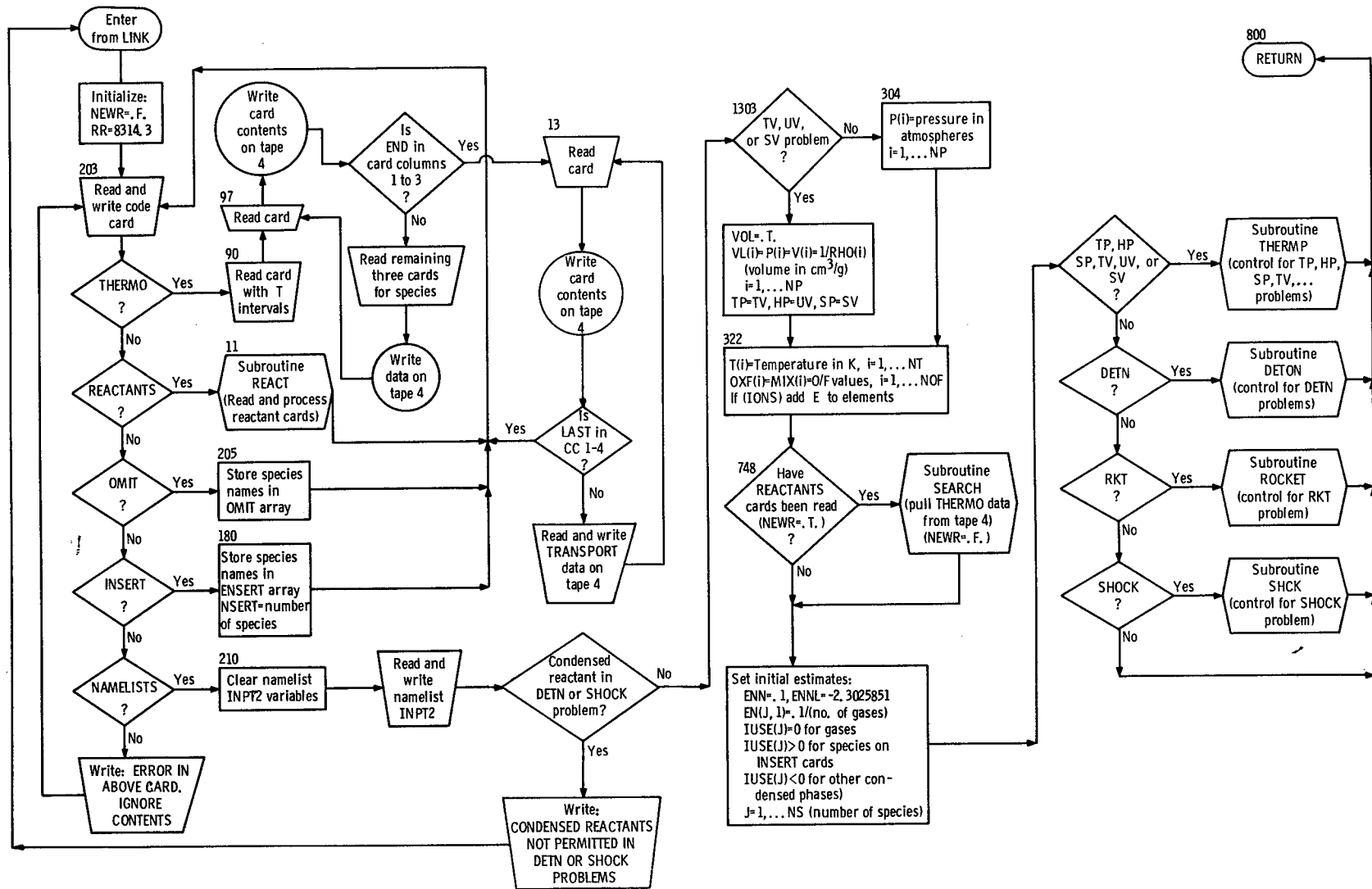


Figure 3. - Subroutine MAIN.

