

A Model for the Influence of Pressure on the Bulk Modulus and the Influence of Temperature on the Solidification Pressure for Liquid Lubricants

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A MODEL FOR THE INFLUENCE OF PRESSURE ON THE BULK MODULUS
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SOLIDIFICATION PRESSURE FOR LIQUID LUBRICANTS

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ABSTRACT

Two pressure chambers, for compression experiments with liquids from zero to 2.2 GPa pressure, are described. The experimentally measured compressions are then compared to theoretical values given by an isothermal model of equation of state recently introduced for solids. The model describes the pressure and bulk modulus as a function of compression for different types of lubricants with a very high accuracy up to the pressure limit of the high pressure chamber used (2.2 GPa).

In addition the influence of temperature on static solidification pressure was found to be a simple function of the thermal expansion of the fluid.

NOMENCLATURE

B	bulk modulus, N/m^2
B_0	bulk modulus at zero pressure, N/m^2
m	mass, kg
p	pressure, N/m^2
t	temperature, °C
v	volume, m^3
v_{sol}	volume at the solidification pressure, m^3

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$v_{sol,0}$	the volume the lubricant should become if it were decompressed from the solid state down to zero pressure keeping the solid state properties, m^3
x	parameter in bulk modulus and pressure equation
x_{sol}	$(v/v_{sol,0})^{1/3}$
α	coefficient of thermal expansion, $^{\circ}C^{-1}$
γ	$\partial\tau_L/\partial p$, shear strength increase with pressure
δ	coefficient of thermal volume expansion, $^{\circ}C^{-1}$
ρ	density of lubricant, kg/m^3
n	parameter in bulk modulus and pressure equation
τ_L	shear strength of lubricant, N/m^2

INTRODUCTION

In the calculation of the oil film thickness in elastohydrodynamic lubrication, the compressibility and the change of lubricant behavior from liquid to solid type, are very important. The compressibility of the lubricant determines the shape and the thickness of the oil film in the central almost parallel part of it. Lubricants with high compressibility give a thinner central oil film than stiff lubricants. If the compressibility is high enough, the minimum film thickness will not appear at the outlet of the elastohydrodynamic contact, but in the center of the contact. There the area of low film thickness will be much larger than the outlet area with low film thickness. Due to the large close contact area and the high pressure in this area, the heating and energy dissipation, if the oil film fails, is much more severe than it should be if the minimum film thickness were the same, but only occupying the side lobes and outlet part of the contact.

The change of solidification pressure with temperature is also important for the lubricant film thickness but is even more important for the power dissipation in the elastohydrodynamic contact. If the temperature rise is

high enough that the oil behaves like a liquid, even in the central part of the contact, the friction forces will decrease and become lower than the limiting shear stress of the lubricant. In this paper two test apparatuses are described, one for measurement of the bulk modulus at low pressures and the other for measurement of the compression curves for high pressures up to 2.2 GPa for liquid lubricants. A physical model, built upon consideration of the atomic interaction forces in the lubricants, describes the pressure-compression relationship, for all lubricants tested, using only two parameters. These parameters are the bulk modulus at zero pressure B_0 and the pressure derivative of the bulk modulus at zero pressure $(\partial B_0 / \partial p)_{p=0}$.

The high pressure chamber was also used to measure the change in solidification pressure with a change in temperature.

The High Pressure Chamber

A detailed description of the high pressure chamber can be found in Ref. 1. Equipped as in Ref. 1, the high pressure chamber can be used to determine the solidification pressure for lubricants by measuring the shear strength of the fluid as a function of pressure. A description of the specially equipped high pressure chamber for high accuracy measurements of the compression of lubricants can be found in Ref. 2.

A drawing of the apparatus is shown in Fig. 1. As is described in Ref. 2 the pressurized volume between the plungers can be measured very accurately. The maximum error being about 2×10^{-4} of the total volume. It is not only possible to measure the compression of the fluid in the high pressure chamber but also to measure the shear strength of the fluid as a function of the pressure. In these experiments the solidification pressure is said to be the pressure at which the shear strength of the fluid starts to increase linearly with pressure as $\partial \tau_L / \partial p = \gamma$.

The high pressure chamber was used for measurement of the compression of the fluids from 0.4225 to 2.20 GPa. At pressures below 0.4225 GPa some of the lubricants with low viscosity at these pressures did leak past the steel seals as the steel seals were not plastically deformed to seal perfectly between the plungers and the inner cylindrical surface of the high pressure chamber.

Apparatus and Method to Determine B_0

Since leakage was observed at the lower pressures, it was not possible to obtain a reliable value of the bulk modulus at zero pressure (B_0). Therefore a new apparatus was built to measure B_0 . It consisted of a closed volume with very thick steel walls and a pressure transducer connected to it.

The volume was then completely filled with the test lubricant and sealed.

A temperature regulation system and a heating coil around the steel cylinder made it possible to keep the temperature and the pressure due to the thermal expansion of the oil at predetermined values. The density of the oil in the steel cylinder was

$$\rho = \frac{m}{v} \quad (1)$$

where m was the mass and v was the volume of the lubricant.

