

CRYOGENIC FLUID TRANSFER - ORBITAL TRANSFER VEHICLE

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EP6598

ORGANIZATION:  
STRUCTURES & PROPULSION  
LABORATORY EP43  
CHART NO.:

MARSHALL SPACE FLIGHT CENTER  
CRYOGENIC FLUID TRANSFER  
ORBITAL TRANSFER VEHICLE

NAME:  
LEON J. HASTINGS

DATE:  
JUNE 1982

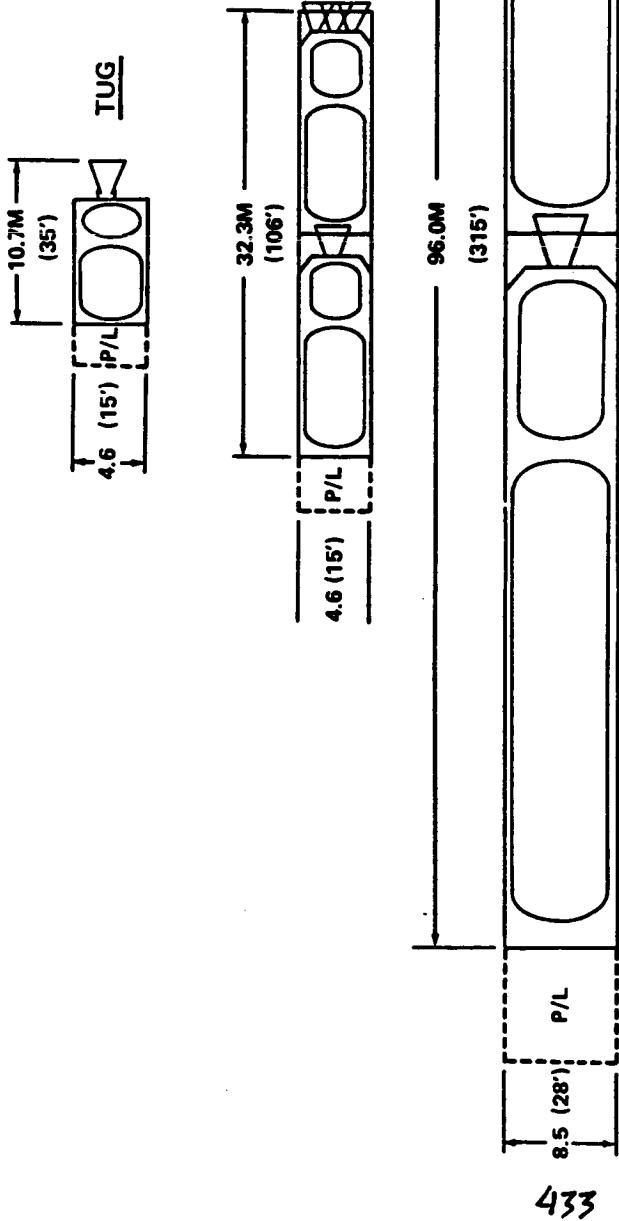
PRESENTATION OUTLINE

- ✓ REQUIREMENT OVERVIEW
  - OTV CONFIGURATIONS
  - SIZE RANGE
  - INTERNAL HARDWARE
  - GENERAL REFUELING CONCEPT
- DESIGN/TECHNOLOGY CONSIDERATIONS
  - TANK CHILLDOWN
  - INITIAL TANK CONDITIONS
  - CHILLDOWN THERMODYNAMICS
  - TANK FILL
  - FILL THERMODYNAMICS
  - SUPPLY TANK EFFECTS
  - SPECIAL ISSUES
  - RESIDUALS
  - START BASKET OR TANK PRESENCE
- CONCLUSIONS

