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# Application of a Computational Model for Vortex Generators in Subsonic Internal Flows

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APPLICATION OF A COMPUTATIONAL MODEL FOR VORTEX GENERATORS IN  
SUBSONIC INTERNAL FLOWS

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SUMMARY

A model for the analysis of vortex generators in a fully viscous subsonic internal flow is evaluated. A vorticity source term is used in a modified form of the "Parabolized" Navier-Stokes equations to model the shed vortex. Computed results are compared with idealized flow vortex paths, and with experimental data for vortex generators embedded in a thick turbulent boundary layer. The analysis is also compared with experimental data for a separated diffusing S-duct and for a diffusing S-duct with vortex generators. Quantitative comparisons are shown for the latter three cases. Emphasis is placed on verifying the ability of the model to predict global distortions in the flow field.

INTRODUCTION

Three-dimensional subsonic diffusers are very common in modern aircraft propulsion systems. Strong secondary flows are generated by the presence of offset bends and changes in cross-sectional shape of the duct. In addition to this phenomena, since the flow is diffusing, the boundary layers may grow to a thickness comparable to the duct radius. These effects weigh heavily on the overall performance of the diffuser.

In efforts to save weight and thereby fuel, it is common to design these ducts to be as short as possible. In these cases the designer must be concerned with the flow separating due to a strong adverse pressure gradient. This separation may have devastating effects on engine performance, such as the engine unstating. To alleviate this problem, vortex generators can be used as a flow control device. The vortex generator will cause a mixing of the high momentum core flow with the low momentum flow in the boundary layer, resulting in a net increase of energy near the surface. This can delay or eliminate the separation depending on the flow conditions. There is a penalty that is paid for the use of the vortex generators and that is the drag of the generator. But, since the vortex generators tend to have small planform areas, this adverse effect is small. An excellent background on forced mixing can be obtained from references 1 to 3.

To solve for the flow fields in these ducts, a complete three-dimensional Navier-Stokes analysis could be used, but large amounts of computer time and storage are required for a detailed solution. However, by making certain approximations to the Navier-Stokes equations, such as neglecting streamwise diffusion, a set of equations can be obtained for fully viscous internal flow that can be solved by forward marching in space. A computer analysis, designated PEP SIG, has been developed using these equations to compute three-dimensional subsonic viscous flow through curved ducts with superelliptic

are both unity.) The known three-dimensional pressure field is represented by  $p_1 = p_1(x_1, x_2, x_3)$  and the unknown one-dimensional viscous blockage correction is  $p_v = p_v(x_3)$ . In this approach,  $p_1$  was computed using a three-dimensional potential flow analysis. This brings the elliptic effects of the geometry into the solution.

The secondary velocities  $v_s$  and  $w_s$  are split into irrotational and rotational components. A scalar potential,  $\varphi$ , corresponding to the irrotational component of the secondary velocity, is defined as

$$v_\varphi = \frac{\partial \varphi}{\partial x_1}$$

$$w_\varphi = \frac{\partial \varphi}{\partial x_2}$$

The continuity equation can then be written as

$$\frac{\partial}{\partial x_1} \left[ \rho h \frac{\partial \varphi}{\partial x_1} \right] + \frac{\partial}{\partial x_2} \left[ \rho h \frac{\partial \varphi}{\partial x_2} \right] + \frac{\partial}{\partial x_3} [\rho u_p] = 0$$

The transverse momentum equations are redefined in terms of a streamwise vorticity-stream function formulation given by