The density change due to a temperature change was

$$\frac{\partial \rho}{\partial t} = - \frac{m}{v^2} \frac{\partial v}{\partial t} = - \frac{\rho^2}{m} \frac{\partial v}{\partial t} \quad (2)$$

$$\frac{\partial v}{\partial t} = - \frac{m}{\rho^2} \frac{\partial \rho}{\partial t} \quad (3)$$

$$\frac{1}{v} \frac{\partial v}{\partial t} = - \frac{1}{\rho} \frac{\partial \rho}{\partial t} \quad (4)$$

The relative increase of the steel cavity volume caused by the temperature increase was $3\alpha\Delta t$ where $\alpha = 11 \times 10^{-6} \text{ } ^\circ\text{C}^{-1}$ was the coefficient of thermal expansion for the steel.

A temperature increase of Δt , created a compression of the lubricant determined by the thermal expansion of the oil minus the thermal expansion of the container minus the elastic increase of the container volume.

The thermal expansion of the lubricant due to the temperature increase was $\partial v / \partial t \cdot \Delta t$ and the thermal expansion of a unit volume of the lubricant was $(\partial v / \partial t) / v \cdot \Delta t$. The thermal expansion of the unit volume of the steel container was $3\alpha v \Delta t / v = 3\alpha \Delta t$. The elastic volume increase of the steel container due to a pressure increase Δp was $\Delta v / \Delta p \cdot \Delta p$ and the relative elastic volume increase of the container was $(1/v) \cdot (\Delta v / \Delta p) \Delta p$. The compression of the lubricant was $(-\partial v / \partial p) \cdot \Delta p$ and the relative compression of the lubricant caused by the pressure increase Δp was $(1/v)(-\partial v / \partial p) \cdot \Delta p$.

$$\left(\frac{1}{v} \frac{\partial v}{\partial p} - 3\alpha \right) \Delta t - \frac{1}{v} \frac{\Delta v}{\Delta p} \cdot \Delta p = - \frac{1}{v} \frac{\partial v}{\partial p} \cdot \Delta p \quad (5)$$

$$\frac{1}{v} \frac{\partial v}{\partial p} = \frac{1}{v} \cdot \frac{\Delta v}{\Delta p} + \left(3\alpha - \frac{1}{v} \frac{\partial v}{\partial t} \right) \frac{\Delta t}{\Delta p} \quad (6)$$

or if Eq. (4) is used

$$\frac{1}{B_0} = \frac{1}{v} \frac{\partial v}{\partial p} = \frac{1}{v} \frac{\Delta v}{\Delta p} + \left(3\alpha + \frac{1}{\rho} \frac{\partial \rho}{\partial t} \right) \frac{\Delta t}{\Delta p} \quad (7)$$

For the apparatus $(1/v)(\Delta v / \Delta t) = 0.015 \text{ GPa}^{-1}$ and $3\alpha = 33 \times 10^{-6} \text{ } ^\circ\text{C}^{-1}$.

For the different fluids the values measured at 20 °C are given in Table I. The values of ρ and $\partial \rho / \partial t$ were measured using a precision scale and calibrated volumes.

Isothermal Volume Change of Lubricants With Pressure

Vinet, Ferrante, Smith, and Rose (3) calculated the pressure as function of compression for ionic, metallic, covalent, and rare gas solids. Their equation of state gave the pressure

$$p = \frac{3B_0}{x^2} (1 - x) \exp(\eta(1 - x)) \quad (8)$$

and the bulk modulus

$$B = \frac{B_0}{x^2} \left[2 + (\eta - 1)x - \eta x^2 \right] \exp(\eta(1 - x)) \quad (9)$$

as a function of the relative compression $x = (v/v_0)^{1/3}$

Here B_0 was the bulk modulus at zero pressure and

$$\eta = \frac{3}{2} \left(\left(\frac{\partial B_0}{\partial p} \right)_{p=0} - 1 \right) \quad (10)$$

was a function of the pressure derivative of the bulk modulus at zero pressure. These equations are valid for solids at isothermal conditions without phase change.

As the interatomic forces are similar in solids and liquids in compression, the equation of state for solids was applied as an approximation for the equation of state for liquid lubricants. If the lubricants behave in the same way as solids, the experimental points will fit the pressure deformation curve given by Eq. (8).

Lubricant molecules are normally large and complex and have different types of bondings. This is why eventually B_0 and η could vary during the compression. The lubricants tested were known to convert from liquid to solid behavior within the pressure range tested. As the pressure range for the test apparatuses described earlier did not overlap, the connection between low pressure and high pressure behavior was done using curve fit techniques. The pressure and bulk modulus equations were assumed to be applicable to lubricants and the constants in the pressure equation was determined by curve fitting of the measured data.

