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Thomas L. Labus

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\_\_\_\_\_  
Advisor

\_\_\_\_\_  
Dean of the Graduate School

The University of Toledo  
July 1976

An Abstract of  
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An experimental and analytical investigation was conducted to determine the free surface shapes of circular liquid jets impinging normal to sharp-edged disks under both normal and zero gravity conditions. An order of magnitude analysis was conducted indicating regions where viscous forces were not significant when computing free surface shapes. The demarcation between the viscous and inviscid region was found to depend upon the flow Reynolds number and the ratio between the jet and disk radius.

Experiments conducted under zero gravity conditions yielded three distinct flow patterns. These flow patterns were defined as surface tension flow, transition flow, and inertia flow. The flow regions were classified in terms of the relative effects of surface tension and inertial forces. The transition between regions was correlated with the system Weber number and the ratio of the jet to the disk radius. The normal gravity plume shapes were observed to jump from one apparently stable flow pattern to another until steady-state was reached.

A zero gravity inviscid analysis was performed in which the governing equations and boundary conditions in the physical plane were transformed into an inverse plane. In the inverse plane, the stream function and velocity potential became the coordinates thus removing the prime difficulty in free surface problems, that of having to guess at the true position of the free surface. The governing equations were nonlinear in the inverse plane thus requiring a numerical solution in which sets of nonlinear algebraic equations were solved simultaneously. Comparisons between experiment and numerical computations were made for the infinite and finite plate cases with the result that good agreement for the free surface shapes were obtained.

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# NOMENCLATURE

A	numerical constant
a	stream function increment
B	numerical constant
Bo	Bond number, $\rho g R_0^2 / \sigma$
b	numerical constant
C	numerical constant
$C_0, C_1, C_2$	numerical constants
c	numerical constant
D	$= 1/\alpha^2$
d	designated reference point
$f_o$	unknown scale factor, m
$f, f_1, f_2$	fictitious points
g	acceleration due to gravity, $m/sec^2$
g	gas
H	distance between plate and nozzle, m
i	any point on free surface
$\hat{i}, \hat{j}$	unit vectors
J	Jacobian
$K\phi$	numerical constant
L	disk radius, m
$\hat{n}$	unit normal on free surface
O	stagnation point
p	pressure, $N/m^2$

$P_o$	unknown scale factor, $N/m^2$
$Q$	$= \frac{(r_1 - r_3)^2}{(r_f - r_4)^2} \cdot \frac{1}{\alpha^2}$
$Q^*$	$= \alpha^2 \frac{(f - z_4)^2}{(z_1 - z_3)^2}$
$R^2$	statistical variable
$RD$	$= L/R_o$
$Re$	Reynolds number, $\rho VR_o/\mu$
$R_{max}$	maximum radius for surface tension model, m
$R_o$	radius of nozzle, m
$R_p$	radius of plume, m
$R_1, R_2$	radii of curvature, m
$r$	radial coordinate, m
$r_o$	unknown scale factor, m
$T^2$	$= \alpha^2 r_o^2 \frac{(f - z_4)^2}{(z_1 - z_3)^2} + 1$
$U_o$	unknown scale factor, m/sec
$u$	radial velocity component, m/sec
$V$	jet velocity, m/sec
$\vec{V}$	vector velocity along free surface, m/sec
$v$	axial velocity component, m/sec
$We$	Weber number, $\rho V^2 R_o / \sigma$
$y$	dimensionless parameter
$z$	axial coordinate, m
$z_1, z_2, z_3, z_4, z_5$	dimensionless parameters

$\alpha$	$\Delta\phi/\Delta\psi$
$\delta/\delta r$	finite difference analogy of $\partial/\partial r$
$\mu$	liquid viscosity, $\text{g/m}^2\text{-sec}$
$\rho$	liquid density, $\text{kg/m}^3$
$\sigma$	liquid surface tension, $\text{N/m}$
$\phi$	velocity potential, $\text{m}^2/\text{sec}$
$x$	$= r_f - r_4$ , m
$\psi$	Stokes' stream function, $\text{m}^3/\text{sec}$

Superscripts and subscripts:

Cr	critical
'	differentiation with respect to $r$
*	denotes dimensionless quantities
1,2,3,4	nodal point locations
s	surface

## I. INTRODUCTION

A knowledge of the dynamics of free liquid jets is required for the solution of a variety of problems associated with fluid flow within propellant tanks under low gravitational conditions. In particular, an understanding of the liquid jet - impact process, as occurs when liquid impinges upon baffles or tank walls during an inflow or reorientation maneuver, will be required in order to predict liquid-propellant location, heat transfer rates and pressure distributions. The area of liquid jet impingement also has direct applicability to the spacecraft fire safety problem, in which water jets are employed as extinguishant agents under low gravity conditions. In order to be able to predict required delivery flow rates, the accurate prediction of flow surface coverage as a function of jet momentum is needed.

There generally appears to be three chief obstacles which have in the past prohibited the attainment of solutions to steady-state liquid jet-solid interaction problems. The major obstacle is the presence of the free surface. In order to apply numerical techniques to the solution of free-jet problems it is necessary to define the area over which the computations are made by boundaries defined by the free liquid surface. Unfortunately, the location of the free-surface is one of the items sought from the solution so that various techniques must be devised to circumvent this situation. Furthermore, analytical techniques are restricted solely to two-dimensional problems, whether

a free surface exists or not. The second obstacle is gravity. Liquid jets in air (free jets), unlike liquid-into-liquid jets and gas-into-gas jets (submerged jets), are affected significantly by gravitational forces. The free-surface shape and velocity profiles are dependent on both the magnitude and the orientation of gravity. The addition of gravity necessarily complicates a model either through the governing equation or through the boundary conditions. Neglecting gravity in the model makes questionable the comparison of the theory with normal-gravity experimental data. The final obstacle is surface tension, an effect which has generally been neglected in almost all studies on free jets. The addition of surface tension into a model leads to non-linear free surface boundary conditions.

The purpose of this report is to present the results of an experimental and analytical study conducted at the NASA Lewis Research Center concerning zero gravity isothermal liquid jet impingement. An axisymmetric liquid jet was impinged normally onto a sharp-edged disk under conditions in which both inertial and surface tension forces are of importance. The experimental free surface shapes were correlated with known system parameters. An analytical model was formulated and the free surface shapes and streamlines were calculated for a number of discrete cases.

## II. LITERATURE SURVEY

### A. Experimental Studies

Very few experimental studies have been conducted to examine free jets impinging on solid surfaces. No work has been conducted where the major concern was either the shape of the free surface or the measurement of velocity profiles within the jet. Also, only one experiment has been conducted using a two-dimensional jet. A two-dimensional jet is one in which the flow emanates from a rectangular slot in which the width of the jet is very large relative to the thickness of the jet. Schach (38) measured the pressure distribution and analytically calculated the free surface shape and velocity distributions for jets impinging onto flat panels at various impingement inclinations relative to the direction of flow. The jet employed had dimensions of 21 by 115 mm. According to Schach, the jet diverged spatially after impinging upon the panel and thus it can only be considered as truly two-dimensional close to the centerline. An excellent account of an elaborate experimental apparatus for obtaining a quiescent circular water jet in normal gravity is given by Donnelly, et al. (11). Their major concern was jet stability under imposed audio frequency disturbances and, therefore, the impingement phenomenon was not directly observed. Rupe (37) and Stephens (41) experimentally measured the pressure distribution caused by circular jets striking solid surfaces in normal gravity. However, neither Rupe or Stephens meas-



ured the free-surface shape or discussed any instabilities which occurred.

In nearly all flows where a circular liquid jet strikes a large flat surface, typically what happens in normal gravity is that the liquid jet impinges on the surface and moves radially outward from the stagnation point until a certain radial distance is reached whereupon an instability known as a circular hydraulic jump occurs. The jump is characterized by an abrupt increase in the liquid depth and turbulent fluid motion. Koloseus, et al. (22) were concerned solely with predicting the behavior of the circular hydraulic jump. A water jet impinging on a flat plate of epoxy material was employed in these experiments. The circular hydraulic jump was the subject for a very complete study conducted by Nirapathdongporn (33), whose report contains an excellent description of various devices for measuring jet shapes and jet diameters.

All of the above mentioned studies deal with normal-gravity, liquid jet-solid impingement. There have been no experimental studies on the impingement of liquid jets under zero-gravity conditions.

#### B. Analytical Studies

1. Steady two-dimensional potential flow. - A number of papers and books have discussed steady-state two-dimensional free jets impinging on a variety of surfaces using analytical techniques. The majority of these studies were concerned with irrotational, incompressible, inviscid flow, in which the effects of gravity and surface tension were neglected. One of the major attractions of this type of problem is that it can be handled using complex potential theory and, therefore, can be treated analytically.

A two-dimensional jet striking an infinitely flat surface at various angles was examined by Batchelor (4), who solved for the limiting stream thickness as a function of flow impingement angle and jet diameter. However, no attempt was made to predict free-streamline shape. Schach (38) treated the impingement as a function of angle using Prandtl's hodograph method, and obtained the equations for the free surface shapes, flow distribution, and pressure distribution for the case of impingement on an infinitely wide plate. Kochin, et al. (21) also examined the impingement of a two-dimensional jet obliquely to an infinite flat plate, and discussed the case of impingement on a plate of finite length. The equation of the free-surface for the case of a two-dimensional jet striking a flat surface at right angles is presented by Milne-Thomson (30) who also solved for the velocity components within the jet. An excellent discussion of the techniques for handling two-dimensional free jet problems is presented by Gurevich (14). Some of the two-dimensional flows examined by Gurevich include flow around a finite wedge, perpendicular to a finite plate, obliquely to an infinite flat plate, and flows where a variety of solid objects are positioned adjacent to one wall or between two walls. Chang, et al. (9) analyzed the two-dimensional flow of a jet interacting with a number of flat segments at angles to one another. The results include flow turning angles but not free surface shapes or velocity profiles. The irrotational flow pattern of a free jet discharging from a slot and flowing past a wedge was analyzed by Arbbabhiraama (3). All of the above texts and articles were concerned with analytical techniques for obtaining solutions. The area of steady two-dimensional potential flow represents the most

complete area of research in the field of jet impingement.

2. Steady axisymmetric viscous flow. - Watson (43) has analytically investigated free jet-impingement for the case of large Reynolds numbers where the viscous forces are confined to a thin boundary layer adjacent to the plate. A similarity solution was obtained for both the two-dimensional and axisymmetric velocity profiles and free surface shapes for the case of normal impingement. As mentioned by Watson, the similarity solution can only be expected to be valid when the radial distance is sufficiently large for the incident jet to have lost its influence. The effects of gravity and surface tension were neglected in the analysis. Watson solved for the radial position of the circular hydraulic jump.

### C. Numerical Studies

1. Steady two-dimensional potential flow. - When the shape of the solid upon which the jet impinges becomes complex, numerical techniques for the solution of free jet problems have to be applied. Jeppson (19) presents an excellent article in this regard. Jeppson employed the stream function and the velocity potential as the independent variables and the coordinates as the dependent variables. A similar inversion approach has been previously used to solve a variety of fluid dynamics problems as shown in references 5, 20, 31, 42, and 44 and is mainly attributable to Thom and Apelt (42). Using this technique, Jeppson was able to circumvent the problem of working in the physical plane and having to guess at the true position of the free surface. The latter iterative approach was used in references 1, 8, 13, 27, 32, 36, and 40 with limited success. Jeppson solved the problem of the two-dimensional flow over a wedge, and, as such, is

the only one to have attempted numerical solutions of this problem. Lastly, Chan (7) applied the finite element method to a number of free-surface flow problems, including the flow from a circular orifice.

2. Steady axisymmetric potential flow. - The solution of axisymmetric flow problems cannot utilize the powerful tool of complex analysis. For this reason, only numerical solutions can be attempted for problems of this nature.

LeClerc (25) studied the impingement of an axially symmetric liquid jet perpendicular to a flat surface. The shape of the free surface was found using an electrical analogy. This method thus fixed the position of the free surface and enabled the author to apply standard finite-differencing methods and employ Southwell's relaxation technique to solve Laplace's equation. Jeppson (19) applied his inversion technique to find the flow pattern and free-surface shape for the case of axisymmetric flow past a variety of bodies of revolution, including cones. Jeppson also applied his technique to the solution of a jet of inviscid, incompressible fluid issuing from a nozzle into the free atmosphere. He indicates how his method may be extended to a variety of other problems. Schach (39) used a semi-analytical technique based on Trefftz's approximate method to find the shape of an axisymmetric free jet impinging normally on a plate. Also presented in Schach's article was the pressure distribution on the plate which was calculated from the velocity distribution using Bernoulli's equation. Young, et al. (45) and Brunauer (6) determined the flow pattern past two disks immersed in axisymmetric flow. Both Young and Brunauer solved Laplace's equation in the physical plane.

No analyses have been conducted for the case in which an inviscid free jet impinges upon a plate of finite thickness.

The articles mentioned above encompass all the known solutions with regard to axisymmetric jet impingement. References 7, 8, 20, 27, and 40 deal specifically with numerical methods applied to free surface problems in which no impingement occurs. Jeppson (20) employed an inverse formulation while the others worked in the physical plane.

3. Unsteady two-dimensional and axisymmetric potential flow. -

Huang (17, 18) has investigated unsteady flows and considered the impact phenomena for both two-dimensional and axisymmetric jets. The major interest in these articles was in obtaining the initial pressure distribution due to liquid impact.

4. Steady potential flow including gravitational effects. -

The addition of gravity in analyses for potential flows causes no serious formulation problem for either the two-dimensional or axisymmetric case. The reason for this is because its effect enters only through the free-surface boundary conditions and not the governing equations. Jeppson (19) included gravity in his analysis of the impingement on a two-dimensional wedge. Moayeri, et al. (31) Southwell, et al. (40) and Chan (8), all considered the effect of gravity in dealing with steady, potential, free-surface problems in which no impingement occurs.

5. Steady potential flow including surface tension. - Zhukovskii (46) has indicated how to include the effects of surface tension. He examined a two-dimensional problem using complex analysis, but his method is not extendable to either axisymmetric or three-dimensional

flows.

6. Steady three-dimensional potential flow. - Until very recently, very little had been accomplished in the area of three-dimensional potential flow with a free surface, much less including impingement. Davis and Jeppson (10) developed a computer program to solve free-surface problems of this type using the inverse method. Michelson (28, 29) also examined jets under these conditions. He treated the case of an axisymmetric jet impinging obliquely on a flat surface, and analytically showed the occurrence of wedge-shaped dry zones when the impingement angle was less than a critical value. Free-surface shapes are not obtainable using Michelson's method.

### III. ORDER OF MAGNITUDE ANALYSIS

#### A. Formulation

The problem under consideration is the viscous flow of a circular liquid jet as it impinges normally to an infinite flat plate, as shown in Figure 1. The objective is to determine the free surface shape of the impinging liquid and the velocity profiles within the jet. In general, flows of the type described will depend on viscous, surface tension, inertial and body forces. Physical intuition tells us that if the velocity is large and the diameter of the plate is sufficiently small, there will be regions wherein viscous forces are not of prime importance in determining the resulting flow behavior, particularly the free surface shape. The viscous forces, in this case, will be confined to a thin boundary layer on the plate which originates from the stagnation point. The location of the stagnation point is shown in Figure 1. The jet or nozzle radius is  $R_0$  and the distance between the plate and nozzle is given as  $H$ . A cylindrical coordinate system  $(r, z)$  emanating from the stagnation point is chosen. An order of magnitude analysis will permit the governing equations to be simplified so that an analytical solution can be attempted. For axisymmetric, isothermal, incompressible steady flow under weightless conditions, the governing equations in cylindrical coordinates can be written:

Continuity:

$$\frac{1}{r} \frac{\partial}{\partial r} (ru) + \frac{\partial v}{\partial z} = 0 \quad (1)$$

Momentum:

r Component:

$$\rho \left( u \frac{\partial u}{\partial r} + v \frac{\partial u}{\partial z} \right) = - \frac{\partial P}{\partial r} + \mu \left\{ \frac{\partial}{\partial r} \left[ \frac{1}{r} \frac{\partial}{\partial r} (ru) \right] + \frac{\partial^2 u}{\partial z^2} \right\} \quad (2)$$

z Component:

$$\rho \left( u \frac{\partial v}{\partial r} + v \frac{\partial v}{\partial z} \right) = - \frac{\partial P}{\partial z} + \mu \left[ \frac{1}{r} \frac{\partial}{\partial r} \left( r \frac{\partial v}{\partial r} \right) + \frac{\partial^2 v}{\partial z^2} \right] \quad (3)$$

Boundary conditions are required on the flat plate, along the axis of symmetry, at the nozzle exit, on the free surface, and at  $r = L$ .

On plate

$$\begin{aligned} u &= 0 \\ v &= 0 \end{aligned} \quad \text{on } z = 0, \text{ all } r \quad (4)$$

Along axis of symmetry

$$\begin{aligned} u &= 0 \\ \frac{\partial v}{\partial r} &= 0 \end{aligned} \quad \text{on } r = 0, \text{ all } z \quad (5)$$

At the nozzle

$$\begin{aligned} v &= -V \\ u &= 0 \end{aligned} \quad \text{on } 0 \leq r \leq R_0, z = H \quad (6)$$

At  $r = L$

$$\begin{aligned} u &= u(z) \\ v &= v(z) \end{aligned} \quad \text{on } r = L, 0 < z \leq f(L) \quad (7)$$

On the free surface, denoted by  $z_s = f(r)$ , two boundary conditions are required since the free surface position is an unknown to be determined as part of the solution. The details of the calculation



for the boundary conditions along the free surface can be found in Appendix A. (See eqs. (A.10) and (A.14).)

On the free surface

$$\frac{1}{2} (u^2 + v^2) - \frac{\sigma}{\rho r} \frac{d}{dr} \left[ \frac{r \frac{df}{dr}}{\sqrt{1 + \left(\frac{df}{dr}\right)^2}} \right] = \frac{1}{2} v^2 - \frac{\sigma}{\rho R_0} \quad \text{on } z_s = f(r) \quad (8)$$

and

$$-u \frac{df}{dr} + v = 0 \quad \text{on } z_s = f(r) \quad (9)$$

In equation (4), the no-flow and no-slip boundary conditions are applied at the wall. Equation (5) is a statement involving the known geometrical symmetry of the problem, while equation (6) imposes an initially uniform velocity profile on the incoming jet. Equation (7) simply states the velocity distribution as the liquid leaves the control volume. Equation (8) is a statement of conservation of mechanical energy along a streamline, while equation (9) states that the normal velocity component on a streamline is zero. The second terms on the left and right sides of equation (8) are the contribution of surface tension to the mechanical energy balance.

The solution of the problem can be greatly facilitated by simplifying equations (1) to (8). Specifically, the method of obtaining the minimum parametric representation of a problem will be employed in order to simplify the governing equations. This method is described in detail by Krantz (23) and is the most systematic approach for scaling the governing equations. The initial step in the minimum parametric representation method is to form dimensionless variables by introducing characteristic scale factors for all dependent and independent

variables. The unknown scale factors are defined as  $U_0, V_0, r_0, z_0, p_0$ , and  $f_0$ .

Dimensionless variables are now defined as:

$$u^* = \frac{u}{U_0}, v^* = \frac{v}{V_0}, r^* = \frac{r}{r_0}, z^* = \frac{z}{z_0}, p^* = \frac{p}{p_0}, f^* = \frac{f}{f_0} \quad (10)$$

Introducing these dimensionless variables into the differential equations and boundary conditions, and arbitrarily making the coefficient of one term in each differential equation and boundary condition equal to unity, results in:

Continuity:

$$\frac{\partial v^*}{\partial z^*} + \frac{U_0 z_0}{V_0 r_0} \frac{1}{r^*} \frac{\partial}{\partial r^*} (r^* u^*) = 0 \quad (11)$$

Momentum:

r Component:

$$\begin{aligned} \frac{\rho U_0 z_0^2}{r_0 \mu} u^* \frac{\partial u^*}{\partial r^*} + \frac{\rho V_0 z_0}{\mu} v^* \frac{\partial u^*}{\partial z^*} = - \frac{p_0 z_0^2}{r_0 \mu U_0} \frac{\partial p^*}{\partial r^*} \\ + \frac{z_0^2}{r_0^2} \frac{\partial}{\partial r^*} \left[ \frac{1}{r^*} \frac{\partial}{\partial r^*} (r^* u^*) \right] + \frac{\partial^2 v^*}{\partial z^{*2}} \end{aligned} \quad (12)$$

z Component:

$$\begin{aligned} \frac{U_0 z_0}{r_0 V_0} u^* \frac{\partial v^*}{\partial r^*} + v^* \frac{\partial v^*}{\partial z^*} = - \frac{p_0}{\rho V_0^2} \frac{\partial p^*}{\partial z^*} \\ + \frac{\mu z_0}{r_0^2 \rho V_0} \frac{1}{r^*} \frac{\partial}{\partial r^*} \left( r^* \frac{\partial v^*}{\partial r^*} \right) + \frac{\mu}{z_0 \rho V_0} \frac{\partial^2 v^*}{\partial z^{*2}} \end{aligned} \quad (13)$$

Boundary conditions:

On wall

$$\begin{aligned} u^* &= 0 \\ v^* &= 0 \end{aligned} \quad \text{on } z^* = 0, \text{ all } r^* \quad (14)$$

Along axis of symmetry

$$\begin{aligned} u^* &= 0 \\ \frac{\partial v^*}{\partial r^*} &= 0 \end{aligned} \quad \text{on } r^* = 0, \text{ all } z^* \quad (15)$$

At the nozzle

$$v^* = -\frac{V}{V_0} \quad 0 \leq r^* \leq \frac{R_0}{r_0} \quad (16)$$

$$u^* = 0 \quad z^* = \frac{H}{R_0}$$

At  $r = L/R_0$

$$\begin{aligned} u^* &= u^*(z^*) \\ v^* &= v^*(z) \end{aligned} \quad \text{on } r^* = \frac{L}{r_0} \quad (17)$$

On the free surface

$$\begin{aligned} \frac{1}{2} \left( u^{*2} \frac{U_0^2}{V_0^2} + v^{*2} \right) - \frac{\sigma}{\rho r^* V_0^2} \frac{f_0}{r_0^2} \frac{d}{dr^*} \left[ \frac{r^* \frac{df^*}{dr^*}}{\sqrt{1 + \frac{f_0^2}{r_0^2} \left( \frac{df^*}{dr^*} \right)^2}} \right] \\ = \frac{1}{2} \frac{V^2}{V_0^2} - \frac{\sigma}{\rho R_0 V_0^2} \quad \text{on } z_s^* = \frac{f^* f_0}{z_0} \quad (18) \end{aligned}$$

and

$$v^* - \frac{U_0 f_0}{V_0 r_0} u^* \frac{df^*}{dr^*} = 0 \quad \text{on } z_s^* = \frac{f^* f_0}{z_0} \quad (19)$$

The scale factors must now be determined. This is done by setting some of the resulting dimensionless groups in the equations and boundary conditions equal to zero or unity, the groups chosen depending upon the physical conditions for which the equations are being scaled (23). Characteristic lengths are usually determined from the dimensionless groups generated by the boundary conditions, while characteristic times, velocities, etc., are determined from dimensionless groups generated by the differential equations. The guidelines in determining the unknown scale factors are:

- (1) Do not introduce any mathematical contradictions
- (2) Do not violate physical intuition.

Boundary conditions. - Examining the boundary conditions, it is apparent that the following dimensionless groups are introduced:

$$\frac{v}{v_o}, \frac{R_o}{r_o}, \frac{H}{z_o}, \frac{L}{r_o}, \frac{f(L)}{z_o}, \frac{U_o^2}{v_o^2}, \frac{\sigma f_o}{\rho v_o^2 r_o^2}, \frac{f_o^2}{r_o^2}, \frac{\sigma}{\rho R_o v_o^2}, \frac{f_o}{z_o}, \frac{U_o f_c}{v_o r_o}$$

It is known that  $v$  has the range 0 to  $-V$ ,  $r$  has the range 0 to  $L$ ,  $z$  has the range 0 to  $H$  and  $f(r)$  also has the range 0 to  $H$ . Therefore, setting,

$$\frac{v}{v_o} = 1 \quad \text{and} \quad \frac{L}{r_o} = 1 \quad (20)$$

implies that

$$v_o = V \quad \text{and} \quad r_o = L \quad (21)$$

and yields two of the six unknown scale factors.

Some of the above remaining dimensionless groups cannot be set equal to one or zero without introducing contradictions. Setting  $v_o = V$  and  $r_o = L$  into the above ratios, and since it would be expected that

$$f_o = z_o \quad (22)$$

the following meaningful ratios remain:

$$\frac{H}{z_o}, \quad \frac{U_o^2}{V^2}, \quad \frac{\sigma z_o}{\rho V^2 L^2}, \quad \frac{z_o^2}{L^2}, \quad \frac{U_o z_o}{VL}$$

Setting the second or fourth ratio equal to one or zero would violate physical intuition. Therefore, the ratios to be considered are

$$\frac{H}{z_o}, \quad \frac{\sigma z_o}{\rho V^2 L^2}, \quad \frac{U_o z_o}{VL}$$

At this point an attempt was made to set  $H/z_o = 1$  such that  $z_o$  would equal  $H$ . This seemed logical because 0 to  $H$  was the range of  $z$ . However, this leads to some confusing results in terms of the physics. For a given flow condition, it is argued that for a certain (minimum) value of  $H$  up to  $H = \infty$ , the flow pattern in the vicinity of the plate is not expected to change. This is shown schematically in Figure 2. This argument has been experimentally verified and will be discussed at some length in Section IV, Experimentation. The major point is that  $H$  cannot be a characteristic length in the problem either with reference to  $z_o$  or  $f_o$ . This leaves two remaining ratios from consideration of the boundary conditions.

$$\frac{\sigma z_o}{\rho V^2 L^2} \quad \text{and} \quad \frac{U_o z_o}{VL}$$

Accordingly, all possible information from the boundary conditions has been obtained. Two of the six scale factors and a relationship between two others has been determined. The governing equations must now be examined.

### B. Continuity Equation

From the physics of the problem, it is known that mass must be conserved. Hence, the continuity equation must be valid in its dimensionless form (eq. (11)). If the dimensionless derivatives  $\partial v^*/\partial z^*$  and  $(1/r^*)(\partial/\partial r^*)(r^*u^*)$  are to be of the same order of magnitude, it is required that

$$\frac{U_o z_o}{V_o r_o} = 1 \quad (23)$$

With  $V_o = V$  and  $r_o = L$ , it is found that

$$\frac{U_o z_o}{VL} = 1 \quad (24)$$

Solving for  $U_o$ ,

$$U_o = \frac{VL}{z_o} \quad (25)$$

This, of course, is an equation relating two unknowns,  $U_o$  and  $z_o$ . It is noted that the same information could have been obtained by setting the second of the two ratios remaining from the consideration of the boundary conditions equal to one.

### C. Momentum Equations

It is the objective of this analysis to define that portion of the flow for which an inviscid solution is valid. For this case, the pressure forces are balanced by the inertia forces. This fact allows us to determine the scale factor for the pressure,  $P_o$ . If the dimensionless pressure gradient in equation (13) is to be the same order of magnitude as the dimensionless inertia term,

$$\frac{P_o}{\rho V_o^2} = 1 \quad (26)$$

This implies that

$$P_o = \rho V_o^2 = \rho V^2 \quad (27)$$

thus, the characteristic pressure is the stagnation value.

#### D. Physics of $z_o$

The remaining unknown to be determined is  $z_o$ . At this point some physical arguments are necessary. Recall that it has been shown that  $H$  cannot be considered as a characteristic scale factor for the problem at hand for reasonably large values of  $H$ . However, the free surface shape is expected to change as  $R_o$  varies (see Fig. 3). Therefore, from physical considerations this suggests that characteristic values of  $z_o$  vary as  $R_o$ . Defining

$$z_o = R_o \quad (28)$$

then  $U_o$  can be found from equation (25).

$$U_o = \frac{VL}{R_o} \quad (29)$$

Summarizing, the following has been determined

$$V_o = V$$

$$r_o = L$$

$$z_o = R_o$$

$$f_o = R_o$$

$$U_o = \frac{VL}{R_o}$$

$$P_o = \rho V^2$$

These scale factors can now be substituted into the governing equations to obtain the minimum parametric representation of the problem. The results are as follows:

$$\begin{aligned} \text{Re } u^* \frac{\partial u^*}{\partial r^*} + \text{Re } v^* \frac{\partial u^*}{\partial z^*} = -\text{Re} \left( \frac{R_0}{L} \right)^2 \frac{\partial p^*}{\partial r^*} \\ + \left( \frac{R_0}{L} \right)^2 \frac{\partial}{\partial r^*} \left[ \frac{1}{r^*} \frac{\partial}{\partial r^*} (r^* u^*) \right] + \frac{\partial^2 v^*}{\partial z^{*2}} \end{aligned} \quad (30)$$

$$\begin{aligned} \text{Re } u^* \frac{\partial v^*}{\partial r^*} + \text{Re } v^* \frac{\partial v^*}{\partial z^*} = -\text{Re} \frac{\partial p^*}{\partial z^*} \\ + \left( \frac{R_0}{L} \right)^2 \frac{1}{r^*} \frac{\partial}{\partial r^*} \left( r^* \frac{\partial v^*}{\partial r^*} \right) + \frac{\partial^2 v^*}{\partial z^{*2}} \end{aligned} \quad (31)$$

where  $\text{Re}$  is the Reynolds number defined as

$$\text{Re} = \frac{\rho V R_0}{\mu} \quad (32)$$

The equations are now in the form in which it can be determined what the conditions must be such that viscous forces are not significant. The major parameters in this problem are  $(R_0/L)$  and  $\text{Re}$ . Since all the starred or dimensionless terms in equations (30) and (31) are of unit order, only the coefficients of the individual terms need be considered in order to make statements regarding simplifications. Considering equation (30), it can be seen that since  $(R_0/L)^2 \ll 1$ , both the inertia and pressure forces will be an order of magnitude greater than the viscous forces provided that,

$$\text{Re} \gg 1$$

$$\text{Re} \left( \frac{R_0}{L} \right)^2 \gg 1 \quad (33)$$

From equation (31), since  $(R_0/L)^2 \ll 1$ , no new information is obtained. The governing equations will be reduced to a simplified form of Euler's equations of motion.



$$u^* \frac{\partial u^*}{\partial r^*} + v^* \frac{\partial u^*}{\partial z^*} = - \left( \frac{R_o}{L} \right)^2 \frac{\partial p^*}{\partial r^*} \quad (34)$$

$$u^* \frac{\partial v^*}{\partial r^*} + v^* \frac{\partial v^*}{\partial z^*} = - \frac{\partial p^*}{\partial z^*} \quad (35)$$

#### E. Results

Restricting the viscous forces to be at least two orders of magnitude smaller than the inertial or pressure forces, there results

$$Re \geq 100$$

$$Re \left( \frac{R_o}{L} \right)^2 \geq 100 \quad (36)$$

Since  $(R_o/L)$  is less than one by definition, the coefficient to consider is the second one in equation (36), since this will be the limiting one. Under the following restrictions,

$$(1) \quad Re \geq 100$$

$$(2) \quad \frac{R_o}{L} < 1 \quad (37)$$

the Euler's equation of motion are obtained. The equation  $Re(R_o/L)^2 = 100$  is shown graphically in Figure 4. The line shown in Figure 4 separates the inviscid from the viscous region. A physical understanding of the problem is made clearer by reference to this plot. The higher the incoming jet Reynolds number becomes, the thinner will be the boundary layer at some fixed radial position from the stagnation point. As seen from Figure 4, at lower values of the ratio  $R_o/L$  (perhaps obtained by increasing the disk radius  $L$ ), higher Reynolds numbers are required in order to avoid viscous influence. Finally, within the viscous region, the boundary layer will

grow until a radial length is reached where it becomes equal to the free surface height. The effective design of an experiment is now possible so that the flow can be considered essentially inviscid.

#### IV. ZERO GRAVITY EXPERIMENTATION

##### A. Apparatus and Procedure

1. Test facility. - The experimental investigation was conducted in the 2.2-second drop tower. The exact specifications of the facility, the mode of operation, and release and recovery systems are described in detail in Appendix B. The drop tower provides us with a 2.2 second weightless environment in which to conduct the tests.

2. Experiment. - The experiment package used to obtain the data for this study is shown in Figure 5. It consists of an aluminum frame in which were mounted the jet reservoir, disk, a 16 millimeter high speed motion picture camera, supply tank, backlighting scheme, and batteries. The major functions were controlled by on-board sequence timers.

A diagram indicating the manner in which the flow system operates is shown in Figure 6. This is a pressure controlled system in which the flow was initiated by opening the solenoid valve. Prior to the drop, liquid was contained in the line between the liquid supply tank and the jet reservoir. In addition, the jet reservoir was completely filled with the test liquid.

Initially, the object was to employ two-dimensional jets during the experiments. Schach (38), was the only author who investigated two-dimensional jets, although it is impossible to determine how rectangular his jets really were. Several attempts were made to fabricate a two-dimensional nozzle (slot) for use in the zero gravity studies.

Initially, the slots built were quite crude; a rectangular hole cut in a section of plexiglass; a balsa wood jet sealed with epoxy cement. Later, slots were accurately designed in order to achieve the desired flow. The slot length was arbitrarily chosen as 5 centimeters and its width as 0.25 centimeters. Approximately  $45^\circ$  tapers were made to the opening along both the wide and narrow sides. The results of the zero gravity testing were as follows: The jet contracted in the long direction (5 cm) and expanded in the narrow direction (0.25 cm). A tendency to become cylindrical probably due to the effects of surface tension, was observed. A redesigned version of the slot was tested, which employed absolutely no taper in the narrow direction. This also failed to yield a rectangular jet. When these approximate slot jets impinged on various flat plates, the jet diverged radially. In other words, it was impossible to prevent spreading in the lateral direction for an unconstrained surface. Various methods were tried to eliminate this lateral spreading and to force the impingement flow to be completely two-dimensional. The flow was impinged on rectangular plates having the same width as that of the slot, 5 centimeters. The result of these tests was that the liquid simply fell off or went around the plate. A large rectangular plate was used and the region greater in width than 5 centimeters was sprayed with fluorocarbon since distilled water does not wet a fluorocarbon surface. This also failed. All attempts at using a two-dimensional slot jet were subsequently abandoned and axisymmetric jets were pursued.

A schematic drawing of the jet reservoir, which was fabricated out of acrylic plastic, is shown in Figures 7(a) and (b). The critical feature of the jet reservoir is the  $45^\circ$  taper to a circular hole of

diameter  $D$ . The range of diameters studied was from 0.5 to 1.5 centimeters. In addition, the transition between the circular hole and conical taper was rounded smooth. The taper prohibits boundary layer buildup and allows the liquid jet to exit from the reservoir with a nearly uniform velocity profile. Based on the experimental results of reference 24, a total angle of  $90^\circ$  is more than sufficient to insure a uniform exiting velocity profile over the range of Reynolds numbers studied.

Sharp-edge disks, also fabricated from acrylic plastic, were mounted above the jet reservoir by means of a threaded rod such that the flat surface of the disk was at right angles to the impinging liquid jet. Sharp-edged disks were employed in the study rather than finite thickness disks in order to develop an analytical model for the flow. As was learned later, the thickness of the disk edge is only of importance for those flows dominated by the effects of surface tension. The diameters,  $2L$ , of the disks were 2.0 and 3.0 centimeters. A schematic drawing of the disks is shown in Figure 8.

3. Test liquids. - Two test liquids were employed, anhydrous ethanol and trichlorotrifluoroethane. Their properties at  $20^\circ\text{C}$  are listed in Table 1. No attempt was made to correct the fluid properties for temperature changes. It is noted that both of these test fluids possess a nearly  $0^\circ$  contact angle on an acrylic plastic surface. However, this was not the reason why they were chosen as test fluids. They were chosen because of their relatively low viscosity and availability.

4. Test procedure. - Prior to a test run, the jet reservoir, disk and supply tanks were cleaned ultrasonically with a mild detergent.

After these parts were rinsed with methanol, they were dried in a warm air dryer. The supply tank was subsequently filled with the test liquid and the jet reservoir was filled by pressurizing the supply tank. This procedure eliminated air bubbles from the lines ensuring accurate flow rates. After the jet reservoir was completely full, the supply tank was sealed and two accumulator bottles (not shown in Fig. 5) were pressurized with gaseous nitrogen to a predetermined value. The accumulator bottles were designed to be of such a volume that no appreciable pressure drop occurred during the drop.

Electrical timers on the experiment package were set to control the initiation and duration of all functions programmed during the drop. The experiment package was then balanced and positioned within the prebalanced drag shield. The wire support was attached to the experiment package through an access hole in the shield (see Fig. B3(a) in Appendix B). Properly sized spikes tips were installed on the drag shield. Then the drag shield, with the experiment package inside, was hoisted to the predrop position at the top of the facility (Fig. B1) and connected to an external electrical power source. The wire support was attached to the release system, and the entire assembly was suspended from the wire. After final electrical checks were made and the experiment package was switched to internal power, the system was released. After completion of the test, the experiment package and drag shield were returned to the preparation area.

## B. Experimental Results

1. General considerations. - In addition to the measurement and observation of steady state liquid flow patterns, two separate phenomena were observed. First, no circular hydraulic jump occurred during any

of the tests even though they are a common occurrence under normal gravity conditions. Secondly, the initial impact of the jet upon the solid surface provided another unusual phenomena, that of the rebounding liquid droplet. At high flow rates, the jet broke up prior to impinging upon the disk. The first droplet tended to impinge upon and stick to the disk, spreading as it did. However, the second droplet impinged and rebounded off this wetted surface sometimes into the incoming liquid jet. This provided no serious problem with the attainment of a steady state flow pattern since this all occurred during the transient phase.

The jet generally appeared to go through three phases during the impingement process. The initial phase, including the droplet pinch-off and subsequent impingement, was termed the transient phase. After a certain period of time, a steady state flow pattern was achieved from which the free surface shapes were measured and observations were made. A third phase was reached shortly after the jet had reached its equilibrium configuration. The flow pattern developed an instability. Initially, the instability started from the jet which began to oscillate, and then spread to the plume. Since the time over which the jet and flow pattern appeared stable and smooth was finite, steady state data could be obtained. It was observed that the time before breakdown was inversely proportional to the back pressure during the flow. At 1 psia, for example, the jet remained stable for 1.5 seconds while at 10 psi, it was stable for approximately 0.4 seconds. An attempt was made to lengthen the time over which stability occurred by packing the nozzle chamber with steel wool. This appeared to be effective in improving the overall stability but had the negative

effect of introducing a low level perturbation throughout the test and, thus, was not employed during any of the experiments.

2. Effect of nozzle height. - Several tests were conducted initially to determine the effect of  $H$ , the distance between the nozzle and the disk, on the experimental flow pattern. It was determined that there is no effect on the liquid flow provided that the ratio of the nozzle height  $H$  to the jet diameter is greater than 3. As a result, all zero gravity experiments were conducted in order to eliminate this effect. This fact, which was determined experimentally, supports the argument made in Section III, Order of Magnitude Analysis, concerning the assertion that  $H$  could not be a scale factor for the axial coordinate.

3. Steady state flow patterns. - The approximate steady state flows for three different jet velocities are shown photographically in Figure 9. The direction of flow of the liquid jet is vertically upwards. The threaded rod and bolt observed in the film clips is the disk holder which connects the sharp-edged disk assembly to the rig frame. The jet velocity increases from left to right in the figure. Three distinct classifications of flow patterns were observed to occur and are shown labeled in Figure 9 as surface tension flow, transition flow, and inertia flow. Surface tension flow (Fig. 9(a)) is defined as that flow in which the liquid flows completely around the disk with no separation occurring from the disk edge. In transition flow (Fig. 9(b)), surface tension and inertia forces are both important. Transition flow is defined as flow in which separation occurs from the disk and the resulting liquid sheet either collects upon itself forming an envelope or has the tendency to do so. Inertia flow (Fig. 9(c))



is defined as that flow in which the liquid separates from the disk with no liquid turning towards the jet centerline attempting to form an envelope. The flow pattern shown for transition flow is not really the steady state flow pattern one would expect if steady state conditions could have been reached. The reason for this is as follows: Some liquid is always traveling toward the disk from the point at which the envelope meets. This liquid flow strikes the back of the baffle and subsequently disrupts the initially formed envelope. The recirculation flow then is a strong function of the geometry of the disk holder, an uncontrollable parameter. This important distinction means that an analysis for free surface shapes would have to account for the geometry of the disk holder in the transition region. The surface tension flow is generally slow and, as a result, does not quite reach a steady state configuration on the back side of the disk. The inertia flow tests (represented by Fig. 9(c)) always reached steady state.

The experimental tests were conducted in the inviscid region of Figure 4. Depending on the particular ratio of  $(R_0/L)$ , there exists a minimum Reynolds number below which the runs can no longer be considered as viscous-free. The experimental results are listed in tabular form in Table 2 in which all the important parameters as well as the flow classifications are contained. One additional parameter, the Weber number, is listed in Table 1. As will be shown in the next section, when the Reynolds number is no longer a parameter to consider for flow classifications, the Weber number and ratio  $(R_0/L)$  remain. The Weber number  $\rho V^2 R_0 / \sigma$ , is basically the ratio of inertia to surface tension forces. In the flow category column, S indicates

surface tension flow, T indicates transition flow, and I is inertia flow. Finally, it is noted that the designated flow classification for some cases, particularly those bordering transition or inertia flow, could easily fit into either category.

4. Zero gravity results. - The data contained in Table 2 is shown graphically in Figure 10. The lines indicated in the figure were faired in by hand and separate the various flow classifications. It is observed that at any particular value of the ratio ( $R_o/L$ ), the flow classification is dependent only on the system Weber number. Two critical Weber numbers occur at a constant value of ( $R_o/L$ ). The lowest critical Weber number separates the surface tension flow from the transition flow while the higher critical Weber number separates the transition flow from the inertia flow. In addition, the critical Weber number between regimes was found to decrease as ( $R_o/L$ ) was increased.

## V. POTENTIAL FORMULATION

### A. Governing Equations and Boundary Conditions in Physical Plane Including Surface Tension

In Section III, Order of Magnitude Analysis, it was shown that at any particular value of  $R_0/L$  if  $Re > Re_{cr}$  the flow in the region of the disk can be considered as viscous free. It is further assumed that the jet will continue to remain viscous free after leaving the disk. There will be no shear stress between the exiting radial jet and the ambient air surrounding it.

1. General formulation. - Consider the flow of a circular liquid jet impinging normally on a circular disk as shown in Figure 11.  $R_0$  is the jet radius,  $L$  is the disk radius, and  $H$  is the distance between the jet reservoir and the disk. The incoming jet velocity is given as  $V$  and the initial velocity profile is assumed to be uniform. There will be two free surfaces involved. The upper free surface is defined as  $z_s = f_1(r)$  and the lower surface as  $z_s = f_2(r)$ . In addition, a third surface is required for the complete formulation of the boundary value problem. Initially, this surface was chosen as the straight line FE shown in Figure 11. However, this proved to be inconvenient since FE is arbitrary and, thus, has no known boundary condition. It was found convenient to instead choose the surface  $z = f_3(r)$  to be a surface along which the velocity potential is constant. Various points in the physical plane have been designated with letters ranging from A to G for convenience. In cylindrical coordinates, the governing

equations and boundary conditions in terms of primary variables (u,v) are given as follows:

Continuity:

$$\frac{1}{r} \frac{\partial}{\partial r} (ru) + \frac{\partial v}{\partial z} = 0 \quad (38)$$

Momentum:

r Component:

$$\rho \left( u \frac{\partial u}{\partial r} + v \frac{\partial u}{\partial z} \right) = - \frac{\partial p}{\partial r} \quad (39)$$

z Component:

$$\rho \left( u \frac{\partial v}{\partial r} + v \frac{\partial v}{\partial z} \right) = - \frac{\partial p}{\partial z} \quad (40)$$

The following boundary conditions are applied,

On DC

$$v = 0 \quad \text{on } z = 0, 0 \leq r \leq L \quad (41)$$

On AB

$$u = 0 \quad 0 \leq r \leq R_0, z = H \quad (42)$$

On BC

$$\frac{\partial v}{\partial r} = 0 \quad r = 0, 0 < z \leq H \quad (43)$$

On AG

$$\frac{1}{2} (u^2 + v^2) - \frac{\sigma}{\rho r} \frac{d}{dr} \left( - \frac{rf'_1}{\sqrt{1 + f'^2_1}} \right) = \frac{1}{2} v^2 - \frac{\sigma}{\rho R_0} \quad \text{on } z_s = f_1(r) \quad (44)$$

And

$$-uf'_1 + v = 0 \quad \text{on } z_s = f_1(r) \quad (45)$$

On DE

$$\frac{1}{2} (u^2 + v^2) - \frac{\sigma}{\rho r} \frac{d}{dr} \left( - \frac{rf'_2}{\sqrt{1 + f'^2_2}} \right) = \frac{1}{2} v^2 - \frac{\sigma}{\rho R_0} \quad \text{on } z_s = f_2(r) \quad (46)$$

And

$$-uf'_2 + v = 0 \quad \text{on } z_g = f_2(r) \quad (47)$$

On GE

$$u + vf'_3(r) = 0 \quad \text{on } z = f_3(r) \quad (48)$$

The derivation for the boundary condition along GE is as follows. Along GE, the velocity potential  $\phi$  is constant. By definition, the velocity vector  $\vec{V}$  is normal to an equipotential surface.

This means that

$$\vec{V} \times \hat{n} = 0 \quad \text{on } z = f_3(r) \quad (49)$$

The unit normal to  $f_3(r)$  is

$$\hat{n} = \frac{-f'_3 \hat{i} + \hat{j}}{\sqrt{f'^2_3 + 1}} \quad (50)$$

where  $\hat{i}$  is the unit vector in the radial direction and  $\hat{j}$  is the unit vector in the axial direction, and

$$\vec{V} = u\hat{i} + v\hat{j} \quad (51)$$

Application of equation (49) results in

$$\frac{u + vf'_3(r)}{\sqrt{f'^2_3 + 1}} = 0 \quad (52)$$

From which equation (48) follows.

**2. Introduction of Stokes Stream Function.** - The primary variables contained in the governing equations are the scalar velocity components  $u$  and  $v$ . The fact that two functions are required to describe one vector field is cumbersome. As shown in the theory of hydrodynamics, the number of functions can be reduced for several important cases, one of these being axisymmetric flow. A function  $\psi$ , defined as Stokes stream function, can be introduced which automatically satisfies

the continuity equation. With the additional requirement of irrotationality, the governing equation in terms of Stokes stream function will result. According to Chan (7), Stokes stream function is a mathematical device used to describe the flow and has the following properties. First, when the stream function is set equal to a constant, it results in different annular stream surfaces in axisymmetric flow. Secondly, when it is differentiated properly, it yields the velocity components. Thirdly, taking the difference between the values at two adjacent stream surfaces yields the flow rate.

Starting with equation (38), the continuity equation for axisymmetric flow, a guess is made at what  $u$  and  $v$  are in order to satisfy continuity identically. Assume

$$u = -\frac{1}{r} \frac{\partial \psi}{\partial z} \quad (53)$$

And

$$v = \frac{1}{r} \frac{\partial \psi}{\partial r} \quad (54)$$

Substitution of equations (53) and (54) into equation (38) shows that continuity is identically satisfied by these two guesses. In addition, the assumption is made that the flow is also irrotational. As a result

$$\text{Curl } \vec{V} = 0 \quad (55)$$

For axisymmetric flow, this can be written,

$$\frac{\partial u}{\partial z} - \frac{\partial v}{\partial r} = 0 \quad (56)$$

Replacing  $u$  and  $v$  in the above by their relationships to  $\psi$  results in the governing equation for axisymmetric flow in terms of Stokes stream function

$$\frac{\partial^2 \psi}{\partial z^2} - \frac{1}{r} \frac{\partial \psi}{\partial r} + \frac{\partial^2 \psi}{\partial r^2} = 0 \quad (57)$$

3. Derivation of boundary conditions in terms of  $\psi$ . - Since BC, CD, and DE are all a part of the same streamline, they must all have the same value for Stokes stream function. Let us arbitrarily set that value equal to zero. The value of  $\psi$  along AB and AG can be calculated from equation (54).

On AB

$$-v = \frac{1}{r} \frac{\partial \psi}{\partial r} \quad (58)$$

Integrating this yields

$$\psi = -\frac{vr^2}{2} \quad (59)$$

On AG since AG is a line of constant  $\psi$ ,

$$\psi = -\frac{vR_o^2}{2} \quad (60)$$

In addition, equation (44) applies. Substitution of equation (53) and (54) into (44) yields

$$\frac{1}{2r^2} \left[ \left( \frac{\partial \psi}{\partial z} \right)^2 + \left( \frac{\partial \psi}{\partial r} \right)^2 \right] - \frac{\sigma}{\rho r} \frac{d}{dr} \left( \frac{rf_1'}{\sqrt{1+f_1'^2}} \right) = \frac{1}{2} v^2 - \frac{\sigma}{\rho R_o} \quad \text{on } z_s = f_1(r) \quad (61)$$

On DE

$$\frac{1}{2r^2} \left[ \left( \frac{\partial \psi}{\partial z} \right)^2 + \left( \frac{\partial \psi}{\partial r} \right)^2 \right] - \frac{\sigma}{\rho r} \frac{d}{dr} \left( \frac{rf_2'}{\sqrt{1+f_2'^2}} \right) = \frac{1}{2} v^2 - \frac{\sigma}{\rho R_o} \quad \text{on } z_s = f_2(r) \quad (62)$$

It is noted that the second boundary conditions on the free surfaces, namely  $-uf_1' + v = 0$  and  $-uf_2' + v = 0$ , are fully equivalent to the specification of the value of Stokes stream function along that

surface. Since  $\psi = \psi(r, z)$ , it can be expanded and  $d\psi$  set equal to zero along AG and ED.

On GE, equation (48) becomes

$$-\frac{\partial \psi}{\partial z} + \frac{\partial \psi}{\partial r} f'_3(r) = 0 \quad \text{on } z = f_3(r) \quad (63)$$

4. Nondimensionalization of governing equations and boundary conditions in physical plane. - The governing equation in terms of Stokes stream function (eq. (57)) and the boundary conditions (eqs. (58) to (63)) are now put into dimensionless form by introducing arbitrary scale factors. Let the scale factor for the stream function be  $-VR_0^2$ . Let dimensionless quantities be represented by stars, i.e.,  $\psi^*$  is dimensionless. The results of this manipulation are shown in Figure 12. Three parameters appear in the specification of boundary conditions. They include the Weber number,  $We$ , and the dimensionless length ratios  $L/R_0$  and  $H/R_0$ . Recalling the arguments in the Order of Magnitude Analysis section,  $H/R_0$  is not really a parameter provided it is larger than some minimum value. The dimensionless velocity components can be calculated from the following expressions

$$\frac{u}{V} = \frac{1}{r^*} \frac{\partial \psi^*}{\partial z^*} \quad (64)$$

$$\frac{v}{V} = -\frac{1}{r^*} \frac{\partial \psi^*}{\partial r^*} \quad (65)$$

The procedure for solution of the boundary value problem as set up in dimensionless form in the physical plane (Fig. 12) would be as follows: Initially, realistic variations for  $f_1^*(r)$ ,  $f_2^*(r)$ , and  $f_3^*(r)$  are assumed. Using only one of the two given boundary conditions on AG and GE (i.e.,  $\psi^* = 1/2$  and  $\psi^* = 0$ ) solve for  $\psi^*$  using finite difference methods. With the initial solution for  $\psi^*$  check the va-



lidity of the second of the two boundary conditions on AG and GE. If the boundary conditions are not satisfied, new variations in  $f_1^*$ ,  $f_2^*$ , and  $f_3^*$  must be assumed. A second iteration to  $\psi^*$  must be obtained and so on. One of the serious drawbacks of this outlined iteration scheme is the lack of knowledge concerning how to update assumed values of  $f_1^*$ ,  $f_2^*$ , and  $f_3^*$  based on previous solutions. In other words, there is no logical way in which to make changes to the shape of the initially assumed control volume.

5. Surface tension dominated model. - For Weber numbers between 5 and 30 (depending on the ratio  $R_0/L$ ), experimental data shows that the resulting steady-state flow pattern is surface tension dominated (see Fig. 9(a)). By previous definition, surface tension flow is defined as that flow in which the liquid flows completely around the disk with no separation from the edge. It is the intent to model this flow in order to solve for the theoretical free surface shapes and velocity profiles. Assuming axisymmetry, the physical plane model is shown in Figure 13. In the model, at some cross-section far downstream, the flow is assumed to approach the initially uniform flow it possessed at AB. The exiting plane is denoted by GE in the model. C and C' are both located at  $r = 0$ ,  $z = 0$ . C is located on top of the plate while C' is on the bottom. The free surface  $f_1(r)$ , is not assumed to possess mirror symmetry about the  $z = 0$  position. In cylindrical coordinates, the governing equations and boundary conditions in terms of the primary variables (u,v) are given as follows:

Continuity:

$$\frac{1}{r} \frac{\partial}{\partial r} (ru) + \frac{\partial v}{\partial z} = 0 \quad (66)$$

Momentum:

r Component

$$\rho \left( u \frac{\partial u}{\partial r} + v \frac{\partial u}{\partial z} \right) = - \frac{\partial p}{\partial r} \quad (67)$$

z Component

$$\rho \left( u \frac{\partial v}{\partial r} + v \frac{\partial v}{\partial z} \right) = - \frac{\partial p}{\partial z} \quad (68)$$

The following boundary conditions are applied

On DC

$$v = 0 \quad \text{on } z = 0, 0 \leq r \leq L \quad (69)$$

On DC'

$$v = 0 \quad \text{on } z = 0, 0 \leq r \leq L \quad (70)$$

On AB

$$u = 0 \quad 0 \leq r \leq R_0, z = H \quad (71)$$

On BC

$$\frac{\partial v}{\partial r} = 0 \quad \text{on } r = 0, 0 < z \leq H \quad (72)$$

On C'E

$$\frac{\partial v}{\partial r} = 0 \quad \text{on } r = 0, -H \leq z < 0 \quad (73)$$

On GE

$$u = 0 \quad 0 \leq r \leq R_0, z = -H \quad (74)$$

On AG

$$\frac{1}{2} (u^2 + v^2) - \frac{\sigma}{\rho r} \frac{d}{dr} \left( \frac{r f_1'}{\sqrt{1 + f_1'^2}} \right) = \frac{1}{2} v^2 - \frac{\sigma}{\rho R_0} \quad \text{on } z_s = f_1(r) \quad (75)$$

and

$$-u f_1' + v = 0 \quad \text{on } z_s = f_1(r) \quad (76)$$

Equations (75) and (76) represent two distinct pieces of information

concerning  $z_s = f_1(r)$ . It is noted that  $f_1'$  can be eliminated from

the set of equations by means of simple substitution. This fact will have implications later in the development leading to a major simplification. The following expression would result,

$$\frac{1}{2} (u^2 + v^2) - \frac{\sigma}{\rho r} \frac{d}{dr} \left( \frac{r}{\sqrt{\frac{u^2}{v^2} + 1}} \right) = \frac{1}{2} v^2 - \frac{\sigma}{\rho R_0} \quad \text{on } z_s = f_1(r) \quad (77)$$

Direct substitution of equations (53) and (54), the relations between the velocity components and Stokes stream function, into the governing equation and boundary conditions for the surface tension model results in the formulation shown in Figure 14 after nondimensionalization.

