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**DESIGN AND EXPERIMENTAL PERFORMANCE  
OF SHORT CURVED WALL DIFFUSERS WITH  
AXIAL SYMMETRY UTILIZING SLOT SUCTION**

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16. Abstract <b>The feasibility of designing short curved wall axially symmetrical subsonic diffusers utilizing suction through slots in the diffuser walls to prevent flow separation was investigated. A potential flow analysis was made, and a digital computer program was written for determining the diffuser wall contour for prescribed boundary conditions. The flow field included branch flow so that the suction slot geometry could be a part of the diffuser design. One bell shaped diffuser and three annular diffusers with area ratios of either 2.5:1 or 3:1 were designed, fabricated, and tested. Minimum suction requirements for metastable operation ranged from 6.3% to 12% when operating with inlet air velocities in the 100 to 250 ft/sec (30 to 76 m/sec) range. For stable operation suction rates from 10% to 22% were required. In all cases the diffuser effectiveness was above 95% based on the conventional definition, and from 81% to 94% when the suction loss was accounted for. The exit velocity profiles were virtually flat with no more than ±9% variation over 95% of the exit area when operated with sufficient suction to prevent flow separation.</b>			
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## SUMMARY

This report presents results of an investigation concerning the analysis, design, and testing of short curved wall axially symmetrical subsonic diffusers utilizing suction through slots in the diffuser walls to prevent flow separation.

A potential flow analysis was made and a digital computer program was written for determining the diffuser wall geometry for prescribed boundary conditions. The prescribed boundary conditions included the following for the fluid velocity at the diffuser walls (both inner and outer walls for the annular diffusers): a region of nearly constant high velocity from the diffuser entrance to the slot; a region of rapid deceleration at the slot, and a region of nearly constant low velocity downstream from the slot to the diffuser exit. Branch flow was included in the flow field and this allowed the suction slot geometry to be a part of the design.

Four diffuser geometries were designed, fabricated and tested:

- (1) a 7-inch (18 cm) exit diameter bell shaped diffuser with an area ratio of 3:1 and a length to inlet radius ratio of 3.5:1.
- (2) a 9-inch (23 cm) exit diameter annular diffuser with an area ratio of 3:1 and a length to inlet width ratio of 5.0:1.
- (3) a 9-inch (23 cm) exit diameter annular diffuser with an area ratio of 2.5:1 and a length to inlet width ratio of 3.9:1.
- (4) an 18-inch (46 cm) exit diameter annular diffuser with an area ratio of 3:1 and a length to inlet width ratio of 3.6:1.

For inlet air velocities in the 200-250 ft/sec (61-76 m/sec) range, metastable operation required 6.5% suction for the bell shaped diffuser while

stable operation required 12% suction. Corresponding suction rates for the 9-inch (23 cm) annular diffuser (3:1 area ratio) were 8.5% and 16.0% for metastable and stable operation respectively. For the 9-inch (23 cm) annular diffuser with 2.5:1 area ratio, 6.3% and 12% suction rates were required. For the 18-inch (46 cm) annular diffuser, only 7% suction was required for metastable operation and 10% for stable operation.

Suction rate requirements were found to increase as inlet velocity was decreased. Thus for stable operation of the 18-inch (46 cm) diffuser the required suction rate was about 20% at 100 ft/sec (30 m/sec) inlet velocity.

In all cases the diffuser effectiveness was above 95% based on the conventional definition, and from 81% to 94% when the suction loss was accounted for. The exit velocity profiles were virtually flat with no more than  $\pm 9\%$  variation over 95% of the exit area when operated with sufficient suction to prevent separation.

Non-uniform inlet tests and tests with periodic shedding of wakes upstream of the diffuser inlet were conducted on the 9-inch (23 cm) annular diffuser with AR=3:1. Non-uniform inlet conditions caused no significant increase in the required suction rates. However, periodic shedding of wakes upstream of the diffuser inlet caused the suction requirement for stable operation to be increased from 16.0% to 18.0%.

A downstream obstruction in the form of a perforated metal sheet at the diffuser exit slightly increased the minimum suction rate requirement at low inlet velocities and had no significant effect upon the suction rate requirement at inlet velocities above 150 ft/sec (46 m/sec).

## LIST OF SYMBOLS

A	Area
AR	Area ratio, exit to inlet
$C_p$	Pressure recovery coefficient, $\frac{P_{s,e} - P_{s,i}}{P_{d,i}}$
D	Diameter
FS	Fraction of inlet flow removed by suction
KE	Kinetic energy per unit mass flowing
$\dot{m}$	Mass flow rate
n	Natural coordinate normal to streamlines
P	Pressure (either static, dynamic, or total depending upon subscript)
Q	Local to upstream velocity vector magnitude ratio
R	Radial coordinate of axially symmetrical system
Re No	Reynold's number, $\left[ \frac{(4 A_{cs}/\text{perimeter})(\text{velocity})}{\text{fluid kinematic viscosity}} \right]_{\text{inlet}}$
s	Natural coordinate along a streamline
U	Fluid velocity outside the boundary layer
$\bar{U}$	Mean velocity at a section
W	Width of diffuser inlet passage
X	Axial coordinate of axially symmetrical system
$\alpha$	Velocity vector angle measured from horizontal
$\delta$	Boundary layer displacement thickness
$\epsilon$	Diffuser effectiveness, $\frac{\dot{m}_e (P_{s,e} - P_{s,i})}{\dot{m}_i (P_{s,e} - P_{s,i})_{\text{ideal}}}$
$\eta$	Diffuser effectiveness, $\frac{(P_{s,e} - P_{s,i})}{(P_{s,e} - P_{s,i})_{\text{ideal}}}$



$\kappa$	Kinetic energy coefficient, $\frac{1}{A} \int_A \left(\frac{U}{\bar{U}}\right)^3 dA$
$\Phi$	Maximum value of the velocity potential function
$\phi$	Velocity potential function
$\Psi$	Maximum value of the stream function
$\psi$	Stream function
$\rho$	Fluid density

### Subscripts

cs	Cross sectional
e	Diffuser exit
d,i	Dynamic inlet
i	Diffuser inlet
max	Maximum
s,e	Static exit
s,i	Static inlet
t,e	Total exit
t,i	Total inlet
1	Upstream
2	Downstream

## SECTION I INTRODUCTION

### 1.1 Background

In an internal flow system, a diffuser is a transitional section which connects a flow passage having a smaller cross-sectional area to a flow passage of larger area. Two desirable characteristics of a diffuser are that it will provide a nearly uniform velocity distribution at its exit plane and that it will transform most of the kinetic energy of the fluid at entrance into potential energy in the form of a higher static pressure at the exit plane.

A previous report by the authors [1]<sup>1</sup> concerned the feasibility of designing short two-dimensional diffusers utilizing suction through the diffuser wall slots. The design philosophy was to prescribe the diffuser wall velocity so as to have essentially constant high velocity upstream of a slot, constant low velocity downstream of the slot, and thus have all the deceleration occur across the slot. By removing through the slot those fluid particles having insufficient kinetic energy to get across the adverse pressure gradient in the region of the slot, flow separation could be avoided. The concept of having deceleration occur abruptly and applying slot suction to this narrow region was originally suggested by A. A. Griffith as reported by Lachmann [2] and is henceforth referred to as the Griffith diffuser.

The two-dimensional Griffith diffusers designed and tested were only partially successful. When sufficient suction was applied to prevent

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<sup>1</sup>Numbers in brackets refer to the references at the end of this report.

separation, the diffuser exit plane velocity distribution was nearly uniform and very low total pressure losses were achieved. However, the suction rates required for stable operation varied from 16% for 2:1 area ratio to 44% for 4:1 area ratio. Problems were encountered in designing the optimum slot geometry and also in controlling the sidewall boundary layer.

In 1952, L. R. Manoni [3] designed several bell channel diffusers based upon the Griffith concept. He used an electrical analogy tank to determine the wall geometry required for the specified wall velocity distribution. While his design method was only approximate and somewhat cumbersome, he was able to demonstrate that such a concept would enable the design and operation of a relatively short diffuser without separation provided that sufficient slot suction could be applied.

In order to design planar flow channel geometries, J. D. Stanitz [4] in 1953 performed a double transformation of the describing equations into a coordinate system where the geometry did not need to be known for the equations to be solved. After the equations were solved on the transformed plane, the inverse transformation yielded the desired geometry.

In 1971, C. D. Nelson [5] extended the work of Stanitz by developing a method for transforming the flow equations of an axially symmetrical coordinate system. Nelson also devised an approximation to account for the branch flow due to the slot by solving the channel design problem with a more complicated set of boundary conditions.

## 1.2 Objective

The objective of the research effort described in this report was to examine the concept and the practicality of a short axially symmetrical subsonic curved wall diffuser using suction through slots in the diffuser walls to prevent flow separation.

## 1.3 Scope

In order to achieve the objective a research program was carried out to

(1) Develop a digital computer program which will determine the wall shape of an axially symmetrical or a two-dimensional diffuser for prescribed boundary conditions.

(2) Utilize the program to design one bell-shaped diffuser and three annular diffusers with area ratios of about 3:1.

(3) Fabricate and test each of the above diffusers to determine

- (a) The minimum suction requirement for unseparated flow as a function of inlet air velocity;
- (b) Performance characteristics such as diffuser effectiveness, total pressure loss, and exit plane velocity distribution;
- (c) Effect of non-uniform inlet velocity distributions;
- (d) Effect of periodic shedding of wakes upstream of the diffuser inlet;
- (e) Effect of imbalance between inner and outer wall suction rates per unit slot length;
- (f) Effect of downstream blockage in the form of perforated steel plates.

SECTION 2  
ANALYSIS AND DESIGN

2.1 Analysis for Determination of Diffuser Geometry

The describing equations of incompressible irrotational motion and continuity in the axially symmetrical coordinate system are

$$\frac{\partial^2 \phi}{\partial R \partial X} - \frac{\partial^2 \phi}{\partial X \partial R} = 0 \quad (1)$$

and

$$\frac{\partial^2 \phi}{\partial X^2} + \frac{\partial^2 \phi}{\partial R^2} + \frac{1}{R} \frac{\partial \phi}{\partial R} = 0 \quad (2)$$

The geometry of the channel being designed might appear as shown in Figure 1.

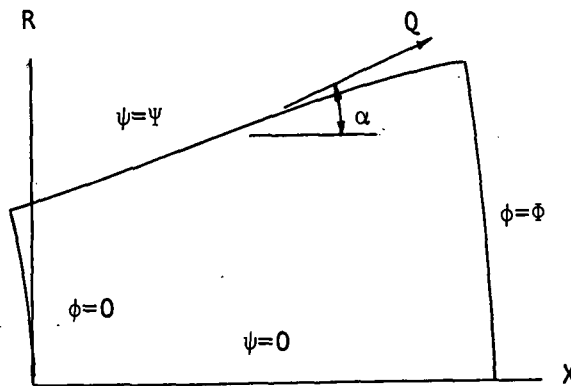


Figure 1. Possible flow channel geometry on the physical plane.

Transforming equations (1) and (2) into natural coordinates by using

$$ds = \cos \alpha dX + \sin \alpha dR \quad (3)$$

$$dn = -\sin \alpha dX + \cos \alpha dR \quad (4)$$

and introducing the stream function and velocity potential in natural coordinates

$$d\psi = R Q dn \quad (5)$$

$$d\phi = Q ds \quad (6)$$

results in the equations

$$\frac{\partial \ln Q}{\partial n} - \frac{\partial \alpha}{\partial s} = 0 \quad (7)$$

and

$$\frac{\partial \ln Q}{\partial s} + \frac{1}{R} \frac{\partial R}{\partial s} + \frac{\partial \alpha}{\partial n} = 0 \quad (8)$$

The channel geometry on the natural coordinate plane might then appear as shown in Figure 2.

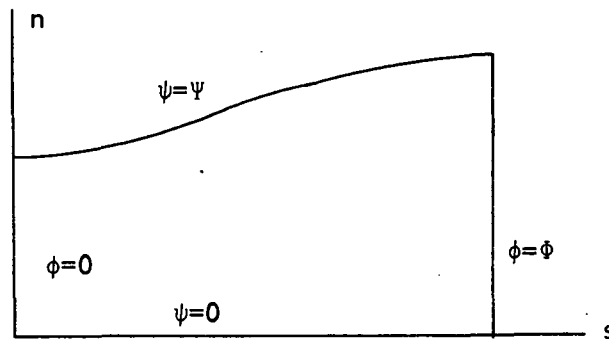


Figure 2. Possible flow channel geometry on natural coordinate system.

Now using equations (5) and (6) to transform from natural coordinates to a  $\phi$ - $\psi$  coordinate system results in the following equations of irrotational motion and continuity.

$$R \frac{\partial \ln Q}{\partial \psi} - \frac{\partial \alpha}{\partial \phi} = 0 \quad (9)$$

and

$$\frac{1}{R} \frac{\partial \ln Q}{\partial \phi} + \frac{1}{R^2} \frac{\partial R}{\partial \phi} + \frac{\partial \alpha}{\partial \psi} = 0 \quad (10)$$

The flow field on the  $\phi$ - $\psi$  plane might appear as shown in Figure 3.

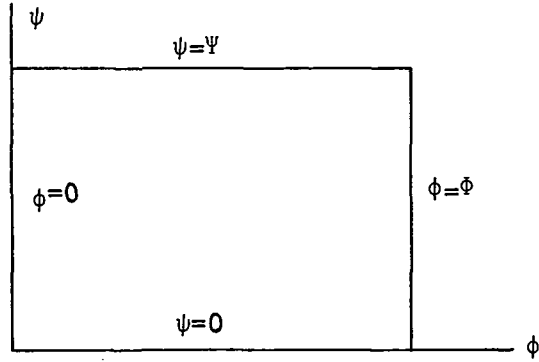


Figure 3. Possible flow field on stream function-velocity potential plane.

Cross differentiation of equations (9) and (10) to eliminate  $\alpha$  yields

$$R^4 \frac{\partial^2 \ln Q}{\partial \psi^2} + R^3 \frac{\partial R}{\partial \psi} \frac{\partial \ln Q}{\partial \psi} + R^2 \frac{\partial^2 \ln Q}{\partial \phi^2} - R \frac{\partial R}{\partial \phi} \frac{\partial \ln Q}{\partial \phi} + R \frac{\partial^2 R}{\partial \phi^2} - 2 \left( \frac{\partial R}{\partial \phi} \right)^2 = 0 \quad (11)$$

The inverse transformations for  $\alpha$ ,  $X$ , and  $R$  are

$$d\alpha = R \frac{\partial \ln Q}{\partial \psi} d\phi - \left( \frac{1}{R} \frac{\partial \ln Q}{\partial \phi} + \frac{1}{R^2} \frac{\partial R}{\partial \phi} \right) d\psi \quad (12)$$

$$dX = \frac{\cos \alpha}{Q} d\phi - \frac{\sin \alpha}{RQ} d\psi \quad (13)$$

$$dR = \frac{\sin \alpha}{Q} d\phi + \frac{\cos \alpha}{RQ} d\psi \quad (14)$$

Since in eqn. (11) the radial coordinate  $R$  remains as a dependent variable, one method of solution consists of assuming values for the radial coordinates and then alternately solving for  $\ln Q$  and  $R$  in an iterative manner.

As a first trial, assume  $R=1$  which reduces equation (11) to

$$\frac{\partial^2 \ln Q}{\partial \psi^2} + \frac{\partial^2 \ln Q}{\partial \phi^2} = 0 \quad (15)$$

which is the same as the corresponding plane flow equation of Stanitz [4]. The term  $\ln Q$  may be found for a given set of boundary conditions by utilizing some numerical scheme such as the Gauss-Siedel method. Boundary conditions are prescribed along the wall streamlines and along the inlet and outlet equipotential lines.

The first approximation to the velocity vector angles  $\alpha$  are then computed from

$$\alpha_2 - \alpha_1 = \int_{\psi} \frac{\partial \ln Q}{\partial \psi} d\phi - \int_{\phi} \frac{\partial \ln Q}{\partial \phi} d\psi \quad (16)$$

where the path of integration is chosen to be along equipotential lines and streamlines.

The R coordinates are then computed using the line integrals

$$R_2 - R_1 = \int_{\psi} \frac{\sin \alpha}{Q} d\phi \quad (17)$$

$$\text{and } R_2^2 - R_1^2 = 2 \int_{\phi} \frac{\cos \alpha}{Q} d\psi \quad (18)$$

These R coordinates are treated as a second approximation to solve equation (11) again for new velocities. New flow angles are computed using the line integrals

$$\alpha_2 - \alpha_1 = \int_{\psi} R \frac{\partial \ln Q}{\partial \psi} d\phi \quad (19)$$

$$\text{and } \alpha_2 - \alpha_1 = - \int_{\phi} \left( \frac{1}{R} \frac{\partial \ln Q}{\partial \phi} + \frac{1}{R^2} \frac{\partial R}{\partial \phi} \right) d\psi \quad (20)$$

Corrected R coordinates are again computed from equations (17) and (18) and the entire process is reiterated until the R coordinates have converged sufficiently.

The axial coordinates are computed next by using the line integrals



$$x_2 - x_1 = \int_{\psi} \frac{\cos \alpha}{Q} d\phi \quad (21)$$

$$\text{and } x_2 - x_1 = - \int_{\phi} \frac{\sin \alpha}{R Q} d\psi \quad (22)$$

In order to account for the branch flow due to slot suction, a more complicated set of boundary conditions are necessary. The physical flow system may now appear as in Figure 4. The formerly simple channel wall now involves curves B, C, D, and E with some of the flow leaving across C. This introduces a stagnation point at A.

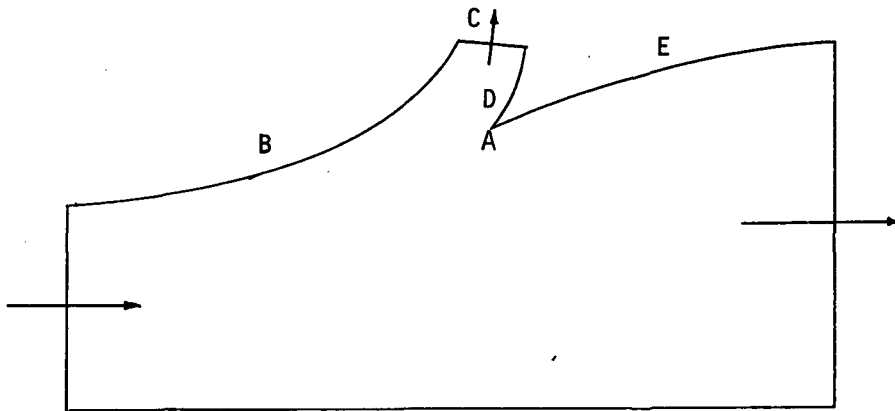


Figure 4. Possible geometry with branch flow.

On streamlines B, D, and E, the value of the desired velocity is prescribed as usual, but on line C, (which is chosen to be a constant potential line),

$$\frac{\partial \ln Q}{\partial \phi} = 0 \quad \text{and} \quad \frac{\partial R}{\partial \phi} = 0$$

are specified which in essence prescribes a parallel flow across C.

The stagnation point A introduces a singularity into equation (11) since  $\ln Q$  is not defined when  $Q = 0$ . In order to circumvent the difficulty introduced

by this singularity, a portion of the potential flow solution for two-dimensional flow around a wedge was patched into a small region around the stagnation point. The introduction of this two-dimensional wedge flow patch yields only an approximate solution which becomes more accurate as the radial dimension of the patch becomes small relative to the distance of the stagnation point from the axis of symmetry.

## 2.2 Digital Computer Design Program

The digital computer program which was used to design the wall contours of the Griffith diffusers described in this report has the following features.

- (1) It may be used to design either planar (two-dimensional) or axially symmetrical (bell shaped or annular) flow channels.
- (2) Branch flow due to slot suction is incorporated into the design program.
- (3) The boundary conditions are flexible; i.e., at either entrance to or exit from the flow channel, the velocities may be prescribed (Dirichlet boundary conditions) or the velocity gradients may be set to zero (Neumann boundary conditions) so as to result in unidirectional flow at either entrance or exit. The wall velocities are prescribed at up to 148 points along each channel wall (both inner and outer walls if annular).
- (4) Up to 148 mesh points may be used in the  $\phi$  direction and up to 48 points may be used in the  $\psi$  direction.
- (5) Printed output includes the coordinates ( $R$  and  $X$ ), velocities ( $Q$ ), and flow angles ( $\alpha$ ) for each mesh point and a summary of the wall coordinates of the channel design.
- (6) Graphical output includes all the streamlines and potential flow

lines on the X-R (or X-Y) plane. Also, the inlet and outlet velocity profiles are plotted as a function of the R (or Y) coordinate.

Using a 48 x 135 grid, a typical axially symmetrical design requires about 45 minutes on an IBM System 360 Model 50 computer. A typical two-dimensional design of comparable grid points requires about 20 minutes.

The program listing is given in Appendix A. Appendix B describes briefly the procedure used in obtaining the 18-inch (46 cm) annular diffuser design.

### 2.3 Griffith Diffuser Geometry

Figures 5, 6, and 7 show the geometries of the bell shaped diffuser, the 9-inch (23 cm) annular diffuser, and the 18-inch (46 cm) annular diffuser respectively. The diffusers were designed to have an area ratio of about 3:1 since this represents a typical diffuser application.

The diffuser geometries were analyzed using the Douglas Neumann technique [6] to predict the velocity distributions along the diffuser walls and at the diffuser inlet and exit planes. A comparison was made between the velocities predicted by the analysis program and those prescribed to the design program. In each case the agreement was good although slight disagreements occurred in the vicinity of the slot.

The bell shaped diffuser had the simplest geometry and was designed and tested first. Only one curved wall had to be considered and its slot was relatively far away from the axis of symmetry.

The second geometry designed and tested was the 9-inch (23 cm) annular diffuser. Since two slotted walls were involved with the inner wall slot being closer to the axis of symmetry, this case provided a more severe test of the slot design procedure using the two-dimensional wedge flow patch.

The third diffuser used the same outer body as the second diffuser, but a smaller inner body was designed so as to change the area ratio from 3:1 to

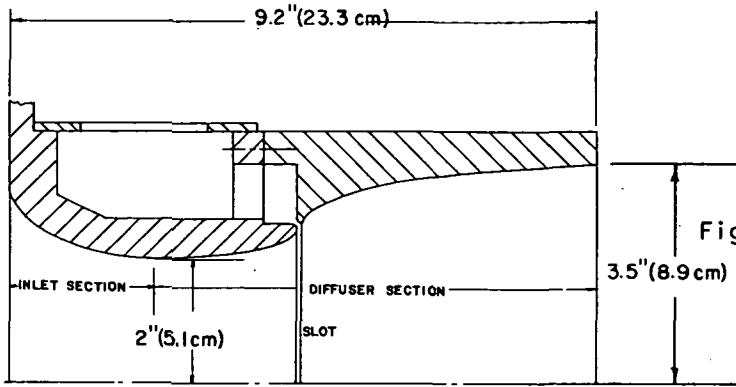


Figure 5. Bell shaped diffuser

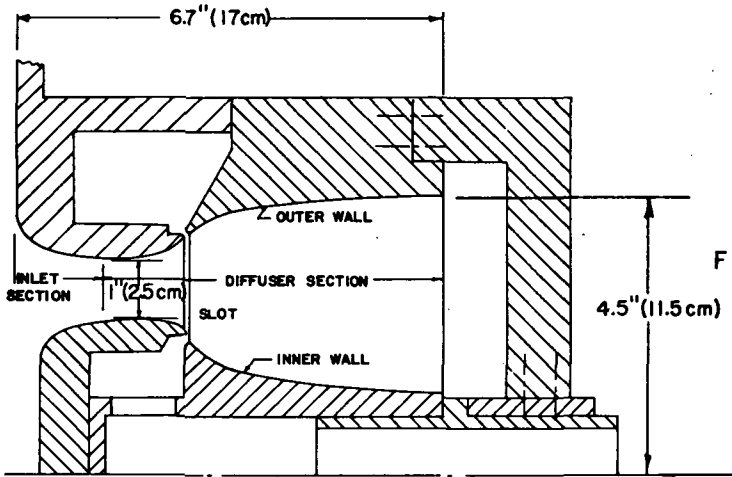


Figure 6. 9" (23 cm) annular diffuser

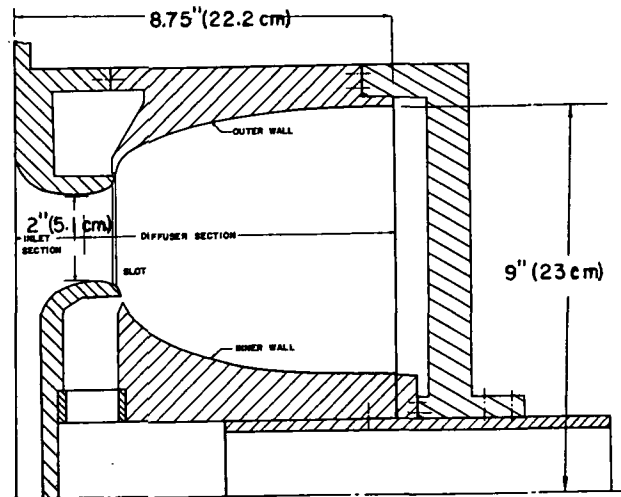


Figure 7. 18" (46 cm) annular diffuser

2.5:1. This diffuser was to demonstrate that a common outer body could be used with more than one inner body thus providing more than one area ratio without a completely new diffuser.

The last diffuser designed and tested was the 18-inch (46 cm) annular diffuser. This diffuser was to verify that a reduction of slot suction can be achieved by reducing the ratio of  $\bar{\delta}/W$ .  $\bar{\delta}$  is the boundary layer displacement thickness just upstream of the slot, and  $W$  is the annular width of the diffuser at inlet.

### SECTION 3 INSTRUMENTATION AND APPARATUS

#### 3.1 Test Facility

Two primary air supplies were used in testing the diffusers. The 18" annular diffuser was tested using a 30,000 CFM ( $14 \text{ m}^3/\text{sec}$ ) industrial fan delivering air through a 42-inch (106 cm) by 48-inch (122 cm) duct 30 ft. (9.1 m) long.

All other diffusers were tested using a 10,000 CFM ( $4.72 \text{ m}^3/\text{sec}$ ) fan delivering air through a 20-inch (51 cm) circular duct 20 ft. (6.1 m) long. Flow straightener tubes and fine mesh screens were installed inside the duct to provide a uniform steady flow to the test section. A shutter type damper at the fan inlet was used to regulate the flow rate.

Two diesel superchargers were installed in parallel providing for up to 900 CFM ( $0.43 \text{ m}^3/\text{sec}$ ) suction air through the diffuser slots. Seven gate valves located in six suction lines and an air bleed line provided a flexible setup for varying both the total amount of slot suction and the distribution of suction between the inner wall and the outer wall of the annular diffusers. Plastic pipe lengths and fittings were attached between the diffuser and the

suction control valves and all joints were sealed with tape to eliminate air leakage.

The diffusers were fabricated from aluminum stock. The wall contours were cut on a pattern lathe. Figure 8 shows the 18-inch (46 cm) annular diffuser attached to the end of the large air supply duct. Figure 9 shows the bell shaped diffuser attached to the small air supply duct.

### 3.2 Instrumentation and Measurements

The stagnation pressure at the end of each duct and the static pressure at the diffuser inlet were measured with a micromanometer having resolution of 0.001 inch of water. Wall static pressure taps were installed in the diffusers by glueing 1/16-inch o.d. brass tubes into holes drilled in the diffuser walls and smoothing the ends to conform to the diffuser contour. The pressure signals were monitored on an inductive type pressure transducer through a rapid scanning mechanism. Up to 48 pressure taps could be scanned in 30 seconds. The output of the pressure transducer was recorded on paper tape with a digital recorder.

Velocity profiles were measured with a constant temperature hot wire probe. The voltage output of the probe was displayed by a multirange digital voltmeter with a selective damping device. The probe was positioned in the diffuser with a traversing mechanism adapted from a milling machine bed.

Depending upon the size of diffuser being tested either five or six flow meters were used to measure the slot suction rates. A manometer bank with 20 legs each 60-inches high employing either water or carbon tetrachloride was used to obtain the flow meter pressure differentials. A copper-constantan thermocouple was used to measure the air temperature, and a well-type barometer was used to obtain atmospheric pressure.

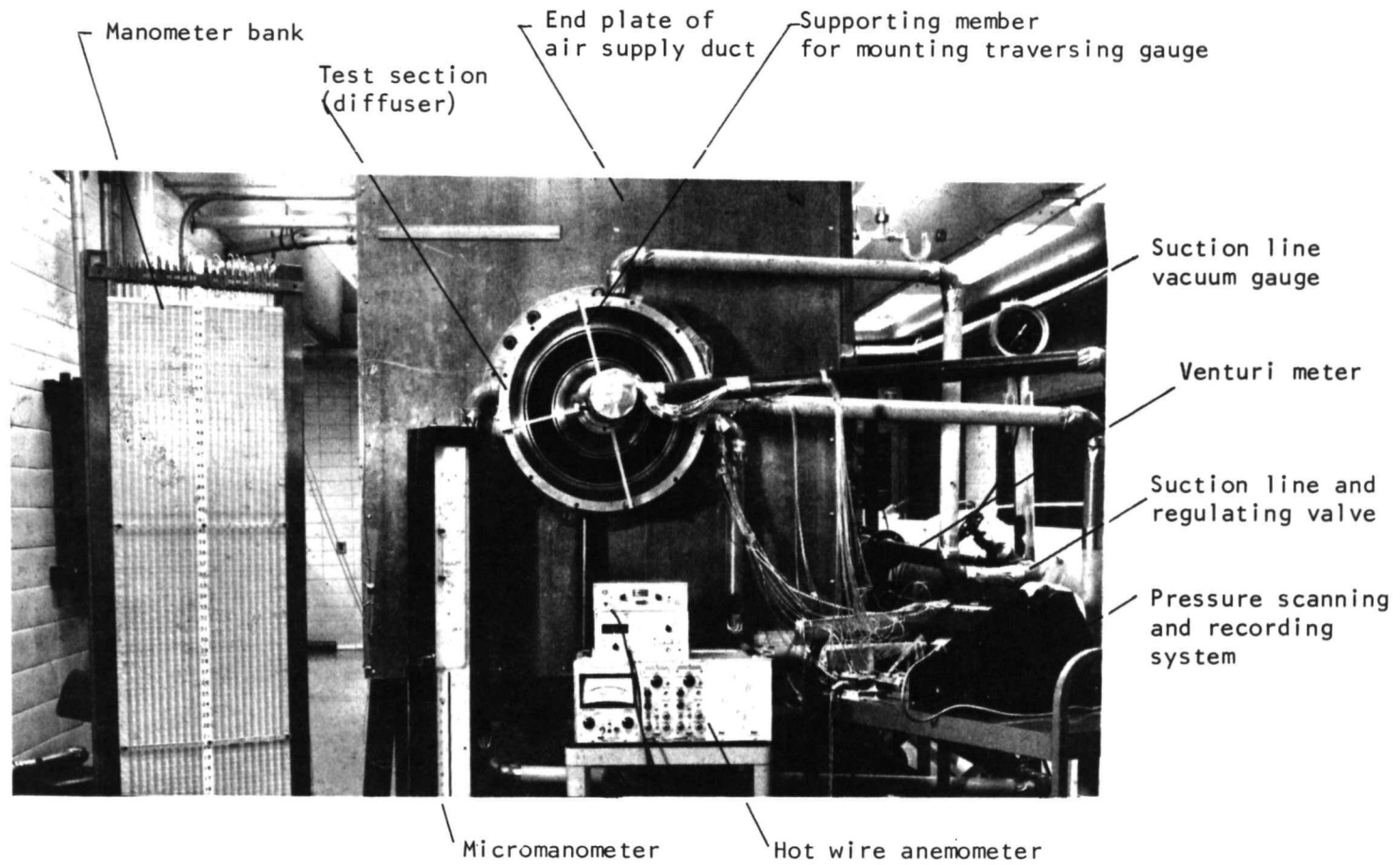


Figure 8. 18" (46 cm) annular diffuser attached to the large air supply duct

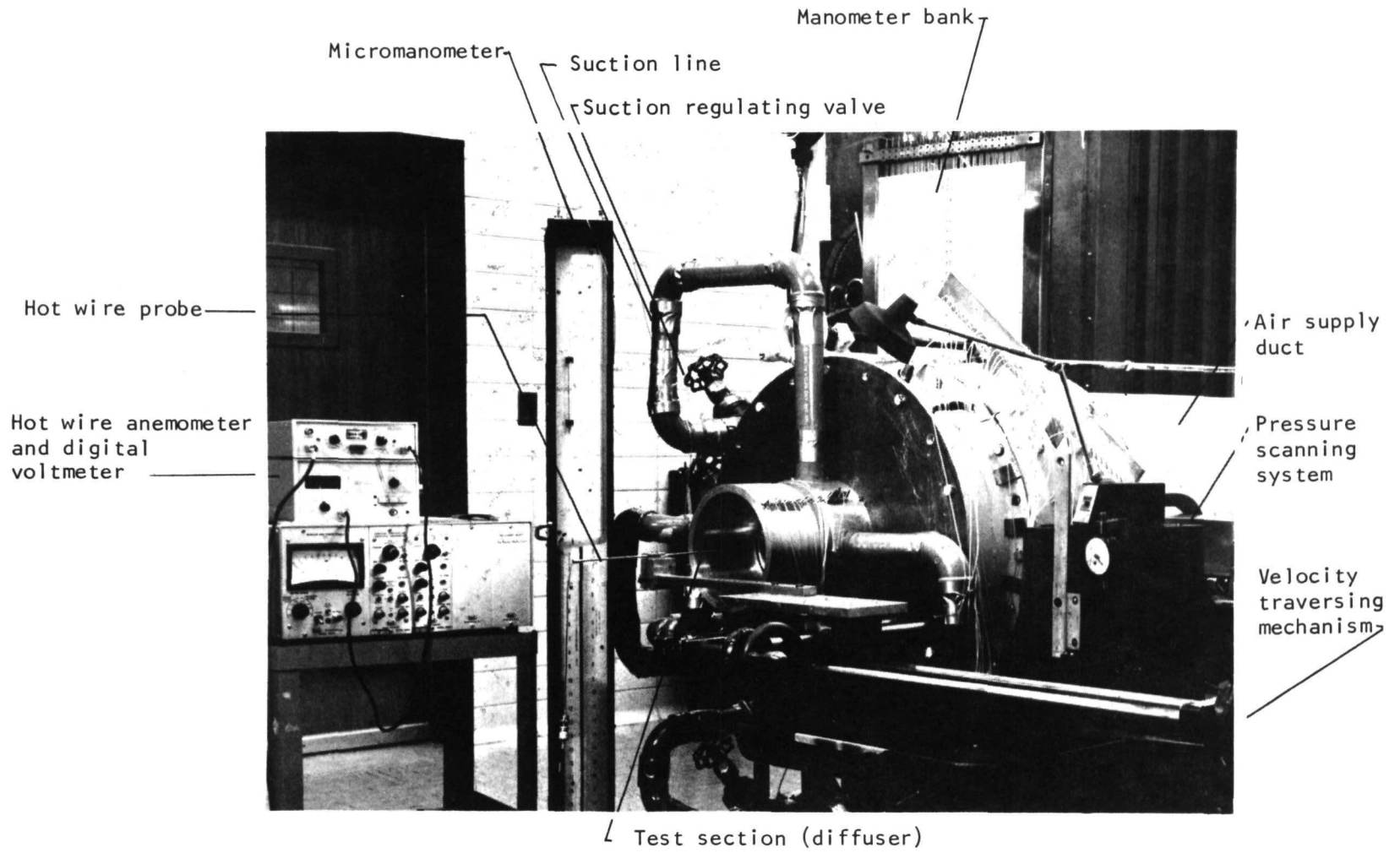


Figure 9. Bell shaped diffuser attached to the small air supply duct



## SECTION 4

### TEST CONDITIONS AND PROCEDURE

#### 4.1 Test Conditions

As reported in reference [1], the Griffith diffuser operates with either very high effectiveness (when unseparated flow exists) or very low effectiveness (when separated flow exists). The minimum suction rate required for unseparated flow is thus a very important diffuser characteristic.

Experimental work showed that two modes of operation with unseparated flow can exist. In the stable mode a flow disturbance may cause temporary flow separation, but unseparated flow will return when the disturbance is removed. In the metastable mode, unseparated flow persists even if a disturbance sufficient to cause separation is removed. Such factors as inlet velocity, area ratio, suction slot width, and diffuser downstream conditions have an effect upon the minimum suction required for both metastable and for stable unseparated flow:

An extensive set of tests were made to determine the minimum suction requirements for unseparated flow for each diffuser. Inlet air velocities were varied from 50 ft/sec (15.2 m/sec) to 280 ft/sec (85 m/sec). For the 9-inch (23 cm) annular diffuser, slot widths of 1/16-inch (0.159 cm) to 1/4-inch (0.635 cm) were used. For the 18-inch (46 cm) annular diffuser, slot widths of 1/8-inch (0.317 cm) to 1/2-inch (1.27 cm) were used. Area ratios of 2.5:1 and 3:1 were used.

The effect of downstream conditions was investigated in two ways.

(1) A perforated sheet metal plate with 51% free area was attached to

the diffuser exit plane of the 9-inch (23 cm) and of the 18-inch (46 cm) annular diffuser. The 18-inch (46 cm) diffuser plate had 5/8-inch (1.59 cm) holes while the 9-inch (23 cm) diffuser plate had 5/16-inch (.79 cm) holes.

- (2) The usual annular diffuser requires struts which may cause flow separation. Three struts located  $120^\circ$  apart were mounted in the downstream constant velocity zone of the 9-inch (23 cm) annular diffuser (AR = 2.5:1) to simulate this structural problem.

The effect of an unsteady inlet velocity was examined by installing a motor driven propeller just upstream of the inlet to the 9-inch (23 cm) diffuser. The effect upon suction requirements when driven at 500 RPM was examined.

In addition to tests made to determine minimum suction requirements, performance tests were made to determine diffuser effectiveness, total pressure loss, wall pressure distribution, exit plane velocity distribution, and center line velocity distribution for the four diffusers when operating with about 200 ft/sec (60 m/sec) inlet velocity and with a suction rate sufficient to maintain unseparated flow.

#### 4.2 Test Procedure

In determining the minimum suction requirement for stable operation, the pressure differential between the end of the supply duct and the end of the diffuser inlet section was observed in order to adjust the damper so as to give the desired inlet velocity. The suction blowers were started with the air bleed valve wide open and the slot suction valves nearly closed, thus having a deficiency of suction. The suction valves were slowly

opened while observing the venturi meter manometers so as to keep the proper ratio of outer wall to inner wall suction rate. This ratio was approximately the same as the slot length ratio. The air bleed valve was slowly closed so as to increase the suction capacity either simultaneously with or subsequent to the opening of the suction valves. Increasing the suction rate sufficiently would cause the flow to become unseparated, and this condition was considered to be the minimum for stable operation.

In determining the minimum suction requirement for metastable operation, the suction rate was decreased from the amount required for stable operation (or from any excess suction rate) until separation occurred. It was again necessary to observe the flow manometers as the suction rate was reduced so as to keep the suction rate per unit length of slot about the same on the inner and outer walls.

For tests involving performance characteristics such as effectiveness, velocity distribution, and wall pressure distribution, three static pressure measurements were made with the micromanometer: (1) at the end of the air supply duct (2) at the diffuser inlet (3) differential between (1) and (2). Flow meter manometers were read and recorded. Wall pressure readings were recorded on paper tape.

For velocity traverses, the reference position of the probe traversing mechanism was observed. Measurements were then made at the various desired stations by manipulating the traversing mechanism to the desired position and recording the hot-wire voltage.

## SECTION 5

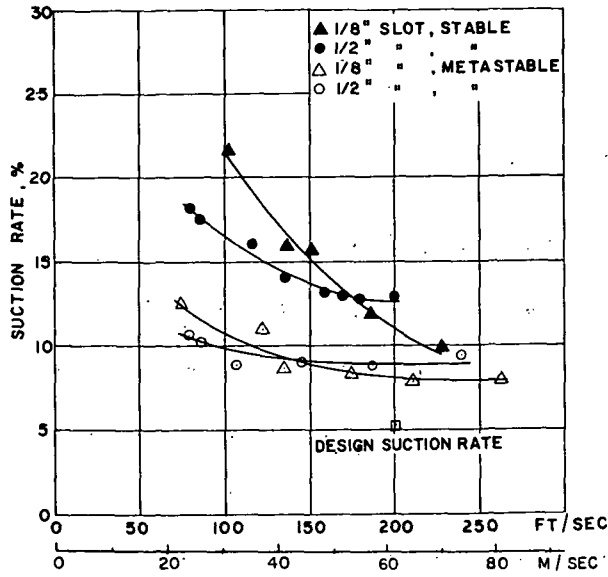
### DISCUSSION OF RESULTS

The results will be presented in the following arrangement. The minimum suction requirements for unseparated flow will be shown first. Then measured and predicted velocity distributions at the exit planes, the walls, and the passage centerlines will be shown. Further the effects of downstream blockage, of non-uniform inlet velocities, and of unsteady inlet velocity will be discussed. Finally a table of diffuser performance characteristics will be presented.