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OTV CONFIGURATION OVERVIEW

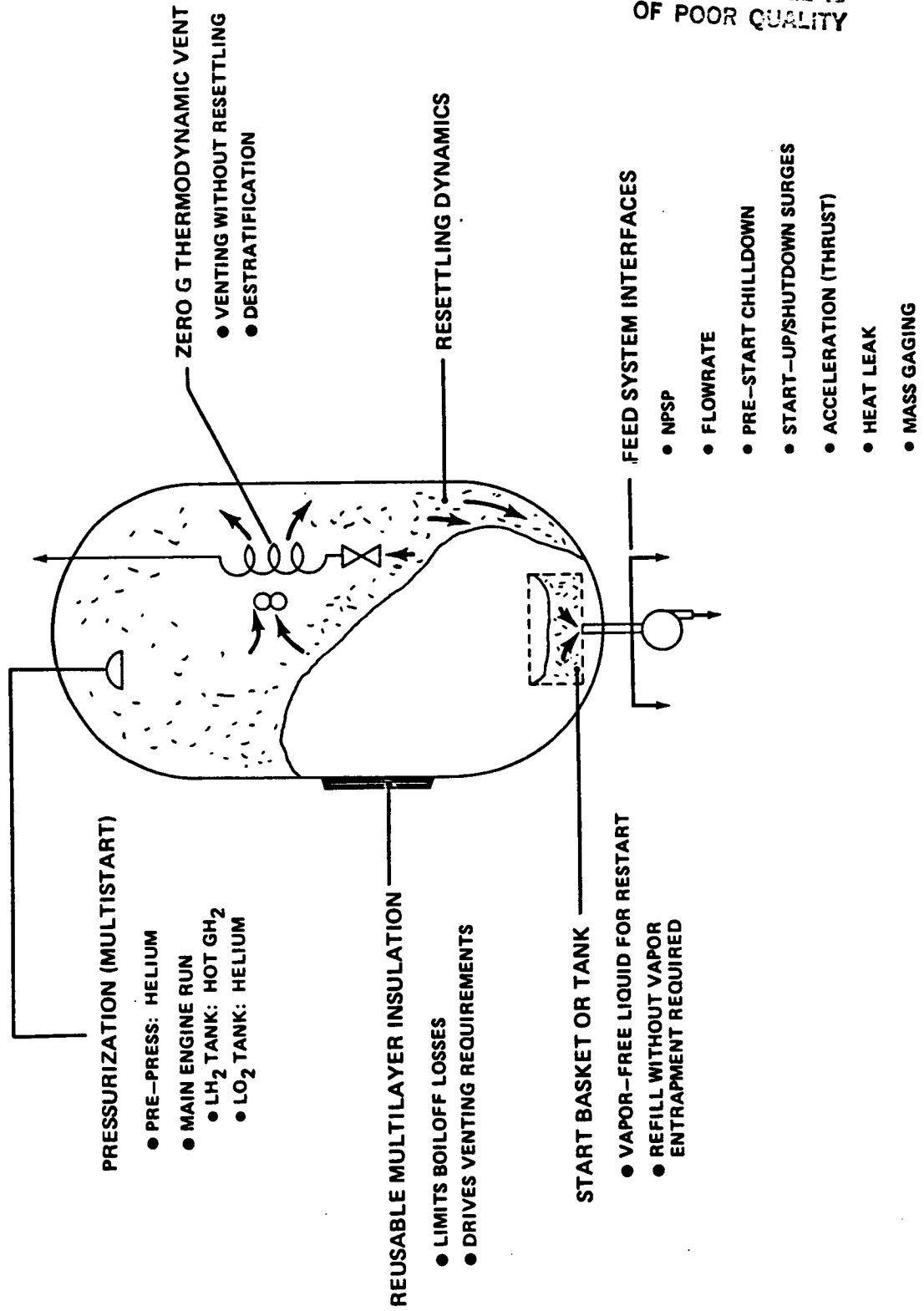
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VEHICLE	PROPELLANT	TANK VOLUME M <sup>3</sup> (FT <sup>3</sup> )	PROPELLANT LOAD KG (LB)	OPERATING PRESS kN/M <sup>2</sup> (PSI)	MISSION
POTV	LO <sub>2</sub>	41 (1450)	44,550 (99,000)	172 (25)	4 MEN FROM LEO TO GEO AND RETURN OR 100K TO GEO AND 60K RETURN WITH GEO REFUELING
COTV	LH <sub>2</sub>	116 (4100)	7,875 (17,500)	172 (25)	500K FROM LEO TO GEO

# OTV CRYOGEN MANAGEMENT CONSIDERATIONS

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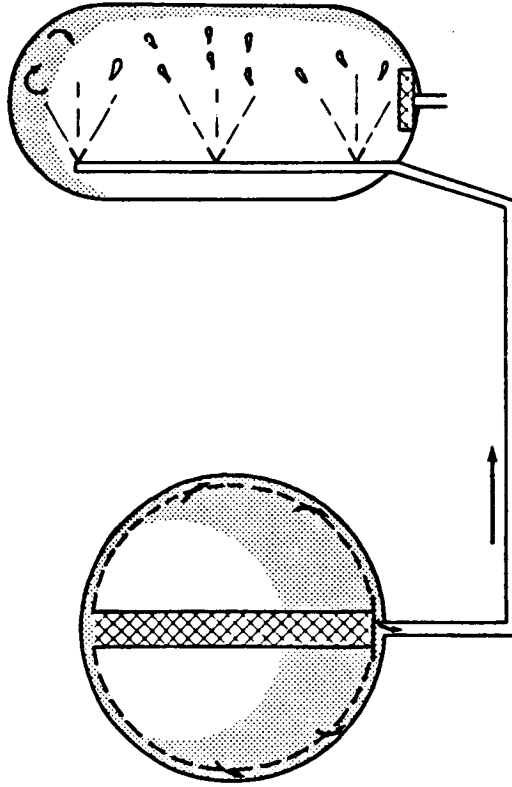


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ORBITAL CRYOGEN TRANSFER CONSIDERATIONS

- RECEIVER (OTV)
- PRECHILL
  - INLET FLOWRATE/DISTRIBUTION
  - WALL CHILLDOWN
  - NO VENT FILL
  - NON-EQUILIBRIUM THERMODYNAMICS
  - HELIUM PRESENCE
  - START BASKET REFILL
  - MASS GAUGING

- SUPPLY TANK
- STORAGE/VENTING
  - ACQUISITION/EXPULSION
  - LIQUID ORIENTATION
  - BOILING/SCREEN DRYING
  - PRESSURIZATION
  - OUTFLOW RATE
  - RESIDUALS