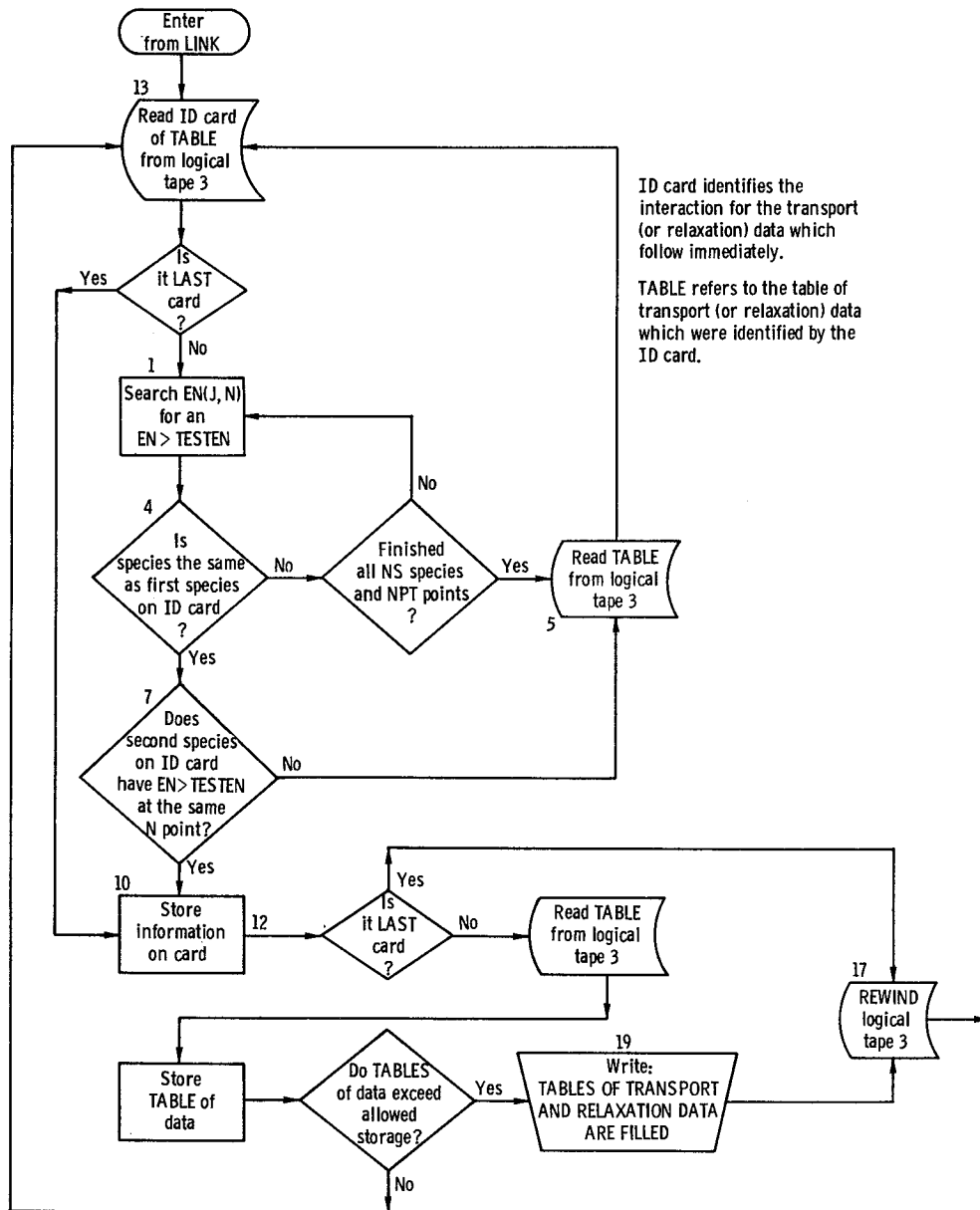