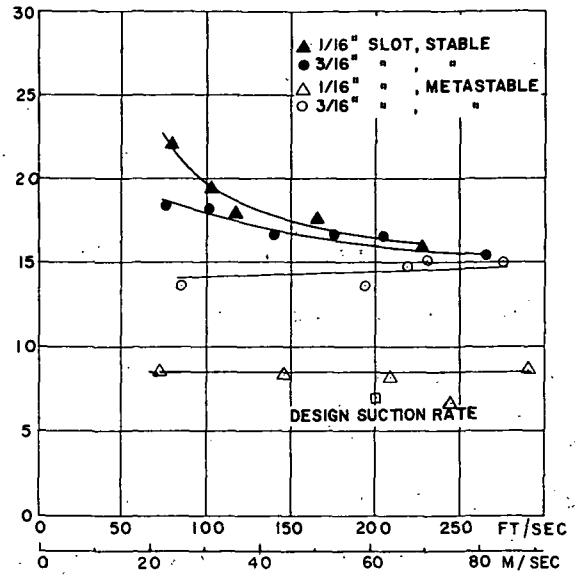
#### 5.1 Minimum Suction Requirement

Figure 10 shows the minimum suction requirements for unseparated flow through the four diffusers when approximately uniform inlet velocities exist. Both stable and metastable requirements are shown when operated with the design slot width (1/8-inch (.32 cm) for 18-inch (46 cm) diffuser, and 1/16-inch (.16 cm) for the other diffusers) and, for two of the diffusers, when operated with a slot width several times wider than the design width. A wider slot enables a given suction rate to be removed with a smaller pressure drop through the slot. In each case the design suction requirement is shown for an inlet velocity of 200 ft/sec (61 m/sec). The design suction was determined by assuming the one-seventh power law for the boundary layer velocity profile and applying Taylor's criterion [7]. This criterion gives an estimate of the amount of fluid which must be removed to prevent flow separation due to an unfavorable pressure gradient across the suction slot. The boundary layer fluid from the solid surface up to where the velocity ratio

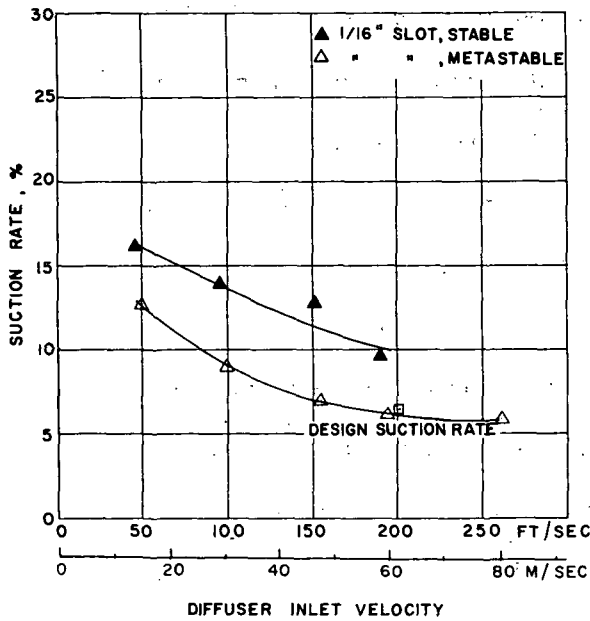
$$\frac{u}{U_1} = \sqrt{1.0 - \left(\frac{U_2}{U_1}\right)^2} \quad (23)$$



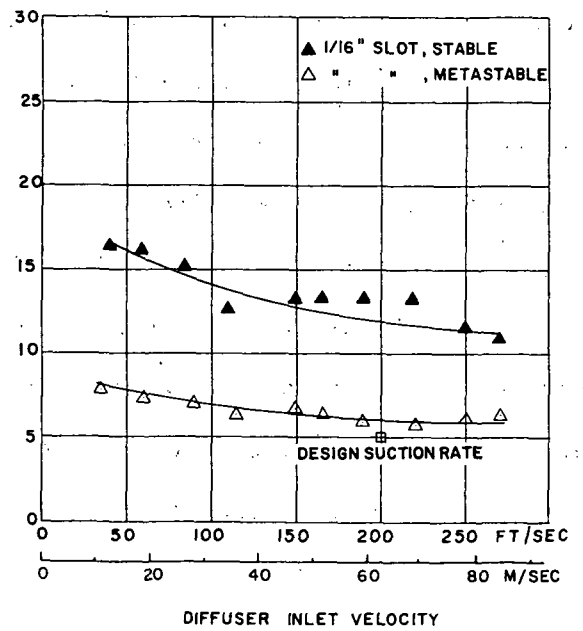
a. 1.8-INCH (46 cm) ANNULAR DIFFUSER AR=3:1



b. 9-INCH (23 cm) ANNULAR DIFFUSER AR=3:1



c. 9-INCH (23 cm) ANNULAR DIFFUSER AR=2.5:1



d. BELL SHAPED DIFFUSER AR=3:1

Figure 10. Minimum suction requirement for unseparated flow when using uniform inlet velocity.

exists must be removed according to Taylor's criterion.  $U_1$  and  $U_2$  are the velocities just upstream and downstream of the slot at the outer edge of the boundary layer, and  $u$  is the velocity within the boundary layer upstream of the slot along that streamline which ends in a stagnation point just downstream of the slot.

The results indicate that the design suction rate was very close to that required for metastable operation for the 9-inch (23 cm) annular diffuser (AR = 2.5:1). For the 9-inch (23 cm) annular (AR = 3:1) and for the bell shaped diffusers the design suction rate was slightly below that required for metastable operation. For the 18-inch (46 cm) diffuser, the design rate of 5% was 40% lower than the 7% actually required for metastable operation.

The suction rates required tended to drop asymptotically as the inlet velocities were increased. Since the boundary layer thickness tends to decrease with increased inlet velocities, this trend was expected.

The bell shaped diffuser required slightly smaller suction rates than the annular diffusers having the same area ratio because only one wall requires suction. Dropping the area ratio from 3:1 to 2.5:1 also reduced the suction requirement as expected.

The suction requirement for stable operation was of course above the metastable operation requirement but the differences tended to become less at higher inlet velocities and with wider slots. The wider slots also tended to make the suction requirement curves flatter or less dependent upon inlet velocities.

For inlet air velocities in the 200-250 ft/sec (61-76 m/sec) range, metastable operation required 6.5% suction for the bell shaped diffuser while stable operation required 12% suction. Corresponding suction rates for the 9-inch (23 cm)

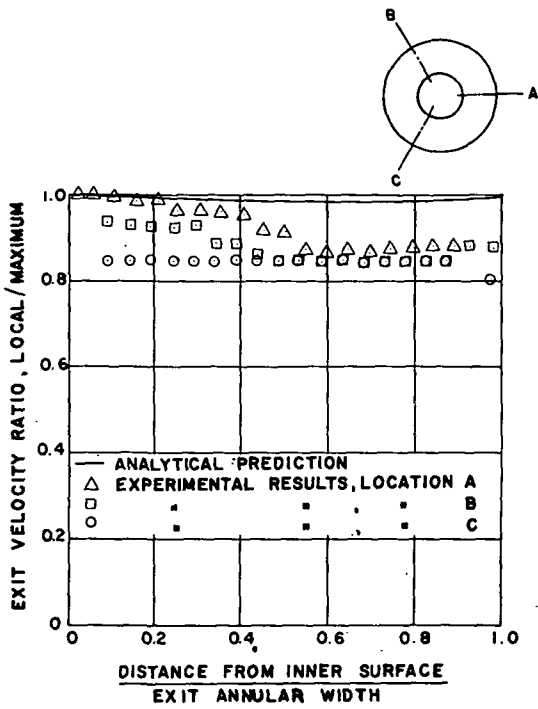
annular diffuser (3:1 AR) were 8.5% for metastable and 16.0% for stable operation. For the 9-inch (23 cm) annular diffuser with 2.5:1 area ratio, 6.3% and 12% suction rates were required, respectively for metastable and stable operation. For the most recently designed diffuser, the 18-inch (46 cm) annular (AR = 3:1), 7% suction was required for metastable operation and 10% for stable operation at an inlet velocity of 230 ft/sec (70 m/sec). For lower inlet velocities the suction rate increased as shown in figure 10a.

## 5.2 Velocity Distributions

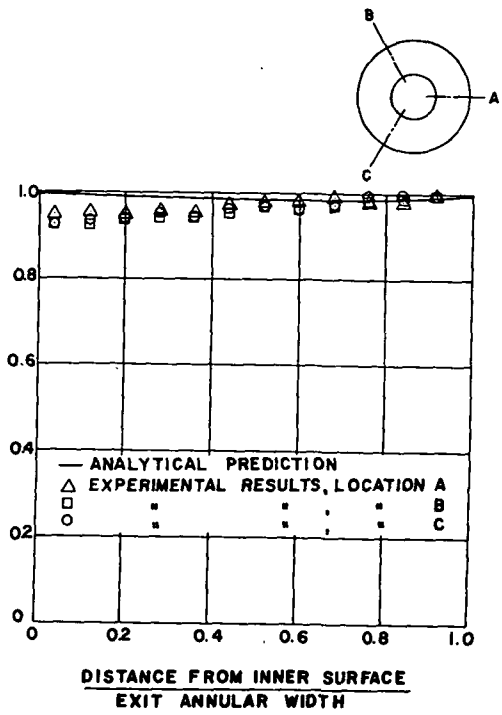
Figure 11 shows the exit plane velocity profiles for the four diffusers when an approximately uniform inlet velocity of 200 ft/sec (61 m/sec) is used and unseparated flow exists. Three sets of velocity measurements resulting from three circumferential locations 120° apart are shown for each diffuser. The velocity distribution predicted by the digital computer analysis program is also shown.

The dominant feature shown by this set of results is the virtually flat exit velocity profile of each of the four diffusers. For the bell shaped diffuser, the velocity ratio (local exit velocity/maximum exit velocity) was  $0.98 \pm 0.02$  over 95% of the exit area. For the 9-inch (23 cm) annular (AR = 3:1) the exit velocity ratio was  $0.96 \pm 0.04$  over 95% of the exit area. For the 9-inch (23 cm) annular (AR = 2.5:1) the exit velocity ratio was  $0.93 \pm 0.07$  over 95% of the exit area. For the 18-inch (46 cm) annular diffuser the exit velocity ratio was  $0.91 \pm 0.09$  over 95% of the exit area. The computer analysis program predicted a virtually flat exit velocity profile for each diffuser as shown.

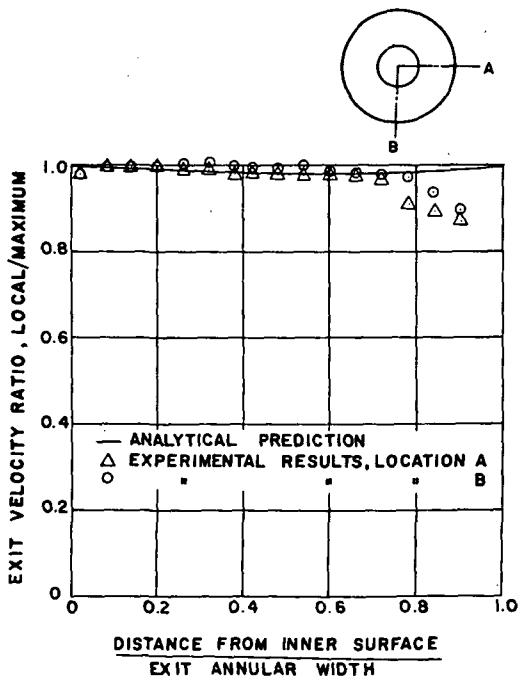
Figure 12 shows the "wall velocity" distribution for unseparated flow through the four diffusers when an approximately uniform inlet velocity of



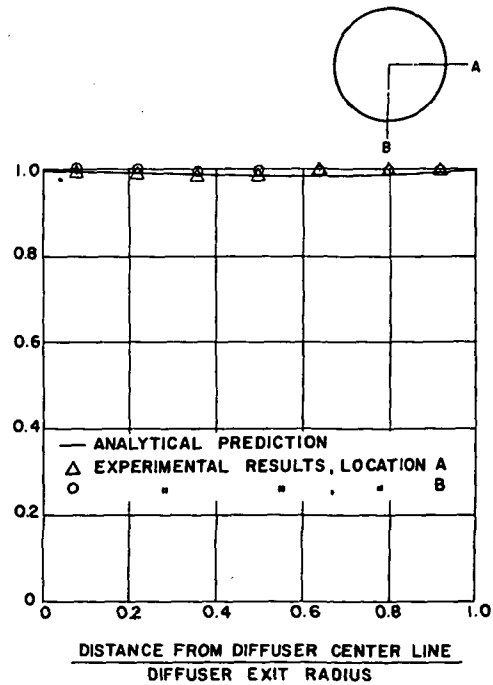
a. 18-INCH(46cm) ANNULAR DIFFUSER AR=3:1



b. 9-INCH(23 cm) ANNULAR DIFFUSER AR=3:1



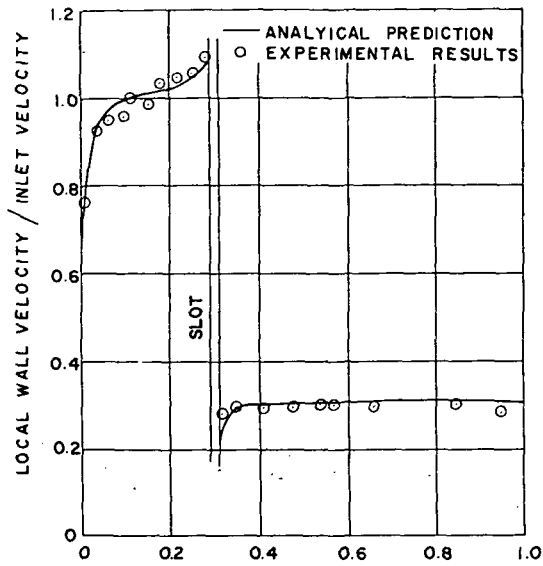
c. 9-INCH(23cm) ANNULAR DIFFUSER AR=25:1



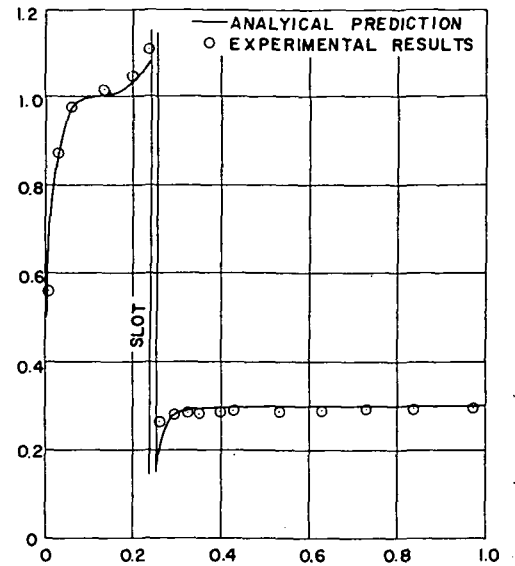
d. BELL SHAPED DIFFUSER AR=3:1

Figure 11. Exit plane velocity distribution for unseparated flow when using uniform inlet velocity.

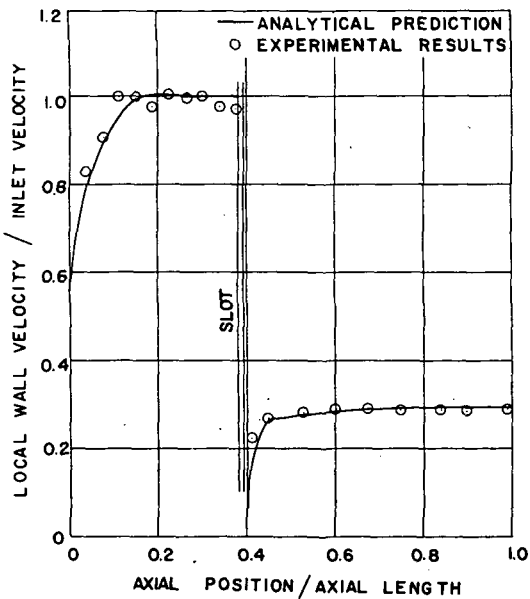




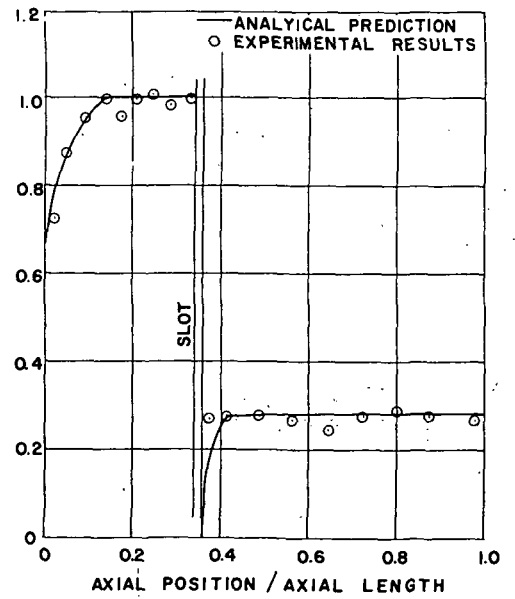
a. 18-INCH(46cm) ANNULAR DIFFUSER UPPER WALL AR=3:1



b. 18-INCH(46cm) ANNULAR DIFFUSER LOWER WALL AR=3:1

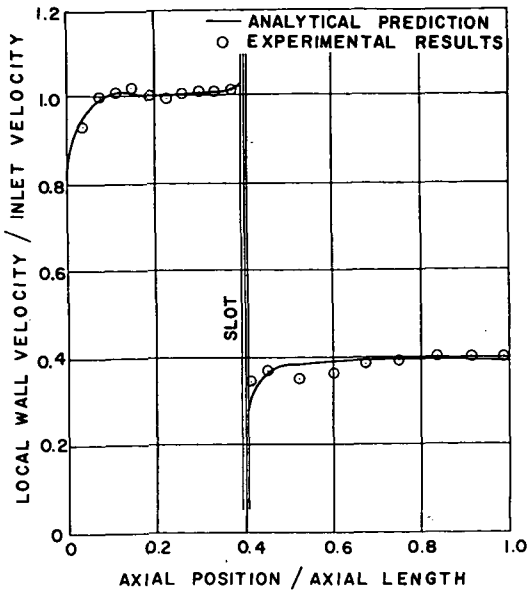


c. 9-INCH(23cm) ANNULAR DIFFUSER UPPER WALL AR=3:1

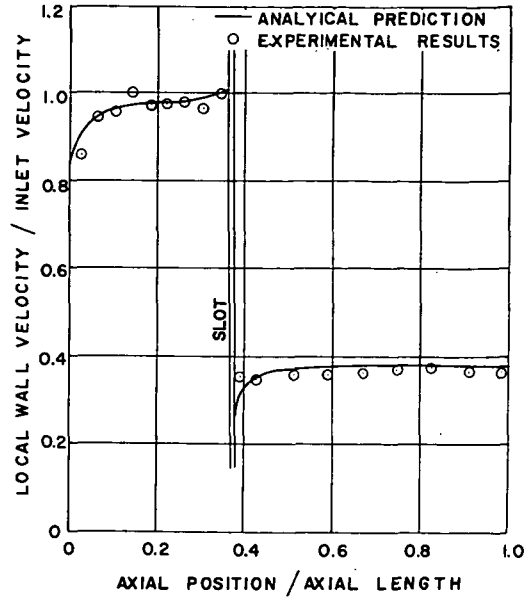


d. 9-INCH(23cm) ANNULAR DIFFUSER LOWER WALL AR=3:1

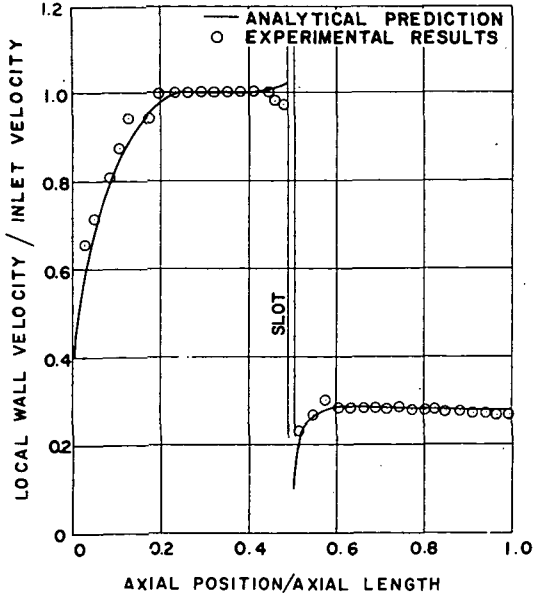
Figure 12. Wall velocity distribution for unseparated flow when using uniform inlet velocity.



e. 9-INCH(23 cm) ANNULAR DIFFUSER UPPER WALL AR=2.5:1



f. 9-INCH(23 cm) ANNULAR DIFFUSER LOWER WALL AR=2.5:1



g. BELL SHAPED DIFFUSER AR=3:1

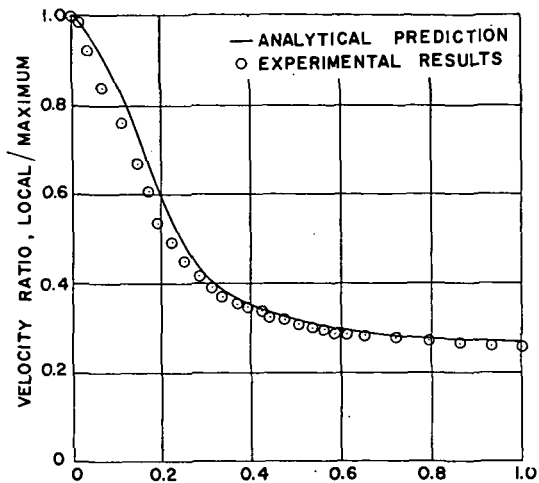
Figure 12 (continued). Wall velocity distribution for unseparated flow when using uniform inlet velocity.

200 ft/sec (61 m/sec) exists. The "wall velocities" were not measured directly but were computed from pressure coefficients obtained from wall pressure taps. Thus they are velocities near the wall just outside the boundary layer. For the three annular diffusers velocity distributions are shown for both the inner and the outer wall. The wall velocity distribution predicted by the computer analysis program is also shown for each diffuser. There is generally good agreement between the wall velocity distribution predicted and that determined from wall pressure measurements.

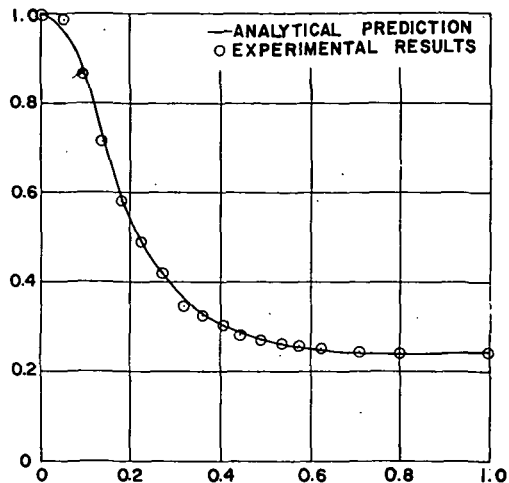
The "wall velocity" distributions show the design philosophy of the Griffith-type diffuser. There is virtually no deceleration along the diffuser walls and thus the "wall velocity" must change drastically at the slot.

One may note the difference between the "wall velocity" distribution and the "centerline velocity" distribution shown by Figure 13. The centerline profiles were determined from velocity measurements along a constant radius near the middle of the flow passage. The deceleration at the center of the flow passage is seen to occur over a significant part of the diffuser length in contrast with the wall deceleration. For the centerline profile the axial position was taken from the diffuser inlet (smallest cross-sectional area), while for the wall velocity profile, the axial length included the nozzle or accelerating portion of the inlet section.

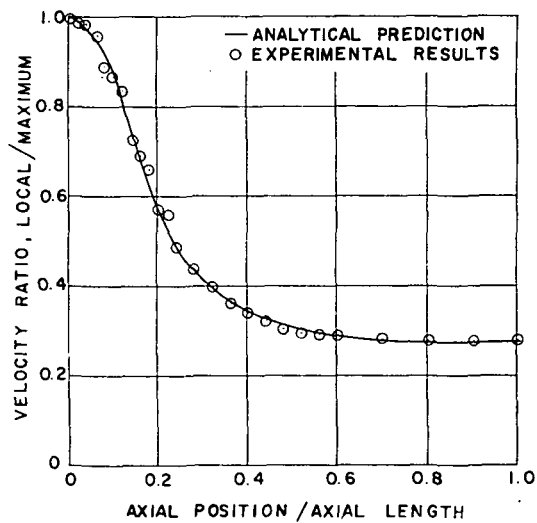
If the velocity distribution were precisely uniform at both the inlet and the exit planes, the velocity ratio along the passage centerline would drop from 1.0 at inlet to  $[(1.0 - FS/AR)]$  at exit. For example, for the 9-inch (23 cm) annular diffuser ( $AR = 3:1$ ) the velocity ratio would, with uniform inlet and exit velocity distribution, drop from 1.0 to  $(1.0 - 0.21)/3.0$  or 0.263 since 21% suction was applied. The measured velocity ratio dropped from 1.0 to 0.24. A suction rate higher than the minimum required for stable



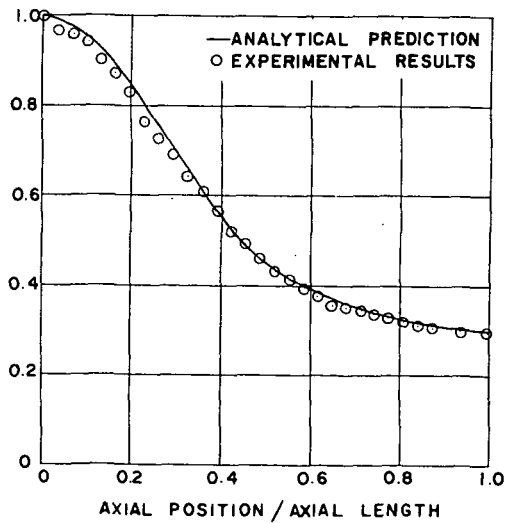
a. 18-INCH (46 cm) ANNULAR DIFFUSER AR=3:1



b. 9-INCH (23 cm) ANNULAR DIFFUSER AR=3:1



c. 9-INCH (23 cm) ANNULAR DIFFUSER AR=2.5:1



d. BELL SHAPED DIFFUSER AR=3:1

Figure 13. Axial velocity profile along a constant radius near the middle of the flow passage.

operation was used in order to minimize the fluctuation of the hot wire measurement caused by wakes shed from the stem of the probe.

### 5.3 Effect of Partial Blockage Downstream

Figure 14 shows the minimum suction requirement for unseparated flow through the 18-inch (46 cm) annular diffuser when a perforated sheet metal plate was attached to the diffuser exit plane. The plate had 5/16-inch (0.825 cm) diameter holes resulting in approximately 51% free area and simulated a partial blockage or obstruction downstream of the diffuser. There was a slight increase in the required suction rate at low inlet velocities when compared with no downstream obstruction. At inlet velocities above 150 ft/sec (46 m/sec) no significant effect was observed. The velocity distribution just upstream of the perforated plate was determined to be very similar to the exit plane velocity distribution when no downstream obstruction existed.

Three struts located 120° apart were mounted in the downstream section of the 9-inch (23 cm) (AR = 2.5:1) annular diffuser to simulate flow interference due to structural members. Figure 15 shows the exit plane circumferential velocity profile when this diffuser was operated with an approximately uniform inlet velocity of 200 ft/sec (61 m/sec). Approximately 10% suction was used to prevent flow separation. The velocity ratio drops to about 0.92 as the strut location is approached. This amount of variation was no more than the radial velocity variation when no struts were present. By taking advantage of the nearly constant velocity zone for the location of the struts, the problem of flow separation was avoided.

### 5.4 Effect of Non-Uniform Inlet Velocities

A series of tests were made to determine the effect of non-uniform diffuser inlet velocities on the 9-inch (23 cm) annular diffuser (AR = 2.5:1). Figure 16 shows the non-uniform duct discharge velocity profiles when a plate in the

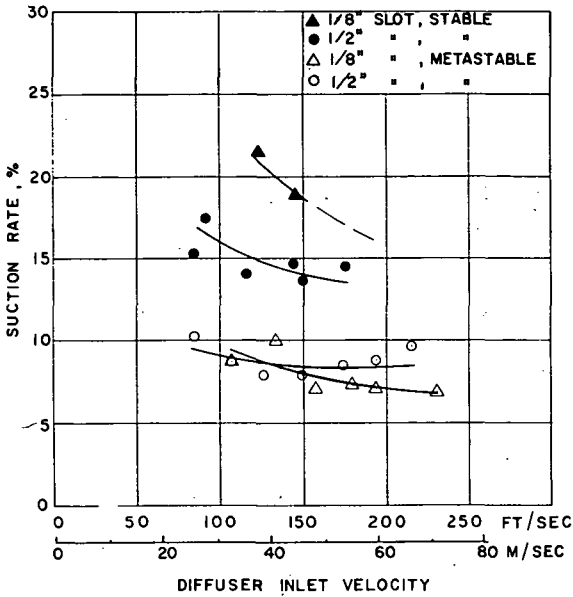


Figure 14. Minimum suction requirement for unseparated flow through 18-inch (46 cm) diffuser having a perforated metal plate at the exit plane.

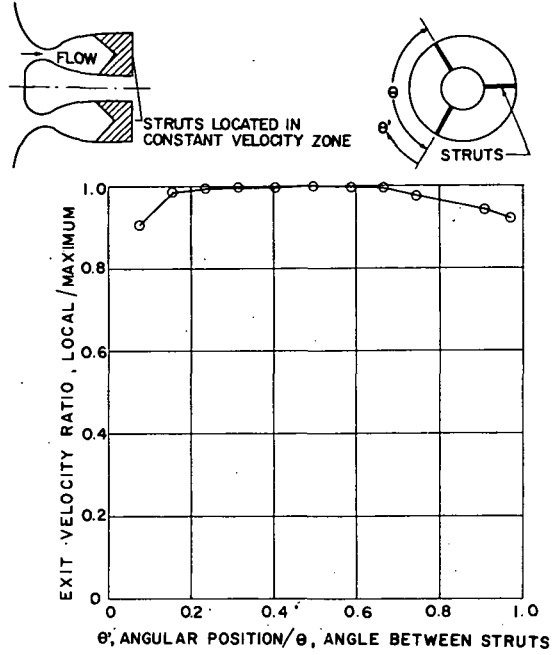


Figure 15. Exit plane circumferential velocity profile when three struts were mounted in the downstream section of the 9-inch (23 cm) (AR=2.5:1) diffuser.

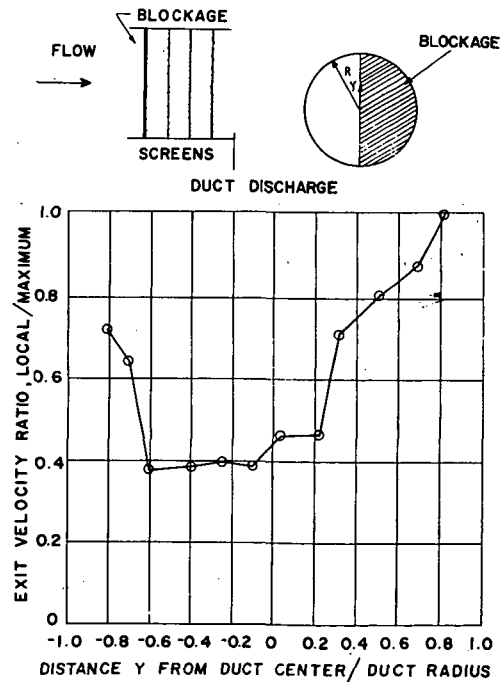
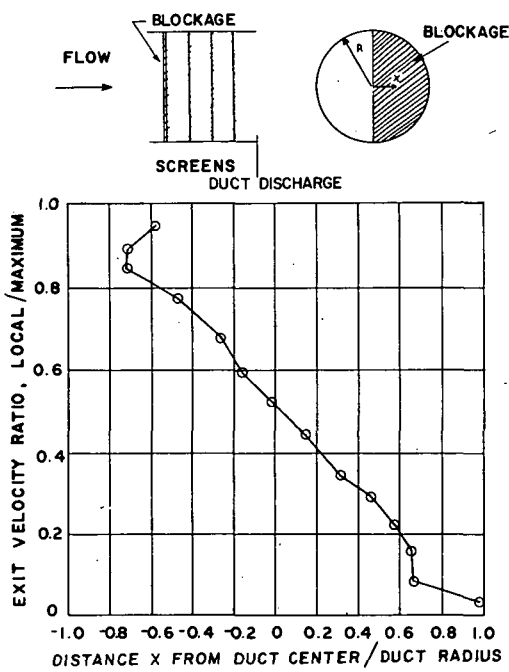


Figure 16. Duct discharge velocity profiles when partial blockage consisting of a semi-circular plate was installed.

shape of a half circle was mounted in the supply duct. These duct discharge velocity profiles were determined before the diffuser was attached to the end of the duct. Subsequent diffuser exit velocity measurements were made after installing the diffuser at the end of the partially blocked air duct. Figure 17 shows the resulting exit radial velocity distribution at two circumferential locations  $90^\circ$  apart. The velocity ratio variation was from a maximum near the inner wall to about 82% of maximum near the outer wall. This variation was only slightly more than when a uniform inlet velocity was used.

Figure 18 shows the non-uniform duct discharge velocity profile when a 14-inch (35 cm) circular plate was installed in the supply duct so as to yield a radially non-uniform duct discharge. Figure 19 shows the diffuser exit velocity profiles which were subsequently determined. As with the circumferential distortion, the diffuser exit radial velocity distribution was determined at two locations  $90^\circ$  apart. The velocity ratio variation was from a maximum near the inner wall to about 83% of maximum near the outer wall. The suction rates required for unseparated flow were approximately the same as with previous tests using uniform inlet velocities.

### 5.5 Effect of Unsteady Inlet Velocity

As previously mentioned, the effect of an unsteady inlet velocity was examined by installing a motor driven propeller which caused wakes to be shed upstream of the 9-inch (23 cm) annular diffuser inlet.

Figure 20 shows the minimum suction requirement for stable operation without and with the propeller. The shedding of wakes from the propeller caused an increase in the suction requirement, but the difference tends to become less as the inlet air velocity is increased. At 200 ft/sec (61 m/sec) the suction requirement for stable operation was increased from 16% to 18% by the propeller.

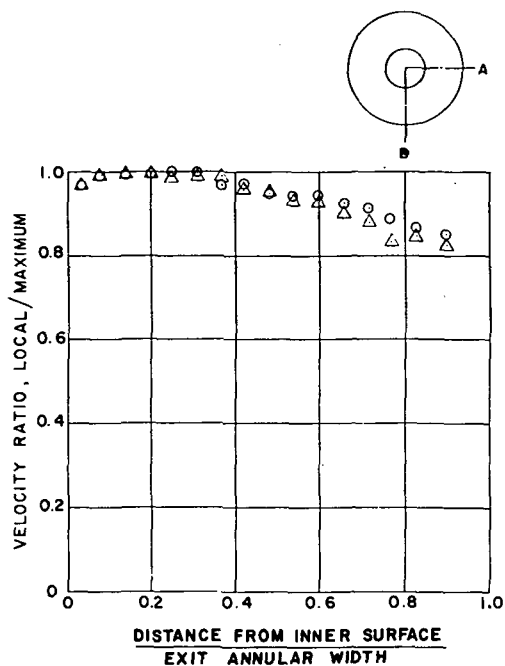


Figure 17. Exit radial velocity profiles of 9-inch (23 cm) diffuser (AR=2.5:1) when supply duct was partially blocked as shown by Fig. 16.

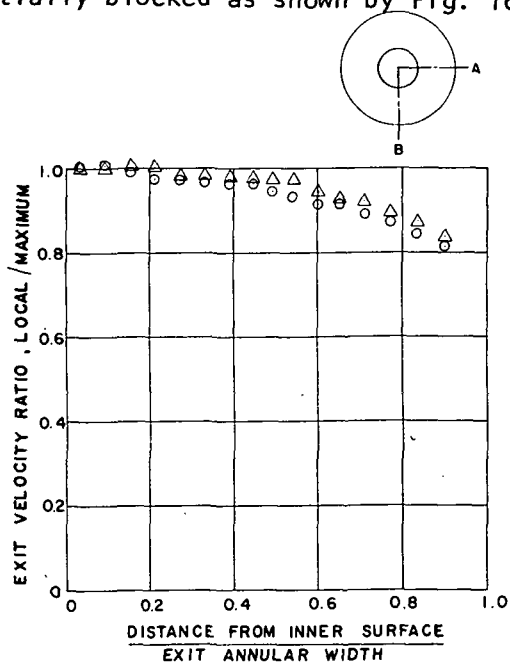


Figure 19. Exit radial velocity profile of 9-inch (23 cm) diffuser (AR=2.5:1) when supply duct was partially blocked as shown by Fig. 18.

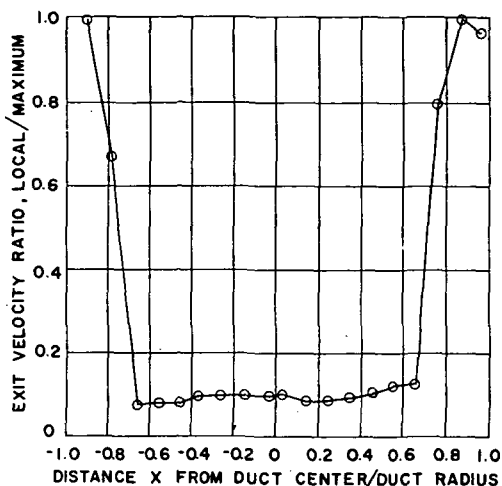
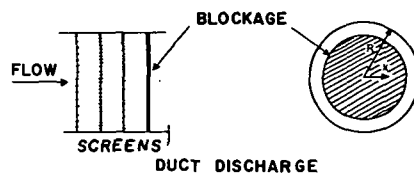


Figure 18. Duct discharge velocity profile when a circular plate was installed at center of duct passage.

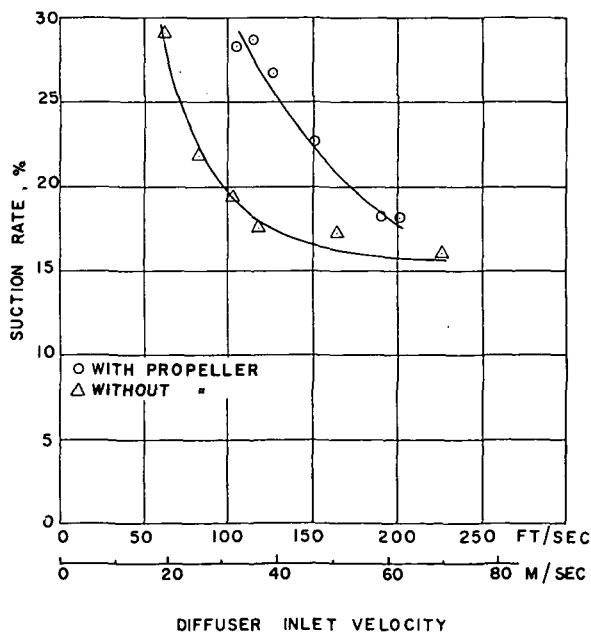


Figure 20. Minimum suction requirement for stable unseparated flow through 9-inch (23 cm) diffuser (AR=3:1) without and with a propeller.



## 5.6 Diffuser Performance

Tests were run to determine the effectiveness of the various Griffith diffusers. The effectiveness of the Griffith-type diffuser should be high when operated without flow separation because it is a very short diffuser and thus friction and turbulence losses should be very low. The price which must be paid is the suction loss, and for the effectiveness to have real meaning, this loss should be accounted for.

For this reason, this report will show both the conventional diffuser effectiveness,  $\eta$  (= actual pressure rise/ideal pressure rise) and a more meaningful effectiveness called  $\epsilon$ .  $\epsilon = (\text{flow rate out})(\text{actual pressure rise})/(\text{flow rate in})(\text{ideal pressure rise})$ . Appendix C derives the following expressions used in computing  $\eta$  and  $\epsilon$ .

$$\eta(\text{conventional}) = \frac{(P_{s,e} - P_{s,i})}{P_{d,i} \left[ \kappa_i - \kappa_e \left( \frac{1.0 - FS}{AR} \right)^2 \right]} \quad (24)$$

$$\epsilon(\text{modified}) = \frac{(1.0 - FS)(P_{s,e} - P_{s,i})}{P_{d,i} \left[ \kappa_i - \kappa_e \left( \frac{1.0 - FS}{AR} \right)^2 \right]} \quad (25)$$

where FS is the fraction removed by suction and  $\kappa$  is the kinetic energy coefficient to account for the non-uniformity of the flow at the diffuser inlet and exit planes. Typical values of  $\kappa_i$  and  $\kappa_e$  were 1.025 and 1.011 respectively.