Similar to the general formulation in the last section, the various lengths in the problem are scaled with respect to  $R_0$  and the scale factor for Stokes stream function is  $-VR_0^2$ .

### B. Inverse Plane Formulations

The procedure for solving for the free surface shapes in the physical plane has been outlined previously. The difficulties encountered when making adjustments to the free surfaces between iterations and the lack of a logical manner in which to make the adjustments have been cited. This would be a time consuming task even in the absence of surface tension. A computerized scheme is sought which offers the possibility of achieving the free-surface results with a minimum of computer iteration time and user interaction.

1. Transformation formulas. - An alternate approach to the physical plane solution is discussed in detail by Jeppson (19). In his article, Jeppson discusses a transformation technique into what is defined as the inverse plane. The coordinate axes in the inverse plane are the velocity potential  $\phi$  and Stokes stream function  $\psi$ . The ad-

vantage to using the  $\phi\psi$  space, or inverse plane, is that the free surface lies along a line of constant  $\psi$  and is, therefore, at a known position. Of course, one must pay the price for knowing the position of the free surface. As will be shown shortly, the governing equation is no longer linear as it was in the physical plane.

2. Introduction of velocity potential. - The use of a scalar function defined as the velocity potential has been used previously in the specification of the boundary GE (the exiting plane). The continuity equation for steady incompressible axisymmetric flow is given by equation (38). The flow is also assumed to be irrotational such that the condition given by equation (56) is also valid. Equation (56) implies that there exists a scalar potential function  $\phi$  such that

$$\vec{V} = \text{grad } \phi \quad (78)$$

from which it follows

$$u = \frac{\partial \phi}{\partial r} \quad (79)$$

and

$$v = \frac{\partial \phi}{\partial z} \quad (80)$$

Substitution of equations (79) and (80) yields the governing equation for steady axisymmetric flow in terms of the velocity potential

$$\frac{\partial^2 \phi}{\partial z^2} + \frac{1}{r} \frac{\partial \phi}{\partial r} + \frac{\partial^2 \phi}{\partial r^2} = 0 \quad (81)$$

3. Relationship between  $\psi$  and  $\phi$ . - It can now be stated that the relationships between the velocity potential and Stokes's stream function are given as:

$$u = \frac{\partial \phi}{\partial r} = - \frac{1}{r} \frac{\partial \psi}{\partial z} \quad (82)$$

and

$$v = \frac{\partial \phi}{\partial z} = \frac{1}{r} \frac{\partial \psi}{\partial r} \quad (83)$$

4. Inverse plane formulation. - In order to formulate the problem in the physical plane,  $r$  and  $z$  must be known as functions of  $\psi$  and  $\phi$ . In other words, we are attempting to reverse the roles of the dependent and independent variables in the inverse plane. The required relationships are obtained noting that if  $\psi = \psi(r, z)$  and  $\phi = \phi(r, z)$ , then there exist inverse functions  $r = r(\phi, \psi)$  and  $z = z(\phi, \psi)$  as shown in reference 13 such that

$$\frac{\partial r}{\partial \phi} = - \frac{1}{J} \frac{\partial \psi}{\partial z} \quad (84)$$

$$\frac{\partial z}{\partial \psi} = - \frac{1}{J} \frac{\partial \phi}{\partial r} \quad (85)$$

$$\frac{\partial z}{\partial \phi} = \frac{1}{J} \frac{\partial \psi}{\partial r} \quad (86)$$

$$\frac{\partial r}{\partial \psi} = \frac{1}{J} \frac{\partial \phi}{\partial z} \quad (87)$$

and where the Jacobian  $J$  is defined as

$$J = \begin{vmatrix} \frac{\partial \phi}{\partial r} & \frac{\partial \phi}{\partial z} \\ \frac{\partial \psi}{\partial r} & \frac{\partial \psi}{\partial z} \end{vmatrix} = \left( \frac{\partial \phi}{\partial r} \right) \left( \frac{\partial \psi}{\partial z} \right) - \left( \frac{\partial \phi}{\partial z} \right) \left( \frac{\partial \psi}{\partial r} \right) \quad (88)$$

From the above set of equations follow two important relations. Substituting into equation (82) the values of  $\partial \phi / \partial r$  and  $\partial \psi / \partial z$  obtained from equations (84) and (85) yields

$$\frac{\partial z}{\partial \psi} = - \frac{1}{r} \frac{\partial r}{\partial \phi} \quad (89)$$

Similarly, substitution of the values of  $\partial \phi / \partial z$  and  $\partial \psi / \partial r$  from equations (86) and (87) into equation (83) yields

$$\frac{\partial r}{\partial \psi} = \frac{1}{r} \frac{\partial z}{\partial \phi} \quad (90)$$

For subsequent relations, it is necessary to express the Jacobian in terms of the inverse function  $r(\psi, \phi)$  and  $z(\psi, \phi)$ . Substituting equations (84) to (87) into equation (88) results in

$$J = J^2 \left[ \left( \frac{\partial z}{\partial \psi} \right) \left( \frac{\partial r}{\partial \phi} \right) - \left( \frac{\partial r}{\partial \psi} \right) \left( \frac{\partial z}{\partial \phi} \right) \right] \quad (91)$$

Now, using equations (89) and (90) in the above yields,

$$J = - \frac{1}{r \left[ \left( \frac{\partial z}{\partial \psi} \right)^2 + \left( \frac{\partial r}{\partial \psi} \right)^2 \right]} = - \frac{r}{\left( \frac{\partial r}{\partial \phi} \right)^2 + \left( \frac{\partial z}{\partial \phi} \right)^2} \quad (92)$$

5. Governing equations for inverse functions. - Differentiating equation (89) with respect to  $\psi$  yields

$$\frac{\partial^2 z}{\partial \psi^2} = - \frac{1}{r} \frac{\partial^2 r}{\partial \psi \partial \phi} + \frac{1}{r^2} \frac{\partial r}{\partial \psi} \frac{\partial r}{\partial \phi} \quad (93)$$

and combining this with the derivatives of equation (90) with respect to  $\phi$ , which is

$$\frac{\partial^2 r}{\partial \phi \partial \psi} = - \frac{1}{r^2} \left( \frac{\partial r}{\partial \phi} \right) \left( \frac{\partial z}{\partial \phi} \right) + \frac{1}{r} \frac{\partial^2 z}{\partial \phi^2} \quad (94)$$

it is found that

$$\frac{\partial^2 z}{\partial \psi^2} = \frac{1}{r^3} \frac{\partial r}{\partial \phi} \frac{\partial z}{\partial \phi} - \frac{1}{r^2} \frac{\partial^2 z}{\partial \phi^2} + \frac{1}{r^2} \frac{\partial r}{\partial \phi} \frac{\partial r}{\partial \psi} \quad (95)$$

By using equations (89) and (90), the terms involving derivatives in equation (95) can be expressed entirely in terms of  $z$ , giving the important equation,

$$r^2 \frac{\partial^2 z}{\partial \psi^2} + \frac{\partial^2 z}{\partial \phi^2} = -2 \frac{\partial z}{\partial \psi} \frac{\partial z}{\partial \phi} \quad (96)$$

On the other hand, differentiating equation (89) with respect to  $\phi$  and equation (90) with respect to  $\psi$  and combining the result leads to the equation

$$\frac{\partial^2 r}{\partial \psi^2} = -\frac{1}{r^2} \frac{\partial^2 r}{\partial \phi^2} + \frac{1}{r^3} \left( \frac{\partial r}{\partial \phi} \right)^2 - \frac{1}{r^2} \frac{\partial r}{\partial \psi} \frac{\partial z}{\partial \phi} \quad (97)$$

By substitution for  $\partial z / \partial \phi$  from equation (90), the following equation for  $r(\phi, \psi)$  is obtained:

$$\frac{\partial^2 r}{\partial \psi^2} + \frac{1}{r^2} \frac{\partial^2 r}{\partial \phi^2} - \frac{1}{r^3} \left( \frac{\partial r}{\partial \phi} \right)^2 + \frac{1}{r} \left( \frac{\partial r}{\partial \psi} \right)^2 = 0 \quad (98)$$

For further discussion, equation (96) will be referred to as the  $z$  equation while equation (98) will be called the  $r$  equation. Both of these equations are nonlinear with the nonlinearity in the  $z$  equation also involving  $r$ . It is further noted that both of these equations are of the elliptic type, as shown in reference 19. This means that boundary conditions are required for all boundaries in the flow region. Since the  $r$  equation (eq. (98)) only involves that variable, a solution to the problem begins with its solution.

One final point involves the fact that the variables discussed in the above inverse transformations are all dimensional. It is noted that nondimensionalization of the above equations similar to the nondimensionalization done in the physical plane allows us to recover the same equation.

Let

$$\left. \begin{aligned} z^* &= \frac{z}{z_0} & \text{where } z_0 &= R_0 \\ r^* &= \frac{r}{r_0} & \text{where } r_0 &= R_0 \\ \psi^* &= \frac{\psi}{\psi_0} & \text{where } \psi_0 &= -VR_0^2 \\ \phi^* &= \frac{\phi}{\phi_0} & \text{where } \phi_0 &= -VR_0 \end{aligned} \right\} \quad (99)$$

The results of this substitution yields exactly the same governing equations and transformation formulas in starred notation. In other words,

$$r^{*2} \frac{\partial^2 z^*}{\partial \psi^{*2}} + \frac{\partial^2 z^*}{\partial \phi^{*2}} = -2 \frac{\partial z^*}{\partial \psi^*} \frac{\partial z^*}{\partial \phi^*} \quad (100a)$$

and

$$\frac{\partial^2 r^*}{\partial \psi^{*2}} + \frac{1}{r^{*2}} \frac{\partial^2 r^*}{\partial \phi^{*2}} - \frac{1}{r^{*3}} \left( \frac{\partial r^*}{\partial \phi^*} \right)^2 + \frac{1}{r^*} \left( \frac{\partial r^*}{\partial \psi^*} \right)^2 = 0 \quad (100b)$$

6. Infinite flat plate excluding surface tension. - The first problem to be examined in which we employ the inverse transformation is the flow of a circular liquid jet normal to a flat plate. At this point, we drop the starred notation to designate dimensionless quantities. It is assumed that all quantities appearing henceforth are dimensionless unless otherwise stated (i.e.,  $r$ ,  $z$ ,  $\psi$ ,  $\phi$ , are now dimensionless). For the case in which surface tension is excluded, the physical plane model depicted in Figure 12 must necessarily change. The model in Figure 12 is for the general case of a finite disk in which surface tension effects are important. For the case of an infinite flat plate, since the free surface ED no longer exists, the designation D does not appear in the model. Furthermore, for the case in which surface tension forces are unimportant, the boundary condition along the upper surface (referring to Fig. 12) can be written as follows:

On AG

$$\frac{1}{r^2} \left[ \left( \frac{\partial \psi}{\partial z} \right)^2 + \left( \frac{\partial \psi}{\partial r} \right)^2 \right] = 1 \quad (101)$$

This expression is obtained by allowing the Weber number to approach



infinity. The reasoning for letting the Weber number become large is because it is the ratio of inertial to surface tension forces. The case we are examining is one in which the surface tension forces become vanishingly small or the inertial forces becoming large. Finally, the boundary GE will be nearly vertical implying that the velocity there is purely radial.

7. Derivation of boundary conditions in inverse plane for  $r$  formulation. -

On AB

$$\left. \begin{array}{l} \text{In the physical plane, } \psi = \frac{1}{2} r^2 \\ \text{In the inverse plane, } r = \sqrt{2\psi} \end{array} \right\} \quad (102)$$

On BC

$$\left. \begin{array}{l} \text{In the physical plane, } \psi = 0 \\ \text{In the inverse plane, } r = 0 \end{array} \right\} \quad (103)$$

On EC

$$\left. \begin{array}{l} \text{In the physical plane, } \psi = 0 \\ \text{Also } v = 0, \text{ by equation (83) this implies that } \frac{\partial \phi}{\partial z} \text{ and } \frac{\partial \psi}{\partial r} = 0. \\ \text{In the inverse plane (via eq. (87)), } \frac{\partial r}{\partial \psi} = 0 \end{array} \right\} \quad (104)$$

On GE

$$\left. \begin{array}{l} \text{In the physical plane, } \frac{\partial \psi}{\partial r} = 0 \\ \text{In the inverse plane, } \frac{\partial r}{\partial \psi} = 0 \end{array} \right\} \quad (105)$$

On AG

$$\text{In the physical plane, } \frac{1}{r^2} \left[ \left( \frac{\partial \psi}{\partial z} \right)^2 + \left( \frac{\partial \psi}{\partial r} \right)^2 \right] = 1$$

In the inverse plane, using equations (82) and (83), this becomes

$$\left(\frac{\partial \phi}{\partial r}\right)^2 + \left(\frac{\partial \phi}{\partial z}\right)^2 = 1$$

and upon using relations (85) and (87)

$$J^2 \left[ \left(\frac{\partial z}{\partial \psi}\right)^2 + \left(\frac{\partial r}{\partial \psi}\right)^2 \right] = 1$$

Substituting in for  $J^2$  from equation (92) and then using (89) and (90) yields the final form

$$\left(\frac{\partial r}{\partial \phi}\right)^2 + r^2 \left(\frac{\partial r}{\partial \psi}\right)^2 = 1 \quad (106)$$

The results of the above calculations are shown in Figure 15(a) in the inverse plane. For the case of flow normal to an infinite flat plate, the  $r$  values can now be completely found once we solve the nonlinear governing equation. The variable  $z$  does not appear anywhere in the formulation. In addition, the boundary conditions for the  $z$  formulation were also derived and are indicated in Figure 15(b). It follows that the  $z$  solution cannot be obtained until after  $r$  values are known since the  $r$  values are required on the free surface boundary and within the interior flow. The boundary conditions for the  $z$  formulation were derived as follows:

8. Derivation of boundary conditions in inverse plane for  $z$  formulation. -

On AB

In the physical plane,  $u = 0$  which implies  $\frac{\partial \phi}{\partial r} = 0$

From equation (85),  $\frac{\partial z}{\partial \psi} = 0$

This implies that  $z = z(\phi)$  alone and since

AB is a line of constant  $\phi$ ,

in the inverse plane  $z = \text{constant}$

(107)

On BC

$$\left. \begin{array}{l} \text{In physical plane, } u = 0 \\ \text{From which it follows, in the inverse plane } \frac{\partial z}{\partial \psi} = 0 \end{array} \right\} \quad (108)$$

On EC

$$\left. \begin{array}{l} \text{In physical plane } \psi = 0 \\ \text{In inverse plane } z = 0 \end{array} \right\} \quad (109)$$

On GE

$$\left. \begin{array}{l} \text{In physical plane, } v = 0 \\ \text{From equation (83), it follows that } \frac{\partial \psi}{\partial r} = 0 \\ \text{and from equation (86), we have in the inverse plane } \frac{\partial z}{\partial \phi} = 0 \end{array} \right\} \quad (110)$$

On AG

$$\left. \begin{array}{l} \text{In the physical plane } \frac{1}{r^2} \left[ \left( \frac{\partial \psi}{\partial z} \right)^2 + \left( \frac{\partial \psi}{\partial r} \right)^2 \right] = 1 \\ \text{In the inverse plane we can take over the equivalent ex-} \\ \text{pression given by equation (106) } \left( \frac{\partial r}{\partial \phi} \right)^2 + r^2 \left( \frac{\partial r}{\partial \psi} \right)^2 = 1 \\ \text{Using equations (89) and (90) to eliminate the derivative} \\ \text{involving } r \text{ results in } r^2 \left( \frac{\partial z}{\partial \psi} \right)^2 + \left( \frac{\partial z}{\partial \phi} \right)^2 = 1 \end{array} \right\} \quad (111)$$

9. Finite plate excluding surface tension. - A second problem to be formulated is concerned with the impingement of a circular liquid jet normal to a disk of finite width. For the case in which surface tension effects are neglected, the model depicted in Figure 12 will vary only slightly. The only difference being that the boundary conditions along the top and bottom free surfaces are now expressed as

$$\frac{1}{r^2} \left[ \left( \frac{\partial \psi}{\partial z} \right)^2 + \left( \frac{\partial \psi}{\partial r} \right)^2 \right] = 1$$

The  $r$  formulation in the inverse plane is shown in Figure 16(a). The only boundary condition that bears some explanation is that along GE, the exiting plane in the physical plane, from Figure 12,

$$\frac{\partial \psi}{\partial z} - \frac{\partial \psi}{\partial r} f'_3 = 0 \quad (112)$$

Using equations (84) and (86) this can be written

$$\frac{\partial r}{\partial \phi} + \frac{\partial z}{\partial \phi} f'_3 = 0 \quad (113)$$

Finally, using equation (90) to eliminate  $\partial z / \partial \phi$ ,

$$\frac{\partial r}{\partial \phi} + r \frac{\partial r}{\partial \psi} f'_3 = 0 \quad (114)$$

or

$$\frac{\partial r}{\partial \phi} + r \left( \frac{\partial r}{\partial \psi} \right) \left( \frac{dz}{dr} \right) = 0 \quad (115)$$

The  $z$  formulation in the inverse plane is shown in Figure 16(b). Here again, only the boundary condition along GE bears some explanation. Continuing with equation (115) and using equations (89) and (90) we obtain

$$r \left( \frac{\partial z}{\partial \psi} \right) - \left( \frac{\partial z}{\partial \phi} \right) \left( \frac{dz}{dr} \right) = 0 \quad (116)$$

The formulation of the problem of flow of a circular liquid jet normal to a finite disk in the inverse plane is now complete. The  $r$  solution (Fig. 16(a)) can no longer be obtained independent of the  $z$  solution due to the exiting jet boundary condition. Thus, the problem will necessitate a simultaneous solution of two partial differential equations of the nonlinear elliptic type.

10. Finite plate including surface tension. - A third problem that is formulated but not solved due to the complexity of applying it to a

real system involves the normal impingement to a finite disk in which both surface tension and inertial forces are important. These would include all the flows experimentally labeled as transition flows. This represents a complete inverse formulation for the exact physical model represented in Figure 12. The results of the inverse formulation for the  $r$  solution are shown in Figure 17. The way in which the inverse boundary conditions along the free surface were derived will be made more clear in the next section.

11. Surface tension dominated model - finite plate. - The final problem to be examined involves the surface tension dominated flow, described in Figure 14. The inverse plane formulation for the  $r$  solution is indicated in Figure 18(a). The boundary conditions are the same as derived previously with the exception of the free surface boundary. Along AG in the physical plane,

$$\frac{1}{2r^2} \left[ \left( \frac{\partial \psi}{\partial z} \right)^2 + \left( \frac{\partial \psi}{\partial r} \right)^2 \right] - \frac{1}{We} \frac{1}{r} \frac{d}{dr} \left[ \frac{r}{\sqrt{\left( \frac{\partial \psi}{\partial z} \right)^2 + 1}} \right] = \frac{1}{2} - \frac{1}{We} \quad (117)$$

In the derivation of equation (106), it was shown that

$$\frac{1}{r^2} \left[ \left( \frac{\partial \psi}{\partial z} \right)^2 + \left( \frac{\partial \psi}{\partial r} \right)^2 \right] = \frac{1}{\left( \frac{\partial r}{\partial \phi} \right)^2 + r^2 \left( \frac{\partial r}{\partial \psi} \right)^2} \quad (118)$$

In addition, using equations (84) and (86),

$$\left( \frac{\frac{\partial \psi}{\partial z}}{\frac{\partial \psi}{\partial r}} \right)^2 = \frac{1}{r^2} \left( \frac{\frac{\partial r}{\partial \phi}}{\frac{\partial r}{\partial \psi}} \right)^2 \quad (119)$$

Therefore, the inverse boundary condition along AG becomes

$$\frac{1}{2} \frac{1}{\left(\frac{\partial r}{\partial \phi}\right)^2 + r^2 \left(\frac{\partial r}{\partial \psi}\right)^2} - \frac{1}{We} \frac{1}{r} \frac{d}{dr} \left[ \frac{r}{\sqrt{\frac{1}{r^2} \left(\frac{\partial r}{\partial \phi}\right)^2 + 1}} \right] = \frac{1}{2} - \frac{1}{We} \quad (120)$$

which can be written

$$\frac{1}{2} \frac{1}{\left(\frac{\partial r}{\partial \phi}\right)^2 + r^2 \left(\frac{\partial r}{\partial \psi}\right)^2} - \frac{1}{We} \frac{1}{r} \frac{d}{dr} \left[ \frac{r^2}{\sqrt{\left(\frac{\partial r}{\partial \phi}\right)^2 + r^2}} \right] = \frac{1}{2} - \frac{1}{We} \quad (121)$$

Multiplying through by 2, and rearranging yields,

$$\left(\frac{\partial r}{\partial \phi}\right)^2 + r^2 \left(\frac{\partial r}{\partial \psi}\right)^2 = \frac{1}{\left\{ 1 - \frac{2}{We} + \frac{2}{We} \frac{1}{r} \frac{d}{dr} \left[ \frac{r^2}{\sqrt{\left(\frac{\partial r}{\partial \phi}\right)^2 + r^2}} \right] \right\}} \quad (122)$$

There has been no symmetry assumed for the  $r$  formulation, only axisymmetry. It is noted that the  $r$  formulation does not involve the variable  $z$ . This means that the  $r$  and  $z$  solutions can be obtained independently. The  $z$  formulation is indicated in Figure 18(b).

## VI. CENTRAL FINITE DIFFERENCE REPRESENTATION

The finite difference operators for the nonlinear  $r$  and  $z$  elliptic partial differential equations resulting from the inversion were put into difference form. It was found from experience that considerable flexibility resulted if the difference equations were derived employing rectangular mesh. The reason for this becomes clearer as we progress into the numerical solution. Suffice to say that this allowed us to control the size of the flow region. Square meshes were originally attempted, but only led to solutions in the cases where the mesh sizes became vanishingly small.

### A. Formulation

1. General considerations. - The partial derivatives appearing in the  $r$  and  $z$  governing equations are replaced by algebraic central finite difference operators. A complete derivation of the various operators is contained in reference 35. The notation used in this report is that shown in Figure 19. If the finite difference analogy of  $\partial/\partial r$  is  $\delta/\delta r$ , the  $r$  derivatives can be written at point 0 as follows,

$$\frac{\delta r}{\delta \phi} = \frac{r_1 - r_3}{2 \Delta \phi} \quad (123)$$

$$\frac{\delta r}{\delta \psi} = \frac{r_2 - r_4}{2 \Delta \psi} \quad (124)$$

$$\frac{\delta^2 r}{\delta \phi^2} = \frac{r_1 + r_3 - 2r_0}{\Delta \phi^2} \quad (125)$$

$$\frac{\delta^2 r}{\delta \psi^2} = \frac{r_2 + r_4 - 2r_o}{\Delta \psi^2} \quad (126)$$

Similarly, the central finite difference representations for the  $z$  derivatives are,

$$\frac{\delta z}{\delta \phi} = \frac{z_1 - z_3}{2 \Delta \phi} \quad (127)$$

$$\frac{\delta z}{\delta \psi} = \frac{z_2 - z_4}{2 \Delta \psi} \quad (128)$$

$$\frac{\delta^2 z}{\delta \phi^2} = \frac{z_1 + z_3 - 2z_o}{\Delta \phi^2} \quad (129)$$

$$\frac{\delta^2 z}{\delta \psi^2} = \frac{z_2 + z_4 - 2z_o}{\Delta \psi^2} \quad (130)$$

2. Interior nodal points. - If equations (123) to (126) are substituted into the  $r$  governing equation (eq. (98)) with  $\alpha = \Delta \phi / \Delta \psi$ , the finite difference expression for all interior nodal points is obtained,

$$r_o^4 - \frac{r_o^3}{2} (r_2 + r_4) + r_o^2 \left[ \frac{1}{\alpha^2} - \frac{1}{8} (r_2 - r_4)^2 \right] - \frac{r_o}{2\alpha^2} (r_1 + r_3) + \frac{1}{8\alpha^2} (r_1 - r_3)^2 = 0 \quad (131)$$

In addition, if equations (127) to (130) are substituted into the  $z$  governing equation (eq. (96)), the finite difference expression for all interior nodal points is obtained

$$z_o = \frac{r_o^2}{2 \left( r_o^2 + \frac{1}{\alpha^2} \right)} (z_2 + z_4) + \frac{1}{2 \left( r_o^2 \alpha^2 + 1 \right)} (z_1 + z_3) + \frac{1}{4 \left( r_o^2 \alpha^2 + \frac{1}{\alpha} \right)} (z_2 - z_4)(z_1 - z_3) \quad (132)$$



where, as in the derivation of equation (131),

$$\alpha = \frac{\Delta\phi}{\Delta\psi} \quad (133)$$

## B. Excluding Surface Tension

1. Infinite flat plate. - The finite difference representation for the infinite flat plate is shown in Figures 20(a) and (b). The algebraic expressions for the boundaries is derived by simultaneous application of the governing equation and boundary conditions at a fixed point. This application involves a fictitious point,  $f$ , outside the boundary which is subsequently eliminated. Point  $G$  represents a special point in the finite difference representation for the  $z$  solution since it is a part of two separate boundaries. The governing  $z$  equation (eq. (132)) was applied at point  $G$  which resulted in two fictitious points. Then the boundary conditions along both  $AG$  and  $GE$  were applied at point  $G$ . This allowed the elimination of the two fictitious points from the resulting finite difference expression. Detailed calculations for the boundaries are contained in Appendix C.

2. Finite plate. - The inverse formulation for the finite plate problem (Fig. 16), is shown in difference form in Figure 21. For this case, the difference operator along  $GE$  is more complicated than in the infinite plate case. In fact, both  $G$  and  $E$  represent special points in the formulation. However, one of these, point  $E$ , is specified as a known position ( $r = \text{constant}$ ). At point  $G$  the equation to be satisfied in the  $r$  formulation is shown at the top of Figure 21(a). In the formulation (Fig. 21(b)), both points  $G$  and  $E$  are special points. The following equations hold there.

At point G

$$z_o = \frac{r_o}{\left(r_o^2 + \frac{1}{\alpha^2}\right)} \left\{ \frac{1}{r_o} \sqrt{\left[a^2 - r_o^2(r_o - r_4)^2\right]} + z_4 \right\} + \frac{z_1 - r_o \alpha (r_o - r_4)}{r_o^2 \alpha^2 + 1} + \frac{r_o - r_4}{r_o^2 + \frac{1}{\alpha^2}} \sqrt{\left[a^2 - r_o^2(r_o - r_4)^2\right]} \quad (134)$$

At point E

$$z_o = \frac{r_o^2}{r_o^2 + \frac{1}{\alpha^2}} \left\{ z_2 - \frac{1}{r_o} \sqrt{\left[a^2 - r_o^2(r_2 - r_o)^2\right]} \right\} + \frac{z_1 - r_o \alpha (r_2 - r_o)}{r_o^2 \alpha^2 + 1} + \frac{r_2 - r_o}{r_o^2 + \frac{1}{\alpha^2}} \sqrt{\left[a^2 - r_o^2(r_2 - r_o)^2\right]} \quad (135)$$

Detailed calculations for all the additional boundaries encountered for the finite plate case are contained in Appendix C.

### C. Surface Tension

The difference formulation corresponding to the Surface Tension model (shown in Fig. 18) is indicated in Figure 22(a) and (b). The only boundary condition that must be explained is the one along the free surface AG. Details of this calculation are contained in Appendix C. It is noted that (see Fig. 22(a)) the  $r$  solution can be obtained independent of the  $z$  solution.

## VII. DISCUSSION OF NUMERICAL TECHNIQUES

Since the governing equations for the  $r$  and  $z$  formulations are nonlinear in the inverse plane, in general, the finite difference operations at the interior and boundary points will be nonlinear (see eqs. (131) and (132)). For the infinite flat plate case, as described in Figure 20, the solution begins with  $r = r(\psi, \phi)$  from Figure 20(a). Secondly, with a knowledge of the  $r$  solution, the  $z$  formulation, shown in Figure 20(b), is solved for  $z(\psi, \phi)$ . However, in the case where the plate is finite, the  $r$  formulation also contains  $z$  along the exiting plane GE (see Fig. 21(a)). As a result, the  $r$  and  $z$  formulations must be solved simultaneously. The surface tension model, described in Figure 22, also allows the solution of the  $r$  equation independent of the  $z$  equations since  $z$  appears nowhere in the formulation.

In any case, when solving the  $r$  equation, the finite difference representation of the problem results in  $N$  nonlinear algebraic equations in  $N$  unknowns. A variety of methods were applied in order to obtain a solution to the simultaneous nonlinear equations. These included Lieberstein's extension of Youngs' work on over-relaxation to nonlinear elliptic partial differential equations (26), and the familiar Newton-Raphson method. None of the above methods were successful in obtaining a convergent solution. The technique suggested by Powell (34) resulted in the method used in this paper to obtain solutions. Basically, Powell developed a subroutine which was essentially

a "compromise between the Newton-Raphson algorithm and the methods of steepest descents." In his paper, a Fortran subroutine is described for solving the nonlinear set of equations,

$$f_K(x_1, x_2, \dots, x_N) = 0 \quad K = 1, 2, \dots, N \quad (138)$$

The objective is to minimize the function

$$F(x_1, x_2, \dots, x_N) = \sum_{K=1}^N [f_K(x_1, x_2, \dots, x_N)]^2 \quad (139)$$

As with many iteration schemes, initial guesses are required for  $X_i$ . This particular algorithm has an advantage in that the initial guessed values do not have to be that close to the exact solution. The computer program for the  $r$  solution contains the main program and three subroutines. The subroutine EQNS is the one supplied by Powell. The user supplies the subroutine MATINV which inverts the matrices and the subroutine CALFUN which contains the nonlinear functions  $F(X_i)$ . A knowledge of the  $r$  solution makes the  $z$  formulation explicit in the unknown  $z_0$  at each nodal point. As a result, a Gauss-Siedel linear iteration scheme was employed to obtain the solution.

For details of the subroutines, the reader is referred to reference 34. As we get into the computer results in the next section, a complete printout of the subroutine will be presented.

## VIII. NUMERICAL RESULTS

### A. Exclusion of Surface Tension

1. Infinite flat plate (Weber number  $\rightarrow \infty$ ). - Initially, the finite flat plate problem was numerically solved employing a very coarse mesh. Referring to Figure 20(a), the total stream function was divided into five equal parts. Recall that  $\psi_G = 1/2$  and  $\psi_A = 0$  which meant that the parameter  $a = \Delta\psi$  was set equal to 0.1. In addition, the  $\phi$  axis was divided up into eight equal parts. This division was purely arbitrary. One consideration was that there would be at least two vertical lines of constant  $\phi$  between points C and B. This resulted in a total of 39 unknown nodal points for the  $r$  formulation indicated in Figure 20(a), and 41 unknown nodal points for the  $z$  formulation shown in Figure 20(b). The value of  $D = \alpha$  where  $\alpha = \Delta\phi/\Delta\psi$ , was set equal to 0.0204. In Figure 20(a), the value of  $C$  along GE was arbitrarily chosen as 4.0 while the value of  $z$  along AB was chosen as 3.315. The major reason for the assignment of these two values for  $r$  and  $z$  was to be able to compare our numerical solution with the semi-analytical results for the infinite flat plate case with Schach (39). Actually, the major variable choice in the entire program is  $D = 1/\alpha^2$ . Basically,  $D$  is a measure of how large the flow system is since rectangular mesh is being used, i.e., a measure of  $\Delta\phi$  and  $\phi$  total. The only concern is that  $\Delta\phi$  is not chosen too small. In that event,  $\phi$  total would be too small to satisfy the incoming and exiting flow boundary conditions.

$\Delta\phi$  is chosen too large, i.e.,  $\alpha$  chosen too large or  $D$  chosen too small, all that is lost is accuracy due to larger mesh spacings. For the coarse mesh infinite flat plate problem, the results of the numerical solution as well as the computer listing and final output can be found in Appendix D - "Computer Solutions/Listings." The solution to the  $r$  formulation (Fig. 20(a)) required 1098 calls of the subroutine used to solve the simultaneous nonlinear equation. The sum of the squares of the error to the exact solution was reduced to 0.00357 at the last iteration.

The final values for the coarse mesh solution ( $r, z$ ) were used to make initial guesses for the values for the fine mesh solution. The  $r$  solution required the simultaneous solution of 159 nonlinear algebraic equations. The  $z$  equation, again being explicit in  $z_0$ , resulted in 164 unknown values of  $z_0$ . The plot of the results from the computer program (details shown in Appendix D) are presented in Figure 24 in a print plot. The computer connected the nodal points with straight line segments. In general, there is very little difference between the fine mesh and coarse mesh solution. The fine mesh solution required the extended storage space option on the 1106 machine. The sum of the squares for the final  $r$  solution was reduced to 0.024 after approximately 1000 calls of the subroutine CALFUN used to solve the simultaneous nonlinear equations. For this case 1000 iterations were required to obtain a satisfactory  $z$  solution.

2. Finite plate. - As mentioned in Section VII, Discussions of Numerical Techniques, the finite plate formulation also contains  $z$  on the exiting jet surface (see Fig. 21(a)). As a result, the method of solution consisted of the following steps:

Initially, assumed values of  $z$  along GE were chosen. These values were used to compute an  $r$  solution. The computed  $r$  solution used 161 calls of the subroutine CALFUN to reduce the sum of the squares of the residuals at the nodal points to 0.00066. With this  $r$  solution, the linear iteration technique was used to calculate the complete  $z$  solution. Since the computed  $z$  solution resulted in refined approximations to the values of  $z$  along GE, changes could then be reflected in a new  $r$  computation.

For the finite disk case in which the ratio of the radius of the liquid jet to the radius of the disk was one-half, a second  $r$  calculation did not change when the  $z$  values were updated. A curve was faired through the calculated nodal points and is shown in Figure 25. Only two of the four available streamlines are shown in the figure. No attempt was made to refine the solution by completely doubling the number of vertical and horizontal grid lines. For this particular case, since no comparison with any existing analytical techniques existed, a more convenient value of 3.3 was chosen for  $K\phi$ . The value of  $D$  employed in the solution was 0.0138. The only specification along GE was that  $Z$  was set equal to 0.25. The computer listing as well as the calculated  $r$  and  $z$  values at each nodal point can be found in Appendix D.

The same method was used to numerically compute the finite plate case in which the ratio of the jet diameter to the disk diameter was three-fourths. There were 38 nodal points required for the  $r$  solution and 45 for the  $z$  solution. A complete print-plot of the results is shown in Figure 26. Two iterations were required for the  $z$  solution as well as for the  $r$  solution. The sum of the squares for the

$r$  solution at the final iteration was 0.001. The computer listing and printout can be found in Appendix D. Again, the value of  $K\phi$  was arbitrarily chosen as 3.3.

The  $z$  solution corresponding to the  $r$  solution was obtained and is also presented in Appendix D along with its complete computer listing. The method applied to obtain the solution was a simple linear iteration technique since equations explicit in  $Z_0$  can be derived both in the interior and along the boundary points. There were 249 iterations required for the  $Z$  solution. Changes between the 248th and 249th iteration occurred in the fifth decimal point.

A physical plane description of the infinite flat plate solution is presented in Figure 23. Only two of the four internal streamlines are shown in the figure. Curves were faired through the available calculated nodal points  $(r,z)$  by a best fit process. There appeared, at the onset, the question of whether or not the coarse mesh employed could sufficiently describe the flow. When applying boundary conditions at the free surface, a larger number of nodal points are desirable. As a result, the existing mesh was doubled. The total  $\psi$  was divided up into ten equal parts such that  $a = \Delta\psi = 0.05$ , and the total  $\phi$  was divided up into 16 equal parts.

#### B. Surface Tension Dominated Model

As previously mentioned, the  $r$  formulation for the surface tension dominated flow can be solved independent of the  $z$  formulation (refer to Figs. 22(a) and (b)). The initial case examined had a Weber number of 4 and the ratio of the radius of the jet to the radius of the disk was one-half. Also, the first solution to this problem as-



sumed only axisymmetry. The results of the numerical solution, employing a coarse mesh, resulted in a symmetrical  $r$  solution; symmetrical about the equipotential line emanating from point D. This allowed us to make a simplification to the problem in that not only could axisymmetry be assumed, but also mirror image symmetry (i.e., symmetry about the  $z = 0$  plane). This is significant for problems in which the surface tension effects are to be taken into account since the surface tension forces are highly dependent on the curvature of the free surface. By taking advantage of the symmetry involved, additional nodal points can be placed on the free surface without using extended computer storage.

Referring now to Figure 22(a), a vertical line was drawn (equipotential line) emanating from point D, where  $r = RD$ .  $RD$  is the dimensionless disk radius. The intersection of this equipotential line with the free surface AG was defined as point M. Along DM, it is known that  $z = 0$ . In addition, the variation of  $r$  with  $\psi$  can be computed. Let us now refer to Figure 27 in which the equipotential line DM is depicted. Since DM is an equipotential line, the velocity along this line must be equal to  $V$ , the incoming jet velocity with the exception of the point  $r = L$  in the physical plane. At point D, a velocity discontinuity will exist. However, we can specify how  $r$  varies with  $\psi$  along this line as follows:

In the physical plane,

On DM

$$u = 0 \quad \text{on } z = 0, L \leq r \leq R_{\max} \quad (140)$$

$$v = -V$$

where  $R_{\max}$  is the maximum radius of the liquid flow pattern.

An expression for the stream function along DM can now be derived since the radial velocity component along DM is 0, we have

$$0 = -\frac{1}{r} \frac{\partial \psi}{\partial z} \quad (141)$$

This implies that  $\psi = \psi(r)$  alone. In order to find what the function is, the definition of the axial velocity is employed, namely,

$v = (1/r)(\partial \psi / \partial r)$ , on DM

$$-v = \frac{1}{r} \frac{\partial \psi}{\partial r} \quad (142)$$

Integrating this

$$\psi = -\frac{vr^2}{2} + \text{Constant} \quad (143)$$

Applying the boundary condition that  $\psi = 0$  at  $r = L$ , the constant in (143) can be calculated. The following expression results,

$$\psi = -\frac{vr^2}{2} + \frac{vL^2}{2} \quad (144)$$

If this equation is nondimensionalized,

$$\psi^* = \frac{r^{*2}}{2} - \frac{1}{2} \left( \frac{L}{R_o} \right)^2 \quad (145)$$

As we have done in the past derivations, the starred notation is dropped.

$$\psi = \frac{r^2}{2} - \frac{1}{2} \left( \frac{L}{R_o} \right)^2 \quad (146)$$

Solving for  $r$ ,

$$r = +\sqrt{2\psi + (RD)^2} \quad (147)$$

where

$$\frac{L}{R_o} = RD \quad (148)$$

Equation (147) represents the boundary condition employed along DM in the inverse plane for the  $r$  formulation. The condition  $z = 0$  was used for the  $z$  formulation.

In the course of finding the solution to the  $z$  formulation, depicted in Figure 22(b), it was necessary to solve a cubic equation for the parameter  $T$  along the free surface. Physical as well as mathematical interpretation was required when choosing the proper root of the cubic since a possibility of three real roots existed. Referring to equation (C-78) in Appendix C, the only mathematically meaningful roots are those in which the absolute value of the parameter  $T$  was greater than or equal to one. However, the possibility still existed that all three roots would be real and in addition satisfy the requirement that their absolute values were greater than one. As a result, some physical insight was required when deciding upon which roots to employ in the equation relating  $T$  to the fictitious point  $f$ , (eq. (C-84)). For example, it is known that as the nozzle exit is approached along the free surface,  $z = f(r)$  becomes steeper (i.e.,  $f'(r)$  approaches infinity). This would coincide with the curvature terms dropping out of the boundary condition in the physical plane formulation. An alternate approach to viewing this is that the fictitious point  $f$  approaches the image point  $z_4$ . As a result, the value of the parameter  $T$  approaches unity. The algorithm selected for choosing the proper root of the cubic was to select the value of  $T$  closest to unity but ensuring that its absolute value was greater than or equal to one. During the course of finding the solution, problems in implementing this algorithm occurred, particularly when close to the nozzle, since the  $T$  values closest to one were slightly less than

one and were automatically discarded by the algorithm. The resulting potential lines and streamlines appeared inaccurate when plotted up. The only way found to circumvent this problem was to set up an additional algorithm which set  $T$  identically equal to one for several free surface nodal points in the vicinity of the nozzle (i.e., those nodal points in which the computed  $r$  value was  $\leq 1.00 N$ ). Physically, this reasoning is justified since it is known that  $f'(r)$  must approach infinity there.

The results of the numerical solution are indicated in Figure 28. The Weber number for this solution was 4 and the ratio of the radius of the liquid jet to the radius of the disk was  $1/2$ . A value of 3.5 was chosen for  $K\phi$ , and  $D$  was set equal to 0.0204. The computer listing can be found in Appendix D along with the computed  $r$  and  $z$  values for the nodal points. The sum of the squares for the  $r$  solution was  $0.77 \times 10^{-6}$  and since the  $r$  solution was independent of the  $z$  solution, a second iteration was unnecessary.

#### C. Discussion of Zero Gravity Results

The numerical solutions were compared with the available semi-analytical results of Schach (39) for the case of the infinite flat plate. The method employed by Schach is attributed to Trefftz. The method used by Schach did not appear readily extendable to more complicated geometrical flows and could not be employed to account for the effects of surface tension. In making the comparison between reference 39 and the numerical results, the fine mesh solution presented in Figure 24 was used. The results of the comparison for the infinite flat plate are shown in Figure 29. The symbols indicated in the figure were obtained from Figure 11 of Schach's paper by using an expandable

scale. As a result there is some unknown error associated with the process of taking the results from the reference. In any case, the agreement looks particularly well with the sole exception of the first  $r$  coordinate greater than unity. One final point with respect to the infinite flat plate solution concerns the extreme left coordinate in Figure 29, namely,  $r = 4$ ,  $z = 0.125$ . These two values are fixed by continuity, both in our numerical program and in the semi-analytical results of Schach. This result was obtained as follows; assuming constant density, the volumetric flow rate into the control volume at AB must balance the flow out of the control volume at GE. In physical coordinates, the flow is given as  $\pi R_o^2 V$  and the flow out by  $2\pi R_{jet} z_G V$ . Equating these and cancelling leads to the fact that  $z_G$  must equal  $R_o^2 / (2R_{jet})$ . Nondimensionalizing with respect to  $R_o$  yields

$$z_G^* = \frac{1}{2R_{jet}^*} \quad (149)$$

Dropping the starred notation and observing that  $R_{jet} = 4$  at the left boundary of the control volume shows that  $z_o$  must equal  $1/8$ .

As far as the finite plate is concerned, there was no available comparisons with past experimental or analytical work. As a result, comparisons were made with respect to our own zero gravity experimental data. The results are shown in dimensionless coordinates in Figures 30 and 31. Figure 30 is for the case where the ratio of the jet radius to the disk radius is one-half and Figure 31 indicates the comparison when the ratio of the jet radius to the disk radius is three-fourths. The comparisons were made with respect to the outer or top free surface since it was impossible to view the lower free surface

because of the way in which the flow occurred. The results were generally good for both ratios compared. Experimental data points were obtained from both sides of the axisymmetric sheet as it flowed around the disk. An averaging procedure was subsequently used to plot the continuous lines indicated in Figures 30 and 31. The analysis corroborated the experiments in the sense that as the ratio ( $R_0/L$ ) becomes smaller, the jet appears to leave the disk more tangentially.

## IX. NORMAL GRAVITY EXPERIMENT SECTION

### A. Apparatus and Procedure

1. Experiment. - The experimental test rig used to obtain the normal gravity data is shown in Figures 32(a) and (b). The rig consisted of an angle-iron frame in which was mounted a 10 gallon supply tank, a settling chamber, a 56 gallon catch basin, a return pump, a control box, a clock, sequence timers, a regulator, and a supply tank. The major functions were controlled through the control box. A high-speed Mitchell Monitor motion picture camera (nominal speed 400 frames/sec) was located directly in front of the experimental test rig. The camera was mounted on a Wollensak camera stand which was fastened to a concrete floor by means of conduit clamps.

The experiment could be conducted in either a pressurized or non-pressurized mode (gravity-feed). To operate in the pressurized mode, two vent valves located above the supply tank were closed and the system was pressurized through the regulator. The pressure level was recorded on the gage located immediately to the right of the regulator as shown in Figure 32(a). For both modes, the return pump was used to resupply liquid to the supply tank in order to maintain a nearly constant level of liquid. Since the supply tank was fabricated from stainless steel and provided no visible means for monitoring liquid level, attempts were made to connect a plastic hose between the needle valve located just upstream of the solenoid valve and the side of the supply tank. This system was generally inaccurate and as a rule the

return pump was normally activated after completing two or three test runs.

In order to maintain a circular liquid jet having an initially uniform velocity profile, a settling chamber was designed to quiet the incoming flow. A similar technique was employed by Donnelly et al. (11) in their study of liquid jet stability. The settling chamber, Fig. 33, was fabricated from stainless-steel and had a 30° tapered approach to a circular hole in order to prevent boundary layer buildup. A total angle of 60° was employed in order to ensure a nearly uniform velocity profile at the exit to the settling chamber. Three settling chambers were employed having outlet diameters of 0.25, 0.50, and 1.0 centimeters. Problems developed when using an unbaﬄed settling chamber in that the entire flow developed a swirling action between 2 and 10 seconds after flow was initiated. In order to circumvent the swirling problem, the cylindrical section of the settling chamber was fitted with a  $1\frac{3}{4}$  inch honeycomb spacer. A sixteen mesh stainless steel screen was mounted below the first screen and both screens were butted up against the bottom of the spacer. This technique seemed to eliminate any noticeable swirl in the flow.

Sharp-edged disks, fabricated from stainless steel, were mounted below the settling chamber and positioned at right angles to the impinging liquid jet. A photograph of the disks employed in the study is shown in Figure 34. Their diameters ranged from 1 to 4 centimeters. The disks were mounted onto a stainless steel device capable of being adjusted at any angle to the incoming flow. However, in this study the impingement was restricted to 90°.

2. Test liquids. - Two test liquids were employed, anhydrous



ethanol and distilled water. Their properties at 20° C are listed in Table 1. No attempt was made to correct these fluid properties for temperature changes.

3. Test procedure. - Prior to a test run the settling chamber was filled with the test liquid by opening the solenoid valve while holding the bottom of the settling chamber closed. The liquid completely filled the settling chamber until it flowed out of the relief screw. At that point, the relief screw was closed and the outlet could be opened without loss of liquid from the settling chamber since it was a stable pressure supported system. This method worked when using distilled water for all the nozzle openings. It did not work for anhydrous ethanol in conjunction with the largest or 1 centimeter diameter opening. As a result, for those tests, the nozzle opening was kept sealed until the solenoid was opened at the start of each test.

Calibration tests were made prior to every series of test runs. Electrical sequence times in the control box were used along with graduated cylinders to determine the volumetric flow rate. At least three calibration tests were made before each series of runs, and an average value for the flow rate was thus determined. The impingement velocity (velocity at the disk) was calculated by correcting for the effect of gravitational forces.

## B. Results

1. Steady-state flow patterns. - Basically, two types of flow patterns were observed in the course of normal gravity liquid jet impingement. The first type occurred when a very high speed jet impinged upon a solid surface and spread out radially as a thin sheet. The sheet became thinner until it became unstable and broke up into

small liquid droplets. A second pattern is shown schematically in Figure 35. No breakup was observed in this pattern; the jet curved upon itself to form a surface of revolution or plume. The incoming jet velocity is  $V$  and the radius of the circular liquid jet is  $R_0$ . The disk radius is denoted as  $L$  while  $H$  is the distance between the nozzle and the disk. The maximum radius that the plume possessed is denoted as  $R_p$ . The maximum plume radius was the primary experimental variable for the normal gravity study since it was easily measurable and characteristic of the entire flow pattern. For the case when the plume was not visibly disturbed, the plume would slowly move to a final  $R_p$ , with visible surface ripples.

2. Unstable jumps. - In attempting to obtain steady-state impingement profiles, an unusual phenomenon was discovered. Instead of a single steady-state flow pattern, a number of unstable flow patterns were observed prior to the attaining of a stable steady state. Typically, the jet impinged upon the solid and formed a plume of some given radius with surface ripples present. If disturbed, either upstream or downstream of the plume, the jet would jump to another apparently stable configuration of larger plume radius. Normally, only one jump would occur in a single test run, but occasionally two jumps or three apparently stable configurations were observed. A series of tests indicating the flow patterns before and after a jump are shown in Figure 36. Figures 36(a), (c), and (e) illustrate the behavior before the respective jumps, while Figures 36(b), (d), and (f) occur after the jumps. The plume size for the final configurations appear to be nearly double what they were initially. However, there does not appear to be any correlation between initial and final size. The jumps

are natural in occurrence, such as when a small liquid droplet rebounds off the disk holder and impinges upon this film, but can be initiated by a disturbance, such as a pencil penetrating the flow. The final steady-state configuration is stable to any additional disturbances, i.e., it remains at some fixed plume shape. Under no circumstances was the plume observed to jump to a smaller plume configuration; all jumps were to larger plume sizes.

The actual cause of these jumps remains unanswered at this writing. Some possible causes have been eliminated, such as swirling flow. If the flow were swirling, the steady-state flow patterns would be significantly affected if half the flow over the disk was obstructed. However, the pattern was not affected at all when this was done. It is tentatively concluded that the jumps are natural in occurrence. The initial states and all transition states are unstable to small disturbances. For the purpose of the experimental investigation, then, the steady-state was chosen as the state in which further disturbances caused no change in the liquid flow pattern.

3. Experimental data. - The experimental runs were conducted such that the viscous dependence would be small. As shown in section III, depending upon the ratio ( $R_0/L$ ), there exists a critical Reynolds number above which the flow can be considered as essentially inviscid. The Reynolds number was calculated at the point of impingement on the disk (i.e., the approach velocity to the disk was corrected for gravitational effects). From analytical considerations, numerous dimensionless parameters arise and thus form the basis for correlating the primary variable, the plume size. These parameters include the Weber number, which is the ratio of inertial to surface tension forces, and

the Bond number, which is the ratio between gravitational and surface tension forces. In addition, several geometrical ratios appear, such as  $R_o/L$ , the ratio of jet to the disk radius, and  $H/R_o$ , the ratio of the nozzle height to the jet radius. The experimental results are listed in tabular form in Table 3. The last column contains the plume radius, nondimensionalized with respect to the jet radius. In examining the difference between zero and normal gravity liquid jet impingement, it can be seen that two additional parameters are required in order to completely define this phenomena in normal gravity. They are the Bond number,  $Bo$ , and the dimensionless nozzle height,  $H/R_o$ . The Bond number relates the relative contribution of gravitational forces, while  $H/R_o$  has an effect in that jets flowing downward under the effect of gravity accelerate and thus shrink in size, thereby having an effect on the resulting flow.

4. Data analysis. - A linear regression analysis was employed in order to correlate the independent variable,  $R_p/R_o$ , with the remaining system parameters. Let us define the following variables,

$$Y = \frac{R_p}{R_o} \quad (150)$$

$$Z_1 = \frac{R_o}{L} \quad (151)$$

$$Z_2 = \frac{H}{R_o} \quad (152)$$

$$Z_3 = We \quad (153)$$

$$Z_4 = Re \quad (154)$$

$$Z_5 = Bo \quad (155)$$

The parameter  $Z_4$ , the Reynolds number, was included to see what

the viscous influence was. The experimental data was fitted to the following complex model

$$\begin{aligned} \frac{R_p}{R_o} = & 22.8241 + 7.67129 X_1 - 41.2001 X_1^2 + 42.9330 X_1^3 + 1.91085 X_2 \\ & + 8.90368 X_3 + 1.46319 X_4 - 2.07823 X_5 + 0.0696939 X_2 X_5 \end{aligned} \quad (156)$$

where

$$X_1 = \frac{\frac{R_o}{L} - 0.371839}{0.154239} \quad (157)$$

$$X_2 = \frac{\frac{H}{R_o} - 9.22727}{7.19571} \quad (158)$$

$$X_3 = \frac{We - 129.227}{75.7108} \quad (159)$$

$$X_4 = \frac{Re - 4663.89}{1897.57} \quad (160)$$

$$X_5 = \frac{Bo - 2.15602}{1.12058} \quad (161)$$

The value of  $R^2$  for the above statistical model was 0.981. This means that 98.1 percent of the total variance in  $R_p/R_o$  is accounted for by the model. An examination of the signs in the equation for the complex model tells us how  $R_p/R_o$  varies with each of the parameters;  $R_p/R_o$  increases slightly as  $H/R_o$  and  $Re$  are increased, and increases significantly with  $X_3$ , the Weber number. Since  $X_5$  is involved in two terms in the correlation, its variation depends on the strongest term (i.e., the one with the largest coefficient). As a result,  $R_p/R_o$  decreases with increasing  $Bo$ . The variation with  $X_1$  is more confusing since it is involved in three terms. The actual data

bears this out,  $R_p/R_o$  sometimes increasing, or sometimes decreasing. The coefficient for  $X_3$  is essentially the largest of all ( $X_3$  is related to  $We$ ). As a result, a simpler model was pursued using only  $We$  as the independent variable. The following equation resulted;

$$\frac{R_p}{R_o} = 21.7059 + 10.1410 \frac{We - 129.227}{75.7108} \quad (162)$$

For this simple model  $R^2 = 0.916$ , which means that the correlation accounts for 91.6 percent of the variance in the data. A plot of the data is displayed in Figure 37.