- TRANSFER LINE
- CHILLDOWN - PRESSURE SURGES
  - FLUID LOADS
  - TRANSIENT
  - STEADY-STATE

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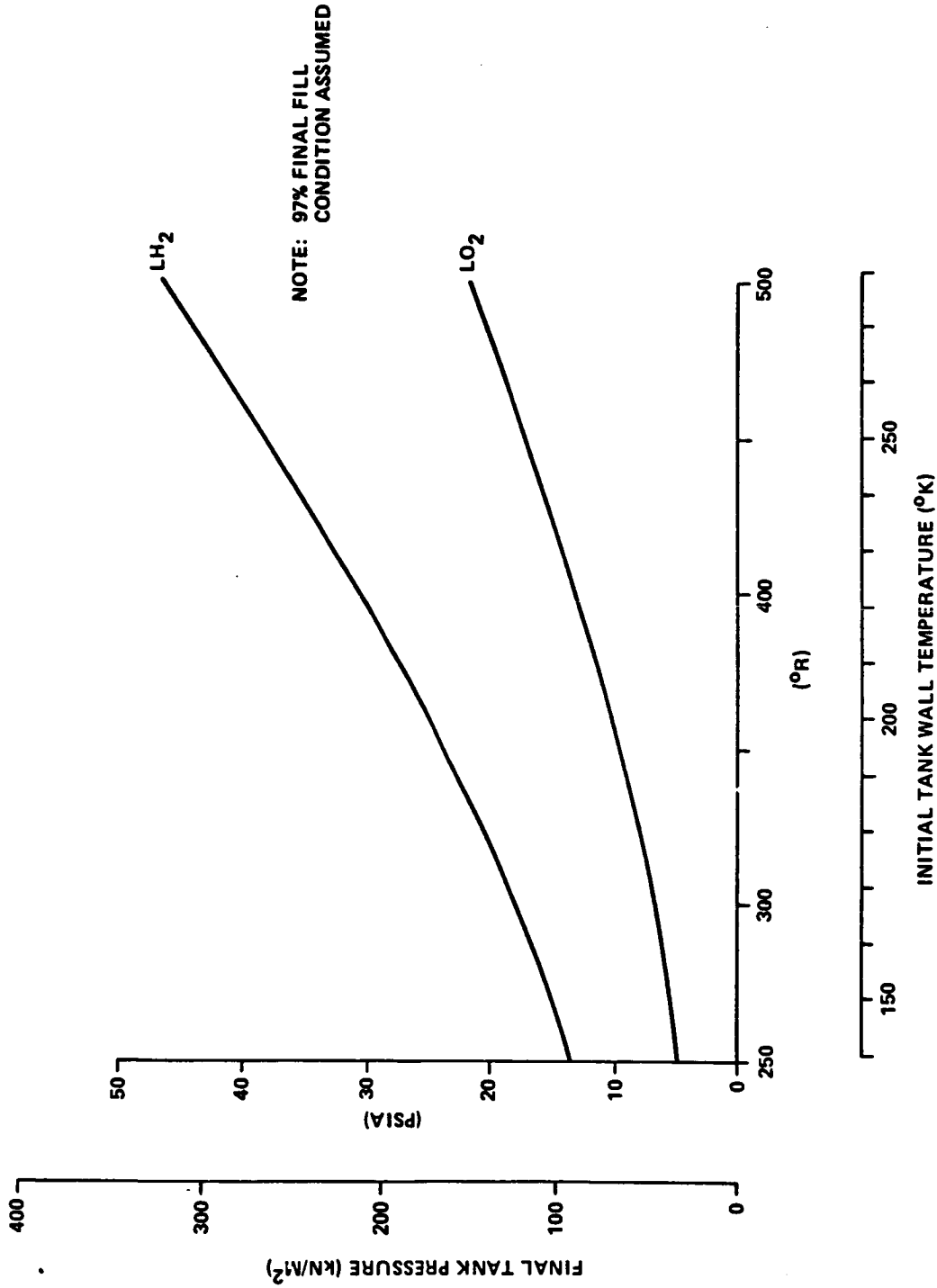
### ✓ DESIGN/TECHNOLOGY CONSIDERATIONS

- TANK CHILLDOWN
- INITIAL TANK CONDITIONS
- CHILLDOWN THERMODYNAMICS
- TANK FILL
- FILL THERMODYNAMICS
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### CONCLUSIONS

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INITIAL WALL TEMPERATURE EFFECTS ON POTV  
LH<sub>2</sub> TANK PRESSURES AFTER FILL