The logic of modifying the conventional effectiveness by the ratio of the exit flow rate to the inlet flow rate becomes evident when one considers that the conventional definition represents a ratio of energy terms per unit mass flowing. When no suction or injection occurs, flow rates in and out cancel.

The total pressure loss (see Appendix C) was computed from

$$P_{t,i} - P_{t,e} = (1-\eta) P_{d,i} \left[ \kappa_i - \kappa_e \left( \frac{1.0 - FS}{AR} \right)^2 \right] \quad (26)$$

and non-dimensionalized to the inlet dynamic pressure  $P_{d,i}$ .

Table I shows the results of the performance tests which were made on the four diffusers. In the 150-250 ft/sec (46-76 m/sec) range of inlet velocities, the diffuser effectiveness values based on the conventional definition were from 97% to 99%. When slot suction was properly charged to the diffusers, the effectiveness values were about 86% for the 9-inch (23 cm) annular (AR = 3:1), 88% for the 9-inch (23 cm) annular (AR = 2.5:1), 89% for the 18-inch (46 cm) annular, and 91% for the bell shaped diffuser. A typical total pressure loss was 2% of the inlet dynamic pressure. Fluctuations from this value were probably due more to slight pressure measurement errors than to actual changes in the total pressure loss.

TABLE 1. GRIFFITH DIFFUSER PERFORMANCE

Test No.	Inlet Velocity		Inlet Reynolds Number	Slot Suction %	Pressure Recovery Coefficient $C_p$	Effectiveness		Total Pressure Loss, % of Inlet Dynamic (Eq. 26)
	Ft./Sec	M/Sec				$\epsilon\%$ (Eq. 25)	$\eta(\%)$ (Eq. 24)	
A. Bell Shaped Diffuser; AR=3:1; Slot Width = 1/16 in. (.159 cm)								
1	82	25	$4.2 \times 10^4$	7.3	0.92	91.5	98.8	1.1
2	145	44	$7.4 \times 10^4$	6.2	0.92	93.6	99.0	0.9
3	235	72	$12.0 \times 10^4$	6.3	0.91	92.0	98.2	1.7
B. 9 in. (23 cm) Annular Diffuser; AR=3:1; Slot Width = 1/16 in. (.159 cm)								
4	79	24	$2.0 \times 10^4$	16.6	0.90	81.3	95.2	4.5
5	142	43	$3.6 \times 10^4$	12.3	0.91	85.5	97.5	2.3
6	236	72	$6.0 \times 10^4$	11.2	0.91	86.5	97.5	2.3
C. 9 in. (23 cm) Annular Diffuser; AR=2.5:1; Slot Width = 1/16 in. (.159 cm)								
7	82	25	$2.8 \times 10^4$	12.8	0.89	86.1	98.8	1.1
8	147	45	$5.0 \times 10^4$	11.0	0.87	86.6	97.4	2.2
9	237	72	$8.0 \times 10^4$	9.5	0.88	89.5	99.0	0.9
D. 18 in. (46 cm) Annular Diffuser; AR=3:1; Slot Width = 1/2 in. (1.27 cm)								
10	84	26	$4.3 \times 10^4$	10.3	0.90	86.7	96.7	3.1
11	144	44	$7.3 \times 10^4$	8.3	0.92	90.9	99.0	0.9
12	229	70	$11.7 \times 10^4$	10.8	0.93	88.5	99.0	0.9

## SECTION 6 CONCLUSIONS

The following conclusions were reached based upon the results of the research program.

- (1) The concept of the Griffith diffuser is a reasonable approach to designing short axially symmetrical diffusers for special applications.
- (2) The potential flow design program utilizing the two dimensional wedge flow patch to approximate the branch flow from the suction slot yields a workable curved wall diffuser. This is not to rule out the possibility of improvement by using a more sophisticated design program such as an improved branch flow patch and the accounting for boundary layer displacement thickness.
- (3) Reasonably good agreement was achieved among the velocity distributions prescribed to the design program, predicted by the analysis program, and determined experimentally.
- (4) The slot suction rate required to prevent separation with stable flow was found to decrease asymptotically with diffuser inlet velocity and radial dimensions. Thus the minimum suction rate was about 10% at 230 fps (69 m/sec) for the largest diffuser tested.
- (5) High performance can be expected from the Griffith diffuser when sufficient suction is used to prevent flow separation. An effectiveness of 88% is a typical value if slot suction is accounted for.
- (6) A reasonably uniform exit velocity profile results from the Griffith type diffuser when sufficient suction to prevent flow separation is used.

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7. Goldstein, Sydney, "Low Drag and Suction Airfoils," Journal of Aeronautical Sciences, Vol. 15, No. 4, April, 1948.

## APPENDIX A - PROGRAM DESCRIPTION AND LISTING

The main program is the controller for the program. It calls each of the subroutines as needed, and it contains the main loop for the iteration of the radial coordinates.

SETUP is a subroutine which computes coefficients which are needed to perform Simpson's Rule integration.

SIMP is a subroutine for integration using Simpson's Rule.

PART I is a subroutine which reads in, checks, and outputs the input data. Obvious errors in input data terminates the program after error explanation is printed. Certain constants to control subsequent calculations are computed and initialization of arrays Q and R are also performed in PART I.

COEF is a subroutine which computes constants used in the solution for the velocity distribution.

RELAX is a subroutine which uses the Gauss-Siedel Technique with overrelaxation to solve for  $\ln Q$  over the region. Where derivatives of the velocity are prescribed as zero, this subroutine corrects those boundary conditions accordingly.

PART II is a subroutine which performs the inverse transformation to get the flow angles,  $\alpha$ , the R coordinates, and finally the X coordinates if the iteration on R is on its last pass. This subroutine also corrects the boundary conditions on R where required. The integration is carried out first along the middle streamline and then along each potential line individually.

OUTPUT is a subroutine which prints out the R array upon request during the iteration on R. At the completion of all computations, it outputs the Q, R, X, and  $\alpha$  arrays and a summary of the wall coordinates of the finished channel design.

GRAPHIC is a subroutine which plots out the streamlines and equipotential lines for the final channel design. Inlet and outlet channel velocity profiles are optionally output.

#### INPUT DATA PREPARATION INSTRUCTIONS

The following is a description of the input data, their meanings, and how they must appear on the data cards.

#### Control Data

##### CARD 1

<u>Column</u>	<u>Variable</u>	<u>Description</u>
1	FLAG1	FLAG1 is the input flag for the plane flow case. FLAG1 = 0 for axially symmetric flow. FLAG1 = 1 for plane flow.
2	FLAG2	FLAG2 is the boundary condition flag. FLAG2 = 0: Dirichlet B.C. are used on the inlet and outlet potential lines and the velocities are set equal to the first and last wall velocities input respectively. FLAG2 = 1: Neumann B.C. are used on the inlet and outlet potential lines. FLAG2 = 2: Dirichlet B.C. are used on the inlet potential line with the velocities being input there and Neumann B.C. are used on the outlet potential line. FLAG2 = 3: Neumann B.C. are used on the inlet potential line and Dirichlet B.C. are used on the outlet potential line with the velocities being input there. FLAG2 = 4: Dirichlet B.C. are used on the inlet and outlet potential lines with the velocities being input on both.
3	FLAG3	FLAG3 is the bell diffuser flag. FLAG3 = 0 if the diffuser is plane or annular. FLAG3 = 1 if the diffuser is a bell diffuser.
4	FLAG4	FLAG4 is the graphical output flag. FLAG4 = 0 if no graphical output is desired. FLAG4 = 1 if graphical output is desired.

<u>Column</u>	<u>Variable</u>	<u>Description</u>
7-66	HEDR	HEDR is a 60 character comment that will be printed out at the top of each page of output.
69-70	DATE1	DATE1 is the two digit number giving the month of the date.
71-72	DATE2	DATE2 is the two digit number giving the day of the date.
73-74	DATE3	DATE3 is the two digit number giving the year of the date.
77-80	CASE	CASE is a four digit case number that will be printed out at the top of each page of output.

CARD 2

<u>Column</u>	<u>Variable</u>	<u>Description</u>
1-10	RMULT	RMULT is a constant by which all computed X and Y coordinates will be multiplied at the completion of the program. If RMULT = 0.0 no multiplication will take place.
11-20	W	W is the relaxation factor. Although the optimum value varies with the grid size, a value of 1.9 has been found to work well in planar cases, 1.9 in bell cases, and 1.7 in annular cases.
21-30	TOLSYS	TOLSYS is the accuracy to which the radial coordinates are to be computed. This accuracy is determined as the largest change of any radial coordinate from the previous iteration.
31-40	TOLDE	TOLDE is the accuracy to which the velocity is to be computed. This accuracy is determined as the largest change of any velocity from the previous iteration.
41-50	MSTAGU	This is the number of the nodal point in the $\phi$ direction at which the upper stagnation point (slot downstream lip) is to be located.
51-60	MSTAGL	This is the number of the nodal point in the $\phi$ direction at which the lower stagnation point is to be located. For plane and bell designs this item is not used.

CARD 3

<u>Column</u>	<u>Variable</u>	<u>Description</u>
1-10	M	The number of mesh points to be used in the $\phi$ direction (The maximum number 148.)



<u>Column</u>	<u>Variable</u>	<u>Description</u>
11-20	N	The number of mesh points to be used in the $\psi$ direction. (The maximum number is 48.)
21-30	MXISYS	The maximum number of iterations allowed to find the radial coordinates. If FLAG1 = 1 then MXISYS = 1. MXISYS = 10 gives good results for annular and bell diffusers.
31-40	MXIDE	The maximum number of iterations allowed to find the velocities; 300-400 usually gives good results for the 2-D case and 50 gives good results for the axially symmetric case.
41-50	NSTAGU	This is the number of nodal points in the $\psi$ direction at which the upper stagnation point (slot downstream lip) is located. N-NSTAGU cannot be less than 3.
51-60	NSTAGL	This is the number of nodal points in the $\psi$ direction at which the lower stagnation point is located. For plane and bell designs this item is not used. NSTAGL cannot be less than 4.

CARD 4

<u>Column</u>	<u>Variable</u>	<u>Description</u>
1-10	RADIN	RADIN is the radial coordinate at the nodal point numbered (1,1) for annular design. If left blank its value is assumed to be 1.0. This item is not used in plane or bell designs.
11-20	MIDJ	The number of the streamline for an annular diffuser. Usually chosen as N/2. Care should be exercised in the choice of MIDJ since an improper choice can cause an annular design to cross the X axis. This results in a divide check, overflow or underflow and a consequent termination of the program. This item is only used for annular designs.
21-30	IPRSYS	The frequency at which intermediate values of the coordinates of the diffuser are printed out during iteration on R. If no intermediate values are desired, make IPRSYS greater than MXIDE.
31-40	IPRDE	The frequency at which intermediate values of the velocity are printed out.
41-50	MSLOTU	The number of the potential line at the bottom of the upper slot. This number is usually only slightly larger than NSTAGU.
51-60	MSLOTL	The number of the potential line at the bottom of the lower slot. This item is only used for annular designs.

## Spacing and Boundary Conditions

The following variables are input six to a card in columns 1-10, 11-20, etc.

<u>Variable</u>	<u>Description</u>
PHI	The values of the velocity potential along a streamline at each nodal point. There should be M values.
Q ( $\phi, \psi_1$ ) upstream	The values of the velocity along the upper wall upstream of and along the upstream wall inside of the slot. There should be MSLOTU of these values.
Q ( $\phi, \psi_2$ ) downstream	The values of the velocity along the upper wall downstream of the slot. There should be M-MSTAGU of these values.
QSLOTU ( $\phi$ )	The values of the velocity along the downstream wall inside of the slot. There should be MSLOTU-MSTAGU of these values.
Q ( $\phi, 0$ ) upstream	The values of the velocity along the lower wall upstream of and along the upstream wall inside of the slot. There should be MSLOTL of these values. Omit for plane and bell designs.
Q ( $\phi, \psi_3$ ) downstream	The values of the velocity along the lower wall downstream of the slot. There should be M-MSTAGL of these values. Omit for plane and bell designs.
QSLOTL ( $\phi$ )	The values of the velocity along the downstream wall inside of the slot. There should be MSLOTL-MSTAGL of these values. Omit for plane and bell designs.
PSI	The values of the stream function along a potential line at each nodal point. There should be N values.
Q (0, $\psi$ )	The value of the velocity at nodal points along the inlet potential line. There should be N values. Values are input only if FLAG2 = 2 or 4.
Q ( $\phi, \psi$ )	The values of the velocity at nodal points along the outlet potential line. There should be NSTAGU values for plane and bell designs and NSTAGU-NSTAGL + 1 values for annular designs. Values are input only if FLAG2 = 3 or 4.

## OUTPUT EXPLANATION

On the first page of output the control data is printed out and the options called for by the control data are listed. Following the printout of the control data comes a printout of the wall boundary conditions and spacing in the  $\phi$  direction. The wall boundary conditions are given in three parts: the inlet wall data, the downstream wall data and data inside the slot. The first column of each set of data gives the arc length,  $S$ , computed along the wall streamline. The second column labeled  $Q$  gives the velocity that is input along the wall streamline. The third column labeled PHI gives the values of  $\phi$  as input. The fourth column labeled DPHI gives  $\Delta\phi$ , the spacing as computed by subtracting adjacent values of  $\phi$ . For annular designs three more sets of wall boundary conditions are output for the diffuser lower wall.

Following the wall streamline boundary conditions the stream function distribution is printed out along with the spacing computed from it. The numbers to the left of these outputs give the number of the node to which the information corresponds.

Following the input data comes a list of the convergence variables ITER, JTER, EPS and DEL for each iteration on R (these are printed out for the axially symmetric case only). ITER is the number of the iteration on R that was then in progress. JTER is the number of iterations on the velocity that have been completed. EPS is the accuracy to which R has been computed. DEL is the accuracy of solution of the  $\ln Q$  equation.

The arrays of  $Q$ ,  $R$ ,  $X$  and ALPHA are output after the last iteration. The arrays QSLOTU, QSLOTL, RSLOTU, RSLOTL, XSLOTU, XSLOTL, ASLOTU, and ASLOTL, the values of the corresponding variables inside the slot on the downstream

wall, are also output. The values of ITER, JTER, EPS and DEL are output in the heading of each array.

A summary of the wall coordinates is output last along with the velocity that was prescribed along the wall, the arc length computed along the wall and the tangent angle along the wall. This output is presented in three parts as was the input data along the walls. For annular channels another set of output is presented for a lower wall.

The following 45 pages is a program listing for the design program.

C	*****	MAIN PROGRAM	*****	MAIN	1
C				MAIN	2
C		CLEMSON UNIVERSITY MECHANICAL ENGINEERING DEPARTMENT		MAIN	3
C				MAIN	4
C		PROGRAM 70-02		MAIN	5
C				MAIN	6
C		AXIALLY SYMMETRIC AND 2-D BRANCHED FLOW CHANNEL DESIGN		MAIN	7
C				MAIN	8
		DIMENSION DX(150),ESIMP(150),FSIMP(150),GSIMP(150),		MAIN	9
1		GRAND(150),GIFT(150),PHI(150),PSI(150),		MAIN	10
2		DPSI(150),DPHI(150),S(150),SBAR(150),S1(150),		MAIN	11
3		SBAR1(150),S2(150),SBAR2(150),HEDR(15),		MAIN	12
4		FPHI(150),FPHI(150),GPHI(150),EPSI(150),		MAIN	13
5		FPSI(150),GPSI(150),RSLOTU(150),RSLOTL(150),		MAIN	14
6		QSLOTU(150),QSLOTL(150),ASLOTU(150),		MAIN	15
7		ASLOTL(150),XSLOTU(150),XSLOTL(150)		MAIN	16
		DOUBLE PRECISION P		MAIN	17
		INTEGER FLAG1,FLAG2,FLAG3,FLAG4,CASE,DATE1,DATE2,DATE3		MAIN	18
		COMMON / C1 / IMINSU,IMAXSU,IMINSI,IMAXSI,GRAND,GIFT,		MAIN	19
1		DX,ESIMP,FSIMP,GSIMP		MAIN	20
		COMMON / C2 / FLAG1,FLAG2,FLAG3,FLAG4,HEDR,DATE1,DATE2,		MAIN	21
1		DATE3,CASE,MXIDE,ICKDE,IPRDE,IMIN,IMAX,		MAIN	22
2		JMIN,JMAX,NUT,M,N,TOLDE,DEL,EPS,JTER,		MAIN	23
3		ITER,DPHI,DPSI,S,SBAR,RMULT,S1,S2,SBAR1,		MAIN	24
4		SBAR2,MSTAGU,NSTAGU,MSLOTU,MSTAGL,NSTAGL,		MAIN	25
5		MSLOTL,RADIN,W,PHI,PSI,RSLOTU,RSLOTL,		MAIN	26
6		QSLOTU,QSLOTL,ASLOTU,ASLOTL,XSLOTU,		MAIN	27
7		XSLOTL,G,MIDJ,TOLSYS		MAIN	28
		COMMON / C3 / EPHI,FPHI,GPHI,EPSI,FPSI,GPSI,MXISYS,		MAIN	29
1		IPRSYS		MAIN	30
		CALL PART1		MAIN	31
		II = 1		MAIN	32
		DO 100 ITER=1,MXISYS		MAIN	33
		CALL COEF		MAIN	34
		CALL RELAX		MAIN	35
		CALL PART2		MAIN	36
		IF (EPS .LE. TOLSYS) GO TO 200		MAIN	37
		IF (ITER .LT. II*IPRSYS) GO TO 100		MAIN	38
		NUT = 1		MAIN	39
		II = II + 1		MAIN	40
		CALL OUTPUT		MAIN	41
100		CONTINUE		MAIN	42
200		NUT = 0		MAIN	43
		CALL OUTPUT		MAIN	44
		IF (FLAG4 .LE. 0) STOP		MAIN	45
		CALL GRAPIC		MAIN	46
		END		MAIN	47
C	*****	SUBROUTINE SETUP	*****	SET	1
C				SET	2
C		COMPUTES COEFFICIENTS FOR USE IN SIMPSON RULE		SET	3
C		INTEGRATION		SET	4
C				SET	5
		SUBROUTINE SETUP		SET	6
		DIMENSION DX(150),ESIMP(150),FSIMP(150),GSIMP(150),		SET	7
1		GRAND(150),GIFT(150)		SET	8
		COMMON / C1 / IMINSU,IMAXSU,IMINSI,IMAXSI,GRAND,GIFT,		SET	9
1		DX,ESIMP,FSIMP,GSIMP		SET	10
		DO 1000 I=IMINSU,IMAXSU		SET	11
		DX1 = DX(I)		SET	12
		DX2 = DX(I+1)		SET	13

	DX1Q = DX1 * DX1 * DX1	SET	14
	DX1SQ = DX1 * DX1	SET	15
	DX2Q = DX2 * DX2 * DX2	SET	16
	DX2SQ = DX2 * DX2	SET	17
	XNUM = 2. * DX1Q + 3. * DX1SQ * DX2 - DX2Q	SET	18
	DEN = 6. * DX1 * ( DX2 + DX1 )	SET	19
	ESIMP(I) = XNUM / DEN	SET	20
	XNUM = DX2Q + DX1Q + 3. * DX2SQ * DX1 + 3. * DX1SQ * DX2	SET	21
	DEN = 6. * DX1 * DX2	SET	22
	FSIMP(I) = XNUM / DEN	SET	23
	XNUM = 2. * DX2Q + 3. * DX2SQ * DX1 - DX1Q	SET	24
	DEN = 6. * DX2 * ( DX2 + DX1 )	SET	25
1000	GSIMP(I) = XNUM / DEN	SET	26
	RETURN	SET	27
	END	SET	28
****			
SIMP			
C	***** SUBROUTINE SIMP *****	SIMP	1
C		SIMP	2
C	THIS SUBROUTINE DOES SIMPSON'S RULE INTEGRATION	SIMP	3
C	OF A FUNCTION, AND RETURNS THE INTEGRATED FUNCTION	SIMP	4
C		SIMP	5
	SUBROUTINE SIMP	SIMP	6
	DIMENSION DX(150),ESIMP(150),FSIMP(150),GSIMP(150),	SIMP	7
1	GRAND(150),GIFT(150)	SIMP	8
	COMMON / C1 / IMINSU,IMAXSU,IMINSI,IMAXSI,GRAND,GIFT,	SIMP	9
1	DX,ESIMP,FSIMP,GSIMP	SIMP	10
	GIFT(IMINSI) = 0.0	SIMP	11
	II = IMINSI + 2	SIMP	12
C		SIMP	13
C	COMPUTE MAIN INTEGRAL	SIMP	14
C		SIMP	15
	DO 1000 I=II,IMAXSI,2	SIMP	16
	III = I	SIMP	17
	SUM = GIFT(I-2) + ESIMP(I-2) * GRAND(I-2)	SIMP	18
	SUM = SUM + FSIMP(I-2) * GRAND(I-1)	SIMP	19
	SUM = SUM + GSIMP(I-2) * GRAND(I)	SIMP	20
1000	GIFT(I) = SUM	SIMP	21
C		SIMP	22
C	COMPUTE INTERMEDIATE VALUES	SIMP	23
C		SIMP	24
	IUP = IMAXSI	SIMP	25
	IF (IMAXSI - III .EQ. 1) IUP = IMAXSI - 2	SIMP	26
	II = IMINSI + 1	SIMP	27
	DO 2000 I=II,IUP,2	SIMP	28
	D1 = DX(I-1)	SIMP	29
	D2 = DX(I)	SIMP	30
	GIFT(I) = D1 * ( 2. * D1 + 3. * D2 ) * GRAND(I-1) /	SIMP	31
	1( 6. * D2 + 6. * D1 )	SIMP	32
	GIFT(I) = GIFT(I) + D1 * ( D1 + 3. * D2 ) * GRAND(I) /	SIMP	33
	1( 6. * D2 )	SIMP	34
2000	GIFT(I) = GIFT(I) - D1 * D1 * D1 * GRAND(I+1) /	SIMP	35
	1( 6. * D2 * D2 + 6. * D2 * D1 ) + GIFT(I-1)	SIMP	36
	IF (IMAXSI - III .EQ. 0) RETURN	SIMP	37
	I = IMAXSI	SIMP	38
	GIFT(I) = ( GRAND(I-1) + GRAND(I) ) * DX(I-1) / 2. + GIFT(I-1)	SIMP	39
	RETURN	SIMP	40
	END	SIMP	41
C	***** SUBROUTINE PART1 *****	PAR1	1
C		PAR1	2
C	THIS SUBROUTINE READS INPUT DATA AND PREPARES	PAR1	3
C	ARRAYS FOR RELAXATION	PAR1	4

		PAR1	5
	SUBROUTINE PART1	PAR1	6
	DIMENSION DX(150),ESIMP(150),FSIMP(150),GSIMP(150),	PAR1	7
1	GRAND(150),GIFT(150),PHI(150),PSI(150),	PAR1	8
2	DPSI(150),DPHI(150),S(150),SBAR(150),S1(150),	PAR1	9
3	SBAR1(150),S2(150),SBAR2(150),HEDR(15),	PAR1	10
4	EPHI(150),FPHI(150),GPHI(150),EPSI(150),	PAR1	11
5	FPSI(150),GPSI(150),RSLOTU(150),RSLOTL(150),	PAR1	12
6	QSLOTU(150),QSLOTL(150),ASLOTU(150),	PAR1	13
7	ASLOTL(150),XSLOTU(150),XSLOTL(150)	PAR1	14
	DIMENSION Q(150,50),R(150,50),X(150,50)	PAR1	15
	DOUBLE PRECISION P	PAR1	16
	INTEGER FLAG1,FLAG2,FLAG3,FLAG4,CASE,DATE1,DATE2,DATE3	PAR1	17
	COMMON / C1 / IMINSU,IMAXSU,IMINSI,IMAXSI,GRAND,GIFT,	PAR1	18
1	DX,ESIMP,FSIMP,GSIMP	PAR1	19
	COMMON / C2 / FLAG1,FLAG2,FLAG3,FLAG4,HEDR,DATE1,DATE2,	PAR1	20
1	DATE3,CASE,MXIDE,ICKDE,IPRDE,IMIN,IMAX,	PAR1	21
2	JMIN,JMAX,NUT,M,N,TOLDE,DEL,EPS,JTER,	PAR1	22
3	ITER,DPHI,DPSI,S,SBAR,RMULT,S1,S2,SBAR1,	PAR1	23
4	SBAR2,MSTAGU,NSTAGU,MSLOTU,MSTAGL,NSTAGL,	PAR1	24
5	MSLOTL,RADIN,W,PHI,PSI,RSLOTU,RSLOTL,	PAR1	25
6	QSLOTU,QSLOTL,ASLOTU,ASLOTL,XSLOTU,	PAR1	26
7	XSLOTL,G,MIDJ,TOLSYS	PAR1	27
	COMMON / C3 / EPHI,FPHI,GPHI,EPSI,FPSI,GPSI,MXISYS,	PAR1	28
1	IPRSYS	PAR1	29
	REWIND 4	PAR1	30
	REWIND 5	PAR1	31
	REWIND 12	PAR1	32
	READ CONTROL DATA	PAR1	33
	READ(1,10)FLAG1,FLAG2,FLAG3,FLAG4,HEDR,DATE1,DATE2,	PAR1	34
1	DATE3,CASE,RMULT,W,TOLSYS,TOLDE,MSTAGU,MSTAGL,	PAR1	35
2	M,N,MXISYS,MXIDE,NSTAGU,NSTAGL,RADIN,MIDJ,	PAR1	36
3	IPRSYS,IPRDE,MSLOTU,MSLOTL	PAR1	37
10	FORMAT(4I1,2X,15A4,2X,3I2,2X,I4/4F10.0,2I10/6I10/	PAR1	38
1	F10.0,5I10)	PAR1	39
	OUTPUT CONTROL DATA AND OPTIONS	PAR1	40
	WRITE(3,20)	PAR1	41
20	FORMAT(1H1//T57,'CLEMSON UNIVERSITY'//T49,	PAR1	42
	1'MECHANICAL ENGINEERING DEPARTMENT')	PAR1	43
	WRITE(3,30)HEDR,DATE1,DATE2,DATE3,CASE,FLAG1,RMULT,	PAR1	44
1	M,RADIN,FLAG2,W,N,MIDJ,FLAG3,TOLSYS,MXISYS,	PAR1	45
2	IPRSYS,FLAG4,TOLDE,MXIDE,IPRDE,MSTAGU,NSTAGU,	PAR1	46
3	MSLOTU,MSTAGL,NSTAGL,MSLOTL	PAR1	47
30	FORMAT(//T59,'PROGRAM 70-02'//T38,	PAR1	48
	1'AXIALLY SYMMETRIC AND 2-D BRANCHED CHANNEL',	PAR1	49
	2T85,' DESIGN'///T11,'*****',T21,15A4,T84,I2,T86,'/',	PAR1	50
	3T87,I2,T89,'/',T90,I2,T96,'CASE NO. ',T107,I4,	PAR1	51
	4T116,'*****',/////T51,'----- CONTROL DATA -----'	PAR1	52
	5/////T16,'FLAG1 = ',T23,I1,T36,'RMULT = ',T45,F11.6,	PAR1	53
	6T66,'M = ',T75,I10,T96,'RADIN = ',T105,F10.5/	PAR1	54
	7T16,'FLAG2 = ',T23,I1,T36,'W = ',T45,F11.6,T66,	PAR1	55
	8'N = ',T75,I10,T96,'MIDJ = ',T105,I10/T16,	PAR1	56
	9'FLAG3 = ',T23,I1,T36,'TOLSYS = ',T45,F11.6,T66,	PAR1	57
	A'MXISYS = ',T75,I10,T96,'IPRSYS = ',T105,I10/T16,	PAR1	58
	B'FLAG4 = ',T23,I1,T36,'TOLDE = ',T45,F11.6,T66,	PAR1	59
	C'MXIDE = ',T75,I10,T96,'IPRDE = ',T105,I10/T36,	PAR1	60
		PAR1	61
		PAR1	62
		PAR1	63
		PAR1	64

D*MSTAGU = ',T46,I10,T66,'NSTAGU = ',T75,I10,	PAR1	65
ET96,'MSLOTU = ',T105,I10/T36,'MSTAGL = ',T46,I10,	PAR1	66
FT66,'NSTAGL = ',T75,I10,T96,'MSLOTL = ',T105,I10////	PAR1	67
GT55,'----- OPTIONS -----')	PAR1	68
EPS = 0.0	PAR1	69
IF (FLAG1 .GT. 0) WRITE(3,40)	PAR1	70
40 FORMAT(///T57,'2-DIMENSIONAL')	PAR1	71
IF (FLAG1 .LE. 0) WRITE(3,50)	PAR1	72
50 FORMAT(///T57,'AXIALLY SYMMETRIC')	PAR1	73
IF ( FLAG2 .EQ. 0 .OR. FLAG2 .EQ. 4 ) WRITE(3,55)	PAR1	74
55 FORMAT(/T57,'DIRICHLET BOUNDARY CONDITIONS')	PAR1	75
IF ( FLAG2 .EQ. 1 ) WRITE(3,60)	PAR1	76
60 FORMAT(/T57,'NEUMANN BOUNDARY CONDITIONS')	PAR1	77
IF ( FLAG2 .EQ. 2 ) WRITE(3,65)	PAR1	78
65 FORMAT(/T57,'DIRICHLET B. C. AT INLET AND NEUMANN ',	PAR1	79
1T94,'B. C. AT OUTLET',/T60,'WITH VELOCITY INPUT AT INLET')	PAR1	80
IF ( FLAG2 .EQ. 3 ) WRITE(3,70)	PAR1	81
70 FORMAT(/T57,'NEUMANN B. C. AT INLET AND DIRICHLET ',	PAR1	82
1T94,'B. C. AT OUTLET',/T60,'WITH VELOCITY INPUT AT OUTLET')	PAR1	83
IF (FLAG3 .GT. 0) WRITE(3,80)	PAR1	84
80 FORMAT(/T57,'BELL DIFFUSER - NOZZLE')	PAR1	85
IF (FLAG3 .LE. 0 .AND. FLAG1 .LE. 0) WRITE(3,90)	PAR1	86
90 FORMAT(/T57,'ANNULAR DIFFUSER - NOZZLE')	PAR1	87
IF (FLAG4 .GT. 0) WRITE(3,100)	PAR1	88
100 FORMAT(/T57,'GRAPHICAL OUTPUT')	PAR1	89
IF (FLAG4 .LE. 0) WRITE(3,110)	PAR1	90
110 FORMAT(/T57,'NO GRAPHICAL OUTPUT SPECIFIED')	PAR1	91
C	PAR1	92
OUTPUT ERRORS DETECTED	PAR1	93
C	PAR1	94
IF (FLAG1 .LE. 0) GO TO 130	PAR1	95
IF (FLAG3 .LE. 0) GO TO 130	PAR1	96
/ WRITE(3,120)	PAR1	97
120 FORMAT(1H1,T1,'OIF FLAG1 GREATER THAN ZERO FLAG3 MUST BE ZERO')	PAR1	98
STOP	PAR1	99
130 IF (FLAG1 .LE. 0) GO TO 150	PAR1	100
IF (MXISYS .EQ. 1) GO TO 150	PAR1	101
WRITE(3,140)	PAR1	102
140 FORMAT(1H1,T1,'OIF FLAG1 GREATER THAN ZERO THEN',T32,	PAR1	103
1' MXISYS MUST BE ONE')	PAR1	104
STOP	PAR1	105
150 NM1 = N - 1	PAR1	106
NP1 = N + 1	PAR1	107
MM1 = M - 1	PAR1	108
MP1 = M + 1	PAR1	109
NM2 = N - 2	PAR1	110
NP2 = N + 2	PAR1	111
MM2 = M - 2	PAR1	112
MP2 = M + 2	PAR1	113
MSLUP1 = MSLOTU + 1	PAR1	114
MSLLP1 = MSLOTL + 1	PAR1	115
NSLLM1 = MSLOTL - 1	PAR1	116
MSTUP1 = MSTAGU + 1	PAR1	117
MSTUP2 = MSTAGU + 2	PAR1	118
MSTUP3 = MSTAGU + 3	PAR1	119
MSTLP1 = MSTAGL + 1	PAR1	120
MSTLP2 = MSTAGL + 2	PAR1	121
MSTLP3 = MSTAGL + 3	PAR1	122
NSTLP1 = NSTAGL + 1	PAR1	123
NSTLP2 = NSTAGL + 2	PAR1	124



	NSTUP1 = NSTAGU + 1	PAR1 125
	NSTUP2 = NSTAGU + 2	PAR1 126
	DO 155 J=1, NP2	PAR1 127
	DO 155 I=1, MP2	PAR1 128
	Q(I, J) = 1.0	PAR1 129
155	R(I, J) = 1.0	PAR1 130
	DO 157 I=1, MP2	PAR1 131
	RSLOTU(I) = 1.0	PAR1 132
	RSLOTL(I) = 1.0	PAR1 133
	QSLOTU(I) = 1.0	PAR1 134
157	QSLOTL(I) = 1.0	PAR1 135
C		PAR1 136
C	READ WALL VELOCITY DISTRIBUTION	PAR1 137
C		PAR1 138
	READ(1,160)(PHI(I), I=2, MP1)	PAR1 139
	READ(1,160)(Q(I, NP1), I=2, MSLUP1)	PAR1 140
	READ(1,160)(Q(I, NSTUP1), I=MSTUP2, MP1)	PAR1 141
	READ(1,160)(QSLOTU(I), I=MSTUP2, MSLUP1)	PAR1 142
160	FORMAT(6F10.0)	PAR1 143
	IF (FLAG1 .GT. 0 .OR. FLAG3 .GT. 0) GO TO 170	PAR1 144
	READ(1,160)(Q(I, 2), I=2, MSLLP1)	PAR1 145
	READ(1,160)(Q(I, NSTLP1), I=MSTLP2, MP1)	PAR1 146
	READ(1,160)(QSLOTL(I), I=MSTLP2, MSLLP1)	PAR1 147
170	DO 180 I=2, M	PAR1 148
180	DPHI(I) = PHI(I+1) - PHI(I)	PAR1 149
	DPHI(1) = DPHI(2)	PAR1 150
	DPHI(MP1) = DPHI(M)	PAR1 151
C		PAR1 152
C	READ STREAM FUNCTION SPACING	PAR1 153
C		PAR1 154
	READ(1,160)(PSI(I), I=2, NP1)	PAR1 155
	DO 190 I=2, N	PAR1 156
190	DPSI(I) = PSI(I+1) - PSI(I)	PAR1 157
	DPSI(1) = DPSI(2)	PAR1 158
	DPSI(NP1) = DPSI(N)	PAR1 159
C		PAR1 160
C	COMPUTE ARC LENGTHS ALONG THE WALL	PAR1 161
C		PAR1 162
	DO 200 I=2, M	PAR1 163
200	DX(I) = DPHI(I)	PAR1 164
	IMINSU = 2	PAR1 165
	IMAXSU = MM1	PAR1 166
	CALL SETUP	PAR1 167
	DO 210 I=2, MSLUP1	PAR1 168
210	GRAND(I) = 1.0 / Q(I, NP1)	PAR1 169
	IMINSI = 2	PAR1 170
	IMAXSI = MSLUP1	PAR1 171
	CALL SIMP	PAR1 172
	DO 220 I=2, MSLUP1	PAR1 173
220	S(I) = GIFT(I)	PAR1 174
	S1(MSTUP1) = 0.0	PAR1 175
	S2(MSTUP1) = 0.0	PAR1 176
	Q(MSTUP1, NSTUP1) = 0.0	PAR1 177
	QSLOTU(MSTUP1) = 0.0	PAR1 178
	S1(MSTUP2) = 2. * DPHI(MSTUP1) / Q(MSTUP2, NSTUP1)	PAR1 179
	S2(MSTUP2) = S1(MSTUP2)	PAR1 180
	DO 230 I=MSTUP2, MP1	PAR1 181
230	GRAND(I) = 1.0 / Q(I, NSTUP1)	PAR1 182
	IMINSI = MSTUP2	PAR1 183
	IMAXSI = MP1	PAR1 184

CALL SIMP	PAR1 185
DO 240 I=MSTUP3,MP1	PAR1 186
240 S1(I) = GIFT(I) + S1(MSTUP2)	PAR1 187
DO 250 I=MSTUP2,MSLUP1	PAR1 188
250 GRAND(I) = 1.0 / QSLOTU(I)	PAR1 189
IMINSI = MSTUP2	PAR1 190
IMAXSI = MSLUP1	PAR1 191
CALL SIMP	PAR1 192
DO 260 I=MSTUP3,MSLUP1	PAR1 193
260 S2(I) = GIFT(I) + S2(MSTUP2)	PAR1 194
IF (FLAG1 .GT. 0 .OR. FLAG3 .GT. 0) GO TO 330	PAR1 195
DO 270 I=2,MSLLP1	PAR1 196
270 GRAND(I) = 1.0 / Q(I,2)	PAR1 197
IMINSI = 2	PAR1 198
IMAXSI = MSLLP1	PAR1 199
CALL SIMP	PAR1 200
DO 280 I=2,MSLLP1	PAR1 201
280 SBAR(I) = GIFT(I)	PAR1 202
SBAR1(MSTLP1) = 0.0	PAR1 203
SBAR2(MSTLP1) = 0.0	PAR1 204
Q(MSTLP1,NSTLP1) = 0.0	PAR1 205
QSLOTL(MSTLP1) = 0.0	PAR1 206
SBAR1(MSTLP2) = 2. * DPHI(MSTLP1) / Q(MSTLP2,NSTLP1)	PAR1 207
SBAR2(MSTLP2) = SBAR1(MSTLP2)	PAR1 208
DO 290 I=MSTLP2,MP1	PAR1 209
290 GRAND(I) = 1.0 / Q(I,NSTLP1)	PAR1 210
IMINSI = MSTLP2	PAR1 211
IMAXSI = MP1	PAR1 212
CALL SIMP	PAR1 213
DO 300 I=MSTLP3,MP1	PAR1 214
300 SBAR1(I) = GIFT(I) + SBAR1(MSTLP2)	PAR1 215
DO 310 I=MSTLP2,MSLLP1	PAR1 216
310 GRAND(I) = 1.0 / QSLOTL(I)	PAR1 217
IMINSI = MSTLP2	PAR1 218
IMAXSI = MSLLP1	PAR1 219
CALL SIMP	PAR1 220
DO 320 I=MSTLP3,MSLLP1	PAR1 221
320 SBAR2(I) = GIFT(I) + SBAR2(MSTLP2)	PAR1 222
C	PAR1 223
C	PAR1 224
C	PAR1 225
C	PAR1 226
330 WRITE(3,20)	PAR1 227
WRITE(3,340)HEDR,DATE1,DATE2,DATE3,CASE	PAR1 228
340 FORMAT(//T2,15A4,T64,I2,T66,'/',T67,I2,T69,'/',T70,I2,	PAR1 229
1T76,'CASE NO. ',T87,I4//T2,'WALL VELOCITY',	PAR1 230
2T15,' DISTRIBUTION AND POTENTIAL SPACING',	PAR1 231
3T50,' UPSTREAM OF SLOT ( UPPER SURFACE )'//T16,'S',	PAR1 232
4T36,'Q',T54,'PHI',T74,'DPHI'//)	PAR1 233
ICOUNT = 1	PAR1 234
DO 360 I=2,MSLUP1	PAR1 235
ICOUNT = ICOUNT + 1	PAR1 236
WRITE(3,350)I,S(I),Q(I,NP1),PHI(I),DPHI(I)	PAR1 237
350 FORMAT(T2,I3,T10,F10.5,T30,F10.5,T50,F10.5/T70,F10.5)	PAR1 238
IF (ICOUNT .LT. 23) GO TO 360	PAR1 239
ICOUNT = 1	PAR1 240
WRITE(3,20)	PAR1 241
WRITE(3,340)HEDR,DATE1,DATE2,DATE3,CASE	PAR1 242
360 CONTINUE	PAR1 243
WRITE(3,20)	PAR1 244