$$\begin{aligned} \frac{\rho u_p}{h} \frac{\partial \Omega}{\partial x_3} + \frac{\partial}{\partial x_1} [\rho v_s \Omega] + \frac{\partial}{\partial x_2} [\rho w_s \Omega] + \frac{\partial w_s}{\partial x_2} \frac{\partial}{\partial x_1} \left( \frac{\rho u_p}{h} \right) - \frac{\partial v_s}{\partial x_3} \frac{\partial}{\partial x_2} \left[ \frac{\rho u_p}{h} \right] \\ - \frac{\partial}{\partial x_1} \left[ \frac{\rho u_p^2}{h} \frac{\partial h}{\partial x_2} \right] + \frac{\partial}{\partial x_2} \left[ \frac{\rho u_p^2}{h} \frac{\partial h}{\partial x_1} \right] + \frac{\partial(\rho v_s)}{\partial x_1} \frac{\partial v_s}{\partial x_2} - \frac{\partial(\rho v_s)}{\partial x_2} \frac{\partial v_s}{\partial x_1} + \frac{\partial(\rho w_s)}{\partial x_1} \frac{\partial w_s}{\partial x_2} \\ - \frac{\partial(\rho w_s)}{\partial x_2} \frac{\partial w_s}{\partial x_1} - \frac{\partial}{\partial x_1} \left[ \frac{1}{h} \frac{\partial}{\partial x_1} [h \mu \Omega] \right] - \frac{\partial}{\partial x_2} \left[ \frac{1}{h} \frac{\partial}{\partial x_2} [h \mu \Omega] \right] = 0 \\ \frac{\partial}{\partial x_1} \left[ \frac{1}{\rho h} \frac{\partial}{\partial x_1} [h \Psi] \right] + \frac{\partial}{\partial x_2} \left[ \frac{1}{\rho h} \frac{\partial}{\partial x_2} [h \Psi] \right] + \Omega = 0 \end{aligned}$$

where

$$v_s = v_\varphi + v_\Psi = v_\varphi + \frac{1}{\rho h} \frac{\partial (h \Psi)}{\partial x_2}$$

$$w_s = w_\varphi + w_\Psi = w_\varphi - \frac{1}{\rho h} \frac{\partial (h \Psi)}{\partial x_1}$$

Here  $\Psi$  is the stream function, or vector potential, corresponding to the rotational component of the secondary velocity, and  $\Omega$  is the vorticity in

The effect of the drag of the vortex generator is also included in the model. The drag on the wing section is a combination of profile drag, which is due to viscous and pressure effects, and induced drag, which is due to the shed vortex. In this model the profile drag of the vortex generator is neglected in comparison to the induced drag because in the cases studied here the generators were small. The induced drag is then proportional to the vortex strength and the crossflow velocity at a point. This term is included in the governing equations as a negative source term in the primary momentum equation.

## IDEAL FLOW RESULTS

The first test case used to verify the vortex generator model was a comparison of the motion of the center of a vortex due to the induced velocity of another vortex. The results of the present analysis were compared with the results of an ideal flow calculation with a wall simulated using image vortices as shown in figure 3. In this method the velocity of a vortex, say vortex A in figure 3, can be calculated at any time by

$$\vec{v}_A = \frac{\Gamma_B \vec{k}}{2\pi} \times \frac{(\vec{r}_A - \vec{r}_B)}{|\vec{r}_A - \vec{r}_B|^2} + \frac{\Gamma_C \vec{k}}{2\pi} \times \frac{(\vec{r}_A - \vec{r}_C)}{|\vec{r}_A - \vec{r}_C|^2} + \frac{\Gamma_D \vec{k}}{2\pi} \frac{(\vec{r}_A - \vec{r}_D)}{|\vec{r}_A - \vec{r}_D|^2}$$

After the velocities at points A and B are calculated new positions can be determined by time integration. In the viscous code this ideal flow problem is approximated by laminar incompressible flow in a circular pipe. The Reynolds number based on pipe diameter was 2000. The boundary layers were thin, only 5 percent of the duct radius, with the vortex generator tip located well outside of the boundary layer. The total drag of the vortex generator was neglected. Four different cases are considered: (1) counter rotating vortices of the same strength that rotate toward each other with  $L/H = 2.5$ , (2) counter rotating vortices of the same strength that rotate away from each other with  $L/H = 2.5$ , (3) co-rotating vortices of the same strength with  $L/H = 2.5$ , and (4) counter rotating vortices, one vortex having double the strength of the other, that rotate away from each other with  $L/H = 4.0$ .

Figure 4(a) shows a comparison between the ideal flow calculation of vortex paths and the calculated values of streamwise vorticity from PEP SIG for case 1. The vortices are rotating away from each other. The graph of the idealized vortex motion shows the centers being attracted to each other for a short time and then they proceed to march away from the wall. The streamwise vorticity contour plots show the same type of motion of the vortices. Since the two vortices are moving toward the center of the duct the curved walls do not affect their motion. Although the viscous calculation was set up to attempt to model the ideal flow the results of figure 4(a) show that the vortex strength is dissipating a significant amount as it moves downstream. Figure 4(b) shows the same comparison for two vortices that are rotating toward each other. The graph of the idealized vortex motion shows the centers being forced towards the wall, then the wall starts to force the two vortices away from each other. The four streamwise vorticity contour plots show the progression of the two vortices as they march down the duct. The vortices exhibit the same basic behavior as the ideal flow results except for the confining effect of the curved walls. Again in these results the strength of the

agree well with the experiment. From this comparison it is evident that the overall effects of the vortex are predicted but if detailed information about skin friction and heat transfer are needed the effect of the wall on the vortex must be better modeled.