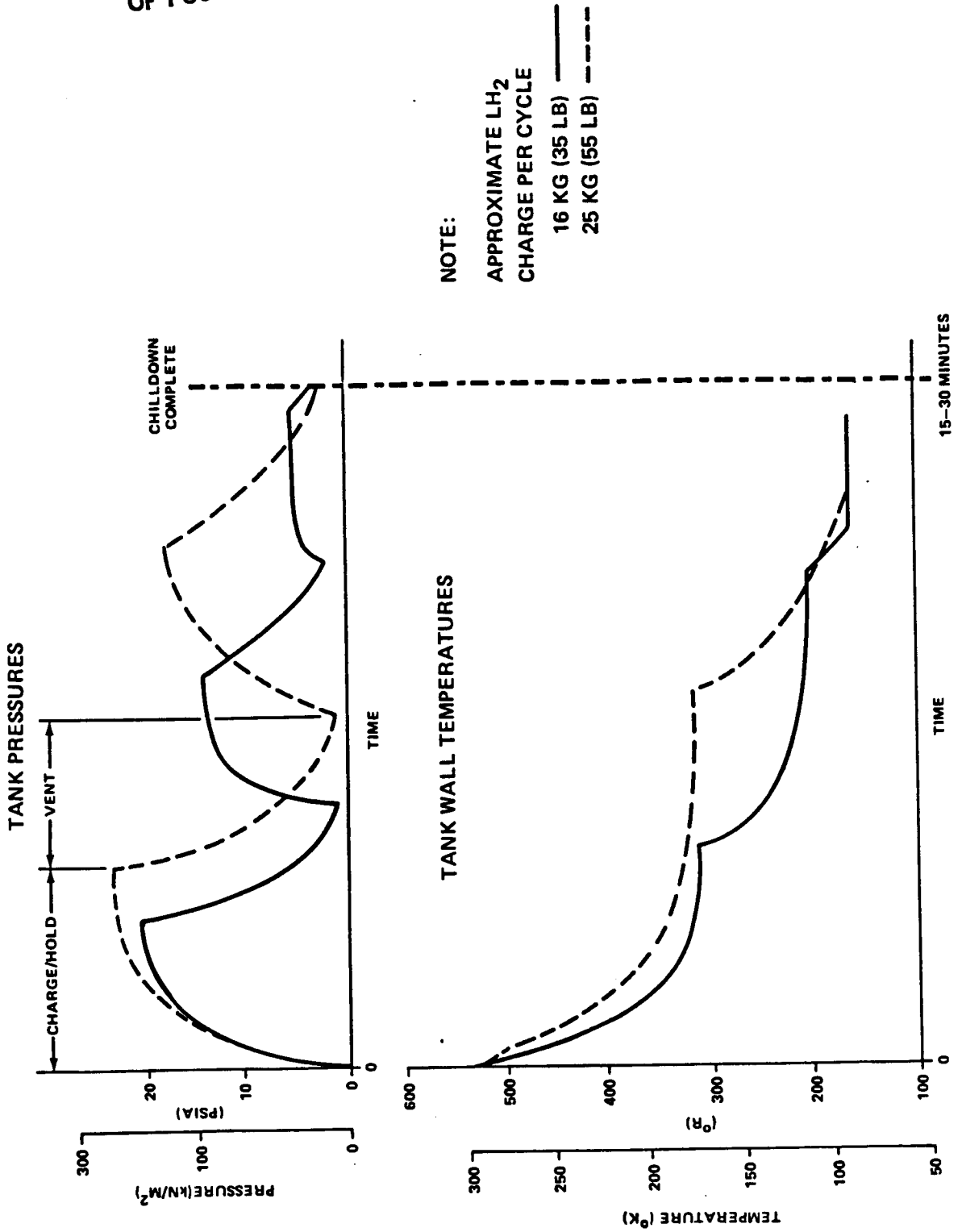


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POTV LH<sub>2</sub> TANK THERMODYNAMICS DURING CHILLDOWN

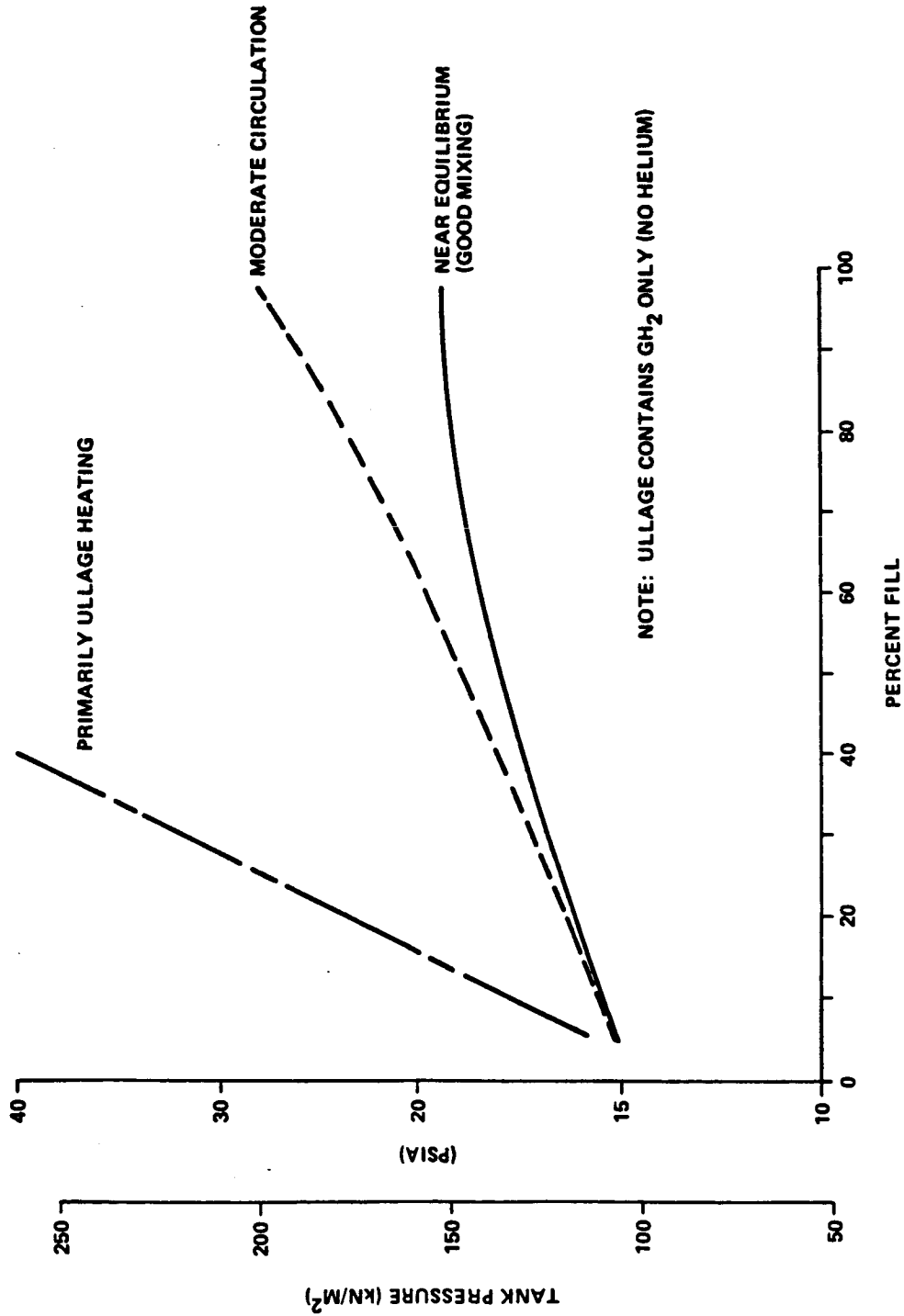
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# POTV LH<sub>2</sub> TANK PRESSURES DURING ORBITAL FILL