WRITE(3,370)HEDR,DATE1,DATE2,DATE3,CASE	PARI 245
370 FORMAT(//T2,15A4,T64,I2,T66,'/',T67,I2,T69,'/',T70,I2,	PARI 246
1T76,'CASE NO. ',T87,I4//T2,'WALL VELOCITY',	PARI 247
2T15,' DISTRIBUTION AND POTENTIAL SPACING',	PARI 248
3T50,' DOWNSTREAM OF SLOT ( UPPER SURFACE )'///T16,'S',	PARI 249
4T36,'Q',T54,'PHI',T74,'DPHI'//)	PARI 250
ICOUNT = 1	PARI 251
DO 380 I=MSTUP1,MP1	PARI 252
ICOUNT = ICOUNT + 1	PARI 253
WRITE(3,350)I,S1(I),Q(I,NSTUP1),PHI(I),DPHI(I)	PARI 254
IF (ICOUNT .LT. 23) GO TO 380	PARI 255
ICOUNT = 1	PARI 256
WRITE(3,20)	PARI 257
WRITE(3,370)HEDR,DATE1,DATE2,DATE3,CASE	PARI 258
380 CONTINUE	PARI 259
WRITE(3,20)	PARI 260
WRITE(3,390)HEDR,DATE1,DATE2,DATE3,CASE	PARI 261
390 FORMAT(//T2,15A4,T64,I2,T66,'/',T67,I2,T69,'/',T70,I2,	PARI 262
1T76,'CASE NO. ',T87,I4//T2,'WALL VELOCITY',	PARI 263
2T15,' DISTRIBUTION AND POTENTIAL SPACING',	PARI 264
3T50,' INSIDE SLOT ( UPPER SURFACE )'///T16,'S',	PARI 265
4T36,'Q',T54,'PHI',T74,'DPHI'//)	PARI 266
ICOUNT = 1	PARI 267
DO 400 I=MSTUP1,MSLUP1	PARI 268
ICOUNT = ICOUNT + 1	PARI 269
WRITE(3,350)I,S2(I),QSLOTU(I),PHI(I),DPHI(I)	PARI 270
IF (ICOUNT .LT. 23) GO TO 400	PARI 271
ICOUNT = 1	PARI 272
WRITE(3,20)	PARI 273
WRITE(3,390)HEDR,DATE1,DATE2,DATE3,CASE	PARI 274
400 CONTINUE	PARI 275
Q(MSTUP1,NSTUP1) = 1.0	PARI 276
QSLOTU(MSTUP1) = 1.0	PARI 277
C	PARI 278
C	PARI 279
C	PARI 280
C	PARI 281
IF (FLAG1 .GT. 0 .OR. FLAG3 .GT. 0) GO TO 470	PARI 282
WRITE(3,20)	PARI 283
WRITE(3,410)HEDR,DATE1,DATE2,DATE3,CASE	PARI 284
410 FORMAT(//T2,15A4,T64,I2,T66,'/',T67,I2,T69,'/',T70,I2,	PARI 285
1T76,'CASE NO. ',T87,I4//T2,'WALL VELOCITY',	PARI 286
2T15,' DISTRIBUTION AND POTENTIAL SPACING',	PARI 287
3T50,' UPSTREAM OF SLOT ( LOWER SURFACE )'///T16,'S',	PARI 288
4T36,'Q',T54,'PHI',T74,'DPHI'//)	PARI 289
ICOUNT = 1	PARI 290
DO 420 I=2,MSLLP1	PARI 291
ICOUNT = ICOUNT + 1	PARI 292
WRITE(3,350)I,SBAR(I),Q(I,2),PHI(I),DPHI(I)	PARI 293
IF (ICOUNT .LT. 23) GO TO 420	PARI 294
ICOUNT = 1	PARI 295
WRITE(3,20)	PARI 296
WRITE(3,410)HEDR,DATE1,DATE2,DATE3,CASE	PARI 297
420 CONTINUE	PARI 298
WRITE(3,20)	PARI 299
WRITE(3,430)HEDR,DATE1,DATE2,DATE3,CASE	PARI 300
430 FORMAT(//T2,15A4,T64,I2,T66,'/',T67,I2,T69,'/',T70,I2,	PARI 301
1T76,'CASE NO. ',T87,I4//T2,'WALL VELOCITY',	PARI 302
2T15,' DISTRIBUTION AND POTENTIAL SPACING',	PARI 303
3T50,' DOWNSTREAM OF SLOT ( LOWER SURFACE )'///T16,'S',	PARI 304

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4T36,'Q',T54,'PHI',T74,'DPHI'///
  ICOUNT = 1
  DO 440 I=MSTLP1,MP1
  ICOUNT = ICOUNT + 1
  WRITE(3,350)I,SBAR1(I),Q(I,NSTLP1),PHI(I),DPHI(I)
  IF (ICOUNT .LT. 23) GO TO 440
  ICOUNT = 1
  WRITE(3,20)
  WRITE(3,430)HEDR,DATE1,DATE2,DATE3,CASE
440 CONTINUE
  WRITE(3,20)
  WRITE(3,450)HEDR,DATE1,DATE2,DATE3,CASE
450 FORMAT(//T2,15A4,T64,I2,T66,'/',T67,I2,T69,'/',T70,I2,
1T76,'CASE NO. ',T87,I4///T2,'WALL VELOCITY',
2T15,' DISTRIBUTION AND POTENTIAL SPACING',
3T50,' INSIDE OF SLOT ( LOWER SURFACE )'///T16,'S',
4T36,'Q',T54,'PHI',T74,'DPHI'///
  ICOUNT = 1
  DO 460 I=MSTLP1,MSLLP1
  ICOUNT = ICOUNT + 1
  WRITE(3,350)I,SBAR2(I),QSLOTL(I),PHI(I),DPHI(I)
  IF (ICOUNT .LT. 23) GO TO 460
  ICOUNT = 1
  WRITE(3,20)
  WRITE(3,450)HEDR,DATE1,DATE2,DATE3,CASE
460 CONTINUE
  Q(MSTLP1,NSTLP1) = 1.0
  QSLOTL(MSTLP1) = 1.0
C
C      OUTPUT STREAM FUNCTION DISTRIBUTION AND
C      SPACING
C
470 WRITE(3,20)
  WRITE(3,480)HEDR,DATE1,DATE2,DATE3,CASE
480 FORMAT(//T2,15A4,T64,I2,T66,'/',T67,I2,T69,'/',T70,I2,
1T76,'CASE NO. ',T87,I4///T2,'STREAM FUNCTION',
2T18,' DISTRIBUTION',///T15,'PSI',T35,'OPSI'///
  ICOUNT = 1
  DO 500 J=2,NP1
  ICOUNT = ICOUNT + 1
  WRITE(3,490)J,PSI(J),DPSI(J)
490 FORMAT(T2,I3,T10,F10.5,/T30,F10.5)
  IF (ICOUNT .LT. 23) GO TO 500
  ICOUNT = 1
  WRITE(3,20)
  WRITE(3,480)HEDR,DATE1,DATE2,DATE3,CASE
500 CONTINUE
C
C      COMPUTE INTEGRATION CONSTANTS INVOLVING DPHI
C
  DO 510 I=2,M
510 DX(I) = DPHI(I)
  IMINSU = 2
  IMAXSU = MM1
  CALL SETUP
  DO 520 I=2,MM1
  EPHI(I) = ESIMP(I)
  FPHI(I) = FSIMP(I)
520 GPHI(I) = GSIMP(I)
C

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C	COMPUTE INTEGRATION CONSTANTS INVOLVING DPSI	PAR1 365
C		PAR1 366
	DO 530 J=2,N	PAR1 367
530	DX(J) = DPSI(J)	PAR1 368
	IMINSU = 2	PAR1 370
	IMAXSU = NM1	PAR1 371
	CALL SETUP	PAR1 372
	DO 540 J=2,NM1	PAR1 373
	EPSI(J) = ESIMP(J)	PAR1 374
	FPSI(J) = FSIMP(J)	PAR1 375
540	GPSI(J) = GSIMP(J)	PAR1 376
C		PAR1 377
C	COMPUTE CONSTANTS TO CONTROL INTEGRATION	PAR1 378
C		PAR1 379
	IMIN = 3	PAR1 380
	IMAX = M	PAR1 381
	JMIN = 2	PAR1 382
	JMAX = NP1	PAR1 383
	IF (FLAG3 .GT. 0) JMIN=3	PAR1 384
	IF (FLAG2 .LE. 0) GO TO 550	PAR1 385
	IMIN = 2	PAR1 386
	IMAX = MP1	PAR1 387
C		PAR1 388
C	INITIALIZE ARRAYS	PAR1 389
C		PAR1 390
550	DO 560 J=2,NP1	PAR1 391
	Q(2,J) = Q(2,NP1)	PAR1 392
560	Q(MP1,J) = Q(MP1,NSTUP1)	PAR1 393
	DO 570 J=1,NP2	PAR1 394
	DO 570 I=1,MP2	PAR1 395
	P = Q(I,J)	PAR1 396
570	Q(I,J) = DLOG(P)	PAR1 397
	DO 580 I=1,MP2	PAR1 398
	P = QSLOTU(I)	PAR1 399
	QSLOTU(I) = DLOG(P)	PAR1 400
	P = QSLOTL(I)	PAR1 401
580	QSLOTL(I) = DLOG(P)	PAR1 402
C		PAR1 403
C	COMPUTE VELOCITIES AROUND STAGNATION POINTS	PAR1 404
C		PAR1 405
	Q(MSTAGU,NSTUP1) = QSLOTU(MSTUP2)	PAR1 406
	Q(MSTUP1,NSTUP2) = QSLOTU(MSTUP2)	PAR1 407
	Q(MSTUP1,NSTAGU) = QSLOTU(MSTUP2)	PAR1 408
	IF (FLAG1 .GT. 0 .OR. FLAG3 .GT. 0) GO TO 610	PAR1 409
	Q(MSTAGL,NSTLP1) = QSLOTL(MSTLP2)	PAR1 410
	Q(MSTLP1,NSTLP2) = QSLOTL(MSTLP2)	PAR1 411
	Q(MSTLP1,NSTAGL) = QSLOTL(MSTLP2)	PAR1 412
610	CONTINUE	PAR1 413
	DO 620 J=1,NP2	PAR1 414
	DO 620 I=1,MP2	PAR1 415
620	X(I,J) = 0.0	PAR1 416
C		PAR1 417
C	READ INLET AND OUTLET VELOCITY PROFILES (IF USED)	PAR1 418
C		PAR1 419
	IF (FLAG2 .NE. 2 .AND. FLAG2 .NE. 4) GO TO 640	PAR1 420
	IMIN = 3	PAR1 421
	READ(1,160)(Q(2,J),J=2,NP1)	PAR1 422
	DO 630 J=2,NP1	PAR1 423
	P = Q(2,J)	PAR1 424
630	Q(2,J) = DLOG(P)	

640	IF (FLAG2 .NE. 3 .AND. FLAG3 .NE. 4) GO TO 660	PARI 425
	IMAX = M	PARI 426
	NSTUP1 = NSTAGU + 1	PARI 427
	IF (FLAG1 .GT. 0 .OR. FLAG3 .GT. 0) READ(1,160)(Q(MP1,J),J=2,	PARI 428
	INSTUP1)	PARI 429
	NSTLP1 = NSTAGL + 1	PARI 430
	IF (FLAG1 .LE. 0 .AND. FLAG3 .LE. 0) READ(1,160)(Q(MP1,J),	PARI 431
	IJ=NSTLP1,NSTUP1)	PARI 432
	DO 650 J=2,NP1	PARI 433
	P = Q(MP1,J)	PARI 434
650	Q(MP1,J) = DLOG(P)	PARI 435
660	CONTINUE	PARI 436
C		PARI 437
C	WRITE HEADING FOR CONVERGENCE VARIABLES	PARI 438
C		PARI 439
	IF (FLAG1 .LE. 0) WRITE(3,670)HEDR,DATE1,DATE2,DATE3,CASE	PARI 440
670	FORMAT(1H1//T57,'CLEMSON UNIVERSITY',//T49,'MECHANICAL ENGINEER	PARI 441
	ING DEPARTMENT',//T2,15A4,T64,I2,T66,'/',T67,I2,T69,'/',T70,I2,	PARI 442
	2T76,'CASE NO. ',T87,I4//)	PARI 443
	IF (FLAG1 .LE. 0) WRITE(3,680)	PARI 444
680	FORMAT(T2,'IMPORTANT VARIABLES FOR EACH ITERATION OF',	PARI 445
	1T43,' THE R COORDINATES'//)	PARI 446
	WRITE(4)((Q(I,J),I=1,MP2),J=1,NP2)	PARI 447
	WRITE(5)((R(I,J),I=1,MP2),J=1,NP2)	PARI 448
	WRITE(12)((X(I,J),I=1,MP2),J=1,NP2)	PARI 449
	RETURN	PARI 450
	END	PARI 451
C	***** SUBROUTINE COEF *****	COEF 1
C	THIS SUBROUTINE COMPUTES COEFFICIENTS TO BE USED	COEF 2
C	IN RELAXATION OF THE DIFFERENTIAL EQUATION	COEF 3
C		COEF 4
	SUBROUTINE COEF	COEF 5
	DIMENSION DPHI(150),DPSI(150),S(150),SBAR(150),	COEF 6
1	S1(150),S2(150),SBAR1(150),SBAR2(150),	COEF 7
2	PHI(150),PSI(150),RSL0TU(150);RSL0TL(150),	COEF 8
3	QSL0TU(150),QSL0TL(150),ASL0TU(150),	COEF 9
4	ASL0TL(150),XSL0TU(150),XSL0TL(150),HEDR(15)	COEF 10
	DIMENSION A(150,50),B(150,50),C(150,50),D(150,50),	COEF 11
1	E(150,50),R(150,50)	COEF 12
	INTEGER FLAG1,FLAG2,FLAG3,FLAG4,CASE,DATE1,DATE2,DATE3	COEF 13
	COMMON / C2 / FLAG1,FLAG2,FLAG3,FLAG4,HEDR,DATE1,DATE2,	COEF 14
1	DATE3,CASE,MXIDE,ICKDE,IPRDE,IMIN,IMAX,	COEF 15
2	JMIN,JMAX,NUT,M,N,TOLDE,DEL,EDS,JTER,	COEF 16
3	ITER,DPHI,DPSI,S,SBAR,RMULT,S1,S2,SBAR1,	COEF 17
4	SBAR2,MSTAGU,NSTAGU,MSL0TU,MSTAGL,NSTAGL,	COEF 18
5	MSL0TL,RADIN,W,PHI,PSI,RSL0TU,RSL0TL,	COEF 19
6	QSL0TU,QSL0TL,ASL0TU,ASL0TL,XSL0TU,	COEF 20
7	XSL0TL,G,MIDJ,TOLSYS	COEF 21
	REWIND 5	COEF 22
	REWIND 6	COEF 23
	REWIND 7	COEF 24
	REWIND 8	COEF 25
	REWIND 9	COEF 26
	REWIND 10	COEF 27
	MP2 = M + 2	COEF 28
	NP2 = N + 2	COEF 29
	NSTUM1 = NSTAGU - 1	COEF 30
	MSTUP2 = MSTAGU + 2	COEF 31
	MSTLP2 = MSTAGL + 2	COEF 32
	MSLUP1 = MSL0TU + 1	COEF 33

MSLLP1 = MSLOT1 + 1	COEF 34
NSTLP1 = NSTAGL + 1	COEF 35
NSTLP2 = NSTAGL + 2	COEF 36
NSTUP2 = NSTAGU + 2	COEF 37
READ(5)((R(I,J),I=1,MP2),J=1,NP2)	COEF 38

C  
C  
C

COMPUTE COEFFICIENTS THROUGHOUT DIFFUSER

DO 100 J=JMIN,JMAX	COEF 42
DD = DPSI(J-1) * DPSI(J)	COEF 43
EE = DPSI(J-1) + DPSI(J)	COEF 44
FF = DPSI(J-1) - DPSI(J)	COEF 45
DO 100 I=IMIN,IMAX	COEF 46
AA = DPHI(I-1) * DPHI(I)	COEF 47
BB = DPHI(I-1) + DPHI(I)	COEF 48
CC = DPHI(I-1) - DPHI(I)	COEF 49
DERX = DPHI(I-1) * R(I+1,J) / ( DPHI(I) * BB )	COEF 50
DERX = DERX - DPHI(I) * R(I-1,J) / ( DPHI(I-1) * BB )	COEF 51
DERX = DERX - CC * R(I,J) / AA	COEF 52
DERY = DPSI(J-1) * R(I,J+1) / ( DPSI(J) * EE )	COEF 53
DERY = DERY - DPSI(J) * R(I,J-1) / ( DPSI(J-1) * EE )	COEF 54
DERY = DERY - FF * R(I,J) / DD	COEF 55
DDERX = 2. * R(I+1,J) / ( DPHI(I) * BB )	COEF 56
DDERX = DDERX + 2. * R(I-1,J) / ( DPHI(I-1) * BB )	COEF 57
DDERX = DDERX - 2. * R(I,J) / AA	COEF 58
F = 2. * R(I,J) * R(I,J) * R(I,J) * R(I,J) / DD	COEF 59
F = F + R(I,J) * R(I,J) * R(I,J) * FF * DERY / DU	COEF 60
F = F + 2. * R(I,J) * R(I,J) * R(I,J) / AA	COEF 61
F = F - R(I,J) * CC * DERX / AA	COEF 62
A(I,J) = 2. * R(I,J) - DPHI(I-1) * DERX	COEF 63
A(I,J) = A(I,J) * W * R(I,J) / ( F * DPHI(I) * BB )	COEF 64
B(I,J) = 2. * R(I,J) + DPHI(I) * DERX	COEF 65
B(I,J) = B(I,J) * W * R(I,J) / ( F * DPHI(I-1) * BB )	COEF 66
R3 = R(I,J) * R(I,J) * R(I,J)	COEF 67
C(I,J) = 2. * R(I,J) + DPSI(J-1) * DERY	COEF 68
C(I,J) = C(I,J) * W * R3 / ( F * DPSI(J) * EE )	COEF 69
D(I,J) = 2. * R(I,J) - DPSI(J) * DERY	COEF 70
D(I,J) = D(I,J) * W * R3 / ( F * DPSI(J-1) * EE )	COEF 71
100 E(I,J) = ( R(I,J) * DDERX - 2. * DERX * DERX ) / F	COEF 72

C  
C  
C

COMPUTE COEFFICIENTS INSIDE UPPER SLOT

J = NSTAGU + 2	COEF 76
DD = DPSI(J-1) * DPSI(J)	COEF 77
EE = DPSI(J-1) + DPSI(J)	COEF 78
FF = DPSI(J-1) - DPSI(J)	COEF 79
DO 200 I=MSTUP2,MSLUP1	COEF 80
AA = DPHI(I-1) * DPHI(I)	COEF 81
BB = DPHI(I-1) + DPHI(I)	COEF 82
CC = DPHI(I-1) - DPHI(I)	COEF 83
DERX = DPHI(I-1) * R(I+1,J) / ( DPHI(I) * BB )	COEF 84
DERX = DERX - DPHI(I) * R(I-1,J) / ( DPHI(I-1) * BB )	COEF 85
DERX = DERX - CC * R(I,J) / AA	COEF 86
DERY = DPSI(J-1) * R(I,J+1) / ( DPSI(J) * EE )	COEF 87
DERY = DERY - DPSI(J) * R(I,J-1) / ( DPSI(J-1) * EE )	COEF 88
DERY = DERY - FF * R(I,J) / DD	COEF 89
DDERX = 2. * R(I+1,J) / ( DPHI(I) * BB )	COEF 90
DDERX = DDERX + 2. * R(I-1,J) / ( DPHI(I-1) * BB )	COEF 91
DDERX = DDERX - 2. * R(I,J) / AA	COEF 92
F = 2. * R(I,J) * R(I,J) * R(I,J) * R(I,J) / DD	COEF 93

	F = F + R(I,J) * R(I,J) * R(I,J) * FF * DERY / DD	COEF 94
	F = F + 2. * R(I,J) * R(I,J) / AA	COEF 95
	F = F - R(I,J) * CC * DERX / AA	COEF 96
	A(I,J) = 2. * R(I,J) - DPHI(I-1) * DERX	COEF 97
	A(I,J) = A(I,J) * W * R(I,J) / ( F * DPHI(I) * BB )	COEF 98
	B(I,J) = 2. * R(I,J) + DPHI(I) * DERX	COEF 99
	B(I,J) = B(I,J) * W * R(I,J) / ( F * DPHI(I-1) * BB )	COEF 100
	R3 = R(I,J) * R(I,J) * R(I,J)	COEF 101
	C(I,J) = 2. * R(I,J) + DPSI(J-1) * DERY	COEF 102
	C(I,J) = C(I,J) * W * R3 / ( F * DPSI(J) * EE )	COEF 103
	D(I,J) = 2. * R(I,J) - DPSI(J) * DERY	COEF 104
	D(I,J) = D(I,J) * W * R3 / ( F * DPSI(J-1) * EE )	COEF 105
200	E(I,J) = ( R(I,J) * DDERX - 2. * DERX * DERX ) / F	COEF 106
C		COEF 107
C	COMPUTE COEFFICIENTS INSIDE LOWER SLOT	COEF 108
C		COEF 109
	IF (FLAG1 .GT. 0 .OR. FLAG3 .GT. 0) GO TO 1000	COEF 110
	J = NSTAGL	COEF 111
	DD = DPSI(J-1) * DPSI(J)	COEF 112
	EE = DPSI(J-1) + DPSI(J)	COEF 113
	FF = DPSI(J-1) - DPSI(J)	COEF 114
	DO 300 I=MSTLP2,MSLLP1	COEF 115
	AA = DPHI(I-1) * DPHI(I)	COEF 116
	BB = DPHI(I-1) + DPHI(I)	COEF 117
	CC = DPHI(I-1) - DPHI(I)	COEF 118
	DERX = DPHI(I-1) * R(I+1,J) / ( DPHI(I) * BB )	COEF 119
	DERX = DERX - DPHI(I) * R(I-1,J) / ( DPHI(I-1) * BB )	COEF 120
	DERX = DERX - CC * R(I,J) / AA	COEF 121
	DERY = DPSI(J-1) * RSL0TL(I) / ( DPSI(J) * EE )	COEF 122
	DERY = DERY - DPSI(J) * R(I,J-1) / ( DPSI(J-1) * EE )	COEF 123
	DERY = DERY - FF * R(I,J) / DD	COEF 124
	DDERX = 2. * R(I+1,J) / ( DPHI(I) * BB )	COEF 125
	DDERX = DDERX + 2. * R(I-1,J) / ( DPHI(I-1) * BB )	COEF 126
	DDERX = DDERX - 2. * R(I,J) / AA	COEF 127
	F = 2. * R(I,J) * R(I,J) * R(I,J) * R(I,J) / DD	COEF 128
	F = F + R(I,J) * R(I,J) * R(I,J) * FF * DERY / DD	COEF 129
	F = F + 2. * R(I,J) * R(I,J) / AA	COEF 130
	F = F - R(I,J) * CC * DERX / AA	COEF 131
	A(I,J) = 2. * R(I,J) - DPHI(I-1) * DERX	COEF 132
	A(I,J) = A(I,J) * W * R(I,J) / ( F * DPHI(I) * BB )	COEF 133
	B(I,J) = 2. * R(I,J) + DPHI(I) * DERX	COEF 134
	B(I,J) = B(I,J) * W * R(I,J) / ( F * DPHI(I-1) * BB )	COEF 135
	R3 = R(I,J) * R(I,J) * R(I,J)	COEF 136
	C(I,J) = 2. * R(I,J) + DPSI(J-1) * DERY	COEF 137
	C(I,J) = C(I,J) * W * R3 / ( F * DPSI(J) * EE )	COEF 138
	D(I,J) = 2. * R(I,J) - DPSI(J) * DERY	COEF 139
	D(I,J) = D(I,J) * W * R3 / ( F * DPSI(J-1) * EE )	COEF 140
300	E(I,J) = ( R(I,J) * DDERX - 2. * DERX * DERX ) / F	COEF 141
1000	CONTINUE	COEF 142
	G = 1. - W	COEF 143
	WRITE(6)((A(I,J),I=1,MP2),J=1,NP2)	COEF 144
	WRITE(7)((B(I,J),I=1,MP2),J=1,NP2)	COEF 145
	WRITE(8)((C(I,J),I=1,MP2),J=1,NP2)	COEF 146
	WRITE(9)((D(I,J),I=1,MP2),J=1,NP2)	COEF 147
	WRITE(10)((E(I,J),I=1,MP2),J=1,NP2)	COEF 148
	RETURN	COEF 149
	END	COEF 150



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C          ***** SUBROUTINE RELAX ***** RELX 1
C          THIS SUBROUTINE RELAXES THE DIFFERENTIAL EQUATION RELX 2
C          USING COEFFICIENTS COMPUTED IN COEF RELX 3
C          RELX 4
C          RELX 5
SUBROUTINE RELAX RELX 6
DIMENSION DPHI(150),DPSI(150),S(150),SBAR(150), RELX 7
1 S1(150),S2(150),SBAR1(150),SBAR2(150), RELX 8
2 PHI(150),PSI(150),RSLOTU(150),RSLOTL(150), RELX 9
3 QSLOTU(150),QSLOTL(150),ASLOTU(150), RELX 10
4 ASLOTL(150),XSLOTU(150),XSLOTL(150),HEDR(15) RELX 11
DIMENSION A(150,50),B(150,50),C(150,50),D(150,50), RELX 12
1 E(150,50),Q(150,50) RELX 13
DOUBLE PRECISION P RELX 14
INTEGER FLAG1,FLAG2,FLAG3,FLAG4,CASE,DATE1,DATE2,DATE3 RELX 15
COMMON / C2 / FLAG1,FLAG2,FLAG3,FLAG4,HEDR,DATE1, RELX 16
1 DATE2,DATE3,CASE,MXIDE,ICKDE,IPRDE,IMIN, RELX 17
2 IMAX,JMIN,JMAX,NUT,M,N,TOLDE,DEL,EPS, RELX 18
3 JTER,ITER,DPHI,DPSI,S,SBAR,RMULT,S1,S2, RELX 19
4 SBAR1,SBAR2,MSTAGU,NSTAGU,MSLOTU,MSTAGL, RELX 20
5 NSTAGL,MSLOTL,RADIN,W,PHI,PSI,RSLOTU, RELX 21
6 RSLOTL,QSLOTU,QSLOTL,ASLOTU,ASLOTL, RELX 22
7 XSLOTU,XSLOTL,G,MIDJ,TOLSYS RELX 23
REWIND 4 RELX 24
REWIND 6 RELX 25
REWIND 7 RELX 26
REWIND 8 RELX 27
REWIND 9 RELX 28
REWIND 10 RELX 29
NP1 = N + 1 RELX 30
MP1 = M + 1 RELX 31
NP2 = N + 2 RELX 32
MP2 = M + 2 RELX 33
NM1 = N - 1 RELX 34
MM1 = M - 1 RELX 35
NM2 = N - 2 RELX 36
MM2 = M - 2 RELX 37
MSTUM1 = MSTAGU - 1 RELX 38
MSTUP1 = MSTAGU + 1 RELX 39
MSTUP2 = MSTAGU + 2 RELX 40
MSTLM1 = MSTAGL - 1 RELX 41
MSTLP2 = MSTAGL + 2 RELX 42
NSTUM1 = NSTAGU - 1 RELX 43
NSTUP1 = NSTAGU + 1 RELX 44
NSTUP2 = NSTAGU + 2 RELX 45
NSTUP3 = NSTAGU + 3 RELX 46
NSTLM1 = NSTAGL - 1 RELX 47
NSTLP1 = NSTAGL + 1 RELX 48
NSTLP2 = NSTAGL + 2 RELX 49
NSTLP3 = NSTAGL + 3 RELX 50
MSLUP1 = MSLOTU + 1 RELX 51
MSLUP2 = MSLOTU + 2 RELX 52
MSLLP1 = MSLOTL + 1 RELX 53
MSLLP2 = MSLOTL + 2 RELX 54
READ(4)((Q(I,J),I=1,MP2),J=1,NP2) RELX 55
READ(6)((A(I,J),I=1,MP2),J=1,NP2) RELX 56
READ(7)((H(I,J),I=1,MP2),J=1,NP2) RELX 57
READ(8)((C(I,J),I=1,MP2),J=1,NP2) RELX 58
READ(9)((D(I,J),I=1,MP2),J=1,NP2) RELX 59
READ(10)((E(I,J),I=1,MP2),J=1,NP2) RELX 60

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II = 1	RELX 61
JTER = 0	RELX 62
DO 3000 ITTT=1,MXIDE	RELX 63
DEL = 0.0	RELX 64
JTER = JTER + 1	RELX 65
C	RELX 66
C	RELX 67
RELAX LOWER PORTION FOR 2-D AND BELL	RELX 68
C	RELX 69
IF (FLAG1 .LE. 0 .AND. FLAG3 .LE. 0) GO TO 30	RELX 70
DO 10 J=3,NSTUM1	RELX 71
DO 10 I=IMIN,IMAX	RELX 72
AA = A(I,J) * Q(I+1,J)	RELX 73
BB = B(I,J) * Q(I-1,J)	RELX 74
CC = C(I,J) * Q(I,J+1)	RELX 75
DD = D(I,J) * Q(I,J-1)	RELX 76
EE = E(I,J) + G * Q(I,J)	RELX 77
QLAST = Q(I,J)	RELX 78
Q(I,J) = AA + BB + CC + DD + EE	RELX 79
DELSTR = ABS(QLAST - Q(I,J))	RELX 80
10 IF (DELSTR .GT. DEL) DEL = DELSTR	RELX 81
IF (FLAG3 .GT. 0) GO TO 110	RELX 82
J = 2	RELX 83
DO 20 I=IMIN,IMAX	RELX 84
AA = A(I,J) * Q(I+1,J)	RELX 85
BB = B(I,J) * Q(I-1,J)	RELX 86
CC = C(I,J) * Q(I,J+1)	RELX 87
DD = D(I,J) * Q(I,J-1)	RELX 88
EE = E(I,J) + G * Q(I,J)	RELX 89
QLAST = Q(I,J)	RELX 90
Q(I,J) = AA + BB + CC + DD + EE	RELX 91
DELSTR = ABS(QLAST - Q(I,J))	RELX 92
20 IF (DELSTR .GT. DEL) DEL = DELSTR	RELX 93
GO TO 110	RELX 94
C	RELX 95
C	RELX 96
RELAX LOWER PORTION OF ANNULAR DIFFUSER	RELX 97
C	RELX 98
30 DO 40 J=3,NSTLMI	RELX 99
DO 40 I=IMIN,MSLLP1	RELX 100
AA = A(I,J) * Q(I+1,J)	RELX 101
BB = B(I,J) * Q(I-1,J)	RELX 102
CC = C(I,J) * Q(I,J+1)	RELX 103
DD = D(I,J) * Q(I,J-1)	RELX 104
EE = E(I,J) + G * Q(I,J)	RELX 105
QLAST = Q(I,J)	RELX 106
Q(I,J) = AA + BB + CC + DD + EE	RELX 107
DELSTR = ABS(QLAST - Q(I,J))	RELX 108
40 IF (DELSTR .GT. DEL) DEL = DELSTR	RELX 109
J = NSTAGL	RELX 110
DO 50 I=IMIN,MSTAGL	RELX 111
AA = A(I,J) * Q(I+1,J)	RELX 112
BB = B(I,J) * Q(I-1,J)	RELX 113
CC = C(I,J) * Q(I,J+1)	RELX 114
DD = D(I,J) * Q(I,J-1)	RELX 115
EE = E(I,J) + G * Q(I,J)	RELX 116
QLAST = Q(I,J)	RELX 117
Q(I,J) = AA + BB + CC + DD + EE	RELX 118
DELSTR = ABS(QLAST - Q(I,J))	RELX 119
50 IF (DELSTR .GT. DEL) DEL = DELSTR	RELX 120
DO 60 I=MSTLP2,MSLLP1	
AA = A(I,J) * Q(I+1,J)	

BB = B(I,J) * Q(I-1,J)	RELX 121
CC = C(I,J) * QSLUTL(I)	RELX 122
DD = D(I,J) * Q(I,J-1)	RELX 123
EE = E(I,J) + G * Q(I,J)	RELX 124
QLAST = Q(I,J)	RELX 125
Q(I,J) = AA + BB + CC + DD + EE	RELX 126
DELSTR = ABS(QLAST - Q(I,J))	RELX 127
60 IF (DELSTR .GT. DEL) DEL = DELSTR	RELX 128
J = NSTAGL + 1	RELX 129
DO 70 I=IMIN,MSTLM1	RELX 130
AA = A(I,J) * Q(I+1,J)	RELX 131
BB = B(I,J) * Q(I-1,J)	RELX 132
CC = C(I,J) * Q(I,J+1)	RELX 133
DD = D(I,J) * Q(I,J-1)	RELX 134
EE = E(I,J) + G * Q(I,J)	RELX 135
QLAST = Q(I,J)	RELX 136
Q(I,J) = AA + BB + CC + DD + EE	RELX 137
DELSTR = ABS(QLAST - Q(I,J))	RELX 138
70 IF (DELSTR .GT. DEL) DEL = DELSTR	RELX 139
J = NSTAGL + 2	RELX 140
DO 80 I=IMIN,MSTAGL	RELX 141
AA = A(I,J) * Q(I+1,J)	RELX 142
BB = B(I,J) * Q(I-1,J)	RELX 143
CC = C(I,J) * Q(I,J+1)	RELX 144
DD = D(I,J) * Q(I,J-1)	RELX 145
EE = E(I,J) + G * Q(I,J)	RELX 146
QLAST = Q(I,J)	RELX 147
Q(I,J) = AA + BB + CC + DD + EE	RELX 148
DELSTR = ABS(QLAST - Q(I,J))	RELX 149
80 IF (DELSTR .GT. DEL) DEL = DELSTR	RELX 150
DO 90 I=MSTLP2,IMAX	RELX 151
AA = A(I,J) * Q(I+1,J)	RELX 152
BB = B(I,J) * Q(I-1,J)	RELX 153
CC = C(I,J) * Q(I,J+1)	RELX 154
DD = D(I,J) * Q(I,J-1)	RELX 155
EE = E(I,J) + G * Q(I,J)	RELX 156
QLAST = Q(I,J)	RELX 157
Q(I,J) = AA + BB + CC + DD + EE	RELX 158
DELSTR = ABS(QLAST - Q(I,J))	RELX 159
90 IF (DELSTR .GT. DEL) DEL = DELSTR	RELX 160
DO 100 I=IMIN,IMAX	RELX 161
DO 100 J=NSTLP3,NSTUM1	RELX 162
AA = A(I,J) * Q(I+1,J)	RELX 163
BB = B(I,J) * Q(I-1,J)	RELX 164
CC = C(I,J) * Q(I,J+1)	RELX 165
DD = D(I,J) * Q(I,J-1)	RELX 166
EE = E(I,J) + G * Q(I,J)	RELX 167
QLAST = Q(I,J)	RELX 168
Q(I,J) = AA + BB + CC + DD + EE	RELX 169
DELSTR = ABS(QLAST - Q(I,J))	RELX 170
100 IF (DELSTR .GT. DEL) DEL = DELSTR	RELX 171
C	RELX 172
C	RELX 173
C	RELX 174
110 J = NSTAGU	RELX 175
DO 120 I=IMIN,MSTAGU	RELX 176
AA = A(I,J) * Q(I+1,J)	RELX 177
BB = B(I,J) * Q(I-1,J)	RELX 178
CC = C(I,J) * Q(I,J+1)	RELX 179
DD = D(I,J) * Q(I,J-1)	RELX 180

EE = E(I,J) + G * Q(I,J)	RELX 181
QLAST = Q(I,J)	RELX 182
Q(I,J) = AA + BB + CC + DD + EE	RELX 193
DELSTR = ABS(QLAST - Q(I,J))	RELX 184
120 IF (DELSTR .GT. DEL) DEL = DELSTR	RELX 185
DO 130 I=MSTUP2,IMAX	RELX 186
AA = A(I,J) * Q(I+1,J)	RELX 187
BB = B(I,J) * Q(I-1,J)	RELX 188
CC = C(I,J) * Q(I,J+1)	RELX 189
DD = D(I,J) * Q(I,J-1)	RELX 190
EE = E(I,J) + G * Q(I,J)	RELX 191
QLAST = Q(I,J)	RELX 192
Q(I,J) = AA + BB + CC + DD + EE	RELX 193
DELSTR = ABS(QLAST - Q(I,J))	RELX 194
130 IF (DELSTR .GT. DEL) DEL = DELSTR	RELX 195
J = NSTAGU + 1	RELX 196
DO 140 I=IMIN,MSTUM1	RELX 197
AA = A(I,J) * Q(I+1,J)	RELX 198
BB = B(I,J) * Q(I-1,J)	RELX 199
CC = C(I,J) * Q(I,J+1)	RELX 200
DD = D(I,J) * Q(I,J-1)	RELX 201
EE = E(I,J) + G * Q(I,J)	RELX 202
QLAST = Q(I,J)	RELX 203
Q(I,J) = AA + BB + CC + DD + EE	RELX 204
DELSTR = ABS(QLAST - Q(I,J))	RELX 205
140 IF (DELSTR .GT. DEL) DEL = DELSTR	RELX 206
J = NSTAGU + 2	RELX 207
DO 150 I=IMIN,MSTAGU	RELX 208
AA = A(I,J) * Q(I+1,J)	RELX 209
BB = B(I,J) * Q(I-1,J)	RELX 210
CC = C(I,J) * Q(I,J+1)	RELX 211
DD = D(I,J) * Q(I,J-1)	RELX 212
EE = E(I,J) + G * Q(I,J)	RELX 213
QLAST = Q(I,J)	RELX 214
Q(I,J) = AA + BB + CC + DD + EE	RELX 215
DELSTR = ABS(QLAST - Q(I,J))	RELX 216
150 IF (DELSTR .GT. DEL) DEL = DELSTR	RELX 217
DO 160 I=MSTUP2,MSLUP1	RELX 218
AA = A(I,J) * Q(I+1,J)	RELX 219
BB = B(I,J) * Q(I-1,J)	RELX 220
CC = C(I,J) * Q(I,J+1)	RELX 221
DD = D(I,J) * Q(I,J-1)	RELX 222
EE = E(I,J) + G * Q(I,J)	RELX 223
QLAST = Q(I,J)	RELX 224
Q(I,J) = AA + BB + CC + DD + EE	RELX 225
DELSTR = ABS(QLAST - Q(I,J))	RELX 226
160 IF (DELSTR .GT. DEL) DEL = DELSTR	RELX 227
DO 170 J=NSTUP3,N	RELX 228
DO 170 I=IMIN,MSLUP1	RELX 229
AA = A(I,J) * Q(I+1,J)	RELX 230
BB = B(I,J) * Q(I-1,J)	RELX 231
CC = C(I,J) * Q(I,J+1)	RELX 232
DD = D(I,J) * Q(I,J-1)	RELX 233
EE = E(I,J) + G * Q(I,J)	RELX 234
QLAST = Q(I,J)	RELX 235
Q(I,J) = AA + BB + CC + DD + EE	RELX 236
DELSTR = ABS(QLAST - Q(I,J))	RELX 237
170 IF (DELSTR .GT. DEL) DEL = DELSTR	RELX 238
	RELX 239
	RELX 240

C  
C

CORRECT BOUNDARY CONDITIONS

	DO 180 I=2,MSLUP1	RELX 241
	Y3 = Q(I,NP1)	RELX 242
	Y2 = Q(I,N)	RELX 243
	Y1 = Q(I,NM1)	RELX 244
	D1 = DPSI(NM1)	RELX 245
	D2 = DPSI(N)	RELX 246
	DER = ( Y3 - Y2 ) * ( D1 + D2 ) / ( D1 * D2 )	RELX 247
	DER = DER - ( Y3 - Y1 ) * D2 / ( D1 * D1 + D1 * D2 )	RELX 248
180	Q(I,NP2) = Y2 + 2. * DER * D2	RELX 249
	IF (FLAG1 .LE. 0 .AND. FLAG3 .LE. 0) GO TO 200	RELX 250
	JOT = 2	RELX 251
	DO 190 I=2,MP1	RELX 252
190	Q(I,1) = Q(I,3)	RELX 253
200	IF(FLAG1 .GT. 0 .OR. FLAG3 .GT. 0) GO TO 220	RELX 254
	JOT = NSTLP1	RELX 255
	DO 210 I=2,MSLLP1	RELX 256
	Y3 = Q(I,4)	RELX 257
	Y2 = Q(I,3)	RELX 258
	Y1 = Q(I,2)	RELX 259
	D1 = DPSI(2)	RELX 260
	D2 = DPSI(3)	RELX 261
	DER = ( Y2 - Y1 ) * ( D1 + D2 ) / ( D1 * D2 )	RELX 262
	DER = DER - ( Y3 - Y1 ) * D1 / ( D1 * D2 + D2 * D2 )	RELX 263
210	Q(I,1) = Y2 - 2. * DER * D1	RELX 264
220	DO 230 J=2,NP1	RELX 265
	Y3 = Q(4,J)	RELX 266
	Y2 = Q(3,J)	RELX 267
	Y1 = Q(2,J)	RELX 268
	D1 = DPHI(2)	RELX 269
	D2 = DPHI(3)	RELX 270
	DER = ( Y2 - Y1 ) * ( D1 + D2 ) / ( D1 * D2 )	RELX 271
	DER = DER - ( Y3 - Y1 ) * D1 / ( D1 * D2 + D2 * D2 )	RELX 272
230	Q(1,J) = Y2 - 2. * DER * D1	RELX 273
	DO 240 J=JOT,NSTAGU	RELX 274
	Y3 = Q(MP1,J)	RELX 275
	Y2 = Q(M,J)	RELX 276
	Y1 = Q(MM1,J)	RELX 277
	D1 = DPHI(MM1)	RELX 278
	D2 = DPHI(M)	RELX 279
	DER = ( Y3 - Y2 ) * ( D1 + D2 ) / ( D1 * D2 )	RELX 280
	DER = DER - ( Y3 - Y1 ) * D2 / ( D1 * D1 + D1 * D2 )	RELX 281
240	Q(MP2,J) = Y2 + 2. * DER * D2	RELX 282
	IF (FLAG1 .GT. 0 .OR. FLAG3 .GT. 0) GO TO 260	RELX 283
	DO 250 J=2,NSTAGL	RELX 284
250	Q(MSLLP2,J) = Q(MSLOTL,J)	RELX 285
	QSLOTL(MSLLP2) = QSLOTL(MSLOTL)	RELX 286
260	DO 270 J=NSTUP2,NP1	RELX 287
270	Q(MSLUP2,J) = Q(MSLOTU,J)	RELX 288
	QSLOTU(MSLUP2) = QSLOTU(MSLOTU)	RELX 289
	IF (FLAG3 .LE. 0) GO TO 285	RELX 290
	DO 280 I=2,MP1	RELX 291
280	Q(I,2) = Q(I,3)	RELX 292
285	IF (FLAG2 .LE. 0) GO TO 1000	RELX 293
	IF (FLAG1 .LE. 0 .AND. FLAG3 .LE. 0) GO TO 310	RELX 294
	IF (FLAG2 .EQ. 2 .OR. FLAG2 .EQ. 4) GO TO 295	RELX 295
	DO 290 J=2,NP1	RELX 296
290	Q(1,J) = Q(3,J)	RELX 297
295	IF (FLAG2 .EQ. 3 .OR. FLAG2 .EQ. 4) GO TO 1000	RELX 298
	DO 300 J=2,NSTAGU	RELX 299
		RELX 300