#### DIFFUSING S-BEND WITHOUT VORTEX GENERATORS

Figure 7 shows the 30 degree-30 degree S-bend diffuser tested experimentally in reference 13. The flow in this duct was turbulent with a Mach number of 0.6 and a Reynolds number based on the duct diameter of 1 760 400. The initial conditions were measured at 1.65 duct diameters upstream of the first bend to remove the influence of the bend on the static pressure. The initial boundary layer thickness was 0.1 times the initial duct radius and the area ratio was 1.51. In both the experiment and the analysis the flow in the duct separated. This is due to the adverse pressure gradient of the area change combined with the effect of the pressure driven secondary flow due to the centerline curvature. The analysis marches through the separated region by using the "flare" approximation. A good explanation of the "flare" approximation is presented in reference 14.

Figure 8(a) shows the computed contours of a total pressure coefficient,  $C_{pt} = (P_t - P_\infty)/q_\infty$ , at various locations in the duct. Figure 8(b) shows the experimental contours of  $C_{pt}$ . The maximum and minimum values of  $C_{pt}$  at each streamwise station are shown on figures 8(a) and (b). Comparing the computed and experimental results indicates that the analysis is able to adequately predict the total pressure distortions for the duct. The reader must be aware that although the computed results in the separated region will not be correct because of the flare approximation, the global effect of the separated region is well modeled. The comparison also shows that at  $\theta = 30$  degrees, the fourth contour plot, the experimental results indicate a larger separated region. In the experiment the streamwise separated region was found to be between  $\theta = 22$  degrees and  $\theta = 44$  degrees, while in the computation the separated region was between  $\theta = 30$  degrees and  $\theta = 54$  degrees. Figures 9 and 10 show comparisons between the computed and experimental secondary velocity profiles at the inflection plane and at the bend exit. The comparison between the two results is very good. At the inflection point the vortex due to the curvature of the centerline is evident in both plots. Also at the inside of the first bend the separated region can be seen in the experimental results, by the region with no data. In the computed results the onset of separation is also evident where there is minimal secondary flow. At the bend exit both results from figure 10 show that the separated region is gone by the large amount of flow being swept toward the outside of the second bend. These results differ from those of a nondiffusing circular cross section S-bend, where the vortex due to the centerline curvature is strengthened in the second bend.

#### DIFFUSING S-BEND WITH VORTEX GENERATORS

After the separation was found experimentally in the S-bend diffuser, three pairs of vortex generators were placed in the duct to remove the separation. Figure 11 shows the specifications for the vortex generators and figure 12 shows a schematic of the diffuser with the axial location of the vortex generators indicated. The generators were placed well upstream of the

600 to 700 grid points per second. This is approximately 150 to 200 times faster than a full Navier-Stokes analysis for comparable accuracy.

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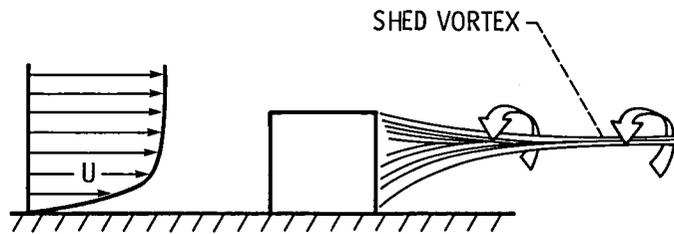
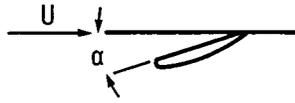
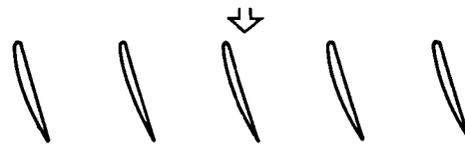
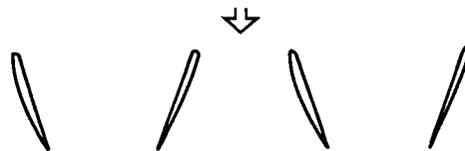


Figure 1. - A typical vortex generator.