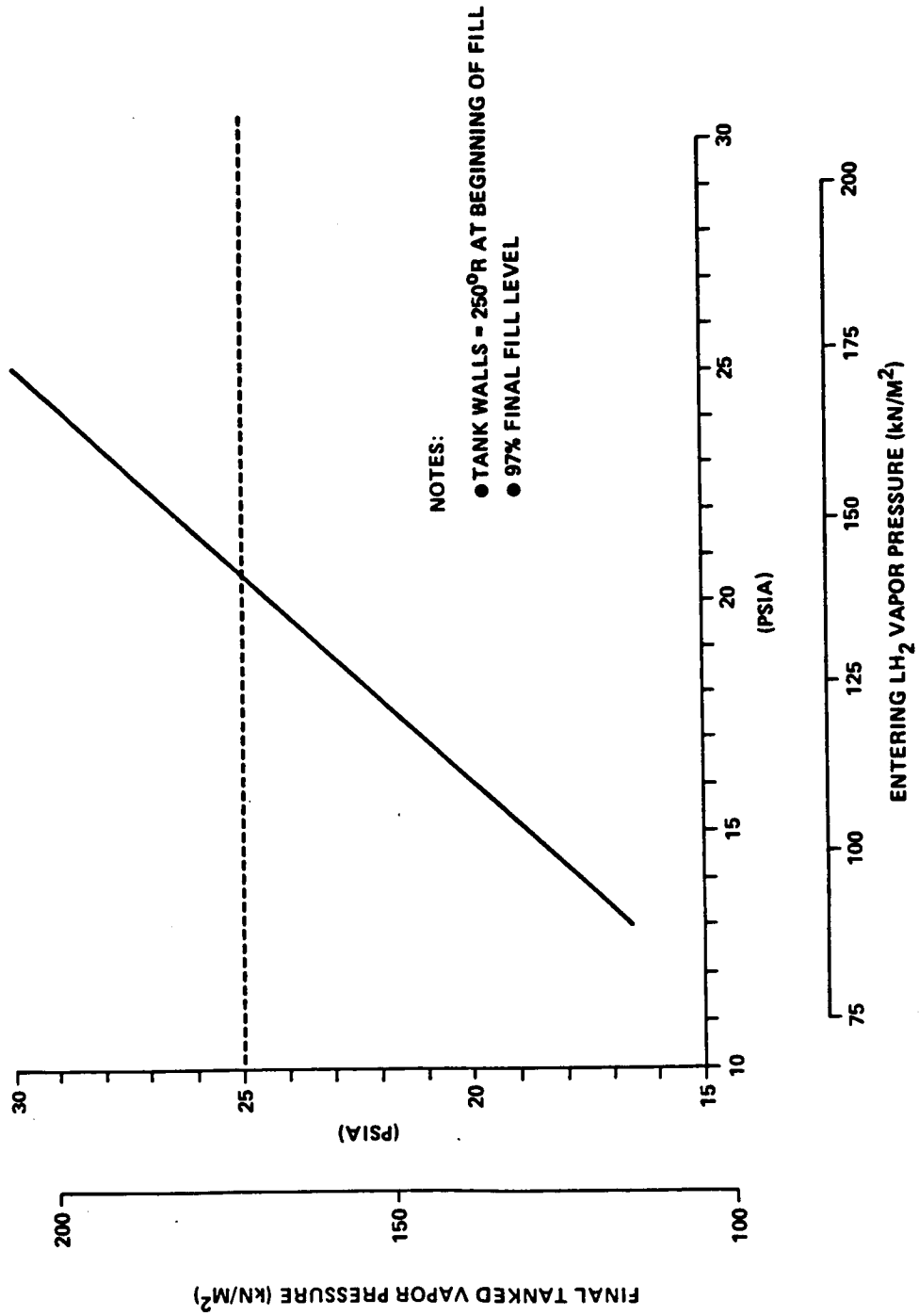


NOTE: ULLAGE CONTAINS GH<sub>2</sub> ONLY (NO HELIUM)

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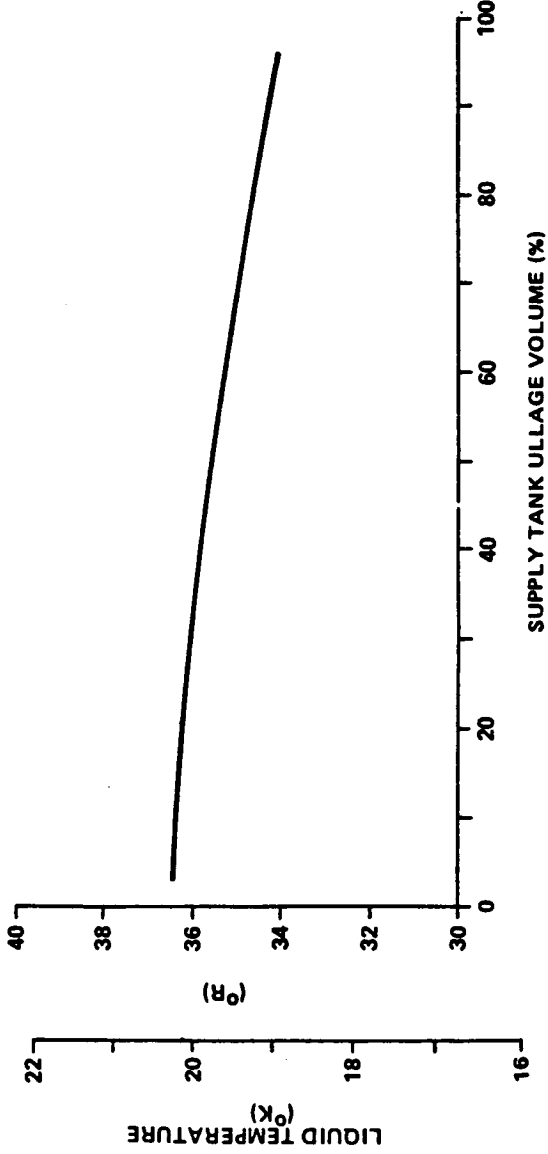
ENTERING LH<sub>2</sub> VAPOR PRESSURE EFFECTS ON POTV  
TANK PRESSURE AT FILL COMPLETION