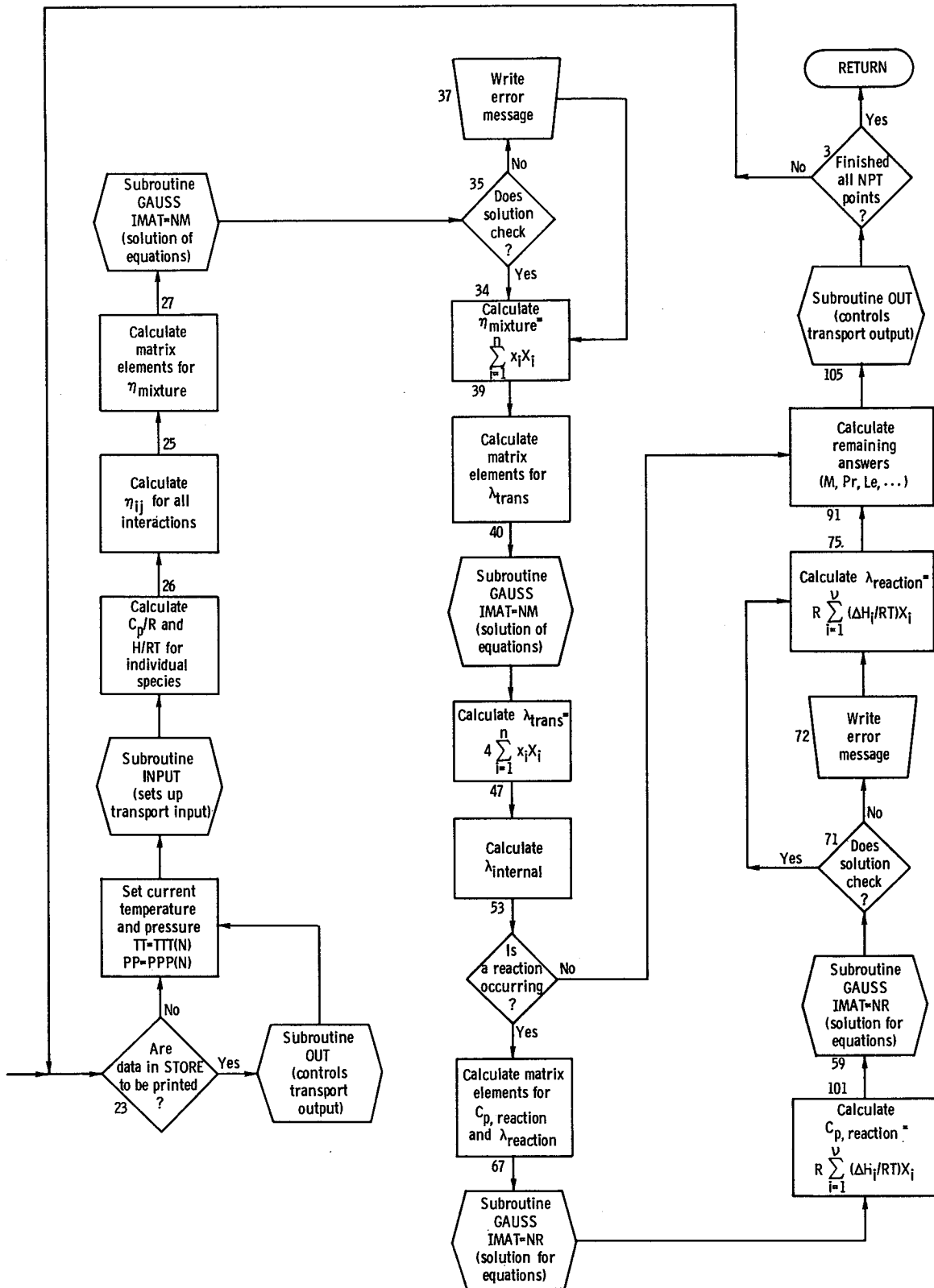


Figure 4. -



Subroutine TRANSP.