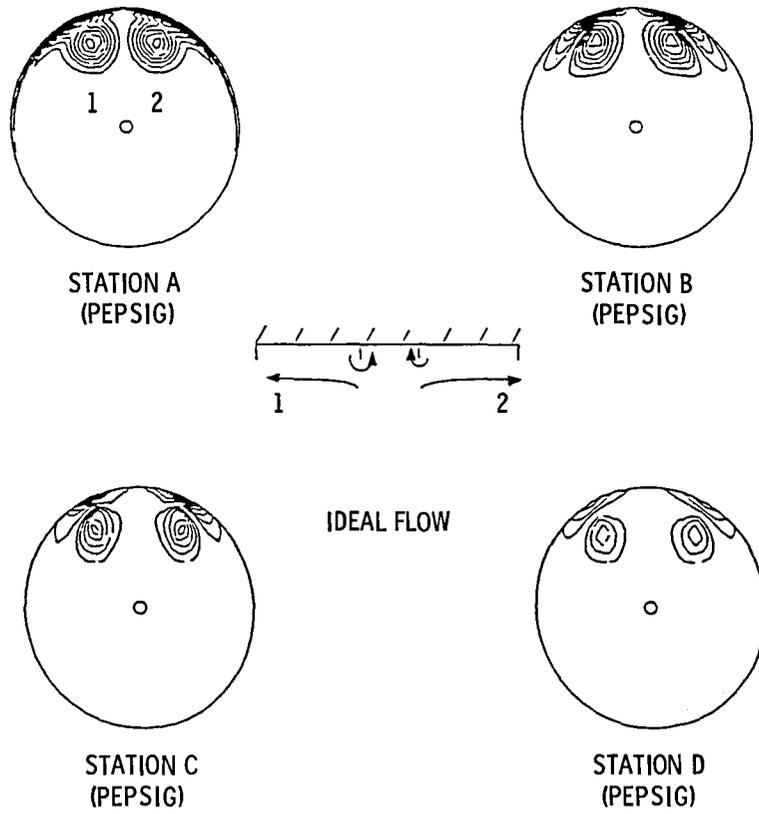


(a) Co-rotating.



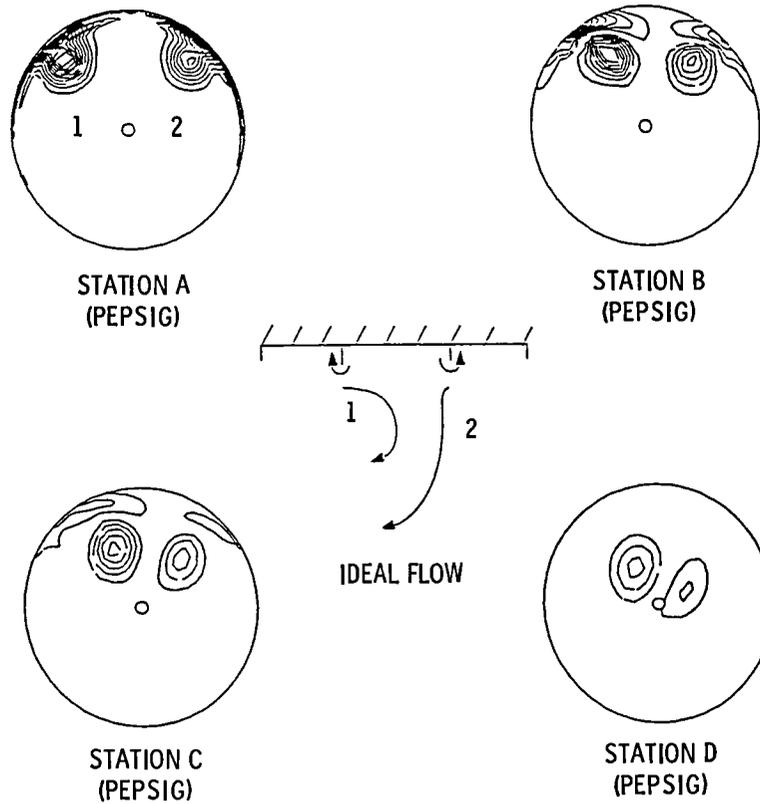
(b) Counter rotating.