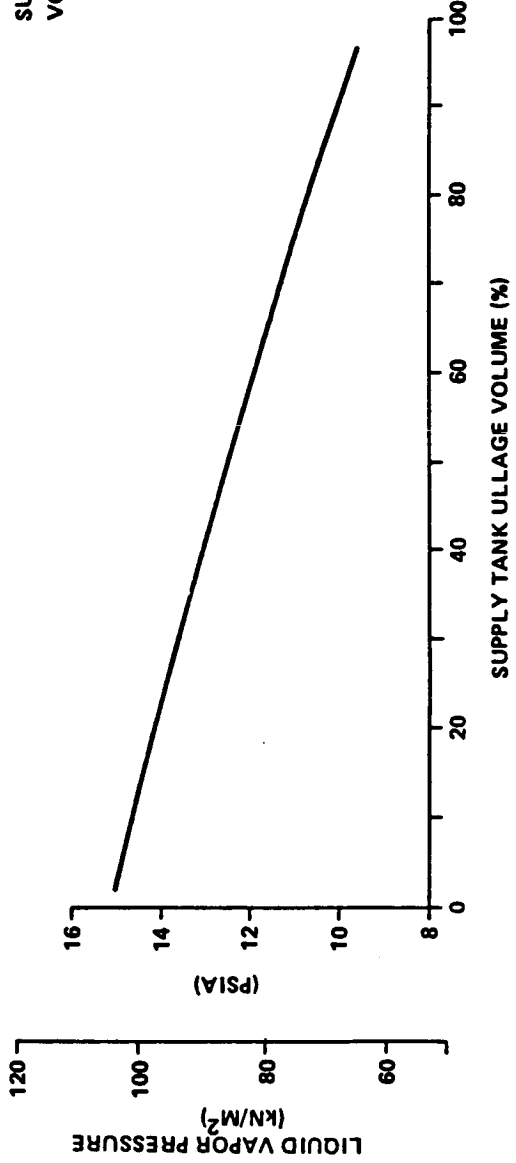
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# LH<sub>2</sub> SUPPLY TANK THERMODYNAMIC CONDITIONS

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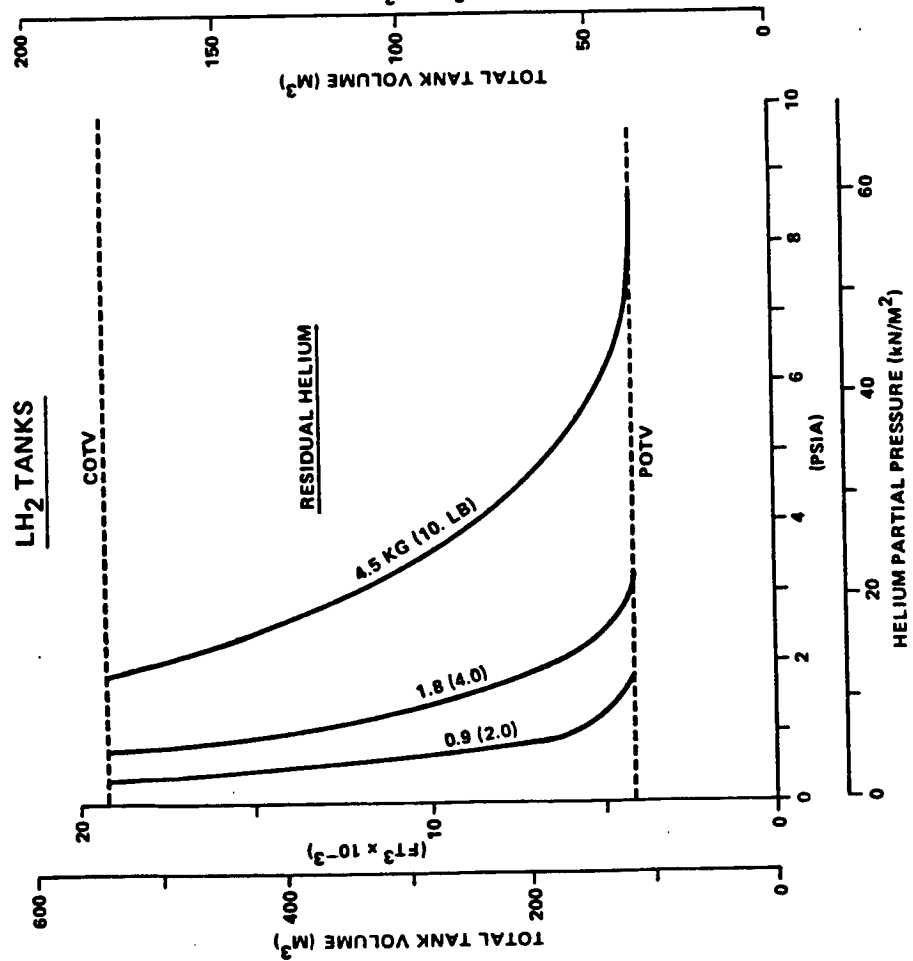
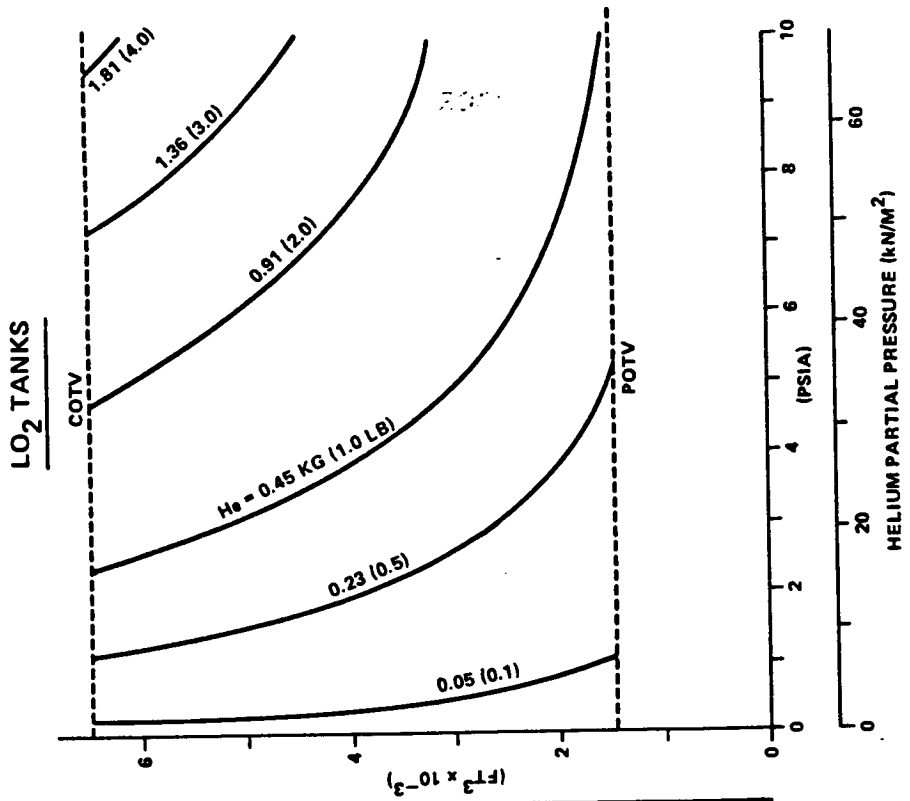