The Weber number turns out to be the most statistically significant variable. This is not to say that the other variables are not significant, but that the Weber number is the most dominant variable in determining  $R_p/R_o$ .

## X. CONCLUSIONS

Zero gravity. - An experimental and analytical investigation was conducted to determine the free surface shape of circular liquid jets impinging normal to sharp-edged disks in zero gravity. The test liquids employed were anhydrous ethanol and trichlorotrifluoroethane. Jet radii were varied from 0.25 to 0.75 centimeter and disk radii of 1.0 and 1.5 centimeters were employed. The jet velocity was varied between 12 and 365 centimeters per second. Under the stipulation that the nozzle was located at least 5 centimeters from the disk, the investigation yielded the following results:

1. It was analytically determined that there exist flow regions where viscous forces are not significant when computing free surface shapes. It was shown that the Reynolds number  $\rho V R_0 / \mu$  and the ratio of jet to disk radius  $R_0 / L$  uniquely define the flow regions. It was further shown that the Reynolds number specifying the transition between viscous and nonviscous flow decreased with increasing jet to disk radius ratio.
2. Within the inviscid region, three distinct flow regimes were experimentally found which depend uniquely on the Weber number  $\rho V^2 R_0 / \sigma$  and the ratio of the jet to disk radius  $R_0 / L$ . These flows were defined as Surface Tension Flow, Transition Flow, and Inertia Flow. The critical Weber number between regimes was found to decrease with increasing jet to disk radius ratio.
3. A numerical solution yielding free surface shapes and stream-

lines was obtained for the case of impingement normal to an infinite flat plate and compared favorably with semi-analytical techniques in the literature.

4. A numerical solution yielding free surface shapes and streamlines was obtained for inertially dominated flows at ratios of jet to disk radius of one-half and three-fourths. The comparison with experiments showed good agreement for the upper free surface.

5. A surface tension dominated flow was formulated and solved numerically. The system Weber number was 4.0 and the ratio of the jet to the disk radius was one-half.

Normal gravity. - An experimental investigation was conducted to determine the characteristics of circular liquid jets impinging normal to a sharp-edged disk in normal gravity. The test liquids employed were distilled water and anhydrous ethanol. Jet radii between 0.125 and 0.50 centimeter were employed and the disk radii were varied between 0.5 and 2.0 centimeters. The jet velocity had the range of 75.5 to 484 centimeters per second. The distance between the nozzle and disk was varied between 0.25 and 5.0 centimeters. Under the stipulation that the Reynolds numbers were such that they exceeded the minimum value required to avoid viscous influence, the investigation yielded the following results:

1. The liquid flow pattern was observed to jump from one apparently stable flow pattern to another until a completely stable configuration was reached. The jumps were triggered by disturbances both upstream and downstream of the disk and were apparently natural in occurrence.

2. The dimensionless plume radius  $R_p/R_0$  was correlated by means



of a linear regression analysis. A simple model, employing only the Weber number, accounted for nearly 92 percent of the experimental data. The following empirical formula resulted

$$\frac{R_p}{R_o} = 21.7059 + 10.140 \frac{We - 129.227}{75.7108}$$

where  $R_p$  is the plume radius,  $R_o$  the nozzle radius, and  $We$  the system Weber number.

## XI, APPENDIXES

### Appendix A - Detailed Calculations of Free Surface Boundary Conditions

There are two boundary conditions required for the case of a free surface in a fluid dynamics problem. This is in comparison to known boundaries in which only one boundary condition is required. The two conditions to be satisfied are:

- (1) Conservation of energy along a streamline
- (2) The velocity normal to the streamline is zero.

Consider the following geometry:

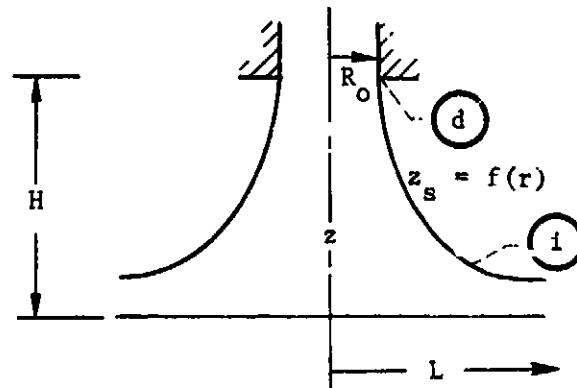


Figure A.1. - Schematic of Liquid Jet Impingement

where "i" represents any point on the free surface  $z_s = f(r)$  and "d" designates the reference point which is chosen as the point where the liquid jet exits from the nozzle.

- (1) Conservation of energy along a streamline

Bernoulli's equation written between points "i" and "d" becomes

$$\frac{1}{2} (u^2 + v^2) + \frac{P_i}{\rho} = \frac{1}{2} V^2 + \frac{P_d}{\rho} \quad \text{on } z_s = f(r) \quad (\text{A } 1)$$

The pressure at point 1,  $p_1$ , is not the same as it is at point d,  $p_d$ , due to the effects of surface tension. In general,

$$p_g - P = \sigma J \quad (A-2)$$

where  $p_g$  = known gas pressure, and

$$J = \frac{1}{R_1} + \frac{1}{R_2} \quad (A-3)$$

where  $R_1, R_2$  are radii of curvature where

$$\frac{1}{R_1} = \frac{f''}{(1 + f'^2)^{3/2}} \quad (A-4)$$

and

$$\frac{1}{R_2} = \frac{f'}{r(1 + f'^2)^{1/2}} \quad (A-5)$$

Combining (A-4) and (A-5) with (A-2) we find

$$p_g - P = \sigma \left[ \frac{f''}{(1 + f'^2)^{3/2}} + \frac{f'}{r(1 + f'^2)^{1/2}} \right] \quad (A-6)$$

which can be combined to yield,

$$p_g - P = \frac{\sigma}{r} \frac{d}{dr} \left( \frac{rf'}{\sqrt{1 + f'^2}} \right) \quad (A-7)$$

Applying at point "d"

$$z = H, \quad r = R_o, \quad \text{and} \quad \frac{df}{dr} = f' = \infty$$

For large  $f'$ ,

$$\sqrt{1 + f'^2} \doteq \sqrt{f'^2} = f'$$

Therefore, substitution into (A-7) yields

$$p_g - p_d = \frac{\sigma}{R_o} \quad (A-8)$$

Applying at point "1"

$$P_g - P_1 = \frac{\sigma}{r} \frac{d}{dr} \left( \frac{rf'}{\sqrt{1+f'^2}} \right) \quad (\text{A-9})$$

Now (A-8) and (A-9) can be substituted into (A-1) to obtain

$$\frac{1}{2} (u^2 + v^2) - \frac{\sigma}{\rho r} \frac{d}{dr} \left( \frac{rf'}{\sqrt{1+f'^2}} \right) = \frac{1}{2} v^2 - \frac{\sigma}{\rho R_o} \quad \text{on } z_s = f(r) \quad (\text{A-10})$$

(2) The velocity normal to the free surface is zero

A portion of the free surface  $z_s = f(r)$  is shown in Figure A.2

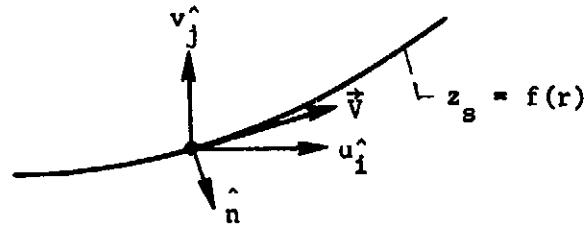


Figure A.2. - Velocity Vector at Free Surface

$\hat{n}$  is the unit outward normal to the surface at some point and  $u$  and  $v$  are the velocity components such that  $\vec{V} = u\hat{i} + v\hat{j}$ . Since the velocity normal to the surface is zero

$$\vec{V} \cdot \hat{n} = 0 \quad (\text{A-11})$$

With the surface given by  $z_s = f(r)$ , the unit normal is given as

$$\hat{n} = \frac{-f'\hat{i} + \hat{j}}{\sqrt{1+f'^2}} \quad (\text{A-12})$$

Hence

$$\vec{V} \cdot \hat{n} = -\frac{uf'}{\sqrt{1+f'^2}} + \frac{v}{\sqrt{1+f'^2}} = 0 \quad (\text{A-13})$$

which simplifies to

$$-uf' + v = 0 \quad \text{on } z_s = f(r) \quad (\text{A-14})$$

## Appendix B - Zero Gravity Drop Tower Test Facility

The experimental data for this study were obtained in the Lewis Research Center's 2.2-Second Zero Gravity Facility. A schematic diagram of this facility is shown in Figure B.1. The facility consists of a building 6.4 meters square by 30.5 meters tall. Contained within the building is a drop area 27 meters long with a cross section 1.5 by 2.75 meters.

The service building has a shop and service area, a calibration room, and a controlled environment room. Those components of the experiment that required special handling were prepared in the controlled environment room of the facility. This air-conditioned and filtered room (shown in Fig. B.2) contains an ultrasonic cleaning system and the laboratory equipment necessary for handling test liquids.

Mode of operation - A 2.2-second period of weightlessness is obtained by allowing the experiment package to free fall from the top of the drop area. In order to minimize drag on the experiment package, it is enclosed in a drag shield designed with a high ratio of weight to frontal area and a low drag coefficient. The relative motion of the experiment package with respect to the drag shield during a test is shown in Figure B.3. Throughout the test, the experiment package and drag shield fall freely and independently of each other; that is, no guide wires, electrical lines, etc., are connected to either. Therefore, the only force acting on the freely falling experiment package

is the air drag associated with the relative motion of the package within the enclosure of the drag shield. This air drag results in an equivalent gravitational acceleration acting on the experiment, which is estimated to be below  $10^{-5}$  g's.

Release system. - The experiment package, installed within the drag shield, is suspended at the top of the drop area by means of a highly stressed music wire attached to the release system. This release system consists of a double-acting air cylinder with a hard-steel knife edge attached to the piston. Pressurization of the air cylinder drives the knife edge against the wire, which is backed by an anvil. The resulting notch causes the wire to fail, smoothly releasing the experiment. No measurable disturbances are imparted to the package by this release procedure.

Recovery system. - After the experiment package and drag shield have traversed the total length of the drop area, they are recovered by deceleration in a 2.2-meter-deep container filled with sand. The deceleration rate (averaging 15 g's) is controlled by selectively varying the tips of the deceleration spikes mounted on the bottom of the drag shield (Fig. B.1). At the time of impact of the drag shield in the decelerator container, the experiment package has traversed the vertical distance within the drag shield (compare Figs. B3(a) and (c)).

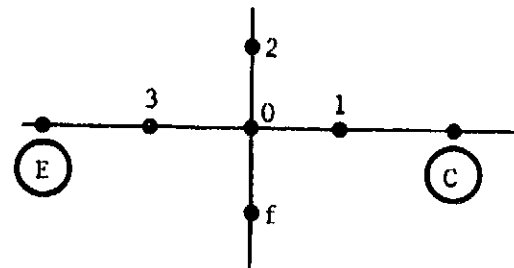
## Appendix C - Detailed Derivations of Finite Difference

### Operators Along Boundaries

#### A. Infinite Flat Plate

The finite difference representations for the derivatives are those shown in the text (eqs. (123) to (130)). Refer to Figures 15(a) and (b).

$$\underline{\frac{\partial r}{\partial \psi} = 0 \text{ on EC}}$$



Applying the  $r$  difference equation (eq. (131)) at point 0, where  $f$  is a fictitious point outside boundary

$$\begin{aligned} r_o^4 - \frac{r_o^3}{2} (r_2 + r_f) + r_o^2 \left[ \frac{1}{\alpha^2} - \frac{1}{8} (r_2 - r_f)^2 \right] - \frac{r_o}{2\alpha^2} (r_1 + r_3) \\ + \frac{1}{8\alpha^2} (r_1 - r_3)^2 = 0 \end{aligned} \quad (C-1)$$

Along EC,  $\frac{\partial r}{\partial \psi} = 0$ . This implies

$$\frac{r_2 - r_f}{2 \Delta \psi} = 0 \quad (C-2)$$

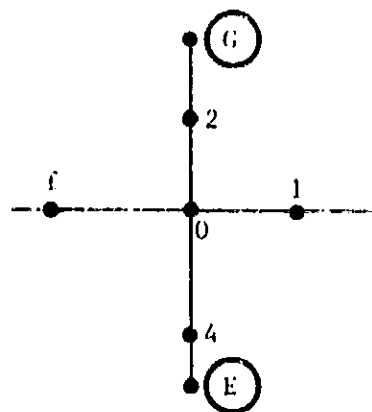
Therefore,

$$r_2 = r_f \quad (C-3)$$

Equation (C-1) becomes

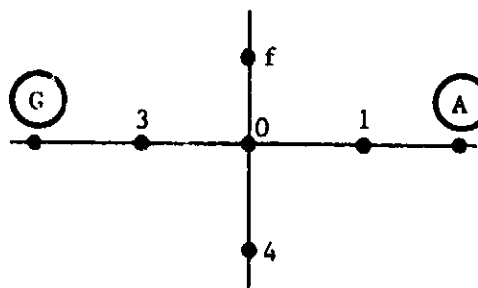
$$r_0^4 - r_0^3 r_2 + r_0^2 \frac{1}{2} - \frac{r_0}{2^2} (r_1 + r_3) + \frac{1}{8\alpha^2} (r_1 - r_3)^2 = 0 \quad (C-4)$$

$$\frac{\partial r}{\partial \psi} = 0 \quad \text{on} \quad GE$$



Application of  $\partial r / \partial \psi$  on GE yields the fact that  $r_2 = r_4$  and does not involve the unknown fictitious point f. However,  $\partial r / \partial \psi = 0$  implies  $r \neq r(\psi)$ . Therefore, r must only be a function of  $\phi$ ,  $r = r(\phi)$ . But, along GE,  $\phi = \text{constant}$ , ( $\phi = 0$ ). Hence,  $r = \text{constant}$  along GE.

$$\left(\frac{\partial r}{\partial \phi}\right)^2 + r^2 \left(\frac{\partial r}{\partial \psi}\right)^2 = 1 \quad \text{on} \quad AG$$



The  $r$  difference equation can be written



$$r_o^4 - \frac{r_o^3}{2} (r_f + r_4) + r_o^2 \left[ \frac{1}{a^2} - \frac{1}{8} (r_f - r_4)^2 \right] - \frac{r_o}{2a^2} (r_1 + r_3) + \frac{1}{8a^2} (r_1 - r_3)^2 = 0 \quad (C-5)$$

Along AC

$$\left( \frac{\partial r}{\partial \phi} \right)^2 + r^2 \left( \frac{\partial r}{\partial \psi} \right)^2 = 1$$

This implies

$$\left( \frac{r_1 - r_3}{2 \Delta \phi} \right)^2 + r_o^2 \left( \frac{r_f - r_4}{2 \Delta \psi} \right)^2 = 1 \quad (C-6)$$

Rearranging and letting  $\Delta \psi = a$  (recalling  $a = \Delta r / \Delta \psi$ )

$$(r_f - r_4)^2 = \frac{1}{r_o^2} \left[ 4a^2 - \frac{1}{a^2} (r_1 - r_3)^2 \right] \quad (C-7)$$

Whereupon we can calculate the two expressions

$$r_f - r_4 = \frac{1}{r_o} \sqrt{\left[ 4a^2 - \frac{1}{a^2} (r_1 - r_3)^2 \right]} \quad (C-8)$$

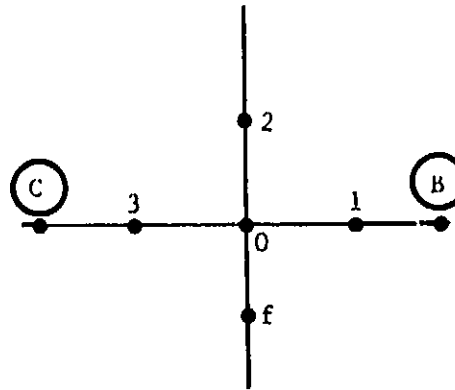
$$r_f + r_4 = \frac{1}{r_o} \sqrt{\left[ 4a^2 - \frac{1}{a^2} (r_1 - r_3)^2 \right]} + 2r_4 \quad (C-9)$$

Inserting (C-8) and (C-9) into (C-5) yields the desired relation

$$r_o^4 - r_o^3 r_4 + r_o^2 \left\{ \frac{1}{a^2} - \frac{1}{2} \sqrt{\left[ 4a^2 - \frac{1}{a^2} (r_1 - r_3)^2 \right]} \right\} - \frac{r_o}{2a^2} (r_1 + r_3) + \frac{1}{8} \left[ \frac{2}{a^2} (r_1 - r_3)^2 - 4a^2 \right] = 0 \quad (C-10)$$

$z = \text{Constant}$  on AB, let  $z = R_0$ .

$$\underline{\frac{\partial z}{\partial \phi} = 0 \text{ on BC}}$$



Applying the  $z$  difference equation (eq. (132)) at point 0, where  $f$  is a fictitious point outside of boundary

$$z_0 = -\frac{r_o^2}{2\left(r_o^2 + \frac{1}{\alpha^2}\right)} (z_2 + z_f) + \frac{1}{2\left(r_o^2 + 1\right)} (z_1 + z_3) + \frac{1}{4\left(r_o^2 + \frac{1}{\alpha^2}\right)} (z_2 - z_f)(z_1 - z_3) \quad (C-11)$$

Along BC,  $\frac{\partial z}{\partial \psi} = 0$ . This implies

$$z_2 - z_f = 0$$

or

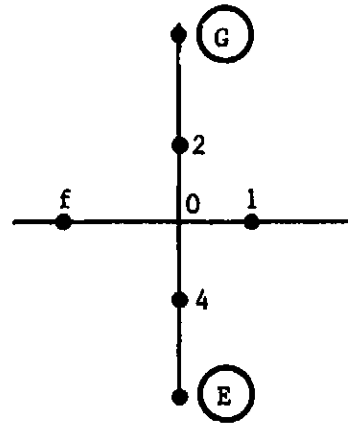
$$z_f = z_2 \quad (C-12)$$

Therefore, equation (C-11) becomes

$$z_0 = \frac{r_o^2 z_2}{r_o^2 + \frac{1}{\alpha^2}} + \frac{1}{2\left(r_o^2 + 1\right)} (z_1 + z_3) \quad (C-13)$$

$$\frac{\partial z}{\partial \phi} = 0 \text{ on GE}$$


---



The  $z$  difference equation can be written

$$z_o = \frac{r_o^2}{2\left(r_o^2 + \frac{1}{\alpha^2}\right)} (z_2 + z_4) + \frac{1}{2\left(r_o^2 \alpha^2 + 1\right)} (z_1 + z_f) + \frac{1}{4\left(r_o^2 \alpha + \frac{1}{\alpha}\right)} (z_2 - z_4)(z_1 - z_f) \quad (C-14)$$

Along GE,  $\frac{\partial z}{\partial \phi} = 0$  this implies  $z_1 - z_f = 0$  or

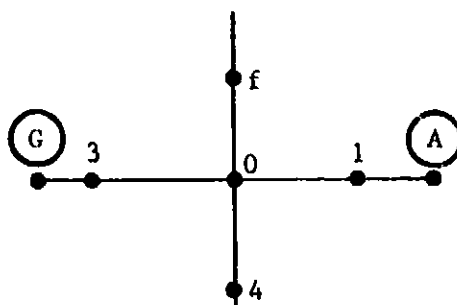
$$z_f = z_1 \quad (C-15)$$

Therefore, equation (C-14) becomes

$$z_o = \frac{r_o^2}{2\left(r_o^2 + \frac{1}{\alpha^2}\right)} (z_2 + z_4) + \frac{z_1}{r_o^2 \alpha^2 + 1} \quad (C-16)$$

$$r^2 \left( \frac{\partial z}{\partial \psi} \right)^2 + \left( \frac{\partial z}{\partial \phi} \right)^2 = 1 \text{ on GA}$$


---



The  $z$  difference equation can be written

$$z_o = \frac{r_o^2}{2\left(r_o^2 + \frac{1}{\alpha^2}\right)} (z_f - z_4) + \frac{1}{2\left(r_o^2 \alpha^2 + 1\right)} (z_1 + z_3) + \frac{1}{4\left(r_o^2 \alpha^2 + \frac{1}{\alpha}\right)} (z_f - z_4)(z_1 - z_3) \quad (C-17)$$

Along AG,  $r^2 \left(\frac{\partial z}{\partial \psi}\right)^2 + \left(\frac{\partial z}{\partial \phi}\right)^2 = 1$ . Hence,

$$r_o^2 \left(\frac{z_f - z_4}{2 \Delta \psi}\right)^2 + \left(\frac{z_1 - z_3}{2 \Delta \phi}\right)^2 = 1 \quad (C-18)$$

which can be expressed as

$$(z_f - z_4)^2 = \frac{1}{r_o^2} \left[ 4a^2 - \frac{1}{\alpha^2} (z_1 - z_3)^2 \right] \quad (C-19)$$

This yields the two relations,

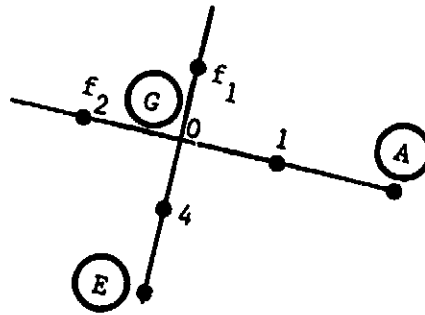
$$z_f - z_4 = \frac{1}{r_o} \sqrt{\left[ 4a^2 - \frac{1}{\alpha^2} (z_1 - z_3)^2 \right]} \quad (C-20)$$

$$z_f + z_4 = \frac{1}{r_o} \sqrt{\left[ 4a^2 - \frac{1}{\alpha^2} (z_1 - z_3)^2 \right]} + 2z_4 \quad (C-21)$$

Inserting these last two equations in (C-17) eliminates the fictitious point  $z_f$ , yielding

$$z_0 = \frac{r_0^2}{2\left(r_0^2 + \frac{1}{\alpha^2}\right)} \left\{ \frac{1}{r_0} \sqrt{\left[4a^2 - \frac{1}{\alpha^2} (z_1 - z_3)^2\right]} + 2z_4 \right\} \\ + \frac{1}{2\left(r_0^2 \alpha^2 + 1\right)} (z_1 + z_3) \\ + \frac{z_1 - z_3}{4r_0\left(r_0^2 \alpha^2 + \frac{1}{\alpha}\right)} \sqrt{\left[4a^2 - \frac{1}{\alpha^2} (z_1 - z_3)^2\right]} \quad (C-22)$$

A special boundary condition is required for point G since it is a part of two separate boundaries



Applying the  $z$  difference equation,

$$z_0 = \frac{r_0^2}{2\left(r_0^2 + \frac{1}{\alpha^2}\right)} (f_1 + z_4) + \frac{1}{2\left(r_0^2 \alpha^2 + 1\right)} (z_1 + f_2) \\ + \frac{1}{4\left(r_0^2 \alpha^2 + \frac{1}{\alpha}\right)} (f_1 - z_4)(z_1 - f_2) \quad (C-23)$$

Applying the boundary condition along GE, namely  $\frac{\partial z}{\partial \phi} = 0$ , it is found that  $f_2 = z_1$ . Therefore, we write

$$z_o = \frac{r_o^2}{2\left(r_o^2 + \frac{1}{a^2}\right)} (f_1 + z_4) + \frac{z_1}{r_o^2 a^2 + 1} \quad (C-24)$$

Applying the boundary condition along AG (see eq. (C-20))

$$f_1 = z_4 + \frac{1}{r_o} \sqrt{\left[4a^2 - \frac{1}{a^2} (z_1 - f_2)^2\right]} \quad (C-25)$$

but  $f_2 = z_1$ , hence we write

$$f_1 = z_4 + \frac{2a}{r_o} \quad (C-26)$$

Equation (C-23) becomes

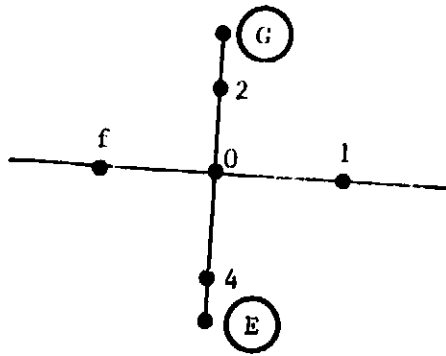
$$z_o = \frac{r_o \left(z_4 + \frac{a}{r_o}\right)}{r_o^2 + \frac{1}{a^2}} + \frac{z_1}{r_o^2 a^2 + 1} \quad (C-27)$$

such that  $z_o = z_o(z_1, z_4)$  at point G.

#### B. Finite Plate

Referring to Figures 16(a) and (b), the changes in the boundary conditions between the infinite and finite plate occur on GE and the addition of the free surface ED. In addition, G becomes a special point in the  $r$  formulation while both G and E become special points in the  $z$  formulation.

$$\underline{\left(\frac{\partial r}{\partial \phi}\right) + r \left(\frac{\partial r}{\partial \psi}\right) \left(\frac{dz}{dr}\right) = 0 \text{ on GE}}$$



Along GE, the  $r$  difference equation is

$$r_o^4 - \frac{r_o^3}{2} (r_2 + r_4) + r_o^2 \left[ \frac{1}{\alpha^2} - \frac{1}{8} (r_2 - r_4)^2 \right] - \frac{r_o}{2\alpha^2} (r_1 + f) + \frac{1}{8\alpha^2} (r_1 - f)^2 = 0 \quad (C-28)$$

in finite difference form, the boundary condition is,

$$\frac{r_1 - f}{\Delta\phi} + \frac{r_o}{\Delta\psi} (z_2 - z_4) = 0 \quad (C-29)$$

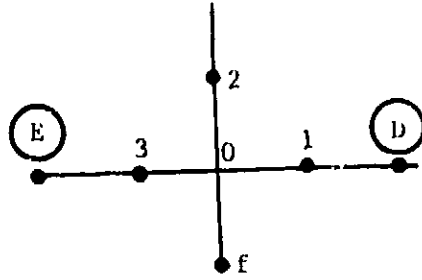
solving for  $f$ ,

$$f = r_1 + \alpha r_o (z_2 - z_4) \quad (C-30)$$

and, inserting this into the  $r$  difference equation yields the desired result.

$$r_o^4 - \frac{r_o^3}{2} (r_2 + r_4) + r_o^2 \left[ \frac{1}{\alpha^2} - \frac{1}{8} (r_2 - r_4)^2 \right] - \frac{r_o}{2\alpha^2} [2r_1 + \alpha r_o (z_2 - z_4)] + \frac{r_o^2}{8} (z_2 - z_4)^2 = 0 \quad (C-31)$$

$$\left( \frac{\partial r}{\partial \phi} \right)^2 + r^2 \left( \frac{\partial r}{\partial \psi} \right)^2 = 1 \quad \text{on ED}$$



The  $r$  difference equation can be written

$$r_o^4 - \frac{r_o^3}{2} (r_2 + r_f) + r_o^2 \left[ \frac{1}{\alpha^2} - \frac{1}{8} (r_2 - r_f)^2 \right] - \frac{r_o}{2\alpha^2} (r_1 + r_3) + \frac{1}{8\alpha^2} (r_1 - r_3)^2 = 0 \quad (C-32)$$

Using  $\left(\frac{\partial r}{\partial \phi}\right)^2 + r^2 \left(\frac{\partial r}{\partial \psi}\right)^2 = 1$  on ED,

$$\left(\frac{r_1 - r_3}{2 \Delta \phi}\right)^2 + r_o^2 \left(\frac{r_2 - r_f}{2 \Delta \psi}\right)^2 = 1 \quad (C-33)$$

Yields

$$(r_2 - r_f)^2 = \frac{1}{r_o^2} \left[ 4a^2 - \frac{1}{\alpha^2} (r_1 - r_3)^2 \right] \quad (C-34)$$

and

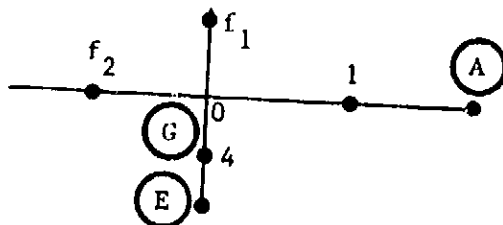
$$r_2 + r_f = 2r_2 - \frac{1}{r_o} \sqrt{\left[ 4a^2 - \frac{1}{\alpha^2} (r_1 - r_3)^2 \right]} \quad (C-35)$$

Substituting (C-34) and (C-35) into (C-32) we obtain

$$r_o^4 - r_o^3 r_2 + r_o^2 \left\{ \frac{1}{\alpha^2} + \frac{1}{2} \sqrt{\left[ 4a^2 - \frac{1}{\alpha^2} (r_1 - r_3)^2 \right]} \right\} - \frac{r_o}{2\alpha^2} (r_1 + r_3) + \frac{1}{8} \left[ -4a^2 + \frac{2}{\alpha^2} (r_1 - r_3)^2 \right] = 0 \quad (C-36)$$



Now, points E and G will be special points since equation (C-31) cannot be directly applied there. One of these positions can be specified as known,  $r_E = \text{constant}$ . Let us examine special point G



Applying equation (C-10) at point G,

$$r_o^4 - r_o^3 r_4 + r_o^2 \left\{ \frac{1}{\alpha^2} - \frac{1}{2} \sqrt{4a^2 - \frac{1}{\alpha^2} (r_1 - f_2)^2} \right\} - \frac{r_o}{2\alpha^2} (r_1 + f_2) + \frac{1}{8} \left[ \frac{2}{\alpha^2} (r_1 - f_2)^2 - 4a^2 \right] = 0 \quad (C-37)$$

Now, applying  $\left(\frac{\partial r}{\partial \phi}\right) + r \left(\frac{\partial r}{\partial \psi}\right) \left(\frac{dz}{dr}\right) = 0$  along GE without involving  $f_1$ ,

$$\left(\frac{r_1 - f_2}{2 \Delta \phi}\right) + r_o \left(\frac{r_o - r_4}{\Delta \psi}\right) \left(\frac{z_o - z_4}{r_o - r_4}\right) = 0 \quad (C-38)$$

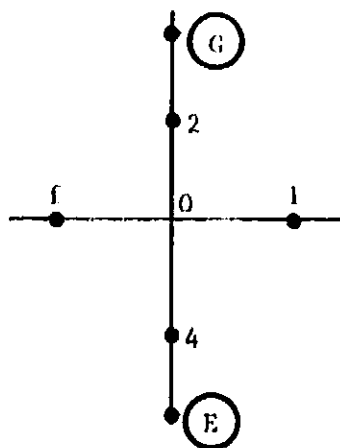
Solving for  $f_2$ ,

$$f_2 = r_1 + 2\alpha r_o (z_o - z_4) \quad (C-39)$$

Therefore, equation (C-37) becomes

$$r_o^4 - r_o^3 r_4 + r_o^2 \left\{ \frac{1}{\alpha^2} - \sqrt{a^2 - r_o^2 (z_o - z_4)^2} \right\} - \frac{r_o}{\alpha^2} [r_1 + \alpha r_o (z_o - z_4)] + \left[ r_o^2 (z_o - z_4)^2 - \frac{a^2}{2} \right] = 0 \quad (C-40)$$

$$\underline{r \left(\frac{\partial z}{\partial \phi}\right) - \left(\frac{\partial z}{\partial \phi}\right) \left(\frac{dz}{dr}\right) = 0 \text{ on GE}}$$



Application of  $z$  difference equation yields,

$$z_o = \frac{r_o^2}{2\left(r_o^2 + \frac{1}{\alpha^2}\right)} (z_2 + z_4) + \frac{z_1 + f}{2(r_o^2 \alpha^2 + 1)} + \frac{(z_2 - z_4)(z_1 - f)}{4\left(r_o^2 \alpha + \frac{1}{\alpha}\right)} \quad (C-41)$$

Now, along GE,  $r\left(\frac{\partial z}{\partial \psi}\right) - \left(\frac{\partial z}{\partial \phi}\right)\left(\frac{dz}{dr}\right) = 0$ , which in difference form can be written,

$$r_o \left( \frac{z_2 - z_4}{2 \Delta \psi} \right) - \left( \frac{z_1 - f}{2 \Delta \phi} \right) \left( \frac{z_2 - z_4}{r_2 - r_4} \right) = 0 \quad (C-42)$$

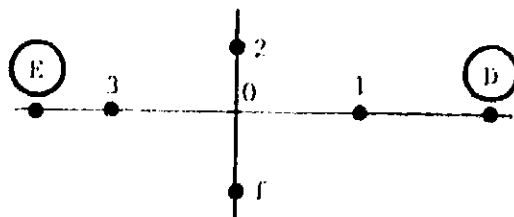
Solving for  $f$ ,

$$f = z_1 - r_o \alpha (r_2 - r_4) \quad (C-43)$$

Hence, equation (C-41) becomes

$$z_o = \frac{r_o^2}{2\left(r_o^2 + \frac{1}{\alpha^2}\right)} (z_2 + z_4) + \frac{2z_1 - r_o \alpha (r_2 - r_4)}{2(r_o^2 \alpha^2 + 1)} + \frac{(z_2 - z_4)[r_o \alpha (r_2 - r_4)]}{4\left(r_o^2 \alpha + \frac{1}{\alpha}\right)} \quad (C-44)$$

$$\underline{r^2 \left( \frac{\partial z}{\partial \psi} \right)^2 + \left( \frac{\partial z}{\partial \phi} \right)^2 = 1 \text{ on ED}}$$



The  $z$  difference equation can be written,

$$z_o = \frac{r_o^2}{2\left(r_o^2 + \frac{1}{a^2}\right)} (z_2 + z_f) + \frac{1}{2\left(r_o^2 + 1\right)} (z_1 + z_3) + \frac{1}{4\left(r_o^2 + \frac{1}{a}\right)} (z_2 - z_f)(z_1 - z_3) \quad (C-45)$$

Applying  $r^2\left(\frac{\partial z}{\partial \psi}\right)^2 + \left(\frac{\partial z}{\partial \phi}\right)^2 = 1$  on ED,

$$r_o^2 \left(\frac{z_2 - z_f}{2 \Delta \psi}\right)^2 + \left(\frac{z_1 - z_3}{2 \Delta \phi}\right)^2 = 1 \quad (C-46)$$

Solving for  $(z_2 - z_f)$ .

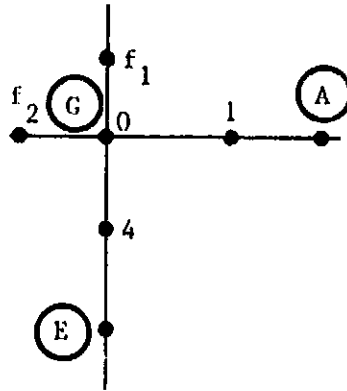
$$z_2 - z_f = \frac{1}{r_o} \sqrt{\left[4a^2 - \frac{1}{a^2} (z_1 - z_3)^2\right]} \quad (C-47)$$

Also,

$$z_f + z_2 = 2z_2 - \frac{1}{r_o} \sqrt{\left[4a^2 - \frac{1}{a^2} (z_1 - z_3)^2\right]} \quad (C-48)$$

Substitution of these last two equations into equation (C-43) yields the desired expression

$$z_o = \frac{r_o^2}{2\left(r_o^2 + \frac{1}{\alpha^2}\right)} \left\{ 2z_2 - \frac{1}{r_o} \sqrt{\left[4a^2 - \frac{1}{\alpha^2} (z_1 - z_3)^2\right]} \right\} + \frac{z_1 + z_3}{2\left(r_o^2 \alpha^2 + 1\right)} \\ + \frac{z_1 - z_3}{4\left(r_o^2 \alpha + \frac{1}{\alpha}\right)} \frac{1}{r_o} \sqrt{\left[4a^2 - \frac{1}{\alpha^2} (z_1 - z_3)^2\right]} \quad (C-49)$$



Applying equation (C-22) at point G yields,

$$z_o = \frac{r_o^2}{2\left(r_o^2 + \frac{1}{\alpha^2}\right)} \left\{ \frac{1}{r_o} \sqrt{\left[4a^2 - \frac{1}{\alpha^2} (z_1 - f_2)^2\right]} + 2z_4 \right\} + \frac{z_1 + f_2}{2\left(r_o^2 \alpha^2 + 1\right)} \\ + \frac{z_1 - f_2}{4r_o\left(r_o^2 \alpha + \frac{1}{\alpha}\right)} \sqrt{\left[4a^2 - \frac{1}{\alpha^2} (z_1 - f_2)^2\right]} \quad (C-50)$$

To find  $f_2$ , we apply  $r\left(\frac{\partial z}{\partial \psi}\right) - \left(\frac{\partial z}{\partial \phi}\right)\left(\frac{dz}{dr}\right) = 0$  without involving  $f_1$ ,

$$r_o \left( \frac{z_o - z_4}{\Delta \psi} \right) - \left( \frac{z_1 - f_2}{2 \Delta \phi} \right) \left( \frac{z_o - z_4}{r_o - r_4} \right) = 0 \quad (C-51)$$

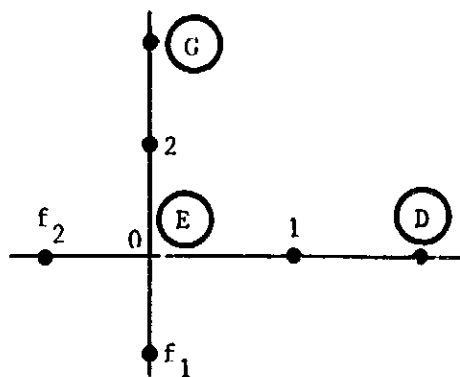
Solving for  $f_2$ ,

$$f_2 = z_1 - 2r_o \alpha (r_o - r_4) \quad (C-52)$$

Substitution into (C-50) yields

$$z_o = \frac{r_o}{r_o^2 + \frac{1}{\alpha^2}} \left\{ \frac{1}{r_o} \sqrt{\left[ a^2 - r_o^2 (r_o - r_h)^2 \right]} + z_h \right\} + \frac{z_1 - r_o \alpha (r_o - r_h)}{r_o^2 \alpha^2 + 1} + \frac{r_o - r_h}{r_o^2 + \frac{1}{\alpha^2}} \sqrt{\left[ a^2 - r_o^2 (r_o - r_h)^2 \right]} \quad (C-53)$$

Let us examine the special point at E



Application of equation (C-49) at point E results in,

$$z_o = \frac{r_o^2}{2 \left( r_o^2 + \frac{1}{\alpha^2} \right)} \left\{ 2z_2 - \frac{1}{r_o} \sqrt{\left[ 4a^2 - \frac{1}{\alpha^2} (z_1 - f_2)^2 \right]} \right. \\ \left. + \frac{1}{2 \left( r_o^2 \alpha^2 + 1 \right)} (z_1 + f_2) \right. \\ \left. + \frac{z_1 - f_2}{4r_o \left( r_o^2 + \frac{1}{\alpha} \right)} \sqrt{\left[ 4a^2 - \frac{1}{\alpha^2} (z_1 - f_2)^2 \right]} \right\} \quad (C-54)$$

In order to find the fictitious point,  $f_2$ , we apply

$$r \left( \frac{\partial z}{\partial \psi} \right) - \left( \frac{\partial z}{\partial \phi} \right) \left( \frac{dz}{d\tau} \right) = 0 \quad \text{on GE, without involving } f_1$$

$$\frac{r_0(z_2 - z_0)}{\Delta\psi} - \frac{z_1 - f_2}{2\Delta\psi} \frac{z_2 - z_0}{r_2 - r_0} = 0 \quad (C-55)$$

Solving for  $f_2$ ,

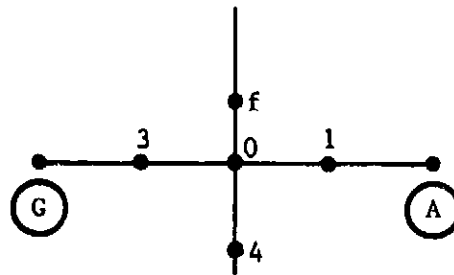
$$f_2 = z_1 - 2r_0\alpha(r_2 - r_0) \quad (C-56)$$

Finally, obtaining from equation (C-54),

$$z_0 = \frac{r_0^2}{r_0^2 + \frac{1}{\alpha^2}} \left\{ z_2 - \frac{1}{r_0} \sqrt{[a^2 - r_0^2(r_2 - r_0)^2]} \right\} + \frac{z_1 - r_0\alpha(r_2 - r_0)}{r_0^2\alpha^2 + 1} + \frac{r_2 - r_0}{r_0^2 + \frac{1}{\alpha^2}} \sqrt{[a^2 - r_0^2(r_2 - r_0)^2]} \quad (C-57)$$

### C. Surface Tension

$$\left(\frac{\partial r}{\partial \phi}\right)^2 + r^2 \left(\frac{\partial r}{\partial \psi}\right)^2 = \frac{1}{\left\{ 1 - \frac{2}{We} + \frac{2}{We} \frac{1}{r} \frac{d}{dr} \left[ \frac{r^2}{\sqrt{\left(\frac{\partial r}{\partial \phi}\right)^2 + r^2}} \right] \right\}} \quad \text{on } \Delta G$$



Applying  $r$  difference equation (eq. (131)) at point 0 where  $f$  is a fictitious point outside the boundary

$$r_o^4 - \frac{r_o^3}{2} (r_f + r_4) + r_o^2 \left[ \frac{1}{\alpha^2} - \frac{1}{8} (r_f - r_4)^2 \right] - \frac{r_o}{2\alpha^2} (r_1 + r_3) + \frac{1}{8\alpha^2} (r_1 - r_3)^2 = 0 \quad (C-58)$$

in difference form, the free surface boundary condition becomes

$$\left( \frac{r_1 - r_3}{2 \Delta \phi} \right)^2 + r_o^2 \left( \frac{r_f - r_4}{2 \Delta \psi} \right)^2 = \frac{1}{1 - \frac{2}{We} + \frac{2}{We} \frac{1}{r_o} \frac{d}{dr_o} \left\{ \frac{r_o^2}{\sqrt{\left[ \frac{(r_1 - r_3)/2 \Delta \phi}{(r_f - r_4)/2 \Delta \psi} \right]^2 + r_o^2}} \right\}} \quad (C-59)$$

Simplifying by using  $\alpha = \Delta \phi / \Delta \psi$  and defining  $\alpha = \Delta \psi$  yields,

$$\frac{1}{\alpha^2} (r_1 - r_3)^2 + r_o^2 (r_f - r_4)^2 = \frac{4\alpha^2}{1 - \frac{2}{We} + \frac{2}{We} \frac{1}{r_o} \frac{d}{dr_o} \left( \frac{r_o^2}{\sqrt{Q + r_o^2}} \right)} \quad (C-60)$$

Now, examine

$$\frac{1}{r_o} \frac{d}{dr_o} \left( \frac{r_o^2}{\sqrt{Q + r_o^2}} \right)$$

As an approximation to this derivative  $Q$  is assumed as a constant.

In actuality,  $Q = f(r_f)$  and  $r_f = f(r_o)$ . Expanding

$$\frac{1}{r_o} \frac{d}{dr_o} \left( \frac{r_o^2}{\sqrt{Q + r_o^2}} \right)$$

yields

$$\frac{1}{r_c} \frac{d}{dr_o} \left( \frac{r_o^2}{\sqrt{Q + r_o^2}} \right) = \left[ \frac{2Q + r_o^2}{\sqrt{(Q + r_o^2)(Q + r_o^2)}} \right] \quad (C-61)$$

Therefore, the finite difference representation for the free surface becomes

$$\frac{1}{\alpha^2} (r_1 - r_3)^2 + r_o^2 (r_f - r_4)^2 = \frac{4a^2}{1 - \frac{2}{We} + \frac{2}{We} \left[ \frac{2Q + r_o^2}{\sqrt{Q + r_o^2}(Q + r_o^2)} \right]} \quad (C-62)$$

$r_f$  must be eliminated between equations (C-58) and (C-62). Let us define

$$X = r_f - r_4 \quad (C-63)$$

Equation (C-62) can be written

$$\frac{1}{\alpha^2} (r_1 - r_3)^2 + r_o^2 X^2 = \frac{4a^2}{1 - \frac{2}{We} + \frac{2}{We} \left[ \frac{2Q + r_o^2}{\sqrt{Q + r_o^2}(Q + r_o^2)} \right]} \quad (C-64)$$

Where

$$Q = \frac{(r_1 - r_3)^2}{X^2} \cdot \frac{1}{\alpha^2} \quad (C-65)$$

Inserting (C-63) into (C-58) yields

$$\frac{r_o^2 X^2}{8} + \frac{r_o^3}{2} X - r_o^4 + r_o^3 r_4 - \frac{r_o^2}{\alpha^2} + \frac{r_o}{2\alpha^2} (r_1 + r_3) - \frac{1}{8\alpha^2} (r_1 - r_3)^2 = 0 \quad (C-66)$$

This is of the form

$$A'X^2 + B'X + C' = 0$$

Hence



$$\chi = \frac{-B' + \sqrt{B'^2 - 4A'C'}}{2A'} \quad (C-67)$$

where

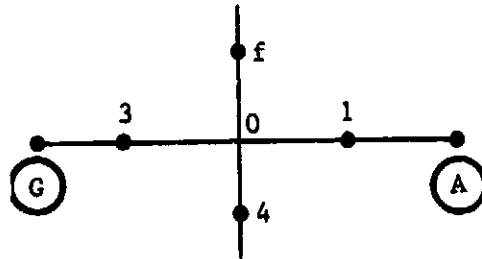
$$A' = \frac{r_o^2}{8} \quad (C-68)$$

$$B' = \frac{r_o^3}{2} \quad (C-69)$$

$$C' = -r_o^4 + r_o^3 r_4 - \frac{r_o^2}{\alpha^2} + \frac{r_o}{2\alpha^2} (r_1 + r_3) - \frac{1}{8\alpha^2} (r_1 - r_3)^2 \quad (C-70)$$

The sign in front of the square root in equation (C-67) was chosen as positive since  $\chi$  must be greater than or equal to zero. In addition,

$$r^2 \left( \frac{\partial z}{\partial \psi} \right)^2 + \left( \frac{\partial z}{\partial \phi} \right)^2 = \frac{1}{1 - \frac{2}{We} + \frac{2}{We} \frac{1}{r} \frac{d}{dr} \left[ \frac{r}{\sqrt{r^2 \left( \frac{\partial z}{\partial \psi} \right)^2 + 1}} \right]} \quad \text{on AG}$$



Applying  $z$  difference equation (132) at point 0 where  $f$  is a fictitious point outside the boundary

$$z_o = \frac{r_o^2}{2 \left( r_o^2 + \frac{1}{\alpha^2} \right)} (f + z_4) + \frac{1}{2 \left( r_o^2 \alpha^2 + 1 \right)} (z_1 + z_3) + \frac{(f - z_4)(z_1 - z_3)}{4 \left( r_o^2 \alpha^2 + \frac{1}{\alpha} \right)} \quad (C-71)$$

In finite difference form, the free surface boundary condition can be written,

$$r_o^2(f - z_4)^2 + \frac{1}{\alpha^2} (z_1 - z_3)^2 = \frac{4a^2}{1 - \frac{2}{We} + \frac{2}{We} \frac{1}{r_o} \frac{d}{dr_o} \left( \frac{r_o}{\sqrt{r_o^2 Q^* + 1}} \right)} \quad (C-72)$$

where,

$$Q^* = \alpha^2 \frac{(f - z_4)^2}{(z_1 - z_3)^2} \quad (C-73)$$

As an approximation,  $Q^*$  is assumed to be a constant. Expanding

$$\frac{1}{r_o} \frac{d}{dr_o} \left( \frac{r_o}{\sqrt{r_o^2 Q^* + 1}} \right)$$

obtaining

$$\frac{1}{r_o} \frac{d}{dr_o} \left( \frac{r_o}{\sqrt{r_o^2 Q^* + 1}} \right) = \frac{1}{r_o (r_o^2 Q^* + 1) \sqrt{r_o^2 Q^* + 1}} \quad (C-74)$$

Therefore, the finite difference representation along the free surface becomes

$$r_o^2(f - z_4)^2 + \frac{1}{\alpha^2} (z_1 - z_3)^2 = \frac{4a^2}{\left[ 1 - \frac{2}{We} + \frac{2}{We} \frac{1}{r_o} \frac{1}{(r_o^2 Q^* + 1) \sqrt{r_o^2 Q^* + 1}} \right]} \quad (C-75)$$

$f$  must now be eliminated between equation (C-71) and (C-75). The manner in which this is done is as follows: Equation (C-75) is solved for  $f = F_{ct}(z_1, z_3, z_4)$ . The results are then inserted into equation (C-71). In this way, equation (C-71) remains explicit in  $z_o$ . Actually, it will be more convenient to solve for the variable  $(f - z_4)$  instead of

f since equation (C-71) can be expressed as,

$$z_o = \frac{r_o^2 z_4}{r_o^2 + \frac{1}{\alpha^2}} + \frac{z_1 + z_3}{2(r_o^2 \alpha^2 + 1)} + (f - z_4) \left[ \frac{2\alpha r_o^2 + (z_1 - z_3)}{4\alpha \left(r_o^2 + \frac{1}{\alpha^2}\right)} \right] \quad (C-76)$$

Turning our attention to equation (C-74), it is solved for  $(f - z_4)$

$$\frac{\alpha^2 r_o^2 (f - z_4)^2}{(z_1 - z_3)^2} + 1 =$$

$$\left\{ \frac{4\alpha^2 \alpha^2}{(z_1 - z_3)^2} \left[ 1 - \frac{2}{We} + \frac{2}{We} \frac{1}{r_o} \frac{1}{\left[ \frac{r_o^2 \alpha^2 (f - z_4)^2}{(z_1 - z_3)^2} + 1 \right]} \right] \sqrt{\frac{r_o^2 \alpha^2 (f - z_4)^2}{(z_1 - z_3)^2} + 1} \right\} \quad (C-77)$$

A new variable  $T^2$  is introduced

$$T^2 = \frac{\alpha^2 r_o^2 (f - z_4)^2}{(z_1 - z_3)^2} + 1 \quad (C-78)$$

Also, let

$$C_0 = \frac{4\alpha^2 \alpha^2}{(z_1 - z_3)^2} \quad (C-79)$$

$$C_1 = 1 - \frac{2}{We} \quad (C-80)$$

$$C_2 = \frac{2}{We} \cdot \frac{1}{r_o} \quad (C-81)$$

Making these substitutions into equation (C-77) results in a cubic equation for  $T$

$$T^3 - \frac{c_0}{c_1} T + \frac{c_2}{c_1} = 0 \quad (C-82)$$

Rewriting this as follows:

$$T^3 + aT + b = 0 \quad (C-83)$$

Once  $T$  is found from (C-83),  $(f - z_4)$  is calculated from equation (C-78) as follows:

$$f - z_4 = \pm \frac{z_1 - z_3}{\alpha r_0} \sqrt{T^2 - 1} \quad (C-84)$$

Appendix D - "Computer Solutions/Listings"

A. Infinite Flat Plate

- I. Computer Listing
- II. Coarse Mesh Solution for  $r$  and  $z$
- III. Computer Listing
- IV. Fine Mesh Solution for  $r$  and  $z$

B. Finite Plate

- V. Computer Listing ( $R_o/L = 1/2$ )
- VI. Coarse Mesh Solution
- VII. Computer Listing ( $R_o/L = 3/4$ )
- VIII. Coarse Mesh Solution

C. Surface Tension Model

- IX. Computer Listing
- X.  $r$  Solution
- XI.  $z$  Solution

## I. F AND Z COMPUTER PROGRAM/INFINITE PLATE/COARSE SOLUTION

DATE 070274 PAGE 1

## INFINITE PLAT PLATE

8FOR=15 MAIN  
FOR 011A-07/0274-15 79 09 1,0)

## MAIN PROGRAM

STORAGE USED CODE(1) 000050: DATA(0) 017271: BLANK COMMON(2) 000000

## EXTERNAL REFERENCES (BLOCK, NAME)

CODE FCMS  
CODE NINTRA  
CODE MPDUS  
CODE MIOIS  
CODE MIOIS  
CODE MIOIS  
CODE MIOIS

## STORAGE ASSIGNMENT (BLOCK, TYPE, RELATIVE LOCATION, NAME)

0000 017261 100F 0001 000014 1076 0000 R 017256 ACC  
0000 R 030062 F 0000 I 017254 IPRINT 0000 I 017253 J  
0000 R 017255 STEP 0000 R 005050 M 0000 R 000000 X  
0000 R 000184 AJINV 0000 R 017260 DMAX  
0000 I 017257 MAXFUN 0000 I 017252 M

00101 10 DIMENSION X(50),F(50),AJINV(50,50),MIS(250)  
00102 20 100 FORMAT (R10.2)  
00103 30 N=50  
00104 40 READ(5,100)X(IJ),J=1,M)  
00105 50 IPRINT=1  
00106 60 STEP=0001  
00107 70 ACC=000001  
00108 80 MAXFUN=500  
00109 90 DMAX=1.0  
00110 100 CALL FOWIN,X,F,AJINV,STEP,DMAX,ACC,MAXFUN,IPRINT,M)  
00111 110 END

END OF COMPILATION NO DIAGNOSTICS.