Figure 2. - Typical vortex generator configurations.



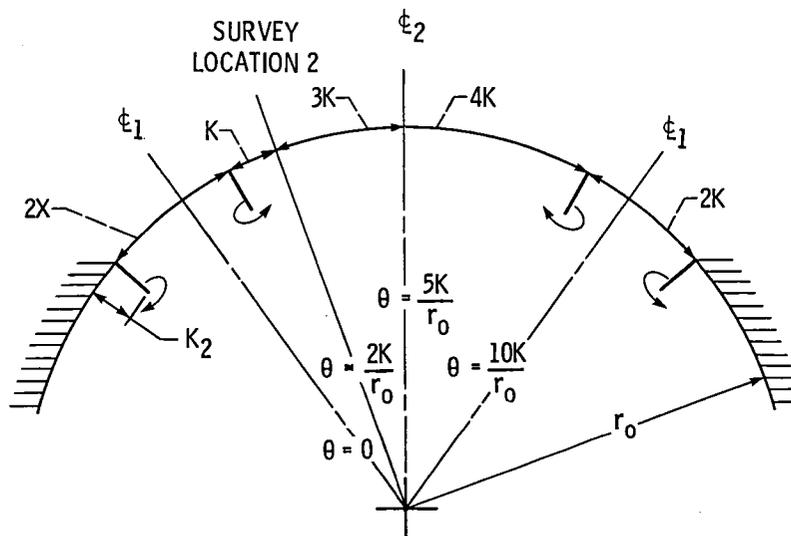
(b) Case 2: Counter rotating vortices of equal strengths rotating towards each other.  $L/H = 2.5$ .

Figure 4. - Continued.



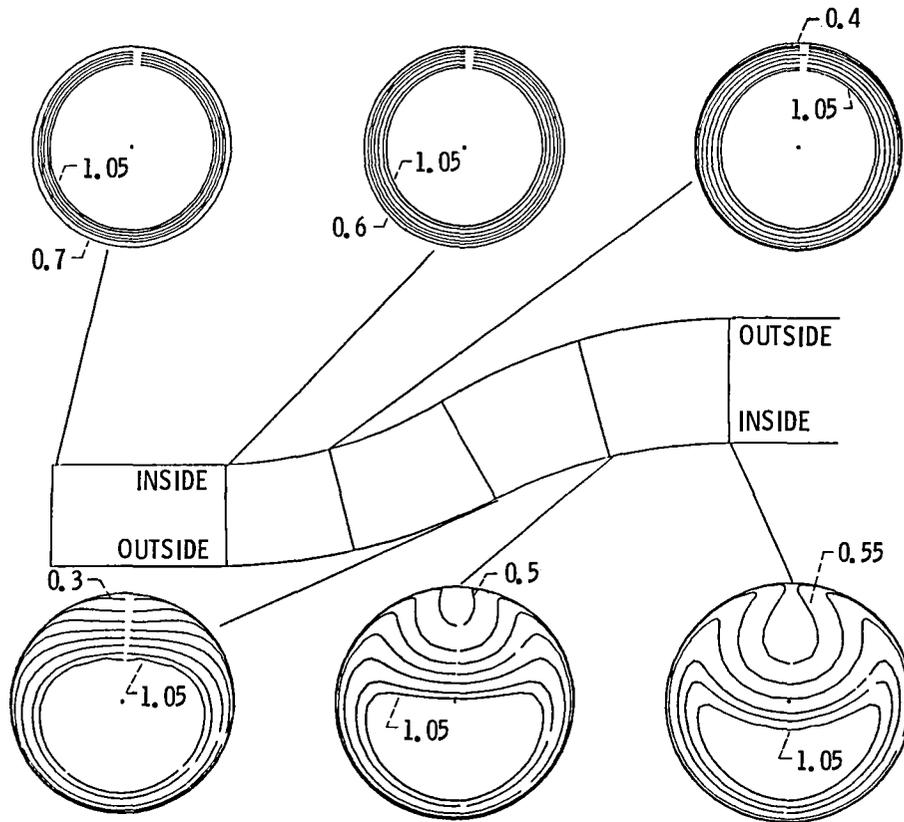
(d) Case 4: Counter rotating vortices with the strength of vortex 1 twice that of vortex 2. Rotation is away from each other.  $L/H = 4.0$ .