300	Q(MP2,J) = Q(M,J)	RELX 301
	GO TO 1000	RELX 302
310	IF (FLAG2 .EQ. 2 .OR. FLAG2 .EQ. 4) GO TO 325	RELX 303
	DO 320 J=2,NP1	RELX 304
320	Q(1,J) = Q(3,J)	RELX 305
325	IF (FLAG2 .EQ. 3 .OR. FLAG2 .EQ. 4) GO TO 1000	RELX 306
	DO 330 J=NSTLP2,NSTAGU	RELX 307
330	Q(MP2,J) = Q(M,J)	RELX 308
1000	CONTINUE	RELX 309
C		RELX 310
C	CHECK FOR CONVERGENCE	RELX 311
C		RELX 312
	IF (DEL .LE. TOLDE) GO TO 4000	RELX 313
	IF (JTER .LT. II*IPRDE) GO TO 3000	RELX 314
	II = II +1	RELX 315
C		RELX 316
C	OUTPUT Q ARRAY	RELX 317
C		RELX 318
	DO 1010 I=2,MP1	RELX 319
	DO 1010 J=2,NP1	RELX 320
	P = Q(I,J)	RELX 321
1010	Q(I,J) = DEXP(P)	RELX 322
	WRITE(3,1020)HEDR,DATE1,DATE2,DATE3,CASE	RELX 323
1020	FORMAT(1H1//T57,'CLEMSON UNIVERSITY',//T49,	RELX 324
	1'MECHANICAL ENGINEERING DEPARTMENT'///T2,15A4,T64,	RELX 325
	2I2,T66,'//',T67,I2,T69,'//',T70,I2,T76,'CASE NO. ',	RELX 326
	3T87,I4)	RELX 327
C		RELX 328
C	OUTPUT ARRAY	RELX 329
C		RELX 330
	WRITE(3,1030)ITER,JTER,EPS,DEL	RELX 331
1030	FORMAT(///T1,'OVELOCITY THROUGHOUT DIFFUSER - NOZZLE',	RELX 332
	1T46,'ITER = ',T53,I4,T61,'JTER = ',T68,I4,T76,'EPS = '	RELX 333
	2,T82,E13.6,T99,'DEL = ',T105,E13.6,///T7,'PHI',T66,	RELX 334
	3'PSI')	RELX 335
	WRITE(3,1040)(PSI(IP),IP=2,NP1)	RELX 336
1040	FORMAT(///(13X,5(7X,E13.6)))	RELX 337
	DO 1050 I=2,MP1	RELX 338
1050	WRITE(3,1060)PHI(I),(Q(I,J),J=2,NP1)	RELX 339
1060	FORMAT(///1X,E13.6,5(7X,E13.6),/(14X,5(7X,E13.6)))	RELX 340
C		RELX 341
C	CHANGE Q BACK TO LOGARITHMIC FORM	RELX 342
C		RELX 343
	DO 1070 I=2,MP1	RELX 344
	DO 1070 J=2,NP1	RELX 345
	P = Q(I,J)	RELX 346
1070	Q(I,J) = DLOG(P)	RELX 347
	DO 1075 I=2,MP1	RELX 348
	P = QSLOTL(I)	RELX 349
	QSLOTL(I) = DEXP(P)	RELX 350
	P = QSLOTU(I)	RELX 351
1075	QSLOTU(I) = DEXP(P)	RELX 352
C		RELX 353
C	OUTPUT Q VALUES ALONG THE SLOT INNER WALLS	RELX 354
C		RELX 355
	WRITE(3,1020)HEDR,DATE1,DATE2,DATE3,CASE	RELX 356
	WRITE(3,1080)ITER,JTER,EPS,DEL	RELX 357
1080	FORMAT(///T1,'OVELOCITY INSIDE OF SLOTS',	RELX 358
	1T46,'ITER = ',T53,I4,T61,'JTER = ',T68,I4,T76,'EPS = '	RELX 359
	2;T82,E13.6,T99,'DEL = ',T105,E13.6,///T7,'PHI',T66,	RELX 360

	3*PSI*)	RELX 361
	WRITE(3,1040)(PHI(IP),IP=2,MP1)	RELX 362
	IF (FLAG1 .GT. 0 .OR. FLAG3 .GT. 0) GO TO 1100	RELX 363
	WRITE(3,1090)	RELX 364
1090	FORMAT(///T2,'LOWER SLOT')	RELX 365
	WRITE(3,1060)PSI(NSTLP1),(QSLOTL(I),I=2,MP1)	RELX 366
1100	WRITE(3,1110)	RELX 367
1110	FORMAT(///T2,'UPPER SLOT')	RELX 368
	WRITE(3,1060)PSI(NSTUP1),(QSLOTU(I),I=2,MP1)	RELX 369
C		RELX 370
C	CHANGE SLOT VALUES BACK TO LOGARITHMIC FORM	RELX 371
C		RELX 372
	DO 1120 I=2,MP1	RELX 373
	P = QSLOTL(I)	RELX 374
	QSLOTL(I) = DLOG(P)	RELX 375
	P = QSLOTU(I)	RELX 376
1120	QSLOTU(I) = DLOG(P)	RELX 377
3000	CONTINUE	RELX 378
4000	REWIND 4	RELX 379
	WRITE(4)((Q(I,J),I=1,MP2),J=1,MP2)	RELX 380
	RETURN	RELX 381
	END	RELX 382
C	***** SUBROUTINE PART2 *****	PAR2 1
C		PAR2 2
C	THIS SUBROUTINE COMPUTES ALPHA , R AND X ARRAYS	PAR2 3
C	AND COMPUTES THE CHANGE OF THE R ARRAY FROM THE	PAR2 4
C	PREVIOUS ITERATION FOR AXISYMMETRIC COMPUTATIONS	PAR2 5
C		PAR2 6
	SUBROUTINE PART2	PAR2 7
	DIMENSION DX(150),ESIMP(150),FSIMP(150),GSIMP(150),	PAR2 8
1	GRAND(150),GIFT(150),PHI(150),PSI(150),	PAR2 9
2	DPSI(150),DPHI(150),S(150),SBAR(150),	PAR2 10
3	S1(150),SBAR1(150),S2(150),SBAR2(150),	PAR2 11
4	HEDR(15),EPHI(150),FPHI(150),GPHI(150),	PAR2 12
5	EPSI(150),ASLOTL(150),XSLOTU(150),XSLOTL(150)	PAR2 13
6	,FPSI(150),GPSI(150),RSLUTU(150),RSLCTL(150),	PAR2 14
7	QSLOTU(150),QSLOTL(150),ASLOTU(150)	PAR2 15
	DIMENSION Q(150,50),R(150,50),X(150,50),ALPHA(150,50),	PAR2 16
1	R1(150,50)	PAR2 17
	DOUBLE PRECISION P	PAR2 18
	INTEGER FLAG1,FLAG2,FLAG3,FLAG4,CASE,DATE1,DATE2,DATE3	PAR2 19
	COMMON / C1 / IMINSU,IMAXSU,IMINSI,IMAXSI,GRAND,GIFT,	PAR2 20
1	DX,ESIMP,FSIMP,GSIMP	PAR2 21
	COMMON / C2 / FLAG1,FLAG2,FLAG3,FLAG4,HEDR,DATE1,DATE2	PAR2 22
1	,DATE3,CASE,MXIDE,ICKDE,IPRDE,IMIN,IMAX,	PAR2 23
2	JMIN,JMAX,NUT,M,N,TOLDE,DEL,EPS,JTER,	PAR2 24
3	ITER,DPHI,DPSI,S,SBAR,RMULT,S1,S2,SBAR1,	PAR2 25
4	SBAR2,MSTAGU,NSTAGU,MSLOTU,MSTAGL,NSTAGL	PAR2 26
5	,MSLOTL,RADIN,W,PHI,PSI,RSLUTU,RSLCTL,	PAR2 27
6	QSLOTU,QSLOTL,ASLOTU,ASLOTL,XSLOTU,	PAR2 28
7	XSLOTL,G,MIDJ,TOLSYS	PAR2 29
	COMMON / C3 / EPHI,FPHI,GPHI,EPSI,FPSI,GPSI,MXISYS,	PAR2 30
1	IPRSYS	PAR2 31
	REWIND 4	PAR2 32
	REWIND 5	PAR2 33
	REWIND 11	PAR2 34
	REWIND 12	PAR2 35
	NM1 = N - 1	PAR2 36
	NP1 = N + 1	PAR2 37
	MM1 = M - 1	PAR2 38

MP1 = M + 1	PAR2 39
NP2 = N + 2	PAR2 40
MP2 = M + 2	PAR2 41
NM2 = N - 2	PAR2 42
MM2 = M - 2	PAR2 43
MSTUM1 = MSTAGU - 1	PAR2 44
MSTUP1 = MSTAGU + 1	PAR2 45
MSTUP2 = MSTAGU + 2	PAR2 46
MSTUP3 = MSTAGU + 3	PAR2 47
MSTLM1 = MSTAGL - 1	PAR2 48
MSTLP1 = MSTAGL + 1	PAR2 49
MSTLP2 = MSTAGL + 2	PAR2 50
MSTLP3 = MSTAGL + 3	PAR2 51
MSLUP1 = MSL0TU + 1	PAR2 52
MSLLP1 = MSL0TL + 1	PAR2 53
NSTUP1 = NSTAGU + 1	PAR2 54
NSTUP2 = NSTAGU + 2	PAR2 55
NSTLP1 = NSTAGL + 1	PAR2 56
NSTLP2 = NSTAGL + 2	PAR2 57
READ(4)((Q(I,J),I=1,MP2),J=1,NP2)	PAR2 58
READ(5)((R(I,J),I=1,MP2),J=1,NP2)	PAR2 59
READ(12)((X(I,J),I=1,MP2),J=1,NP2)	PAR2 60
C	PAR2 61
C	PAR2 62
C	PAR2 63
DO 5 I=1,MP1	PAR2 64
ASLOTU(I) = 1.0	PAR2 65
5 ASLOTL(I) = 1.0	PAR2 66
DO 10 I=2,MM1	PAR2 67
ESIMP(I) = EPHI(I)	PAR2 68
FSIMP(I) = FPHI(I)	PAR2 69
10 GSIMP(I) = GPHI(I)	PAR2 70
K = 2	PAR2 71
IF (FLAG1 .LE. 0 .AND. FLAG3 .LE. 0) K = MIDJ + 1	PAR2 72
J = K	PAR2 73
D1 = DPSI(J-1)	PAR2 74
D2 = DPSI(J)	PAR2 75
DO 20 I=2,MP1	PAR2 76
DER = D1 * Q(I,J+1) / ( D2 * D1 + D2 * D2 )	PAR2 77
DER = DER - D2 * Q(I,J-1) / ( D1 * D1 + D1 * D2 )	PAR2 78
DER = DER - ( D1 - D2 ) * Q(I,J) / ( D1 * D2 )	PAR2 79
20 GRAND(I) = R(I,J) * DER	PAR2 80
IMINSI = 2	PAR2 81
IMAXSI = MP1	PAR2 82
DO 30 I=2,MP1	PAR2 83
30 DX(I) = DPHI(I)	PAR2 84
CALL SIMP	PAR2 85
DO 40 I=2,MP1	PAR2 86
40 ALPHA(I,J) = GIFT(I)	PAR2 87
C	PAR2 88
C	PAR2 89
C	PAR2 90
JOT = 2	PAR2 91
IF (FLAG3 .GT. 0) JOT = 3	PAR2 92
DO 70 I=2,MP1	PAR2 93
D1 = DPHI(I-1)	PAR2 94
D2 = DPHI(I)	PAR2 95
DO 70 J=JCT,NP1	PAR2 96
DER = D1 * Q(I+1,J) / ( D2 * D1 + D2 * D2 )	PAR2 97
DER = DER - D2 * Q(I-1,J) / ( D1 * D1 + D1 * D2 )	PAR2 98



DER = DER - ( D1 - D2 ) * Q(I,J) / ( D1 * D2 )	PAR2 99
R1(I,J) = - DER / R(I,J)	PAR2 100
DER = D1 * R(I+1,J) / ( D2 * D1 + D2 * D2 )	PAR2 101
DER = DER - D2 * R(I-1,J) / ( D1 * D1 + D1 * D2 )	PAR2 102
DER = DER - ( D1 - D2 ) * R(I,J) / ( D1 * D2 )	PAR2 103
70 R1(I,J) = - DER / ( R(I,J) * R(I,J) ) + R1(I,J)	PAR2 104
IF (FLAG3 .LE. 0) GO TO 60	PAR2 105
DO 50 I=2,MP1	PAR2 106
50 R1(I,2) = 0.0	PAR2 107
60 CONTINUE	PAR2 108
C	PAR2 109
C	PAR2 110
C	PAR2 111
COMPUTE ALPHAS IN THE UPPER PORTION OF THE DIFFUSER	PAR2 112
I = MSTAGU	PAR2 113
J = NSTUP1	PAR2 114
D1 = DPHI(I-1)	PAR2 115
D2 = DPHI(I)	PAR2 116
DER = ( Q(I,J) - Q(I-1,J) ) / D1	PAR2 117
R1(I,J) = - DER / R(I,J)	PAR2 118
DER = D1 * R(I+1,J) / ( D2 * D1 + D2 * D2 )	PAR2 119
DER = DER - D2 * R(I-1,J) / ( D1 * D1 + D1 * D2 )	PAR2 120
DER = DER - ( D1 - D2 ) * R(I,J) / ( D1 * D2 )	PAR2 121
R1(I,J) = - DER / ( R(I,J) * R(I,J) ) + R1(I,J)	PAR2 122
I = MSTUP2	PAR2 123
J = NSTUP1	PAR2 124
D1 = DPHI(I-1)	PAR2 125
D2 = DPHI(I)	PAR2 126
DER = ( Q(I+1,J) - Q(I,J) ) / D2	PAR2 127
R1(I,J) = - DER / R(I,J)	PAR2 128
DER = D1 * R(I+1,J) / ( D2 * D1 + D2 * D2 )	PAR2 129
DER = DER - D2 * R(I-1,J) / ( D1 * D1 + D1 * D2 )	PAR2 130
DER = DER - ( D1 - D2 ) * R(I,J) / ( D1 * D2 )	PAR2 131
R1(I,J) = - DER / ( R(I,J) * R(I,J) ) + R1(I,J)	PAR2 132
IF ( FLAG1 .GT. 0 .OR. FLAG3 .GT. 0 ) GO TO 80	PAR2 133
I = MSTAGL	PAR2 134
J = NSTLP1	PAR2 135
D1 = DPHI(I-1)	PAR2 136
D2 = DPHI(I)	PAR2 137
DER = ( Q(I,J) - Q(I-1,J) ) / D1	PAR2 138
R1(I,J) = - DER / R(I,J)	PAR2 139
DER = D1 * R(I+1,J) / ( D2 * D1 + D2 * D2 )	PAR2 140
DER = DER - D2 * R(I-1,J) / ( D1 * D1 + D1 * D2 )	PAR2 141
DER = DER - ( D1 - D2 ) * R(I,J) / ( D1 * D2 )	PAR2 142
R1(I,J) = - DER / ( R(I,J) * R(I,J) ) + R1(I,J)	PAR2 143
I = MSTLP2	PAR2 144
J = NSTLP1	PAR2 145
D1 = DPHI(I-1)	PAR2 146
D2 = DPHI(I)	PAR2 147
DER = ( Q(I+1,J) - Q(I,J) ) / D2	PAR2 148
R1(I,J) = - DER / R(I,J)	PAR2 149
DER = D1 * R(I+1,J) / ( D2 * D1 + D2 * D2 )	PAR2 150
DER = DER - D2 * R(I-1,J) / ( D1 * D1 + D1 * D2 )	PAR2 151
DER = DER - ( D1 - D2 ) * R(I,J) / ( D1 * D2 )	PAR2 152
R1(I,J) = - DER / ( R(I,J) * R(I,J) ) + R1(I,J)	PAR2 153
80 DO 90 J=2,NM1	PAR2 154
ESIMP(J) = EPSI(J)	PAR2 155
FSIMP(J) = FPSI(J)	PAR2 156
90 GSIMP(J) = GPSI(J)	PAR2 157
DO 100 J=2,NP1	PAR2 158
100 DX(J) = DPSI(J)	

	IMINSI = K	PAR2 159
	IMAXSI = NP1	PAR2 160
	DO 120 I=2,MP1	PAR2 161
	DO 110 J=K,NP1	PAR2 162
110	GRAND(J) = R1(I,J)	PAR2 163
	IF (I .GT. MSTUP1) GRAND(NSTUP2) = GRAND(NSTAGU)	PAR2 164
	CALL SIMP	PAR2 165
	TEMP = ALPHA(I,K)	PAR2 166
	DO 120 J=K,NP1	PAR2 167
120	ALPHA(I,J) = GIFT(J) + TEMP	PAR2 168
C		PAR2 169
C	COMPUTE ALPHAS IN UPPER SLOT	PAR2 170
C		PAR2 171
	DO 150 I=2,MM1	PAR2 172
	ESIMP(I) = EPHI(I)	PAR2 173
	FSIMP(I) = FPHI(I)	PAR2 174
150	GSIMP(I) = GPHI(I)	PAR2 175
	DO 160 I=2,MP1	PAR2 176
160	DX(I) = DPHI(I)	PAR2 177
	IMINSI = MSTUM1	PAR2 178
	IMAXSI = MSLUP1	PAR2 179
	J = NP1	PAR2 180
	D1 = DPSI(N)	PAR2 181
	D2 = D1	PAR2 182
	DO 170 I=MSTUM1,MSLUP1	PAR2 183
	DER = D1 * Q(I,J+1) / ( D2 * D1 + D2 * D2 )	PAR2 184
	DER = DER - D2 * Q(I,J-1) / ( D1 * D1 + D1 * D2 )	PAR2 185
	DER = DER - ( D1 - D2 ) * Q(I,J) / ( D1 * D2 )	PAR2 186
170	GRAND(I) = R(I,J) * DER	PAR2 187
	CALL SIMP	PAR2 188
	DO 180 I=MSTAGU,MSLUP1	PAR2 189
180	ALPHA(I,J) = ALPHA(MSTUM1,J) + GIFT(I)	PAR2 190
	I = MSTUP2	PAR2 191
	J = NSTUP1	PAR2 192
	D1 = DPHI(I-1)	PAR2 193
	D2 = DPHI(I)	PAR2 194
	DER = ( QSLOTU(I+1) - QSLOTU(I) ) / D2	PAR2 195
	R1(I,J) = - DER / RSLOTU(I)	PAR2 196
	DER = D1 * RSLOTU(I+1) / ( D2 * D1 + D2 * D2 )	PAR2 197
	DER = DER - D2 * RSLOTU(I-1) / ( D1 * D1 + D1 * D2 )	PAR2 198
	DER = DER - ( D1 - D2 ) * RSLOTU(I) / ( D1 * D2 )	PAR2 199
	R1(I,J) = - DER / ( RSLOTU(I) * RSLOTU(I) ) + R1(I,J)	PAR2 200
	DO 190 I=MSTUP3,MSLUP1	PAR2 201
	D1 = DPHI(I-1)	PAR2 202
	D2 = DPHI(I)	PAR2 203
	DER = D1 * QSLOTU(I+1) / ( D2 * D1 + D2 * D2 )	PAR2 204
	DER = DER - D2 * QSLOTU(I-1) / ( D1 * D1 + D1 * D2 )	PAR2 205
	DER = DER - ( D1 - D2 ) * QSLOTU(I) / ( D1 * D2 )	PAR2 206
	R1(I,J) = - DER / RSLOTU(I)	PAR2 207
	DER = D1 * RSLOTU(I+1) / ( D2 * D1 + D2 * D2 )	PAR2 208
	DER = DER - D2 * RSLOTU(I-1) / ( D1 * D1 + D1 * D2 )	PAR2 209
	DER = DER - ( D1 - D2 ) * RSLOTU(I) / ( D1 * D2 )	PAR2 210
190	R1(I,J) = - DER / ( RSLOTU(I) * RSLOTU(I) ) + R1(I,J)	PAR2 211
	DO 200 J=2,NM1	PAR2 212
	ESIMP(J) = EPSI(J)	PAR2 213
	FSIMP(J) = FPSI(J)	PAR2 214
200	GSIMP(J) = GPSI(J)	PAR2 215
	DO 205 J=2,N	PAR2 216
205	DX(J) = DPSI(J)	PAR2 217
	IMINSI = NSTUP1	PAR2 218

	IMAXSI = NP1	PAR2 219
	DO 220 I=MSTAGU,MSLUP1	PAR2 220
	DO 210 J=NSTUP1,NP1	PAR2 221
210	GRAND(J) = R1(I,J)	PAR2 222
	CALL SIMP	PAR2 223
	TEMP = ALPHA(I,NP1) - GIFT(NP1)	PAR2 224
	DO 215 J=NSTUP2,NP1	PAR2 225
215	ALPHA(I,J) = GIFT(J) + TEMP	PAR2 226
220	ASLOTU(I) = GIFT(NSTUP1) + TEMP	PAR2 227
	I = MSTUP1	PAR2 228
	J = NSTUP1	PAR2 229
	ALPHA(I,J) = ASLOTU(I)	PAR2 230
C		PAR2 231
C	COMPUTE ALPHAS IN LOWER PORTION OF DIFFUSER	PAR2 232
C		PAR2 233
	IF ( FLAG1 .GT. 0 .OR. FLAG3 .GT. 0 ) GO TO 400	PAR2 234
	DO 240 I=2,MSTAGL	PAR2 235
	DO 230 J=2,K	PAR2 236
230	GRAND(J) = R1(I,J)	PAR2 237
	KM1 = K - 1	PAR2 238
	IMINSI = 2	PAR2 239
	IMAXSI = K	PAR2 240
	CALL SIMP	PAR2 241
	TEMP = ALPHA(I,K) - GIFT(K)	PAR2 242
	DO 240 J=2,KM1	PAR2 243
240	ALPHA(I,J) = GIFT(J) + TEMP	PAR2 244
	I = MSTLP1	PAR2 245
	DO 260 J=NSTLP2,K	PAR2 246
260	GRAND(J) = R1(I,J)	PAR2 247
	IMINSI = NSTLP2	PAR2 248
	IMAXSI = K	PAR2 249
	CALL SIMP	PAR2 250
	TEMP = ALPHA(I,K) - GIFT(K)	PAR2 251
	DO 270 J=NSTLP2,KM1	PAR2 252
270	ALPHA(I,J) = GIFT(J) + TEMP	PAR2 253
	IMINSI = NSTLP1	PAR2 254
	IMAXSI = K	PAR2 255
	DO 300 I=MSTLP2,MP1	PAR2 256
	DO 290 J=NSTLP1,K	PAR2 257
290	GRAND(J) = R1(I,J)	PAR2 258
	CALL SIMP	PAR2 259
	TEMP = ALPHA(I,K) - GIFT(K)	PAR2 260
	DO 300 J=NSTLP1,KM1	PAR2 261
300	ALPHA(I,J) = GIFT(J) + TEMP	PAR2 262
C		PAR2 263
C	COMPUTE ALPHAS INSIDE LOWER SLOT	PAR2 264
C		PAR2 265
	DO 310 I=2,MM1	PAR2 266
	ESIMP(I) = EPHI(I)	PAR2 267
	FSIMP(I) = FPHI(I)	PAR2 268
310	GSIMP(I) = GPHI(I)	PAR2 269
	DO 320 I=2,MP1	PAR2 270
320	DX(I) = DPHI(I)	PAR2 271
	IMINSI = MSTLM1	PAR2 272
	IMAXSI = MSLLP1	PAR2 273
	J = 2	PAR2 274
	D1 = DPSI(2)	PAR2 275
	D2 = D1	PAR2 276
	DO 330 I=MSTLM1,MSLLP1	PAR2 277
	DER = D1 * Q(I,J+1) / ( D2 * D1 + D2 * D2)	PAR2 278

	DER = DER - D2 * Q(I,J-1) / ( D1 * D1 + D1 * D2 )	PAR2 279
	DER = DER - ( D1 - D2 ) * Q(I,J) / ( D1 * D2 )	PAR2 280
330	GRAND(I) = R(I,J) * DER	PAR2 281
	CALL SIMP	PAR2 282
	DO 340 I=MSTAGL,MSLLP1	PAR2 283
340	ALPHA(I,J) = ALPHA(MSTLM1,J) + GIFT(I)	PAR2 284
	I = MSTLP2	PAR2 285
	J = NSTUP1	PAR2 286
	D1 = DPHI(I-1)	PAR2 287
	D2 = DPHI(I)	PAR2 288
	DER = ( QSLOTL(I+1) - QSLOTL(I) ) / D2	PAR2 289
	R1(I,J) = - DER / RSLOTL(I)	PAR2 290
	DER = D1 * RSLOTL(I+1) / ( D2 * D1 + D2 * D2 )	PAR2 291
	DER = DER - D2 * RSLOTL(I-1) / ( D1 * D1 + D1 * D2 )	PAR2 292
	DER = DER - ( D1 - D2 ) * RSLOTL(I) / ( D1 * D2 )	PAR2 293
	R1(I,J) = - DER / ( RSLOTL(I) * RSLOTL(I) ) + R1(I,J)	PAR2 294
	DO 350 I=MSTLP3,MSLLP1	PAR2 295
	D1 = DPHI(I-1)	PAR2 296
	D2 = DPHI(I)	PAR2 297
	DER = D1 * QSLOTL(I+1) / ( D2 * D1 + D2 * D2 )	PAR2 298
	DER = DER - D2 * QSLOTL(I-1) / ( D1 * D1 + D1 * D2 )	PAR2 299
	DER = DER - ( D1 - D2 ) * QSLOTL(I) / ( D1 * D2 )	PAR2 300
	R1(I,J) = - DER / RSLOTL(I)	PAR2 301
	DER = D1 * RSLOTL(I+1) / ( D2 * D1 + D2 * D2 )	PAR2 302
	DER = DER - D2 * RSLOTL(I-1) / ( D1 * D1 + D1 * D2 )	PAR2 303
	DER = DER - ( D1 - D2 ) * RSLOTL(I) / ( D1 * D2 )	PAR2 304
350	R1(I,J) = - DER / ( RSLOTL(I) * RSLOTL(I) ) + R1(I,J)	PAR2 305
	DO 360 J=2,NM1	PAR2 306
	ESIMP(J) = EPSI(J)	PAR2 307
	FSIMP(J) = FPSI(J)	PAR2 308
360	GSIMP(J) = GPSI(J)	PAR2 309
	DO 370 J=2,N	PAR2 310
370	DX(J) = DPSI(J)	PAR2 311
	IMINSI = 2	PAR2 312
	IMAXSI = NSTLP1	PAR2 313
	DO 390 I=MSTAGL,MSLLP1	PAR2 314
	DO 380 J=2,NSTLP1	PAR2 315
380	GRAND(J) = R1(I,J)	PAR2 316
	CALL SIMP	PAR2 317
	DO 385 J=3,NSTAGL	PAR2 318
385	ALPHA(I,J) = ALPHA(I,2) + GIFT(J)	PAR2 319
390	ASLOTL(I) = GIFT(NSTLP1) + ALPHA(I,2)	PAR2 320
	I = MSTAGL	PAR2 321
	J = NSTLP1	PAR2 322
	ALPHA(I,J) = ASLOTL(I)	PAR2 323
	ALPHA(I+1,J) = ALPHA(I,J)	PAR2 324
400	CONTINUE	PAR2 325
C		PAR2 326
C	COMPUTE INLET R COORDINATES	PAR2 327
C		PAR2 328
	DO 410 J=2,NM1	PAR2 329
	ESIMP(J) = EPSI(J)	PAR2 330
	FSIMP(J) = FPSI(J)	PAR2 331
410	GSIMP(J) = GPSI(J)	PAR2 332
	DO 420 J=2,N	PAR2 333
420	DX(J) = DPSI(J)	PAR2 334
	IMINSI = 2	PAR2 335
	IMAXSI = NP1	PAR2 336
	IF (RADIN .GT. 0.0) R(2,2) = RADIN	PAR2 337
	IF (FLAG1 .GT. 0 .OR. FLAG3 .GT. 0) R(2,2) = 0.0	PAR2 338

	DO 430 J=2,NP1	PAR2 339
	P= Q(2,J)	PAR2 340
43C	GRAND(J) = 2. * COS(ALPHA(2,J)) / DEXP(P)	PAR2 341
	CALL SIMP	PAR2 342
	POW = .5	PAR2 343
	DIV = 1.0	PAR2 344
	IF (FLAG1 .GT. 0) POW = 1.0	PAR2 345
	IF (FLAG1 .GT. 0) DIV = 2.0	PAR2 346
	DO 440 J=3,NP1	PAR2 347
	RAT = ABS( GIFT(J) / DIV + R(2,2) * R(2,2) )	PAR2 348
44C	R(2,J) = ( RAT )**POW	PAR2 349
C		PAR2 350
C	COMPUTE R ALONG MIDDLE STREAMLINE	PAR2 351
C		PAR2 352
	DO 450 I=2,MM1	PAR2 353
	ESIMP(I) = EPHI(I)	PAR2 354
	FSIMP(I) = FPHI(I)	PAR2 355
450	GSIMP(I) = GPHI(I)	PAR2 356
	DO 460 I=2,M	PAR2 357
460	DX(I) = DPHI(I)	PAR2 358
	IMINSI = 2	PAR2 359
	IMAXSI = MP1	PAR2 360
	J = K	PAR2 361
	DO 470 I=2,MP1	PAR2 362
	P = Q(I,J)	PAR2 363
470	GRAND(I) = SIN(ALPHA(I,J)) / DEXP(P)	PAR2 364
	CALL SIMP	PAR2 365
	DO 480 I=3,MP1	PAR2 366
480	R(I,J) = R(2,J) + GIFT(I)	PAR2 367
C		PAR2 368
C	COMPUTE R THROUGHOUT UPPER PORTION OF DIFFUSER	PAR2 369
C		PAR2 370
	DO 490 J=2,NM1	PAR2 371
	ESIMP(J) = EPSI(J)	PAR2 372
	FSIMP(J) = FPSI(J)	PAR2 373
490	GSIMP(J) = GPSI(J)	PAR2 374
	DO 500 J=2,N	PAR2 375
500	DX(J) = DPSI(J)	PAR2 376
	IMINSI = K	PAR2 377
	IMAXSI = NP1	PAR2 378
	DO 520 I=3,MP1	PAR2 379
	DO 510 J=K,NP1	PAR2 380
	P = Q(I,J)	PAR2 381
510	GRAND(J) = 2. * COS(ALPHA(I,J)) / DEXP(P)	PAR2 382
	IF (I .GT. MSTUP1) GRAND(NSTUP2) = GRAND(NSTAGU)	PAR2 383
	CALL SIMP	PAR2 384
	KP1 = K + 1	PAR2 385
	DO 520 J= KP1,NP1	PAR2 386
	RAT = ABS( GIFT(J) / DIV + R(I,K) * R(I,K) )	PAR2 387
520	R(I,J) = ( RAT )**POW	PAR2 388
C		PAR2 389
C	COMPUTE R COORDINATES INSIDE UPPER SLOT	PAR2 390
C		PAR2 391
560	DO 570 I=2,MM1	PAR2 392
	ESIMP(I) = EPHI(I)	PAR2 393
	FSIMP(I) = FPHI(I)	PAR2 394
570	GSIMP(I) = GPHI(I)	PAR2 395
	DO 580 I=2,M	PAR2 396
580	DX(I) = DPHI(I)	PAR2 397
	IMINSI = MSTUM1	PAR2 398

IMAXSI = MSLUP1	PAR2 399
J = NP1	PAR2 400
DO 590 I=MSTUM1,MSLUP1	PAR2 401
P = Q(I,J)	PAR2 402
590 GRAND(I) = SIN(ALPHA(I,J)) / DEXP(P)	PAR2 403
CALL SIMP	PAR2 404
DO 600 I=MSTAGU,MSLUP1	PAR2 405
600 R(I,J) = R(MSTUM1,J) + GIFT(I)	PAR2 406
DO 605 J=2,NM1	PAR2 407
ESIMP(J) = EPSI(J)	PAR2 408
FSIMP(J) = FPSI(J)	PAR2 409
605 GSIMP(J) = GPSI(J)	PAR2 410
DO 610 J=2,N	PAR2 411
610 DX(J) = DPSI(J)	PAR2 412
IMINSI = NSTUP1	PAR2 413
IMAXSI = NP1	PAR2 414
DO 650 I=MSTAGU,MSLUP1	PAR2 415
DO 620 J=NSTUP2,NP1	PAR2 416
P = Q(I,J)	PAR2 417
620 GRAND(J) = 2. * COS(ALPHA(I,J)) / DEXP(P)	PAR2 418
P = QSL0TU(I)	PAR2 419
GRAND(NSTUP1) = 2. * COS(ASLOTU(I)) / DEXP(P)	PAR2 420
CALL SIMP	PAR2 421
TEMP = R(I,NP1) * R(I,NP1) - GIFT(NP1)	PAR2 422
DO 630 J=NSTUP2,N	PAR2 423
630 R(I,J) = ( ABS( GIFT(J) + TEMP ) )**0.5	PAR2 424
RSLOTU(I) = ( ABS( GIFT(NSTUP1) + TEMP ) )**0.5	PAR2 425
IF (FLAG1 .LE. 0) GO TO 650	PAR2 426
TEMP = R(I,NP1) - GIFT(NP1) / 2.	PAR2 427
DO 640 J=NSTUP2,N	PAR2 428
640 R(I,J) = GIFT(J) / 2. + TEMP	PAR2 429
RSLOTU(I) = GIFT(NSTUP1) / 2. + TEMP	PAR2 430
650 CONTINUE	PAR2 431
I = MSTUP1	PAR2 432
J = NSTUP1	PAR2 433
P = Q(I-1,J)	PAR2 434
R(I,J) = R(I-1,J) + SIN(ALPHA(I-1,J)) * DPHI(I-1) / DEXP(P)	PAR2 435
C	PAR2 436
COMPUTE R OVER LOWER PORTION OF DIFFUSER	PAR2 437
C	PAR2 438
IF (FLAG1 .GT. 0 .OR. FLAG3 .GT. 0) GO TO 840	PAR2 439
DO 670 I=2,MSTAGL	PAR2 440
DO 655 J=2,K	PAR2 441
P = Q(I,J)	PAR2 442
655 GRAND(J) = 2. * COS(ALPHA(I,J)) / DEXP(P)	PAR2 443
IMINSI = 2	PAR2 444
IMAXSI = K	PAR2 445
CALL SIMP	PAR2 446
TEMP = R(I,K) * R(I,K) - GIFT(K)	PAR2 447
DO 660 J=2,KM1	PAR2 448
660 R(I,J) = ( ABS( GIFT(J) + TEMP ) )**0.5	PAR2 449
670 CONTINUE	PAR2 450
I = MSTLP1	PAR2 451
DO 675 J=NSTLP2,K	PAR2 452
P = Q(I,J)	PAR2 453
675 GRAND(J) = 2. * COS(ALPHA(I,J)) / DEXP(P)	PAR2 454
IMINSI = NSTLP2	PAR2 455
IMAXSI = K	PAR2 456
CALL SIMP	PAR2 457
TEMP = R(I,K) * R(I,K) - GIFT(K)	PAR2 458

DO 680 J=NSTLP2,KM1	PAR2 459
680 R(I,J) = ( ABS( GIFT(J) + TEMP ) )**0.5	PAR2 460
690 CONTINUE	PAR2 461
DO 702 I=MSTLP2,MP1	PAR2 462
DO 695 J=NSTLP1,K	PAR2 463
P = Q(I,J)	PAR2 464
695 GRAND(J) = 2. * COS(ALPHA(I,J) ) / DEXP(P)	PAR2 465
IMINSI = NSTLP1	PAR2 466
IMAXSI = K	PAR2 467
CALL SIMP	PAR2 468
TEMP = R(I,K) * R(I,K) - GIFT(K)	PAR2 469
DO 697 J=NSTLP1,KM1	PAR2 470
697 R(I,J) = ( ABS( GIFT(J) + TEMP ) )**0.5	PAR2 471
702 CONTINUE	PAR2 472
C	PAR2 473
COMPUTE R INSIDE LOWER SLOTS	PAR2 474
C	PAR2 475
DO 740 I=2,MM1	PAR2 476
ESIMP(I) = EPHI(I)	PAR2 477
FSIMP(I) = FPHI(I)	PAR2 478
740 GSIMP(I) = GPHI(I)	PAR2 479
DO 750 I=2,M	PAR2 480
750 DX(I) = DPHI(I)	PAR2 481
DO 760 I=MSTLM1,MSLLP1	PAR2 482
P = Q(I,2)	PAR2 483
760 GRAND(I) = SIN(ALPHA(I,2)) / DEXP(P)	PAR2 484
IMINSI = MSTLM1	PAR2 485
IMAXSI = MSLLP1	PAR2 486
CALL SIMP	PAR2 487
DO 770 I=MSTAGL,MSLLP1	PAR2 488
770 R(I,2) = R(MSTLM1,2) + GIFT(I)	PAR2 489
DO 780 J=2,NM1	PAR2 490
ESIMP(J) = EPSI(J)	PAR2 491
FSIMP(J) = FPSI(J)	PAR2 492
780 GSIMP(J) = GPSI(J)	PAR2 493
DO 790 J=2,N	PAR2 494
790 DX(J) = DPSI(J)	PAR2 495
IMINSI = 2	PAR2 496
IMAXSI = NSTLP1	PAR2 497
DO 830 I=MSTAGL,MSLLP1	PAR2 498
DO 800 J=2,NSTAGL	PAR2 499
P = Q(I,J)	PAR2 500
800 GRAND(J) = 2. * COS(ALPHA(I,J)) / DEXP(P)	PAR2 501
P = QSLOTL(I)	PAR2 502
GRAND(NSTLP1) = 2. * COS(ASLOTL(I)) / DEXP(P)	PAR2 503
CALL SIMP	PAR2 504
DO 810 J=3,NSTAGL	PAR2 505
RAT = ABS( GIFT(J) + R(I,2) * R(I,2) )	PAR2 506
810 R(I,J) = ( RAT )**0.5	PAR2 507
RAT = ABS( GIFT(NSTLP1) + R(I,2) * R(I,2) )	PAR2 508
RSLOTL(I) = ( RAT )**0.5	PAR2 509
IF (FLAG1 .GT. 0) GO TO 830	PAR2 510
DO 820 J=3,NSTAGL	PAR2 511
820 R(I,J) = R(I,2) + GIFT(J) / 2.	PAR2 512
RSLOTL(I) = R(I,2) + GIFT(NSTLP1) / 2.	PAR2 513
830 CONTINUE	PAR2 514
I = MSTLP1	PAR2 515
J = NSTLP1	PAR2 516
P = Q(I-1,J)	PAR2 517
R(I,J) = R(I-1,J) + SIN(ALPHA(I-1,J)) * DPHI(I-1) / DEXP(P)	PAR2 518