# ORIGINAL PAGE IS OF POOR QUALITY

INFINITE FLAT PLATE

2FOR-15 EO  
FOR 011A-07/02/77-15 29 13 (,0)

SUBROUTINE EQNS ENTRY POINT 002561

STORAGE USED CODE(1) 002736: DATA(0) 005200: WANN COMMON(12) 000000

EXTERNAL REFERENCES (BLOCK, NAME)

0003 CALFUN  
0004 MATINV  
0005 WADUS  
0006 N1024  
0007 N1018  
0010 N1025  
0011 SORT  
0012 NERR35

STORAGE ASSIGNMENT (BLOCK, TYPE, RELATIVE LOCATION, NAME)

0001	002302 11	0001	000210 10L	0001	002164 10116	0001	002250 10336	0001	002304 10456
0001	002330 10540	0001	002366 10706	0001	002372 10746	0001	000300 11L	0001	002460 11176
0001	002406 11246	0001	002470 13L	0001	000120 1406	0001	000276 14L	0000	005020 16F
0001	000155 1516	0001	000234 17L	0000	005037 19F	0001	000244 2356	0001	000317 22L
0000	005054 23F	0001	000362 24L	0001	000344 2576	0000	005070 26F	0001	002024 27L
0001	000406 2736	0001	000226 28L	0001	000443 29L	0001	000130 31	0001	000374 30L
0001	000455 3126	0001	000427 32L	0001	000432 33L	0001	000590 3306	0001	000542 3336
0001	000613 3526	0001	000614 3576	0001	000660 3646	0001	000661 3676	0001	000673 38L
0001	000176 41L	0001	000725 4006	0001	000734 4066	0001	001052 41L	0001	001030 43L
0001	001037 4356	0001	001022 44L	0000	005101 45F	0001	001110 4636	0001	001114 4676
0001	001102 44L	0001	000173 5L	0001	001307 50L	0001	001246 5246	0001	001200 53L
0001	001325 5456	0001	001166 56L	0001	001364 5606	0001	001375 5656	0001	001421 58L
0001	001331 60L	0001	001434 6036	0001	001446 6116	0001	001526 64L	0001	001550 6446
0001	001561 6516	0001	001467 66L	0001	001614 6646	0001	001635 6756	0001	001512 68L
0001	001517 69L	0000	004765 7F	0001	001604 70L	0001	001662 7046	0001	001730 7216
0001	001742 7326	0001	002002 7426	0001	002063 7706	0000	005001 8F	0001	001741 80L
0001	002253 81L	0001	002152 83L	0001	004764 86F	0001	002186 87L	0001	005011 9F
0001	002422 95L	0001	001231 98L	0000	004747 86F	0001	000000 8JNV	0000	004717 00
0000	004721 0M	0000	004722 0M	0000	004745 0MUL1	0000	004742 0N	0000	004741 0S
0000	004720 0SS	0000	004707 0TEST	0000	004746 0M	0000	004716 0M	0000	004757 0MP
0000	004725 0SC	0000	004726 1	0000	004731 1C	0000	005131 1NJP5	0000	004721 1S
0000	004728 1	0000	004732 1	0000	004732 1K	0000	004734 1M	0000	004751 1PA
0000	004733 1S	0000	004730 1S16	0000	004704 1M4C	0000	004733 1W	0000	004762 1M4P1
0000	004734 1S	0000	004731 1M	0000	004736 1M4C	0000	004737 1M4CIP	0000	004750 1M4P1
0000	004735 1M	0000	004734 1M	0000	004736 1M4C	0000	004737 1M4CIP	0000	004750 1M4P1
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0000	004742 1M	0000	004741 1M	0000	004736 1M4C	0000	004737 1M4CIP	0000	004750 1M4P1
0000	004743 1M	0000	004742 1M	0000	004736 1M4C	0000	004737 1M4CIP	0000	004750 1M4P1
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0000	004746 1M	0000	004745 1M	0000	004736 1M4C	0000	004737 1M4CIP	0000	004750 1M4P1
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0000	004755 1M	0000	004754 1M	0000	004736 1M4C	0000	004737 1M4CIP	0000	004750 1M4P1
0000	004756 1M	0000	004755 1M	0000	004736 1M4C	0000	004737 1M4CIP	0000	004750 1M4P1
0000	004757 1M	0000	004756 1M	0000	004736 1M4C	0000	004737 1M4CIP	0000	004750 1M4P1
0000	004758 1M	0000	004757 1M	0000	004736 1M4C	0000	004737 1M4CIP	0000	004750 1M4P1
0000	004759 1M	0000	004758 1M	0000	004736 1M4C	0000	004737 1M4CIP	0000	004750 1M4P1
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0000	004769 1M	0000	004768 1M	0000	004736 1M4C	0000	004737 1M4CIP	0000	004750 1M4P1
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0000	004802 1M	0000	004801 1M	0000	004736 1M4C	0000	004737 1M4CIP	0000	004750 1M4P1
0000	004803 1M	0000	004802 1M	0000	004736 1M4C	0000	004737 1M4CIP	0000	004750 1

INFINITE FLAY PLATE

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20 DIMENSION X(1),F(1),AJINW(1),N(1),W(1)
30 DIMENSION B(1)(50,50)
40 SET VARIOUS PARAMETERS
50 MAXC = 5
60 MAXC COUNTS THE NUMBER OF CALLS OF CALFUM
70
80
90
100
110 MT= N**
120 MTEST= NT
130
140 NY AND MTEST CAUSE AN ERROR RETURN IF FIX) DOES NOT DECREASE
150
160 DTEST = FLOATIN*N) -0.5
170
180 DTEST IS USED TO MAINTAIN LINEAR INDEPENDENCE
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[illegible]

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## INFINITE FLAT PLATE

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1170 00270
1171 00271 DO 31 I=1,M
1172 00272   NP1 = MX + I
1173 00273   NP2 = MY + I
1174 00274   WINXP1 = X11
1175 00275   WINYP1 = Y11
1176 00276   WINPP1 = F11
1177 00277   51 CONTINUE
1178 00300
1179 00301 C
1180 00302 C CALCULATE A NEW JACOBIAN APPROXIMATION
1181 00303 C
1182 00304 32 IC = 0
1183 00305 33 IS = 3
1184 00306 33 IC = IC + 1
1185 00307   X11C = X11C + DSTEP
1186 00308   60 Y0 I
1187 00309 29 K = IC
1188 00310 DO 34 I=1,M
1189 00311   NP1 = MY + I
1190 00312   WIN1 = (F11)-WINPP1/DSTEP
1191 00313   K = K + 1
1192 00314 34 CONTINUE
1193 00315   NP1C = MX + IC
1194 00316   X11C = WINXP1C
1195 00317   IF (IC-M) 33,35,35
1196 00318 C
1197 00319 C CALCULATE THE INVERSE OF THE JACOBIAN AND SET THE DIRECTION MATRIX
1198 00320 C
1199 00321 35 K=0
1200 00322 DO 36 I=1,M
1201 00323 DO 37 J=1,M
1202 00324   K = K + 1
1203 00325   AJINV(I,J)=WIN1
1204 00326   WDP1 = MD + K
1205 00327 57 CONTINUE
1206 00328   WDCPI = WDCPI + K
1207 00329   WDCPIP = WDCPI + K
1208 00330   WINDCPIP = 1.0/FLOATIN-I
1209 00331 56 CONTINUE
1210 00332 DO 1000 I = 1,M
1211 00333 DO 1000 J = 1,M
1212 00334   CALL MATINV(AJINV,M,KSIG)
1213 00335 DO 1001 I = 1,M
1214 00336 DO 1001 J = 1,M
1215 00337   1001 AJINV(I,J) = 9JINV(I,J)
1216 00338 C
1217 00339 C START ITERATION BY PREDICTING THE DESCENT AND NEWTON MINIMA
1218 00340 C
1219 00341 38 CS = 0.0
1220 00342   DN = 0.0
1221 00343   SE = 0.0
1222 00344 DO 39 I=1,M
1223 00345   X11 = 0.0
1224 00346   Y11 = 0.0
1225 00347 39
1226 00348 9000

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## INFINITE FLAT PLATE

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DATE 070274 P167

291

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C 2300 IF(DD-DD) 53,54,56
C 2310 TEST WHETHER INITIAL VALUE OF DD HAS BEEN SET
C 2320
C 2330
C 2340
C 2350 54 IF(DD) 55,55.56
C 2360 55 DD = AMAX1(DS,AMIN1(DM,DS))
C 2370 DS = DS/(DMULT*DMULT)
C 2380 56 TO 41
C 2390
C 2400 SET THE MULTIPLIER OF THE STEEPEST DESCENT DIRECTION
C 2410
C 2420 56 AMULT = 0.0
C 2430 DMULT = DMULT*SORT1(DM/DS)
C 2440 GO TO 98
C 2450
C 2460 INTERPOLATE BETWEEN STEEPEST DESCENT AND NEWTON DIRECTIONS
C 2470
C 2480
C 2490 53 SP = SP*DMULT
C 2500 AMULT = (DD-DS)/(1*SP-DS)*SORT1(SP-DD)*2*(DM-DD)*(DD-DS))
C 2510 DMULT = DMULT*(1.0-AMULT)
C 2520
C 2530 CALCULATE THE CHANGE IN X AND ITS ANGLE WITH THE FIRST DIRECTION
C 2540
C 2550 98 DM = 0.0
C 2560 SP = 0.0
C 2570 DO 57 I=1,N
C 2580 F(I) = DMULT*X(I)*AMULT*F(I)
C 2590 DM = DM*F(I)*F(I)
C 2600 NCPI = ND + I
C 2610 SP = SP*F(I)*WINOPI
C 2620 57 CONTINUE
C 2630 DS = .25* DM
C 2640
C 2650 TEST WHETHER AN EXTRA STEP IS NEEDED FOR INDEPENDENCE
C 2660
C 2670 IF(MINOC(I)-DIEST) 58,58.59
C 2680 59 IF(SP*SP-DS) 60,59.58
C 2690
C 2700 TAKE THE EXTRA STEP AND UPDATE THE DIRECTION MATRIX
C 2710
C 2720 50 IS = 2
C 2730 DO 60 61 I=1,N
C 2740 NXPI = NX + I
C 2750 NCPI = NC + I
C 2760 NDI = ND + I
C 2770 X(I) = WINXPI + DSTEP*WINOPI
C 2780 WINOPI = WINOPI*(1 + I-C
C 2790 61 CONTINUE
C 2800 WINO = 1.0
C 2810 DO 62 I=1,N
C 2820 M = ND+I
C 2830 SP = WINI
C 2840 CC(I) = CC+N
C 2850 MPN = M + N
C 2860 WINI = WINPI
C 2870 M = MPN
C 2880

```

# ORIGINAL PAGE IS OF POOR QUALITY

INFINITE FLAT PLATE

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63 CONTINUE  
MIN) = SP  
62 CONTINUE  
60 TO 1  
C  
C EXPRESS THE NEW DIRECTION IN TERMS OF THOSE OF THE DIRECTION  
C MATRIX, AND UPDATE THE COUNTS IN WINDC+1) ETC.  
C  
58 SP= 0.  
K= ND  
DO 64 I=1,N  
WDCPI = WDC + I  
X(I) = DW  
DW = 0.  
DO 65 J=1,N  
K= N+1  
DW = DW\*(J)\*W(N)  
65 CONTINUE  
60 TO 168,66)) IS  
66 WINDC(1) = WINDCPI+1.0  
SP= SP-DW\*DW  
IF (SP-DS1 64,64,67  
67 IS=1  
KK=I  
X(I) = DW  
60 TO 69  
68 X(I) = DW  
WDCPI = WDC + I  
69 WINDCPI) = WINDCPI+1.0  
64 CONTINUE  
WIND) = 1.0  
C  
C REORDER THE DIRECTIONS SO THAT KK IS FIRST  
C  
71 KK= WDC\*W(N)  
DO 72 I=1,N  
K= K+I  
SP = W(N)  
DO 73 J=2,N  
W(N) = X - N  
W(N) = W(N)  
K= K-N  
73 CONTINUE  
MIN) = SP  
72 CONTINUE  
C  
C GENERATE THE NEW ORTHOGONAL DIRECTION MATRIX  
C  
70 DO 74 I=1,N  
WDCPI = WDC + I  
WINDCPI) = 0.0  
74 CONTINUE  
SP= X(I)\*X(I)  
K= ND  
DO 75 I=2,N  
DS = SORT(SP\*(SP+X(I))\*X(I)))

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INFINITE FLAT PLATE

```

00700 3890 DB = SP/DS
00701 3900 DS = X(1)/DS
00702 3910 SP = SP-X(1)*X(1)
00703 3920 DO 76 J=1,N
00704 3930 K= K+1
00705 3940 MNPJ = MNP + J
00706 3950 MNPJ = K * N
00707 3960 MNPJ = MNPJ+X(1)-X(1)*X(1)
00708 3970 WIK = DMNP(MNPJ)-DS*(MNPJ)
00709 3980 76 CONTINUE
00710 3990 75 CONTINUE
00711 4000 SP = 1.0/SORT(DM)
00712 4010 DO 77 I=1,M
00713 4020 K= K+1
00714 4030 WIK = SP*(I)
00715 4040 77 CONTINUE
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## INFINITE FLAT PLATE

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TINC = PJ/SP  
 DD = AMIN(DM, SP\*DD)  
 DO 80 TO 83  
 C IF F(I) IMPROVES STORE THE NEW VALUE OF X  
 C  
 87 IF (F50 - FMIN) 03.50.50  
 83 FMIN = F50  
 DO 88 I=1,M  
 SP = X(I)  
 NXPI = NX + I  
 NFPI = NF + I  
 X(I) = MINXPI  
 MINXPI = SP  
 SP = F(I)  
 F(I) = MINFPI  
 MINFPI = SP  
 MINMPI = -MINMPI  
 88 CONTINUE  
 IF (IIS-I) 28.28.50  
 C CALCULATE THE CHANGES IN F AND X  
 C  
 28 DO 89 I=1,M  
 NXPI = NX + I  
 NFPI = NF + I  
 X(I) = X(I) - MINMPI  
 F(I) = F(I) - MINMPI  
 89 CONTINUE  
 C UPDATE THE APPROXIMATIONS TO J AND AJINU  
 C  
 N = 0  
 DO 90 I=1,M  
 MPI = NI + I  
 MPI = NI + I  
 MINMPI = X(I)  
 MINMPI = F(I)  
 DO 91 J=1,M  
 MINMPI = MINMPI - AJINU(I,J)\*F(J)  
 K=K+1  
 MINMPI = MINMPI - MINMPI  
 91 CONTINUE  
 90 CONTINUE  
 SP = 0.0  
 SS = 0.0  
 DO 92 I=1,M  
 DS = 0.0  
 DO 93 J=1,M  
 DS = DS + AJINU(I,J)\*X(J)  
 93 CONTINUE  
 SP = SP + DS\*F(I)  
 SS = SS + X(I)\*X(I)  
 F(I) = DS  
 92 CONTINUE  
 DMULT = 1.0

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01137	574*
01140	575*

```

IF (ABS(ESP)-.1)SS) 94,95,95
94 DMULT = D.2
95 PJ = DMULT*SS
PA = DMULT/(DMULT+SP+1-D-DMULT)*SS)
DO 96 I=1,N
  MUPI = MU + I
  MUPI = MU + I
  SP = PJ+MU*UPI)
  SS = PA+MU*UPI)
DO 97 J=1,M
  K = K+1
  WIK = MIN(SPE*(J)
  AJINVI(J) = AJINVI(J)+SS*(J)
97 CONTINUE
96 CONTINUE
  GO TO 38
END

```

END OF COMPIATION



INFINITE FLAT PLATE

FOR 15 MATIN  
FOR 011A-07/0274-15 29 31 (0)

SUBROUTINE MATINM ENTRY POINT 000655

STORAGE USED CODE(1) 000715: DATA(0) 012003: BLANK COMMON(2) 000000

EXTERNAL REFERENCES (BLOCK, NAME)

0003 WEP25

STORAGE ASSIGNMENT

0001 000007 1L	0001 000327 11L	0001 000376 13L	0001 000127 1376	0001 000133 1436
0001 000423 15L	0001 000156 1516	0001 000174 1556	0001 000231 1736	0001 000040 2L
0001 000250 2056	0001 000562 21L	0001 000284 2136	0001 000302 2216	0001 000614 23L
0001 000352 2356	0001 000366 2426	0001 000412 2516	0001 000427 2636	0001 000435 2676
0001 000444 2726	0001 000450 2766	0001 000455 3L	0001 000520 3116	0001 000522 3146
0001 000325 3206	0001 000601 3356	0001 000602 3406	0001 000553 4L	0001 000060 5L
0001 000206 7L	0000 000062 A	0000 R 000072 DELT	0000 R 000104 DELT	0000 R 000073 EPS
0001 000077 I	0000 011726 INJPS	0000 I 000100 J	0000 I 000000 K	0000 I 000101 L
0000 I 000074 LOOPS	0000 I 000075 M	0000 L 000070 MATIN	0000 I 000076 MM	0000 I 000071 MMAX
0000 I 000102 M	0000 D 000066 PROD	0000 D 000064 R	0000 I 000077 N	0000 R 000103 TEST
0000 D 000105 Z1	0000 D 000105 Z2			

MINV 2

SUBROUTINE MATINM(S,MX,MS16)  
MATRIX INVERSION BY GAUSS-JORDAN ELIMINATION

```

1* DIMENSION S(50,50),T(50,50),Z1(50,50),Z2(50,50),K(50)
2* DOUBLE PRECISION A,R,PROD,T,Z1,Z2
3* LOGICAL MATIN
4* DATA MMAX, DELT, EPS, LOOPS/ 5.0,0.001,1.0E-8,1/
5* MATIN=.TRUE.
6* GO TO 1
7* C.....INITIALIZE ROUTINE AND TEST MX (=ORDER OF MATRIX)
8* 1 N=MX
9* IF(M-S,1-AND-M,LE-MMAX) GO TO 5
10* IF(M-EQ-1) GO TO 2
11* MS16=MS16+1
12* RETURN
13* 2 PROD=S(1,1)
14* THE TEST FOR EQUALITY BETWEEN NON-INTEGERS MAY NOT BE MEANINGFUL-
15* IF(PROD-NE-0.0) GO TO 4
16* 3 MS16=MS16+2
17* 4 RETURN
18* 5 S(1,1)=1-D/PROD
19* GO TO 23
20* 6 PROD=1.0
21* MM=N-1
22* DO 6 I=1,M
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OF POOR QUALITY

117

INFINITE FLAT PLATE	DATE	070274	PAGE	13
00141	250	W=I	MINV	28
00142	260	DO 6 J=1,M	MINV	29
00143	270	6 Y(I,J)=S(I,J)		
00144	280	C-----BEGIN BY FINDING LARGEST PIVOTAL ELEMENT		
00145	290	DO 11 I=1,M	MINV	31
00146	300	A=Q=0	MINV	32
00147	310	DO 7 J=1,M	MINV	33
00148	320	IF (ABS(T(I,J))-LE-A) 60 TO 7	MINV	34
00149	330	A=ABS(T(I,J))		
00150	340	L=J	MINV	37
00151	350	7 CONTINUE	MINV	38
00152	360	*DIAGNOSTIC* THE TEST FOR EQUALITY BETWEEN NON-INTEGERS MAY NOT BE MEANINGFUL.		
00153	370	IF (A.EQ.O) 60 TO 3	MINV	39
00154	380	C-----REARRANGE ROWS AND ORDER ARRAY	MINV	40
00155	390	N=K(L)	MINV	41
00156	400	K(L)=K(I)	MINV	42
00157	410	K(I)=M	MINV	43
00158	420	DO 8 J=1,M	MINV	44
00159	430	A=T(I,J)		
00160	440	T(I,J)=T(L,J)		
00161	450	8 T(L,J)=A		
00162	460	C-----REDUCE PIVOTAL ROW	MINV	48
00163	470	A=T(L,I)	MINV	50
00164	480	IF (.NOT. MATIN) PROD=PROD*A	MINV	51
00165	490	DO 9 J=1,M		
00166	500	9 T(I,J)=T(I,J)/A	MINV	54
00167	510	T(I,M)=1.0/A	MINV	55
00168	520	C-----REDUCE REMAINING ROWS	MINV	56
00169	530	DO 11 L=1,M		
00170	540	IF (A.EQ.1) 60 TO 11	MINV	58
00171	550	A=T(L,I)		
00172	560	DO 10 M=1,M		
00173	570	T(L,M)=T(L,M)-A*T(I,M)		
00174	580	T(L,M)=A*T(I,M)		
00175	590	11 CONTINUE	MINV	62
00176	600	C-----UNSCRAMBLE INVERTED MATRIX	MINV	63
00177	610	DO 15 I=1,M	MINV	64
00178	620	IF (ABS(T(I,M))-LT.(ABS(T(L,M-1))+EPS)) T(L,M)=O.O	MINV	65
00179	630	PROD=PROD	MINV	66
00180	640	DO 12 J=1,M	MINV	67
00181	650	12 IF (A(J)-EQ.I) 60 TO 13	MINV	68
00182	660	60 TO 3	MINV	69
00183	670	13 DO 14 L=1,M	MINV	70
00184	680	A=T(L,I)		
00185	690	T(L,I)=T(L,J)		
00186	700	14 T(L,J)=A		
00187	710	K(J)=K(I)	MINV	74
00188	720	15 CONTINUE	MINV	75
00189	730	C-----OBTAIN ERROR MATRIX	MINV	76
00190	740	DO 20 M=1,LOOPS	MINV	77
00191	750	TEST=O.O	MINV	78
00192	760	DO 17 I=1,M	MINV	79
00193	770	DO 17 J=1,M	MINV	80
00194	780	R=O.O	MINV	81
00195	790	DO 16 L=1,M	MINV	82
00196	800	16 R=R-21T(L,J)*S(I,L)		

OF 1000 QUALITY

INFINITE FLAT PLATE

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00302 IF1.EQ.JJ R=01.0
00303 TEST=ABS(1-TEST,ABSARD)
00304 17 2211.L1=R
00305 00 19 1=1.M
00306 00 19 J=1.M
00307 A=0.0
00308 00 18 1=1.M
00309 18 A=0.2111.L1=0.2211.JJ
00310 19 2111.JJ=2111.JJ+A
00311 IF1.EQ.JJ DELT 60 TO 21
00312 20 CONTINUE
00313 2116=RS16+J
00314 C.....TRANSFER FINAL INVERSE
00315 21 00 22 1=1.M
00316 00 22 J=1.M
00317 -2 511.JJ=2111.JJ
00318 .3 IF1.EQ.JJ RETURN
00319 DET=PROD
00320 RETURN
00321 END

```

MINV 84  
MINV 85  
MINV 87  
MINV 88  
MINV 89  
MINV 90  
MINV 93  
MINV 94  
MINV 95  
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MINV 100  
MINV 101  
MINV 102  
MINV 103

END OF COMPILATION 2 DIAGNOSTICS.

## INFINITE FLAT PLATE

DATE 070279 PAGE 15

8PM.15 CAL  
FOR 011A-07/02/79-15 29 39 1.01

SUBROUTINE CALFUN ENTRY POINT 001224

STORAGE USED CODE(1) 001227; DATA(1) 000203; BLANK COMMON(2) 000000

EXTERNAL REFERENCES (BLOCK, NAME)

0003 SORT  
0004 WEARR3

STORAGE ASSIGNMENT (BLOCK, TYPE, RELATIVE LOCATION, NAME)

0001 000206 1216 0001 000919 1366 0001 000517 1466 0001 000600 1616 0001 000666 1706  
0001 000736 1766 0001 001001 2046 0001 001050 2126 0001 001112 2206 0001 001151 2266  
0001 000957 62L 0000 R 000066 AL 0000 R 000064 D 0000 I 000070 IS  
0000 I 000071 IY 0000 I 000067 K 0000 R 000072 MR 0000 I 000070 IS  
0000 R 000065 PSIG 0000 R 000062 MS

SUBROUTINE CALFUN(N,Y,F)

DIMENSION U(50)

DIMENSION Y(50)

DIMENSION F(50)

REAL MS

MS=1.

US=MS\*\*2

D=-0.0204

PSIG=MS/2.

AL=PSIG/5.

C ALL STATEMENT NUMBERS LOCAL TO CAL

C DEFINE F(I) IN TERMS OF Y(I)

50 U(I)=0.0AL\*\*2/US-DefY(I)-0.0002

IF U(I).LE.0.0U(I)=0.0

F(I)=Y(I)\*0.0001

1711002010--5\*SORT(U(I))--Y(I)\*0.0001

212.0001Y(I)-0.0002-0.0AL\*\*2/US)/8.

DO 60 M=2,6

U(M)=0.0AL\*\*2/US-DefY(M)-Y(M-1)\*0.0002

IF U(M).LE.0.0U(M)=0.0

F(M)=Y(M)\*0.0001

1711002010--5\*SORT(U(M))--Y(M)\*0.0001

212.0001Y(M)-0.0002-0.0AL\*\*2/US)/8.

60 CONTINUE

U(71)=0.0AL\*\*2/US-11.-Y(61)\*0.0002

IF U(71).LE.0.0U(71)=0.0

F(71)=Y(71)\*0.0001

1711002010--5\*SORT(U(71))--Y(71)\*0.0001

212.0001Y(71)-0.0002-0.0AL\*\*2/US)/8.

DO 61 M=8,29,7

DO 61 M=8,29,7

DATE 070274 PAGE 34

## INFINITE FLAT PLATE

```

00100 310      FIK=YIK**3-YIK**3*(YIK-7)*YIK**2/2.
00101 320      YIK**2*(ID-.125*(YIK-7)-YIK**2)/2.
00102 330      2*YIK**2*(YIK-1)*YIK**2/2.
00103 340      2*YIK**2*(YIK-1)*YIK**2/2.
00104 350      2*YIK**2*(YIK-1)*YIK**2/2.
00105 360      2*YIK**2*(YIK-1)*YIK**2/2.
00106 370      2*YIK**2*(YIK-1)*YIK**2/2.
00107 380      2*YIK**2*(YIK-1)*YIK**2/2.
00108 390      2*YIK**2*(YIK-1)*YIK**2/2.
00109 400      2*YIK**2*(YIK-1)*YIK**2/2.
00110 410      2*YIK**2*(YIK-1)*YIK**2/2.
00111 420      2*YIK**2*(YIK-1)*YIK**2/2.
00112 430      2*YIK**2*(YIK-1)*YIK**2/2.
00113 440      2*YIK**2*(YIK-1)*YIK**2/2.
00114 450      2*YIK**2*(YIK-1)*YIK**2/2.
00115 460      2*YIK**2*(YIK-1)*YIK**2/2.
00116 470      2*YIK**2*(YIK-1)*YIK**2/2.
00117 480      2*YIK**2*(YIK-1)*YIK**2/2.
00118 490      2*YIK**2*(YIK-1)*YIK**2/2.
00119 500      2*YIK**2*(YIK-1)*YIK**2/2.
00120 510      2*YIK**2*(YIK-1)*YIK**2/2.
00121 520      2*YIK**2*(YIK-1)*YIK**2/2.
00122 530      2*YIK**2*(YIK-1)*YIK**2/2.
00123 540      2*YIK**2*(YIK-1)*YIK**2/2.
00124 550      2*YIK**2*(YIK-1)*YIK**2/2.
00125 560      2*YIK**2*(YIK-1)*YIK**2/2.
00126 570      2*YIK**2*(YIK-1)*YIK**2/2.
00127 580      2*YIK**2*(YIK-1)*YIK**2/2.
00128 590      2*YIK**2*(YIK-1)*YIK**2/2.
00129 600      2*YIK**2*(YIK-1)*YIK**2/2.
00130 610      2*YIK**2*(YIK-1)*YIK**2/2.
00131 620      2*YIK**2*(YIK-1)*YIK**2/2.
00132 630      2*YIK**2*(YIK-1)*YIK**2/2.
00133 640      2*YIK**2*(YIK-1)*YIK**2/2.
00134 650      2*YIK**2*(YIK-1)*YIK**2/2.
00135 660      2*YIK**2*(YIK-1)*YIK**2/2.
00136 670      2*YIK**2*(YIK-1)*YIK**2/2.
00137 680      2*YIK**2*(YIK-1)*YIK**2/2.
00138 690      2*YIK**2*(YIK-1)*YIK**2/2.
00139 700      2*YIK**2*(YIK-1)*YIK**2/2.
00140 710      2*YIK**2*(YIK-1)*YIK**2/2.
00141 720      2*YIK**2*(YIK-1)*YIK**2/2.
00142 730      2*YIK**2*(YIK-1)*YIK**2/2.
00143 740      2*YIK**2*(YIK-1)*YIK**2/2.
00144 750      2*YIK**2*(YIK-1)*YIK**2/2.
00145 760      2*YIK**2*(YIK-1)*YIK**2/2.
00146 770      2*YIK**2*(YIK-1)*YIK**2/2.
00147 780      2*YIK**2*(YIK-1)*YIK**2/2.
00148 790      2*YIK**2*(YIK-1)*YIK**2/2.
00149 800      2*YIK**2*(YIK-1)*YIK**2/2.

```

END OF COMPILATION NO DIAGNOSTICS.

DATE 040570 PAGE 257

INFINITE FLAT PLATE

AT THE 310 TH CALL OF CALFUM WE HAVE

F11

1	-26541012-01	-50244020-02
2	-26165584-01	-63966683-02
3	-22680394-01	-10192208-01
4	-15253005-01	-19077991-02
5	-10540853-01	-77230529-02
6	-10241688-01	-36837752-02
7	-19074260-01	-12102634-02
8	-36554089-01	-10294695-01
9	-26161744-01	-14457410-01
10	-22327907-01	-21219265-01
11	-19919475-01	-35230514-02
12	-96486716-00	-34360909-02
13	-91838167-00	-92781783-03
14	-90438066-00	-50812014-03
15	-36525446-01	-10723316-01
16	-26160268-01	-13809766-01
17	-22123906-01	-20670719-01
18	-14605228-01	-57012009-02
19	-84933027-00	-10842451-02
20	-80562543-00	-13186946-02
21	-78436679-00	-86075103-03
22	-36509466-01	-11411039-01
23	-26161283-01	-12569365-01
24	-21977497-01	-20706584-01
25	-14338906-01	-38107553-02
26	-70283066-00	-01968715-04
27	-65509400-00	-88849347-03
28	-64302110-00	-99666334-03
29	-36492280-01	-11610316-01
30	-26163948-01	-11036446-01
31	-21800748-01	-22334901-01
32	-14129902-01	-74147554-02
33	-49379254-00	-10728177-04
34	-85625703-00	-93313094-03
35	-44746030-00	-89681619-03
36	-36487271-01	-50850507-02
37	-26164498-01	-51837265-02
38	-21868414-01	-11770964-01
39	-14038445-01	-42180943-02

THE SUM OF SQUARES IS -35713191-02  
 ERROR RETURN BECAUSE FIX FAILED TO DECREASE USINGA NEW JACOBEAN

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DATE 091770 PAGE 1

INFINITE PLATE 2 SOLUTION

SPON.75-MAIN  
FOR 011A-09/17/79-10 26 18 6.01

MAIN PROGRAM

STORAGE USED CODE(1) 000752; DATA(1) 000315; BLANK COMMON(2) 000000

EXTERNAL REFERENCES (BLOCK, NAME)

0003 MINTPS  
0004 MRCUS  
0005 MIOIS  
0006 MIOZS  
0007 MUDUS  
0010 SORT  
0011 MSTOPA

STORAGE ASSIGNMENT (BLOCK, TYPE, RELATIVE LOCATION, NAME)

0000 000244 100F 0001 000032 1206 0001 000044 1266 0001 000211 1626  
0001 000372 2005 0001 000450 2106 0001 000517 2216 0000 000246 247  
0001 000415 3L 0001 000553 50L 0000 000257 8F 0000 R 000234 AL  
0000 1 000237 COUNT 0000 R 000232 D 0000 1 000240 I 0000 1 000242 IS  
0000 1 000236 J 0000 1 000241 K 0000 R 000227 K0 0000 1 000235 M  
0000 R 000228 NS 0000 R 000233 PS16 0000 R 000231 US 0000 R 000042 V  
0000 R 000144 Z

00101 10 DIMENSION U4501  
00103 20 DIMENSION Y4501  
00104 30 DIMENSION Z4501  
00105 40  
00106 50 REAL NS  
00107 60 REAL NS  
00110 70 MM=250  
00111 80 NS=1  
00112 90 US=NS\*\*2  
00113 100 D=-0204  
00114 110 PSIG=NS/2  
00115 120 AL=PS16/5  
00116 130  
00117 140 READ(15,100) (Y(I),J=1,M)  
00118 150 READ(15,100) (Z(I),J=1,M)  
00119 160 100 FORMAT(10F10.23)  
00120 170 NO=3.315  
00121 180 INTEGER COUNT  
00122 190 COUNT=D  
00123 200 50 COUNT=COUNT+1  
00124 210 IF COUNT=CE-MMI 50 TO 99  
00125 220 THIS STATEMENT HAS TOO MANY LEFT PARENTHESES.  
00126 230 26 FORMAT(1H,6X) THAT THE 15,1X25MM ITERATION WE HAVE!  
00127 240 WRITE(16,26) COUNT  
00128 250 8 FORMAT(1H,4X) MI,9X)N2(I) // (15,(17-8))  
00129 260 WRITE(16,8) (1,Z(I),I=1,M)

DATE 091770 PAGE 2

## INFINITE PLATE 2 SOLUTION

```

00155 250 00155= N-0AL002/US-D0(Z12)-125002
00156 260 IF(U01)-LE-0.0) U01=0.0
00160 270 Z11=V11002+ISORT(U01)/12-0.2+Z19)/12-0(V11002+D)) +
00160 280 1121210-1253/12-0(V11002+D0+1.1)+
00160 290 2121210-1253+ISORT(U01)/14-0(V11002+2/SORT(D0)+SORT(D1))
00161 300 DO 7 K=2,6
00161 310 U07= N-0AL002/US-D0(Z1K-1)-Z1K-11002
00165 320 IF(U0K)-LE-0.0) U0K=0.0
00167 330 Z1K=V1K002+ISORT(U0K)/12-0(Z1K-03)/12-0(V1K002+D)) +
00167 340 1121K01+Z1K-1)/12-0(V1K002+D0+1.1)+
00167 350 2121K01+Z1K-1)/12-0(V1K002+D0+1.1)+
00170 360 7 CONTINUE
00172 370 U071= N-0AL002/US-D0(K0-Z16)-002
00173 380 IF(U07)-LE-0.0) U07=0.0
00175 390 Z17=V17002+ISORT(U07)/12-0(Z15)/12-0(V17002+D)) +
00175 400 11K0-Z16)/12-0(V17002+D0+1.1)+
00175 410 21K0-Z16)/12-0(V17002+D0+1.1)+
00176 420 21K0-Z16)/12-0(V17002+D0+1.1)+
00176 430 1219)/12-0(V18002+D0+1.1)+
00177 440 DO 2 K=16,24,8
00202 450 Z1K= V1K002+Z1K-8)+Z1K-8)/12-0(V1K002+D)) +
00202 460 121K-1)/12-0(V1K002+D0+1.1)+
00203 470 2 CONTINUE
00205 480 15=9
00206 490 3 IT= 15 + 5
00207 500 DO 4 K=15,17
00212 510 Z1K=V1K002+Z1K-8)+Z1K-8)/12-0(V1K002+D)) +
00212 520 1121K-1)/12-0(V1K002+D0+1.1)+
00212 530 2121K-8)+Z1K-8)/12-0(V1K002+D0+1.1)+
00213 540 4 CONTINUE
00215 550 15=15+8
00216 560 IF(15-LE-25)60 TO 3
00220 570 DO 5 K=15,31,8
00223 580 Z1K=V1K002+Z1K-8)+Z1K-8)/12-0(V1K002+D)) +
00223 590 11K0+Z1K-1)/12-0(V1K002+D0+1.1)+
00223 600 2121K-8)+Z1K-8)/12-0(V1K002+D0+1.1)+
00224 610 5 CONTINUE
00226 620 Z1321=V1321002+Z12)/12-0(V1321002+D)) +
00227 630 DO 6 K=35,37
00232 640 Z1K=V1K002+Z1K-8)/12-0(V1K002+D)) +
00232 650 1121K-1)/12-0(V1K002+D0+1.1)+
00232 660 2121K-8)+Z1K-1)/12-0(V1K002+D0+1.1)+
00233 670 6 CONTINUE
00235 680 Z1381=V1381002+Z130)+Z130)/12-0(V1381002+D)) +
00235 690 1121391+Z137)/12-0(V1381002+D0+1.1)+
00235 700 2121391+Z140)/12-0(V1381002+D0+1.1)+
00235 710 21391=V1391002+Z131)+Z131)/12-0(V1391002+D)) +
00236 720 11K0+Z130)/12-0(V1391002+D0+1.1)+
00236 730 212131+Z131)/12-0(V1391002+D0+1.1)+
00237 740 Z1401=V1401002+Z1381)/12-0(V1401002+D)) +
00237 750 112141)/12-0(V1401002+D0+1.1)+
00240 760 21411=V1411002+Z1391)/12-0(V1411002+D)) +
00240 770 11K0+Z140)/12-0(V1411002+D0+1.1)+
00241 780 DO 10 50
00242 790 99 END

```



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AT THE 249 TH ITERATION WE HAVE

1	-13719856+00
2	-19091896+00
3	-22606329+00
4	-36715700+00
5	-87868027+00
6	-14526295+01
7	-23448205+01
8	-10003767+00
9	-10985776+00
10	-15276201+00
11	-18180807+00
12	-30835310+00
13	-81400262+00
14	-14499685+01
15	-23491339+01
16	-75050307+01
17	-82451005+01
18	-11458908+00
19	-13698362+00
20	-23945656+00
21	-7381828+00
22	-14382671+01
23	-23461986+01
24	-50044650+01
25	-54994802+01
26	-74401815+01
27	-91624808+01
28	-16603524+00
29	-62519554+00
30	-14139405+01
31	-23390695+01

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INFINITE PLATE 2 SOLUTION

32	.25025193-01
33	.27505639-01
34	.38203740-01
35	.45913611-01
36	.85872217-01
37	.45195695-00
38	.13611427-01
39	.23212366-01
40	.11050000-01
41	.22100000-01

OFIN

$$\psi=0$$

E

C

B

④

# III. Y AND Z COMPUTER PROGRAM/INFINITE PLATE/FINE SOLUTION

DATE 082779 PAGE 3

## INFINITE PLATE PLATE

3PC0.15 MAYN  
FOR 0118-06/2779-17 12 12 (0)

### MAIN PROGRAM

STORAGE USED CODE(1) 070051; DATA(0) 000516; BLANK COMMON(2) 000070

### COMMON BLOCKS

0003 A C61301  
0004 B C61301  
0005 C 165140  
0006 D C61301

### EXTERNAL REFERENCES (BLOCK, TYPE, RELATIVE LOCATION, NAME)

0007 FONS  
0010 NINTRA  
0011 NROUS  
0012 NIOIS  
0013 NIOZS  
0014 NSTOPS

### STORAGE ASSIGNMENT (BLOCK, TYPE, RELATIVE LOCATION, NAME)

0000 000505 10CF 0001 000017 1156 0000 R 000502 ACC 0004 000000 AJINV 0006 000000 BJINV  
0000 R 000500 DMAX 0000 P 000237 F 0000 I 000500 IPRINT 0000 I 000477 J 0000 I 000503 MAXFUN  
0000 I 000476 N 0000 R 000501 STEP 0003 000000 T 0000 R 000000 W 0000 R 000000 X

00101 1\* COMPILER(XN=1)  
00103 2\* DIMENSION X(159),F(159)  
00105 3\* COMMON/A/1159,159  
00106 4\* COMMON/B/AJINV:159,159  
00107 5\* COMMON/C/A(60000)  
00110 6\* COMMON/D/BJINV(159,159)  
00111 7\* TOD FORM(1 (61610.2))  
00112 8\* N=159  
00113 9\* REWIND(1001XVJ),J=1,N  
00121 10\* IPRINT=1  
00122 11\* STEP=0001  
00123 12\* ACC=000001  
00124 13\* MAXFUN=700  
00125 14\* DMAX=1.0  
00126 15\* CALL FORMINT,F,STEP,DMAX,TCC,MAXFUN,IPRINT  
00127 16\* END

END OF COMPILATION

NO DIAGNOSTICS.

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OF POOR QUALITY

INFINITE FLAT PLATE

FOR 15 EC  
FOR 011A-08/2774-17 12 21 4.01

SUBROUTINE EOMS ENTRY POINT 002525

STORAGE USED CODE(1) 002652; DATA(1) 000276; PLANK COMMON(2) 000000

COMMON BLOCKS

0003 A 061301  
0004 B 061301  
0005 C 165190  
0006 D 061301

EXTERNAL REFERENCES (BLOCK, NAME)

0007 CALFUM  
0010 MATINY  
0011 MUDUS  
0012 MIOZS  
0013 MIDIS  
0014 MERZS  
0015 SORT  
0016 MERZS

STORAGE ASSIGNMENT (BLOCK, TYPE, RELATIVE LOCATION, NAME)

0001	000110	1L	0001	000216	10L	0001	002137	10:46	0001	002221	10:46	0001	002253	10526
0001	002277	10616	0001	002335	10756	0001	000306	11L	0001	002341	11016	0001	002424	11246
0001	002452	11316	0001	000276	13L	0001	000126	1456	0001	000304	15L	0000	000114	16F
0001	000163	1666	0001	000242	17L	0000	000133	19F	0001	000325	22L	0001	000252	2226
0000	000150	23F	0001	000370	24L	0000	000164	26F	0001	000352	2646	0001	001777	27L
0001	002201	28L	0001	000451	29L	0001	000136	31L	0001	000402	30L	0001	000414	30C6
0001	000463	3176	0001	000435	32L	0001	000440	33L	0001	000533	3356	0001	000535	34C6
0001	002405	3576	0001	000606	3626	0001	000641	3716	0001	000642	3746	0001	000654	38L
0001	000204	4L	0001	000700	4056	0001	001025	41L	0001	000707	4136	0001	001003	43L
0001	000775	44L	0001	001012	442C	0000	000175	45F	0001	001063	4706	0001	001067	4746
0001	001055	48L	0001	000201	5L	0001	001262	50L	0001	001153	53L	0001	001221	5316
0001	001300	5526	0001	001141	56L	0001	001337	5656	0001	001350	5726	0001	001374	58L
0001	001264	60L	0001	001467	6106	0001	001421	6166	0001	001501	64L	0001	001523	6516
0001	001334	656C	0001	001442	66L	0001	001567	6716	0001	001465	68L	0001	001472	69L
0000	000061	7F	0001	001557	70L	0001	001610	7026	0001	001635	7116	0001	001703	7266
0001	001725	7376	0001	001755	7476	0001	002036	7756	0000	000075	8F	0001	001714	80L
0001	002026	81L	0001	001725	83L	0000	000060	86F	0001	002121	87L	0000	000105	9F
0001	002474	95L	0001	001204	98L	0001	000000	AJINY	0000	000063	ANMULY	0006	000000	8JINY
0000	000013	00	0000	000015	00	0000	000016	00W	0000	000041	00MULY	0000	000036	00W
0000	000035	DS	0000	000014	05S	0000	000003	0TEST	0000	000042	00	0000	000012	FMIN
0001	000031	FMP	0000	000021	F50	0000	000022	I	0000	000025	IC	0000	000225	INJPS
0000	000017	I	0000	000030	J	0000	000026	K	0000	000046	KK	0000	000050	MMN
0000	000026	KPN	0000	000047	MS	0000	000034	MS16	0000	000000	MAXC	0000	000007	MW
0000	000036	MPI	0000	000011	NO	0000	000010	NOC	0000	000032	NDCPI	0000	000033	NDCPIP
0000	000044	N0PT	0000	000031	N0PM	0000	000005	NF	0000	000023	NFPJ	0000	000040	NFPJ
0000	000001	NY	0000	000002	NTEST	0000	000006	NW	0000	000051	NUPJ	0000	000052	NUPJ

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INFINITE FLAT PLATE

```

0000 I 00000000 0000 I 000024 NXPI 0000 I 000027 PA 0000 R 000055 PJ
0000 P 000037 SP 0000 P 000054 SS 0003 000000 T 0000 R 000020 TINC 0005 R 000000 M

COMPILER=HLL
SUBROUTINE EGASIN,X,F,DSILP,DMAX,ACC,MANFUN,IPRINT)
  DIMENSION X(1),F(1)
  COMMON/A/T(159,159)
  COMMON/B/AJIN(159,159)
  COMMON/C/N(6000)
  COMMON/D/BJIN(159,159)

  SET VARIOUS PARAMETERS
  MAXC = 0
  MAXC COUNTS THE NUMBER OF CALLS OF CALFUN
  NTE = N+4
  NTESTE = N1
  N1 AND NTEST CAUSE AN ERROR RETURN IF F(X) DOES NOT DECREASE
  DYEST = FLOAT(N) - 0.5
  DYEST IS USED TO MAINTAIN LINEAR INDEPENDENCE
  NX = N+4
  NY = N+4
  NZ = N+4
  NN = N+4
  NN = N+4
  NDC = N+4
  ND = NDC+4
  THESE PARAMETERS SEPARATE THE WORKING SPACE ARRAY M

  DD = 0.0
  DSS = DSTEP+DSTEP
  DM = DMAX+DMAX
  DMN = 4.0+DM
  IS = 5
  IS CONTROLS A GO TO STATEMENT FOLLOWING A CALL OF CALFUN
  TINC = 1.0
  TINC IS USED IN THE CRITERION TO INCREASE THE STEP LENGTH
  START A NEW PAGE FOR PRINTING
  IF IPRINT) 1,1785
  85 WRITE(6,86)
  86 FORMAT(I17)

```



[illegible]



```

INFINITE FLAT PLATE
      DO 1001 J = 1,N
      1001 AJINV(I,J) = AJINV(I,J)
C
C      START ITERATION BY PREDICTING THE DESCENT AND NEWTON MINIMA
C
      10 DS = 0.0
      11 GN = 0.0
      12 SP = 0.0
      13 DO 30 I=1,N
      14 XI(I) = 0.0
      15 FI(I) = 0.0
      16 ME = 1
      17 DO 40 J=1,N
      18 NP(J) = NF + J
      19 XI(I) = XI(I) - XI(I)*NP(J)
      20 FI(I) = FI(I) - AJINV(I,J)*NP(J)
      21 ME = ME*N
      22 40 CONTINUE
      23 DS = DS + XI(I)*XI(I)
      24 GN = GN*FI(I)*FI(I)
      25 SP = SP*XI(I)*FI(I)
      26 30 CONTINUE
C
C      TEST WHETHER A NEARBY STATIONARY POINT IS PREDICTED
C
      27 IF (FI(1)-GN*DS) 41,41,42
      28 IF (FI(1)-GN*DS) 41,41,42
C
C      IF SO THEN RETURN OR REVISE JACOBIAN
C
      29 GO TO 43
      30 WRITE (6,*)
      31 FORMAT (1H, 6X, 'ERROR RETURN BECAUSE A NEARBY STATIONARY POINT
      32 OF FIX IS PREDICTED')
      33 NTST = 0
      34 GO TO 17
      35 DO 46 I=1,N
      36 XI(I) = XI(I)
      37 46 CONTINUE
      38 GO TO 32
C
C      TEST WHETHER TO APPLY THE FULL NEWTON CORRECTION
C
      41 IS = 2
      42 IF (GN-DS) 47,47,48
      43 DO 44 AXI(1,DS)
      44 DS = 25*DS
      45 TINC = 1.0
      46 IF (DS-DS) 49,49,50
      47 IS = 4
      48 GO TO 80
C
C      CALCULATE THE LENGTH OF THE STEEPEST DESCENT STEP
C
      49 ME = 0
      50 DS = 0.0
      51 I=1,N
      52 52

```

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INFINITE FLAT PLATE

00472	2230	00 52 0-0	
00473	2240	00 52 0-1,N	
00474	2250	N = N+1	
00475	2260	00 = 00 + MIN(X,F1)	
00476	2270	52 CONTINUE	
00500	2280	DMULT = DMULT*DM*DU	
00501	2290	51 CONTINUE	
00502	2300	DMULT = DS/DMULT	
00503	2310	DS = DS + DMULT*DMULT	
00504	2320		
00505	2330		
00506	2340		
00507	2350	TEST WHETHER TO USE THE STEEPEST DESCENT DIRECTION	
00508	2360	IF(DS-0.01) 53,54,55	
00509	2370		
00510	2380	TEST WHETHER INITIAL VALUE OF DD HAS BEEN SET	
00511	2390		
00512	2400	54 IF(DD) 55,55,56	
00513	2410	55 DD = MAX(DS,AMIN(DM,DS))	
00514	2420	DS = DS/DMULT	
00515	2430	60 GO 41	
00516	2440		
00517	2450	SET THE MULTIPLIER OF THE STEEPEST DESCENT DIRECTION	
00518	2460		
00519	2470	56 ANNULE = 0-0	
00520	2480	DMULT = DMULT*SORTDD/DS	
00521	2490	60 TO 98	
00522	2500		
00523	2510	INTERPOLATE BETWEEN STEEPEST DESCENT AND NEWTON DIRECTIONS	
00524	2520	53 SP = SP*DMULT	
00525	2530	ANNULE = (DD-DS)/(SP-DS) + SORTDD*(DS-0.01)/(DD-DS)	
00526	2540	DMULT = DMULT*(1.0-ANNULE)	
00527	2550		
00528	2560	CALCULATE THE CHANGE IN X AND ITS ANGLE WITH THE FIRST DIRECTION	
00529	2570		
00530	2580	98 DM = 0-0	
00531	2590	SP = 0-0	
00532	2600	00 57 1-1,N	
00533	2610	F11 = DMULT*(X11) + ANNULE*(F1)	
00534	2620	ONE ON F11*(F11)	
00535	2630	NDPI = ND + 1	
00536	2640	SP = SP*(1+NDPI)	
00537	2650	57 CONTINUE	
00538	2660	DS = .25* DM	
00539	2670		
00540	2680	TEST WHETHER AN EXTRA STEP IS NEEDED FOR INDEPENDENCE	
00541	2690		
00542	2700	IF(MINDC(1)-DPLST) 58,58,59	
00543	2710	58 IF(SP-DS) 60,58,58	
00544	2720		
00545	2730	TAKE THE EXTRA STEP AND UPDATE THE DIRECTION MATRIX	
00546	2740		
00547	2750	60 15 1-1	
00548	2760	00 51 1-1,N	
00549	2770	NXP = NX + 1	
00550	2780	NODI = NOD + 1	
00551	2790	NPI = NI + 1	

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## INFINITE FLAT PLATE

```

00557 239  X(1) = MINCP(1) + DS(1)*MINCP(1)
00558 240  MINCP(1) = MINCP(1) + 1.0
00559 241  61 CONTINUE
00560 242  WIND(1) = 1.0
00561 243  DO 62 I=1,N
00562 244  W(1) = 1.0
00563 245  SP = W(1)
00564 246  DO 63 J=1,M
00565 247  DD(63) = J+M
00566 248  KPN = K + M
00567 249  W(1) = MINCP(1)
00568 250  W(1) = MINCP(1)
00569 251  63 CONTINUE
00570 252  W(1) = SP
00571 253  62 CONTINUE
00572 254  GO TO 1
00573 255  C
00574 256  C
00575 257  C
00576 258  C
00577 259  C
00578 260  C
00579 261  C
00580 262  C
00581 263  C
00582 264  C
00583 265  C
00584 266  C
00585 267  C
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00991 673  C
00992 674  C
00993 675  C
00994 676  C
00995 677  C
00996 678  C
00997 679  C
00998 680  C
00999 681  C
01000 682  C

```



IMPAIRED TO INCREASE THE STEP LENGTH

Address	Hex	Assembly
00767	3940	
00767	3950	
00767	3950	
00772	3960	
00772	3960	
00773	3970	
00773	3970	
00774	3980	
00774	3980	
00777	3990	
00777	3990	
01000	4000	
01000	4000	
01001	4010	
01001	4010	
01002	4020	
01002	4020	
01009	4030	
01009	4030	
01005	4040	
01005	4040	
01006	4050	
01006	4050	
01007	4060	
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01045	4650	
01045	4660	
01045	4660	

DATE 082774 PAGE 13

## INFINITE FLAT PLATE

```

01072 4510 33 0.0
01076 4520 DO 92 I=1,N
01077 4530 DS = 0.7
01100 4540 DO 93 J=1,N
01101 4550 DS = DS + AJINVIJ,1300(J)
01102 4560 03 CONTINUE
01106 4570 SP = SP + DS*F(I)
01107 4580 SS = SS + X(I)*F(I)
01108 4590 F(I) = 0.5
01110 4600 02 CONTINUE
01111 4610 CMULT = 1.0
01112 4620 IF (ABS(SS)-.1055) 94,95,95
01114 4630 94 CMULT = 7.0
01117 4640 05 IJ = CMULT/SS
01120 4650 PA = CMULT/CMULT*SP+.110-CMULT*SS
01121 4660 K = 0
01122 4670 DO 96 I=1,N
01123 4680 WAPJ = WAP + 1
01126 4690 WAPJ = WAP + 1
01127 4700 SP = SP+WAPJ
01130 4710 SS = SP+WAPJ
01131 4720 DO 97 J=1,N
01132 4730 W = W + 1
01135 4740 WAPJ = WAPJ+SP*W
01137 4750 AJINVIJ,1300(J)
01140 4760 07 CONTINUE
01142 4770 06 CONTINUE
01144 4780 GO TO 34
01145 4790 END

```

END OF COMPILATION NO DIAGNOSTICS.









# ORIGINAL SOURCE

## OF DATA

INFINITE FLAT PLATE

DATE 082774

PAGE 15

FOR IS CAL

FOR C11A-082774-17 12 56 (C)

SUBROUTINE CALCON ENTRY POINT 001236

STORAGE USED CODE(1) 001262; DATA(1) 000361; BLANK COMMON(12) 000000

COMMON BLOCKS

0003 A 061301  
 0004 B 061301  
 0005 C 165140  
 0006 D 061301

EXTERNAL REFERENCES (BLOCK, NAME)

0007 SORT  
 0010 MERRIS

STORAGE ASSIGNMENT (BLOCK, TYPE, RELATIVE LOCATION, NAME)

0001 000255 1276 0001 000425 1446 0001 000530 1546 0001 000677 1766  
 0001 000747 2046 0001 001012 2126 0001 001061 2206 0001 001162 2346  
 0001 000470 621 0004 000000 AJ1M 0000 R 030243 AL 0000 P 000241 D  
 0000 000262 INJPS 0003 I 030245 IS 0000 I 000244 M 0000 R 000247 MR  
 0000 R 000237 NS 0000 W 000242 PSIG 0003 000000 Y 0000 R 000240 US  
 0005 000000 V

COMPILER IN=1

SUBROUTINE CALCON(V,F)

DIMENSION U(159)

DIMENSION Y(159)

DIMENSION F(159)

COMMON/A/T(159,159)

COMMON/B/AJ1M(159,159)

COMMON/C/W(16000)

COMMON/D/BJ1M(159,159)

REAL NS

NS=1.

US=NS+2

D=-002

PSIG=NS/2.

AL=PSIG/10.

C ALL STATEMENT NUMBERS LOCAL TO CAL

C DEFINE F(1) IN TERMS OF Y(1)

50 U(1)=AL+2/US-D+Y(1)-4.1+2

IF U(1)-LE.O-DU(1)=O.O

F(1)=Y(1)+68-Y(15)+Y(1)+3.