Figure 4. - Concluded.



$\phi_1$  = CENTERLINE OF ELEMENT PAIR  
 $\phi_2$  = CENTERLINE OF ADJACENT PAIRS  
 $K$  = ELEMENT HEIGHT  
 $r_0$  = CHANNEL RADIUS  
 $\theta$  = AZIMUTHAL LOCATION MEASURED FROM  $\phi$  OF AN ELEMENT PAIR

Figure 5. - Schematic of vortex generator locations in a straight duct.



(a) Computed total pressure coefficient contours for S-duct without v.g.'s.

Figure 8.

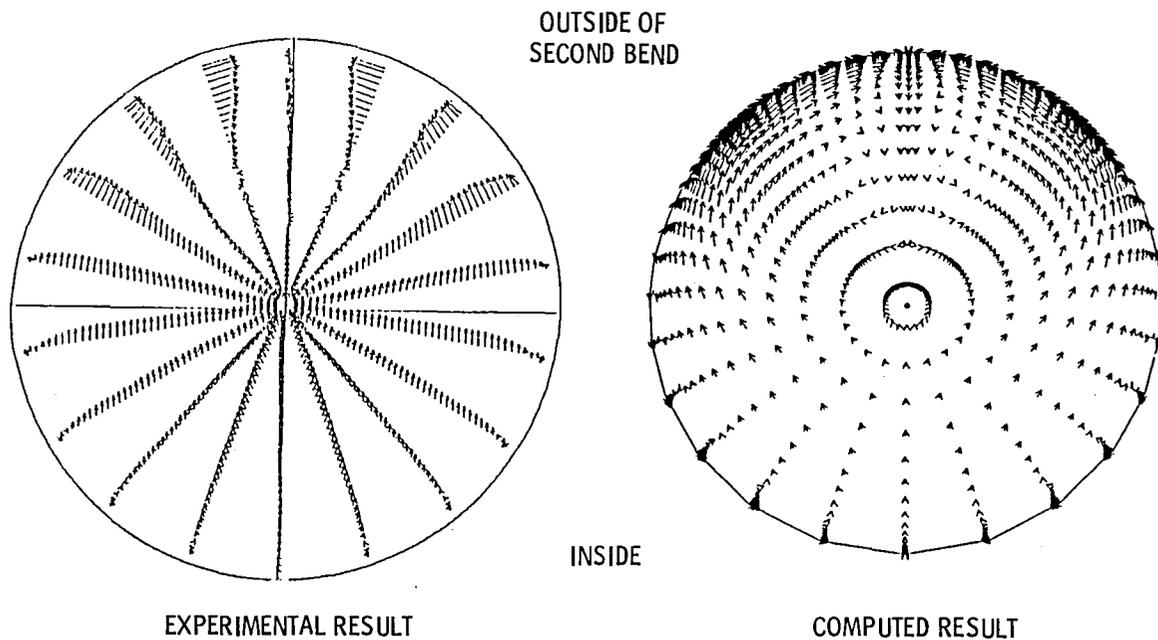
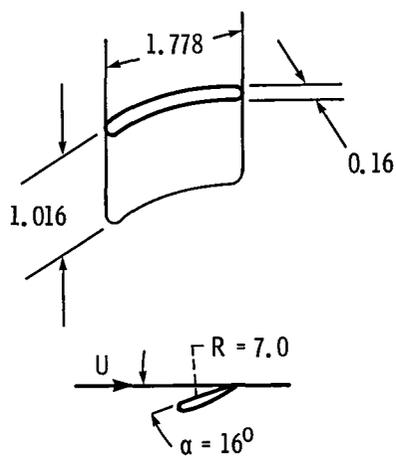
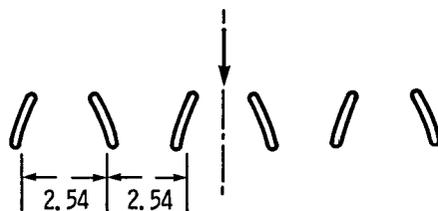


Figure 10. - Comparison of secondary flow at the exit plane for S-duct without v.g.'s.