	R(I-1,J) = RSLCTL(I-1)	PAR2 519
840	CONTINUE	PAR2 520
C		PAR2 521
C	COMPUTE CONVERGENCE CRITERION	PAR2 522
C		PAR2 523
	REWIND 5	PAR2 524
	READ(5)((R1(I,J),I=1,MP2),J=1,NP2)	PAR2 525
	EPS = 0.0	PAR2 526
	DO 845 J=2,NP1	PAR2 527
	DO 845 I=2,MP1	PAR2 528
	EPSTR = ABS(R1(I,J) - R(I,J))	PAR2 529
	IF (EPSTR .LE. EPS) GO TO 845	PAR2 530
	EPS = EPSTR	PAR2 531
845	CONTINUE	PAR2 532
C		PAR2 533
C	COMPUTE INLET X COORDINATES	PAR2 534
C		PAR2 535
	IF (ITER .LT. MXISYS .AND. EPS .GT. TOLSYS) GO TO 3000	PAR2 536
	DO 848 I=1,MP1	PAR2 537
	XSLOTU(I) = 1.0	PAR2 538
848	XSLOTL(I) = 1.0	PAR2 539
	DO 850 J=2,NM1	PAR2 540
	ESIMP(J) = EPSI(J)	PAR2 541
850	GSIMP(J) = GPSI(J)	PAR2 542
	FSIMP(J) = FPSI(J)	PAR2 543
	DO 860 J=2,N	PAR2 544
860	DX(J) = DPSI(J)	PAR2 545
	IMINSI = 2	PAR2 546
	IMAXSI = NP1	PAR2 547
	JOT = 2	PAR2 548
	IF (FLAG3 .GT. 0) JOT = 3	PAR2 549
	DO 870 J=JOT,NP1	PAR2 550
	P = Q(2,J)	PAR2 551
	GRAND(J) = - SIN(ALPHA(2,J)) / DEXP(P)	PAR2 552
870	IF (FLAG1 .LE. 0) GRAND(J) = GRAND(J) / R(2,J)	PAR2 553
	IF (FLAG3 .GT. 0) GRAND(2) = 0.0	PAR2 554
	CALL SIMP	PAR2 555
	DO 880 J=2,NP1	PAR2 556
880	X(2,J) = GIFT(J)	PAR2 557
C		PAR2 558
C	COMPUTE X ALONG THE MIDDLE STREAMLINE	PAR2 559
C		PAR2 560
	DO 890 I=2,MM1	PAR2 561
	ESIMP(I) = EPHI(I)	PAR2 562
	FSIMP(I) = FPHI(I)	PAR2 563
890	GSIMP(I) = GPHI(I)	PAR2 564
	DO 900 I=2,M	PAR2 565
900	DX(I) = DPHI(I)	PAR2 566
	IMINSI = 2	PAR2 567
	IMAXSI = MP1	PAR2 568
	J = K	PAR2 569
	DO 910 I=2,MP1	PAR2 570
	P = Q(I,J)	PAR2 571
910	GRAND(I) = COS(ALPHA(I,J)) / DEXP(P)	PAR2 572
	CALL SIMP	PAR2 573
	DO 920 I=3,MP1	PAR2 574
920	X(I,J) = X(2,J) + GIFT(I)	PAR2 575
C		PAR2 576
C	COMPUTE X THROUGHOUT UPPER PORTION OF DIFFUSER	PAR2 577
C		PAR2 578



DO 930 J=2,NM1	PAR2 579
ESIMP(J) = EPSI(J)	PAR2 580
FSIMP(J) = FPSI(J)	PAR2 581
930 GSIMP(J) = GPSI(J)	PAR2 582
DO 940 J=2,N	PAR2 583
940 DX(J) = DPSI(J)	PAR2 584
IMINSI = K	PAR2 585
IMAXSI = NP1	PAR2 586
JET = K	PAR2 586
IF (FLAG3 .GT. 0) JET = 3	PAR2 586
DO 960 I=3,MP1	PAR2 587
DO 950 J=JET,NP1	PAR2 588
P = Q(I,J)	PAR2 589
GRAND(J) = - SIN(ALPHA(I,J)) / DEXP(P)	PAR2 590
950 IF (FLAG1 .LE. 0) GRAND(J) = GRAND(J) / R(I,J)	PAR2 591
IF (FLAG3 .GT. 0) GRAND(2) = 0.0	PAR2 592
IF (I .GT. MSTUP1) GRAND(NSTUP2) = GRAND(NSTAGU)	PAR2 593
CALL SIMP	PAR2 594
KP1 = K + 1	PAR2 595
DO 960 J=KP1,NP1	PAR2 596
960 X(I,J) = X(I,K) + GIFT(J)	PAR2 597
C	PAR2 598
C	PAR2 599
C	PAR2 600
DO 990 I=2,MM1	PAR2 601
ESIMP(I) = EPHI(I)	PAR2 602
FSIMP(I) = FPHI(I)	PAR2 603
990 GSIMP(I) = GPHI(I)	PAR2 604
DO 1000 I=2,M	PAR2 605
1000 DX(I) = DPHI(I)	PAR2 606
IMINSI = MSTUM1	PAR2 607
IMAXSI = MSLUP1	PAR2 608
J = NP1	PAR2 609
DO 1010 I=MSTUM1,MSLUP1	PAR2 610
P = Q(I,J)	PAR2 611
1010 GRAND(I) = COS(ALPHA(I,J)) / DEXP(P)	PAR2 612
CALL SIMP	PAR2 613
DO 1020 I=MSTAGU,MSLUP1	PAR2 614
1020 X(I,J) = X(MSTUM1,J) + GIFT(I)	PAR2 615
DO 1030 J=2,NM1	PAR2 616
ESIMP(J) = EPSI(J)	PAR2 617
FSIMP(J) = FPSI(J)	PAR2 618
1030 GSIMP(J) = GPSI(J)	PAR2 619
DO 1035 J=2,N	PAR2 620
1035 DX(J) = DPSI(J)	PAR2 621
IMINSI = NSTUP1	PAR2 622
IMAXSI = NP1	PAR2 623
DO 1060 I=MSTAGU,MSLUP1	PAR2 624
DO 1040 J=NSTUP2,NP1	PAR2 625
P = Q(I,J)	PAR2 626
GRAND(J) = - SIN(ALPHA(I,J)) / DEXP(P)	PAR2 627
1040 IF (FLAG1 .LE. 0) GRAND(J) = GRAND(J) / R(I,J)	PAR2 628
P = QSLOTU(I)	PAR2 629
GRAND(NSTUP1) = - SIN(ASLOTU(I)) / DEXP(P)	PAR2 630
IF ( FLAG1 .LE. 0 ) GRAND(NSTUP1) = GRAND(NSTUP1) /	PAR2 631
IRSLOTU(I)	PAR2 632
CALL SIMP	PAR2 633
TEMP = X(I,NP1) - GIFT(NP1)	PAR2 634
DO 1050 J=NSTUP2,N	PAR2 635
1050 X(I,J) = GIFT(J) + TEMP	PAR2 636
1060 XSLOTU(I) = GIFT(NSTUP1) + TEMP	PAR2 637
I = MSTUP1	PAR2 638

	J = NSTUP1	PAR2 639
	P = Q(I-1,J)	PAR2 640
	X(I,J) = X(I-1,J) + COS(ALPHA(I-1,J)) * DPHI(I-1) / DEXP(P)	PAR2 641
C		PAR2 642
C	COMPUTE X OVER LOWER PORTION OF DIFFUSER	PAR2 643
C		PAR2 644
	IF ( FLAG1 .GT. 0 .OR. FLAG3 .GT. 0 ) GO TO 3000	PAR2 645
	DO 1070 I=2,MSTAGL	PAR2 646
	DO 1065 J=2,K	PAR2 647
	P = Q(I,J)	PAR2 648
1065	GRAND(J) = - SIN(ALPHA(I,J)) / ( DEXP(P) * R(I,J) )	PAR2 649
	IMINSI = 2	PAR2 650
	IMAXSI = K	PAR2 651
	CALL SIMP	PAR2 652
	TEMP = X(I,K) - GIFT(K)	PAR2 653
	DO 1070 J=2,KM1	PAR2 654
1070	X(I,J) = GIFT(J) + TEMP	PAR2 655
	I = MSTLP1	PAR2 656
	DO 1075 J =NSTLP2,NP1	PAR2 657
	P = Q(I,J)	PAR2 658
1075	GRAND(J) = - SIN(ALPHA(I,J)) / ( DEXP(P) * R(I,J) )	PAR2 659
	IMINSI = NSTLP2	PAR2 660
	IMAXSI = K	PAR2 661
	CALL SIMP	PAR2 662
	TEMP = X(I,K) - GIFT(K)	PAR2 663
	DO 1080 J=NSTLP2,KM1	PAR2 664
1080	X(I,J) = GIFT(J) + TEMP	PAR2 665
	DO 1090 I=MSTLP2,MP1	PAR2 666
	DO 1085 J=NSTLP1,K	PAR2 667
	P = Q(I,J)	PAR2 668
1085	GRAND(J) = - SIN(ALPHA(I,J)) / ( DEXP(P) * R(I,J) )	PAR2 669
	IMINSI = NSTLP1	PAR2 670
	IMAXSI = K	PAR2 671
	CALL SIMP	PAR2 672
	TEMP = X(I,K) - GIFT(K)	PAR2 673
	DO 1090 J=NSTLP1,KM1	PAR2 674
1090	X(I,J) = GIFT(J) + TEMP	PAR2 675
C		PAR2 676
C	COMPUTE X INSIDE LOWER SLOTS	PAR2 677
C		PAR2 678
	DO 1120 I=2,MM1	PAR2 679
	ESIMP(I) = EPHI(I)	PAR2 680
	FSIMP(I) = FPHI(I)	PAR2 681
1120	GSIMP(I) = GPHI(I)	PAR2 682
	DO 1130 I=2,M	PAR2 683
1130	DX(I) = DPHI(I)	PAR2 684
	DO 1140 I=MSTLM1,MSLLP1	PAR2 685
	P = Q(I,2)	PAR2 686
1140	GRAND(I) = COS(ALPHA(I,2)) / DEXP(P)	PAR2 687
	IMINSI = MSTLM1	PAR2 688
	IMAXSI = MSLLP1	PAR2 689
	CALL SIMP	PAR2 690
	DO 1150 I=MSTAGL,MSLLP1	PAR2 691
1150	X(I,2) = X(MSTLM1,2) + GIFT(I)	PAR2 692
	DO 1160 J=2,NM1	PAR2 693
	ESIMP(J) = EPSI(J)	PAR2 694
	FSIMP(J) = FPSI(J)	PAR2 695
1160	GSIMP(J) = GPSI(J)	PAR2 696
	DO 1170 J=2,N	PAR2 697
1170	DX(J) = DPSI(J)	PAR2 698

IMINSI = 2	PAR2 699
IMAXSI = NSTLP1	PAR2 700
DO 1200 I=MSTAGL,MSLLP1	PAR2 701
DO 1180 J=2,NSTAGL	PAR2 702
P = Q(I,J)	PAR2 703
GRAND(J) = - SIN(ALPHA(I,J)) / DEXP(P)	PAR2 704
1180 IF (FLAG1 .LE. 0) GRAND(J) = GRAND(J) / R(I,J)	PAR2 705
P = QSLOTL(I)	PAR2 706
GRAND(NSTLP1) = - SIN(ASLOTL(I)) / DEXP(P)	PAR2 707
IF (FLAG1 .LE. 0) GRAND(NSTLP1) = GRAND(NSTLP1) /	PAR2 708
IRSLOTL(I)	PAR2 709
CALL SIMP	PAR2 710
DO 1190 J=3,NSTAGL	PAR2 711
1190 X(I,J) = X(I,2) + GIFT(J)	PAR2 712
1200 XSLOTL(I) = X(I,2) + GIFT(NSTLP1)	PAR2 713
1210 I = MSTLP1	PAR2 714
J = NSTLP1	PAR2 715
P = Q(I-1,J)	PAR2 716
X(I,J) = X(I-1,J) + COS(ALPHA(I-1,J)) * DPHI(I-1) / DEXP(P)	PAR2 717
3000 CONTINUE	PAR2 718
ASLOTU(MSTUP1) = ALPHA(MSTUP1,NSTUP1)	PAR2 719
RSLOTU(MSTUP1) = R(MSTUP1,NSTUP1)	PAR2 720
XSLOTU(MSTUP1) = X(MSTUP1,NSTUP1)	PAR2 721
ASLOTL(MSTLP1) = ALPHA(MSTLP1,NSTLP1)	PAR2 722
RSLOTL(MSTLP1) = R(MSTLP1,NSTLP1)	PAR2 723
XSLOTL(MSTLP1) = X(MSTLP1,NSTLP1)	PAR2 724
C	PAR2 725
C	PAR2 726
SET UP BOUNDARY CONDITIONS FOR NEXT ITERATION	PAR2 727
C	PAR2 728
IOT = MP1	PAR2 729
IF (FLAG1 .LE. 0 .AND. FLAG3 .LE. 0) IOT = MSLLP1	PAR2 730
DO 2010 I=2,IOT	PAR2 731
Y3 = R(I,4)	PAR2 732
Y2 = R(I,3)	PAR2 733
Y1 = R(I,2)	PAR2 734
D1 = DPSI(2)	PAR2 735
D2 = DPSI(3)	PAR2 736
DER = ( Y2 - Y1 ) * ( D1 + D2 ) / ( D1 * D2 )	PAR2 737
DER = DER - ( Y3 - Y1 ) * D1 / ( D1 * D2 + D2 * D2 )	PAR2 738
2010 R(I,1) = Y2 - 2. * DER * D1	PAR2 739
IOT = MSLUP1	PAR2 740
DO 2020 I=2,IOT	PAR2 741
Y3 = R(I,NP1)	PAR2 742
Y2 = R(I,N)	PAR2 743
Y1 = R(I,NM1)	PAR2 744
D1 = DPSI(NM1)	PAR2 745
D2 = DPSI(N)	PAR2 746
DER = ( Y3 - Y2 ) * ( D1 + D2 ) / ( D1 * D2 )	PAR2 747
DER = DER - ( Y3 - Y1 ) * D2 / ( D1 * D1 + D1 * D2 )	PAR2 748
2020 R(I,NP2) = Y2 + 2. * DER * D2	PAR2 749
DO 2030 J=2,NP1	PAR2 750
Y3 = R(4,J)	PAR2 751
Y2 = R(3,J)	PAR2 752
Y1 = R(2,J)	PAR2 753
D1 = DPHI(2)	PAR2 754
D2 = DPHI(3)	PAR2 755
DER = ( Y2 - Y1 ) * ( D1 + D2 ) / ( D1 * D2 )	PAR2 756
DER = DER - ( Y3 - Y1 ) * D1 / ( D1 * D2 + D2 * D2 )	PAR2 757
2030 R(1,J) = Y2 - 2. * DER * D1	PAR2 758
DO 2035 J=2,NP1	PAR2 759
Y3 = R(MP1,J)	PAR2 759

Y2 = R(M,J)	PAR2 760
Y1 = R(MM1,J)	PAR2 761
D1 = DPHI(MM1)	PAR2 762
D2 = DPHI(M)	PAR2 763
DER = ( Y3 - Y2 ) * ( D1 + D2 ) / ( D1 * D2 )	PAR2 764
DER = DER - ( Y3 - Y1 ) * D2 / ( D1 * D1 + D1 * D2 )	PAR2 765
2035 R(MP2,J) = Y2 + 2. * DER * D2	PAR2 766
IF (FLAG2 .LE. 0) GO TO 2050	PAR2 767
DO 2040 J=2, NP1	PAR2 768
R(1,J) = R(3,J)	PAR2 769
2040 R(MP2,J) = R(M,J)	PAR2 770
2050 CONTINUE	PAR2 771
C	PAR2 772
C WRITE CONVERGENCE VARIABLES	PAR2 773
C	PAR2 774
IF (FLAG1 .LE. 0) WRITE(3,2060) ITER, JTER, EPS, DEL	PAR2 775
2060 FORMAT(/T2, 'ITER = ', T9, I5, T25, 'JTER = ', T32, I5, T50,	PAR2 776
1'EPS = ', T56, E13.6, T75, 'DEL = ', T80, E13.6)	PAR2 777
C	PAR2 778
C CHECK BELL CHANNEL SOLUTION	PAR2 779
C	PAR2 780
IF (FLAG3 .LE. 0) GO TO 2130	PAR2 781
IF (EPS .GT. TOLSYS .AND. ITER .LT. MXISYS) GO TO 2130	PAR2 782
IMINSU = 2	PAR2 783
IMAXSU = NSTAGU - 1	PAR2 784
IMINSI = 2	PAR2 785
IMAXSI = NSTAGU + 1	PAR2 786
ERROR = 0.0	PAR2 787
DO 2090 I=2, MP1	PAR2 788
DO 2070 J=2, NSTAGU	PAR2 789
2070 DX(J) = SQRT( ( ABS( X(I,J+1) - X(I,J) ) )**2.	PAR2 790
1+ ( ABS( R(I,J+1) - R(I,J) ) )**2. )	PAR2 791
CALL SETUP	PAR2 792
NSTUP1 = NSTAGU + 1	PAR2 793
DO 2080 J=2, NSTUP1	PAR2 794
2080 GRAND(J) = R(I,J) * EXP(Q(I,J))	PAR2 795
CALL SIMP	PAR2 796
ERR = ABS( PSI(NSTUP1) - GIFT(NSTUP1) )	PAR2 797
IF ( ERR .GT. ERROR ) FNC = GIFT(NSTUP1)	PAR2 798
2090 IF ( ERR .GT. ERROR ) ERROR = ERR	PAR2 799
PCE = 100. * ERROR / PSI(NSTUP1)	PAR2 800
WRITE(3,2100) HEDR, DATE1, DATE2, DATE3, CASE	PAR2 801
2100 FORMAT(1H1//T57, 'CLEMSON UNIVERSITY', //T49, 'MECHANICAL ENGINEERI	PAR2 802
NG DEPARTMENT', //T2, I5A4, T64, I2, T66, '//', T67, I2, T69, '//', T70, I2,	PAR2 803
2T76, 'CASE NO. ', T87, I4//)	PAR2 804
WRITE(3,2110)	PAR2 805
2110 FORMAT(T2, 'THE ACCURACY OF THE SOLUTION FOR THE',	PAR2 806
1T38, ' BELL CHANNEL DESIGNED')	PAR2 807
WRITE(3,2120) ERROR, FNC, PCE	PAR2 808
2120 FORMAT(///T2, 'ERROR = ', F10.6//)	PAR2 809
1T2, 'INCORRECT VALUE = ', F10.6//)	PAR2 810
2T2, 'PERCENT ERROR = ', F10.6)	PAR2 811
2130 CONTINUE	PAR2 812
REWIND 5	PAR2 813
REWIND 12	PAR2 814
WRITE(5)((R(I,J), I=1, MP2), J=1, NP2)	PAR2 815
WRITE(11)((ALPHA(I,J), I=1, MP2), J=1, NP2)	PAR2 816
WRITE(12)((X(I,J), I=1, MP2), J=1, NP2)	PAR2 817
RETURN	PAR2 818
END	PAR2 819

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C          *****      SUBROUTINE  OUTPUT      *****      OUT   1
C          THIS SUBROUTINE PROVIDES PRINTER OUTPUT OF THE      OUT   2
C          RESULTS OF THE MAIN PROGRAM                        OUT   3
C          SUBROUTINE OUTPUT                                OUT   4
C          DIMENSION DX(150),ESIMP(150),FSIMP(150),GSIMP(150), OUT   5
1          GRAND(150),GIFT(150),PHI(150),PSI(150),          OUT   6
2          DPSI(150),DPHI(150),S(150),SBAR(150),          OUT   7
3          S1(150),SBAR1(150),S2(150),SBAR2(150),          OUT   8
4          HEDR(15),EPhi(150),FPhi(150),GPhi(150),          OUT   9
5          EPSI(150),ASLOTL(150),XSLOTU(150),XSLOTL(150)   OUT  10
6          ,FPSI(150),GPSI(150),RSLOTU(150),RSLOTL(150),   OUT  11
7          QSLOTU(150),QSLOTL(150),ASLOTU(150)             OUT  12
DIMENSION Q(150,50),R(150,50),X(150,50),ALPHA(150,50)     OUT  13
DOUBLE PRECISION P                                          OUT  14
INTEGER FLAG1,FLAG2,FLAG3,FLAG4,CASE,DATE1,DATE2,DATE3     OUT  15
COMMON / C2 / FLAG1,FLAG2,FLAG3,FLAG4,HEDR,DATE1,DATE2     OUT  16
1          ,DATE3,CASE,MXIDE,ICKDE,IPROE,IMIN,IMAX,          OUT  17
2          JMIN,JMAX,NUT,M,N,TOLDE,DEL,EPS,JTER,           OUT  18
3          ITER,DPHI,DPSI,S,SBAR,RMULT,S1,S2,SBAR1,        OUT  19
4          SBAR2,MSTAGU,NSTAGU,MSLOTU,MSTAGL,NSTAGL         OUT  20
5          ,MSLOTL,RADIN,W,PHI,PSI,RSLOTU,RSLOTL,          OUT  21
6          QSLOTU,QSLOTL,ASLOTU,ASLOTL,XSLOTU,             OUT  22
7          XSLOTL,G,MIDJ                                     OUT  23
C          CHANGE Q BACK TO VELOCITY AND OUTPUT              OUT  24
C          MP1 = M + 1                                       OUT  25
C          NP1 = N + 1                                       OUT  26
C          MM1 = M - 1                                       OUT  27
C          NM1 = N - 1                                       OUT  28
C          MP2 = M + 2                                       OUT  29
C          NP2 = N + 2                                       OUT  30
C          NSTLP1 = NSTAGL + 1                                  OUT  31
C          NSTUP1 = NSTAGU + 1                                  OUT  32
C          MSTUP1 = MSTAGU + 1                                  OUT  33
C          MSTLP1 = MSTAGL + 1                                  OUT  34
C          MSLLP1 = MSLOTL + 1                                  OUT  35
C          MSLUP1 = MSLOTU + 1                                  OUT  36
C          REWIND 4                                           OUT  37
C          REWIND 5                                           OUT  38
C          REWIND 11                                          OUT  39
C          REWIND 12                                          OUT  40
C          READ(4)((Q(I,J),I=1,MP2),J=1,NP2)                 OUT  41
C          READ(5)((R(I,J),I=1,MP2),J=1,NP2)                 OUT  42
C          READ(11)((ALPHA(I,J),I=1,MP2),J=1,NP2)            OUT  43
C          READ(12)((X(I,J),I=1,MP2),J=1,NP2)                OUT  44
C          IF (NUT .EQ. 1) GO TO 1000                          OUT  45
C          DO 10 I=2,MP1                                       OUT  46
C          DO 10 J=2,NP1                                       OUT  47
C          P = Q(I,J)                                          OUT  48
10 Q(I,J) = DEXP(P)                                          OUT  49
C          Q(MSTUP1,NSTUP1) = 0.0                             OUT  50
C          Q(MSTLP1,NSTLP1) = 0.0                             OUT  51
C          OUTPUT Q ARRAY                                     OUT  52
C          WRITE(3,20)HEDR,DATE1,DATE2,DATE3,CASE           OUT  53
20 FORMAT(1H1//T57,'CLEMSON UNIVERSITY',//T49,             OUT  54
C          OUT  55
C          OUT  56
C          OUT  57
C          OUT  58
C          OUT  59
C          OUT  60

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1	'MECHANICAL ENGINEERING DEPARTMENT',///T2,15A4,T64,	OUT	61
2	I2,T66,'/',T67,I2,T69,'/',T70,I2,T76,'CASE NO. ',	OUT	62
	3T87,I4)	OUT	63
	WRITE(3,30)ITER,JTER,EPS,DEL	OUT	64
30	FORMAT(///T1,'VELOCITY THROUGHOUT DIFFUSER',	OUT	65
	1T46,'ITER = ',T53,I4,T61,'JTER = ',T68,I4,T76,'EPS = '	OUT	66
	2,T82,E13.6,T99,'DEL = ',T105,E13.6,///T7,'PHI',T66,	OUT	67
	3'PSI')	OUT	68
	WRITE(3,40)(PSI(IP),IP=2,NP1)	OUT	69
40	FORMAT(//(13X,5(7X,E13.6)))	OUT	70
	DO 50 I=2,MP1	OUT	71
50	WRITE(3,60)PHI(I),(Q(I,J),J=2,NP1)	OUT	72
60	FORMAT(//1X,E13.6,5(7X,E13.6),/(14X,5(7X,E13.6)))	OUT	73
C		OUT	74
C	CHANGE Q BACK TO LOGARITHMIC FORM	OUT	75
C		OUT	76
	Q(MSTUP1,NSTUP1) = 1.0	OUT	77
	Q(MSTLP1,NSTLP1) = 1.0	OUT	78
	DO 70 I=2,MP1	OUT	79
	DO 70 J=2,NP1	OUT	80
	P = Q(I,J)	OUT	81
	70 Q(I,J) = DLOG(P)	OUT	82
C		OUT	83
C	OUTPUT VELOCITY IN SLOTS	OUT	84
C		OUT	85
	DO 75 I=2,MP1	OUT	86
	P = QSLOTL(I)	OUT	87
	QSLOTL(I) = DEXP(P)	OUT	88
	P = QSLOTU(I)	OUT	89
75	QSLOTU(I) = DEXP(P)	OUT	90
	QSLOTU(MSTUP1) = 0.0	OUT	91
	QSLOTL(MSTLP1) = 0.0	OUT	92
	WRITE(3,20)HEDR,DATE1,DATE2,DATE3,CASE	OUT	93
	WRITE(3,80)ITER,JTER,EPS,DEL	OUT	94
80	FORMAT(///T2,'VELOCITY INSIDE SLOTS',T46,	OUT	95
	1'ITER = ',T53,I4,T61,'JTER = ',T68,I4,T76,'EPS = ',	OUT	96
	2T82,E13.6,T99,'DEL = ',T105,E13.6,///T7,'PSI',T66,	OUT	97
	3'PHI')	OUT	98
	WRITE(3,40)(PHI(IP),IP=2,MP1)	OUT	99
	IF (FLAG1 .GT. 0 .OR. FLAG3 .GT. 0) GO TO 90	OUT	100
	WRITE(3,85)	OUT	101
85	FORMAT(///T2,'LOWER SLOT')	OUT	102
	WRITE(3,60)PSI(NSTLP1),(QSLOTL(IP),IP=2,MP1)	OUT	103
90	WRITE(3,100)	OUT	104
100	FORMAT(///T2,'UPPER SLOT')	OUT	105
	WRITE(3,60)PSI(NSTUP1),(QSLOTU(IP),IP=2,MP1)	OUT	106
	QSLOTU(MSTUP1) = 1.0	OUT	107
	QSLOTL(MSTLP1) = 1.0	OUT	108
	DO 105 I=2,NP1	OUT	109
	P = QSLOTL(I)	OUT	110
	QSLOTL(I) = DLOG(P)	OUT	111
	P = QSLOTU(I)	OUT	112
105	QSLOTU(I) = DLOG(P)	OUT	113
C		OUT	114
C	OUTPUT OF R-COORDINATES ( Y-COORDINATES FOR 2-D )	OUT	115
C		OUT	116
1000	WRITE(3,20)HEDR,DATE1,DATE2,DATE3,CASE	OUT	117
	WRITE(3,110)ITER,JTER,EPS,DEL	OUT	118
110	FORMAT(///T1,'OR - COORDINATES ( UNTRANSFORMED )',	OUT	119
	1T46,'ITER = ',T53,I4,T61,'JTER = ',T68,I4,T76,'EPS = '	OUT	120

	2,T82,E13.6,T99,'DEL = ',T105,E13.6,///T7,'PHI',T66,	OUT	121
	3'PSI')	OUT	122
	WRITE(3,40)(PSI(IP),IP=2,NP1)	OUT	123
	DO 120 I=2,MP1	OUT	124
	120 WRITE(3,60)PHI(I),(R(I,J),J=2,NP1)	OUT	125
C		OUT	126
C	OUTPUT R COORDINATES INSIDE SLOTS	OUT	127
C		OUT	128
	WRITE(3,20)HEDR,DATE1,DATE2,DATE3,CASE	OUT	129
	WRITE(3,130)ITER,JTER,EPS,DEL	OUT	130
	130 FORMAT(///T2,'R - COORDINATES INSIDE SLOTS',	OUT	131
	1T46,'ITER = ',T53,I4,T61,'JTER = ',T68,I4,T76,'EPS = '	OUT	132
	2,T82,E13.6,T99,'DEL = ',T105,E13.6,///T7,'PSI',T66,	OUT	133
	3'PHI')	OUT	134
	WRITE(3,40)(PHI(IP),IP=2,MP1)	OUT	135
	IF (FLAG1 .GT. 0 .OR. FLAG3 .GT. 0) GO TO 150	OUT	136
	WRITE(3,140)	OUT	137
	140 FORMAT(//T2,'LOWER SLOT')	OUT	138
	WRITE(3,60)PSI(NSTLP1),(RSLOTL(IP),IP=2,MP1)	OUT	139
	150 WRITE(3,160)	OUT	140
	160 FORMAT(//T2,'UPPER SLOT')	OUT	141
	WRITE(3,60)PSI(NSTUP1),(RSLOTU(IP),IP=2,MP1)	OUT	142
	IF (NUT .EQ.1)RETURN	OUT	143
C		OUT	144
C	OUTPUT OF X - COORDINATES	OUT	145
	WRITE(3,20)HEDR,DATE1,DATE2,DATE3,CASE	OUT	146
	WRITE(3,170)ITER,JTER,EPS,DEL	OUT	147
	170 FORMAT(///T2,'X - COORDINATES ( UNTRANSFORMED )',	OUT	148
	1T46,'ITER = ',T53,I4,T61,'JTER = ',T68,I4,T76,'EPS = '	OUT	149
	2,T82,E13.6,T99,'DEL = ',T105,E13.6,///T7,'PHI',T66,	OUT	150
	3'PSI')	OUT	151
	WRITE(3,40)(PSI(IP),IP=2,NP1)	OUT	152
	DO 180 I=2,MP1	OUT	153
	180 WRITE(3,60)PHI(I),(X(I,J),J=2,NP1)	OUT	154
C		OUT	155
C	OUTPUT X VALUES INSIDE SLOTS	OUT	156
C		OUT	157
	WRITE(3,20)HEDR,DATE1,DATE2,DATE3,CASE	OUT	158
	WRITE(3,190)ITER,JTER,EPS,DEL	OUT	159
	190 FORMAT(///T2,'X - COORDINATES INSIDE SLOTS',T46,	OUT	160
	1'ITER = ',T53,I4,T61,'JTER = ',T68,I4,T76,'EPS = ',	OUT	161
	2T82,E13.6,T99,'DEL = ',T105,E13.6,///T7,'PSI',T66,	OUT	162
	3'PHI')	OUT	163
	WRITE(3,40)(PHI(IP),IP=2,MP1)	OUT	164
	IF (FLAG1 .GT. 0 .OR. FLAG3 .GT. 0) GO TO 200	OUT	165
	WRITE(3,140)	OUT	166
	WRITE(3,60)PSI(NSTLP1),(XSLOTL(IP),IP=2,MP1)	OUT	167
	200 WRITE(3,160)	OUT	168
	WRITE(3,60)PSI(NSTUP1),(XSLOTU(IP),IP=2,MP1)	OUT	169
C		OUT	170
C	OUTPUT VELOCITY VECTOR ANGLES ( ALPHA )	OUT	171
C		OUT	172
	WRITE(3,20)HEDR,DATE1,DATE2,DATE3,CASE	OUT	173
	WRITE(3,210)ITER,JTER,EPS,DEL	OUT	174
	210 FORMAT(///T1,'OFLOW ANGLES ( ALPHA )',T46,'ITER = ',	OUT	175
	1T53,I4,T61,'JTER = ',T68,I4,T76,'EPS = ',T82,E13.6,	OUT	176
	2T99,'DEL = ',T105,E13.6,///T7,'PHI',T66,'PSI')	OUT	177
	WRITE(3,40)(PSI(IP),IP=2,NP1)	OUT	178
	DO 220 I=2,MP1	OUT	179
	220 WRITE(3,60)PHI(I),(ALPHA(I,J),J=2,NP1)	OUT	180

C		OUT	181
C	OUTPUT FLOW ANGLES INSIDE SLOTS	OUT	182
C		OUT	183
	WRITE(3,20)HEDR,DATE1,DATE2,DATE3,CASE	OUT	184
	WRITE(3,230)ITER,JTER,EPS,DEL	OUT	185
230	FORMAT(///T2,'FLOW ANGLES INSIDE SLOTS',T46,'ITER = ',	OUT	186
	1T53,I4,T61,'JTER = ',T68,I4,T76,'EPS = ',T82,E13.6,	OUT	187
	2T99,'DEL = ',T105,E13.6,///T7,'PSI',T66,'PHI')	OUT	188
	WRITE(3,40)(PHI(IP),IP=2,MP1)	OUT	189
	IF (FLAG1 .GT. 0 .OR. FLAG3 .GT. 0) GO TO 240	OUT	190
	WRITE(3,140)	OUT	191
	WRITE(3,60)PSI(NSTLP1),(ASLOTL(IP),IP=2,MP1)	OUT	192
240	WRITE(3,160)	OUT	193
	WRITE(3,60)PSI(NSTUP1),(ASLOTU(IP),IP=2,MP1)	OUT	194
C		OUT	195
C	OUTPUT X AND R - COORDINATES ( TRANSFORMED )	OUT	196
C	IF RMULT > 0	OUT	197
C		OUT	198
	IF (RMULT .LE. 0.0) GO TO 2000	OUT	199
	YMIN=0.999E6	OUT	199A
	DO 166 I=2,MP1	OUT	199B
	IF(R(I,NP1).LT.YMIN)YMIN=R(I,NP1)	OUT	199C
166	CONTINUE	OUT	199D
	RMULT=RMULT/YMIN	OUT	199E
	DO 250 J=2,NP1	OUT	200
	DO 250 I=2,MP1	OUT	201
	R(I,J) = RMULT * R(I,J)	OUT	202
250	X(I,J) = RMULT * X(I,J)	OUT	203
	DO 260 I=2,MP1	OUT	204
	XSLOTL(I) = RMULT * XSLOTL(I)	OUT	205
	XSLOTU(I) = RMULT * XSLOTU(I)	OUT	206
	RSLOTL(I) = RMULT * RSLOTL(I)	OUT	207
260	RSLOTU(I) = RMULT * RSLOTU(I)	OUT	208
	REWIND 5	OUT	208A
	REWIND 12	OUT	208B
	WRITE(5)((R(I,J),I=1,MP2),J=1,NP2)	OUT	208C
	WRITE(12)((X(I,J),I=1,MP2),J=1,NP2)	OUT	208D
	WRITE(3,20)HEDR,DATE1,DATE2,DATE3,CASE	OUT	209
	WRITE(3,270)ITER,JTER,EPS,DEL	OUT	210
270	FORMAT(///T1,'OR - COORDINATES ( TRANSFORMED )',T46,	OUT	211
	1'ITER = ',T53,I4,T61,'JTER = ',T68,I4,T76,'EPS = ',	OUT	212
	2T82,E13.6,T99,'DEL = ',T105,E13.6,///T7,'PHI',T66,	OUT	213
	3'PSI')	OUT	214
	WRITE(3,40)(PSI(IP),IP=2,NP1)	OUT	215
	DO 280 I=2,MP1	OUT	216
280	WRITE(3,60)PHI(I),(R(I,J),J=2,NP1)	OUT	217
	WRITE(3,20)HEDR,DATE1,DATE2,DATE3,CASE	OUT	218
	WRITE(3,290)ITER,JTER,EPS,DEL	OUT	219
290	FORMAT(///T2,'R - COORDINATES IN SLOT ( TRANSFORMED )'	OUT	220
	1,T46,'ITER = ',T53,I4,T61,'JTER = ',T68,I4,T76,	OUT	221
	2'EPS = ',T82,E13.6,T99,'DEL = ',T105,E13.6,///T7,	OUT	222
	3'PSI',T66,'PHI')	OUT	223
	WRITE(3,40)(PHI(IP),IP=2,MP1)	OUT	224
	IF (FLAG1 .GT. 0 .OR. FLAG3 .GT. 0) GO TO 300	OUT	225
	WRITE(3,140)	OUT	226
	WRITE(3,60)PSI(NSTLP1),(RSLOTL(IP),IP=2,MP1)	OUT	227
300	WRITE(3,160)	OUT	228
	WRITE(3,60)PSI(NSTUP1),(RSLOTU(IP),IP=2,MP1)	OUT	229
	WRITE(3,20)HEDR,DATE1,DATE2,DATE3,CASE	OUT	230
	WRITE(3,310)ITER,JTER,EPS,DEL	OUT	231



310	FORMAT(///T1,'OX - COORDINATES ( TRANSFORMED )',T46,	OUT	232
	1'ITER = ',T53,I4,T61,'JTER = ',T68,I4,T76,'EPS = ',	OUT	233
	2T82,E13.6,T99,'DEL = ',T105,E13.6,///T7,'PHI',T66,	OUT	234
	3'PSI')	OUT	235
	WRITE(3,40)(PSI(IP),IP=2,NP1)	OUT	236
	DO 320 I=2,MP1	OUT	237
320	WRITE(3,60)PHI(I),(X(I,J),J=2,NP1)	OUT	238
	WRITE(3,20)HEDR,DATE1,DATE2,DATE3,CASE	OUT	239
	WRITE(3,330)ITER,JTER,EPS,DEL	OUT	240
330	FORMAT(///T2,'X - COORDINATES IN SLOT ( TRANSFORMED )'	OUT	241
	1,T46,'ITER = ',T53,I4,T61,'JTER = ',T68,I4,T76,	OUT	242
	2'EPS = ',T82,E13.6,T99,'DEL = ',T105,E13.6,///T7,	OUT	243
	3'PSI',T66,'PHI')	OUT	244
	WRITE(3,40)(PHI(IP),IP=2,MP1)	OUT	245
	IF (FLAG1 .GT. 0 .OR. FLAG3 .GT. 0) GO TO 340	OUT	246
	WRITE(3,140)	OUT	247
	WRITE(3,60)PSI(NSTLP1),(XSLOTL(IP),IP=2,MP1)	OUT	248
340	WRITE(3,160)	OUT	249
	WRITE(3,60)PSI(NSTUP1),(XSLOTU(IP),IP=2,MP1)	OUT	250
C		OUT	251
C	SUMMARY OF WALL STREAMLINE COORDINATES	OUT	252
C		OUT	253
2000	I = MSTAGU + 1	OUT	254
	J = NSTAGU + 1	OUT	255
	Q(MSTUP1,NSTUP1) = 0.0	OUT	256
	Q(MSTLP1,NSTLP1) = 0.0	OUT	257
	QSLOTU(MSTUP1) = 0.0	OUT	258
	QSLOTL(MSTLP1) = 0.0	OUT	259
	SS = SQRT( (X(I,J)-X(I+1,J))*(X(I,J)-X(I+1,J))	OUT	260
	1 + (R(I,J)-R(I+1,J))*(R(I,J)-R(I+1,J)) )	OUT	261
	SS = SS - S1(I+1)	OUT	262
	SSS = SQRT( (XSLOTU(I)-XSLOTU(I+1))*(XSLOTU(I)-XSLOTU(I+1))	OUT	263
	1 + (RSLOTU(I) -RSLOTU(I+1))*(RSLOTU(I) -RSLOTU(I+1)) )	OUT	264
	SSS = SSS - S2(I+1)	OUT	265
	MSTUP2 = MSTAGU + 2	OUT	266
	DO 345 I=MSTUP2,MP1	OUT	267
	S1(I) = S1(I) + SS	OUT	268
345	S2(I) = S2(I) + SSS	OUT	269
	WRITE(3,20)HEDR,DATE1,DATE2,DATE3,CASE	OUT	270
	DO 350 I=2,MP1	OUT	271
	DO 350 J=2,NP1	OUT	272
	P = Q(I,J)	OUT	273
350	Q(I,J) = DEXP(P)	OUT	274
	WRITE(3,360)	OUT	275
360	FORMAT(///T1,'OSUMMARY OF INLET WALL COORDINATES OF ',	OUT	276
	1T39,'DIFFUSER (UPPER WALL)',///T8,'X',T27,'R',T47,'Q',	OUT	277
	2T68,'S',T85,'ALPHA'//)	OUT	278
	ICOUNT = 1	OUT	279
	DO 370 I=2,MSLUP1	OUT	280
	ICOUNT = ICOUNT + 1	OUT	281
	IF (ICOUNT .LT. 23) GO TO 370	OUT	282
	ICOUNT = 1	OUT	283
	WRITE(3,20)HEDR,DATE1,DATE2,DATE3,CASE	OUT	284
	WRITE(3,360)	OUT	285
370	WRITE(3,375)X(I,NP1),R(I,NP1),Q(I,NP1),S(I),	OUT	286
	1ALPHA(I,NP1)	OUT	287
375	FORMAT(/1X,E13.6,4(7X,E13.6))	OUT	288
	WRITE(3,20)HEDR,DATE1,DATE2,DATE3,CASE	OUT	289
	WRITE(3,380)	OUT	290
380	FORMAT(///T2,'SUMMARY OF DOWNSTREAM WALL COORDINATES',	OUT	291