Compression Through the Solidification Boundary

For the liquid state the Eqs. (8) and (9) were used up to the solidification pressure. In the solid state the same types of equations were used, but the values of η , B_0 , and x were changed.

$$p = \frac{3B_{os}}{x_{ss}^2} (1 - x_{ss}) \exp(\eta_s(1 - x_{ss})) \quad (11)$$

Here, B_{os} was the bulk modulus for the solid state at zero pressure. It could not be directly measured, but it was calculated using the equation

$$B = \frac{B_{os}}{x_{ss}^2} \left[2 + (\eta_s - 1) x_{ss} - \eta_s x_{ss}^2 \right] \exp(\eta_s(1 - x_{ss})) \quad (12)$$

and the assumption that the bulk modulus was a continuous function of pressure, which means that B for the solid state and B for the liquid state at the solidification pressure was the same. At the solidification pressure $B = B_s$, $p = p_s$, and $x_{ss} = x_{sol}$

$$p_s = \frac{3B_{os}}{x_{sol}^2} (1 - x_{sol}) \exp(\eta_s(1 - x_{sol})) \quad (13)$$

The pressure in the solidified state can be written as

$$p = \frac{3(1 - x_{ss})}{x_{ss}^2} \exp(\eta_s(1 - x_{ss})) \cdot \frac{p_s x_{sol}^2}{3(1 - x_{sol}) \exp(\eta_s(1 - x_{sol}))} \quad (14)$$

$$\frac{p}{p_s} = \frac{(1 - x_{os} \cdot x_{sol})}{x_{os}^2 (1 - x_{sol})} \exp(\eta_s x_{sol}(1 - x_{os})) \quad (15)$$

where $x_{os} = (v/v_{sol})^{1/3}$ was the relative volume calculated from the solidification volume raised to the power 1/3.

x_{sol} was the relative volume at the solidification pressure raised to the power 1/3 assuming solid type behavior all the way down to zero pressure.

$$x_{ss} = x_{os} \cdot x_{sol} \quad (16)$$

Curvefitting the experimental points gave x_{sol} and η_s .

Analytical Solution for x_{sol}

It is possible to solve for x_{sol} if B_o , η_L , η_s , B_s , and p_s are known. The equations for the pressure as a function of relative volume

change are Eq. (8) for pressures up to the solidification pressure p_s and Eq. (15) for pressures above p_s .

x_{sol} can be solved for by using the fact that the bulk modulus is the same at the solidification pressure for both the liquid and solid state.

x_{sol} is then a function of the solidification pressure p_s , the bulk modulus B_s , and the parameter η_s for the solid state.

$$B_s = \frac{B_0}{x^2} \left[2 + (\eta_L - 1)x - \eta_L x^2 \right] \exp(\eta_L(1 - x))$$

$$= \frac{B_{os}}{x_{sol}^2} \left[2 + (\eta_s - 1) x_{sol} - \eta_s x_{sol}^2 \right] \exp(\eta_s(1 - x_{sol})) \quad (17)$$

But from Eq. (13)

$$\frac{B_{os} \exp(\eta_s(1 - x_{sol}))}{x_{sol}^2} = \frac{p_s}{3(1 - x_{sol})} \quad (18)$$

$$B_s = \frac{B_0}{x^2} \left[2 + (\eta_L - 1)x - \eta_L x^2 \right] \exp(\eta_L(1 - x))$$

$$= \frac{p_s}{3(1 - x_{sol})} \left[2 + (\eta_s - 1) x_{sol} - \eta_s x_{sol}^2 \right] = \frac{p_s}{3} \left[\frac{1}{1 - x_{sol}} + 1 + \eta_s x_{sol} \right] \quad (19)$$

$$x_{sol} = \frac{1}{2} \left(\frac{3B_s}{\eta_s p_s} + 1 - \frac{1}{\eta_s} \right) - \sqrt{\frac{1}{4} \left(\frac{3B_s}{\eta_s p_s} + 1 - \frac{1}{\eta_s} \right)^2 - \left(\frac{3B_s}{p_s} - 2 \right)} \quad (20)$$

If $\eta_s = 0$, as the experimental measurements suggest.

$$B_s = \frac{p_s}{3} \left[\frac{1}{1 - x_{sol}} + 1 \right] \quad (21)$$

or

$$x_{sol} = 1 - \frac{1}{\frac{3B_s}{p_s} - 1} \quad (22)$$

and

$$\frac{3B_{0s}}{p_s} = \frac{x_{s01}^2}{1 - x_{s01}} \quad (23)$$

x_{s01} can be used to determine the temperature influence on the solidification pressure, as will be shown at the end of this paper.

Numerical Calculations of B_0 and n_L

In the equations for p and B the values of x and n are not known. The compression of the fluid is only known relative to the volume at the initial pressure 0.4225 GPa. The equation for p will contain this unknown compression.