Y(1)=2+O-D-5+SORT(U(1))-Y(1)+O+Y(12)+4.1/2.

Z(1)=O+Y(12)-4.1+2-8.-AL+2/US/8.

INFINITE FLAT PLATE

DATE 002779 PAGE

[illegible]

	INFINITE FLAT PLATE	DATE 092774	PAGE 17
00231	80*		
00235	81*		
00236	82*		
00236	83*		
00237	84*		
00241	85*		
00242	86*		

```

22 CONTINUE
DO 130 M=159,159
  FMT=YK1000-FIX10030YU-151-DAYIN1002
  1-DAYIN+IVIN-111/2,0-DYIN-11002/9.
  130 CONTINUE
  RETURN
END

```

END OF COMPILATION NO DIAGNOSTICS.

DATE 082774 PAGE 995

# ORIGINAL PAGE IS OF POOR QUALITY

## INFINITE FLAT PLATE

142 -35502090-01 --10223294-01  
143 -31082110-01 --20614537-02  
144 -35507895-01 --99112722-02  
145 -23763375-01 --85941342-02  
146 -21749562-01 --85690398-02  
147 -17930298-01 --44024225-02  
148 -11946247-01 --27326857-02  
149 -3203375-01 --25541993-01  
THE SUM OF SQUARES IS .28419073-01  
AT THE 247 TH CALL OF CALC IN WE HAVE  
F(12)

I

XII

1 -35756208-01 --25943897-01  
2 -3693167-01 --11893987-01  
3 -3131326-01 --22705568-02  
4 -26524121-01 --12444356-01  
5 -34702245-01 --11217318-01  
6 -22716574-01 --53595324-02  
7 -18692573-01 --47812623-02  
8 -15520390-01 --55619132-02  
9 -1303920-01 --26925764-02  
10 -10592116-01 --32782186-03  
11 -13403279-01 --50723555-03  
12 -1212715-01 --40999346-03  
13 -10155921-01 --18096924-02  
14 -10281590-01 --16916617-02  
15 -10339740-01 --76844120-03  
16 -1658476-01 --43987804-01  
17 -26901187-01 --22641685-01  
18 -4126145-01 --11711255-01  
19 -2437401-01 --23134743-01  
20 -24518697-01 --19077322-01  
21 -22536223-01 --10415060-01  
22 -14799610-01 --76425035-02  
23 -1260587-01 --5163511-02  
24 -1268019-01 --13625547-02  
25 -12113753-01 --94485866-03  
26 -9214919-01 --53441818-03  
27 -27148565-01 --55613314-03  
28 -26761750-01 --73801924-03  
29 -95789875-01 --11344055-02  
30 -95165323-01 --43603234-03  
31 -13479794-01 --40374468-01  
32 -5415480-01 --20637518-01  
33 -31219312-01 --61907623-02  
34 -26553943-01 --27038824-01  
35 -24150747-01 --15187123-01  
36 -18628429-01 --70203774-02  
37 -15024835-01 --24964997-02  
38 -12279647-01 --27543803-02  
39 -93016921-01 --9215371-03  
40 -91761503-01 --27313177-04  
41 -91057323-01 --51264857-03  
42 -90310314-01 --55634428-03  
43 -49835249-01 --30165501-03  
44  
45

DATE 082778 PAGE 996

## INFINITE FLAT PLATE

46	-38388188+01	-38706297-01
47	-36780452+01	-20197899-01
48	-31201432+01	-89057230-02
49	-26188053+01	-16703597-01
50	-242221447+01	-13602154-01
51	-22222895+01	-87 79557-02
52	-18475638+01	-4 987181-02
53	-14799536+01	-86388752-02
54	-11874722+01	-38466383-02
55	-90510487+00	-56023805-03
56	-68231392+00	-38250503-03
57	-86017717+00	-20055662-03
58	-85280239+00	-44289521-04
59	-84510340+00	-10085039-03
60	-84014207+00	-57532958-04
61	-38310136+01	-2638608-01
62	-36476018+01	-20513883-01
63	-31169728+01	-61903790-02
64	-26057286+01	-1524898-01
65	-24101633+01	-12482065-01
66	-22105391+01	-77308029-02
67	-18336881+01	-81287756-02
68	-14599760+01	-3890658-02
69	-1139441+01	-28453780-02
70	-8945985+00	-19575331-03
71	-8203443+00	-56284290-03
72	-7977782+00	-35806775-03
73	-79068265+00	-39780119-03
74	-78315047+00	-2732580-03
75	-77819248+00	-2172752-03
76	-3824888+01	-35651930-01
77	-36622369+01	-14936249-01
78	-31142508+01	-61575244-02
79	-25980272+01	-15174482-01
80	-23999427+01	-11578275-01
81	-21998200+01	-76504316-02
82	-18212293+01	-55705432-02
83	-14423754+01	-2572987-02
84	-10862246+01	-32284358-02
85	-77541749+00	-25583759-02
86	-75107636+00	-24852378-03
87	-72831628+00	-1308171-03
88	-72350990+00	-95529417-04
89	-71457072+00	-59446591-04
90	-70702825+00	-96217276-05
91	-68192244+01	-35782138-01
92	-65577310+01	-20363048-01
93	-63119849+01	-75230513-02
94	-6013869+01	-14678319-01
95	-57198612+01	-17716965-01
96	-54107416+01	-80629537-02
97	-51265759+01	-73292132-02
98	-48252684+01	-35431104-02
99	-45706470+00	-23450935-02
100	-43723223+00	-17705861-03
101	-41723223+00	-97315728-03
102	-40040720+00	-27966634-03

997

PAGE

DATE 082779

## INFINITE FLAT PLATE

102	0.6941901+00	2702304-03
103	63629708+00	2928274-03
104	63766577+00	15301102-03
105	38152350+01	31873726-01
106	36543093+01	20015015-01
107	31102727+01	62071178-02
108	25567629+01	15182895-01
109	21846911+01	12317716-01
110	2137790+01	84554983-02
111	18028988+01	61725041-02
112	14139583+01	15246652-02
113	95452069+00	87481745-03
114	62458644+00	87672418-03
115	58187600+00	26508491-03
116	55969283+00	38865030-03
117	55448864+00	33286708-03
118	54930135+00	30949425-03
119	54621821+00	30219442-03
120	36123794+01	34852651-01
121	36319618+01	16660110-01
122	31090327+01	67789138-02
123	25812305+01	1583001-01
124	23798207+01	1353847-01
125	21786797+01	89943574-02
126	17973654+01	58854267-02
127	1403501+01	23707625-02
128	8764081+00	21822436-02
129	49678179+00	58371871-03
130	47661173+00	48337271-04
131	45596735+00	14605951-03
132	45172288+00	86756361-04
133	44739817+00	44401193-04
134	44599961+00	30522881-04
135	38107646+01	37951167-01
136	36505533+01	19526803-01
137	31083069+01	84611035-02
138	2581789+01	16796501-01
139	23769747+01	14634226-01
140	21756909+01	96733702-02
141	17939216+01	65851919-02
142	13076636+01	42003277-02
143	79864386+00	26023505-02
144	35883618+00	77200018-03
145	34218295+00	83770400-03
146	32432985+00	5306468-03
147	32055951+00	49848927-03
148	31593683+00	40657101-03
149	31502046+00	40653087-03
150	31005192+01	14179488-01
151	36502033+01	10307302-01
152	31082098+01	19307238-02
153	25807864+01	99584091-02
154	23763276+01	85446792-02
155	21749593+01	5677543-02
156	17930288+01	48125743-02
157	15956358+01	27904659-02
158	72634797+00	2539310-01
159		

# ORIGINAL PAGE IS OF POOR QUALITY

FOR IS MAIN  
FOR 311A-11104/74-15 07 30 (0.0)

MAIN PROGRAM

STORAGE USED CODE(1) 001001 DATA(0) 001044 SLAN\* COMMON(2) 000000

EXTERNAL REFERENCES (BLOCK NAME)

0003 NINTPS  
0004 NDEUS  
0005 NIOIS  
0006 NIOZS  
0007 SQRT  
0010 NUCUS  
0011 NSTOPS

STORAGE ASSIGNMENT (BLOCK, TYPE, RELATIVE LOCATION, NAME)

BLOCK	TYPE	RELATIVE LOCATION	NAME
0000	000772	100F	0001 000032 1206
0001	000423	1740	0001 000467 2056
0001	000773	2510	0001 000774 26F
0001	000782	99L	0001 000782 99L
0001	000787	15	0001 000787 15
0001	000786	MM	0001 000786 MM
0001	000787	US	0001 000787 US
0001	000162	1866	0001 000162 1866
0001	000602	2226	0001 000602 2226
0001	000053	SOL	0001 000053 SOL
0001	000760	D	0001 000760 D
0001	000766	M	0001 000766 M
0001	000761	PSIG	0001 000761 PSIG
0001	000345	1846	0001 000345 1846
0001	000712	2326	0001 000712 2326
0001	001005	8F	0001 001005 8F
0001	000771	I	0001 000771 I
0001	000755	NO	0001 000755 NO
0001	000000	U	0001 000000 U

0001 10  
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0001 1000





[illegible]

## END OF COMPILATION

100-405015-240  
 100-405015-240  
 100-405015-240

ADDRESS	WORDS	WORDS	WORDS
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[illegible]

ORIGINAL PAGE IS  
OF POOR QUALITY

510) 043616 044661  
512) BLANKSCOMMON

511) 010534 011534

514

SYSTEMS. LEVEL 109-11  
END OF COLLECTION - TIME 1.788 SECONDS  
AT THE 1000 TH ITERATION WE HAVE  
1 211)

1 .129160000000  
2 .135571900000  
3 .159786710000  
4 .188211340000  
5 .202910218000  
6 .221122200000  
7 .267165780000  
8 .340900180000  
9 .482654500000  
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ORIGINAL PAGES  
OF FOUR QUALITY

49	.0C+0001-01
50	.0002065-01
51	.1111750-00
52	.1317700-00
53	.1421010-00
54	.1554022-00
55	.1681100-00
56	.2436026-00
57	.2774052-00
58	.2852330-00
59	.1235145-01
60	.1740306-01
61	.2254020-01
62	.2741700-01
63	.2105903-01
64	.2501770-01
65	.2750970-01
66	.0141147-01
67	.0591965-01
68	.1109039-00
69	.1210598-00
70	.1312041-00
71	.1610065-00
72	.2101000-00
73	.3350000-00
74	.7109171-00
75	.1200010-01
76	.1710000-01
77	.2228151-01
78	.2711191-01
79	.3107911-01
80	.6252712-01
81	.6609341-01
82	.6757000-01
83	.7096350-01
84	.0003000-01
85	.1010000-00
86	.1110075-00
87	.1307005-00
88	.1700000-00
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104	.7600000-01
105	.8100000-01

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 149 .23327000+01  
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 151 .27120000+01  
 152 .34105710+01  
 153 .40125718+01  
 154 .28481440+00  
 155 .44482380+00  
 156 .34486770+01  
 157 .10121690+01  
 158 .24241166+01  
 159 .20667200+01  
 160 .45546096+00  
 161 .11406666+01  
 162 .16194666+01

100-443427-27624956-01

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#### IV. INFINITE PLATE/FINE MESH

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# ORIGINAL PAGE IS OF POOR QUALITY

V. T AND Z COMPUTER PROGRAM/FINITE PLATE/(R<sub>0</sub>/L = 1/2)

DATE 120374 PAGE 2

FINITE PLATE

FOR IS MAIN  
FOR D11A-12/03/74-12 56 39 1.03

MAIN PROGRAM

STORAGE USED CODE(1) 000050: DATA(1) 017271: BLANK COMMON(2) 000000

EXTERNAL REFERENCES (BLOCK, NAME)

0003 FOMS  
0004 MINIRS  
0005 MROUS  
0006 MIOIS  
0007 MIOZS  
0010 MSTOPA

STORAGE ASSIGNMENT (BLOCK, TYPE, RELATIVE LOCATION, NAME)

0000 017261 100F 0001 000014 1076 0000 R 017256 ACC  
0000 R 000062 F 0000 017254 IPRINT 0000 I 017253 J  
0000 W 017255 STEP 0000 R 000050 M 0000 R 000000 X

0000 R 000144 AJINV 0000 R 01726C DMAX  
0000 I 017257 MAXFUN 0000 I 017252 N

0101 10 DIMENSION N150,F(50),AJINV150,50,M152501  
0103 20 100 FORMAT (8F10.2)  
0104 30 N=4  
0105 40 READ(5,100)(X(J),J=1,N)  
0113 50 IPRINT=1  
0114 60 STEP=001  
0115 70 ACC=00001  
0116 80 MAXFUN=200  
0117 90 DMAX=1.0  
0120 100 CALL COMSEN,X,F,AJINV,STEP,DMAX,ACC,MAXFUN,IPRINT,M)  
0121 110 END

END OF COMPILATION NO DIAGNOSTICS.











ORIGINAL PAGE IS  
OF POOR QUALITY

DATE 120374 PAGE 153

FIMTE PLATE

3	.26339348-01	.89025083-03
4	.20496580-01	.26680096-02
5	.10386839-01	.26348730-03
6	.10024565-01	.13316048-03
7	.94448553-00	.1335246-02
8	.99317597-00	.15506664-02
9	.39148330-01	.94371713-02
10	.33799877-01	.74407990-02
11	.26106225-01	.13415673-02
12	.20334443-01	.12815797-02
13	.95577931-00	.35519752-03
14	.89745270-00	.84258494-04
15	.80014006-00	.10337803-02
16	.88891198-00	.10970674-02
17	.5854268-01	.91589284-02
18	.33609975-01	.76580360-02
19	.25869103-01	.81492195-03
20	.20196086-01	.21348814-03
21	.75271550-00	.12450665-03
22	.7723162-00	.19464283-03
23	.76865365-05	.89114238-04
24	.76702218-00	.25911929-05
25	.38756332-01	.91446014-02
26	.33419447-01	.77525818-02
27	.25628153-01	.18746395-02
28	.20090393-01	.12175383-02
29	.72095893-03	.13866364-03
30	.63205345-00	.25432670-03
31	.62298401-00	.30392579-03
32	.62162420-00	.22793029-03
33	.38556731-01	.84254769-02
34	.33228296-01	.75184951-02
35	.25381564-01	.1358411-02
36	.20025854-01	.90075942-04
37	.54323023-00	.46073110-04
38	.43624437-00	.20977520-03
39	.42829492-00	.25629085-03
40	.42754654-00	.23420318-03
41	.38349743-01	.44051141-02
42	.23736727-01	.34352653-02
43	.25124594-01	.77474740-03
44	.24445411-00	.37299299-04

THE SUM OF SQUARES IS .66368485-03  
AT THE 161 TH CALL OF CALFUN WE HAVE  
F(11)

1	.19334570-01	.86902741-02
2	.33986154-01	.35526160-02
3	.26339348-01	.97243446-03
4	.22895302-01	.26114930-02
5	.13386733-01	.16562782-03
6	.15224502-01	.13255415-03
7	.94448553-00	.13623016-02
8	.99317597-00	.15613231-02
9	.39148330-01	.92544462-02
10	.33799877-01	.74521824-02
11	.26106225-01	.13167506-02

PROGRAM IS MAIN  
FOR 1119-12/24/74-11 29 57 (P)

MAIN PROGRAM

STORAGE USED CODE(1) 21105; DATA(0) 000324; BLANK COMMON(2) 000000

EXTERNAL REFERENCES (BLOCK, NAME)

0001 NINTPS  
0004 NRPUS  
0005 NIOIS  
0006 NIOZS  
0007 NRSUS  
0010 SORT  
0011 NSTOP5

STORAGE ASSIGNMENT INLOCN, TYPE, RELATIVE LOCATION, NAME

000	00046 1001	0001	000037 1226	0001	000051 1306	0001	000134 1516
001	000303 1706	0001	000016 2060	0001	000465 2176	0001	000566 2336
002	000250 246	0001	000347 30	0001	000060 501	0001	001103 991
003	000134 41	0001	000241 COUNT	0000	000261 8F	0000	000244 15
004	000246 17	0000	000240 J	0000	000242 I	0000	000227 K0
005	000230 44	0000	000235 N	0000	000237 ME	0000	000236 RD
006	000000 U	0000	000231 JS	0000	000233 PS16	0000	000236 RD
		0000	000062 Y	0000	000144 Z		

0101	10	DIMENSION U1501
0104	20	DIMENSION Y1501
0106	30	DIMENSION Z1501
0108	40	REAL N5
0109	50	REAL K0
0110	60	MM250
0111	70	NS11
0112	80	US250+2
0113	90	DE-0178
0114	100	PS16NS42
0115	110	AL-PS1075
0116	120	N495
0117	130	RO220
0118	140	MF244
0119	150	REAR15,1201 AYAU,JE1,NEP
0120	160	REAR15,1201 AYAU,JE1,NEP
0121	170	170 FORMATTED(10,21)
0122	180	W211.5
0123	190	INTEGER COUNT
0124	200	COUNT50
0125	210	50 COUNT-COUNT+1
0126	220	IF(COUNT-COUNT+1) GO TO 90
0127	230	THIS STATEMENT HAS TOO MANY LEFT PARENTHESES.
0128	240	70 FORMATTED(10,21) MAY THE 15,1975 IN ITERATION WE HAVE
0129	250	WRITE(16,26) COUNT
0130	260	

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250 01097
260 0150
270 0157
280 0160
290 0163
300 0166
310 0166
320 0166
330 0166
340 0167
350 0171
360 0172
370 0174
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580 0222
590 0224
600 0224
610 0227
620 0227
630 0230
640 0230
650 0230
660 0232
670 0235
680 0235
690 0235
700 0237
710 0237
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730 0241
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770 0243
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VI. FINITE PLATE/(R<sub>0</sub>/L) = 1/2

$\epsilon_1 = .075$	$\epsilon_2 = .085$	$\epsilon_3 = .051$	$\epsilon_4 = .050$	$\epsilon_5 = .047$	$\epsilon_6 = .113$	$\epsilon_7 = .111$	$\epsilon_8 = .111$
$\gamma_1 = 3.94$	$\gamma_2 = 3.40$	$\gamma_3 = 2.63$	$\gamma_4 = 2.04$	$\gamma_5 = 1.93$	$\gamma_6 = 1.09$	$\gamma_7 = .994$	$\gamma_8 = .994$
$\epsilon_9 = .077$	$\epsilon_{10} = .114$	$\epsilon_{11} = .043$	$\epsilon_{12} = .199$	$\epsilon_{13} = .559$	$\epsilon_{14} = 1.05$	$\epsilon_{15} = 1.05$	$\epsilon_{16} = .993$
$\gamma_9 = 1.91$	$\gamma_{10} = 1.47$	$\gamma_{11} = 2.61$	$\gamma_{12} = 2.93$	$\gamma_{13} = .958$	$\gamma_{14} = .892$	$\gamma_{15} = .879$	$\gamma_{16} = .883$
$\epsilon_{17} = .289$	$\epsilon_{18} = .143$	$\epsilon_{19} = .933$	$\epsilon_{20} = .151$	$\epsilon_{21} = .559$	$\epsilon_{22} = .958$	$\epsilon_{23} = 1.05$	$\epsilon_{24} = .993$
$\gamma_{17} = 3.02$	$\gamma_{18} = 3.46$	$\gamma_{19} = .96$	$\gamma_{20} = 2.01$	$\gamma_{21} = .832$	$\gamma_{22} = .775$	$\gamma_{23} = .668$	$\gamma_{24} = .672$
$\epsilon_{25} = .308$	$\epsilon_{26} = .173$	$\epsilon_{27} = .933$	$\epsilon_{28} = .151$	$\epsilon_{29} = .552$	$\epsilon_{30} = .957$	$\epsilon_{31} = 1.05$	$\epsilon_{32} = .993$
$\gamma_{25} = 3.52$	$\gamma_{26} = 3.45$	$\gamma_{27} = .96$	$\gamma_{28} = 2.00$	$\gamma_{29} = .750$	$\gamma_{30} = .672$	$\gamma_{31} = .672$	$\gamma_{32} = .672$
$\epsilon_{33} = .376$	$\epsilon_{34} = .173$	$\epsilon_{35} = .933$	$\epsilon_{36} = .151$	$\epsilon_{37} = .552$	$\epsilon_{38} = .957$	$\epsilon_{39} = 1.05$	$\epsilon_{40} = .993$
$\gamma_{33} = 3.85$	$\gamma_{34} = 3.45$	$\gamma_{35} = .96$	$\gamma_{36} = 2.00$	$\gamma_{37} = .750$	$\gamma_{38} = .672$	$\gamma_{39} = .672$	$\gamma_{40} = .672$
$\epsilon_{41} = .383$	$\epsilon_{42} = .173$	$\epsilon_{43} = .933$	$\epsilon_{44} = .151$	$\epsilon_{45} = .552$	$\epsilon_{46} = .957$	$\epsilon_{47} = 1.05$	$\epsilon_{48} = .993$
$\gamma_{41} = 3.85$	$\gamma_{42} = 3.45$	$\gamma_{43} = .96$	$\gamma_{44} = 2.00$	$\gamma_{45} = .750$	$\gamma_{46} = .672$	$\gamma_{47} = .672$	$\gamma_{48} = .672$

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FEDERAL BUREAU OF INVESTIGATION  
WASHINGTON, D.C. 20535

Year	1950	1951	1952	1953	1954	1955	1956	1957	1958	1959	1960	1961	1962	1963	1964	1965	1966	1967	1968	1969	1970	1971	1972	1973	1974	1975	1976	1977	1978	1979	1980	1981	1982	1983	1984	1985	1986	1987	1988	1989	1990	1991	1992	1993	1994	1995	1996	1997	1998	1999	2000	2001	2002	2003	2004	2005	2006	2007	2008	2009	2010	2011	2012	2013	2014	2015	2016	2017	2018	2019	2020	2021	2022	2023	2024	2025	2026	2027	2028	2029	2030	2031	2032	2033	2034	2035	2036	2037	2038	2039	2040	2041	2042	2043	2044	2045	2046	2047	2048	2049	2050	2051	2052	2053	2054	2055	2056	2057	2058	2059	2060	2061	2062	2063	2064	2065	2066	2067	2068	2069	2070	2071	2072	2073	2074	2075	2076	2077	2078	2079	2080	2081	2082	2083	2084	2085	2086	2087	2088	2089	2090	2091	2092	2093	2094	2095	2096	2097	2098	2099	2100
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**FIFTE PLATE**

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DATE 120578 PAGE 17

## FINITE PLATE

00225	89*	F(42)EY(42)000-Y(42)003+Y(34)*
00226	90*	Y(42)000+Y(42)003+Y(42)003+Y(42)003
00227	91*	Y(42)000+Y(42)003+Y(42)003+Y(42)003
00228	92*	Y(42)000+Y(42)003+Y(42)003+Y(42)003
00229	93*	Y(42)000+Y(42)003+Y(42)003+Y(42)003
00230	94*	Y(42)000+Y(42)003+Y(42)003+Y(42)003
00231	95*	Y(42)000+Y(42)003+Y(42)003+Y(42)003
00232	96*	Y(42)000+Y(42)003+Y(42)003+Y(42)003
00233	97*	Y(42)000+Y(42)003+Y(42)003+Y(42)003
00234	98*	Y(42)000+Y(42)003+Y(42)003+Y(42)003
00235	99*	Y(42)000+Y(42)003+Y(42)003+Y(42)003
00236	100*	Y(42)000+Y(42)003+Y(42)003+Y(42)003
00237	101*	Y(42)000+Y(42)003+Y(42)003+Y(42)003
00238	102*	Y(42)000+Y(42)003+Y(42)003+Y(42)003

END OF COMPILATION NO DIAGNOSTICS.

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DATE 12/5/74 PAGE 104

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SINTE PLATE		DATE	120574	PAGE	145
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22	24220353-01	21134575-03			
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24	23112169-00	24715135-03			
25	20222079-00	2728776-03			
26	22211327-00	21851113-03			
27	29240071-01	2304718-02			
28	21244011-01	22176419-02			
29	29127900-01	24076002-00			
30	23775028-01	2422077-03			
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## MAIN PROGRAM

STORAGE USED (CORE) 01115: DATA(0) 00025: PLAN( COMMONIZ) 00000

## EXTERNAL REFERENCES (BLOCK, NAME)

0003 NINTPS  
0006 NRDUS  
0008 NIOIS  
000A NIOZS  
0007 NRDUS  
0010 SQNT  
0011 NSTOPS

## STORAGE ASSIGNMENT (BLOCK, TYPE, RELATIVE LOCATION, NAME)

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0003 000003 1766 0001 000016 2266 0001 000465 2176 0001 000122 2256 0001 000566 2316  
0004 000000 167 0001 000347 2L 0001 000060 20L 0001 000123 8F 0001 001103 99L  
0005 000034 8L 0001 000241 0004Y 0001 000272 0 0001 000124 1 0001 000244 15  
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0007 000045 1F 0001 000240 0 0001 000243 M 0001 000125 1 0001 000227 K0  
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2157 250 8 FORMAT(1HP,4XIME,2X02(I7/(C55,C17,0))
2158 250 5RTE(6,3) (1,2(19,1E1,N)
2159 270 2(11E-1,4)
2160 280 DO 1 K=2,7
2161 290 UIM3=4*0.01**2ZUS-0*(ZIK+11)-ZIK-111**2
2162 300 IF(UIM3).LE.0.5 UIM3=0
2163 310 2IK=ZIK**2+2*(SORT(UIM3)/VIM3+2*(ZIK+8))/(C2*VIM3**2+0.3)+
2164 320 1*(ZIK+11)-ZIK-111/12*(VIM3**2+0.1)+
2165 330 2*(ZIK+11)-ZIK-111*(SORT(UIM3)/(UIM3+VIM3)+(VIM3+7/SORT(101)*SORT(103))
2166 340 1 CONTINUE
2167 350 UIM3=4*0.01**2ZUS-0*(UIC-ZIK11**2
2168 360 IF(UIM3).LE.0.5UIM3=0
2169 370 2(6)VIM3**2*(SORT(UIM3)/VIM3+2*(ZIK+11)/(C2*VIM3**2+0.3)+
2170 380 1*(UIC-ZIK11)/12*(VIM3**2+0.1)+
2171 390 2*(UIC-ZIK11)*SORT(UIM3)/(UIM3+VIM3)**2/SORT(101)*SORT(103))
2172 400 2(7) 429.43,0
2173 410 2(6)VIM3**2*(ZIK+11)-ZIK-111**2*(C2*VIM3**2+0.3)+
2174 420 1*(ZIK+11)-ZIK-111/12*(VIM3**2+0.1)+SORT(101)/12*(VIM3**2+0.1)+
2175 430 2*(ZIK+11)-ZIK-111*(SORT(UIM3)/(UIM3+VIM3)+(VIM3+7/SORT(101)*SORT(103))
2176 440 2 CONTINUE
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 171. MARKETING  
 172. SALES  
 173. RESEARCH  
 174. DEVELOPMENT  
 175. MANUFACTURING  
 176. DISTRIBUTION  
 177. FINANCIAL  
 178. LEGAL  
 179. ADMINISTRATIVE  
 180. OTHER  
 181. REMARKS  
 182. DATE  
 183. SIGNATURE  
 184. PRINTED NAME  
 185. TITLE  
 186. COMPANY  
 187. INDUSTRY  
 188. PRODUCTS  
 189. SERVICES  
 190. MARKETING  
 191. SALES  
 192. RESEARCH  
 193. DEVELOPMENT  
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 197. LEGAL  
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 199. OTHER  
 200. REMARKS  
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 202. SIGNATURE  
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[illegible]

ORIGINAL PAGE IS  
OF POOR QUALITY

43 --49109983\*E  
44 --11700000\*E  
45 --22100000\*E  
AT THE 249 TH ITERATION WE HAVE:  
Z(1)  
1 --18000000\*E  
2 --46180336\*E  
3 --33000133\*E  
4 --302452 \*E  
5 --57006993\*E  
6 --89335826\*E  
7 --17222387\*E  
8 --28459164\*E  
9 --10177222\*E  
10 --9065479\*E  
11 --36431603\*E  
12 --28277105\*E  
13 --47660211\*E  
14 --80372937\*E  
15 --16317861\*E  
16 --27757206\*E  
17 --18352173\*E  
18 --9315911\*E  
19 --39831503\*E  
20 --16244318\*E  
21 --37593754\*E  
22 --59001792\*E  
23 --16286178\*E  
24 --27026399\*E  
25 --16525366\*E  
26 --95684376\*E  
27 --42880629\*E  
28 --12166324\*E  
29 --26627696\*E  
30 --56893156\*E  
31 --15544137\*E  
32 --26144431\*E  
33 --14696506\*E  
34 --98240872\*E  
35 --45975687\*E  
36 --60706190\*E  
37 --14376329\*E  
38 --37423098\*E  
39 --14354850\*E  
40 --24927655\*E  
41 --14965498\*E  
42 --10082602\*E  
43 --49113024\*E  
44 --11000000\*E  
45 --22100000\*E

VIII. FINITE PLATE/(R<sub>0</sub>/L) = 3/4

1	2	3	4	5	6	7	8	A
z <sub>1</sub> = -1.40	z <sub>2</sub> = -1.887	z <sub>3</sub> = -1.341	z <sub>4</sub> = .296	z <sub>5</sub> = .597	z <sub>6</sub> = 1.04	z <sub>7</sub> = 1.88	z <sub>8</sub> = 2.94	E = 3.3 ν = 1
v <sub>1</sub> = 1.05	v <sub>2</sub> = 1.49	v <sub>3</sub> = 1.67	v <sub>4</sub> = 1.55	v <sub>5</sub> = 1.05	v <sub>6</sub> = 1.00	v <sub>7</sub> = .995	v <sub>8</sub> = .994	K = 3.3 r = .895
z <sub>9</sub> = -1.317	z <sub>10</sub> = -1.373	z <sub>11</sub> = -1.173	z <sub>12</sub> = .238	z <sub>13</sub> = .505	z <sub>14</sub> = .948	z <sub>15</sub> = 1.84	z <sub>16</sub> = 2.86	K = 3.3 r = .895
v <sub>9</sub> = 1.04	v <sub>10</sub> = 1.47	v <sub>11</sub> = 1.66	v <sub>12</sub> = 1.50	v <sub>13</sub> = .956	v <sub>14</sub> = .897	v <sub>15</sub> = .889	v <sub>16</sub> = .888	K = 3.3 r = .895
z <sub>17</sub> = -1.344	z <sub>18</sub> = -1.948	z <sub>19</sub> = -1.504	z <sub>20</sub> = .179	z <sub>21</sub> = .404	z <sub>22</sub> = .842	z <sub>23</sub> = 1.77	z <sub>24</sub> = 2.77	K = 3.3 r = .895
v <sub>17</sub> = 1.01	v <sub>18</sub> = 1.44	v <sub>19</sub> = 1.64	v <sub>20</sub> = 1.46	v <sub>21</sub> = .845	v <sub>22</sub> = .776	v <sub>23</sub> = .768	v <sub>24</sub> = .767	K = 3.3 r = .895
z <sub>25</sub> = -1.343	z <sub>26</sub> = -1.965	z <sub>27</sub> = -1.517	z <sub>28</sub> = .119	z <sub>29</sub> = .290	z <sub>30</sub> = .702	z <sub>31</sub> = 1.68	z <sub>32</sub> = 2.67	K = 3.3 r = .895
v <sub>25</sub> = 1.00	v <sub>26</sub> = 1.43	v <sub>27</sub> = 1.62	v <sub>28</sub> = 1.42	v <sub>29</sub> = .710	v <sub>30</sub> = .641	v <sub>31</sub> = .634	v <sub>32</sub> = .627	K = 3.3 r = .895
z <sub>33</sub> = -1.368	z <sub>34</sub> = -1.994	z <sub>35</sub> = -1.570	z <sub>36</sub> = .059	z <sub>37</sub> = .159	z <sub>38</sub> = .491	z <sub>39</sub> = 1.55	z <sub>40</sub> = 2.55	K = 3.3 r = .895
v <sub>33</sub> = 1.02	v <sub>34</sub> = 1.40	v <sub>35</sub> = 1.61	v <sub>36</sub> = 1.41	v <sub>37</sub> = .544	v <sub>38</sub> = .436	v <sub>39</sub> = .4289	v <sub>40</sub> = .428	K = 3.3 r = .895
z <sub>41</sub> = -1.384	z <sub>42</sub> = -2.013	z <sub>43</sub> = -1.604				z <sub>44</sub> = 1.40	z <sub>45</sub> = 2.40	K = 3.3 r = .895
v <sub>41</sub> = 1.06	v <sub>42</sub> = 1.38	v <sub>43</sub> = 1.59				v <sub>44</sub> = 1.40	v <sub>45</sub> = 1.40	K = 3.3 r = .895

## IX. COMPUTER LISTING/SURFACE TENSION MODEL

FINITE PLATE				
TOP.13 MAIN				
FOR D11A-08/10/75-17 35 58 (60)				
MAIN PROGRAM				
STORES USED CODE(1) 000000; DATA(0) 000000; BLANK COMMENTS 000000				
COMMON BLOCKS				
0001 A	057420			
0002	057420			
0003 C	165180			
0004 D	057420			
EXTERNAL REFERENCES (BLOCK, NAME)				
0007 FONS				
010 M1075				
011 M1075				
012 M1016				
013 M1016				
014 M1025				
015 M1025				
INTERNAL ASSIGNMENT BLOCK, TYPE, RELATIVE LOCATION, NAME				
000 000077 1705	1701	000017 1156	0000 000077 ACC	0004 000000 RJINA
000 000078 0000	0000	000000 0000	0000 000077 IPRINT	0000 000075 MARFUM
000 000079 0000	0000	000000 0000	0000 000077 STEP	0000 000000 X
COMPLETION(0000)				
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July 1943

FD-35 (4)

00-68970-15  
PC 107223

530345 USN 650122Z 147403 000005: 21844 0000042) 000000

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13 MAY 1961 2307Z 120000Z 70000Z

SECRET  
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STORAGE ASSIGNED BLOCK, TYPE, RELATIVE LOCATION, NAME)

0001	0000707	1635	00001	0000457	21
0001	000350	2330	0001	000195	2025
0001	000495	2730	0001	000715	3016
0001	002113	3316	0000	002151	3572
0000	000000	4154	0000	000078	41
0000	000475	7054	0000	000572	49
0000	000504	71	0000	000476	4
0000	000472	40	0003	000000	1

0004 000517 1466  
0001 001265 2765  
0001 001602 2450  
0001 001752 3230  
0000 001847 A  
0007 001951 F  
0000 002003 IS  
0000 002005 C  
0000 002010 X

0011	10	EMPIRE/EM11
0012	20	SO-CALTING CALIFORNIA, V.F.F
0013	30	EMPIRE/EM12
0014	40	EMPIRE/EM13
0015	50	EMPIRE/EM14
0016	60	EMPIRE/EM15
0017	70	EMPIRE/EM16
0018	80	EMPIRE/EM17
0019	90	EMPIRE/EM18
0020	100	EMPIRE/EM19
0021	110	EMPIRE/EM20
0022	120	EMPIRE/EM21
0023	130	EMPIRE/EM22
0024	140	EMPIRE/EM23
0025	150	EMPIRE/EM24
0026	160	EMPIRE/EM25
0027	170	EMPIRE/EM26
0028	180	EMPIRE/EM27
0029	190	EMPIRE/EM28
0030	200	EMPIRE/EM29





VINYL PLATE			DATE 06/1978	PAGE 33
00217	778	6 CONTINUE		
00221	780	15= 15 + 15		
00222	782	IF(15,15,122) 60 TO 5		
00224	800	DO 1.		
00225	810	DO 7 N=30,135,15		
00230	920	WRITE VIN(000-50VIN0000 VIN-150VIN0000		
00232	930	VIN(00200-0VIN-15)-VIN(15002/2,1-		
00233	940	2-50VIN0000SUP(12,0110-MANUAL)0VIN-130-		
00234	950	30450Y02-0110-00)0011-VIN-11002/2.		
00235	960	DO 12 N=1.		
00236	970	7 CONTINUE		
00237	980	DO 8 N=130,116		
00238	990	WRITE VIN(000-50VIN0000VIN-15)0VIN00200-10-VIN-15002/2.		
00239	1000	1-50VIN0000VIN(1150GR(12,0011) + 00VIN0013-50Y12,0013002/2.		
00240	1010	9 CONTINUE		
00241	1020	DO 9 N=137,139		
00242	1030	WRITE VIN(000-50VIN0000VIN-15)02/2.		
00243	1040	1VIN(00200-0VIN-15)002/20.1-50VIN0000VIN-1300		
00244	1050	204VIN(11-0VIN-11)002/2.		
00245	1060	9 CONTINUE		
00246	1070	DO 11 N=100,102		
00247	1080	WRITE VIN(000-50VIN0000VIN-15)0VIN001102/2.		
00248	1090	1VIN(00200-0VIN-15)002/20.1-50VIN0000VIN-13002/2.		
00249	1100	204VIN(11-0VIN-11)002/2.		
00250	1110	9 CONTINUE		
00251	1120	DO 12 N=107,109		
00252	1130	WRITE VIN(000-50VIN0000VIN-15)02/2.		
00253	1140	1VIN(00200-0VIN-15)002/20.1-50VIN0000VIN-13002/2.		
00254	1150	204VIN(11-0VIN-11)002/2.		
00255	1160	9 CONTINUE		
00256	1170	DO 13 N=107,109		
00257	1180	WRITE VIN(000-50VIN0000VIN-15)02/2.		
00258	1190	1VIN(00200-0VIN-15)002/20.1-50VIN0000VIN-13002/2.		
00259	1200	204VIN(11-0VIN-11)002/2.		
00260	1210	9 CONTINUE		
00261	1220	DO 14 N=107,109		
00262	1230	WRITE VIN(000-50VIN0000VIN-15)02/2.		
00263	1240	1VIN(00200-0VIN-15)002/20.1-50VIN0000VIN-13002/2.		
00264	1250	204VIN(11-0VIN-11)002/2.		
00265	1260	9 CONTINUE		
00266	1270	DO 15 N=107,109		
00267	1280	WRITE VIN(000-50VIN0000VIN-15)02/2.		
00268	1290	1VIN(00200-0VIN-15)002/20.1-50VIN0000VIN-13002/2.		
00269	1300	204VIN(11-0VIN-11)002/2.		
00270	1310	9 CONTINUE		
00271	1320	DO 16 N=107,109		
00272	1330	WRITE VIN(000-50VIN0000VIN-15)02/2.		
00273	1340	1VIN(00200-0VIN-15)002/20.1-50VIN0000VIN-13002/2.		
00274	1350	204VIN(11-0VIN-11)002/2.		
00275	1360	9 CONTINUE		
00276	1370	DO 17 N=107,109		
00277	1380	WRITE VIN(000-50VIN0000VIN-15)02/2.		
00278	1390	1VIN(00200-0VIN-15)002/20.1-50VIN0000VIN-13002/2.		
00279	1400	204VIN(11-0VIN-11)002/2.		
00280	1410	9 CONTINUE		
00281	1420	DO 18 N=107,109		
00282	1430	WRITE VIN(000-50VIN0000VIN-15)02/2.		
00283	1440	1VIN(00200-0VIN-15)002/20.1-50VIN0000VIN-13002/2.		
00284	1450	204VIN(11-0VIN-11)002/2.		
00285	1460	9 CONTINUE		
00286	1470	DO 19 N=107,109		
00287	1480	WRITE VIN(000-50VIN0000VIN-15)02/2.		
00288	1490	1VIN(00200-0VIN-15)002/20.1-50VIN0000VIN-13002/2.		
00289	1500	204VIN(11-0VIN-11)002/2.		
00290	1510	9 CONTINUE		
00291	1520	DO 20 N=107,109		
00292	1530	WRITE VIN(000-50VIN0000VIN-15)02/2.		
00293	1540	1VIN(00200-0VIN-15)002/20.1-50VIN0000VIN-13002/2.		
00294	1550	204VIN(11-0VIN-11)002/2.		
00295	1560	9 CONTINUE		
00296	1570	DO 21 N=107,109		
00297	1580	WRITE VIN(000-50VIN0000VIN-15)02/2.		
00298	1590	1VIN(00200-0VIN-15)002/20.1-50VIN0000VIN-13002/2.		
00299	1600	204VIN(11-0VIN-11)002/2.		
00300	1610	9 CONTINUE		

44-38861-10000  
JAN 24 1964  
FBI - NEW YORK

[illegible]

• 50115045419

CONFIDENTIAL

ORIGINAL PAGE IS  
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THIS VOLUME

FIVE PLATE		DATE 051075	PAGE 28
112	-1374948901	-10038509-02	
113	-2073448101	-00000000	
114	-1377627801	-38455729-02	
115	-8469666700	-32924126-02	
116	-5898817900	-40753812-03	
117	-5517953300	-32418407-03	
118	-5895467400	-58954602-04	
119	-5984669300	-83145680-05	
120	-5981075900	-77902000-05	
121	-4478877300	-13638503-03	
122	-4487765700	-19533507-03	
123	-4494287700	-15184014-03	
124	-4512025900	-14648568-03	
125	-4491245100	-44453074-03	
126	-5613103900	-36694615-02	
127	-1363414901	-3022110-02	
128	-20493901401	-00003000	
129	-1364761401	-33995814-02	
130	-5617159800	-36786389-02	
131	-4441264500	-44512353-03	
132	-4512023400	-14645684-03	
133	-4498285700	-15185056-03	
134	-4487764300	-14531991-03	
135	-4478877000	-13638160-03	
136	-3740262500	-37402606-03	
137	-3150147800	-31294888-03	
138	-3165775900	-30752484-03	
139	-3199643400	-28722718-03	
140	-3541916400	-14894305-03	
141	-4748997100	-45549141-02	
142	-1355160701	-28534887-02	
143	-2024845701	-00003000	
144	-1358929101	-33374926-02	
145	-4740632300	-45599598-02	
146	-3821849500	-14954713-03	
147	-3199644700	-24724359-03	
148	-3165775900	-36752497-03	
149	-3150147800	-33295525-03	
150	-3140262500	-30667049-03	
151	-2472576000	-15004302-02	
152	-4460184100	-30220743-02	
153	-1351774601	-13546498-02	
154	-1355633501	-16045955-02	
155	-4463295800	-30111035-02	
156	-2472602900	-15003054-02	
THE SUM OF SQUARES IS .63935093-03			
ERROR RETURN BECAUSE THERE HAVE BEEN 400 CALLS OF CALFUN			
THE FINAL SOLUTION REQUIRED 400 CALLS OF CALFUN AND 75			
F113			
1	-1000337301	-2655924-74	
2	-1000726601	-32745402-04	
3	-1001651001	-34843735-04	
4	-1005931501	-15685440-03	
5	-1019615401	-13530743-03	
6	-1029532701	-15972726-02	
7	-1024969801	-10145134-01	

0-3

FIVE CLIP

DATE 081075 PAGE 29

1	00000000	00000000
2	00000000	00000000
3	00000000	00000000
4	00000000	00000000
5	00000000	00000000
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7	00000000	00000000
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99	00000000	00000000
100	00000000	00000000

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FINITE PLATE		SITE 01075 PAGE 30	
55	7770512400	-22030730-01	
56	6551075800	-23063190-02	
57	1013513200	-03507060-02	
58	2100761100	-00000000	
59	1012000200	-03050110-02	
60	551302700	-23750750-02	
61	707200700	-22090000-03	
62	7705701000	-22060710-03	
63	770372700	-07270030-00	
64	7700000000	-20100000-00	
65	7700000000	-20000000-00	
66	7700000000	-20000000-00	
67	7700000000	-20000000-00	
68	7700000000	-20000000-00	
69	7700000000	-20000000-00	
70	7700000000	-20000000-00	
71	7700000000	-20000000-00	
72	7700000000	-20000000-00	
73	7700000000	-20000000-00	
74	7700000000	-20000000-00	
75	7700000000	-20000000-00	
76	7700000000	-20000000-00	
77	7700000000	-20000000-00	
78	7700000000	-20000000-00	
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85	7700000000	-20000000-00	
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98	7700000000	-20000000-00	
99	7700000000	-20000000-00	
100	7700000000	-20000000-00	
101	7700000000	-20000000-00	
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105	7700000000	-20000000-00	
106	7700000000	-20000000-00	
107	7700000000	-20000000-00	
108	7700000000	-20000000-00	
109	7700000000	-20000000-00	
110	7700000000	-20000000-00	
111	7700000000	-20000000-00	
112	7700000000	-20000000-00	
113	7700000000	-20000000-00	
114	7700000000	-20000000-00	
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116	7700000000	-20000000-00	
117	7700000000	-20000000-00	
118	7700000000	-20000000-00	
119	7700000000	-20000000-00	
120	7700000000	-20000000-00	

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	VALUE	DATE	PAGE	31
122	-0087760-00	-1052983-03		
123	-0092860-00	-15187012-03		
124	-0512021-00	-10651273-03		
125	-00912981-00	-00016998-03		
126	-0513100-00	-106190755-02		
127	-136-0151-01	-10195750-02		
128	-0093901-01	-00000000		
129	-13667589-01	-13596199-02		
130	-06711661-00	-106782055-02		
131	-00912796-00	-00076176-03		
132	-0512021-00	-10651188-03		
133	-0092860-00	-15183060-03		
134	-0087760-00	-10530419-03		
135	-05708760-00	-13637024-03		
136	-11002831-00	-10661240-03		
137	-11501483-00	-13295283-03		
138	-11657765-00	-10733011-03		
139	-11996497-00	-10723609-03		
140	-10819173-00	-10899262-03		
141	-07189087-00	-05508266-02		
142	-13531628-01	-10577865-02		
143	-20288457-01	-00003000		
144	-13589257-01	-13208710-02		
145	-07006639-00	-05598721-02		
146	-10819100-00	-10936355-03		
147	-11996496-00	-10725278-03		
148	-11657765-00	-10733011-03		
149	-11501483-00	-13295283-03		
150	-11002831-00	-10661240-03		
151	-10725278-00	-10500318-02		
152	-0087760-00	-1052983-02		
153	-13517915-01	-13566850-02		
154	-13539429-01	-10600320-02		
155	-00632924-00	-10113108-02		
156	-10725278-00	-10500318-02		
THE SUM OF SQUARES IS				-03937107-03

4F24

00100	1*	C	00/L=1/2
00001	3*		01M5838A Y11502
00002	3*		01M5838A Z11508
00100	3*		01A1 M0
00105	3*		00M=1000
00108	3*		02A8200
00109	3*		00M=0.00000000000001
00110	3*		00M=0
00111	3*		P310000
00112	3*		AL000310/10.