1T40,' OF DIFFUSER (UPPER WALL)',///T8,'X',T27,'R',T47,	OUT	292
2'Q',T67,'S',T85,'ALPHA'//)	OUT	293
ICOUNT = 1	OUT	294
DO 390 I=MSTUP1,MP1	OUT	295
ICOUNT = ICOUNT + 1	OUT	296
IF (ICOUNT .LT. 23) GO TO 390	OUT	297
ICOUNT = 1	OUT	298
WRITE(3,20)HEDR,DATE1,DATE2,DATE3,CASE	OUT	299
WRITE(3,380)	OUT	300
390 WRITE(3,375)X(I,NSTUP1),R(I,NSTUP1),Q(I,NSTUP1),	OUT	301
1S1(I),ALPHA(I,NSTUP1)	OUT	302
WRITE(3,20)HEDR,DATE1,DATE2,DATE3,CASE	OUT	303
WRITE(3,400)	OUT	304
400 FORMAT(///T2,'SUMMARY OF WALL COORDINATES INSIDE OF ',	OUT	305
1T40,'DIFFUSER SLOT (UPPER WALL)',///T8,'X',T27,'R',	OUT	306
2T47,'Q',T67,'S',T85,'ALPHA'//)	OUT	307
ICOUNT = 1	OUT	308
DO 410 I=MSTUP1,MSLUP1	OUT	309
ICOUNT = ICOUNT + 1	OUT	310
IF (ICOUNT .LT. 23) GO TO 410	OUT	311
ICOUNT = 1	OUT	312
WRITE(3,20)HEDR,DATE1,DATE2,DATE3,CASE	OUT	313
WRITE(3,400)	OUT	314
410 WRITE(3,375)XSLOTU(I),RSLOTU(I),QSLOTU(I),S2(I),	OUT	315
1ASLOTU(I)	OUT	316
IF (FLAG1 .GT. 0 .OR. FLAG3 .GT. 0) RETURN	OUT	317
I = MSTAGL + 1	OUT	318
J = NSTAGL + 1	OUT	319
SS = SQRT( (X(I,J)-X(I+1,J))*(X(I,J)-X(I+1,J))	OUT	320
1 + (R(I,J)-R(I+1,J))*(R(I,J)-R(I+1,J)) )	OUT	321
SS = SS - SBAR1(I+1)	OUT	322
SSS = SQRT( (XSLOTL(I)-XSLOTL(I+1))*(XSLOTL(I)-XSLOTL(I+1))	OUT	323
1 + (RSLOTL(I)-RSLOTL(I+1))*(RSLOTL(I)-RSLOTL(I+1)) )	OUT	324
SSS = SSS - SBAR2(I+1)	OUT	325
MSTLP2 = MSTAGL + 2	OUT	326
DO 415 I=MSTLP2,MP1	OUT	327
SBAR1(I) = SBAR1(I) + SS	OUT	328
415 SBAR2(I) = SBAR2(I) + SSS	OUT	329
WRITE(3,20)HEDR,DATE1,DATE2,DATE3,CASE	OUT	330
WRITE(3,420)	OUT	331
420 FORMAT(///T2,'SUMMARY OF INLET WALL COORDINATES OF ',	OUT	332
1T39,'DIFFUSER (LOWER WALL)',///T8,'X',T27,'R',T47,'Q',	OUT	333
2T67,'S',T85,'ALPHA'//)	OUT	334
ICOUNT = 1	OUT	335
DO 430 I=2,MSLLP1	OUT	336
ICOUNT = ICOUNT + 1	OUT	337
IF (ICOUNT .LT. 23) GO TO 430	OUT	338
ICOUNT = 1	OUT	339
WRITE(3,20)HEDR,DATE1,DATE2,DATE3,CASE	OUT	340
WRITE(3,420)	OUT	341
430 WRITE(3,375)X(I,2),R(I,2),Q(I,2),SBAR(I),ALPHA(I,2)	OUT	342
WRITE(3,20)HEDR,DATE1,DATE2,DATE3,CASE	OUT	343
WRITE(3,440)	OUT	344
440 FORMAT(///T2,'SUMMARY OF DOWNSTREAM WALL COORDINATES',	OUT	345
1T40,' OF DIFFUSER (LOWER WALL)',///T8,'X',T27,'R',T47,'Q'	OUT	346
2,T67,'S',T85,'ALPHA'//)	OUT	347
ICOUNT = 1	OUT	348
DO 450 I=MSTLP1,MP1	OUT	349
ICOUNT = ICOUNT + 1	OUT	350
IF (ICOUNT .LT. 23) GO TO 450	OUT	351

ICOUNT = 1	OUT 352
WRITE(3,20)HEDR,DATE1,DATE2,DATE3,CASE	OUT 353
WRITE(3,440)	OUT 354
450 WRITE(3,375)X(I,NSTLP1),R(I,NSTLP1),Q(I,NSTLP1),	OUT 355
1SBAR1(I),ALPHA(I,NSTLP1)	OUT 356
WRITE(3,20)HEDR,DATE1,DATE2,DATE3,CASE	OUT 357
WRITE(3,460)	OUT 358
460 FORMAT(///T2,'SUMMARY OF WALL COORDINATES INSIDE OF ',	OUT 359
1T40,'DIFFUSER SLOT (LOWER WALL)',///T8,'X',T27,'R',	OUT 360
2T47,'Q',T67,'S',T85,'ALPHA'//)	OUT 361
ICOUNT = 1	OUT 362
DO 470 I=MSTLP1,MSLLP1	OUT 363
ICOUNT = ICOUNT + 1	OUT 364
IF (ICOUNT .LT. 23) GO TO 470	OUT 365
ICOUNT = 1	OUT 366
WRITE(3,20)HEDR,DATE1,DATE2,DATE3,CASE	OUT 367
WRITE(3,460)	OUT 368
470 WRITE(3,375)XSLOTL(I),RSLOTL(I),QSLOTL(I),SBAR2(I),	OUT 369
1ASLOTL(I)	OUT 370
RETURN	OUT 371
END	OUT 372
C ***** SUBROUTINE GRAPIC *****	GRAP 1
C	GRAP 2
C THIS SUBROUTINE PROVIDES GRAPHICAL OUTPUT FOR MAIN	GRAP 3
C	GRAP 4
SUBROUTINE GRAPIC	GRAP 5
DIMENSION BUFR(500)	GRAP 6
DIMENSION DX(150),ESIMP(150),FSIMP(150),GSIMP(150),	GRAP 7
1 GRAND(150),GIFT(150),PHI(150),PSI(150),	GRAP 8
2 DPSI(150),DPHI(150),S(150),SBAR(150),	GRAP 9
3 S1(150),SBAR1(150),S2(150),SBAR2(150),	GRAP 10
4 HEDR(15),EPhi(150),FPhi(150),GPhi(150),	GRAP 11
5 EPSI(150),ASLOTL(150),XSLOTU(150),XSLOTL(150)	GRAP 12
6 ,FPSI(150),GPSI(150),RSLOTU(150),RSLOTL(150),	GRAP 13
7 QSLOTU(150),QSLOTL(150),ASLOTU(150)	GRAP 14
DIMENSION Q(150,50),R(150,50),X(150,50)	GRAP 15
DIMENSION XX(150),XY(150),LABL(20),RABL(20),WABL(20)	GRAP 16
DOUBLE PRECISION P	GRAP 17
INTEGER FLAG1,FLAG2,FLAG3,FLAG4,CASE,DATE1,DATE2,DATE3	GRAP 18
COMMON / C2 / FLAG1,FLAG2,FLAG3,FLAG4,HEDR,DATE1,DATE2	GRAP 19
1 ,DATE3,CASE,MXIDE,ICKDE,IPRDE,IMIN,IMAX,	GRAP 20
2 JMIN,JMAX,NUT,M,N,TOLDE,DEL,EPS,JTER,	GRAP 21
3 ITER,DPHI,DPSI,S,SBAR,RMULT,S1,S2,SBAR1,	GRAP 22
4 SBAR2,MSTAGU,NSTAGU,MSLOTU,MSTAGL,NSTAGL	GRAP 23
5 ,MSLOTL,RADIN,W,PHI,PSI,RSLOTU,RSLOTL,	GRAP 24
6 QSLOTU,QSLOTL,ASLOTU,ASLOTL,XSLOTU,	GRAP 25
7 XSLOTL,G,MIDJ	GRAP 26
REWIND 4	GRAP 27
REWIND 5	GRAP 28
REWIND 12	GRAP 29
MPI = M + 1	GRAP 30
NP1 = N + 1	GRAP 31
MP2 = M + 2	GRAP 32
NP2 = N + 2	GRAP 33
MM1 = M - 1	GRAP 34
NM1 = N - 1	GRAP 35
MSTUP2 = MSTAGU + 2	GRAP 36
MSTUP1 = MSTAGU + 1	GRAP 37
MSTUM1 = MSTAGU - 1	GRAP 38
NSTUP1 = NSTAGU + 1	GRAP 39

	NSTUM1 = NSTAGU - 1	GRAP 40
	MSTLP2 = MSTAGL + 2	GRAP 41
	MSTLP1 = MSTAGL + 1	GRAP 42
	MSTLM1 = MSTAGL - 1	GRAP 43
	NSTLP1 = NSTAGL + 1	GRAP 44
	NSTLM1 = NSTAGL - 1	GRAP 45
	MSLUP1 = MSLOTU + 1	GRAP 46
	MSLUM1 = MSLOTU - 1	GRAP 47
	NSLUP1 = NSLOTU + 1	GRAP 48
	NSLUM1 = NSLOTU - 1	GRAP 49
	MSLLP1 = MSLOTL + 1	GRAP 50
	MSLLM1 = MSLOTL - 1	GRAP 51
	NSLLP1 = NSLOTL + 1	GRAP 52
	NSLLM1 = NSLOTL - 1	GRAP 53
	READ(4)((O(I,J),I=1,MP2),J=1,NP2)	GRAP 54
	READ(5)((R(I,J),I=1,MP2),J=1,NP2)	GRAP 55
	READ(12)((X(I,J),I=1,MP2),J=1,NP2)	GRAP 56
	CALL PLOTS(BUFR,100)	GRAP 57
	DATA LABL(1)/* /*,LABL(2)/* /*,LABL(3)/* /*,	GRAP 58
1	LABL(4)/* /*	GRAP 59
	DATA LABL(5)/* X A/*,LABL(6)/*XIS /*	GRAP 60
	DATA LABL(7)/* /*,LABL(8)/* /*,LABL(9)/* /*,	GRAP 61
1	LABL(10)/* /*	GRAP 62
	DATA LABL(11)/* /*,LABL(12)/* /*,	GRAP 63
1	LABL(13)/* /*,LABL(14)/* /*	GRAP 64
	DATA LABL(15)/*Y-R /*,LABL(16)/*AXIS/*	GRAP 65
	DATA LABL(17)/* /*,LABL(18)/* /*,	GRAP 66
1	LABL(19)/* /*,LABL(20)/* /*	GRAP 67
C		GRAP 68
C	WRITE HEDR	GRAP 69
C		GRAP 70
	CALL SYMBOL(0.5,0.0,0.14,HEDR,90.0,60)	GRAP 71
C		GRAP 72
C	GRAPH 2-D AND BELL DIFFUSERS	GRAP 73
C		GRAP 74
	IF (FLAG1 .LE. 0 .AND. FLAG3 .LE. 0) GO TO 1000	GRAP 75
	DO 10 J=1,N	GRAP 76
10	XX(J) = R(MP1,J+1)	GRAP 77
	CALL ADJUST(XX,N,1,9.0,0.0,SCAL,XMIN,XY,1)	GRAP 78
	DO 20 I=2,MP1	GRAP 79
	DO 20 J=2,NP1	GRAP 80
	X(I,J) = X(I,J) / SCAL	GRAP 81
20	R(I,J) = R(I,J) / SCAL	GRAP 82
	DO 30 I=MSTUP1,MSLUP1	GRAP 83
	XSLOTU(I) = XSLOTU(I) / SCAL	GRAP 84
30	RSLOTU(I) = RSLOTU(I) / SCAL	GRAP 85
C		GRAP 86
C	DRAW AXES FOR DIFFUSER PLOT	GRAP 87
C		GRAP 88
	CALL CGAXES(3.0,0.5,X(MP1,2),9.0,SCAL,SCAL,X(2,2),	GRAP 89
	IP(2,2),LABL,0)	GRAP 90
	DO 40 I=1,M	GRAP 91
	DO 40 J=2,NP1	GRAP 92
	X(I,J) = X(I+1,J)	GRAP 93
40	R(I,J) = R(I+1,J)	GRAP 94
	DO 50 I=1,M	GRAP 95
	DO 50 J=1,N	GRAP 96
	X(I,J) = X(I,J+1)	GRAP 97
50	R(I,J) = R(I,J+1)	GRAP 98
C		GRAP 99

C	GRAPH STREAM LINES	GRAP 100
C		GRAP 101
	DO 70 J=1,NSTAGU	GRAP 102
	DO 60 I=1,M	GRAP 103
	XX(I) = X(I,J) + 3.0	GRAP 104
6C	XY(I) = R(I,J) + 0.5	GRAP 105
70	CALL LINE(XX,XY,M,1,0,0)	GRAP 106
	DO 90 J=NSTUPL,N	GRAP 107
	DO 80 I=1,MSLOTU	GRAP 108
	XX(I) = X(I,J) + 3.0	GRAP 109
80	XY(I) = R(I,J) + 0.5	GRAP 110
90	CALL LINE(XX,XY,MSLOTU,1,0,0)	GRAP 111
	IOT = MSLUPL - MSTAGU	GRAP 112
	DO 100 I=1,IOT	GRAP 113
	XX(I) = XSLOTU(I+MSTAGU) + 3.0	GRAP 114
100	XY(I) = RSLOTU(I+MSTAGU) + 0.5	GRAP 115
	CALL LINE(XX,XY,IOT,1,0,0)	GRAP 116
C		GRAP 117
C	GRAPH POTENTIAL LINES	GRAP 118
C		GRAP 119
	DO 120 I=1,MSTAGU	GRAP 120
	DO 110 J=1,N	GRAP 121
	XX(J) = X(I,J) + 3.0	GRAP 122
110	XY(J) = R(I,J) + 0.5	GRAP 123
120	CALL LINE(XX,XY,N,1,0,0)	GRAP 124
	DO 140 I= MSTUPL,M	GRAP 125
	DO 130 J=1,NSTAGU	GRAP 126
	XX(J) = X(I,J) + 3.0	GRAP 127
130	XY(J) = R(I,J) + 0.5	GRAP 128
140	CALL LINE(XX,XY,NSTAGU,1,0,0)	GRAP 129
	JOT = N - NSTUML	GRAP 130
	DO 160 I=MSTUPL,MSLOTU	GRAP 131
	DO 150 J=2,JOT	GRAP 132
	XX(J) = X(I,J+NSTUML) + 3.0	GRAP 133
150	XY(J) = R(I,J+NSTUML) + 0.5	GRAP 134
	XX(1) = XSLOTU(I+1) + 3.0	GRAP 135
	XY(1) = RSLOTU(I+1) + 0.5	GRAP 136
160	CALL LINE(XX,XY,JOT,1,0,0)	GRAP 137
	XLIN = X(M,1) + 9.0	GRAP 138
	GO TO 2000	GRAP 139
C		GRAP 140
C	GRAPH ANNULAR DIFFUSER	GRAP 141
C		GRAP 142
1000	CONTINUE	GRAP 143
	ASH1 = R(MP1,NSTLPL)	GRAP 144
	ASH = ASH1	GRAP 145
	ASH2 = RSLOTL(MSLLPL)	GRAP 146
	IF (ASH2 .LT. ASH1) ASH = ASH2	GRAP 147
	IF ( R(2,2) .LT. ASH ) ASH = R(2,2)	GRAP 148
	DO 170 J=2,NPL	GRAP 149
	DO 170 I=2,MP1	GRAP 150
170	R(I,J) = R(I,J) - ASH	GRAP 151
	DO 173 I=MSTUPL,MSLUP1	GRAP 152
173	RSLOTU(I) = RSLOTU(I) - ASH	GRAP 153
	DO 176 I=MSTLPL,MSLLPL	GRAP 154
176	RSLOTL(I) = RSLOTL(I) - ASH	GRAP 155
	JOT = NSTAGU - NSTAGL + 1	GRAP 156
	TRASH1 = R(MP1,NSTUPL)	GRAP 157
	TRASH = TRASH1	GRAP 158
	TRASH2 = RSLOTU(MSLUP1)	GRAP 159

IF ( TRASH2 .GT. TRASH1 ) TRASH = TRASH2	GRAP 160
IF ( R(2,NP1) .GT. TRASH ) TRASH = R(2,NP1)	GRAP 161
DO 180 J=1,JOT	GRAP 162
180 XX(J) = R(MP1,J+NSTAGL) + ASH	GRAP 163
XX(1) = ASH	GRAP 164
XX(JOT) = TRASH	GRAP 165
CALL ADJST(XX,JOT,1,9.0,0.5,SCAL,XMIN,XY,1)	GRAP 166
DO 190 I=2,MP1	GRAP 167
DO 190 J=2,NP1	GRAP 168
X(I,J) = X(I,J) / SCAL	GRAP 169
190 R(I,J) = R(I,J) / SCAL + ASH - XMIN	GRAP 170
CALL CGAXES(3.0,0.5,X(MP1,NSTLP1),9.0,SCAL,SCAL,X(2,2),XMIN,	GRAP 171
1LABL,0)	GRAP 172
DO 200 I=MSTLP1,MSLLP1	GRAP 173
XSLOTL(I) = XSLOTL(I) / SCAL	GRAP 174
200 RSLOTL(I) = RSLOTL(I) / SCAL + ASH - XMIN	GRAP 175
DO 210 I=MSTUP1,MSLUP1	GRAP 176
XSLOTU(I) = XSLOTU(I) / SCAL	GRAP 177
210 RSLOTU(I) = RSLOTU(I) / SCAL + ASH - XMIN	GRAP 178
DO 220 I=1,M	GRAP 179
DO 220 J=2,NP1	GRAP 180
X(I,J) = X(I+1,J)	GRAP 181
220 R(I,J) = R(I+1,J)	GRAP 182
DO 230 I=1,M	GRAP 183
DO 230 J=1,N	GRAP 184
X(I,J) = X(I,J+1)	GRAP 185
230 R(I,J) = R(I,J+1)	GRAP 186
C	GRAP 187
C	GRAP 188
C	GRAP 189
GRAPH STREAMLINES	GRAP 190
DO 250 J=1,NSTLM1	GRAP 191
DO 240 I=1,MSLOTL	GRAP 192
XX(I) = X(I,J) + 3.0	GRAP 193
240 XY(I) = R(I,J) + 0.5	GRAP 194
250 CALL LINE(XX,XY,MSLOTL,1,0,0)	GRAP 195
DO 270 J=NSTAGL,NSTAGU	GRAP 196
DO 260 I=1,MP1	GRAP 197
XX(I) = X(I,J) + 3.0	GRAP 198
260 XY(I) = R(I,J) + 0.5	GRAP 199
270 CALL LINE(XX,XY,M,1,0,0)	GRAP 200
DO 290 J=NSTUP1,N	GRAP 201
DO 280 I=1,MSLOTU	GRAP 202
XX(I) = X(I,J) + 3.0	GRAP 203
280 XY(I) = R(I,J) + 0.5	GRAP 204
290 CALL LINE(XX,XY,MSLOTU,1,0,0)	GRAP 205
IOT = MSLOTL - MSTAGL + 1	GRAP 206
DO 300 I=1,IOT	GRAP 207
XX(I) = XSLOTL(I+MSTAGL) + 3.0	GRAP 208
300 XY(I) = RSLOTL(I+MSTAGL) + 0.5	GRAP 209
CALL LINE(XX,XY,IOT,1,0,0)	GRAP 210
IOT = MSLOTU - MSTAGU + 1	GRAP 211
DO 310 I=1,IOT	GRAP 212
XX(I) = XSLOTU(I+MSTAGU) + 3.0	GRAP 213
310 XY(I) = RSLOTU(I+MSTAGU) + 0.5	GRAP 214
CALL LINE(XX,XY,IOT,1,0,0)	GRAP 215
C	GRAP 216
C	GRAP 217
C	GRAP 218
GRAPH POTENTIAL LINES	GRAP 219
MINN = MSTAGL	GRAP 218
MAXX = MSTAGU	GRAP 219

IF (MSTAGU .LT. MSTAGL) MAXX = MSTAGL	GRAP 220
IF (MSTAGU .LT. MSTAGL) MINN = MSTAGU	GRAP 221
DO 330 I=1,MINN	GRAP 222
DO 320 J=1,N	GRAP 223
XX(J) = X(I,J) + 3.0	GRAP 224
320 XY(J) = R(I,J) + 0.5	GRAP 225
330 CALL LINE(XX,XY,N,1,0,0)	GRAP 226
MINNPI = MINN + 1	GRAP 227
IF (MSTAGL .EQ. MSTAGU) GO TO 415	GRAP 228
DO 410 I=MINNPI,MAXX	GRAP 229
IF (MSTAGL .GT. MSTAGU) GO TO 380	GRAP 230
DO 360 J=1,NSTLM1	GRAP 231
XX(J) = X(I,J) + 3.0	GRAP 232
360 XY(J) = R(I,J) + 0.5	GRAP 233
XX(NSTAGL) = XSLOTL(I) + 3.0	GRAP 234
XY(NSTAGL) = RSLOTL(I) + 0.5	GRAP 235
CALL LINE(XX,XY,NSTAGL,1,0,0)	GRAP 236
JOT = N - NSTAGL + 1	GRAP 237
DO 370 J=1,JOT	GRAP 238
XX(J) = X(I,J+NSTLM1) + 3.0	GRAP 239
370 XY(J) = R(I,J+NSTLM1) + 0.5	GRAP 240
CALL LINE(XX,XY,JOT,1,0,0)	GRAP 241
GO TO 410	GRAP 242
380 DO 390 J=1,NSTAGU	GRAP 243
XX(J) = X(I,J) + 3.0	GRAP 244
390 XY(J) = R(I,J) + 0.5	GRAP 245
CALL LINE(XX,XY,NSTAGU,1,0,0)	GRAP 246
JOT = N - NSTAGU + 1	GRAP 247
DO 400 J=2,JOT	GRAP 248
XX(J) = X(I,J+NSTUM1) + 3.0	GRAP 249
400 XY(J) = R(I,J+NSTUM1) + 0.5	GRAP 250
XX(1) = XSLOTU(I) + 3.0	GRAP 251
XY(1) = RSLOTU(I) + 0.5	GRAP 252
CALL LINE(XX,XY,JOT,1,0,0)	GRAP 253
410 CONTINUE	GRAP 254
415 CONTINUE	GRAP 255
JOT = NSTAGU - NSTAGL + 1	GRAP 256
DO 430 I=MAXX,M	GRAP 257
DO 420 J=1,JOT	GRAP 258
XX(J) = X(I,NSTLM1+J) + 3.0	GRAP 259
420 XY(J) = R(I,NSTLM1+J) + 0.5	GRAP 260
430 CALL LINE(XX,XY,JOT,1,0,0)	GRAP 261
JOT = NSTAGL - 1	GRAP 262
DO 450 I=MSTLP1,MSLOTL	GRAP 263
DO 440 J=1,JOT	GRAP 264
XX(J) = X(I,J) + 3.0	GRAP 265
440 XY(J) = R(I,J) + 0.5	GRAP 266
XX(NSTAGL) = XSLOTL(I+1) + 3.0	GRAP 267
XY(NSTAGL) = RSLOTL(I+1) + 0.5	GRAP 268
450 CALL LINE(XX,XY,NSTAGL,1,0,0)	GRAP 269
JOT = N - NSTAGU + 1	GRAP 270
DO 470 I=MSTUP1,MSLOTU	GRAP 271
DO 460 J=2,JOT	GRAP 272
XX(J) = X(I,J+NSTUM1) + 3.0	GRAP 273
460 XY(J) = R(I,J+NSTUM1) + 0.5	GRAP 274
XX(1) = XSLOTU(I+1) + 3.0	GRAP 275
XY(1) = RSLOTU(I+1) + 0.5	GRAP 276
470 CALL LINE(XX,XY,JOT,1,0,0)	GRAP 277
XLIN = X(M,NSTAGL) + 9.0	GRAP 278
	GRAP 279

C

C	GRAPH ANNULAR DIFFUSER IN PERSPECTIVE	GRAP 280
C		GRAP 281
	DO 480 J=1,N	GRAP 282
	DO 480 I=1,M	GRAP 283
	R(I,J) = SCAL * R(I,J) + ASH	GRAP 284
480	X(I,J) = SCAL * X(I,J)	GRAP 285
	JOT = NSTAGU - NSTAGL + 1	GRAP 286
	DO 490 J=1,JOT	GRAP 287
490	XX(J) = R(M,NSTAGL+J)	GRAP 288
	XX(1) = 0.0	GRAP 289
	XX(JOT) = TRASH + ASH	GRAP 290
	CALL ADJUST(XX,JOT,1,9.0,0.5,ZCAL,XMIN,XY,1)	GRAP 291
	DO 500 I=1,M	GRAP 292
	DO 500 J=1,N	GRAP 293
	X(I,J) = X(I,J) / ZCAL	GRAP 294
500	R(I,J) = R(I,J) / ZCAL	GRAP 295
	DO 510 I=MSTLPL,MSLLPL	GRAP 296
	XSLOTL(I) = ( XSLOTL(I) * SCAL ) / ZCAL	GRAP 297
510	RSLOTL(I) = ( RSLOTL(I) * SCAL + ASH ) / ZCAL	GRAP 298
	DO 520 I=MSTUPL,MSLUP1	GRAP 299
	XSLOTU(I) = ( XSLOTU(I) * SCAL ) / ZCAL	GRAP 300
520	RSLOTU(I) = ( RSLOTU(I) * SCAL + ASH ) / ZCAL	GRAP 301
	CALL CGAXES(XLIN,0.5,X(M,NSTAGL),9.0,ZCAL,ZCAL,0.0,0.0,LABL,0)	GRAP 302
C		GRAP 303
C	GRAPH STREAMLINES	GRAP 304
C		GRAP 305
	DO 530 I=1,MSLOTL	GRAP 306
	XX(I) = X(I,1) + XLIN	GRAP 307
530	XY(I) = R(I,1) + 0.5	GRAP 308
	CALL LINE(XX,XY,MSLOTL,1,0,0)	GRAP 309
	IOT = M - MSTAGL + 1	GRAP 310
	DO 540 I=1,IOT	GRAP 311
	XX(I) = X(I+MSTLM1,NSTAGL) + XLIN	GRAP 312
540	XY(I) = R(I+MSTLM1,NSTAGL) + 0.5	GRAP 313
	CALL LINE(XX,XY,IOT,1,0,0)	GRAP 314
	IOT = MSLOTL - MSTAGL + 1	GRAP 315
	DO 550 I=1,IOT	GRAP 316
	XX(I) = XSLOTL(I+MSTAGL) + XLIN	GRAP 317
550	XY(I) = RSLOTL(I+MSTAGL) + 0.5	GRAP 318
	CALL LINE(XX,XY,IOT,1,0,0)	GRAP 319
	DO 560 I=1,MSLOTU	GRAP 320
	XX(I) = X(I,N) + XLIN	GRAP 321
560	XY(I) = R(I,N) + 0.5	GRAP 322
	CALL LINE(XX,XY,MSLOTU,1,0,0)	GRAP 323
	IOT = M - MSTAGU + 1	GRAP 324
	DO 570 I=1,IOT	GRAP 325
	XX(I) = X(I+MSTUM1,NSTAGU) + XLIN	GRAP 326
570	XY(I) = R(I+MSTUM1,NSTAGU) + 0.5	GRAP 327
	CALL LINE(XX,XY,IOT,1,0,0)	GRAP 328
	IOT = MSLOTU - MSTAGU + 1	GRAP 329
	DO 580 I=1,IOT	GRAP 330
	XX(I) = XSLOTU(I+MSTAGU) + XLIN	GRAP 331
580	XY(I) = RSLOTU(I+MSTAGU) + 0.5	GRAP 332
	CALL LINE(XX,XY,IOT,1,0,0)	GRAP 333
C		GRAP 334
C	GRAPH POTENTIAL LINES	GRAP 335
C		GRAP 336
	DO 590 J=1,N	GRAP 337
	XX(J) = X(1,J) + XLIN	GRAP 338
590	XY(J) = R(1,J) + 0.5	GRAP 339



CALL LINE(XX,XY,N,1,0,0)	GRAP 340
JOT = NSTAGU - NSTAGL + 1	GRAP 341
DO 600 J=1,JOT	GRAP 342
XX(J) = X(M,J+NSTLM1) + XLIN	GRAP 343
600 XY(J) = R(M,J+NSTLM1) + 0.5	GRAP 344
CALL LINE(XX,XY,JOT,1,0,0)	GRAP 345
DO 610 I=1,M	GRAP 346
DO 610 J=1,N	GRAP 347
X(I,J) = ( X(I,J) * ZCAL ) / SCAL	GRAP 348
610 R(I,J) = ( R(I,J) * ZCAL - ASH ) / SCAL	GRAP 349
XLIN = XLIN + X(M,NSTAGL) + 9.0	GRAP 350
C	GRAP 351
C	GRAP 352
C	GRAP 353
C	GRAP 354
2000 IF (FLAG2 .LE. 0) GO TO 3000	GRAP 355
DATA WABL(1)/' ',WABL(2)/' ',WABL(3)/' ',	GRAP 356
1 WABL(4)/' ',	GRAP 357
DATA WABL(5)/' Q A',WABL(6)/' XIS '	GRAP 358
DATA WABL(7)/' ',WABL(8)/' ',WABL(9)/' ',	GRAP 359
1 WABL(10)/' ',	GRAP 360
DATA WABL(11)/' ',WABL(12)/' ',	GRAP 361
1 WABL(13)/' ',WABL(14)/' ',	GRAP 362
DATA WABL(15)/' N A',WABL(16)/' XIS '	GRAP 363
DATA WABL(17)/' ',WABL(18)/' ',	GRAP 364
1 WABL(19)/' ',WABL(20)/' ',	GRAP 365
DO 615 J=2,NP1	GRAP 366
DO 615 I=2,MP1	GRAP 367
P = Q(I,J)	GRAP 368
615 Q(I,J) = DEXP(P)	GRAP 369
XX(NP1) = 0.0	GRAP 370
DO 620 J=1,N	GRAP 371
620 XX(J) = Q(2,J+1)	GRAP 372
CALL ADJST(XX,NP1,1,9.0,0.5,SSCAL,XMIN,XY,1)	GRAP 373
CALL CGAXES(XLIN,0.5,12.0,9.0,SSCAL,SCAL,XMIN,0.0,WABL,0)	GRAP 375
DO 630 J=1,N	GRAP 376
XX(J) = ( Q(2,J+1) - XMIN ) / SSCAL + XLIN	GRAP 377
630 XY(J) = R(1,J) + 0.5	GRAP 378
CALL LINE(XX,XY,N,1,0,0)	GRAP 379
IF (FLAG1 .GT. 0 .OR. FLAG3 .GT. 0) NSTAGL = 1	GRAP 380
JOT = NSTAGU - NSTAGL + 1	GRAP 381
DO 640 J=1,JOT	GRAP 382
XX(J) = ( Q(MP1,J+NSTAGL) - XMIN ) / SSCAL + XLIN	GRAP 383
640 XY(J) = R(M,J+NSTAGL-1) + 0.5	GRAP 384
CALL LINE(XX,XY,JOT,1,0,0)	GRAP 385
C	GRAP 386
C	GRAP 387
C	GRAP 388
3000 XSET = XLIN + 15.0	GRAP 389
CALL PLOT1(XSET,0.0,-3)	GRAP 390
WRITE(3,650)	GRAP 391
650 FORMAT(1H1,T2,'GRAPHICAL OUTPUT COMPLETED PROGRAM ',	GRAP 392
1T37,'SIGNING OFF')	GRAP 393
RETURN	GRAP 394
END	GRAP 394

## APPENDIX B - DIFFUSER DESIGN

This appendix describes the procedure used in designing the 18-inch (46 cm) annular diffuser. One should realize that the final design contour is rarely if ever the result of a first trial program. Several reruns are nearly always necessary to achieve the desired geometry because such parameters as AR and L/W are not input directly even though specific values of these may be the ultimate goal.

For the 18-inch (46 cm) annular diffuser, the aim was to design a diffuser with the following features: (1) an area ratio of about 3:1 (2) an inlet width of about 2 inches (5.08 cm) (3) an exit outer diameter of about 18-inches (46 cm) (4) an effective length for boundary layer growth upstream of the slot of about 3 inches (7.6 cm). Items (1) and (4) were the same as the previously designed 9-inch (23 cm) diffuser, while items (2) and (3) were twice as large.

The design program was used to design both the accelerating nozzle (inlet section) and the diffuser itself as one flow channel. Wall velocity vector magnitude ratio ( $Q$ ) increasing from 1.0 to 3.0 in the nozzle portion and from 3.0 to 3.5 from the narrowest portion of the channel to the slot were prescribed. By prescribing a favorable velocity gradient upstream of the slot, it was thought that slot widths ranging from the design width to several times the design width could be tested. (As the slot is widened, there is a tendency for the wall velocity just upstream of the slot to decrease, thus producing a possibly unfavorable velocity gradient.) Downstream of the slot,  $Q$  along the wall was prescribed to be constant at 0.83. The  $Q$  ratio of 3.0 at diffuser inlet to 0.83 at exit is larger than the desired AR because suction

removes some of the flow and because the diffuser inlet and exit profiles were not precisely uniform. The value 0.83 was arrived at after several trial runs. (A good first trial for  $Q$  is  $\frac{(1 - FS) Q_i}{AR}$  which is 0.95 in this case.) To get the appropriate values of  $\phi$  for the desired velocities, recognize that

$$\phi_2 - \phi_1 = \int_{S_1}^{S_2} Q \, dS$$

After adopting a model such as Figure 21 corresponding values of  $Q$  and  $\phi$  can be found.

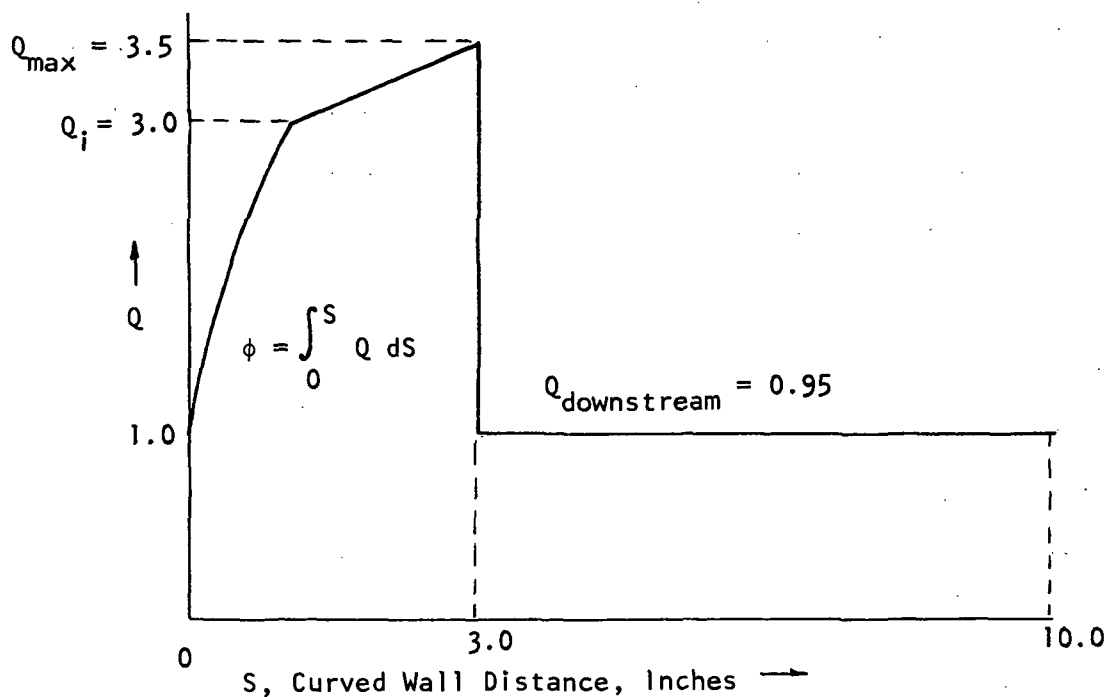


Figure 21. Prescribed wall velocity as design input.

The proper range of  $\psi$  can be determined by applying  $R_2^2 - R_1^2 = 2 \int_{\phi} \frac{\cos \alpha}{Q} d\psi$  at either the inlet or the exit passage. At inlet, a 7-inch (17.8 cm) outer radius and a 5-inch (12.7 cm) inner radius were desirable since these dimensions

would enable the first three items of the previously listed characteristics to be attainable. Thus

$$\Psi \cong \frac{3(7^2 - 5^2)}{2} = 36$$

was a good first trial value. (For the final design,  $\Psi$  was adjusted to 33.5.) Increments  $\Delta\psi$  were selected to be much smaller at each wall, and increments  $\Delta\phi$  were selected smaller in the vicinity of the slot. This enabled better resolution to be obtained in the troublesome slot region and a minimizing of the error introduced by the wedge flow patch at the stagnation point. The program requires that  $\Delta\phi = \Delta\psi$  in the grid network immediately around the stagnation point, and these were arbitrarily given a value of 0.05 for this program. The upper slot contained 7 streamlines (including wall and stagnation point streamlines) and 4 potential flow lines. The lower slot contained 6 streamlines and 4 potential flow lines. The number of streamlines contained in each slot and the exact value of each  $\Delta\psi$  in the vicinity of the slot must be adjusted so that the flow area represented by these  $\Delta\psi$ 's is sufficient to pass the design suction flow for that slot. If, for example, 2% suction is desired through the inner slot and 4% through the outer slot (these values were close to but not precisely the design suction rates), then

$$\begin{array}{l} \Sigma \Delta\psi = .02 \Sigma \Delta\psi = .02\Psi \\ \text{across inner slot} \quad \text{total} \end{array}$$

$$\text{and} \quad \begin{array}{l} \Sigma \Delta\psi = .04 \Sigma \Delta\psi = .04\Psi \\ \text{across outer slot} \quad \text{total} \end{array}$$

For the previously named first trial  $\Psi$  of 36, this would yield 0.72 as the value of  $\psi$  for the lower slot stagnation streamline and  $36.0 - 1.44$  or 34.56 for the upper slot stagnation streamline. The final design had 0.65 as the lower slot stagnation streamline, 32.4 for the upper slot stagnation stream-

line, and 33.5 for  $\Psi$ . This is equivalent to 0.65/33.5 or 1.94% lower slot suction and  $(33.5 - 32.4)/33.5$  or 3.28% upper slot suction and 5.22% total suction. The design suction percentage was determined by assuming the boundary layer growth to be the same as that along a flat plate, and the velocity profile to obey the 1/7 power law, and applying Taylor's criterion to determine how much fluid must be removed.

The total number of potential flow lines,  $M$ , was arbitrarily selected as 127 (a maximum of 148 may be used), while 45 total streamlines ( $N$ ) were used (maximum 48).  $MIDJ$ , the number of the "center streamline," was 21.  $MIDJ$  and the  $\Delta\psi$  values in the vicinity of this streamline may have to be adjusted from the first trial values to prevent the design from becoming extremely asymmetrical, possibly crossing the  $X$ -axis. This situation will result in a divide check, an overflow, or an underflow, with subsequent program termination.

Dirichlet boundary conditions were used at the flow channel inlet (not to be confused with the diffuser inlet) with a constant velocity magnitude ratio,  $Q$ , (not parallel) across the channel of 1.0 being specified. At the flow channel exit (which was also the diffuser exit), Neumann boundary conditions were specified to yield parallel (not necessarily uniform) flow across the exit plane.

The next two pages show the input data which was used to design the 18-inch (46 cm) annular diffuser. Following the input data is the first page of output which summarizes the control input data. Then the graphical output (figure 22) is shown reduced in size from the original output. Also shown is a listing of inner and outer wall radii.