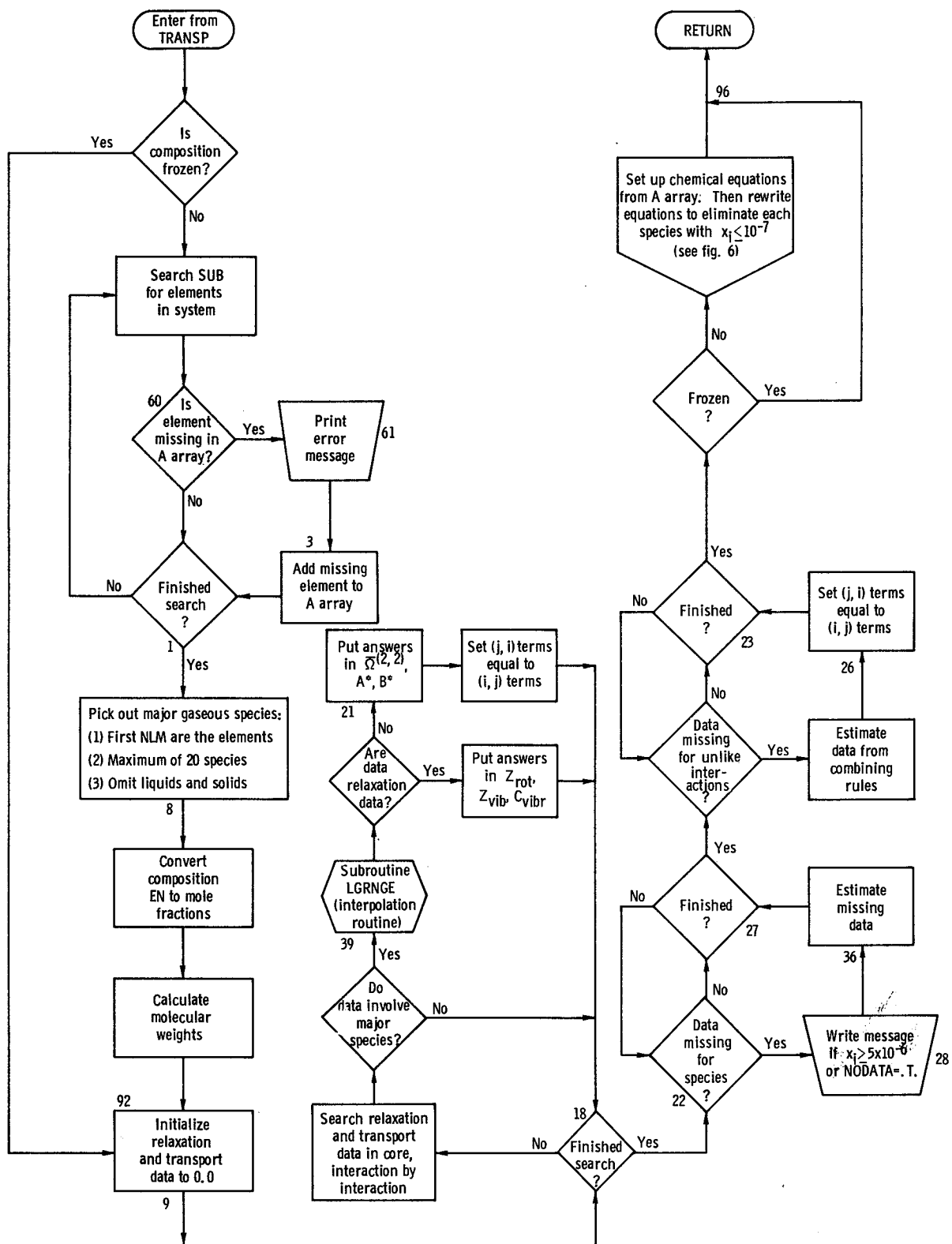


Figure 5. - Subroutine INPUT.