SUPPLY TANK  
VOLUME = 85M<sup>3</sup> (3000 FT<sup>3</sup>)

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RESIDUAL HELIUM PARTIAL PRESSURES  
AT 97% FILL LEVEL

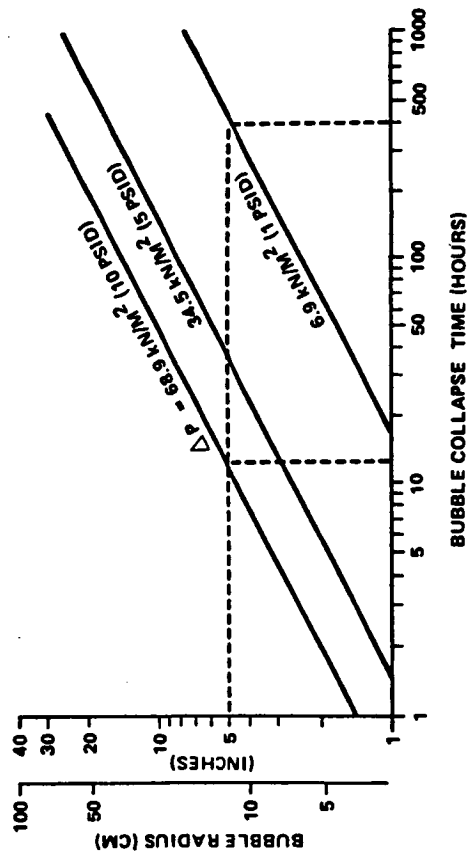
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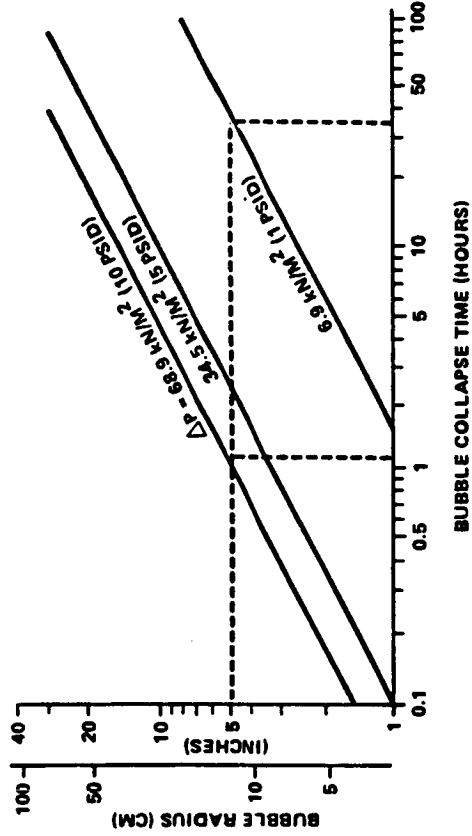
PROPELLANT BUBBLE COLLAPSE  
BY INCREASING ULLAGE PRESSURE