If the volume at zero pressure is v_0 and the volume at the starting pressure is v_s the equation for the liquid state pressure is the same as Eq. (8) where x is now given as

$$x = \left(\frac{v}{v_0}\right)^{1/3} = \left(\frac{v}{v_s} \cdot \frac{v_s}{v_0}\right)^{1/3} = \left(\frac{v}{v_s}\right)^{1/3} \left(\frac{v_s}{v_0}\right)^{1/3} = \left(\frac{v}{v_s}\right)^{1/3} x_s \quad (24)$$

v/v_s is the relative volume calculated from the starting pressure

$$x = \left(\frac{v}{v_s}\right)^{1/3} x_s = x_0 x_s \quad (25)$$

Using this expression for the relative volume, the pressure, and bulk modulus equations will be

$$p = \frac{3B_0}{x_0^2 x_s^2} (1 - x_0 x_s) \exp(n_L(1 - x_0 x_s)) \quad (26)$$

$$B = B_0 \left[\frac{2}{x_0^2 x_s^2} + \frac{n_L - 1}{x_0 x_s} - n_L \right] \exp(n_L(1 - x_0 x_s)) \quad (27)$$

Here only the two values of x_s and η_L are unknown. They can be solved for by least squares techniques using the measured values of p and x_0 .

Results From Curvefitting of the Experimental Measurements

As the values of B_0 and η are different in the liquid and solid states for the lubricants, it is possible to find the solidification pressure for a lubricant using curvefitting techniques. The solidification pressures found in this way, just by observing the change in curvature for the pressure-volume curve, are compared to the solidification pressures found by measuring the shear strength of the lubricants in Table II. The two completely different methods to determine the solidification pressures give a good agreement. The mean absolute difference being about 5 percent and the maximum difference being 8.9 percent. The solidification pressure in the curve fitting experiments has been assumed to coincide with one of the measured pressures. The pressure step from one experimental point to the next at the solidification pressure could be as much as 15 percent though, explaining most of the scatter. In Table II are also given the measured or calculated parameter values for the different lubricants. $v_{start}/v_0 = x_s^3$ is the relative volume of the lubricant at the start pressure, 0.4225 GPa, of the experiment. η_L is the slope parameter describing the slope of the curves in Fig. 3. The parameter η_s for the solid state of all tested lubricants was found to be zero. v_{sol}/v_{start} is the volume at the solidification pressure divided by the volume at the pressure 0.4225 GPa. If the stiffness of the oil was the same as at the solidification pressure and the parameter $\eta_s = 0$ from zero pressure to the solidification pressure, the fictitious relative volume at the solidification pressure should be $v_{sol}/v_{sol,0}$. This relative volume, also given in Table II, will be used in the calculations of the change of solidification pressure with temperature.

In Fig. 2 the compression as a function of the pressure is shown for six different fluids. The solid lines are the theoretical curves from Ref. 3 fitted to the experimental points shown in the figures. The fits between the theoretical curves and the experimental points are remarkably good. In Fig. 3 the natural logarithm of the nondimensional bulk modulus is shown as a function of the compression parameter $x = (v/v_0)^{1/3}$. The theoretical solid lines and the experimental points are shown for the six fluids. The parameter η in Eq. (8) is shown in this type of plot as the slope of the curves. It is clearly visible from all six diagrams in Fig. 3 that the parameter η_s for the solid state is zero.

The Change of Solidification Pressure Caused by a Temperature Change

As earlier mentioned Vinet, Ferrante, Smith, and Rose (3) published equations for the pressure as a function of compression and the bulk modulus as a function of pressure. These equations were valid for isothermal conditions without phase changes. Experiments with lubricating oils showed that the bulk modulus at low pressures is almost independent of the temperature. The total pressure and compression of an oil needed to convert it from a liquid to a solid state increases with increasing temperature. The idea behind this part of the paper is that the absolute density (or volume) determines the switch from liquid to solid state for lubricants. This means that the thermal expansion due to a temperature increase has to be compensated by a pressure increase which increases the density to the value needed for solidification.

If the volume coefficient of thermal expansion for the fluid is $\delta \text{ } ^\circ\text{C}^{-1}$, the change in solidification pressure with temperature is given by the thermal expansion

$$v\delta \cdot \Delta t = 3 \Delta x v \quad (28)$$

where

$$\frac{v + \Delta v}{v} = x^3 = (1 + \Delta x)^3 = 1 + 3 \Delta x + 3 \Delta x^2 + \Delta x^3 \quad (29)$$

$$\frac{\Delta v}{v} \approx 3 \Delta x \quad \text{since} \quad \Delta x \ll 1 \quad (30)$$

where x is the parameter in the pressure equation. The pressure as a function of B_0 , x , and η is given by Eq. (8).

The experimental measurements in Fig. 3 show that the parameter value η in the solid state is $\eta_s = 0$. This indicates a simple method to calculate the change in solidification pressure caused by a change in temperature.

At the solidification pressure for a lubricant with the temperature t_1 Eq. (8) can be rewritten as

$$\ln \left[\frac{p_{s1} \cdot x_{sol}^2}{3(1-x_{sol})B_{os}} \right] = (1 - x_{sol})\eta_s = 0 \quad (31)$$

where $x_{sol}^3 = v_{sol}/v_{sol,0}$ is given in Table II.