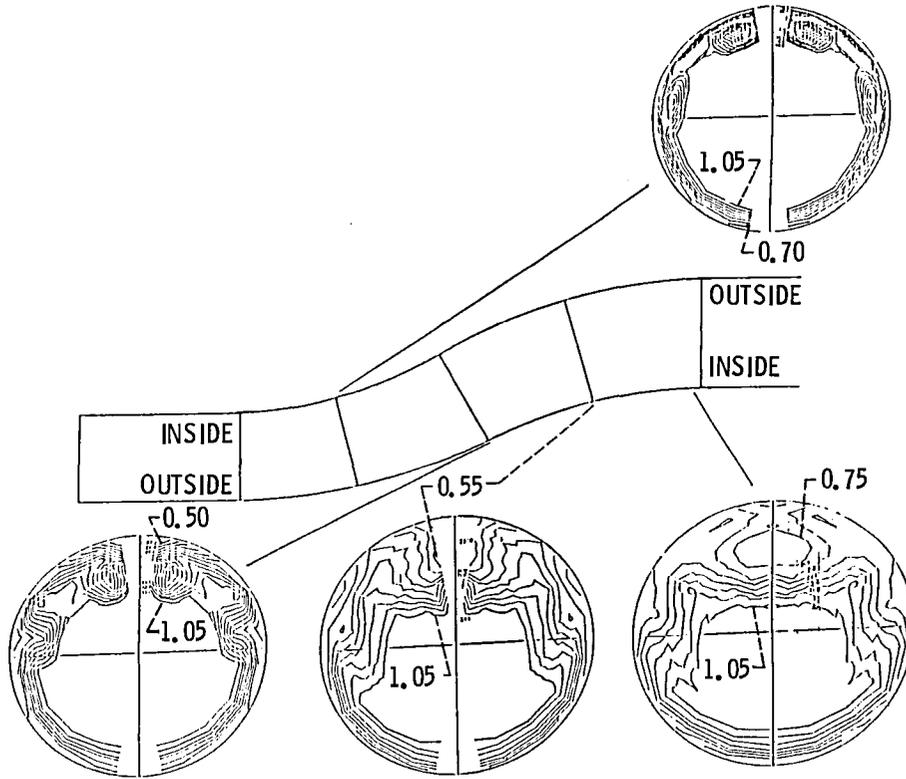


(a) Dimensions of vortex generator.



(b) Dimensions of v.g. configuration.  
All dimensions in cm.

Figure 11. - Vortex generator configuration for S-duct diffuser.



(b) Experimental total pressure coefficient contours for S-duct with v.g.'s.  
Figure 13. - Concluded.

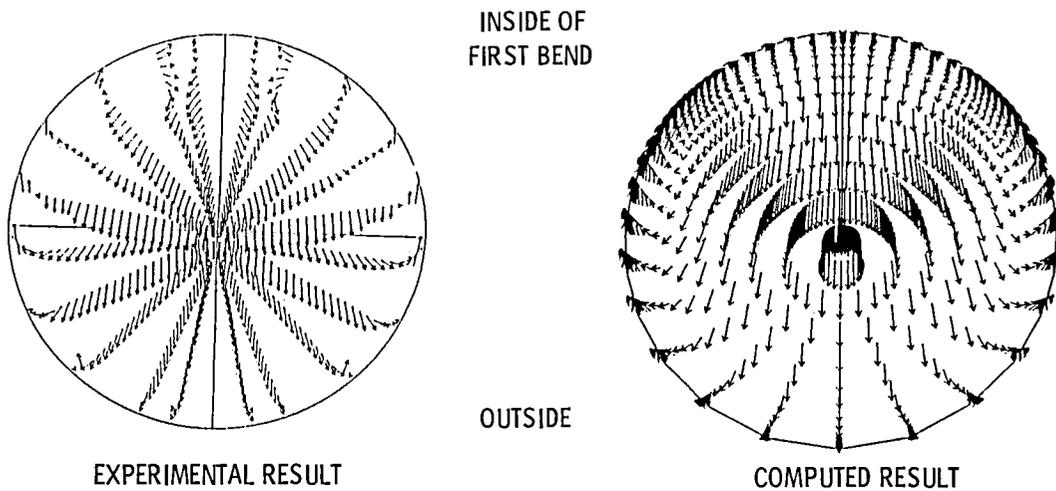


Figure 14. - Comparison of secondary flow at the inflection plane for S-duct with v.g.'s.

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