00111	110	
00112	110	N=156
00113	110	HEAD(5,100)I(0,0)J(1,N)
00114	110	READ(5,100)I(1,1)J(1,N)
00115	110	100 FORMAT(10,23)
00116	110	N=156
00117	110	INTEGER COUNT
00118	110	COUNT=0
00119	110	50 COUNT=COUNT+1
00120	110	IF(COUNT.EQ.50) GO TO 50
00121	110	COUNT=COUNT+1
00122	110	COUNT=COUNT+1
00123	110	COUNT=COUNT+1
00124	110	COUNT=COUNT+1
00125	110	COUNT=COUNT+1
00126	110	COUNT=COUNT+1
00127	110	COUNT=COUNT+1
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00221	110	COUNT=COUNT+1
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00226	110	COUNT=COUNT+1
00227	110	COUNT=COUNT+1
00228	110	COUNT=COUNT+1
00229	110	COUNT=COUNT+1
00230	110	COUNT=COUNT+1
00231	110	COUNT=COUNT+1
00232	110	COUNT=COUNT+1



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ORIGINAL PAGE  
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00954	1820	181012,0Y151002,2-SORTID0100-21010111/19,0Y151002,0011
00955	1821	DO 51 M=16,136,15
00956	1822	Z101=V101002,21010111/12,0Y151002,0011
00957	1823	10210111-1011/12,0Y151002,0011
00958	1824	21210111-1011/12,0Y151002,0011
00959	1825	51 CONTINUE
00960	1826	15217
00961	1827	52 17=15,12
00962	1828	DO 51 M=15,11
00963	1829	Z101=V101002,21010111/12,0Y151002,0011
00964	1830	10210111-1011/12,0Y151002,0011
00965	1831	21210111-1011/12,0Y151002,0011
00966	1832	51 CONTINUE
00967	1833	15217
00968	1834	52 17=15,12
00969	1835	DO 51 M=15,11
00970	1836	Z101=V101002,21010111/12,0Y151002,0011
00971	1837	10210111-1011/12,0Y151002,0011
00972	1838	21210111-1011/12,0Y151002,0011
00973	1839	51 CONTINUE
00974	1840	15217
00975	1841	52 17=15,12
00976	1842	DO 51 M=15,11
00977	1843	Z101=V101002,21010111/12,0Y151002,0011
00978	1844	10210111-1011/12,0Y151002,0011
00979	1845	21210111-1011/12,0Y151002,0011
00980	1846	51 CONTINUE
00981	1847	15217
00982	1848	52 17=15,12
00983	1849	DO 51 M=15,11
00984	1850	Z101=V101002,21010111/12,0Y151002,0011
00985	1851	10210111-1011/12,0Y151002,0011
00986	1852	21210111-1011/12,0Y151002,0011
00987	1853	51 CONTINUE
00988	1854	15217
00989	1855	52 17=15,12
00990	1856	DO 51 M=15,11
00991	1857	Z101=V101002,21010111/12,0Y151002,0011
00992	1858	10210111-1011/12,0Y151002,0011
00993	1859	21210111-1011/12,0Y151002,0011
00994	1860	51 CONTINUE
00995	1861	15217
00996	1862	52 17=15,12
00997	1863	DO 51 M=15,11
00998	1864	Z101=V101002,21010111/12,0Y151002,0011
00999	1865	10210111-1011/12,0Y151002,0011
01000	1866	21210111-1011/12,0Y151002,0011
01001	1867	51 CONTINUE
01002	1868	15217
01003	1869	52 17=15,12
01004	1870	DO 51 M=15,11
01005	1871	Z101=V101002,21010111/12,0Y151002,0011
01006	1872	10210111-1011/12,0Y151002,0011
01007	1873	21210111-1011/12,0Y151002,0011
01008	1874	51 CONTINUE
01009	1875	15217
01010	1876	52 17=15,12
01011	1877	DO 51 M=15,11
01012	1878	Z101=V101002,21010111/12,0Y151002,0011
01013	1879	10210111-1011/12,0Y151002,0011
01014	1880	21210111-1011/12,0Y151002,0011
01015	1881	51 CONTINUE
01016	1882	15217
01017	1883	52 17=15,12
01018	1884	DO 51 M=15,11
01019	1885	Z101=V101002,21010111/12,0Y151002,0011
01020	1886	10210111-1011/12,0Y151002,0011
01021	1887	21210111-1011/12,0Y151002,0011
01022	1888	51 CONTINUE
01023	1889	15217
01024	1890	52 17=15,12
01025	1891	DO 51 M=15,11
01026	1892	Z101=V101002,21010111/12,0Y151002,0011
01027	1893	10210111-1011/12,0Y151002,0011
01028	1894	21210111-1011/12,0Y151002,0011
01029	1895	51 CONTINUE
01030	1896	15217
01031	1897	52 17=15,12
01032	1898	DO 51 M=15,11
01033	1899	Z101=V101002,21010111/12,0Y151002,0011
01034	1900	10210111-1011/12,0Y151002,0011
01035	1901	21210111-1011/12,0Y151002,0011
01036	1902	51 CONTINUE
01037	1903	15217
01038	1904	52 17=15,12
01039	1905	DO 51 M=15,11
01040	1906	Z101=V101002,21010111/12,0Y151002,0011
01041	1907	10210111-1011/12,0Y151002,0011
01042	1908	21210111-1011/12,0Y151002,0011
01043	1909	51 CONTINUE
01044	1910	15217
01045	1911	52 17=15,12
01046	1912	DO 51 M=15,11
01047	1913	Z101=V101002,21010111/12,0Y151002,0011
01048	1914	10210111-1011/12,0Y151002,0011
01049	1915	21210111-1011/12,0Y151002,0011
01050	1916	51 CONTINUE
01051	1917	15217
01052	1918	52 17=15,12
01053	1919	DO 51 M=15,11
01054	1920	Z101=V101002,21010111/12,0Y151002,0011
01055	1921	10210111-1011/12,0Y151002,0011
01056	1922	21210111-1011/12,0Y151002,0011
01057	1923	51 CONTINUE
01058	1924	15217
01059	1925	52 17=15,12
01060	1926	DO 51 M=15,11
01061	1927	Z101=V101002,21010111/12,0Y151002,0011
01062	1928	10210111-1011/12,0Y151002,0011
01063	1929	21210111-1011/12,0Y151002,0011
01064	1930	51 CONTINUE
01065	1931	15217
01066	1932	52 17=15,12
01067	1933	DO 51 M=15,11
01068	1934	Z101=V101002,21010111/12,0Y151002,0011
01069	1935	10210111-1011/12,0Y151002,0011
01070	1936	21210111-1011/12,0Y151002,0011
01071	1937	51 CONTINUE
01072	1938	15217
01073	1939	52 17=15,12
01074	1940	DO 51 M=15,11
01075	1941	Z101=V101002,21010111/12,0Y151002,0011
01076	1942	10210111-1011/12,0Y151002,0011
01077	1943	21210111-1011/12,0Y151002,0011
01078	1944	51 CONTINUE
01079	1945	15217
01080	1946	52 17=15,12
01081	1947	DO 51 M=15,11
01082	1948	Z101=V101002,21010111/12,0Y151002,0011
01083	1949	10210111-1011/12,0Y151002,0011
01084	1950	21210111-1011/12,0Y151002,0011
01085	1951	51 CONTINUE
01086	1952	15217
01087	1953	52 17=15,12
01088	1954	DO 51 M=15,11
01089	1955	Z101=V101002,21010111/12,0Y151002,0011
01090	1956	10210111-1011/12,0Y151002,0011
01091	1957	21210111-1011/12,0Y151002,0011
01092	1958	51 CONTINUE
01093	1959	15217
01094	1960	52 17=15,12
01095	1961	DO 51 M=15,11
01096	1962	Z101=V101002,21010111/12,0Y151002,0011
01097	1963	10210111-1011/12,0Y151002,0011
01098	1964	21210111-1011/12,0Y151002,0011
01099	1965	51 CONTINUE
01100	1966	15217
01101	1967	52 17=15,12
01102	1968	DO 51 M=15,11
01103	1969	Z101=V101002,21010111/12,0Y151002,0011
01104	1970	10210111-1011/12,0Y151002,0011
01105	1971	21210111-1011/12,0Y151002,0011
01106	1972	51 CONTINUE
01107	1973	15217
01108	1974	52 17=15,12
01109	1975	DO 51 M=15,11
01110	1976	Z101=V101002,21010111/12,0Y151002,0011
01111	1977	10210111-1011/12,0Y151002,0011
01112	1978	21210111-1011/12,0Y151002,0011
01113	1979	51 CONTINUE
01114	1980	15217
01115	1981	52 17=15,12
01116	1982	DO 51 M=15,11
01117	1983	Z101=V101002,21010111/12,0Y151002,0011
01118	1984	10210111-1011/12,0Y151002,0011
01119	1985	21210111-1011/12,0Y151002,0011
01120	1986	51 CONTINUE
01121	1987	15217
01122	1988	52 17=15,12
01123	1989	DO 51 M=15,11
01124	1990	Z101=V101002,21010111/12,0Y151002,0011
01125	1991	10210111-1011/12,0Y151002,0011
01126	1992	21210111-1011/12,0Y151002,0011
01127	1993	51 CONTINUE
01128	1994	15217
01129	1995	52 17=15,12
01130	1996	DO 51 M=15,11
01131	1997	Z101=V101002,21010111/12,0Y151002,0011
01132	1998	10210111-1011/12,0Y151002,0011
01133	1999	21210111-1011/12,0Y151002,0011
01134	2000	51 CONTINUE
01135	2001	15217
01136	2002	52 17=15,12
01137	2003	DO 51 M=15,11
01138	2004	Z101=V101002,21010111/12,0Y151002,0011
01139	2005	10210111-1011/12,0Y151002,0011
01140	2006	21210111-1011/12,0Y151002,0011
01141	2007	51 CONTINUE
01142	2008	15217
01143	2009	52 17=15,12
01144	2010	DO 51 M=15,11
01145	2011	Z101=V101002,21010111/12,0Y151002,0011
01146	2012	10210111-1011/12,0Y151002,0011
01147	2013	21210111-1011/12,0Y151002,0011
01148	2014	51 CONTINUE
01149	2015	15217
01150	2016	52 17=15,12
01151	2017	DO 51 M=15,11
01152	2018	Z101=V101002,21010111/12,0Y151002,0011
01153	2019	10210111-1011/12,0Y151002,0011
01154	2020	21210111-1011/12,0Y151002,0011
01155	2021	51 CONTINUE
01156	2022	15217
01157	2023	52 17=15,12
01158	2024	DO 51 M=15,11
01159	2025	Z101=V101002,21010111/12,0Y151002,0011
01160	2026	10210111-1011/12,0Y151002,0011
01161	2027	21210111-1011/12,0Y151002,0011
01162	2028	51 CONTINUE
01163	2029	15217
01164	2030	52 17=15,12
01165	2031	DO 51 M=15,11
01166	2032	Z101=V101002,21010111/12,0Y151002,0011
01167	2033	10210111-1011/12,0Y151002,0011
01168	2034	21210111-1011/12,0Y151002,0011
01169	2035	51 CONTINUE
01170	2036	15217
01171	2037	52 17=15,12
01172	2038	DO 51 M=15,11
01173	2039	Z101=V101002,21010111/12,0Y151002,0011
01174	2040	10210111-1011/12,0Y151002,0011
01175	2041	21210111-1011/12,0Y151002,0011
01176	2042	51 CONTINUE
01177	2043	15217
01178	2044	52 17=15,12
01179	2045	DO 51 M=15,11
01180	2046	Z101=V101002,21010111/12,0Y151002,0011
01181	2047	10210111-1011/12,0Y151002,0011
01182	2048	21210111-1011/12,0Y151002,0011
01183	2049	51 CONTINUE
01184	2050	15217
01185	2051	52 17=15,12
01186	2052	DO 51 M=15,11
01187	2053	Z101=V101002,21010111/12,0Y151002,0011
01188	2054	10210111-1011/12,0Y151002,0011
01189	2055	21210111-1011/12,0Y151002,0011
01190	2056	51 CONTINUE
01191	2057	15217
01192	2058	52 17=15,12
01193	2059	DO 51 M=15,11
01194	2060	Z101=V101002,21010111/12,0Y151002,0011
01195	2061	10210111-1011/12,0Y151002,0011
01196	2062	21210111-1011/12,0Y151002,0011
01197	2063	51 CONTINUE
01198	2064	15217
01199	2065	52 17=15,12
01200	2066	DO 51 M=15,11
01201	2067	Z101=V101002,21010111/12,0Y151002,0011
01202	2068	10210111-1011/12,0Y151002,0011
01203	2069	21210111-1011/12,0Y151002,0011
01204	2070	51 CONTINUE
01205	2071	15217
01206	2072	52 17=15,12
01207	2073	

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ADDRESS LINE  
STREET ADDRESS

01768 01769  
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01772 BANK BUDS OFFICIAL  
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11/23/72 0000-5	5111 010122 010146	5121 001207 001302
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11/23/72 0000-7	5111 010210 010202	5121 001403 001500
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11/23/72 0000-9	5111 011393 010357	5121 001513 001514
11/23/72 0000-10	5111 011393 010357	5121 001515 001516
11/23/72 0000-11	5111 011393 010357	5121 001517 001518
11/23/72 0000-12	5111 011393 010357	5121 001519 001520
11/23/72 0000-13	5111 011393 010357	5121 001521 001522
11/23/72 0000-14	5111 011393 010357	5121 001523 001524
11/23/72 0000-15	5111 011393 010357	5121 001525 001526
11/23/72 0000-16	5111 011393 010357	5121 001527 001528
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11/23/72 0000-18	5111 011393 010357	5121 001531 001532
11/23/72 0000-19	5111 011393 010357	5121 001533 001534
11/23/72 0000-20	5111 011393 010357	5121 001535 001536
11/23/72 0000-21	5111 011393 010357	5121 001537 001538
11/23/72 0000-22	5111 011393 010357	5121 001539 001540
11/23/72 0000-23	5111 011393 010357	5121 001541 001542
11/23/72 0000-24	5111 011393 010357	5121 001543 001544
11/23/72 0000-25	5111 011393 010357	5121 001545 001546
11/23/72 0000-26	5111 011393 010357	5121 001547 001548
11/23/72 0000-27	5111 011393 010357	5121 001549 001550
11/23/72 0000-28	5111 011393 010357	5121 001551 001552
11/23/72 0000-29	5111 011393 010357	5121 001553 001554
11/23/72 0000-30	5111 011393 010357	5121 001555 001556
11/23/72 0000-31	5111 011393 010357	5121 001557 001558
11/23/72 0000-32	5111 011393 010357	5121 001559 001560
11/23/72 0000-33	5111 011393 010357	5121 001561 001562
11/23/72 0000-34	5111 011393 010357	5121 001563 001564
11/23/72 0000-35	5111 011393 010357	5121 001565 001566
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11/23/72 0000-41	5111 011393 010357	5121 001577 001578
11/23/72 0000-42	5111 011393 010357	5121 001579 001580
11/23/72 0000-43	5111 011393 010357	5121 001581 001582
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11/23/72 0000-50	5111 011393 010357	5121 001595 001596
11/23/72 0000-51	5111 011393 010357	5121 001597 001598
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11/23/72 0000-79	5111 011393 010357	5121 001653 001654
11/23/72 0000-80	5111 011393 010357	5121 001655 001656
11/23/72 0000-81	5111 011393 010357	5121 001657 001658
11/23/72 0000-82	5111 011393 010357	5121 001659 001660
11/23/72 0000-83	5111 011393 010357	5121 001661 001662
11/23/72 0000-84	5111 011393 010357	5121 001663 001664
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11/23/72 0000-87	5111 011393 010357	5121 001669 001670
11/23/72 0000-88	5111 011393 010357	5121 001671 001672
11/23/72 0000-89	5111 011393 010357	5121 001673 001674
11/23/72 0000-90	5111 011393 010357	5121 001675 001676
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SYSTEMS - LEVEL 100-11  
END OF COLLECTION - TIME 1.230 SLONES

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1	--5127282*01
2	--2779956*01
3	--2958878*01
4	--2271115*01
5	--1740465*01
6	--1399179*01
7	--5899288*00
8	--5000000
9	--5913397*00
10	--1188838*01
11	--1747012*01
12	--2107935*01
13	--2996851*01
14	--2775272*01
15	--2161288*01
16	--3100216*01
17	--2775188*01
18	--2939742*01
19	--2058525*01
20	--1711593*01
21	--1310619*01
22	--2920355*00
23	--2988352*05
24	--5803530*00
25	--1310291*01
26	--1712571*01
27	--2065071*01
28	--2932339*01
29	--2786298*01
30	--2153710*01
31	--2136726*01
32	--2767267*01
33	--2918023*01
34	--2030338*01
35	--1872932*01
36	--1273108*01

ORIGINAL PAGE IS  
OF POOR QUALITY

37	-33503012-00
38	-1329075-00
39	-5292087-00
40	-1271799-01
41	-10770883-01
42	-20330345-01
43	-2012008-01
44	-2770096-02
45	-11985700-01
46	-11300890-01
47	-2753171-01
48	-2393355-01
49	-20003567-01
50	-10270062-01
51	-1207001-01
52	-30306263-00
53	-1270302-00
54	-00081208-00
55	-12082104-01
56	-10300734-01
57	-20011084-01
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59	-27592870-01
60	-3139226-00
61	-31225151-01
62	-2730300-01
63	-23020001-01
64	-19093425-01
65	-15755559-01
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67	-03170882-00
68	-19325260-00
69	-29710712-00
70	-11349321-01
71	-15755598-01
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75	-01203000-01
76	-11110011-01
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78	-23287555-01
79	-19203065-01
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81	-01063500-01
82	-30033700-00
83	-10907013-00
84	-10603177-00
85	-10609327-01
86	-15111520-01
87	-10211158-01
88	-23200527-01
89	-27133370-01
90	-11350176-01
91	-03170883-01
92	-03010893-01
93	-22000750-01

ORIGIN: 1000  
05 1000 400000

94	-18850222-01
95	-18516820-01
96	-18516820-01
97	-18233620-00
98	-17001381-00
99	-12362361-00
100	-18728135-00
101	-18516716-01
102	-18491138-01
103	-2221897-01
104	-28921488-01
105	-31300457-01
106	-18728135-01
107	-2651895-01
108	-2221897-01
109	-17001381-01
110	-1321759-01
111	-18516820-00
112	-2583521-02
113	-18516820-00
114	-2583521-02
115	-85061176-00
116	-1321759-01
117	-17001381-01
118	-2221897-01
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120	-18728135-01
121	-18516820-01
122	-2583521-01
123	-21388525-01
124	-18516820-01
125	-18516820-01
126	-18516820-01
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146	-18516820-01
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148	-18516820-01
149	-18516820-01
150	-18516820-01

151 --26250000-01  
152 --17500000-01  
153 --87899999-00  
154 --87899999-00  
155 --17500000-01  
156 --26250000-01

2010



[illegible]

## XI. SURFACE TENSION DOMINATED z FORMULATION

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TABLE 1. - LIQUID PROPERTIES AT 20° C

Liquid	Surface tension, N/cm	Density, g/cm <sup>3</sup>	Absolute viscosity, g/cm-sec
Anhydrous ethanol	$22.3 \times 10^{-5}$	0.789	$1.200 \times 10^{-2}$
Trichlorotrifluoroethane	18.6	1.579	0.700
Distilled water	72.5	1.00	1.0037

TABLE 2. - SUMMARY OF PARAMETERS - ZERO GRAVITY

Test liquid	Nozzle radius, $R_0$ , cm	Disk radius, L, cm	Ratio, $R_0/L$	Velocity of jet, cm/sec	Reynolds number, $\rho V R_0 / \nu$	Weber number, $\rho V^2 R_0 / \sigma$	Flow category
Freon TF	0.25	1.0	0.23	34.3	1934	24.8	S
Freon TF				38.0	2133	30.5	S
Freon TF				43.7	2464	40.4	T
Ethanol				77.0	1278	52.2	T
Freon TF				50.5	2848	54.0	T
Ethanol				58.8	3316	73.4	T
Freon TF				101.0	1662	90.1	T
Ethanol				79.0	4460	113.2	T
Freon TF				131.3	2160	151.9	I
Ethanol				88.6	5000	161.5	I
Freon TF	.50	1.5	.33	149.8	2465	197.8	I
Ethanol				237.7	3911	498	I
Ethanol				282.2	4642	703	I
Ethanol				365.6	6014	1180	I
Ethanol				26.4	868	12.2	S
Ethanol				19.5	1815	16.1	S
Freon TF				37.7	1240	25.1	S
Ethanol				27.4	3090	31.8	T
Freon TF				46.0	1513	37.2	T
Ethanol				53.9	1773	51.2	T
Freon TF	.75	2.0	.38	37.6	4240	60.0	T
Ethanol				59.6	1900	62.0	T
Freon TF				42.75	4830	77.6	I

TABLE 2. - Concluded.

Test liquid	Nozzle radius, $R_o$ , cm	Disk radius, $L$ , cm	Ratio, $R_o/L$	Velocity of jet, cm/sec	Reynolds number, $\rho V R_o / \mu$	Weber number, $\rho V^2 R_o / \sigma$	Flow category
Ethanol	0.75	1.5	0.50	15.4	760	6.2	S
Ethanol	.75	1.5		19.1	942	9.6	S
Ethanol	.75	1.5		19.9	986	10.5	S
Ethanol	.50	1.0		26.4	868	12.2	S
Freon TF	.50	1.0		17.7	1996	13.2	S
Ethanol	.75	1.5		28.2	1891	21.0	S
Ethanol	.50	1.0		34.9	1148	21.3	T
Freon TF	.50	1.0		23.3	2628	23.0	T
Ethanol	.75	1.5		34.4	1697	31.2	T
Ethanol	.50	1.0		46.1	1516	37.4	T
Freon TF	.50	1.0		31.9	3490	43.2	T
Ethanol	.75	1.5		41.2	2036	44.7	I
Ethanol	.50	1.0		52.3	1720	48.2	T
Freon TF	.50	1.0		37.5	4230	59.5	I
Ethanol	.75	1.5		47.5	2347	59.6	I
Ethanol	.50	1.0		85.7	2820	129.0	I
Ethanol	.75	1.0	.75	12.7	630	4.2	S
Ethanol				22.5	1110	13.3	S
Ethanol				24.8	1227	16.2	S
Ethanol				27.3	1350	19.7	T
Ethanol				29.4	1454	22.9	T
Ethanol				32.0	1580	27.0	T
Ethanol				35.0	1730	32.3	T
Ethanol				39.1	1930	40.2	I



TABLE 3. - SUMMARY OF PARAMETERS - NORMAL GRAVITY

Test liquid	Nozzle radius, $R_o$ , cm	Disk radius, $L$ , cm	Ratio, $R_o/L$	Ratio, $H/R_o$	Weber number, $\rho V^2 R_o / \sigma$	Reynolds number, $\rho V R_o / \mu$	Bord number, $\rho g R_o^2 / \sigma$	Ratio, $R_o / R_o$
Distilled water	0.25	0.50	0.50	4	121	4775	0.852	19.96
		.50	.50	20		5261		22.56
		.75	.33	4		4775		22.88
		.75	.33	20		5261		24.68
		1.0	.25	4		4775		23.38
		1.0	.25	20		5261		25.0
		1.5	.167	4		4775		20.96
		1.5	.167	20		5261		22.78
		2.0	.125	4		4775		18.42
		2.0	.125	20		5261		19.14
	.50	.75	.667	2	26	3775	3.42	5.76
		.75	.667	10		5815		9.26
		1.0	.50	2		3775		5.86
		1.0	.50	10		5815		9.32
		1.5	.33	2		3775		6.33
		1.5	.33	10		5815		9.47
		2.0	.25	2		3775		5.03
		2.0	.25	10		5815		8.80
		.75	.667	2	44	4550	3.39	7.07
		.75	.667	5		5300		9.04
		.75	.667	10		6350		10.90
		1.0	.50	2		4550		8.34
		1.0	.50	10		6330		10.40
		1.5	.333	2		4550		8.33
		1.5	.333	10		6330		11.62
		2.0	.25	2		4550		7.88
		2.0	.25	10		6330		10.62
		.75	.667	2	102	6470	3.40	15.89
		.75	.667	10		7850		19.38
		1.0	.50	2		6470		16.34
		1.0	.50	10		7850		20.71
		1.5	.333	2		6470		16.72
		1.5	.333	10		7850		20.71
		2.0	.250	2		6470		16.34
		2.0	.250	10		7850		19.18

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TABLE 3. - Concluded.

Test liquid	Nozzle radius, $R_o$ , cm	Disk radius, $L$ , cm	Ratio, $R_o/L$	Ratio, $H/R_o$	Weber number, $V^2 R_o / \sigma$	Reynolds number, $VR_o/\nu$	Bond number, $PgR_o^3/\sigma$	Ratio, $R_p/R_o$
Distilled water	0.25	0.50	0.50	4	235	6573	0.852	35.14
		.50	.50	20		6922		38.80
		.75	.33	4		6573		38.50
		.75	.33	20		6922		43.86
		1.0	.25	4		6573		37.96
		1.0	.25	20		6922		41.56
		1.5	.167	4		6573		35.65
		1.5	.167	20		6922		38.27
		2.0	.125	4		6573		33.55
		.50	.50	4	62.5	1558	2.16	12.08
		.50	.50	20		2128		15.36
		.75	.33	20		2128		16.98
				4		1558		11.66
				4	157	2307		24.30
				20		2725		31.80
		1.0	.25	20		2725		36.76
Ethanol	0.25	1.0	.25	4		2307		23.28
		.50	.50	2	200	2520		24.92
				4		2571		24.12
				10		2720		27.12
				20		2953		29.82
		.125	.25	2	224	1857	.54	32.80
				4		1866		34.95
				10		1892		32.28
				20		1936		32.60
				?	177	1657		35.92
		.30		4		1667		36.87
		.50		10		1696		36.65
				20		1744		38.32
		.25	.50	4	213	2761	2.16	29.35
				20		3119		31.32
		.75	.33	20		3119		36.48
		.75	.33	4		2761		32.65
		1.0	.25	4		2761		32.75
		1.0	.25	20		3119		32.65

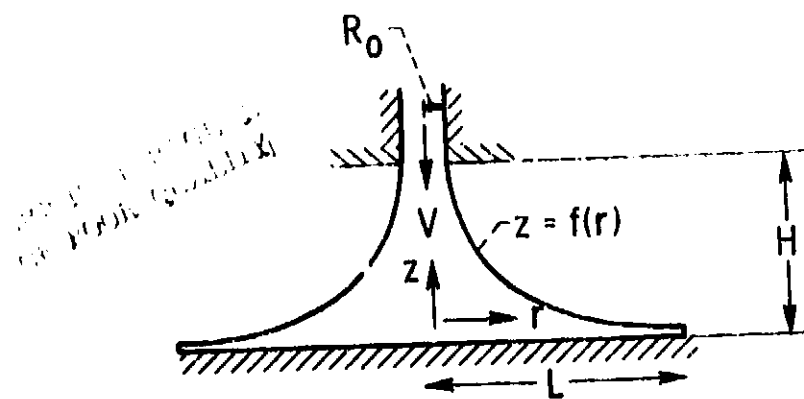


Figure 1. - Schematic of liquid jet impinging on a flat plate.

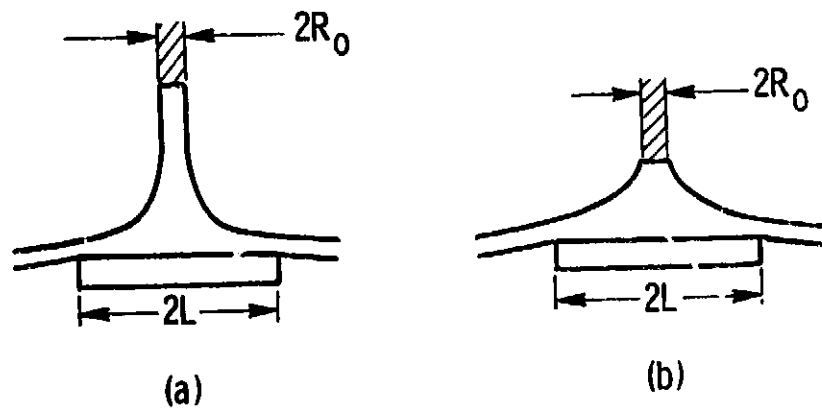


Figure 2. - Flow pattern as a function of nozzle height.

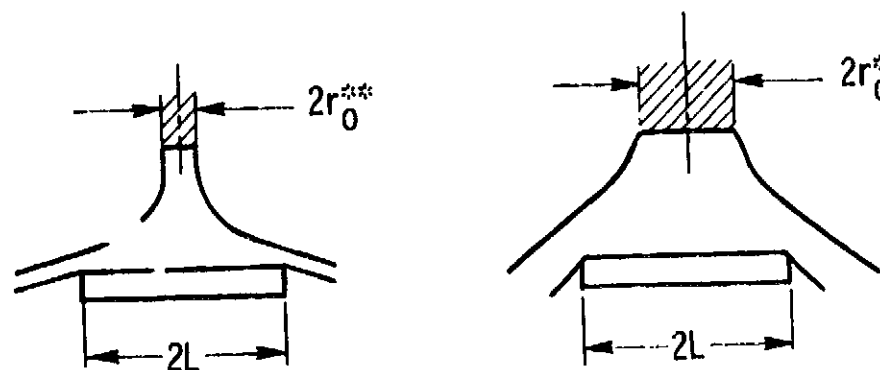


Figure 3. - Flow pattern as a function of jet radius.

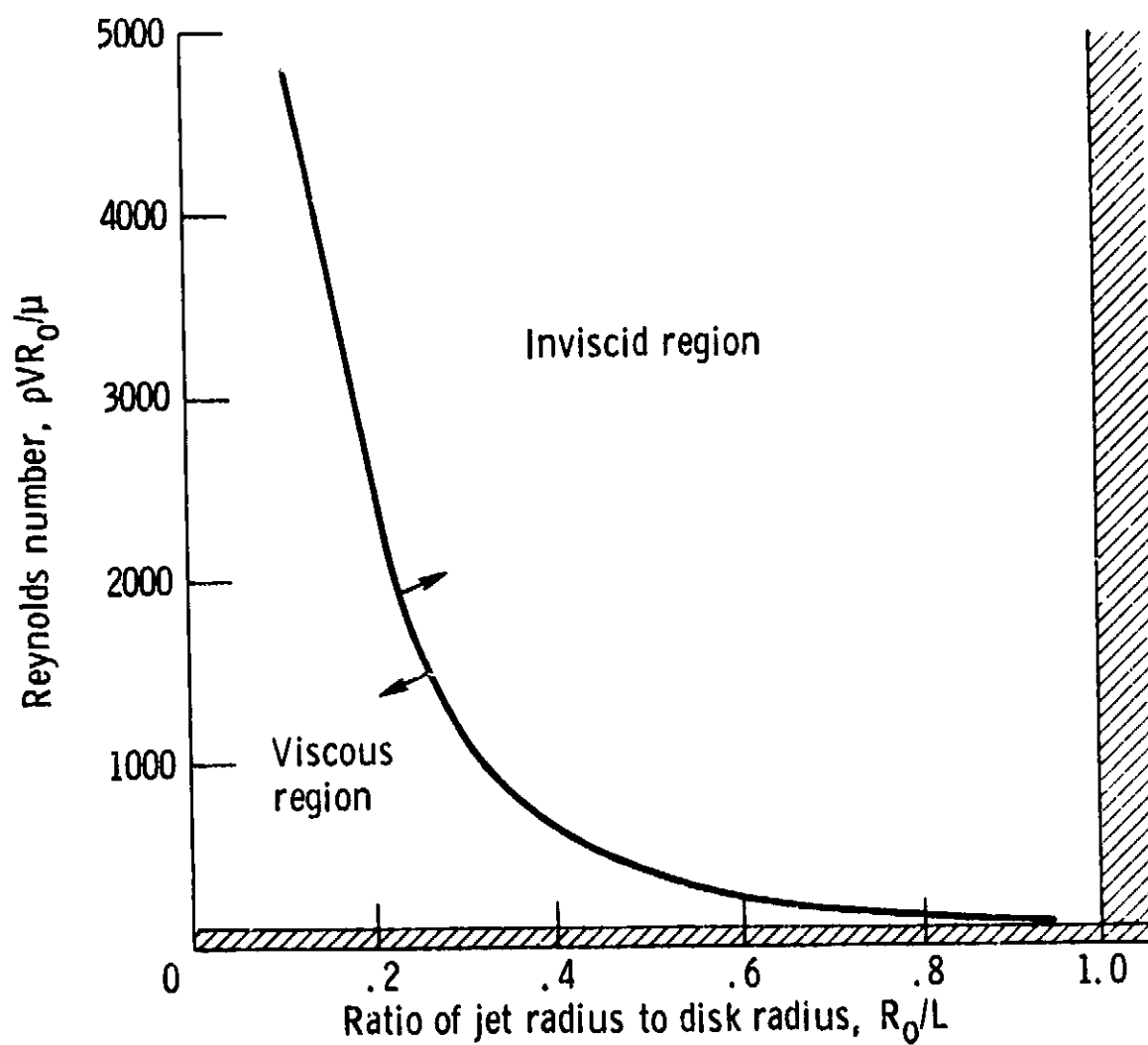


Figure 4. - Results of order of magnitude analysis.

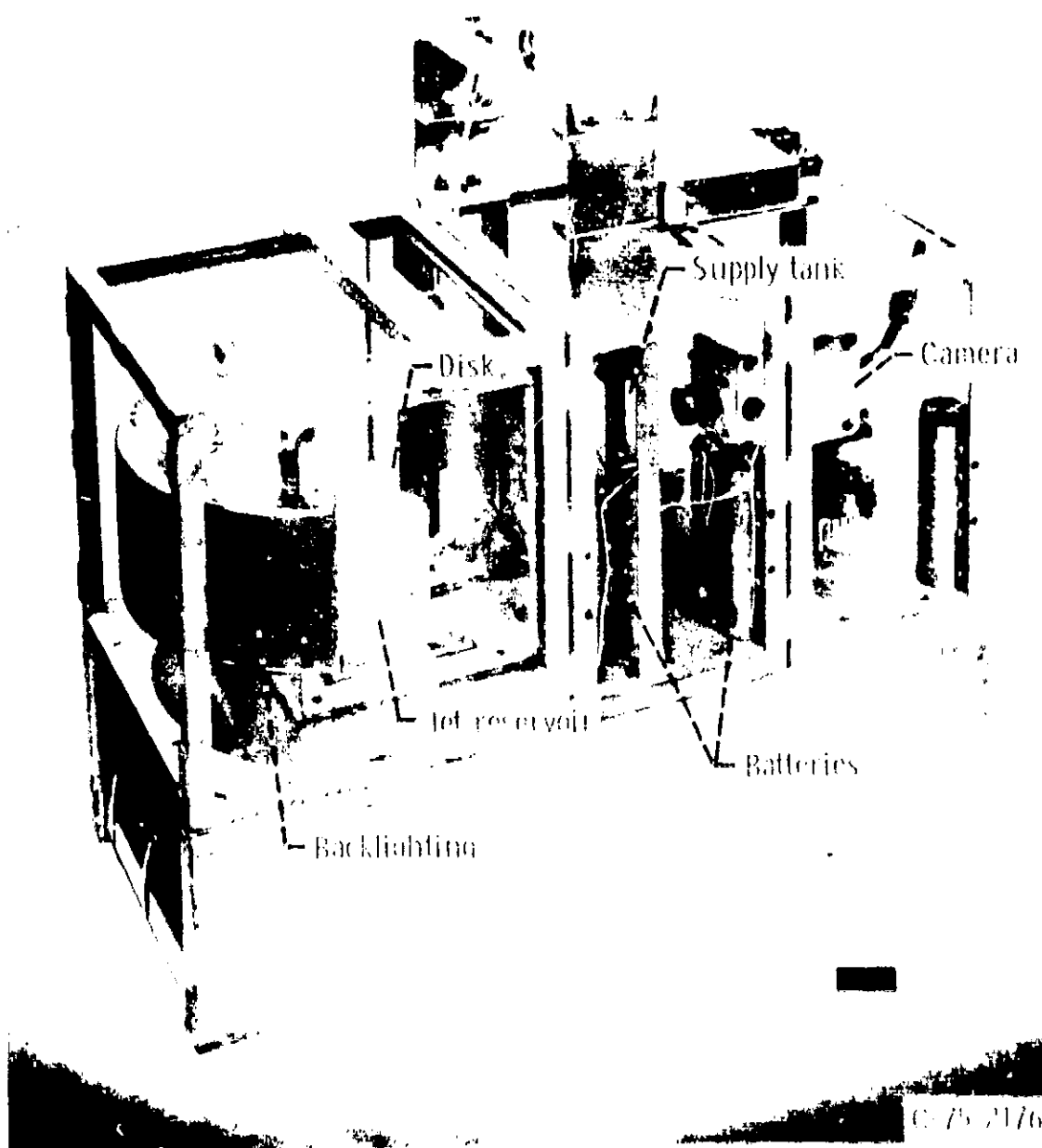


Figure 5. -- Experiment package.

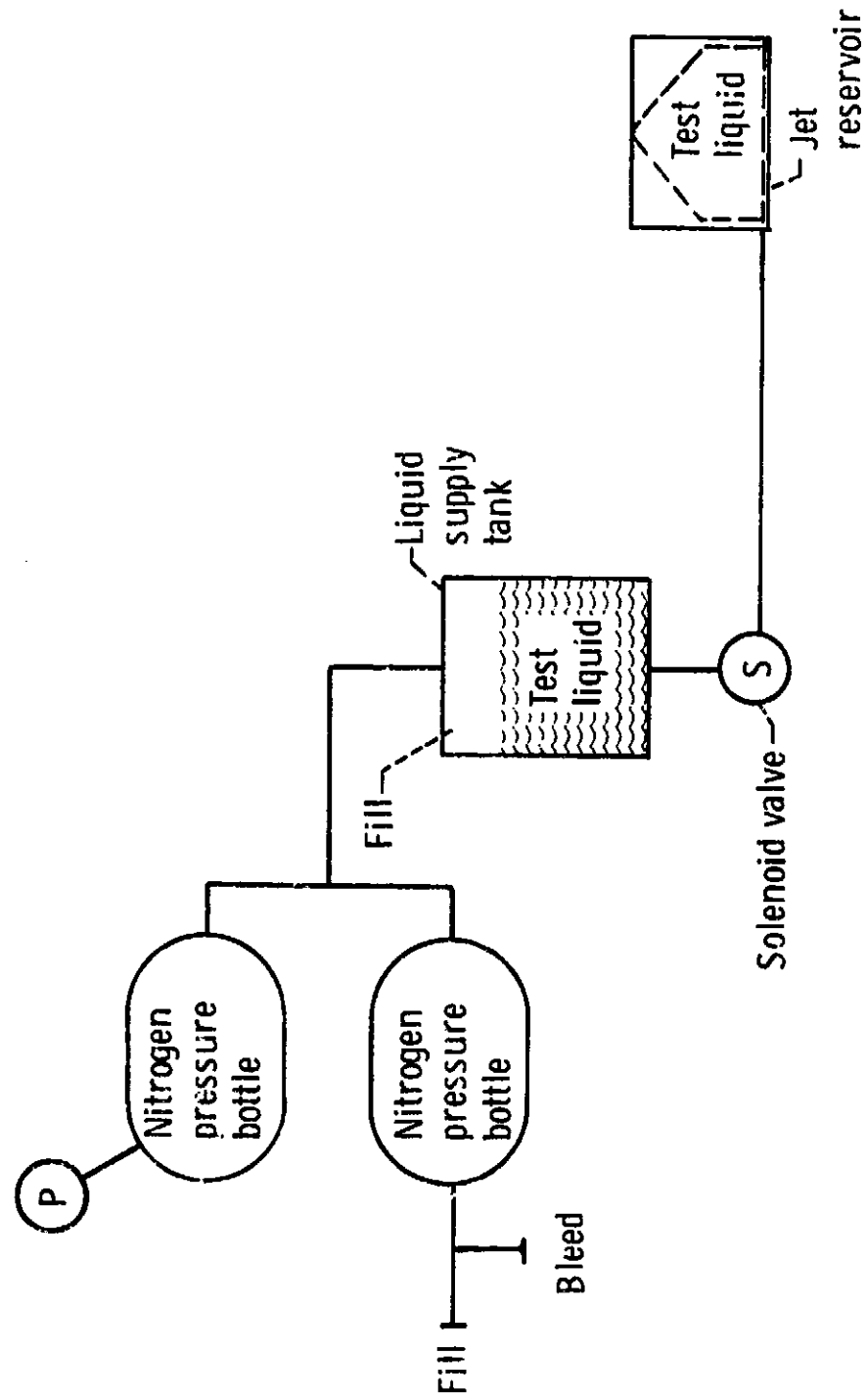


Figure 6. - Flow system schematic.

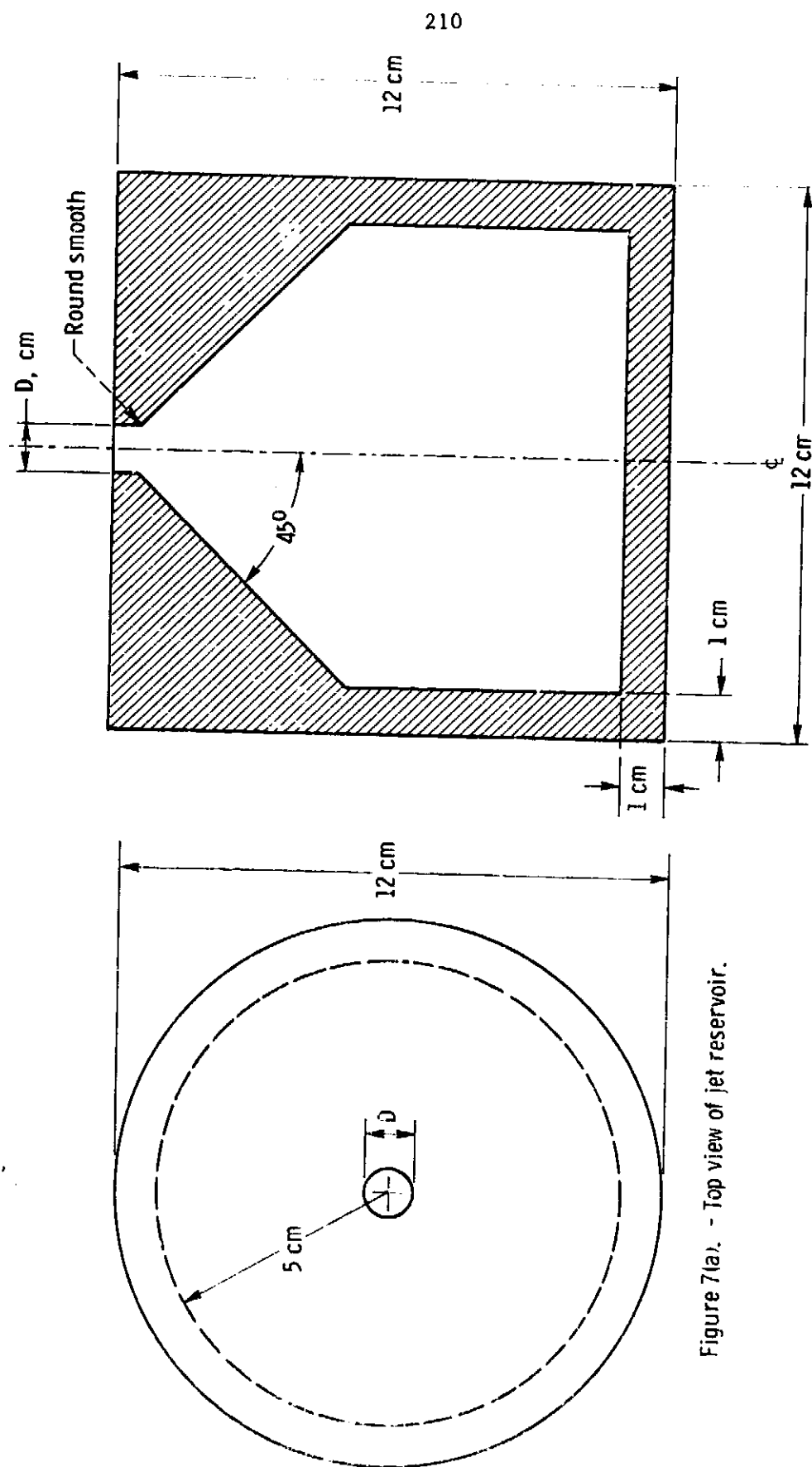


Figure 7(a). - Top view of jet reservoir.

**Figure 7(b). - Side view of jet reservoir.**

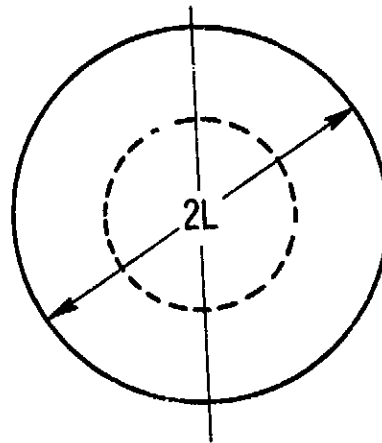
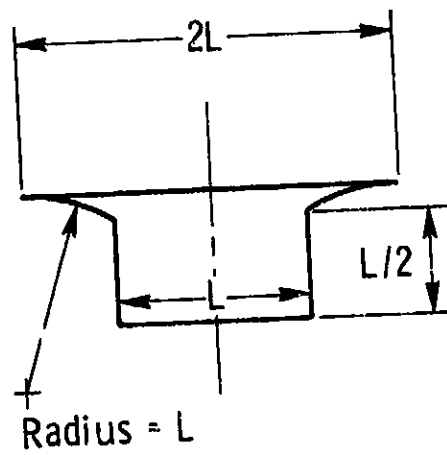
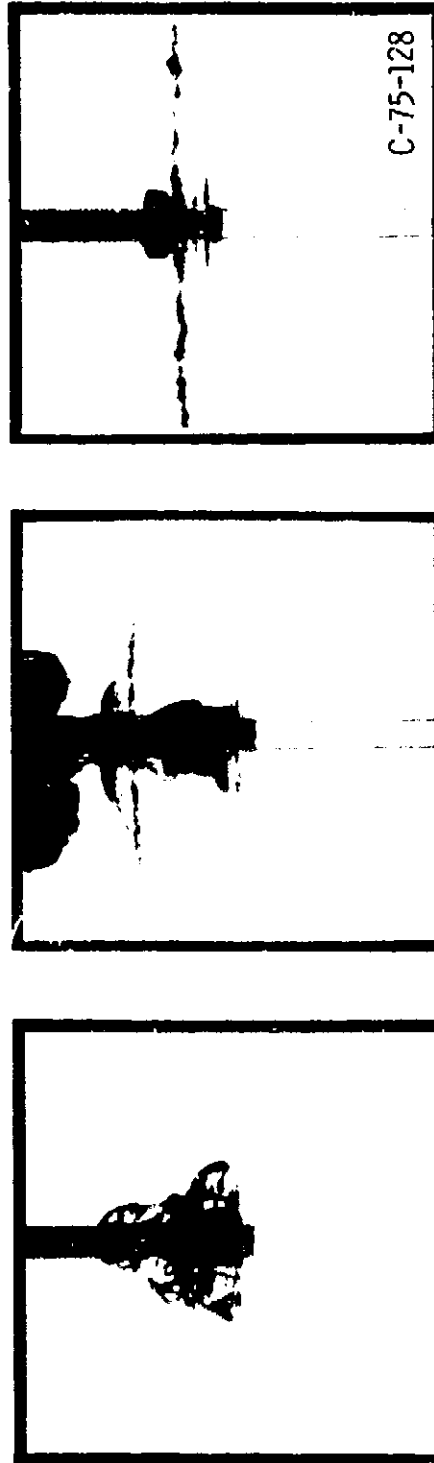


Figure 8. - Schematic diagram of sharp-edged disk.

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(a) Surface tension flow.

(b) Transition flow.

(c) Inertia flow.

Figure 9. - Liquid jet impinging on flat solid plate.

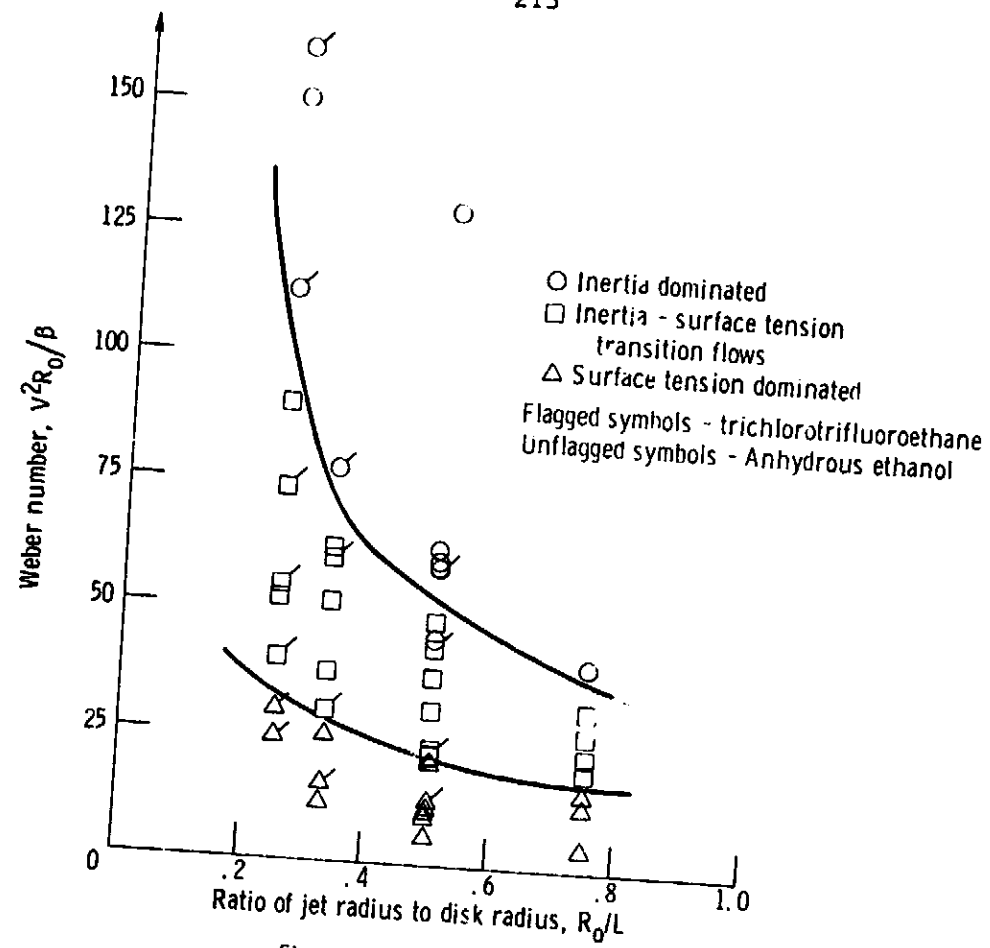


Figure 10. - Zero gravity experimental results.

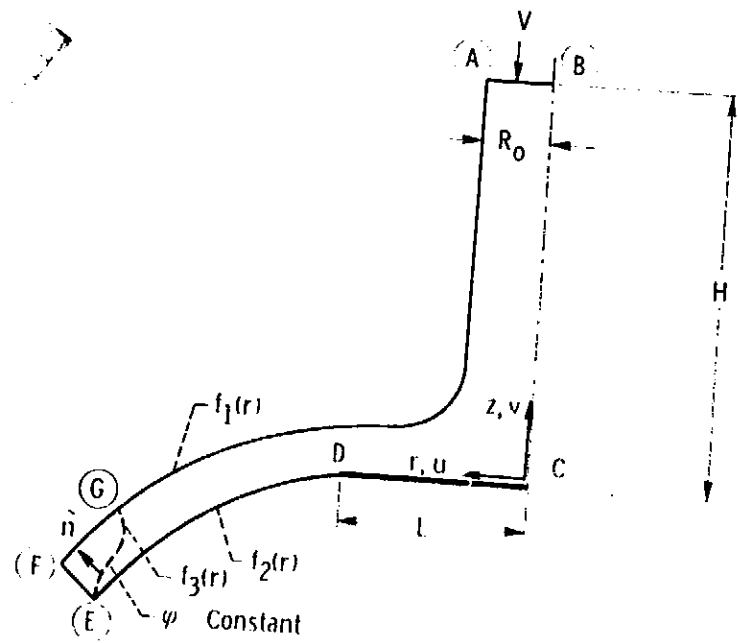


Figure 11. - Physical plane model of liquid jet impingement.

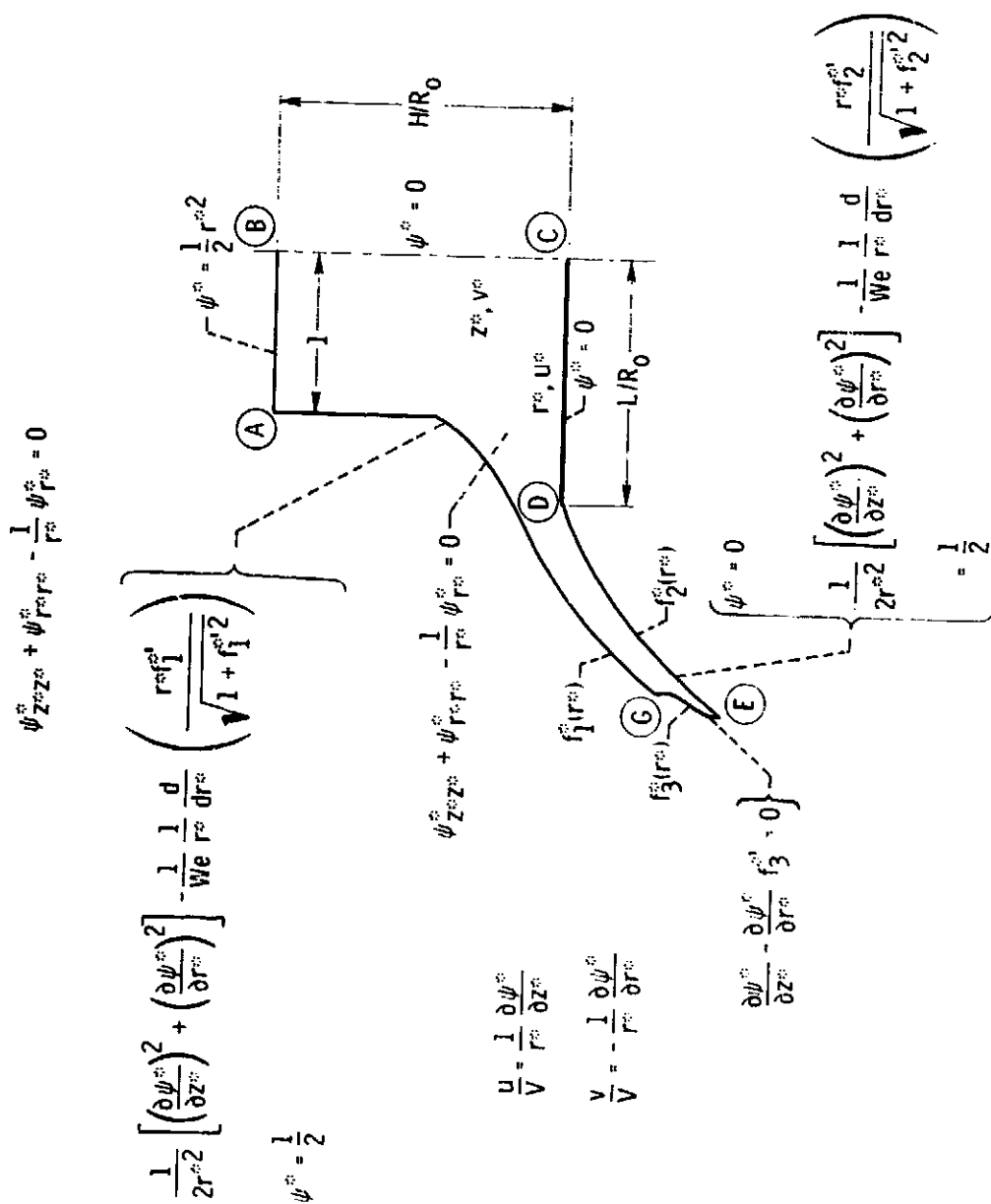


Figure 12. - Dimensionless governing equation and boundary conditions in physical plane employing Stokes' stream function.

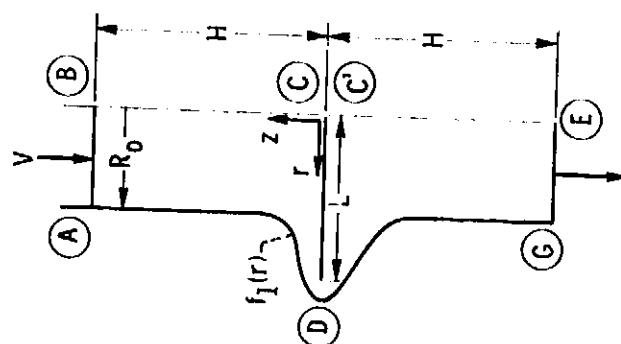


Figure 13. - Surface tension model in physical plane.

$$\psi_{z^*z^*}^* + \psi_{r^*r^*}^* - \frac{1}{r^*} \psi_{r^*}^* = 0$$

$$\text{where } We = \frac{\rho V^2 R_0}{\sigma}$$

$$u^* = \frac{1}{r^*} \frac{\partial \psi^*}{\partial z^*}$$

$$v^* = -\frac{1}{r^*} \frac{\partial \psi^*}{\partial r^*}$$

$$\frac{\partial^2 \psi^*}{\partial z^{*2}} + \frac{\partial^2 \psi^*}{\partial r^{*2}} - \frac{1}{r^*} \frac{\partial \psi^*}{\partial r^*} = 0$$

$$\psi^* = \frac{1}{2}$$

$$\frac{1}{2r^{*2}} \left[ \left( \frac{\partial \psi^*}{\partial z^*} \right)^2 + \left( \frac{\partial \psi^*}{\partial r^*} \right)^2 \right]$$

$$- \frac{1}{We} \frac{1}{r^*} \frac{d}{dr^*} \left[ \frac{r^*}{\sqrt{\left( \frac{\partial \psi^*}{\partial z^*} \right)^2 + 1}} \right]$$

$$= \frac{1}{2} - \frac{1}{We}$$

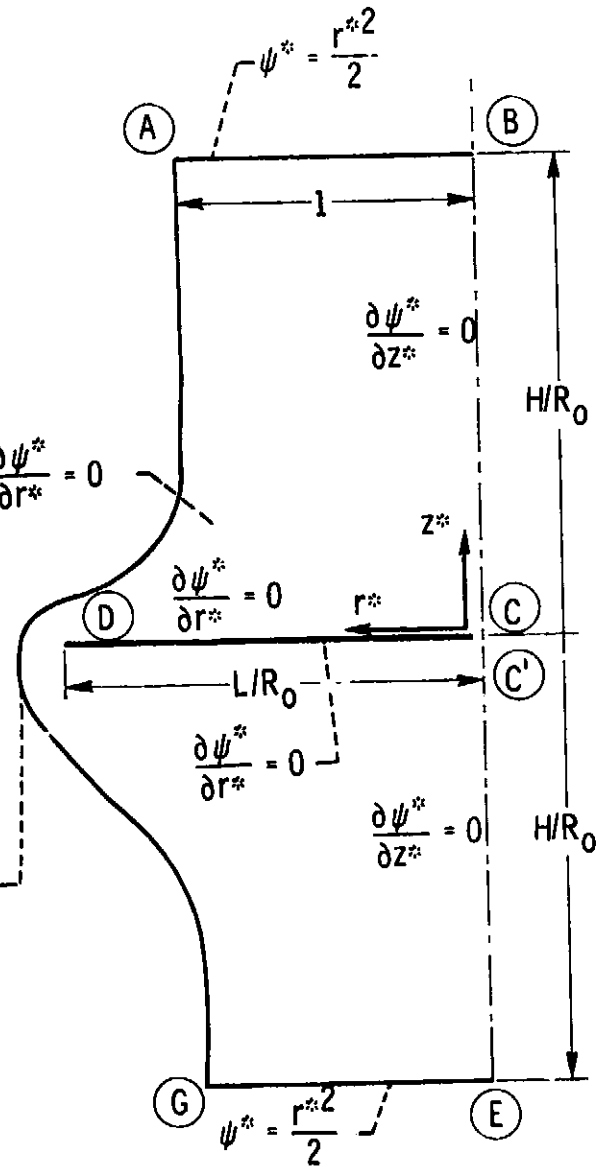


Figure 14. - Dimensionless governing equations and boundary conditions.

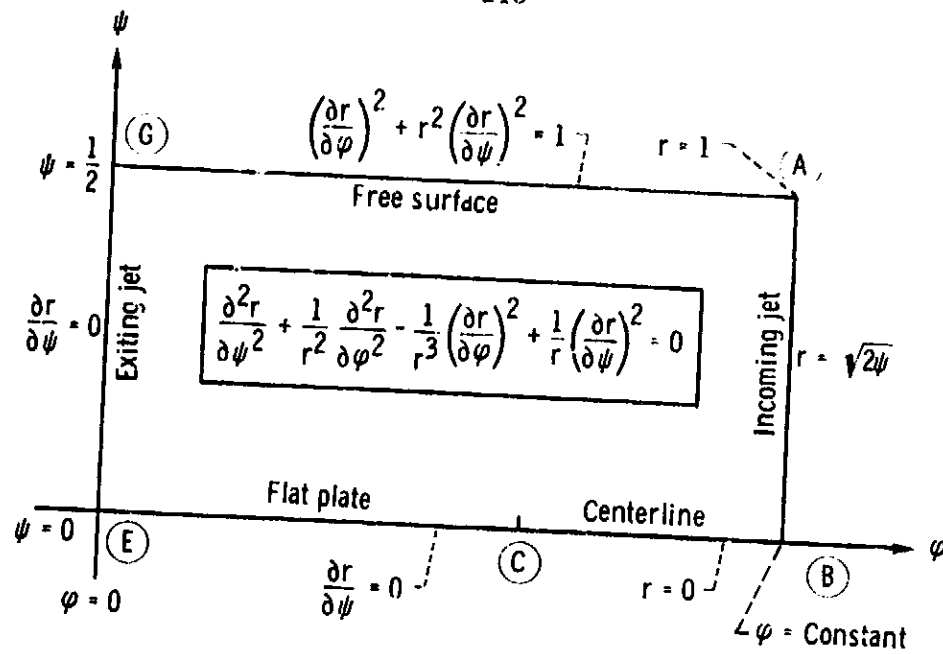


Figure 15(a). - Inverse formulation excluding surface tension ( $r$  solution) for infinite plate.