If the lubricant then is further compressed to the pressure p_{s2} and heated to the temperature t_2 , giving the thermal expansion $3 \Delta x = \delta(t_2 - t_1)$ from Eq. (28), then Eq. (8) will give

$$\ln \left[\frac{p_{s2} \cdot (x_{sol} - \Delta x)^2}{3(1 - x_{sol} + \Delta x)B_{os}} \right] = (1 - x_{sol} + \Delta x)\eta_s = 0 \quad (32)$$

The solidification pressure at temperature t_2 divided by the solidification pressure at temperature t_1 can then be solved for from Eqs. (31) and (32).

$$\frac{p_{s2}}{p_{s1}} = \left(\frac{x_{sol}}{x_{sol} - \Delta x} \right)^2 \cdot \frac{1 - x_{sol} + \Delta x}{1 - x_{sol}} \quad (33)$$

Example

For a typical lubricating oil η_L is of the order 10 to 30 and $\eta_s \approx 0$. The compression needed to solidify it is $\Delta v/v_0 = 0.2 \pm 0.05$ and if the oil had had the same stiffness as in the solidified state the compression needed

to reach the solidification pressure would have been $(\Delta v/v_0)_{sol} = 0.040 - 0.084$. The thermal expansion caused by a temperature increase of 20 °C (from 20 to 40 °C) is from Table I.

$$\Delta x = 7.25 \times 10^{-4} \times 20/3 = 0.00483$$

and from Table II $x_{sol}^3 = 0.9359$, $x_{sol} = 0.978$ for the lubricant ditridecyladipate 26 cSt.

This gives

$$\frac{p_{s1} x_{sol}^2}{1 - x_{sol}} = \frac{p_{s2}(x_{sol} - \Delta x)^2}{1 - x_{sol} + \Delta x} \quad (34)$$

$$\frac{p_{s2}}{p_{s1}} = \left(\frac{x_{sol}}{x_{sol} - \Delta x} \right)^2 \cdot \frac{1 - x_{sol} + \Delta x}{1 - x_{sol}} = \left(\frac{0.978}{0.978 - 0.00483} \right)^2 \cdot \frac{0.02683}{0.022} \quad (35)$$

$$\frac{p_{s2}}{p_{s1}} = 1.232 \quad (36)$$

The compression experiments gave for the two temperatures 40 and 20 °C, $p_{s2}/p_{s1} = 1.95/1.58 = 1.234$.

For a 450 cst polyalphaolefine lubricant $x_{s1} = 0.971$, $\Delta x = 0.003937$ for $\Delta t = 20$ °C gave $p_{s2}/p_{s1} = 1.147$ and the compression experiments gave $p_{s2}/p_{s1} = 2.06/1.80 = 1.144$.

For a naphthenic base distillate with a very low solidification pressure ($p_s = 0.67$ GPa at 20 °C) the constants from the numerical curve fitting was $x_{sol} = 0.9865$ $\Delta x = 0.00896$ for a temperature change of 40 °C.

$$\frac{p_{s2}}{p_{s1}} = \left(\frac{0.9865}{0.97754} \right)^2 \cdot \frac{0.02246}{0.01350} = 1.694 \quad (37)$$

and the experiments gave $p_{s2}/p_{s1} = 1.13/0.67 = 1.687$.

These values show a remarkably good agreement between theory and experiments.

CONCLUSIONS

Two pressure chambers, for measurement of compressibility and bulk modulus for liquids from zero to 2.2 GPa pressure, are described. The experimentally measured compressions are then compared to values given by an isothermal equation of state for solids in compression. The equation describes the pressure and bulk modulus for different types of lubricants with a very high accuracy up to the pressure limit of the high pressure chamber used (2.2 GPa).

The influence of temperature on static solidification pressure was found to be a simple function of the thermal expansion of the fluid.

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TABLE I. - EXPERIMENTAL RESULTS

Lubricant, nr	ρ	$\frac{\partial \rho}{\partial t}$	$\frac{\Delta t}{\Delta p}$	$\frac{1}{v} \frac{\partial v}{\partial p}$	B_0
	kg/m ³	kg/m ³ °C	°C/GPa	GPa ⁻¹	GPa
1	846	-0.591	1043	-0.679	1.473
2	910	-.660	910	-.615	1.626
3	1005	-.726	995	-.672	1.488
4	1004	-.716	910	-.604	1.656
5	931	-.626	940	-.586	1.706
6	892	-.629	910	-.597	1.675

TABLE II. - MEASURED AND CALCULATED VALUES

Oil, nr	Solidification pressure from curve fit, GPa	Solidification pressure from shear strength measurement, GPa	Bulk modulus at zero pres- sure B_0 , GPa	$\frac{v_{start}}{v_0}$ x_s^3	$\frac{3}{2} \left(\left(\frac{\partial B}{\partial p_0} \right)^L - 1 \right)$	$\frac{v_{sol}}{v_{start}}$	$\frac{v_{sol}}{v_{sol,0}}$ x_{sol}^3	Lubricant type
1	1.650	1.682	1.473	0.8654	13.65	0.8718	0.9161	Polyalphaole- fine 450 est
2	1.449	1.561	1.626	.8697	13.47	.8899	.9359	Ditridecylade- pate 26 cst
3	0.995	1.092	1.488	.8736	14.84	.9252	.9581	Polypropylene- glycole 175 cst
4	1.124	1.213	1.656	.8734	13.71	.9247	.9525	Polypropylene- glycole 80 cst
5	.676	0.706	1.706	.9014	25.27	.9759	.9600	Naphthenic base distillate 26 cst
6	.834	.839	1.675	.8945	20.93	.9564	.9501	Naphthenic base raffinate 23 cst