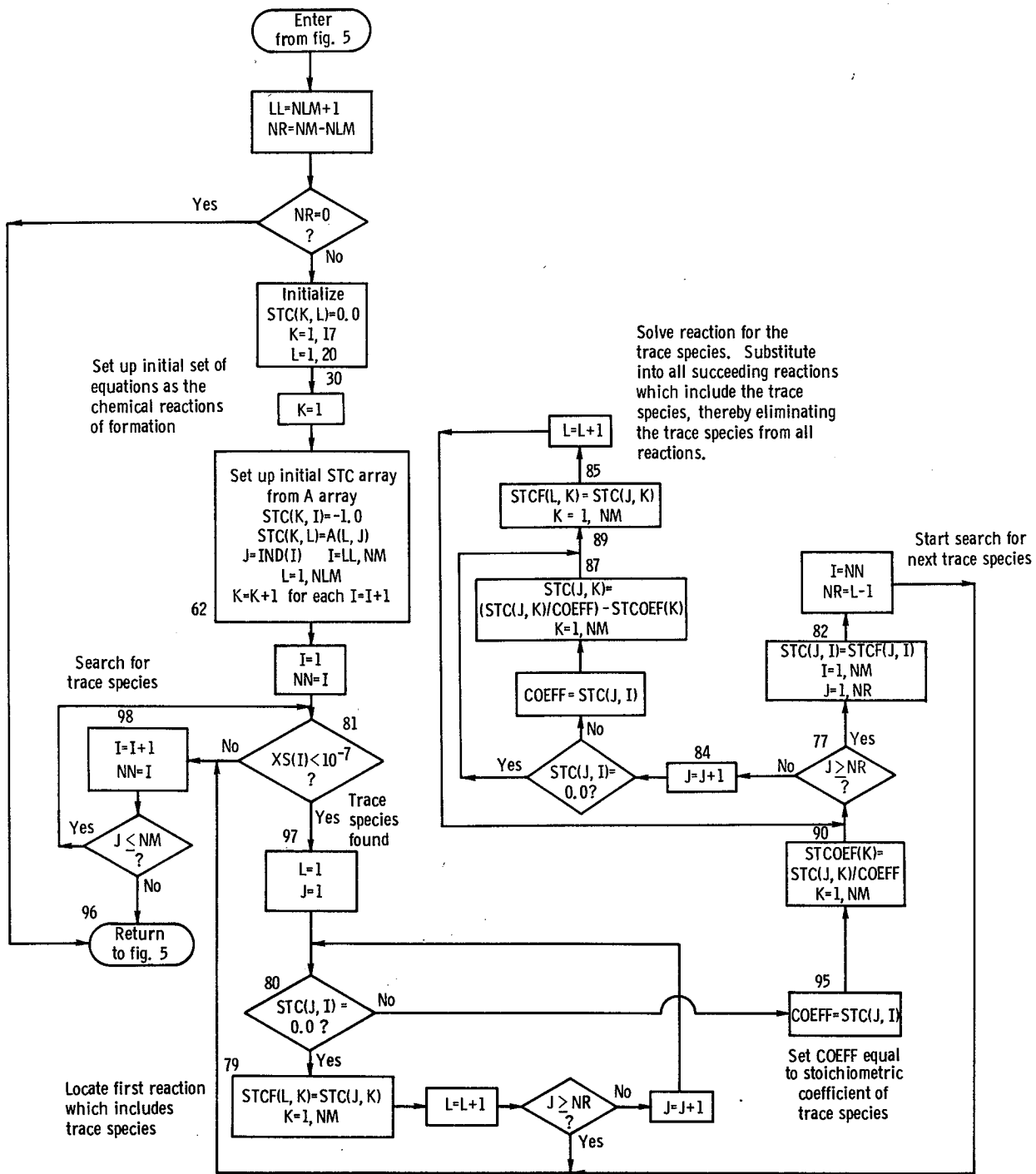


Figure 6. - Rewrite equations to eliminate trace species section in subroutine INPUT.