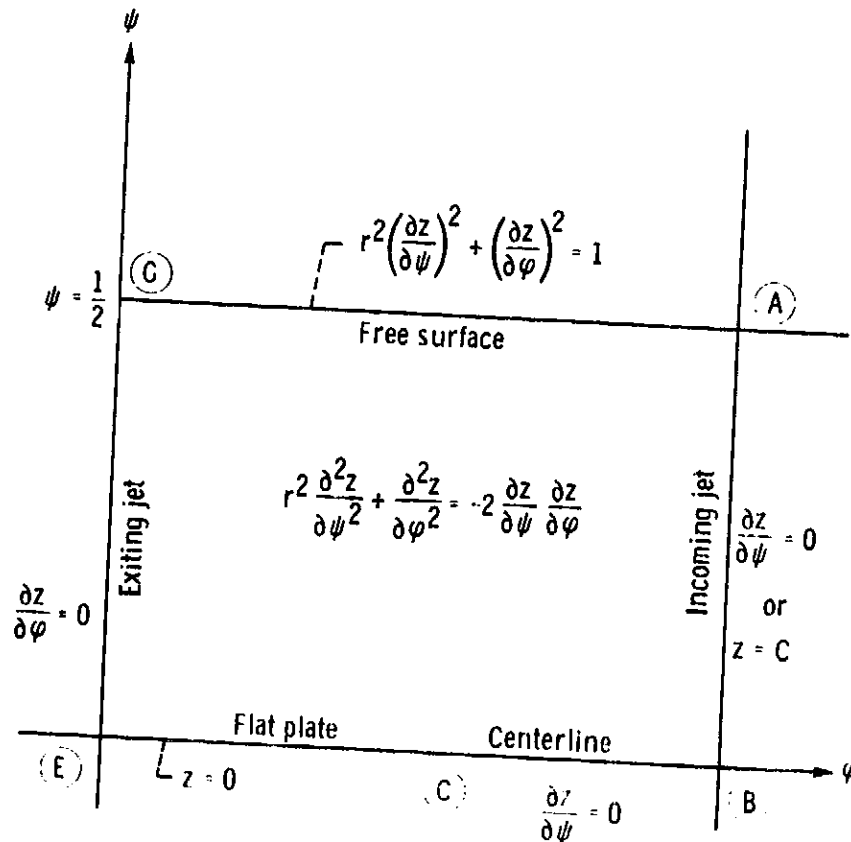


Figure 15(b). - Inverse formulation excluding surface tension ( $z$  solution) for infinite plate.

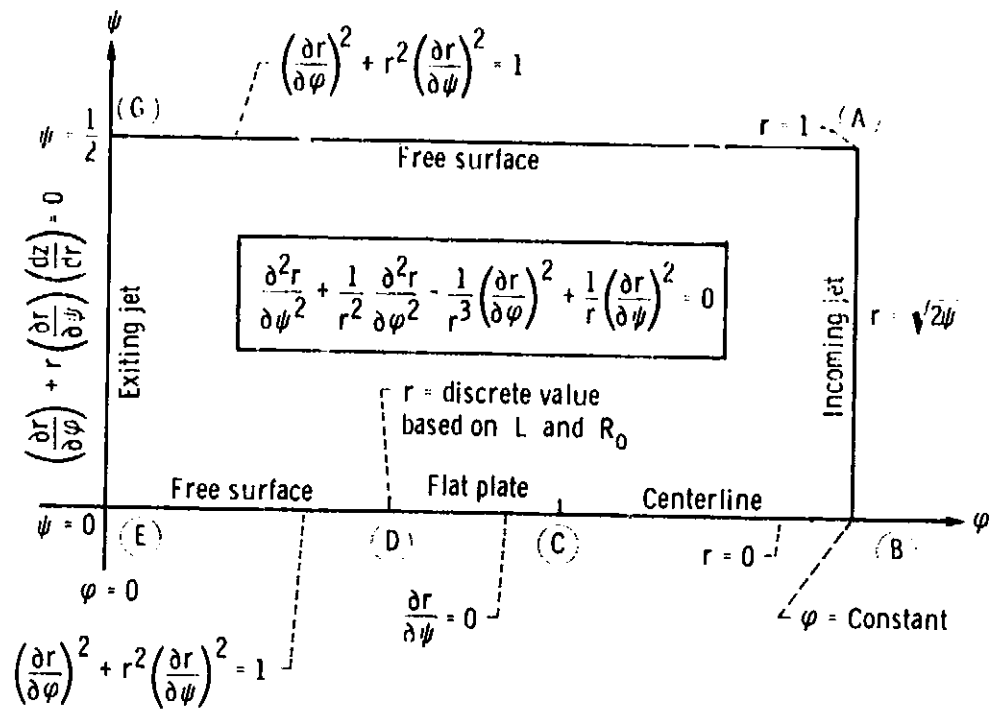


Figure 16(a). - Inverse formulation excluding surface tension ( $r$  solution) for finite plate.

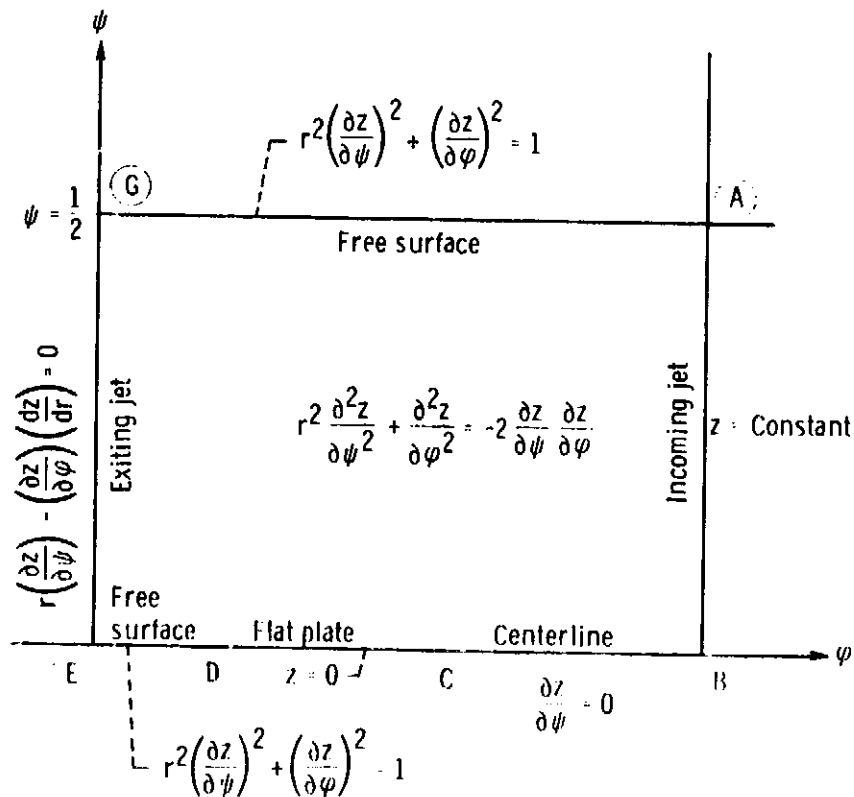


Figure 16(b). - Inverse formulation excluding surface tension ( $z$  solution) for finite plate.

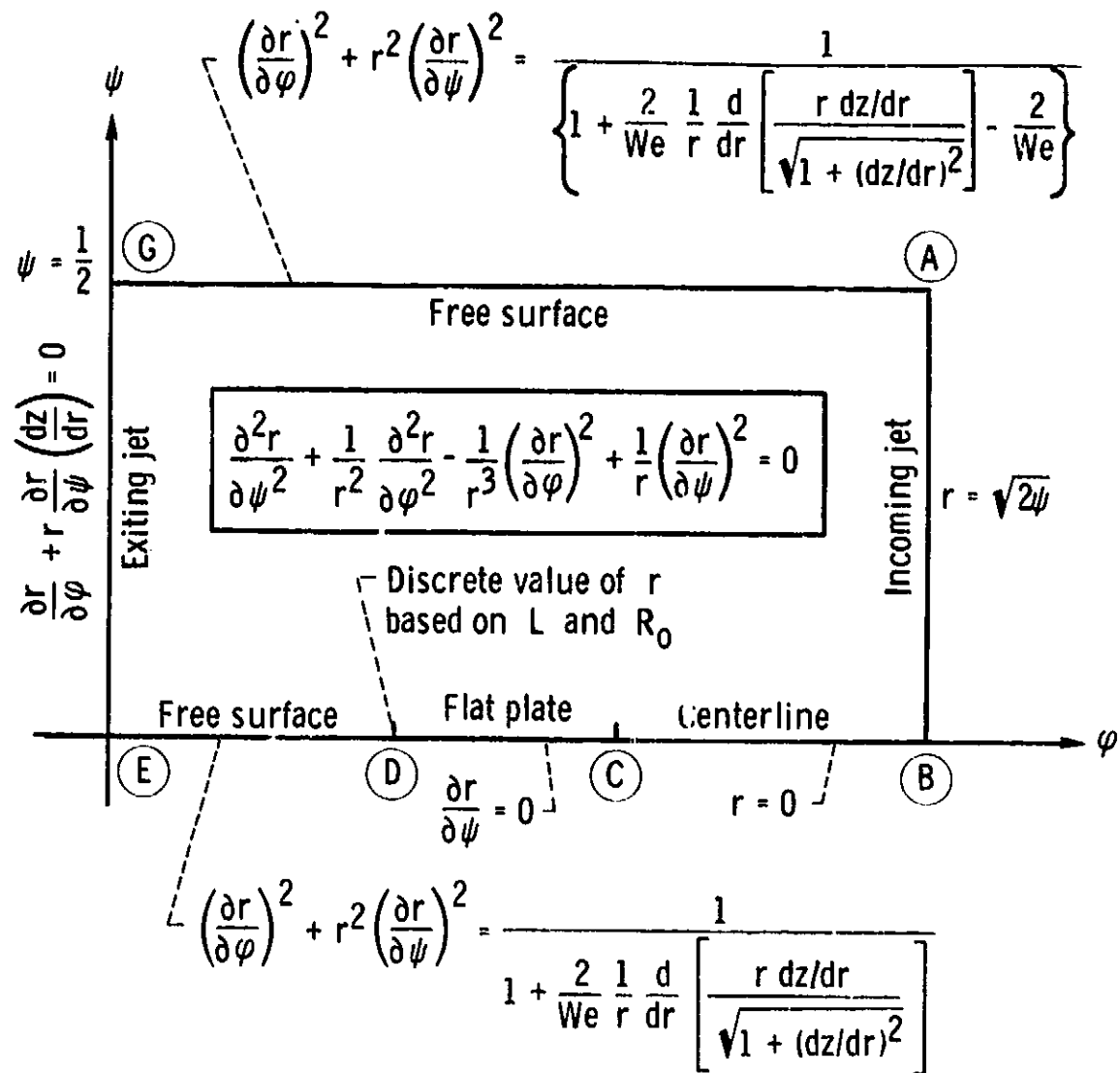
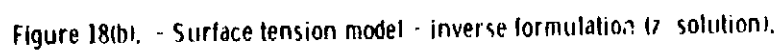
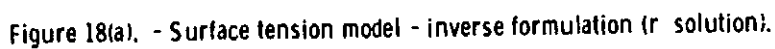


Figure 17. - Inverse formulation including surface tension ( $r$  solution) for finite plate.





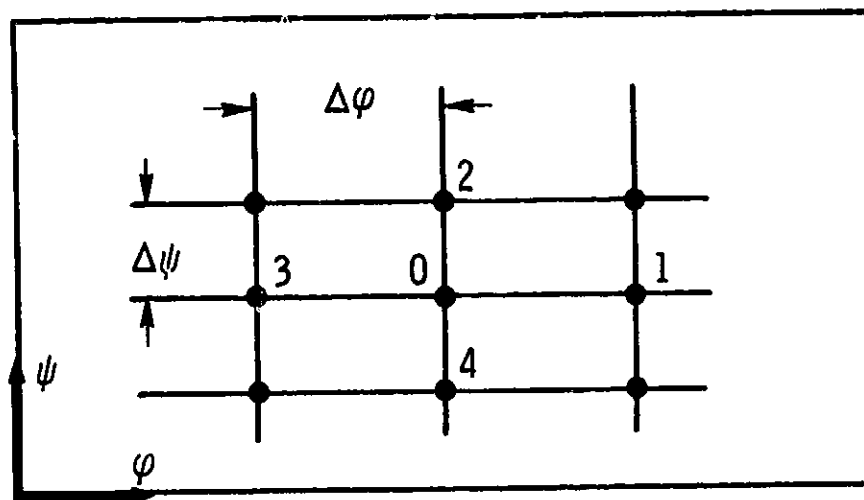


Figure 19. - Nodal point representation for rectangular mesh.

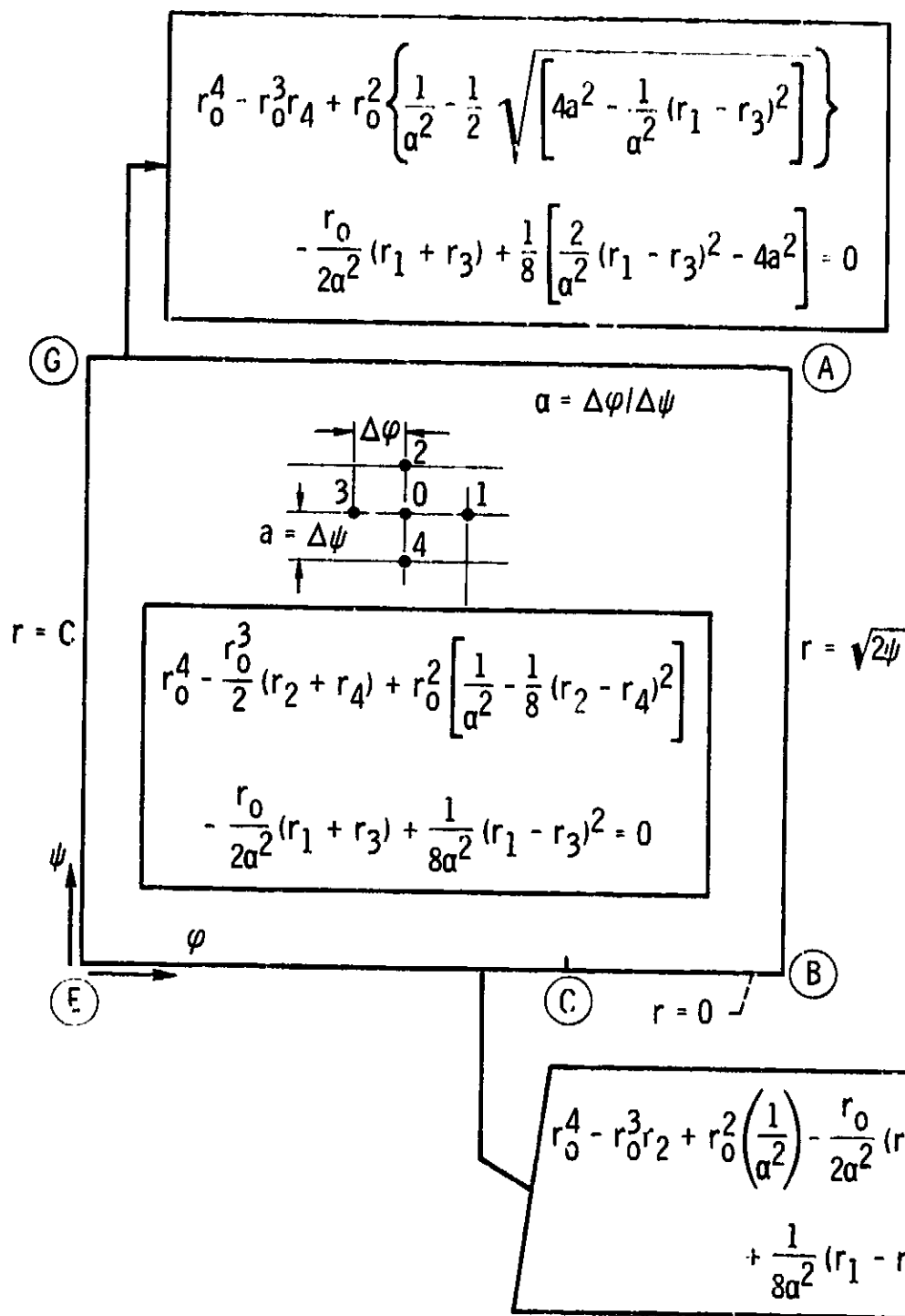


Figure 20(a). - Finite difference representation for infinite plate (r solution).

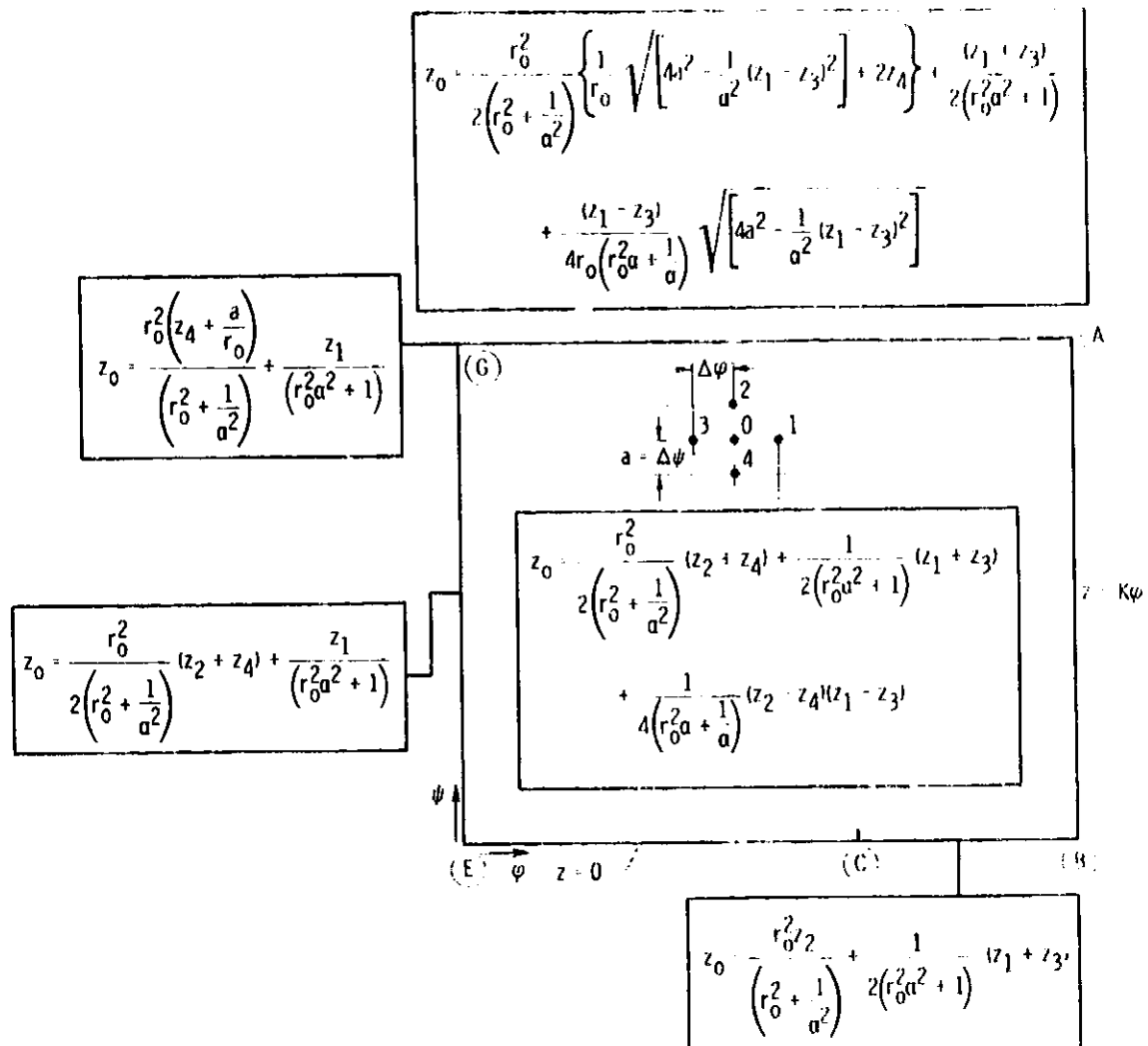


Figure 20(b). - Finite difference representation for infinite plate (z solution).

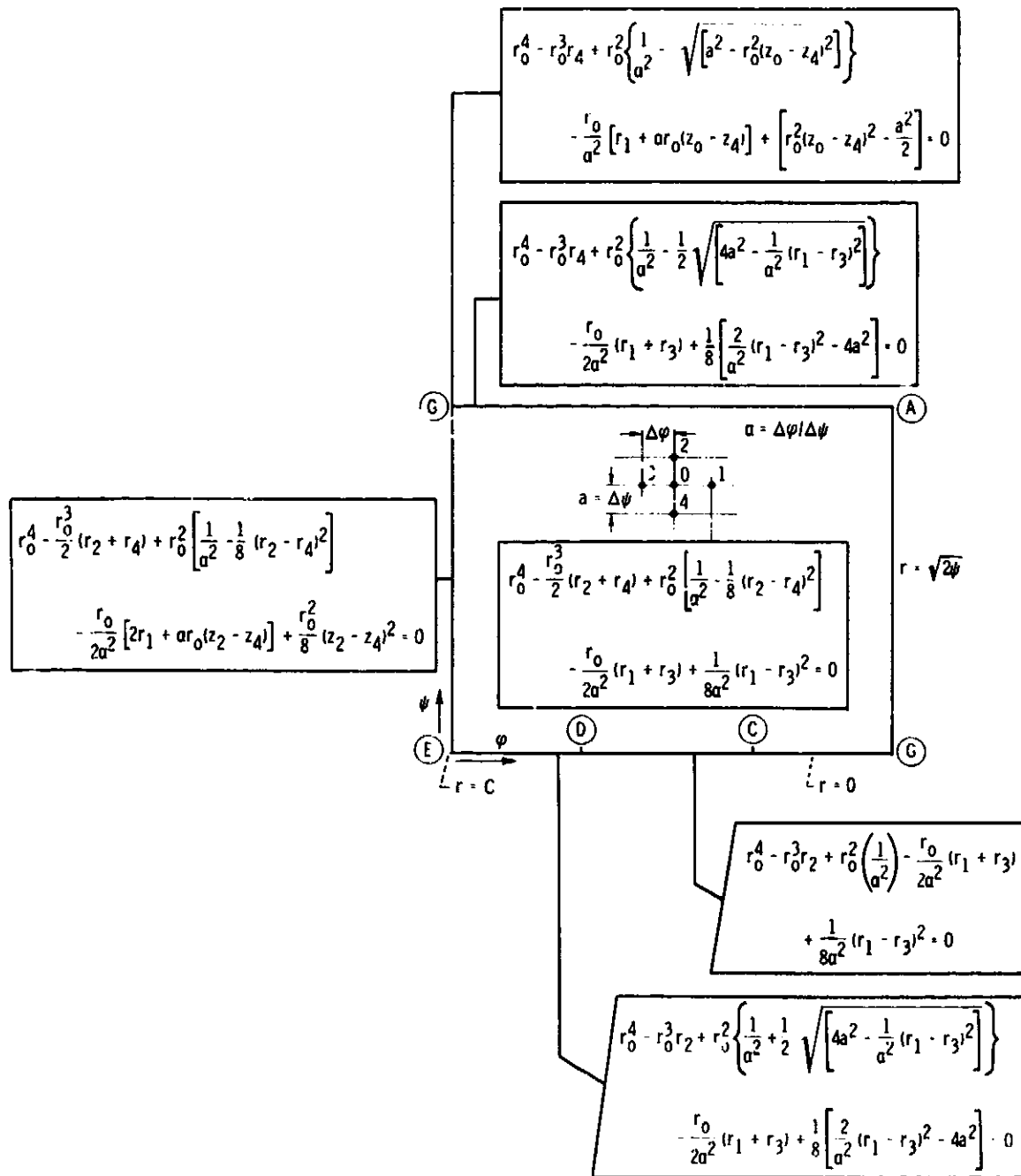


Figure 21(a). - Finite difference representation for finite plate (r solution).

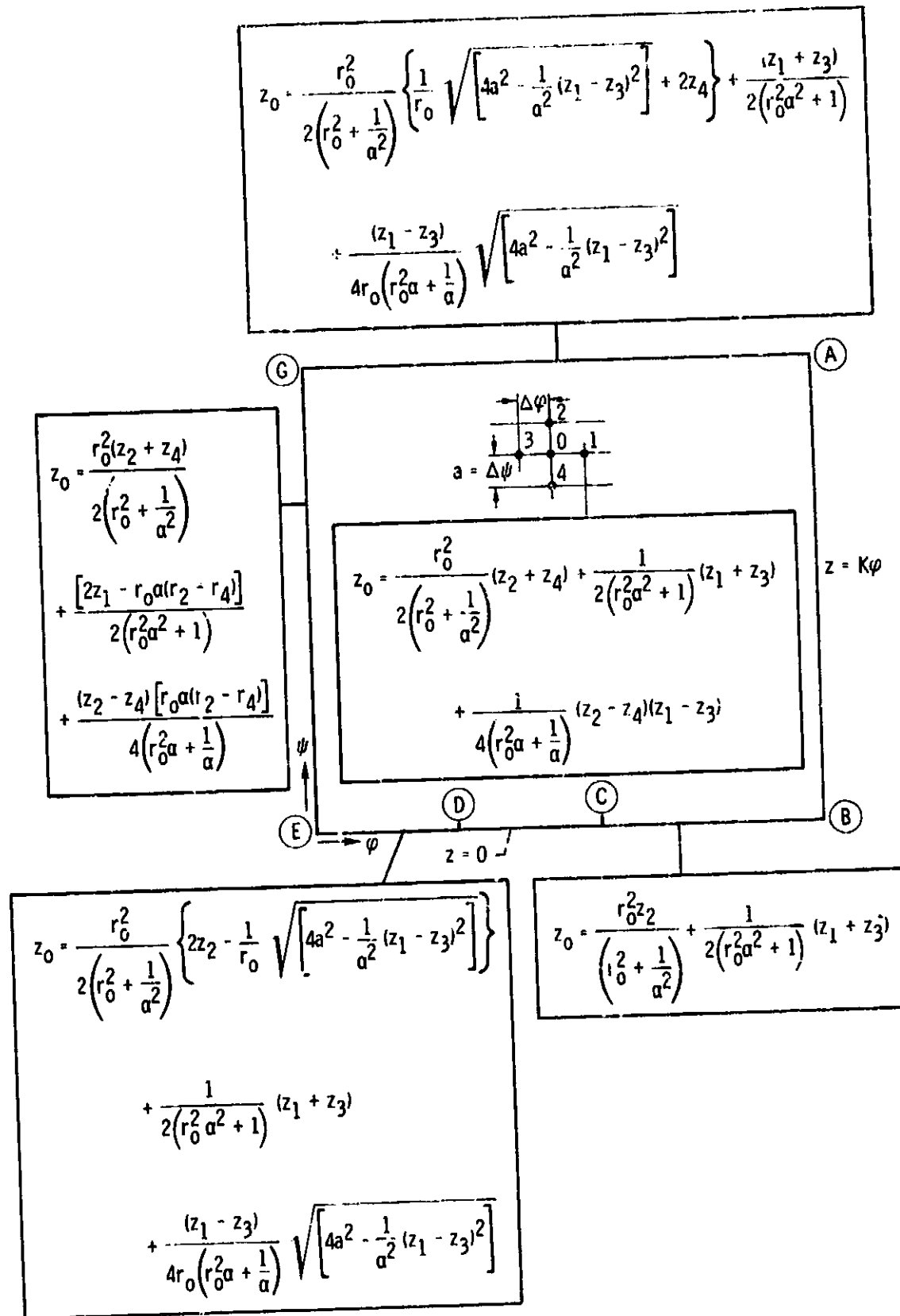


Figure 21(b). - Finite difference representation for finite plate (z solution).

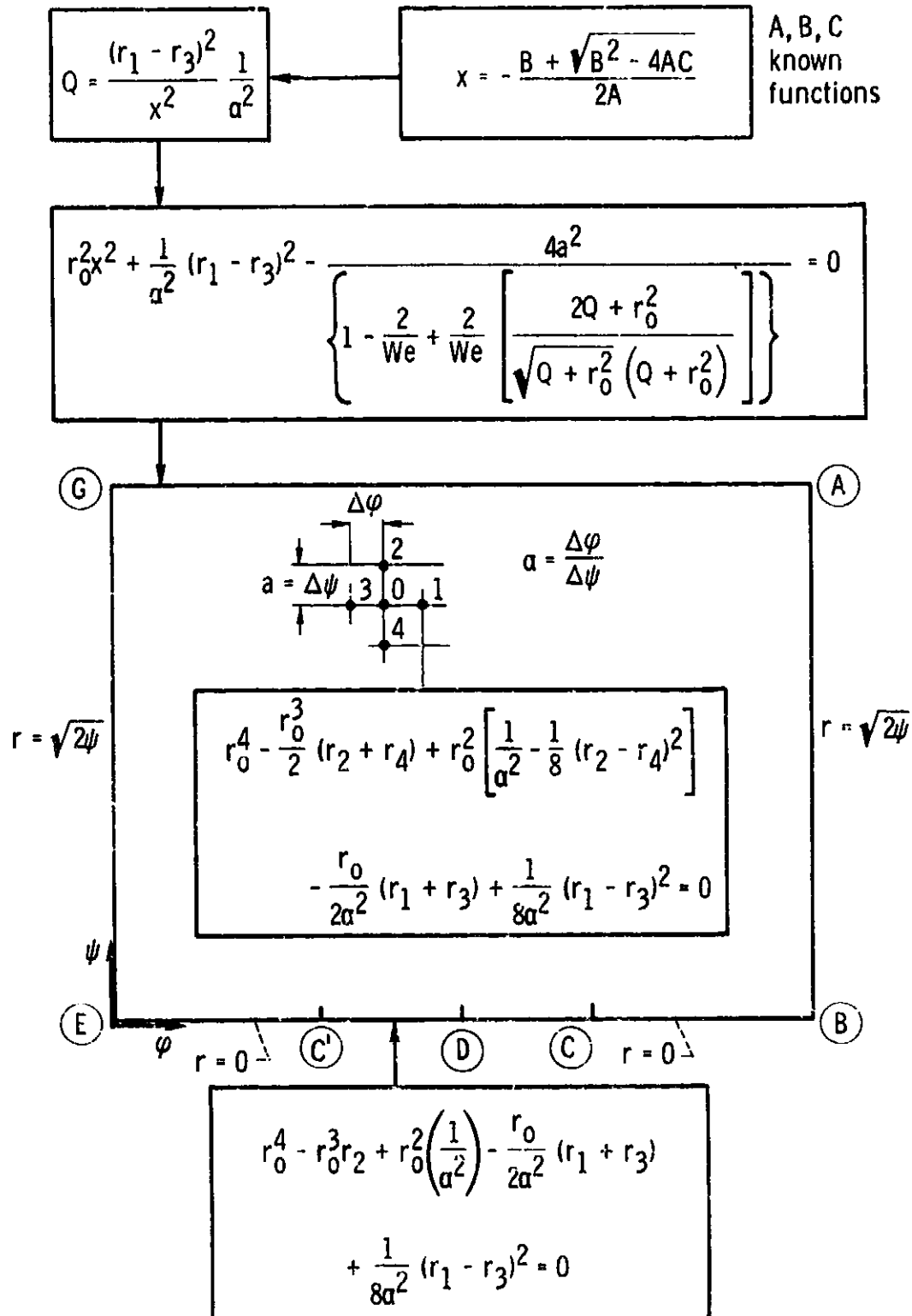


Figure 22(a). - Finite difference representation for surface tension dominated model ( $r$  solution).

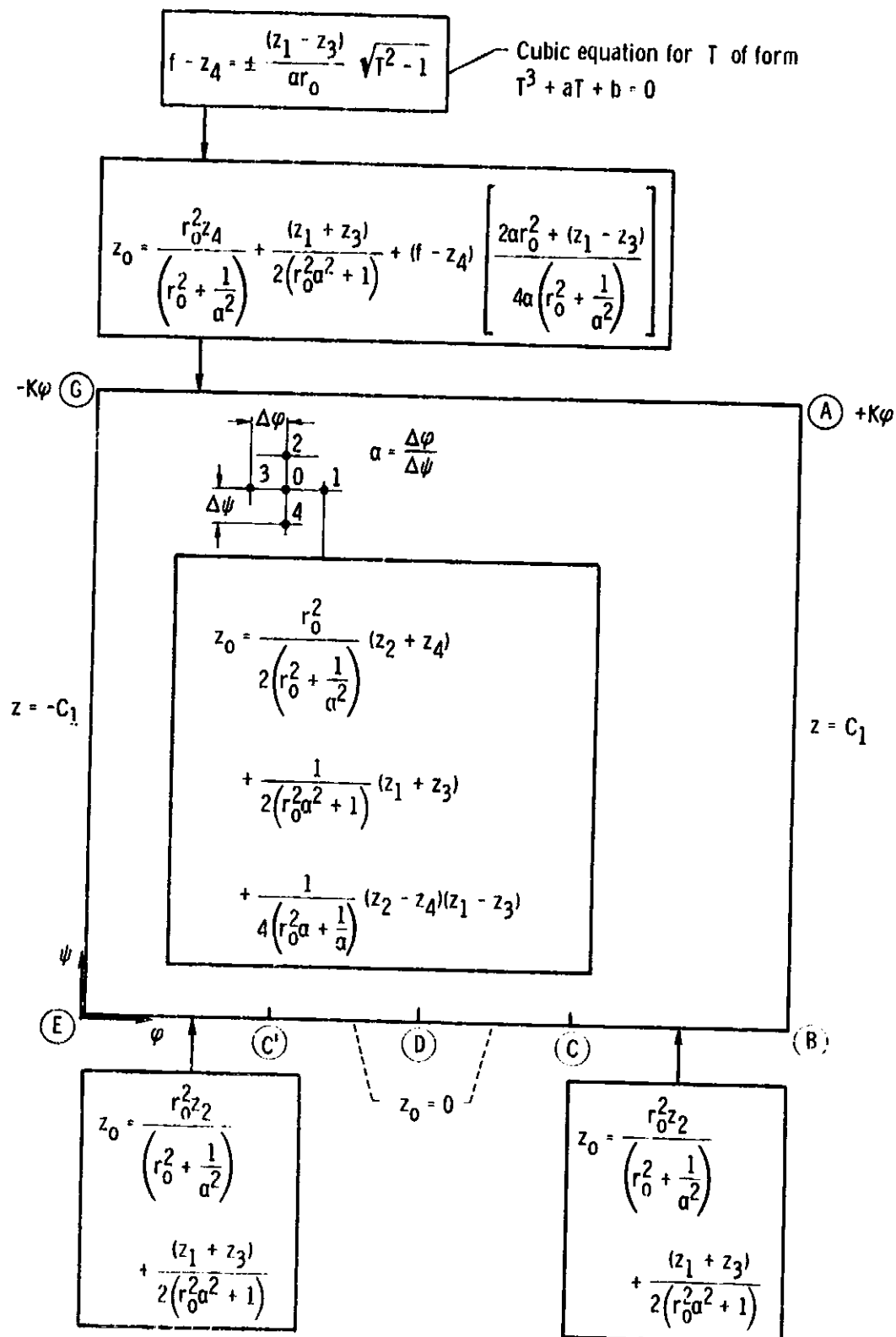


Figure 22(b). - Finite difference representation for surface tension dominated model ( $z$  solution).

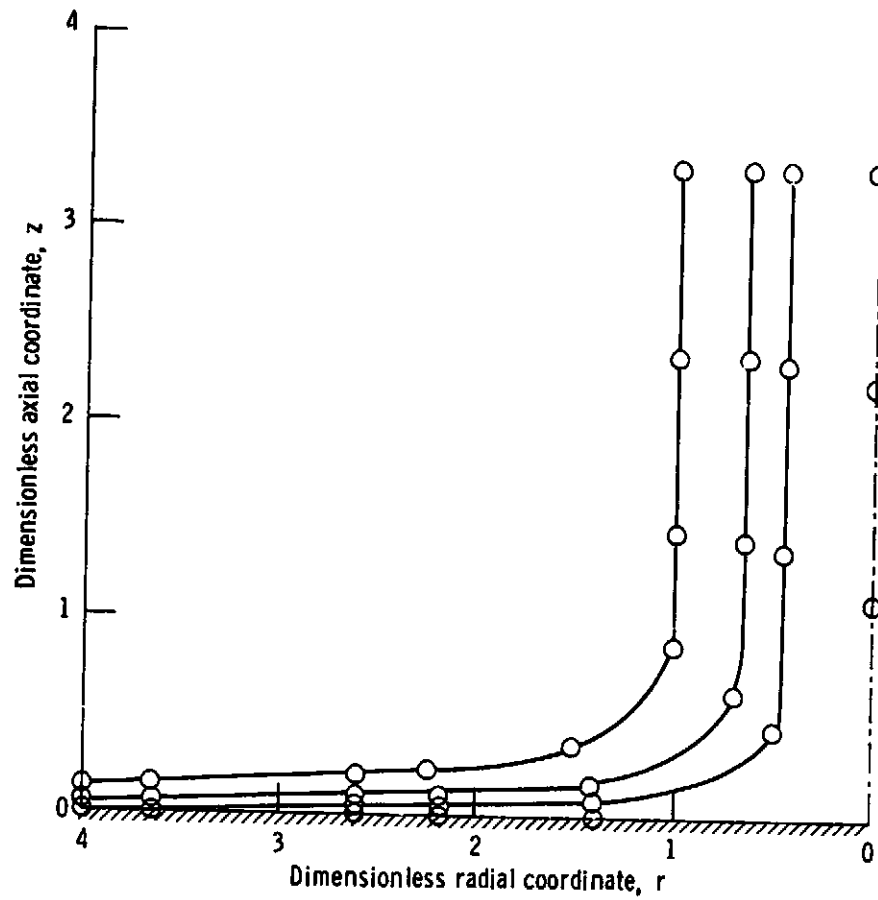


Figure 23. - Numerical solution of liquid jet impinging on infinite flat plate (coarse mesh).

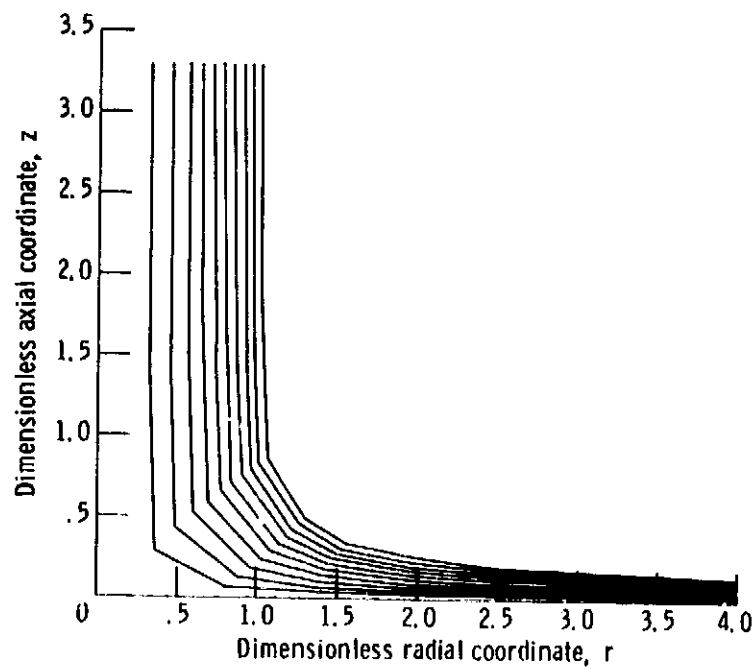


Figure 24. - Print-plot of liquid jet impinging on infinite flat plate (fine mesh).



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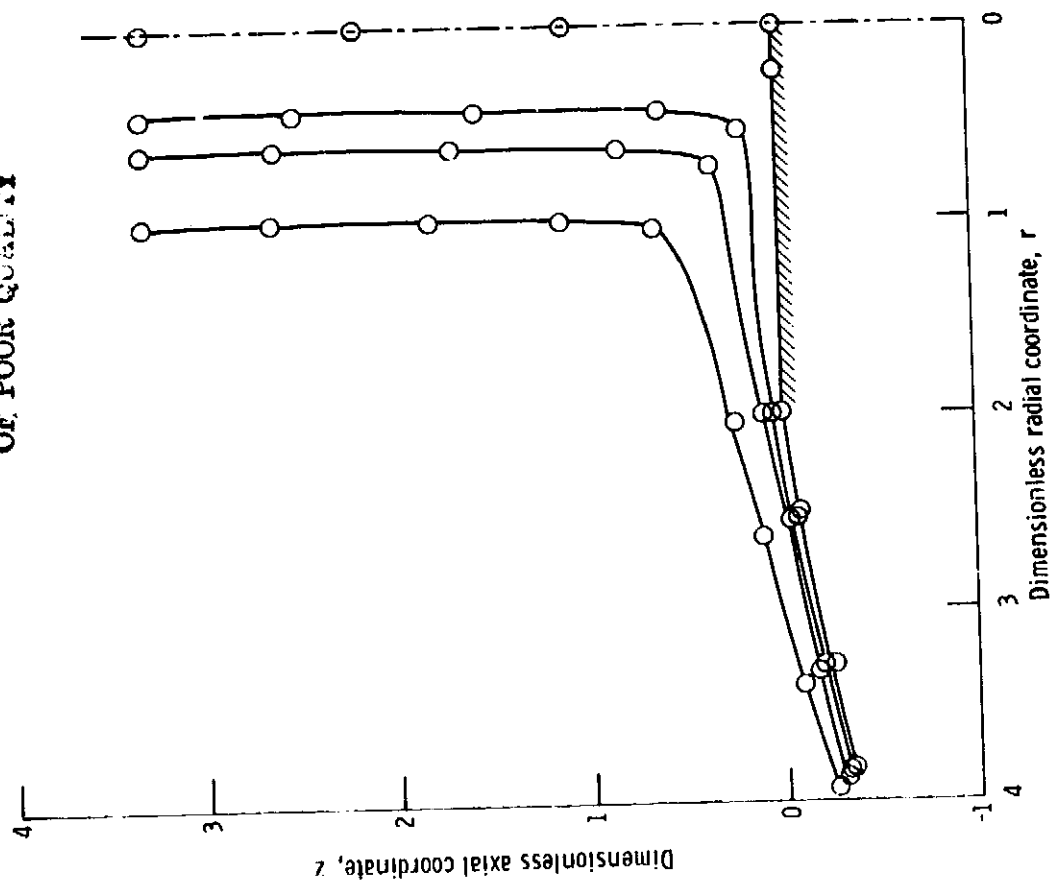


Figure 25. - Numerical solution of liquid jet impinging on finite plate  
( $R_0/L = 1/2$ ).

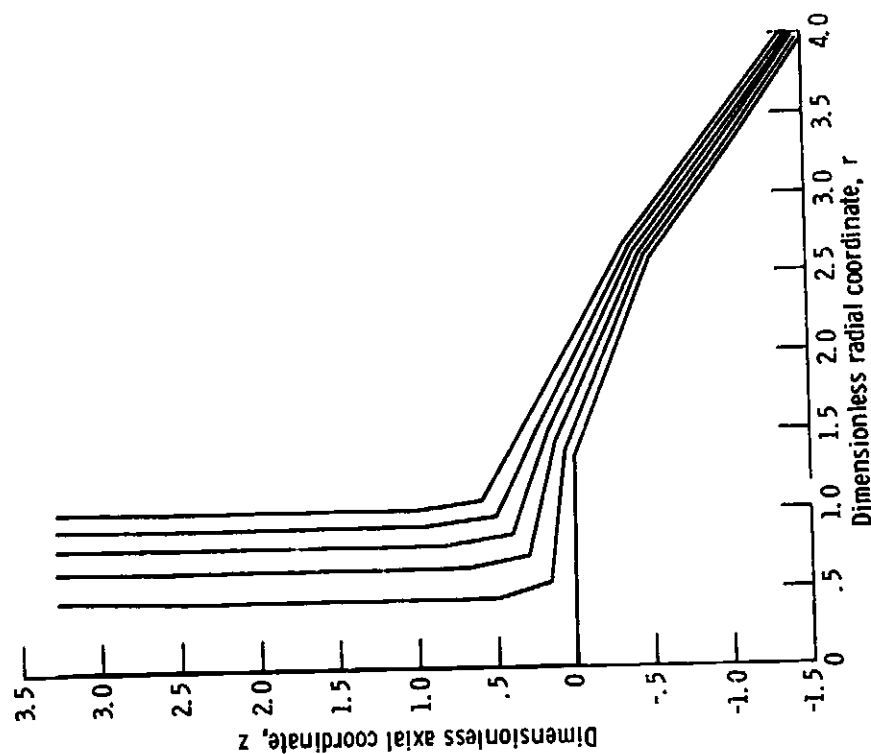


Figure 26. - Print-plot of numerical solution for impingement  
on a finite plate ( $R_0/L = 3/4$ ).

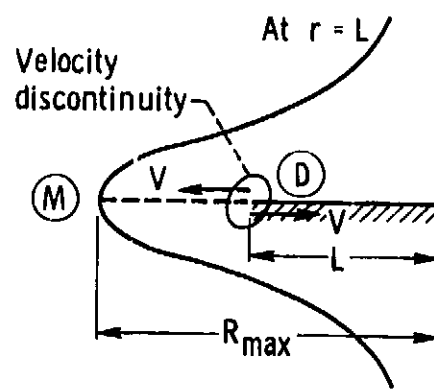


Figure 27. - Schematic diagram of velocity discontinuity occurring in surface tension model.

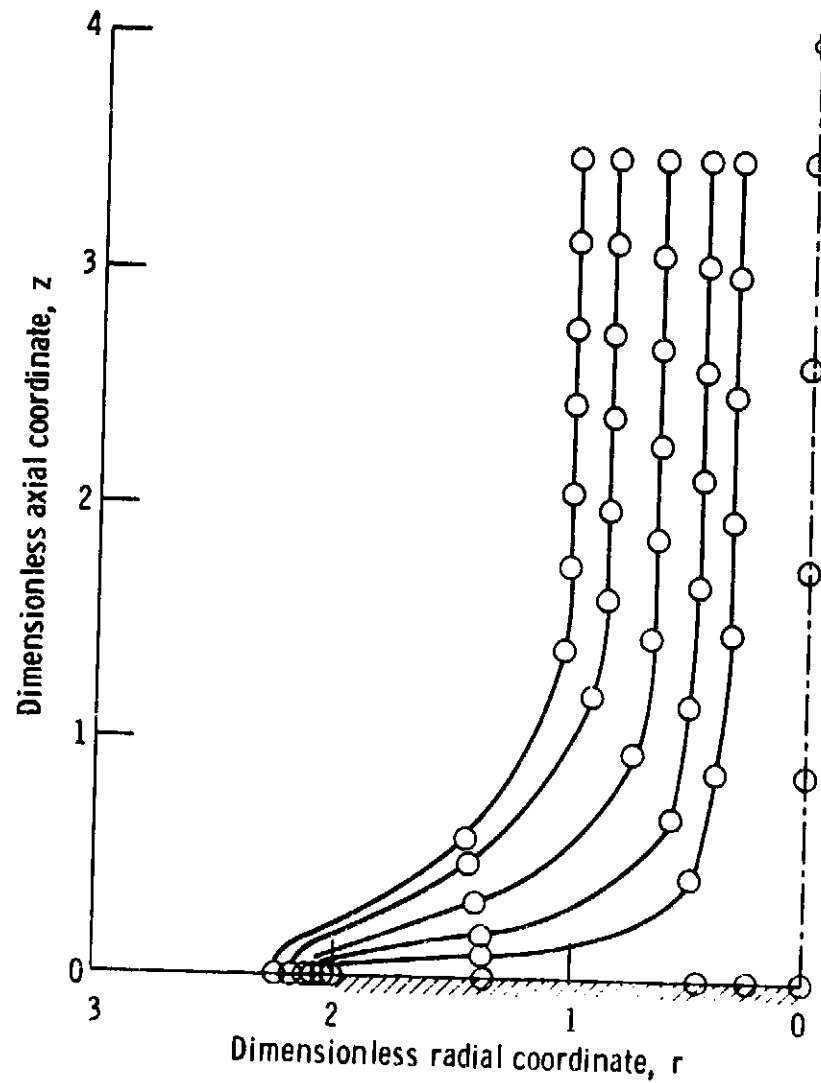


Figure 28. - Numerical solution of surface tension dominated model ( $We = 4$ ,  $R_0/L = 1/2$ ).

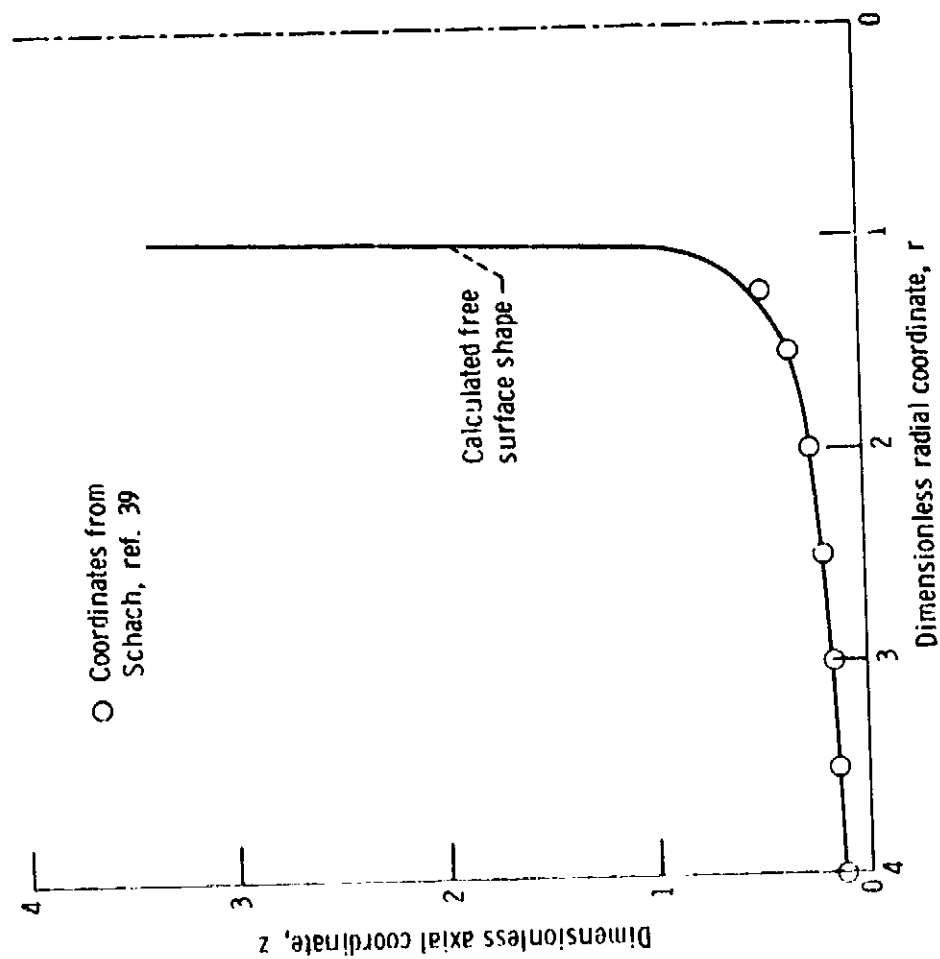


Figure 29. - Comparison of numerical results for infinite plate with reference 39.

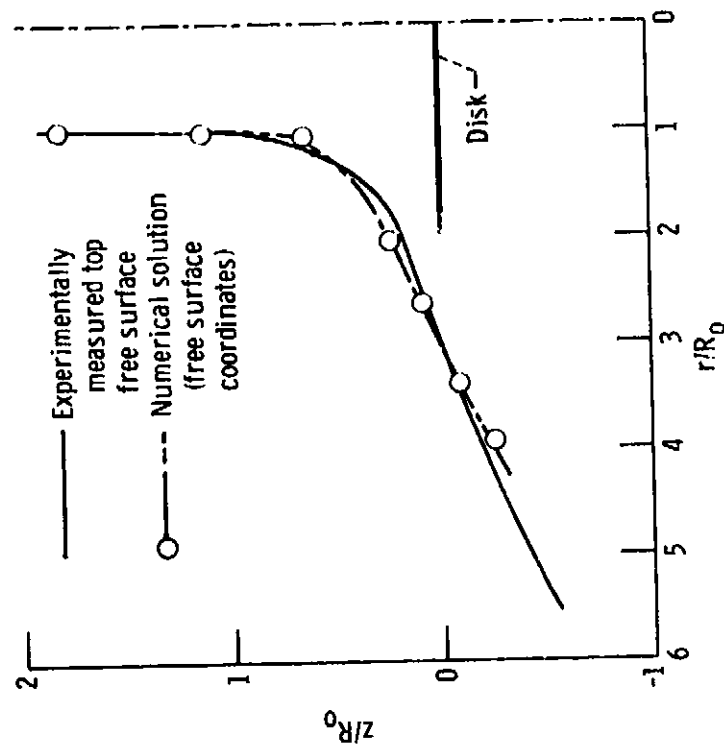


Figure 30. - Comparison of numerical results for finite plate - inertial flow with experiments ( $R_0/L = 1/2$ ).