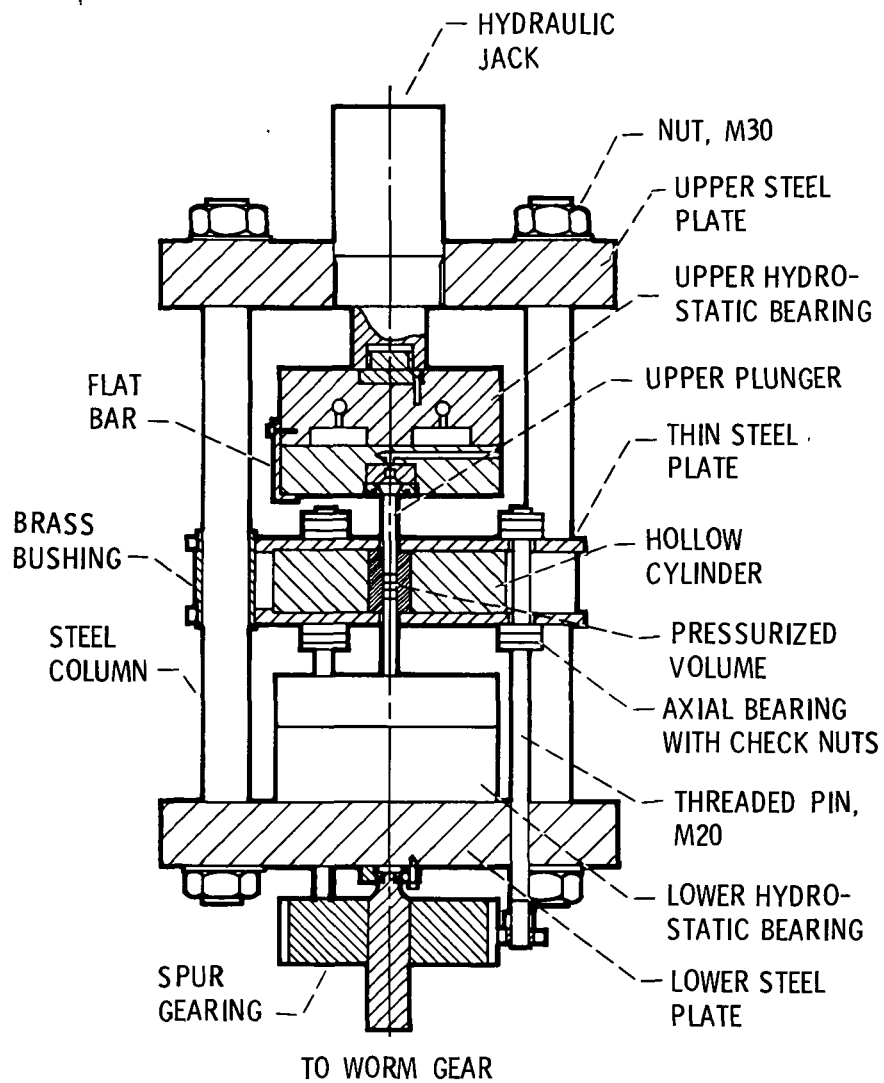


Figure 1. - Main parts of experimental apparatus.