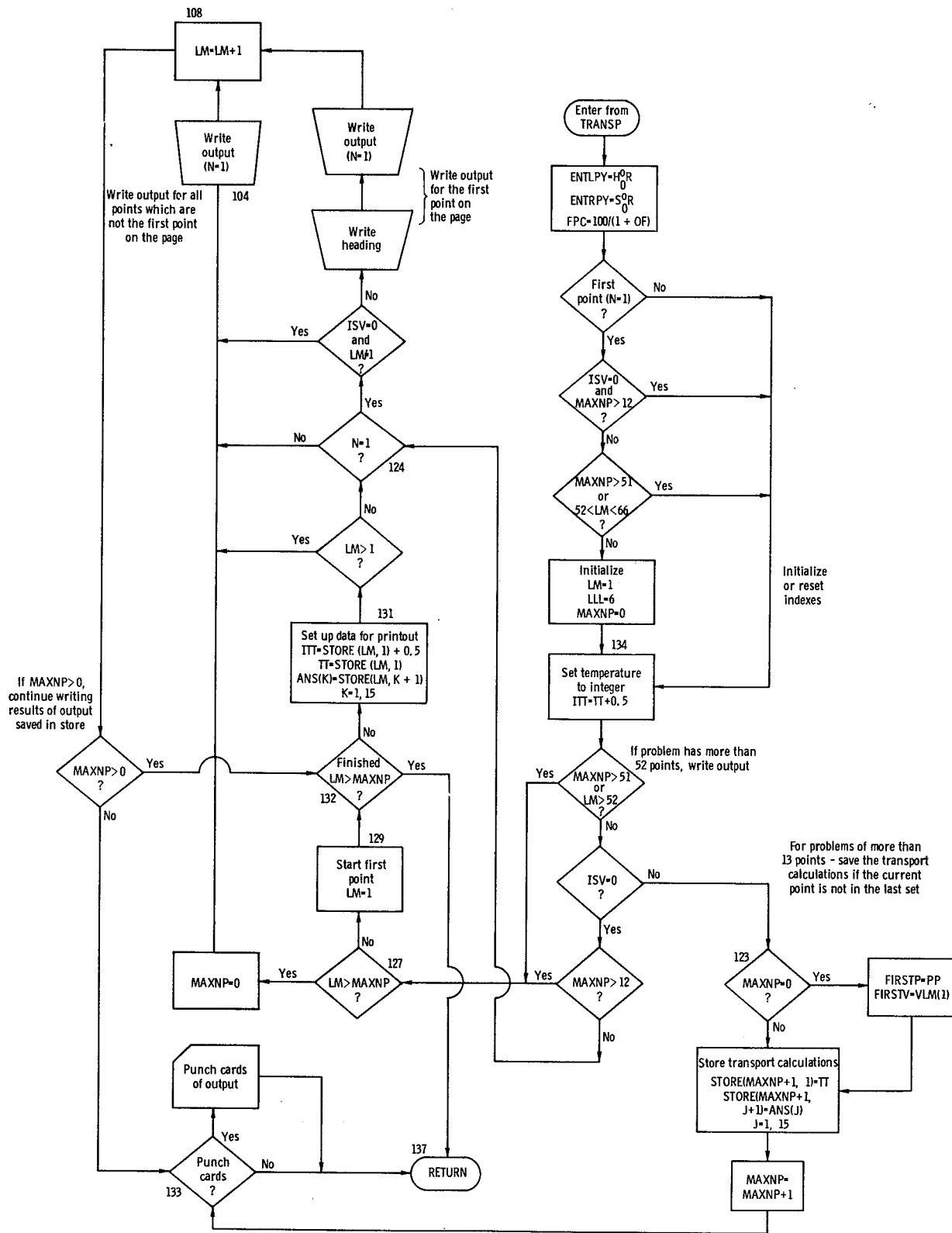


Figure 7. - Subroutine OUT.