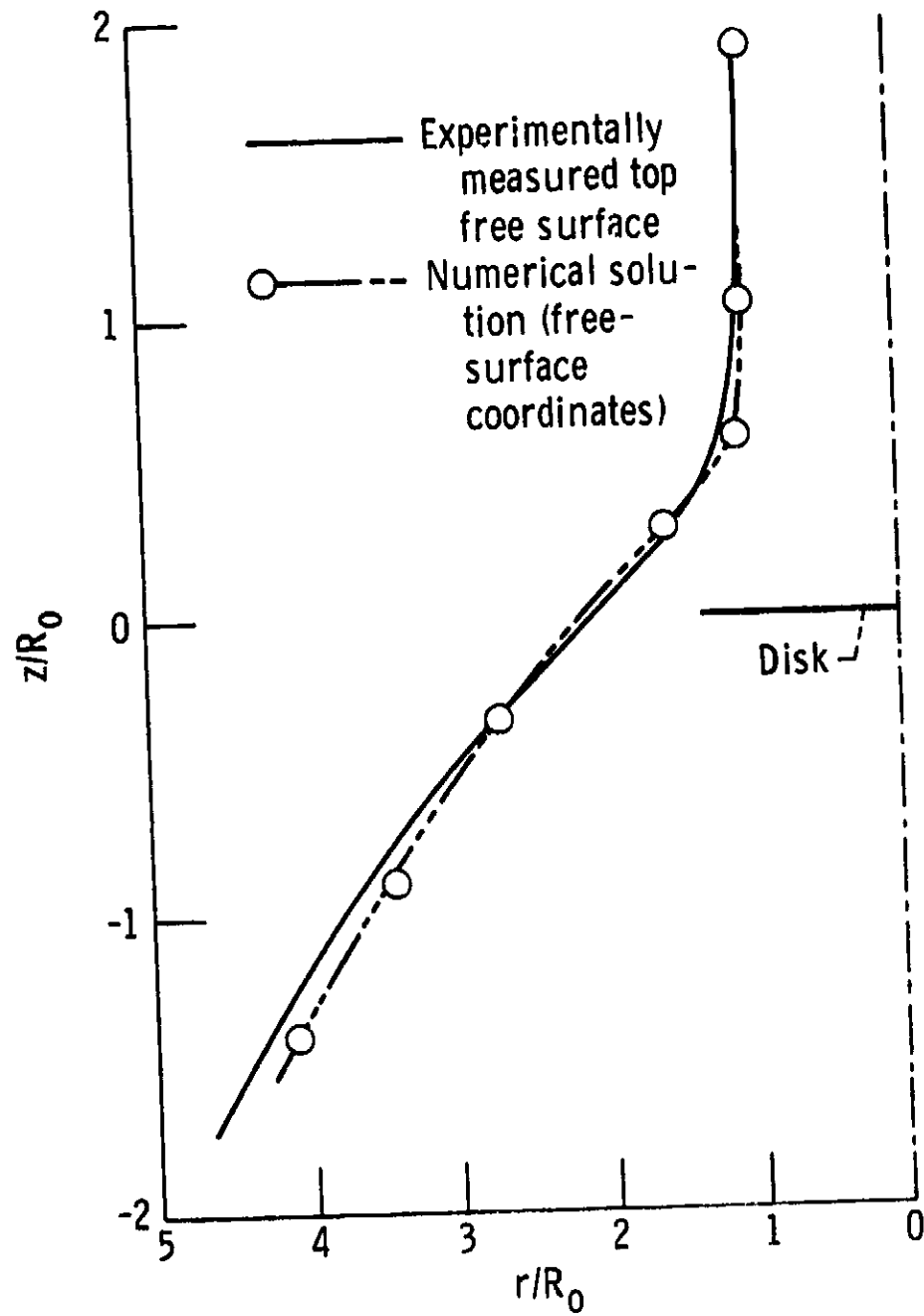


Figure 31. - Comparison of numerical results for finite plate - inertial flow with experiments ( $R_0/L = 3/4$ ).

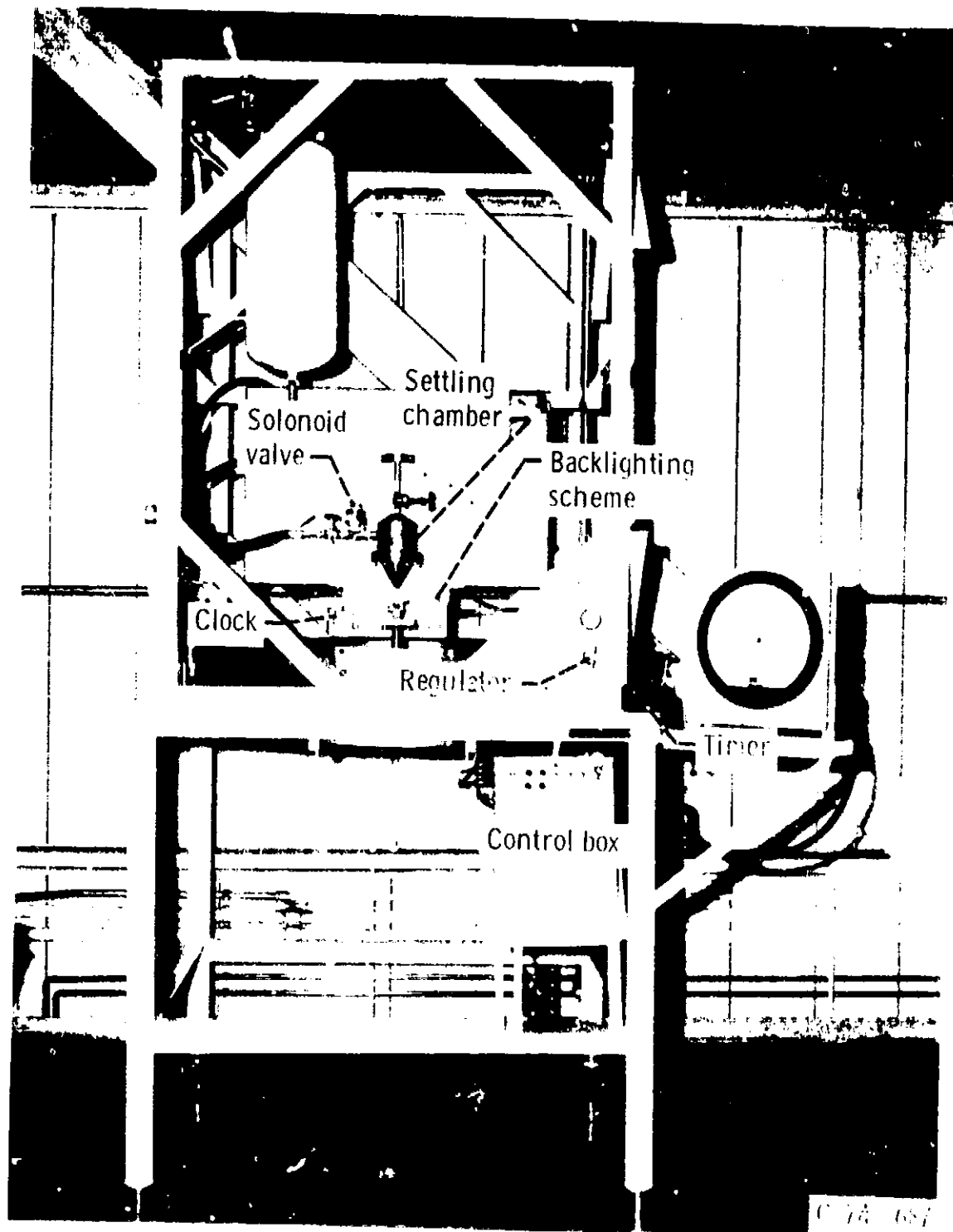


Figure 32(a). - Experimental test rig - front view.

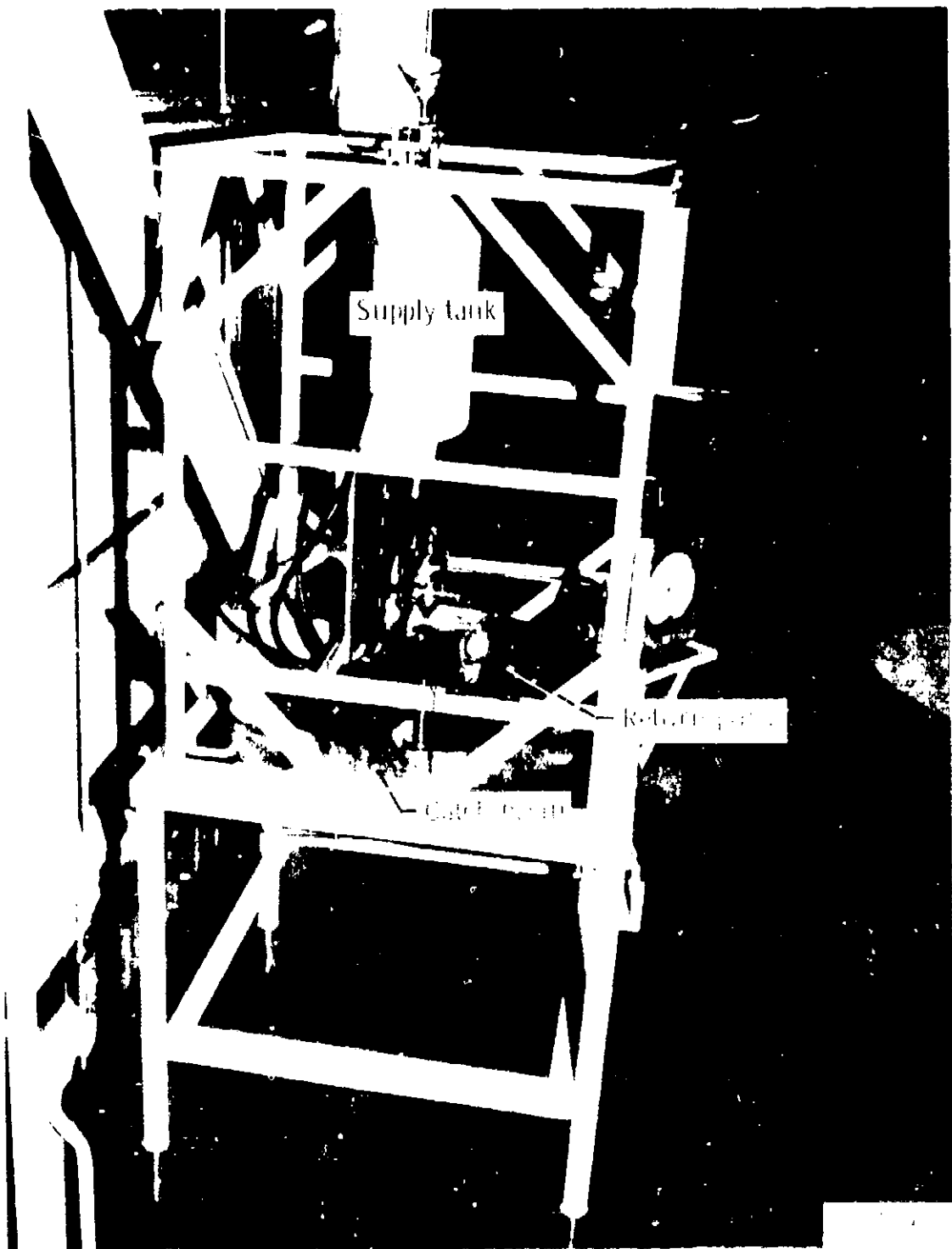


Figure 32(b). - Experimental test rig - side view.

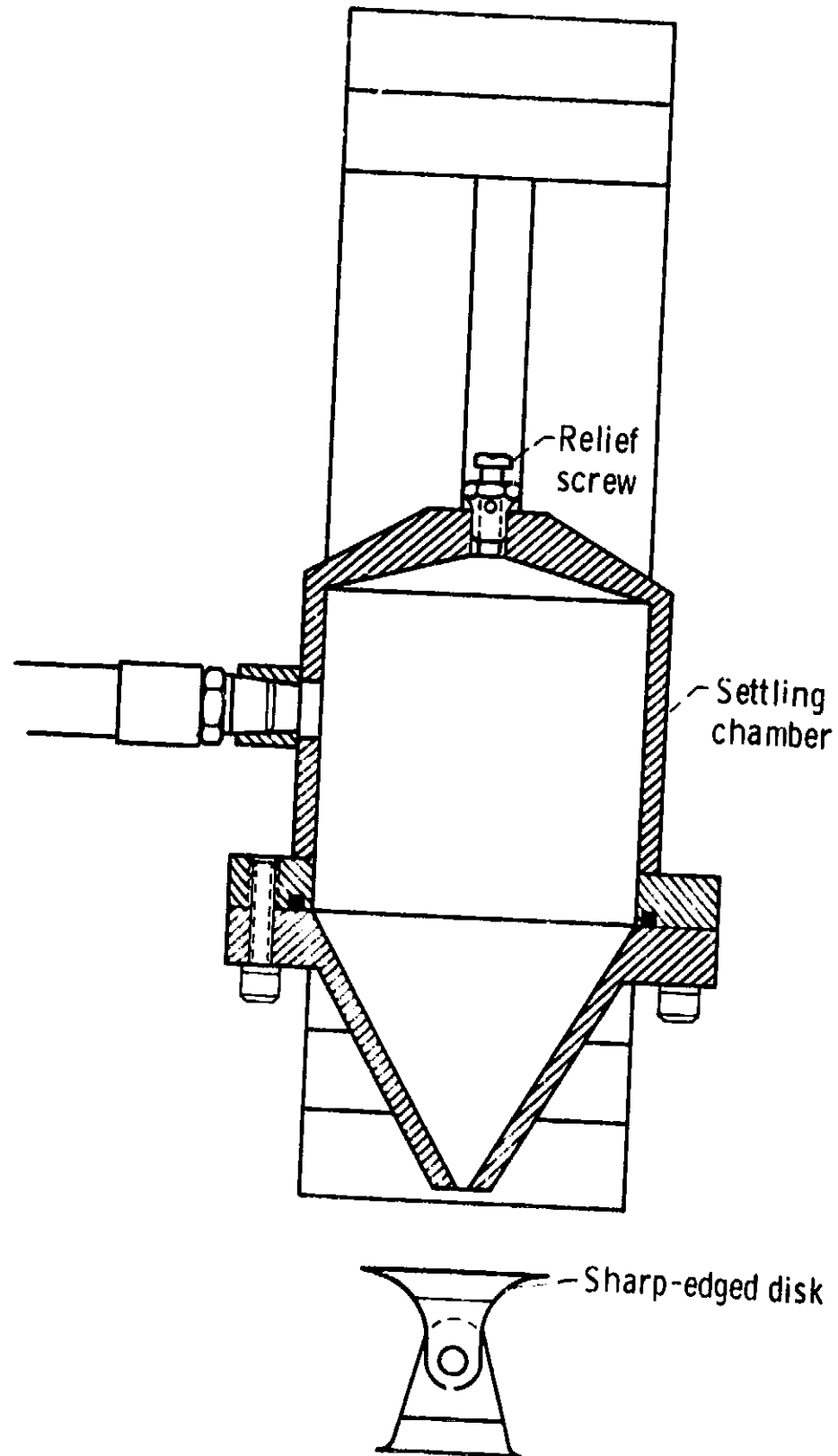


Figure 33. - Cross-section of settling chamber.

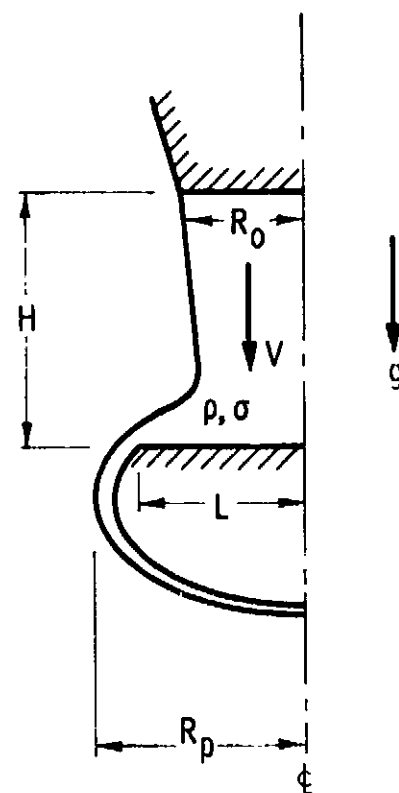


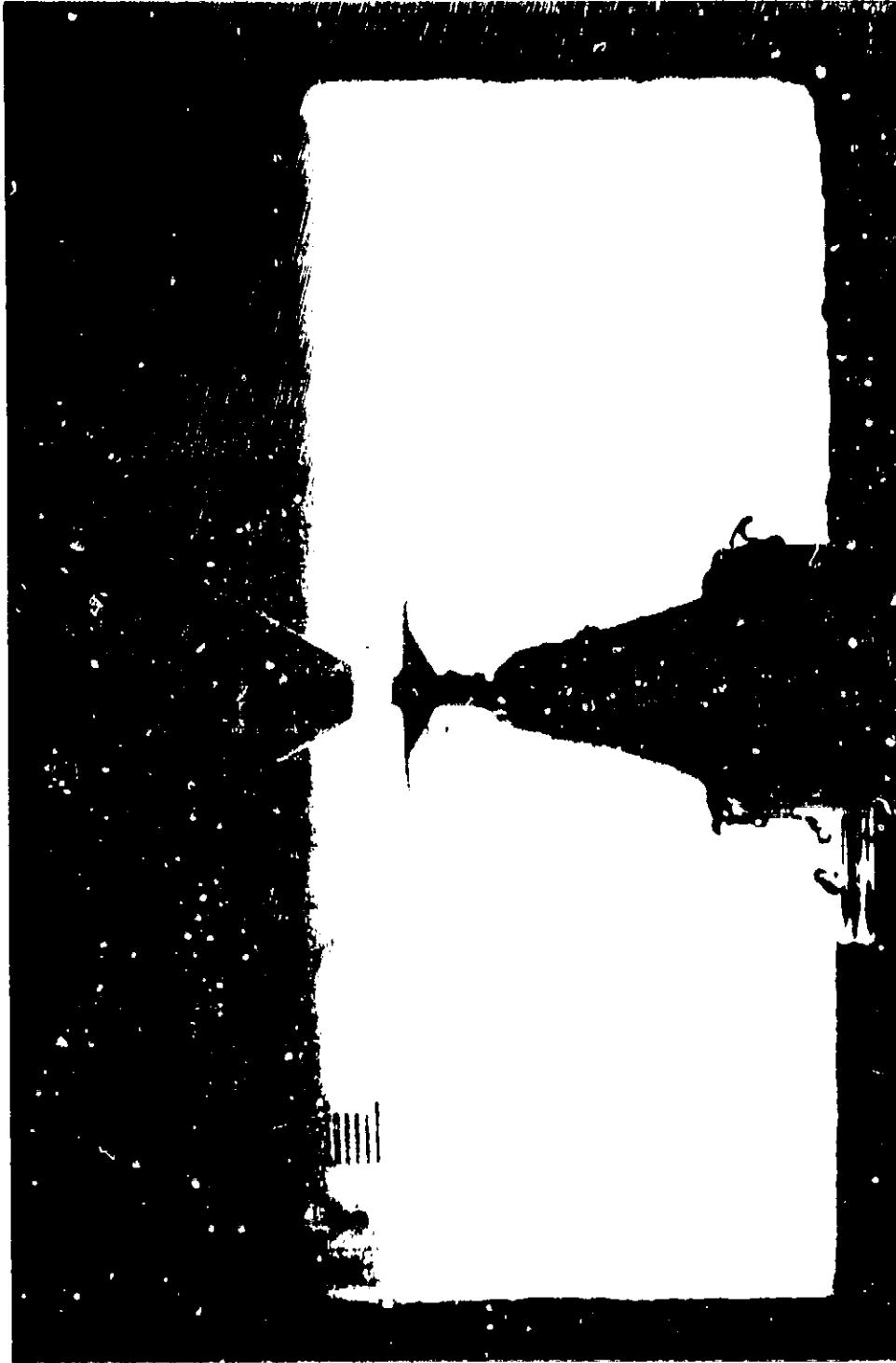
Figure 35. - Schematic of steady state normal gravity impingement.

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Figure 34. - Photograph of sharp edge disks.

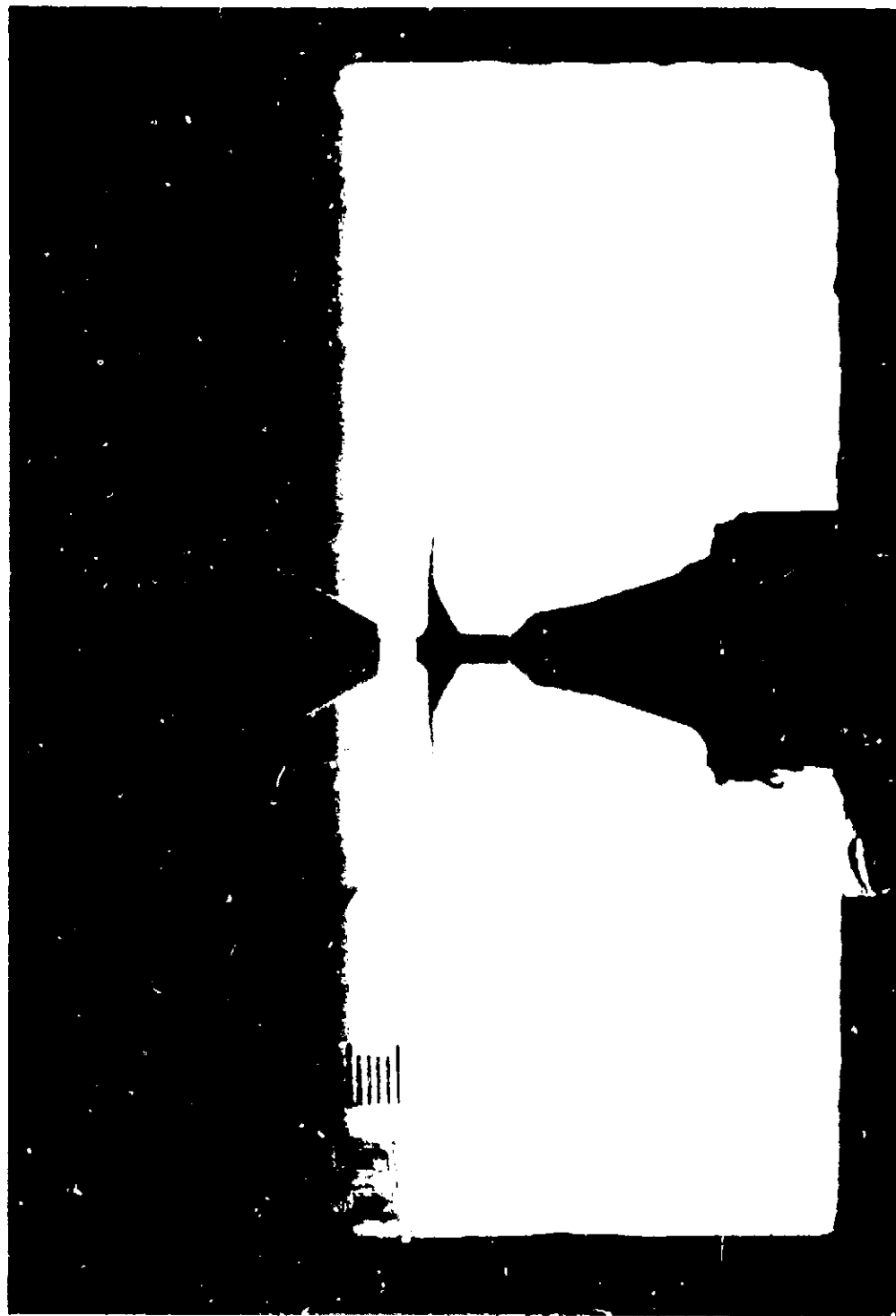


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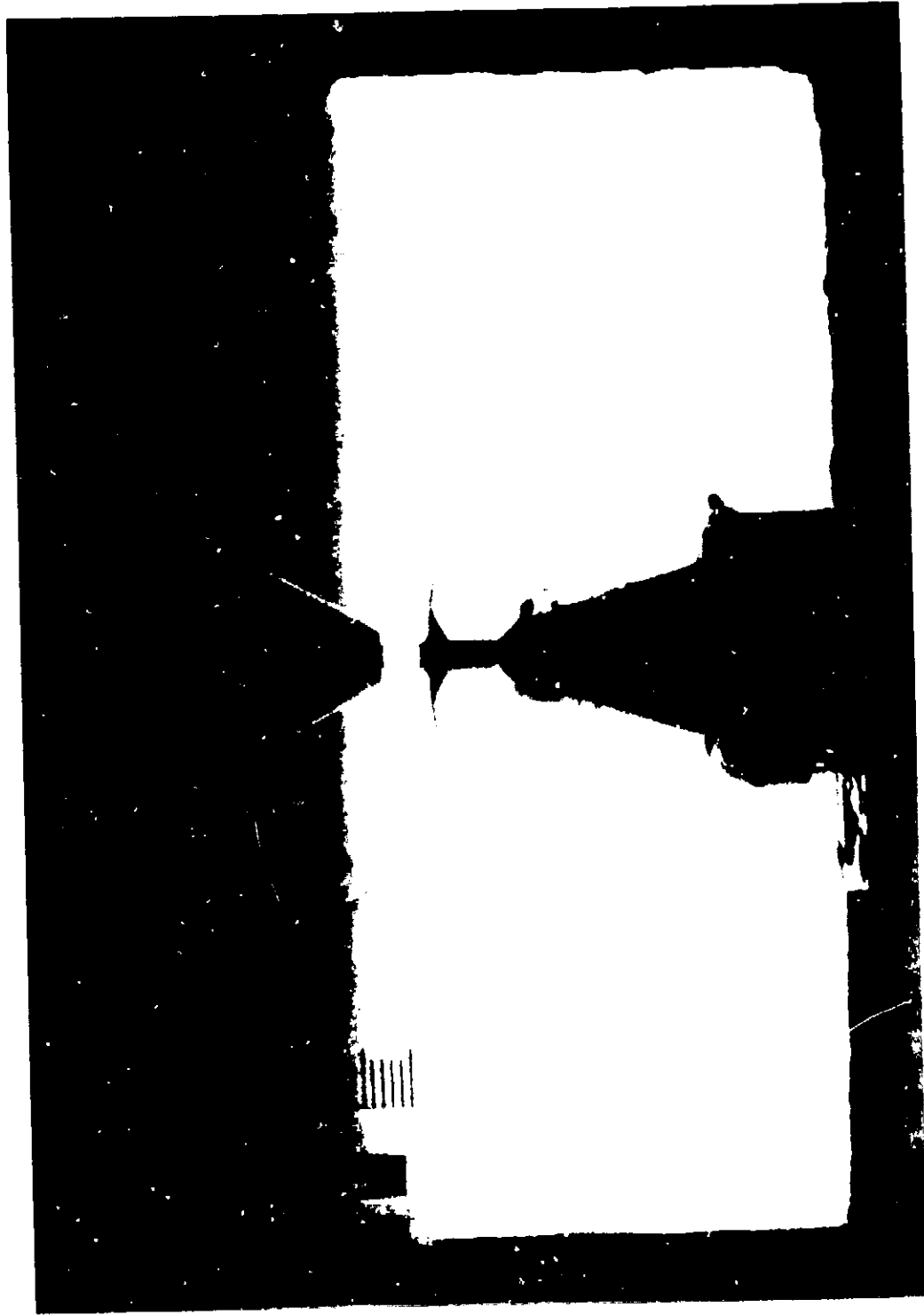
(a) Disc radius, 3.0 cm.

Figure 36. - Test liquid, distilled water; nozzle diameter, 0.5 cm; jet velocity, 286 cm/sec; distance between nozzle and disk, 1 cm.



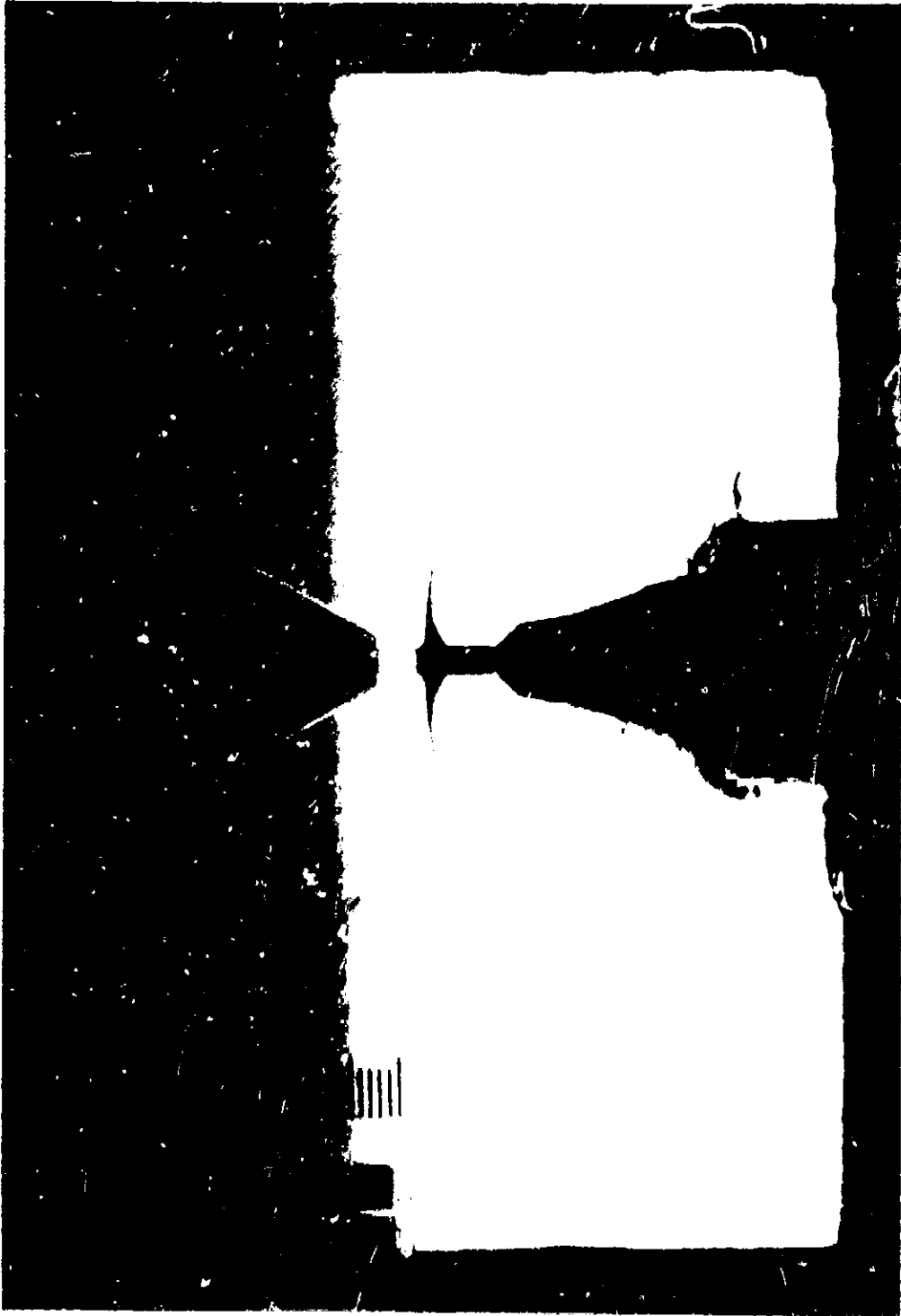
(b) Disk radius, 3.0 cm.

Figure 36. - Continued.



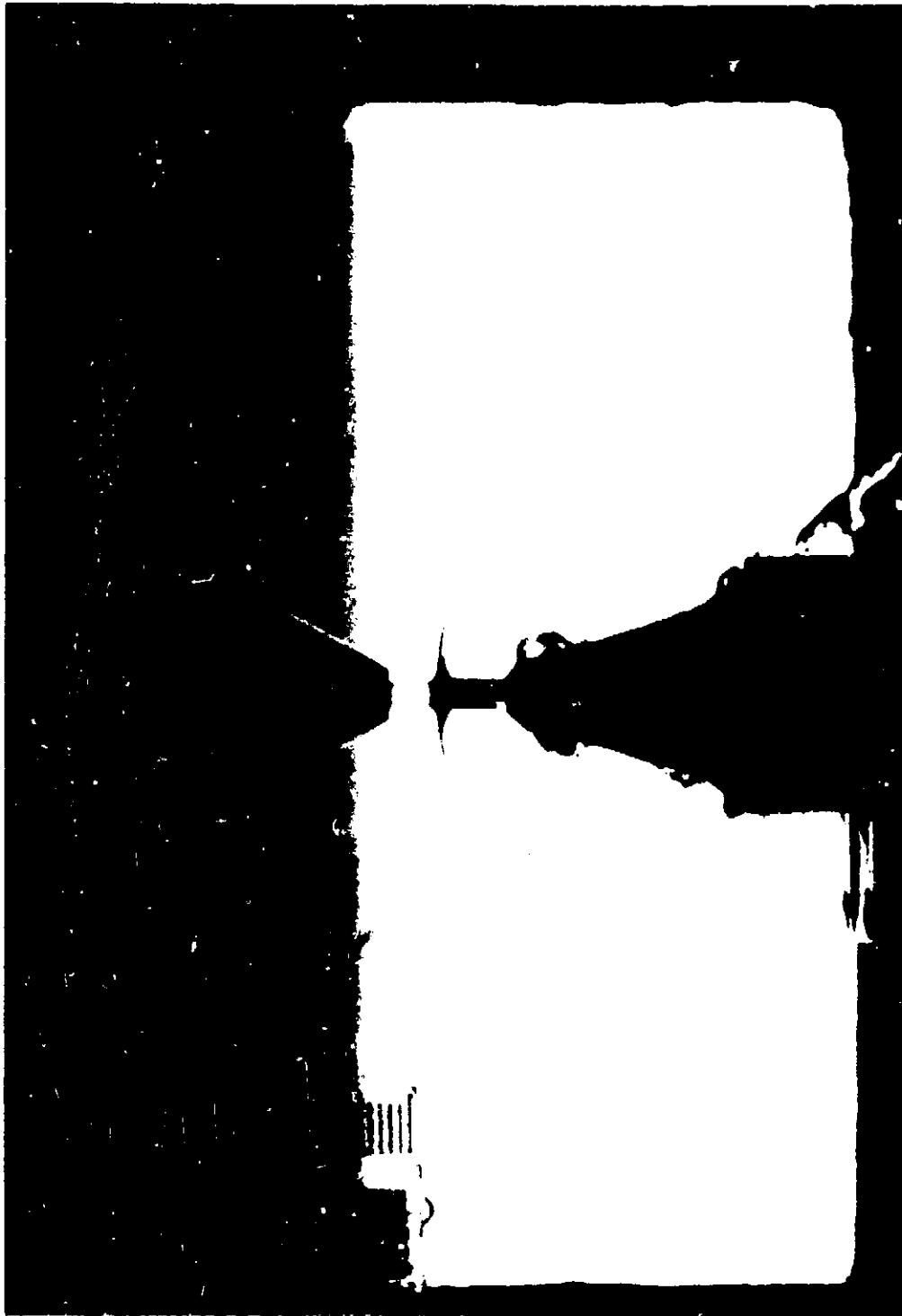
(c) Disk radius, 2.0 cm.

Figure 36. - Continued.



(d) Disk radius, 2.0 cm.

Figure 36. - Continued.



(e) Disk radius, 1.5 cm.

Figure 36. - Continued.

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(f) Disk radius, 1.5 cm.

Figure 36. - Concluded.

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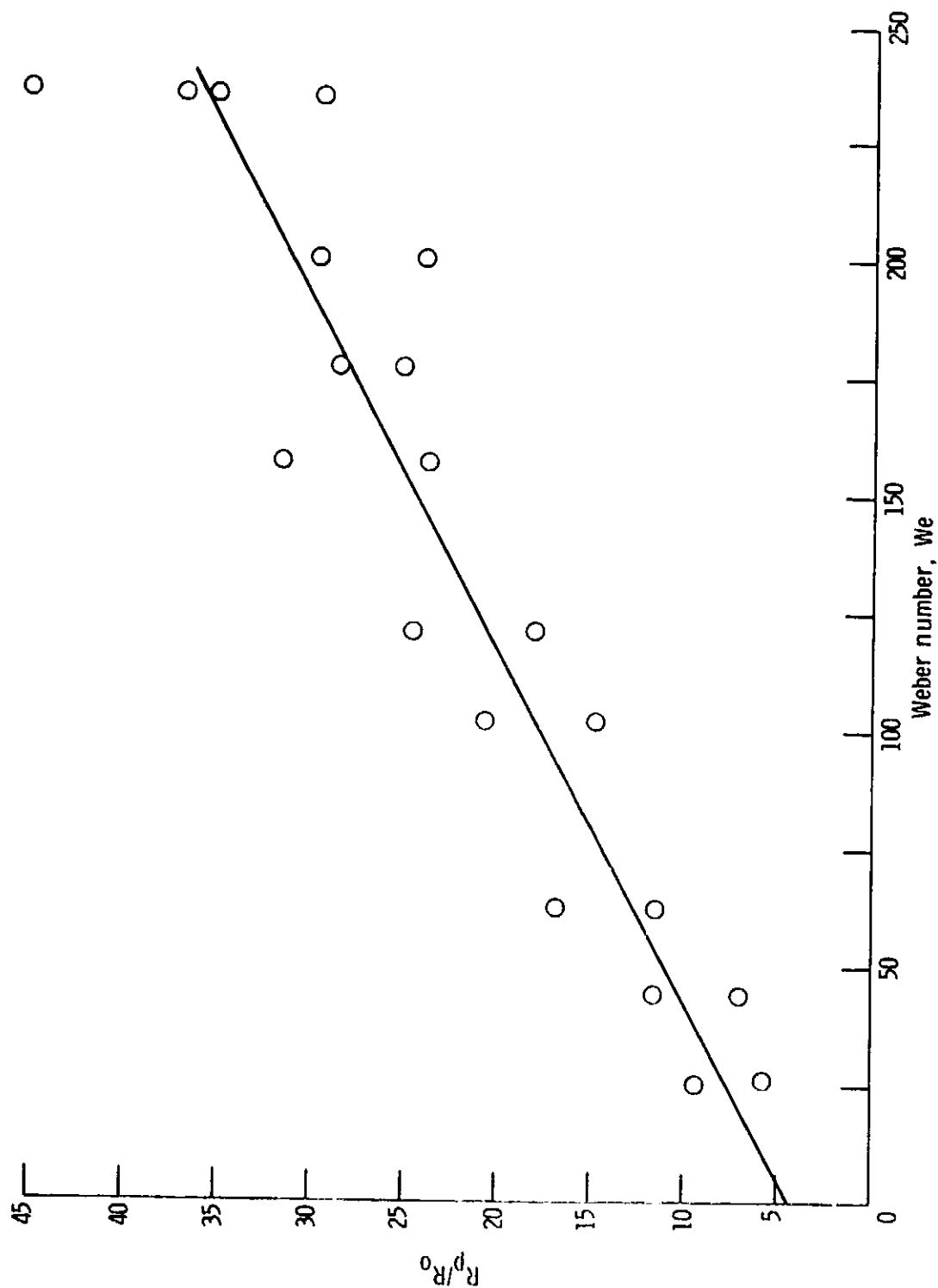


Figure 37. - Variation of plume width with Weber number  $R_p/R_0 = 4.3968 + 0.1334 We$ .

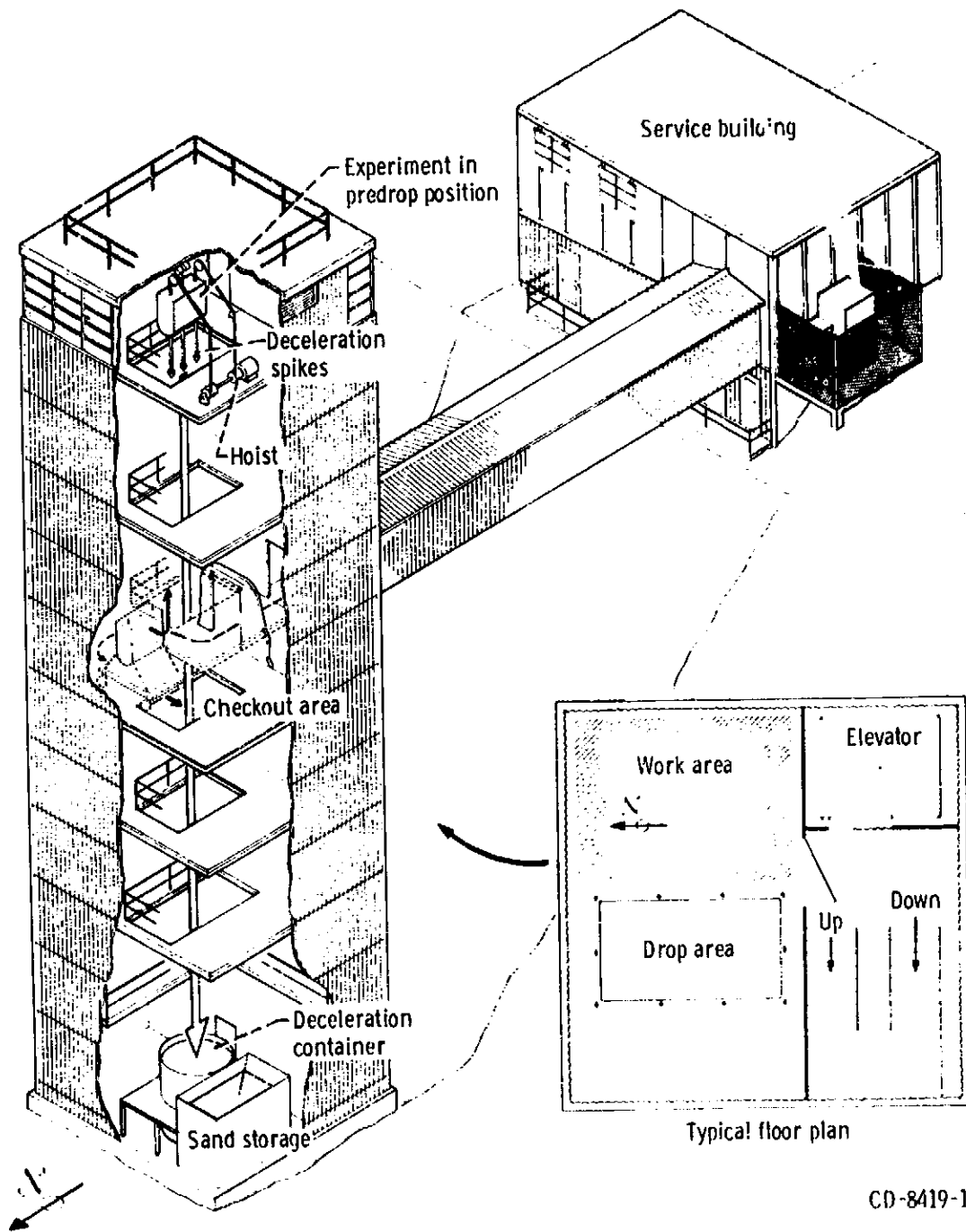
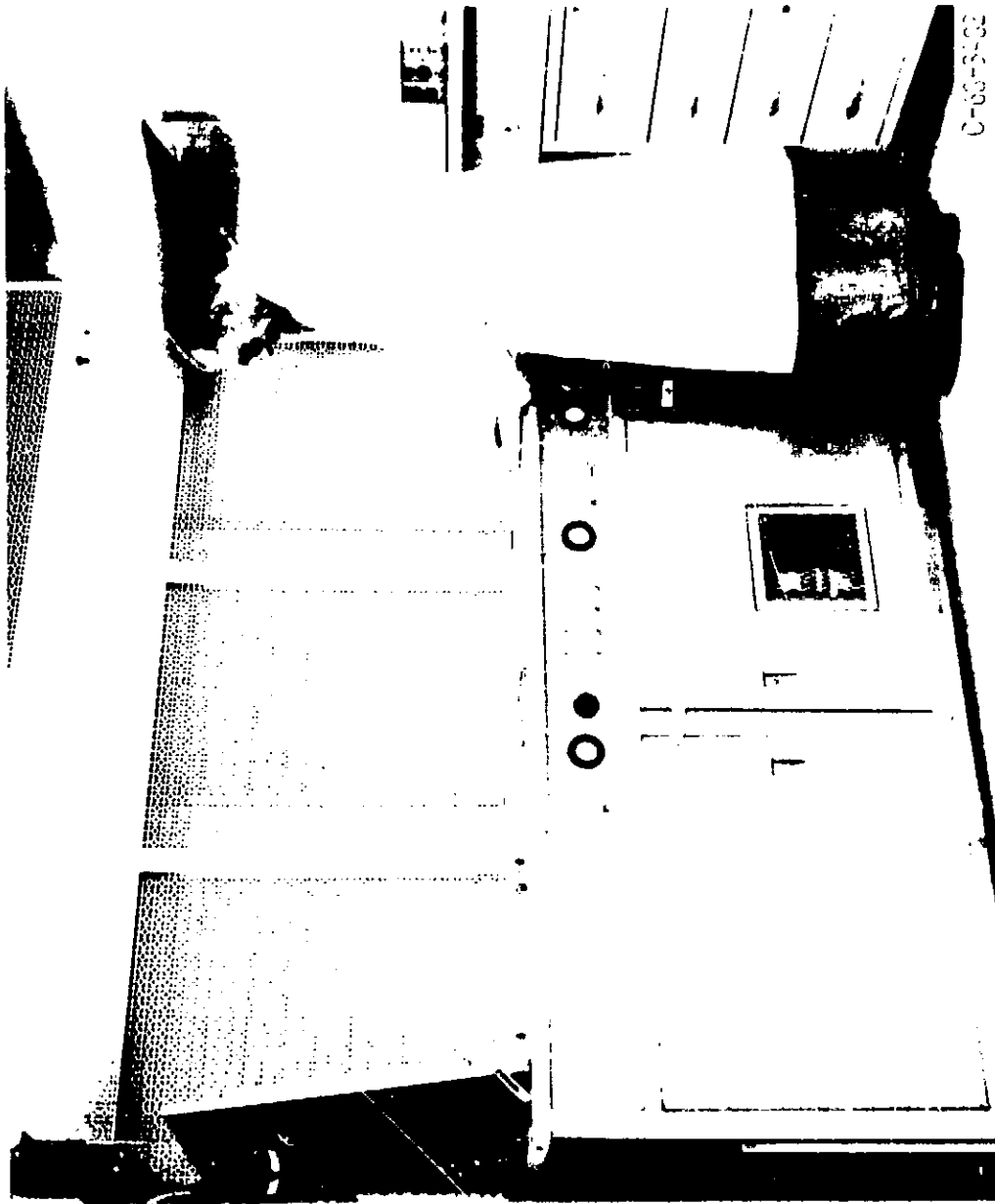


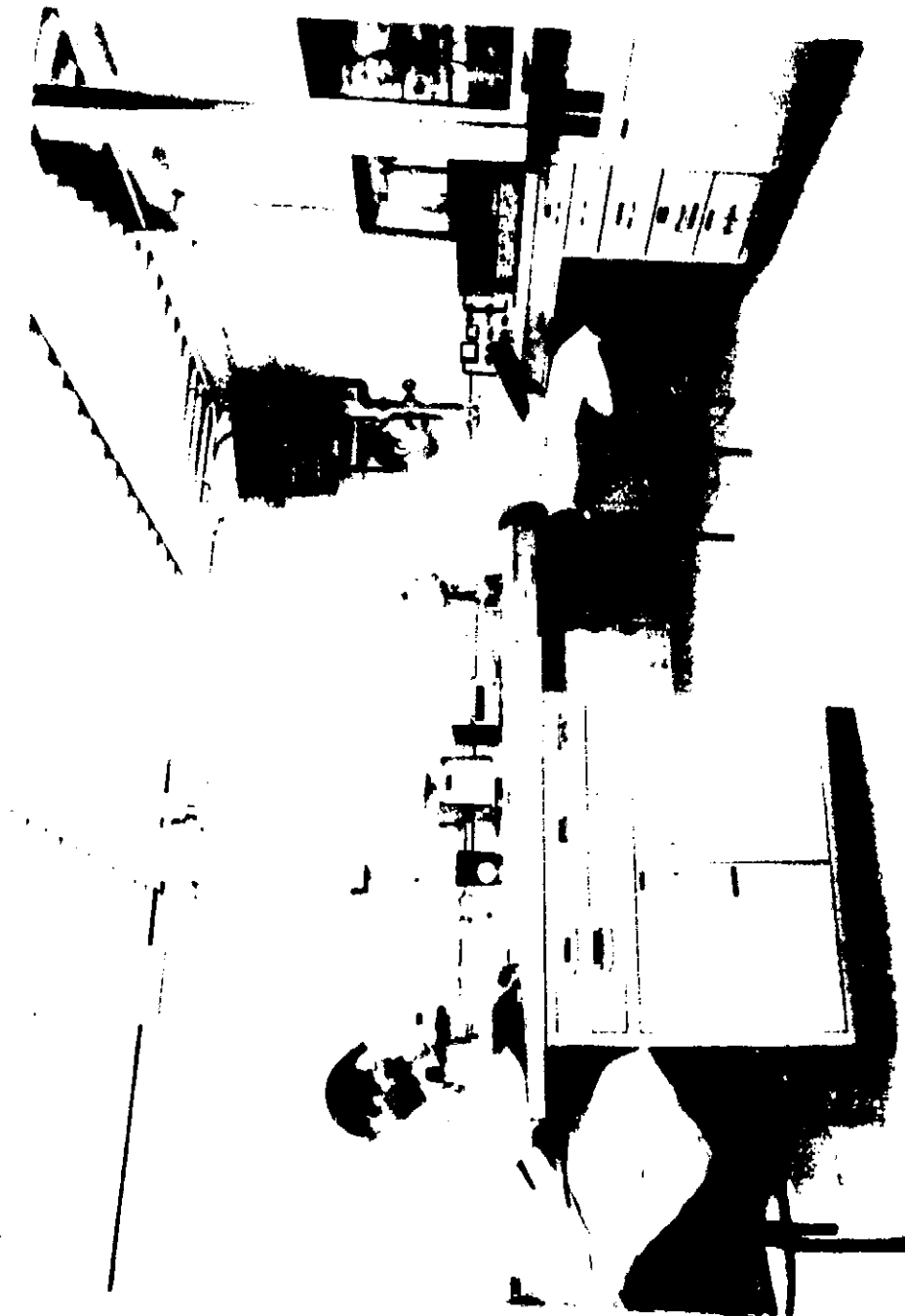
Figure B1. - 2.2-Second zero-gravity facility.





(a) Ultrasonic cleaning system.

Figure B2. - Controlled environment room.



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(b) Laboratory equipment.  
Figure 82. - Concluded.

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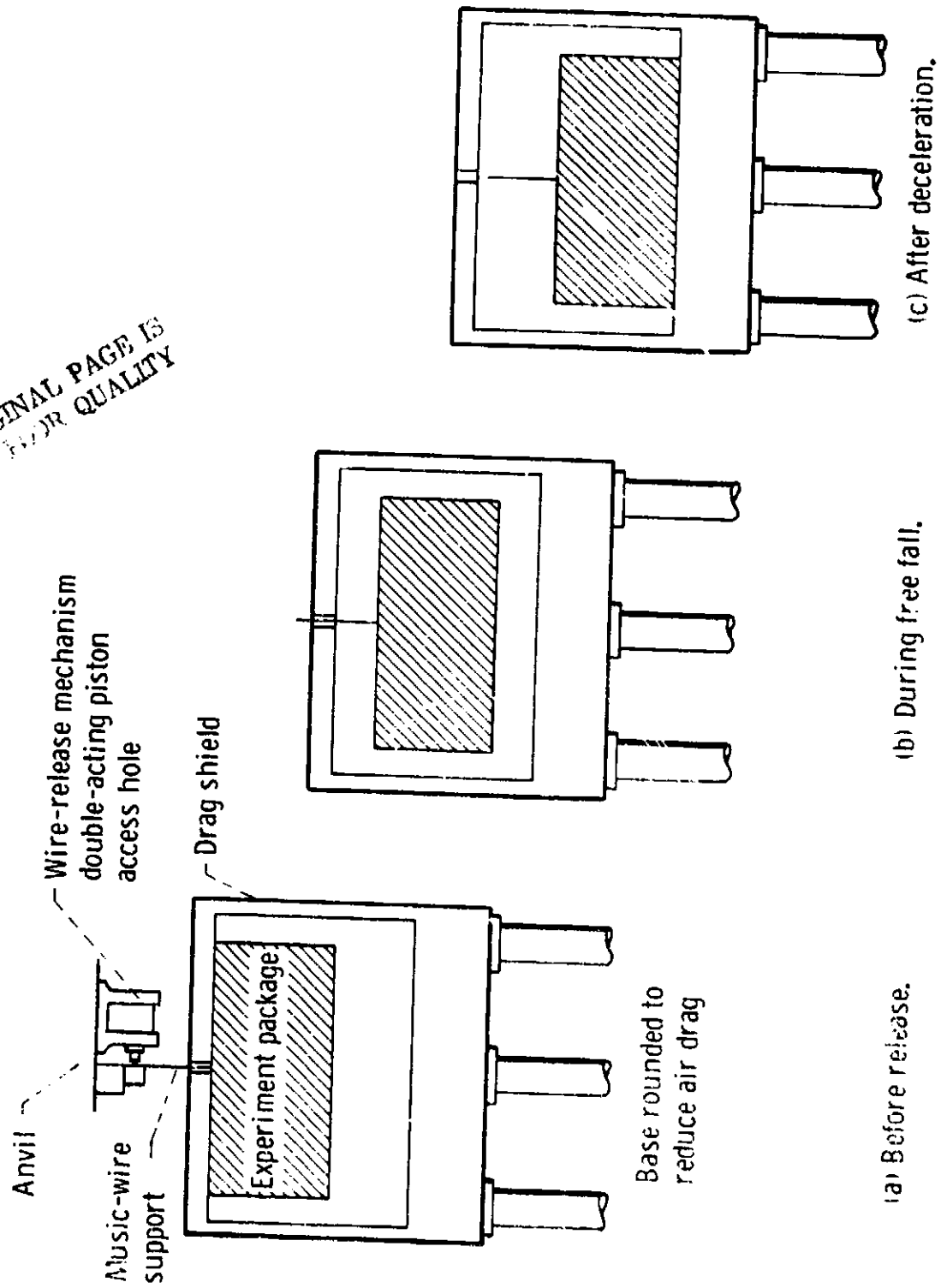


Figure B3. - Position of experiment package and drag shield before, during, and after test drop.