$(1 - x^3)$ vs P

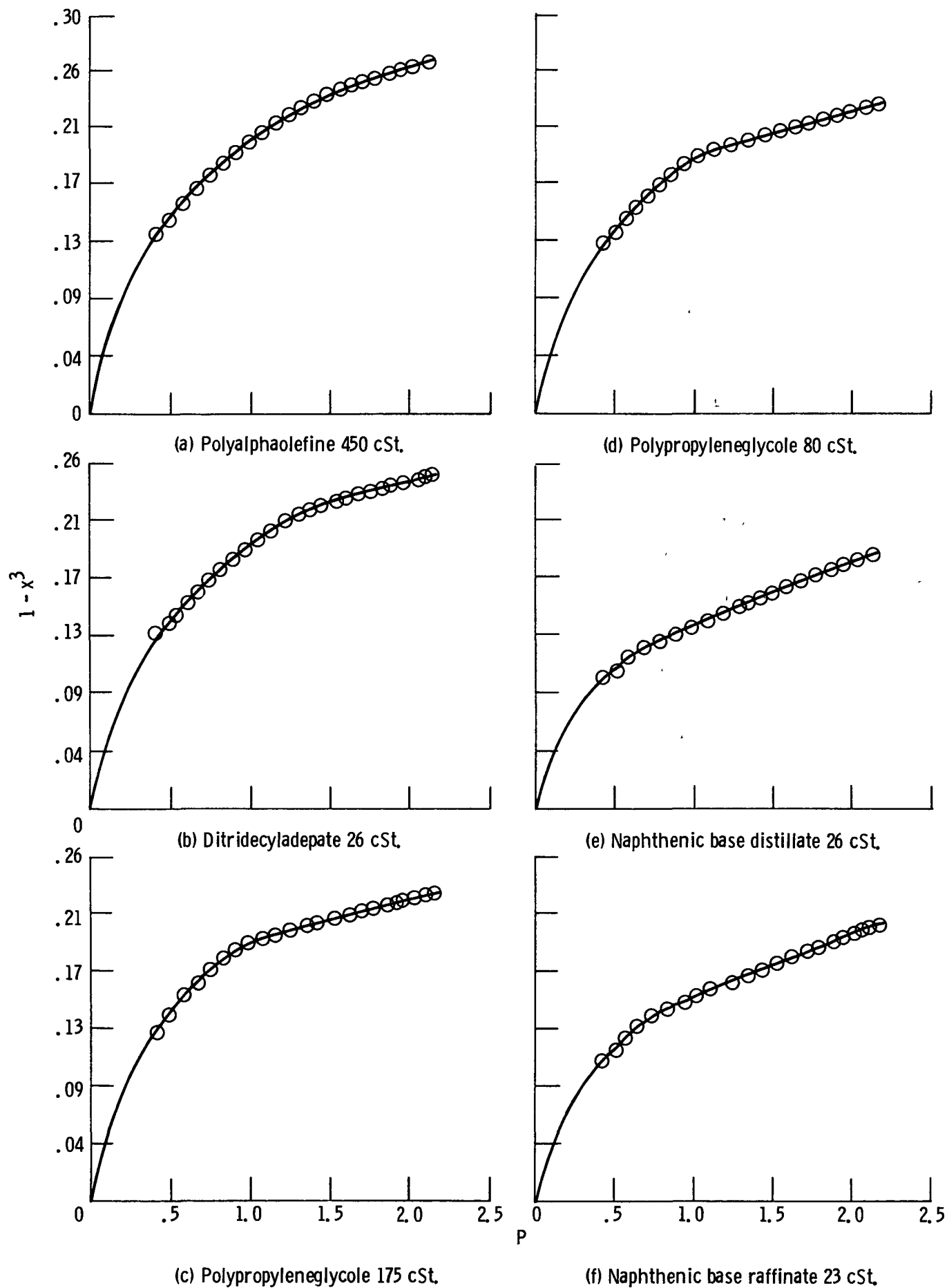
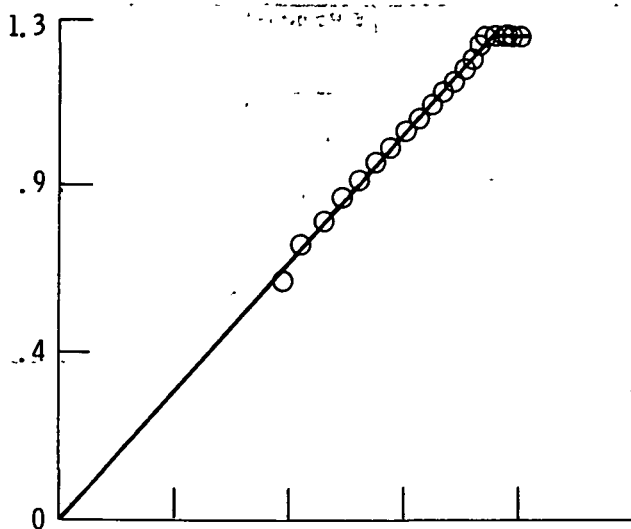
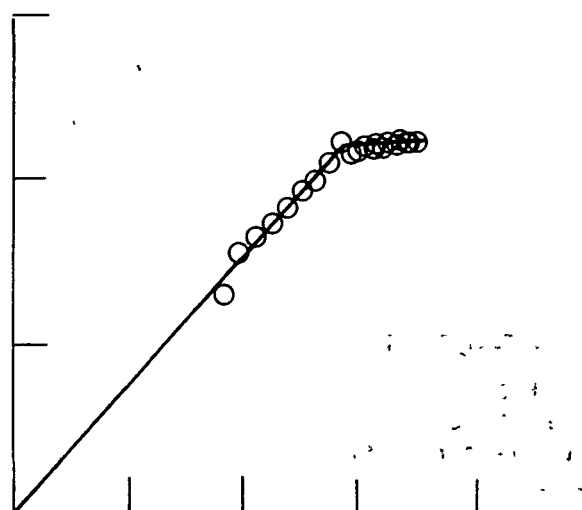


Figure 2 - Theoretical compression curves and experimental points for the six lubricants tested.