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LIQUID HYDROGEN



LIQUID OXYGEN



NOTE:  $\Delta P$  = ULLAGE PRESSURE - SATURATION PRESSURE

CONCLUSION: COLLAPSE OF BUBBLES IN START BASKETS  
COULD REQUIRE ACTIVE CIRCULATION

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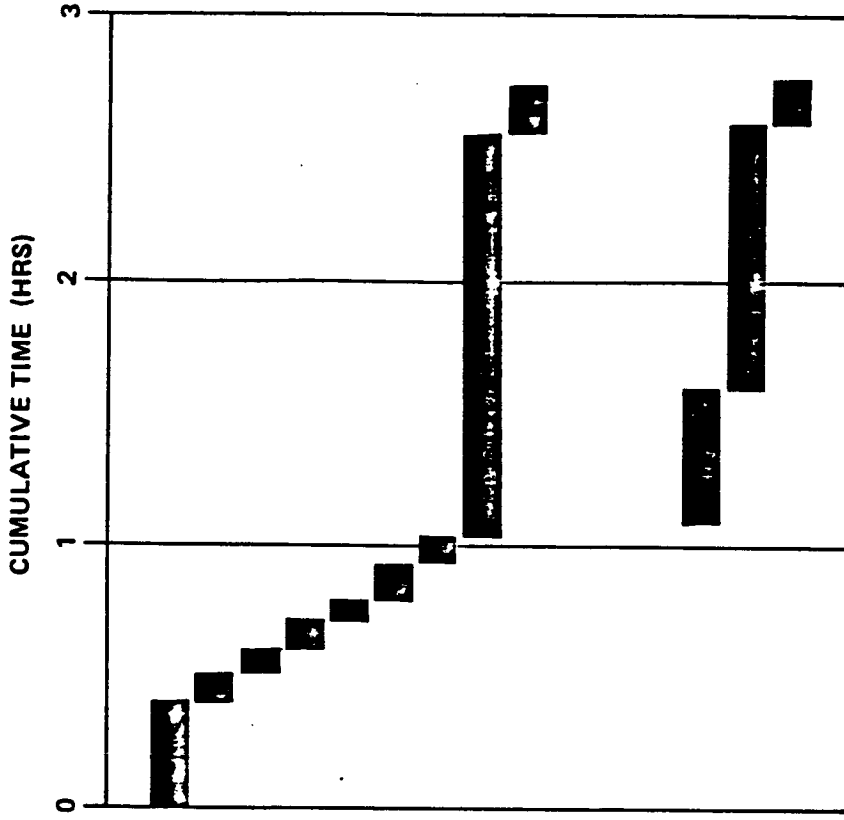
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### ✓ CONCLUSIONS

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POTV PROPELLANT TRANSFER TIMELINE



EVENT

- LH<sub>2</sub> TRANSFER
  - 1) INITIAL LH<sub>2</sub> TANK VENT
    - INJECT LH<sub>2</sub> AND HOLD
    - VENT TANK
  - 2) PRECHILL
    - INJECT LH<sub>2</sub> AND HOLD
    - VENT TANK
  - 3) FILL
    - INJECT LH<sub>2</sub> AND HOLD
    - VENT TANK
    - LH<sub>2</sub> TRANSFER
    - TOPPING FLOW RATE
- LO<sub>2</sub> TRANSFER
  - 1) INITIAL LO<sub>2</sub> TANK VENT\*
    - LO<sub>2</sub> TRANSFER
    - TOPPING FLOW RATE
  - 2) FILL

NOTES:

- TWO OR MORE ADDITIONAL VENT CYCLES REQUIRED IF HELIUM PRESENT
- TIMELINE IS FOR REFUELING TO 50% LEVEL

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## CONCLUSIONS

### PRE-CHILL PREPARATIONS

● DILUTION OF HELIUM RESIDUALS PRIOR TO REFUELING REQUIRED TO PREVENT:

- EXCESSIVE PRESSURES AT END OF FILL
- INACCURATE KNOWLEDGE OF PROPELLANT VAPOR PRESSURES
- START BASKET HELIUM ENTRAPMENT
- INACCURATE THERMODYNAMIC MASS GAUGING
- APPROXIMATE DILUTION LEVELS REQUIRED (POTV)

● LH<sub>2</sub> < .9 KG (2 LBS)

● LO<sub>2</sub> < .09 KG (.2 LBS)

} FURTHER DILUTION REQUIRED IF  
THERMODYNAMIC MASS GAUGING  
UTILIZED

- PROCEDURAL/TECHNOLOGY CONCERNS
- DURATION OF VENT/HOLD CYCLES
- KNOWLEDGE OF HELIUM RESIDUAL MAGNITUDE

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### TRANSFER LINE/TANK CHILLDOWN:

- REQUIREMENT: REDUCE TRANSFER LINE/TANK WALL TEMPERATURES SUFFICIENTLY TO PREVENT EXCESSIVE LINE PRESSURE/FLOW SURGES AND TO ENABLE A NON-VENTED TANK FILL
- PROCEDURAL/TECHNOLOGY CONCERNS:
  - TANK CHARGE/HOLD/VENT CYCLE DEFINITION
  - SEMI-EMPIRICAL MODELING LACKS EXPERIMENTAL DATA
  - LACK OF HARDWARE EXPERIENCE
  - WALL CHILLDOWN CRITERION: CURRENT RANGE = 95°K TO 200°K (170°R TO 360°R)
  - CHARGE MASS/FLOWRATE SELECTION: CURRENT LH<sub>2</sub> RANGE = 20 TO 70 KG (40 TO 155 LB) @ .5 TO 1.5 KG/SEC (1 TO 3 LB/SEC)
- LACK OF TRANSFER LINE CHILLDOWN EXPERIENCE – PREVENTION OF EXCESSIVE SURGES AND LINE LOADS
- INSTRUMENTATION TO MONITOR CHILLDOWN PROCESS

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### TANK FILL

- REQUIREMENT: LH<sub>2</sub> & LO<sub>2</sub> TANK FILL WITHOUT VENTING
- PROCEDURAL/TECHNOLOGY CONCERNS:
  - ASSURANCE OF ADEQUATE CIRCULATION TO MAINTAIN NEAR-THERMAL EQUILIBRIUM, i.e., LOW PRESSURES
  - GOOD MIXING/HEAT EXCHANGE BETWEEN ULLAGE/LIQUID REQUIRED
  - EXISTING SEMI-EMPIRICAL MODELS LACK EXPERIMENTAL DATA
  - LACK OF IN-FLIGHT HARDWARE EXPERIENCE
  - MECHANICAL MIXER PROBABLY REQUIRED
  - LACK OF ZERO-G MASS GAUGING DEVICE
  - SPECIAL FILL PROVISIONS FOR START BASKET
  - BLEED LINE FOR DIRECT FILL OF BASKET
  - ACTIVE CIRCULATION TO ASSURE ENTRAPPED VAPOR COLLAPSE
- SUPPLY TANK VAPOR PRESSURE  $\leq 2.2$  kN/M<sup>2</sup> (15 PSIA), NO HELIUM PASSAGE ALLOWABLE
- PREVENTION OF EXCESSIVE TRANSFER LINE LOADS AT  $\dot{m} = 1-1.5$  KG/SEC (2-3 LB/SEC)

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