THE FOLLOWING DATA WAS INPUT TO DESIGN THE 18-INCH ANNULAR DIFFUSER

2 1 BIG ANNULAR DIFFUSER DESIGN

070171 0011

0.00	1.70	.00005000	.00005000	84	84
127	45	10	50	39	6
3.9100	21	11	51	87	87
0.0	0.1	0.2	0.3	0.4	0.5
0.6	0.7	0.8	0.9	1.0	1.1
1.2	1.3	1.4	1.5	1.6	1.7
1.8	1.9	2.0	2.1	2.2	2.3
2.4	2.5	2.6	2.7	2.8	2.9
3.0	3.1	3.2	3.3	3.4	3.5
3.6	3.7	3.8	3.9	4.0	4.1
4.2	4.3	4.4	4.5	4.6	4.7
4.8	4.9	5.0	5.1	5.2	5.3
5.4	5.5	5.6	5.7	5.8	5.9
6.0	6.1	6.2	6.3	6.4	6.5
6.6	6.7	6.8	6.9	7.0	7.1
7.2	7.3	7.4	7.5	7.6	7.7
7.8	7.9	8.0	8.1	8.15	8.20
8.25	8.30	8.35	8.4	8.45	8.5
8.6	8.7	8.8	8.9	9.05	9.2
9.35	9.50	9.65	9.80	9.95	10.10
10.25	10.40	10.55	10.70	10.85	11.00
11.15	11.30	11.45	11.60	11.75	11.90
12.05	12.20	12.35	12.50	12.65	12.80
12.95	13.10	13.25	13.40	13.55	13.70
13.85					
1.000	1.28412	1.49755	1.65381	1.79784	1.91427
2.02216	2.10813	2.18835	2.26306	2.33251	2.39693
2.44696	2.50280	2.54602	2.58637	2.62400	2.65903
2.69126	2.72190	2.75002	2.77611	2.80031	2.81842
2.83958	2.85926	2.87403	2.89137	2.90763	2.91993
2.93457	2.94576	2.95923	2.96967	2.98243	2.99249
3.00500	3.01500	3.02750	3.03750	3.05000	3.06000
3.07000	3.08000	3.09247	3.10250	3.11250	3.12500
3.13500	3.14500	3.15500	3.16750	3.17748	3.18750
3.19748	3.20747	3.21748	3.22998	3.23998	3.24998
3.25998	3.26998	3.27998	3.28998	3.29998	3.30998
3.31998	3.32998	3.33998	3.34998	3.35998	3.36998
3.37998	3.38998	3.39998	3.40998	3.41998	3.42997
3.43997	3.44747	3.45747	3.46747	3.47247	3.47747
3.48247	3.48747	3.49247			
0.830	0.830	0.830	0.830	0.830	0.830
0.830	0.830	0.830	0.830	0.830	0.830
0.830	0.830	0.830	0.830	0.830	0.830
0.830	0.830	0.830	0.830	0.830	0.830
0.830	0.830	0.830	0.830	0.830	0.830
0.830	0.830	0.830	0.830	0.830	0.830
0.830	0.830	0.830	0.830	0.830	0.830
0.830	0.830	0.830	0.830	0.830	0.830
0.830	0.830	0.830	0.830	0.830	0.830
0.830	0.830	0.830	0.830	0.830	0.830
1.00000	1.28412	1.49755	1.65381	1.79784	1.91427
2.02216	2.10813	2.18835	2.26306	2.33251	2.39693
2.44696	2.50280	2.54602	2.58637	2.62400	2.65903
2.69126	2.72190	2.75002	2.77611	2.80031	2.81842
2.83958	2.85926	2.87403	2.89137	2.90763	2.91993
2.93457	2.94576	2.95923	2.96967	2.98243	2.99249



CLEMSON UNIVERSITY

MECHANICAL ENGINEERING DEPARTMENT

PROGRAM 70-02

AXIALLY SYMMETRIC AND 2-D BRANCHED CHANNEL DESIGN

\*\*\*\*\* BIG ANNULAR DIFFUSER DESIGN

7/ 1/71 CASE NO. 11 \*\*\*\*\*

----- CONTROL DATA -----

FLAG1 =0	RMULT =	0.0	M =	127	RADIN =	3.91000
FLAG2 =2	W =	1.700000	N =	45	MIDJ =	21
FLAG3 =0	TOLSYS =	0.000050	MXISYS =	10	IPRSYS =	11
FLAG4 =1	TOLDE =	0.000050	MXIDE =	50	IPRDE =	51
	MSTAGU =	84	NSTAGU =	39	MSLOTU =	87
	MSTAGL =	84	NSTAGL =	6	MSLOTL =	87

----- OPTIONS -----

AXIALLY SYMMETRIC

DIRICHLET B. C. AT INLET AND NEUMANN B. C. AT OUTLET  
WITH VELOCITY INPUT AT INLET

ANNULAR DIFFUSER - NOZZLE

GRAPHICAL OUTPUT



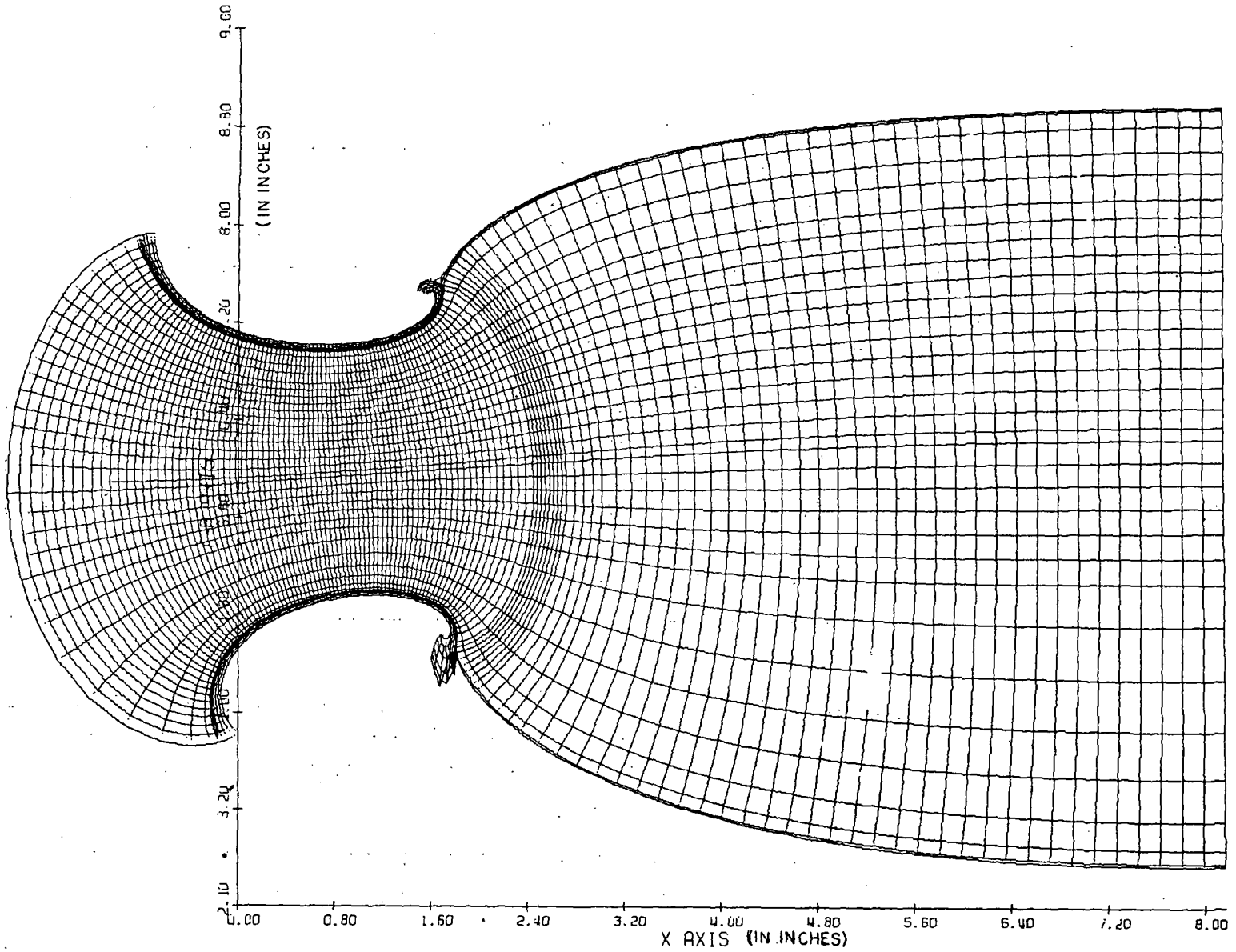


Figure 22. Graphical output showing streamlines and equipotential lines and wall coordinates for 18-inch (46 cm) annular diffuser.

SUMMARY OF INLET WALL COORDINATES OF DIFFUSER (UPPER WALL)

X	R	Q	S	ALPHA
-0.699307E 00	0.801371E 01	0.100000E 01	0.0	-0.157854E 01
-0.697799E 00	0.793128E 01	0.128412E 01	0.880181E-01	-0.147606E 01
-0.685813E 00	0.785777E 01	0.149755E 01	0.159424E 00	-0.137102E 01
-0.668520E 00	0.779451E 01	0.165381E 01	0.222923E 00	-0.127491E 01
-0.647939E 00	0.773845E 01	0.179784E 01	0.280845E 00	-0.118974E 01
-0.624546E 00	0.768814E 01	0.191427E 01	0.334726E 00	-0.111102E 01
-0.599172E 00	0.764241E 01	0.202216E 01	0.385522E 00	-0.103905E 01
-0.571913E 00	0.760064E 01	0.210813E 01	0.433943E 00	-0.973163E 00
-0.543409E 00	0.756214E 01	0.218835E 01	0.480485E 00	-0.914747E 00
-0.513902E 00	0.752656E 01	0.226306E 01	0.525411E 00	-0.860717E 00
-0.483603E 00	0.749362E 01	0.233251E 01	0.568925E 00	-0.809925E 00
-0.452665E 00	0.746310E 01	0.239693E 01	0.611196E 00	-0.760975E 00
-0.421096E 00	0.743480E 01	0.244696E 01	0.652465E 00	-0.716066E 00
-0.389138E 00	0.740842E 01	0.250280E 01	0.692856E 00	-0.673961E 00
-0.356773E 00	0.738393E 01	0.254602E 01	0.732453E 00	-0.633235E 00
-0.324080E 00	0.736108E 01	0.258637E 01	0.771419E 00	-0.595931E 00
-0.291140E 00	0.733977E 01	0.262400E 01	0.809801E 00	-0.560900E 00
-0.257984E 00	0.731986E 01	0.265903E 01	0.847655E 00	-0.527809E 00
-0.224671E 00	0.730128E 01	0.269126E 01	0.885033E 00	-0.496518E 00
-0.191245E 00	0.728393E 01	0.272190E 01	0.921978E 00	-0.466752E 00
-0.157726E 00	0.726773E 01	0.275001E 01	0.958525E 00	-0.438289E 00
-0.124130E 00	0.725264E 01	0.277611E 01	0.994715E 00	-0.411107E 00
-0.904713E-01	0.723856E 01	0.280030E 01	0.103058E 01	-0.384790E 00
-0.567531E-01	0.722548E 01	0.281841E 01	0.106618E 01	-0.360296E 00
-0.230089E-01	0.721326E 01	0.283957E 01	0.110153E 01	-0.337472E 00
0.107403E-01	0.720190E 01	0.285925E 01	0.113662E 01	-0.314906E 00
0.445117E-01	0.719135E 01	0.287403E 01	0.117149E 01	-0.293746E 00
0.782807E-01	0.718154E 01	0.289136E 01	0.120618E 01	-0.273918E 00
0.112004E 00	0.717245E 01	0.290763E 01	0.124067E 01	-0.254252E 00
0.145722E 00	0.716407E 01	0.291992E 01	0.127499E 01	-0.235669E 00
0.179415E 00	0.715632E 01	0.293456E 01	0.130915E 01	-0.217955E 00
0.213065E 00	0.714920E 01	0.294576E 01	0.134317E 01	-0.200973E 00
0.246683E 00	0.714266E 01	0.295922E 01	0.137704E 01	-0.184706E 00
0.280251E 00	0.713669E 01	0.296967E 01	0.141077E 01	-0.169009E 00
0.313775E 00	0.713125E 01	0.298243E 01	0.144438E 01	-0.153909E 00
0.347243E 00	0.712633E 01	0.299249E 01	0.147785E 01	-0.139307E 00
0.380622E 00	0.712190E 01	0.300499E 01	0.151120E 01	-0.125108E 00
0.413945E 00	0.711797E 01	0.301498E 01	0.154443E 01	-0.111278E 00
0.447179E 00	0.711449E 01	0.302749E 01	0.157753E 01	-0.977013E-01

0.480333E 00	0.711148E 01	0.303748E 01	0.161050E 01	-0.843255E-01
0.513400E 00	0.710892E 01	0.304999E 01	0.164336E 01	-0.710913E-01
0.546371E 00	0.710681E 01	0.305999E 01	0.167609E 01	-0.577618E-01
0.579260E 00	0.710513E 01	0.306998E 01	0.170872E 01	-0.448380E-01
0.612046E 00	0.710388E 01	0.307998E 01	0.174124E 01	-0.322427E-01
0.644735E 00	0.710303E 01	0.309246E 01	0.177364E 01	-0.194190E-01
0.677315E 00	0.710262E 01	0.310248E 01	0.180593E 01	-0.629646E-02
0.709790E 00	0.710264E 01	0.311249E 01	0.183811E 01	0.647169E-02
0.742153E 00	0.710306E 01	0.312498E 01	0.187017E 01	0.196210E-01
0.774394E 00	0.710392E 01	0.313499E 01	0.190211E 01	0.332333E-01
0.806537E 00	0.710521E 01	0.314498E 01	0.193396E 01	0.467528E-01
0.838545E 00	0.710693E 01	0.315499E 01	0.196571E 01	0.603038E-01
0.870418E 00	0.710907E 01	0.316748E 01	0.199734E 01	0.744864E-01
0.902163E 00	0.711168E 01	0.317747E 01	0.202886E 01	0.893180E-01
0.933763E 00	0.711475E 01	0.318748E 01	0.206028E 01	0.104379E 00
0.965232E 00	0.711829E 01	0.319747E 01	0.209160E 01	0.119833E 00
0.996552E 00	0.712232E 01	0.320746E 01	0.212282E 01	0.135771E 00
0.102771E 01	0.712683E 01	0.321748E 01	0.215395E 01	0.152148E 00
0.105871E 01	0.713184E 01	0.322997E 01	0.218497E 01	0.169524E 00
0.108951E 01	0.713740E 01	0.323997E 01	0.221588E 01	0.188011E 00
0.112012E 01	0.714351E 01	0.324997E 01	0.224670E 01	0.207168E 00
0.115053E 01	0.715021E 01	0.325998E 01	0.227742E 01	0.227265E 00
0.118073E 01	0.715751E 01	0.326997E 01	0.230804E 01	0.248460E 00
0.121068E 01	0.716545E 01	0.327997E 01	0.233858E 01	0.270872E 00
0.124036E 01	0.717405E 01	0.328997E 01	0.236902E 01	0.294692E 00
0.126977E 01	0.718335E 01	0.329997E 01	0.239937E 01	0.320056E 00
0.129887E 01	0.719339E 01	0.330997E 01	0.242962E 01	0.347209E 00
0.132758E 01	0.720421E 01	0.331997E 01	0.245979E 01	0.376464E 00
0.135591E 01	0.721587E 01	0.332997E 01	0.248986E 01	0.408066E 00
0.138377E 01	0.722842E 01	0.333997E 01	0.251985E 01	0.442398E 00
0.141111E 01	0.724191E 01	0.334997E 01	0.254974E 01	0.479924E 00
0.143785E 01	0.725643E 01	0.335997E 01	0.257955E 01	0.521236E 00
0.146388E 01	0.727204E 01	0.336998E 01	0.260926E 01	0.567117E 00
0.148907E 01	0.728884E 01	0.337997E 01	0.263889E 01	0.618589E 00
0.151325E 01	0.730691E 01	0.338997E 01	0.266844E 01	0.677078E 00
0.153619E 01	0.732637E 01	0.339997E 01	0.269789E 01	0.744553E 00
0.155760E 01	0.734732E 01	0.340997E 01	0.272726E 01	0.823958E 00
0.157704E 01	0.736986E 01	0.341998E 01	0.275654E 01	0.919744E 00
0.159392E 01	0.739412E 01	0.342996E 01	0.278574E 01	0.103900E 01
0.160736E 01	0.742018E 01	0.343996E 01	0.281485E 01	0.119361E 01
0.161615E 01	0.744842E 01	0.344746E 01	0.284389E 01	0.140277E 01
0.161876E 01	0.748096E 01	0.345747E 01	0.287285E 01	0.169840E 01
0.161507E 01	0.752623E 01	0.346746E 01	0.290173E 01	0.213280E 01
0.160530E 01	0.753676E 01	0.347246E 01	0.291614E 01	0.250805E 01

0.159233E 01	0.754261E 01	0.347746E 01	0.293053E 01	0.294370E 01
0.157811E 01	0.754202E 01	0.348246E 01	0.294490E 01	0.341566E 01
0.156573E 01	0.753508E 01	0.348746E 01	0.295924E 01	0.389990E 01
0.155818E 01	0.752339E 01	0.349246E 01	0.297357E 01	0.437780E 01

SUMMARY OF DOWNSTREAM WALL COORDINATES OF DIFFUSER (UPPER WALL).

X	R	Q	S	ALPHA
0.167012E 01	0.765809E 01	0.100000E 01	0.0	0.285718E 01
0.170109E 01	0.770311E 01	0.830000E 00	0.546426E-01	0.111739E 01
0.173193E 01	0.775789E 01	0.830000E 00	0.114883E 00	0.101841E 01
0.176704E 01	0.780935E 01	0.830000E 00	0.175124E 00	0.937877E 00
0.180540E 01	0.785774E 01	0.830000E 00	0.235365E 00	0.871287E 00
0.184630E 01	0.790338E 01	0.830000E 00	0.295606E 00	0.814893E 00
0.188910E 01	0.794649E 01	0.830000E 00	0.355847E 00	0.766357E 00
0.197973E 01	0.802632E 01	0.830000E 00	0.476328E 00	0.685222E 00
0.207568E 01	0.809920E 01	0.830000E 00	0.596810E 00	0.619281E 00
0.217554E 01	0.816603E 01	0.830000E 00	0.717291E 00	0.554065E 00
0.227840E 01	0.822757E 01	0.830000E 00	0.837773E 00	0.516799E 00
0.243722E 01	0.831117E 01	0.830000E 00	0.101850E 01	0.456696E 00
0.260025E 01	0.833592E 01	0.830000E 00	0.119922E 01	0.406356E 00
0.276643E 01	0.845301E 01	0.830000E 00	0.137994E 01	0.363449E 00
0.293509E 01	0.851342E 01	0.830000E 00	0.156066E 01	0.326374E 00
0.310570E 01	0.856796E 01	0.830000E 00	0.174138E 01	0.293998E 00
0.327788E 01	0.861730E 01	0.830000E 00	0.192210E 01	0.265491E 00
0.345135E 01	0.866203E 01	0.830000E 00	0.210283E 01	0.240230E 00
0.362587E 01	0.870262E 01	0.830000E 00	0.228355E 01	0.217724E 00
0.380126E 01	0.873950E 01	0.830000E 00	0.246427E 01	0.197582E 00
0.397739E 01	0.877304E 01	0.830000E 00	0.264499E 01	0.179487E 00
0.415413E 01	0.880357E 01	0.830000E 00	0.282571E 01	0.163181E 00
0.433140E 01	0.883136E 01	0.830000E 00	0.300644E 01	0.148448E 00
0.450910E 01	0.885669E 01	0.830000E 00	0.318716E 01	0.135097E 00
0.468719E 01	0.887976E 01	0.830000E 00	0.336788E 01	0.122973E 00
0.486561E 01	0.890077E 01	0.830000E 00	0.354860E 01	0.111936E 00
0.504430E 01	0.891992E 01	0.830000E 00	0.372932E 01	0.101870E 00
0.522323E 01	0.893736E 01	0.830000E 00	0.391004E 01	0.926709E-01
0.540238E 01	0.895322E 01	0.830000E 00	0.409076E 01	0.842395E-01
0.558170E 01	0.896764E 01	0.830000E 00	0.427149E 01	0.764982E-01
0.576119E 01	0.898073E 01	0.830000E 00	0.445221E 01	0.693699E-01
0.594080E 01	0.899261E 01	0.830000E 00	0.463293E 01	0.627882E-01
0.612055E 01	0.900334E 01	0.830000E 00	0.481365E 01	0.566900E-01

0.630040E 01	0.901302E 01	0.830000E 00	0.499438E 01	0.510197E-01
0.648033E 01	0.902172E 01	0.830000E 00	0.517510E 01	0.457353E-01
0.666034E 01	0.902951E 01	0.830000E 00	0.535582E 01	0.407826E-01
0.684046E 01	0.903642E 01	0.830000E 00	0.553654E 01	0.360934E-01
0.702063E 01	0.904253E 01	0.830000E 00	0.571726E 01	0.316626E-01
0.720085E 01	0.904785E 01	0.830000E 00	0.589798E 01	0.274436E-01
0.738112E 01	0.905242E 01	0.830000E 00	0.607871E 01	0.234045E-01
0.756142E 01	0.905630E 01	0.830000E 00	0.625943E 01	0.195101E-01
0.774174E 01	0.905946E 01	0.830000E 00	0.644015E 01	0.157398E-01
0.792213E 01	0.906198E 01	0.830000E 00	0.662087E 01	0.120344E-01
0.810067E 01	0.906380E 01	0.830000E 00	0.680159E 01	0.974582E-02

SUMMARY OF WALL COORDINATES INSIDE OF DIFFUSER SLOT (UPPER WALL)

X	R	Q	S	ALPHA
0.167012E 01	0.765809E 01	0.0	0.0	0.285718E 01
0.195353E 01	0.763134E 01	0.830000E 00	0.119616E 00	0.341848E 01
0.190178E 01	0.760217E 01	0.830000E 00	0.179856E 00	0.390385E 01
0.146956E 01	0.754968E 01	0.830000E 00	0.240097E 00	0.444185E 01

SUMMARY OF INLET WALL COORDINATES OF DIFFUSER (LOWER WALL)

X	R	Q	S	ALPHA
0.0	0.391000E 01	0.100000E 01	0.0	0.224947E 01
-0.522614E-01	0.396167E 01	0.128412E 01	0.880181E-01	0.211946E 01
-0.888348E-01	0.401695E 01	0.149755E 01	0.159424E 00	0.198959E 01
-0.113682E 00	0.406892E 01	0.165381E 01	0.222923E 00	0.186774E 01
-0.130419E 00	0.411868E 01	0.179784E 01	0.280845E 00	0.175798E 01
-0.140355E 00	0.416647E 01	0.191427E 01	0.334726E 00	0.165572E 01
-0.144936E 00	0.421239E 01	0.202216E 01	0.385522E 00	0.156114E 01
-0.144800E 00	0.425654E 01	0.210813E 01	0.433943E 00	0.147362E 01
-0.140841E 00	0.429900E 01	0.218835E 01	0.480485E 00	0.139454E 01
-0.133610E 00	0.433975E 01	0.226306E 01	0.525411E 00	0.132079E 01
-0.123518E 00	0.437879E 01	0.233251E 01	0.568925E 00	0.125124E 01
-0.110930E 00	0.441609E 01	0.239693E 01	0.611196E 00	0.118445E 01
-0.960225E-01	0.445176E 01	0.244696E 01	0.652465E 00	0.112266E 01
-0.792452E-01	0.448588E 01	0.250280E 01	0.692856E 00	0.106459E 01
-0.606857E-01	0.451840E 01	0.254602E 01	0.732453E 00	0.100879E 01

-0.405791E-01	0.454947E 01	0.258637E 01	-0.771419E 00	0.957263E 00
-0.191262E-01	0.457912E 01	0.262400E 01	0.809801E 00	0.908799E 00
0.352591E-02	0.460741E 01	0.265903E 01	0.847655E 00	0.863020E 00
0.272374E-01	0.463437E 01	0.269126E 01	0.885033E 00	0.819772E 00
0.518910E-01	0.466007E 01	0.272190E 01	0.921978E 00	0.778762E 00
0.773776E-01	0.468454E 01	0.275001E 01	0.958525E 00	0.739717E 00
0.103615E 00	0.470784E 01	0.277611E 01	0.994715E 00	0.702566E 00
0.130536E 00	0.473001E 01	0.280030E 01	0.103058E 01	0.666868E 00
0.158077E 00	0.475108E 01	0.281841E 01	0.106618E 01	0.633534E 00
0.186144E 00	0.477117E 01	0.283957E 01	0.110153E 01	0.602375E 00
0.214680E 00	0.479026E 01	0.285925E 01	0.113662E 01	0.571968E 00
0.243651E 00	0.480840E 01	0.287403E 01	0.117149E 01	0.543395E 00
0.273003E 00	0.482567E 01	0.289136E 01	0.120618E 01	0.516572E 00
0.302662E 00	0.484207E 01	0.290763E 01	0.124067E 01	0.490305E 00
0.332642E 00	0.485764E 01	0.291992E 01	0.127499E 01	0.465504E 00
0.362884E 00	0.487243E 01	0.293456E 01	0.130915E 01	0.441922E 00
0.393351E 00	0.488645E 01	0.294576E 01	0.134317E 01	0.419361E 00
0.424039E 00	0.489977E 01	0.295922E 01	0.137704E 01	0.397831E 00
0.454915E 00	0.491239E 01	0.296967E 01	0.141077E 01	0.377158E 00
0.485929E 00	0.492434E 01	0.298243E 01	0.144438E 01	0.357297E 00
0.517078E 00	0.493564E 01	0.299249E 01	0.147785E 01	0.338157E 00
0.548330E 00	0.494633E 01	0.300499E 01	0.151120E 01	0.319648E 00
0.579686E 00	0.495640E 01	0.301498E 01	0.154443E 01	0.301689E 00
0.611099E 00	0.496589E 01	0.302749E 01	0.157753E 01	0.284139E 00
0.642576E 00	0.497480E 01	0.303748E 01	0.161050E 01	0.266941E 00
0.674103E 00	0.498315E 01	0.304999E 01	0.164336E 01	0.250018E 00
0.705672E 00	0.499093E 01	0.305999E 01	0.167609E 01	0.233135E 00
0.737271E 00	0.499817E 01	0.306998E 01	0.170872E 01	0.216764E 00
0.768873E 00	0.500487E 01	0.307998E 01	0.174124E 01	0.200804E 00
0.800478E 00	0.501105E 01	0.309246E 01	0.177364E 01	0.184669E 00
0.832075E 00	0.501669E 01	0.310248E 01	0.180593E 01	0.168287E 00
0.863653E 00	0.502180E 01	0.311249E 01	0.183811E 01	0.152290E 00
0.895206E 00	0.502639E 01	0.312498E 01	0.187017E 01	0.135944E 00
0.926719E 00	0.503043E 01	0.313499E 01	0.190211E 01	0.119151E 00
0.958192E 00	0.503394E 01	0.314498E 01	0.193396E 01	0.102403E 00
0.989616E 00	0.503690E 01	0.315499E 01	0.196571E 01	0.856250E-01
0.102098E 01	0.503933E 01	0.316748E 01	0.199734E 01	0.682125E-01
0.105227E 01	0.504119E 01	0.317747E 01	0.202886E 01	0.500863E-01
0.108348E 01	0.504247E 01	0.318748E 01	0.206028E 01	0.316566E-01
0.111461E 01	0.504317E 01	0.319747E 01	0.209160E 01	0.127478E-01
0.114564E 01	0.504327E 01	0.320746E 01	0.212282E 01	-0.674397E-02
0.117657E 01	0.504276E 01	0.321748E 01	0.215395E 01	-0.267645E-01
0.120737E 01	0.504162E 01	0.322997E 01	0.218497E 01	-0.479249E-01

0.123800E 01	0.503981E 01	0.323997E 01	0.221588E 01	-0.703674E-01
0.126848E 01	0.503731E 01	0.324997E 01	0.224670E 01	-0.936477E-01
0.129879E 01	0.503410E 01	0.325998E 01	0.227742E 01	-0.118046E 00
0.132890E 01	0.503015E 01	0.326997E 01	0.230804E 01	-0.143745E 00
0.135878E 01	0.502542E 01	0.327997E 01	0.233858E 01	-0.170900E 00
0.138838E 01	0.501987E 01	0.328997E 01	0.236902E 01	-0.199717E 00
0.141771E 01	0.501347E 01	0.329997E 01	0.239937E 01	-0.230362E 00
0.144670E 01	0.500618E 01	0.330997E 01	0.242962E 01	-0.263106E 00
0.147530E 01	0.499794E 01	0.331997E 01	0.245979E 01	-0.298234E 00
0.150346E 01	0.498870E 01	0.332997E 01	0.248986E 01	-0.336049E 00
0.153111E 01	0.497839E 01	0.333997E 01	0.251985E 01	-0.376996E 00
0.155817E 01	0.496697E 01	0.334997E 01	0.254974E 01	-0.421537E 00
0.158454E 01	0.495435E 01	0.335997E 01	0.257955E 01	-0.470326E 00
0.161008E 01	0.494046E 01	0.336998E 01	0.260926E 01	-0.524174E 00
0.163467E 01	0.492521E 01	0.337997E 01	0.263889E 01	-0.584081E 00
0.165811E 01	0.490850E 01	0.338997E 01	0.266844E 01	-0.651456E 00
0.168017E 01	0.489023E 01	0.339997E 01	0.269789E 01	-0.728252E 00
0.170051E 01	0.487028E 01	0.340997E 01	0.272726E 01	-0.817324E 00
0.171874E 01	0.484854E 01	0.341998E 01	0.275654E 01	-0.922945E 00
0.173429E 01	0.482486E 01	0.342996E 01	0.278574E 01	-0.105212E 01
0.174630E 01	0.479917E 01	0.343996E 01	0.281485E 01	-0.121754E 01
0.175348E 01	0.477157E 01	0.344746E 01	0.284389E 01	-0.144259E 01
0.175356E 01	0.474217E 01	0.345747E 01	0.287285E 01	-0.177140E 01
0.174206E 01	0.470084E 01	0.346746E 01	0.290173E 01	-0.223506E 01
0.173120E 01	0.469145E 01	0.347246E 01	0.291614E 01	-0.262596E 01
0.171761E 01	0.468730E 01	0.347746E 01	0.293053E 01	-0.308083E 01
0.170361E 01	0.469006E 01	0.348246E 01	0.294490E 01	-0.359190E 01
0.169320E 01	0.469947E 01	0.348746E 01	0.295924E 01	-0.418724E 01
0.169154E 01	0.471257E 01	0.349246E 01	0.297357E 01	-0.498664E 01
0.175667E 01	0.458115E 01	0.100000E 01	0.0	-0.218438E 01
0.181034E 01	0.451745E 01	0.830000E 00	0.832936E-01	-0.119029E 01
0.183357E 01	0.446427E 01	0.830000E 00	0.143534E 00	-0.112576E 01
0.186179E 01	0.441100E 01	0.830000E 00	0.203775E 00	-0.105386E 01
0.189374E 01	0.435939E 01	0.830000E 00	0.264016E 00	-0.991186E 00
0.192869E 01	0.430960E 01	0.830000E 00	0.324257E 00	-0.937046E 00
0.196589E 01	0.426172E 01	0.830000E 00	0.384498E 00	-0.889833E 00
0.204624E 01	0.417120E 01	0.830000E 00	0.504979E 00	-0.810058E 00
0.213314E 01	0.408652E 01	0.830000E 00	0.625461E 00	-0.744371E 00
0.222510E 01	0.400710E 01	0.830000E 00	0.745942E 00	-0.688474E 00
0.232113E 01	0.393247E 01	0.830000E 00	0.866424E 00	-0.639811E 00
0.247151E 01	0.382874E 01	0.830000E 00	0.104715E 01	-0.576649E 00
0.262797E 01	0.373373E 01	0.830000E 00	0.122787E 01	-0.522485E 00
0.278921E 01	0.364658E 01	0.830000E 00	0.140859E 01	-0.475141E 00
0.295431E 01	0.356659E 01	0.830000E 00	0.158931E 01	-0.433169E 00

0.312255E 01	0.349313E 01	0.830000E 00	0.177003E 01	-0.395560E 00
0.329335E 01	0.342566E 01	0.830000E 00	0.195075E 01	-0.361601E 00
0.346626E 01	0.336371E 01	0.830000E 00	0.213148E 01	-0.330746E 00
0.364092E 01	0.330685E 01	0.830000E 00	0.231220E 01	-0.302564E 00
0.381699E 01	0.325471E 01	0.830000E 00	0.249292E 01	-0.276731E 00
0.399425E 01	0.320693E 01	0.830000E 00	0.267364E 01	-0.252966E 00

SUMMARY OF DOWNSTREAM WALL COORDINATES OF DIFFUSER (LOWER WALL)

X	R	Q	S	ALPHA
0.417248E 01	0.316320E 01	0.830000E 00	0.285436E 01	-0.231034E 00
0.435152E 01	0.312323E 01	0.830000E 00	0.303509E 01	-0.210757E 00
0.453121E 01	0.308675E 01	0.830000E 00	0.321581E 01	-0.191969E 00
0.471141E 01	0.305353E 01	0.830000E 00	0.339653E 01	-0.174548E 00
0.489205E 01	0.302335E 01	0.830000E 00	0.357725E 01	-0.158349E 00
0.507306E 01	0.299599E 01	0.830000E 00	0.375797E 01	-0.143253E 00
0.525433E 01	0.297127E 01	0.830000E 00	0.393869E 01	-0.129187E 00
0.543581E 01	0.294901E 01	0.830000E 00	0.411942E 01	-0.116060E 00
0.561747E 01	0.292906E 01	0.830000E 00	0.430014E 01	-0.103781E 00
0.579930E 01	0.291127E 01	0.830000E 00	0.448086E 01	-0.922359E-01
0.598122E 01	0.289551E 01	0.830000E 00	0.466158E 01	-0.814096E-01
0.616319E 01	0.288166E 01	0.830000E 00	0.484231E 01	-0.712363E-01
0.634525E 01	0.286960E 01	0.830000E 00	0.502303E 01	-0.616213E-01
0.652733E 01	0.285924E 01	0.830000E 00	0.520375E 01	-0.525319E-01
0.670947E 01	0.285049E 01	0.830000E 00	0.538447E 01	-0.438809E-01
0.689171E 01	0.284327E 01	0.830000E 00	0.556519E 01	-0.356087E-01
0.707392E 01	0.283755E 01	0.830000E 00	0.574591E 01	-0.277206E-01
0.725615E 01	0.283321E 01	0.830000E 00	0.592663E 01	-0.201385E-01
0.743837E 01	0.283023E 01	0.830000E 00	0.610736E 01	-0.128521E-01
0.762058E 01	0.282853E 01	0.830000E 00	0.628808E 01	-0.581392E-02
0.780279E 01	0.282812E 01	0.830000E 00	0.646880E 01	0.996035E-03
0.798498E 01	0.282889E 01	0.830000E 00	0.664952E 01	0.752290E-02
0.816144E 01	0.283079E 01	0.830000E 00	0.683024E 01	0.974635E-02

SUMMARY OF WALL COORDINATES INSIDE OF DIFFUSER SLOT (LOWER WALL)

X	R	Q	S	ALPHA
0.175667E 01	0.458115E 01	0.0	0.0	-0.218438E 01
0.166674E 01	0.430126E 01	0.830000E 00	0.293985E 00	-0.354095E 01
0.161743E 01	0.442754E 01	0.830000E 00	0.354225E 00	-0.397032E 01
0.159443E 01	0.453362E 01	0.830000E 00	0.414466E 00	-0.395741E 01



## APPENDIX C. DEVELOPMENT OF PERFORMANCE EQUATIONS

The following assumptions were made in the derivation of the performance equations:

- (1) Tests were conducted under steady state steady flow conditions.
- (2) The temperature (and thus the internal energy) and the pressure were uniform across the inlet section and across the exit section.
- (3) The fluid density was constant. Since the maximum velocities encountered resulted in a Mach number of about 0.25, the resultant error should be negligible.

Define the effectiveness  $\epsilon$  as follows:

$$\epsilon = \frac{\dot{m}_e (P_{s,e} - P_{s,i})/\rho}{\dot{m}_i (KE_i - KE_e)} \quad (27)$$

where  $\dot{m}$  represents the mass flow rate and KE is the kinetic energy per unit mass flowing.

$$\dot{m}_i KE_i = \int_{A_i} \frac{U_i^2}{2} (U_i \rho) dA_i \quad (28)$$

$$\dot{m}_i KE_e = \left(\frac{\dot{m}_i}{\dot{m}_e}\right) \dot{m}_e KE_e = \left(\frac{\dot{m}_i}{\dot{m}_e}\right) \int_{A_e} \frac{U_e^2}{2} (U_e \rho) dA_e \quad (29)$$

$$\epsilon = \frac{\dot{m}_e (P_{s,e} - P_{s,i})/\rho}{\int_{A_i} \frac{U_i^2}{2} (U_i \rho) dA_i - \left(\frac{\dot{m}_i}{\dot{m}_e}\right) \int_{A_e} \frac{U_e^2}{2} (U_e \rho) dA_e} \quad (30)$$

Now define a kinetic energy coefficient  $\kappa$ :

$$\kappa_i = \frac{\int_{A_i} \frac{U_i^2}{2} (\rho U_i) dA_i}{\frac{\rho}{2} \bar{U}_i^3 A_i} \quad \text{and} \quad \kappa_e = \frac{\int_{A_e} \frac{U_e^2}{2} (\rho U_e) dA_e}{\frac{\rho}{2} \bar{U}_e^3 A_e} \quad (31)$$

so that the effectiveness expression becomes

$$\epsilon = \frac{\dot{m}_e (P_{s,e} - P_{s,i})}{\kappa_i \frac{\rho}{2} \bar{U}_i^3 A_i - \kappa_e \frac{\dot{m}_i}{\dot{m}_e} \frac{\rho}{2} \bar{U}_e^3 A_e} = \frac{\dot{m}_e (P_{s,e} - P_{s,i})}{(\kappa_i \dot{m}_i \bar{U}_i^2 - \kappa_e \dot{m}_i \bar{U}_e^2)/2} \quad (32)$$

$$\epsilon = \frac{\dot{m}_e (P_{s,e} - P_{s,i})}{\frac{\dot{m}_i}{2} (\kappa_i \bar{U}_i^2 - \kappa_e \bar{U}_e^2)} = \frac{\dot{m}_e (P_{s,e} - P_{s,i})}{\frac{\dot{m}_i \bar{U}_i^2}{2} \left[ \kappa_i - \kappa_e \left( \frac{\bar{U}_e}{\bar{U}_i} \right)^2 \right]} \quad (33)$$

$$\text{But} \left( \frac{\bar{U}_e}{\bar{U}_i} \right)^2 = \left( \frac{1.0 - FS}{AR} \right)^2 \quad (34)$$

$$\text{and} \frac{\dot{m}_e}{\dot{m}_i} = (1.0 - FS) \quad (35)$$

$$\text{so} \quad \epsilon = \frac{(1.0 - FS) (P_{s,e} - P_{s,i})}{P_{d,i} \left[ \kappa_i - \kappa_e \left( \frac{1.0 - FS}{AR} \right)^2 \right]} \quad (25)$$

This was the expression used to compute the effectiveness  $\epsilon$ . The more conventional expression for the effectiveness is similar to equation 25 except that the ratio of mass flow rates is deleted.

Thus

$$\eta = \frac{(P_{s,e} - P_{s,i})}{P_{d,i} \left[ \kappa_i - \kappa_e \left( \frac{1.0 - FS}{AR} \right)^2 \right]} \quad (24)$$

Considering the total pressure loss,

$$P_{t,i} - P_{t,e} = (P_{s,i} + \rho KE_i) - (P_{s,e} + \rho KE_e) \quad (36)$$

$$\begin{aligned} &= \frac{\rho}{2} (\kappa_i \bar{U}_i^2 - \kappa_e \bar{U}_e^2) - (P_{s,e} - P_{s,i}) \\ &= \frac{\rho}{2} \bar{U}_i^2 \left[ \kappa_i - \kappa_e \left( \frac{\bar{U}_e}{\bar{U}_i} \right)^2 \right] - \eta \frac{\rho \bar{U}_i^2}{2} \left[ \kappa_i - \kappa_e \left( \frac{1.0 - FS}{AR} \right)^2 \right] \end{aligned}$$

$$P_{t,i} - P_{t,e} = (1-\eta) P_{d,i} \left[ \kappa_i - \kappa_e \left( \frac{1.0 - FS}{AR} \right)^2 \right] \quad (26)$$

Values of  $\kappa_i$  (and  $\kappa_e$ ) were computed from measured velocities as follows. Consider  $n$  velocities  $U_j$  at  $n$  radii  $r_j$  incremented by a constant interval (where  $j = 1, 2, \dots, n$ ). If we let the velocity  $U_j$  be representative of the annular area between radii

$$\frac{r_{j+1} + r_j}{2} \quad \text{and} \quad \frac{r_j + r_{j-1}}{2}, \quad \text{then}$$

$$\kappa = \frac{1}{A} \int_A \left( \frac{U}{\bar{U}} \right)^3 dA \cong \frac{1}{A} \sum_{j=1}^n \left( \frac{U_j}{\bar{U}} \right)^3 \frac{\pi}{4} [r_{j+1}^2 - r_{j-1}^2 + 2r_j(r_{j+1} - r_{j-1})] \quad (37)$$

where

$$\bar{U} \cong \frac{1}{A} \sum_{j=1}^n U_j [r_{j+1}^2 - r_{j-1}^2 + 2r_j(r_{j+1} - r_{j-1})] \quad (38)$$

In equation (38) the radii  $r_0$  and  $r_{n+1}$  are equal to the inner and outer diffuser wall radii respectively. All other radii,  $r_1$  to  $r_n$ , are readily obtained since the increment between radii is a constant. Using equation (37), typical values obtained were 1.025 for  $K_i$  and 1.011 for  $K_e$ .