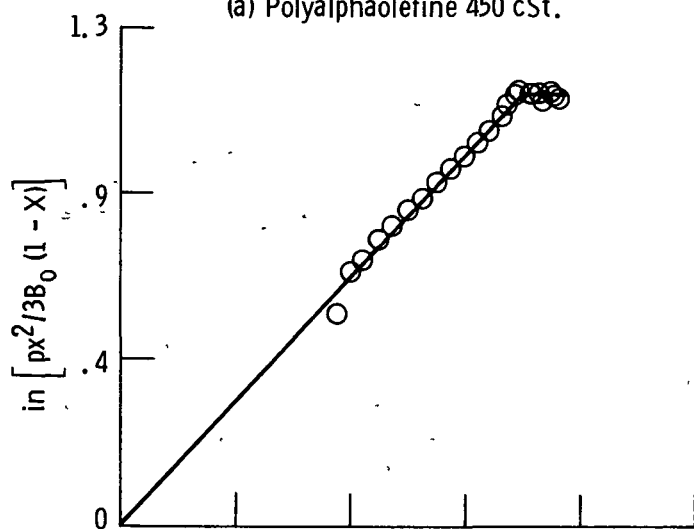
$$\ln \left[\frac{px^3}{3B_0(1-x)} \right] \text{ VS } (1-x)$$



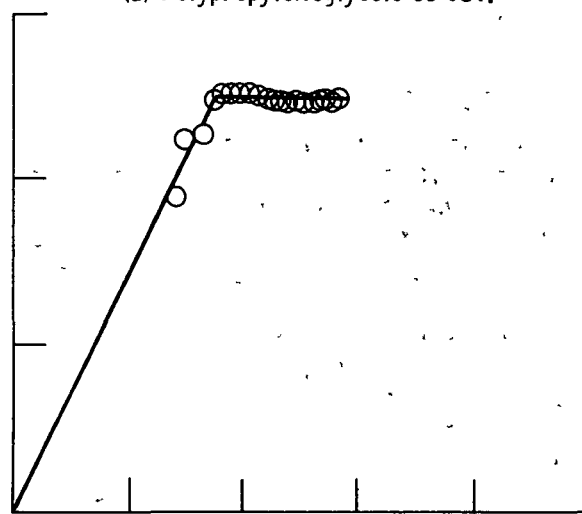
(a) Polyalphaolefine 450 cSt.



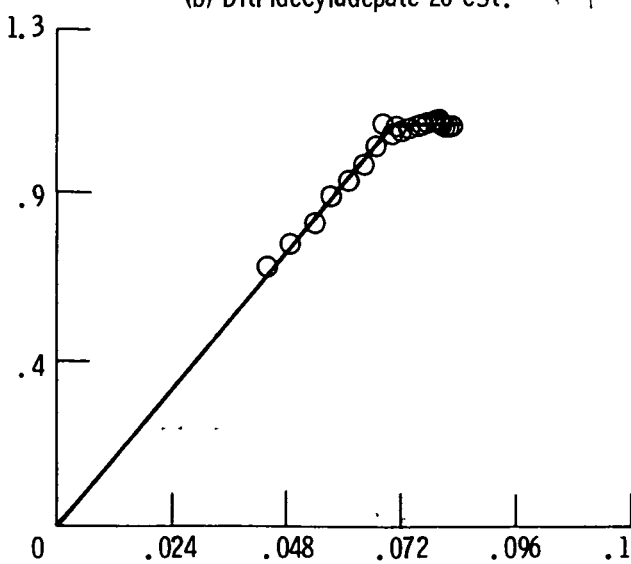
(d) Polypropyleneglycole 80 cSt.



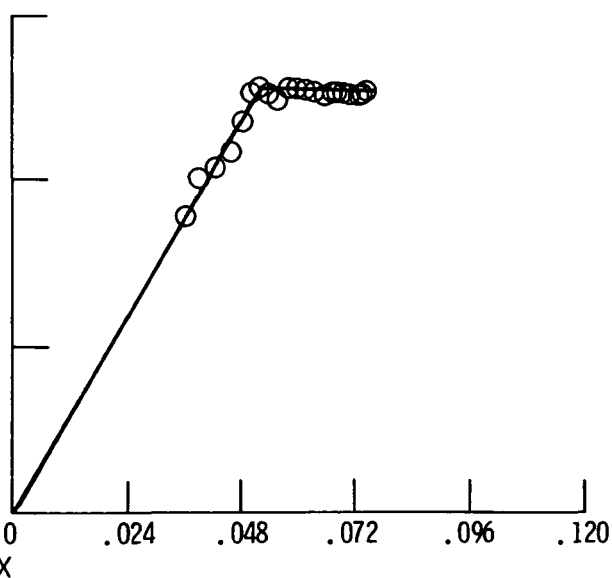
(b) Ditridecyladepate 26 cSt.



(e) Naphthenic base distillate 26 cSt.



(c) Polypropyleneglycole 175 cSt.



(f) Naphthenic base raffinate 23 cSt.

Figure 3. - Theoretical curves and experimental points showing $\ln \left(\frac{px^2}{3B_0(1-x)} \right)$ as a function of $1-x$ for the six lubricants.

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16 Abstract Two pressure chambers, for compression experiments with liquids from zero to 2.2 GPa pressure, are described. The experimentally measured compressions are then compared to theoretical values given by an isothermal model of equation of state recently introduced for solids. The model describes the pressure and bulk modulus as a function of compression for different types of lubricants with a very high accuracy up to the pressure limit of the high pressure chamber used (2.2 GPa). In addition the influence of temperature on static solidification pressure was found to be a simple function of the thermal expansion of the fluid.					
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