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# A REVIEW OF REACTION RATES AND THERMODYNAMIC AND TRANSPORT PROPERTIES FOR THE 11-SPECIES AIR MODEL FOR CHEMICAL AND THERMAL NONEQUILIBRIUM CALCULATIONS TO 30000 K 




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## Summary

Reaction rate coefficients and thermodynamic and transport properties are provided for the 11 -species air model which can be used for analyzing flows in chemical and thermal nonequilibrium. Such flows will likely occur around currently planned and future hypersonic vehicles. Guidelines for determining the state of the surrounding environment are provided. Approximate and more exact formulas are provided for computing the properties of partially ionized air mixtures in such environments.

## Introduction

Currently envisaged transatmospheric and aeroassist missions (refs. 1,2.3, and 4) have created a resurgence of interest in the aerothermodynamic design of hypersonic vehicles. However, the velocities and altitudes at which these proposed craft would operate are different, and sometimes more severe, than have been experienced in the past. As a result, the nonequilibrium flow environment which will surround these vehicles will considerably impact the vehicle aerodynamics, thermal loads, and propulsion system efficiency. Since such an environment is difficult to simulate in current ground based-test facilities, the design of these future vehicles will rely heavily on numeric calculations. In turn, these calculations will require a good understanding of the physical modelling required to simulate these phenomena.

Under hypersonic flight conditions, a vehicle travelling through the atmosphere will excite the air which flows around the body to very high temperatures as kinetic energy from the vehicle is transferred. Depending on the flight velocity, various chemical reactions will be produced behind a shock wave as shown in figure 1 (which is adapted from ref. 5) for the stagnation region of a 30.5 cm ( 1 ft ) radius sphere. These reactions will affect the properties of air and cause considerable deviation from those of a thermally and calorifically perfect gas. A vehicle flying through the higher reaches of the atmosphere at high velocities may also experience thermal nonequilibrium (fig. 1), since the lower density reduces the collision frequency, and the high velocity results in smaller transit times for the air molecules. Both of these processes create a delay in the equilibration of translational, rotational and vibrational modes of the thermal energy. Under these conditions, the modelling of the air chemistry requires a multi-temperature approach in contrast to classical single temperature formulations.

Figure 1 delineates four regions (I through IV), showing when the various chemical activities are initiated at a given altitude and velocity. Similarly, it also depicts through Regions A, B and C the initiation of chemical and thermal nonequilibrium processes for different velocity and altitude conditions. This figure clearly shows that the reaction rate coefficients and thermodynamic and transport properties would change continuously for a given flight trajectory. For example, in regions A and B (i.e., before initiation of thermal nonequilibrium), the specific heat at constant pressure $C_{p}$ would change as follows:
$C_{p}=$ constant in Region I, before the excitation of vibrational energy mode
$=C_{p}(T)$ in Region I, after the excitation of vibrational energy mode and before the dissociation of oxygen
$=C_{p}\left(C_{i}, T\right)$ after the dissociation of oxygen
Similarly, the equation of state would change along the flight trajectory as the thermal equilibrium and thermal nonequilibrium regions (ref. 6) are traversed.

$$
\begin{aligned}
& p=\rho \frac{R_{u n i v}}{\bar{M}} T \\
& \text { in Regions } \mathrm{A} \text { and } \mathrm{B} \\
&=\rho \frac{R_{u n i v}}{\bar{M}} T_{t r} \\
& \text { in Region } \mathrm{C}
\end{aligned}
$$

In numerical simulations, the thermodynamic and transport properties and reaction rate coefficients (in the case of finite rate chemistry) are typically required. It is obvious from the previous discussion that these properties and the equation of state should be evaluated carefully when chemical and thermal nonequilibrium conditions exist in the flowfield around a hypersonic vehicle. Under chemical and thermal equilibrium conditions, the transport and thermodynamic properties of high temperature air and its components are well documented in the literature (refs. 7,8, and 9). However, for flows with finite-rate chemistry the individual species properties and appropriate mixing laws which are required are not as well established. For example, in a partially ionized gas mixture, the conventional mixing laws (refs. 10 and 11) developed for non-ionized mixtures can not be extended to higher temperatures without considerable error (ref. 12).

The purpose of this report is to provide thermodynamic and transport properties and the reaction rate coefficients of the most important reactions for the 11 constituent species of air ( $\mathrm{N}, \mathrm{O}, \mathrm{N}_{2}, \mathrm{O}_{2}, \mathrm{NO}, \mathrm{N}^{+}, \mathrm{O}^{+}, \mathrm{N}_{2}^{+}, \mathrm{O}_{2}^{+}, \mathrm{NO}^{+}, e^{-}$) for temperatures up to 30000 K . Approximate and more exact mixing laws are also provided for partially ionized gas mixtures. Sources of the input data used in the calculation of various flowfield properties are identified. Appropriate formulas are provided for using these propertics in computations of flows with thermal nonequilibrium.

## Symbols

| $A_{n}$ | coefficients of polynomial curve-fits for thermodynamic properties, $n=1,2 \ldots, 7$ |
| :---: | :---: |
| $A_{b, r}$ | coefficient in the Arrhenius form of backward reaction rate con stant |
| $A_{f, r}$ | coefficient in the Arrhenius form of forward reaction rate constant |
| $A_{i j}$ | nondiagonal matrix elements of the first Chapman-Enskog formula |
| $A_{i j}^{*}$ | ratio of collision cross sections, $\bar{\Omega}_{i j}^{(2,2)} / \bar{\Omega}_{i j}^{(1,1)}$ |
|  | curve-fit coefficients for diffusion coefficient $\bar{D}_{i j}$ |
|  | $, E_{K_{f, i}}$ <br> coefficients of polynomial curve fits for frozen thermal conductivity of species $i$ |
|  | rve-fit coefficients for viscosity of species $i$ |
|  | $D_{\bar{\Omega}_{i j}^{(i, 1)}}^{(1)}$ <br> rve-fit coefficients for collision cross section $\bar{\Omega}_{i j}^{(1,1)}$ |


|  |  |
| :---: | :---: |
|  |  |
|  | curve-fit coefficients for collision cross section ratio $B_{i j}{ }^{*}$ |
| $B_{i j}^{*}$ | ratio of collision cross sections, ( $\left.5 \bar{\Omega}_{i j}^{(1,2)}-4 \bar{\Omega}_{i j}^{(1,3)}\right) / \bar{\Omega}_{i j}^{(1,1)}$ |
| $B_{b, r}$ | temperature exponent for backward reaction rate constant |
| $B_{f, r}$ | temperature exponent for forward reaction rate constant |
| $C_{i}$ | mass fraction of species $i$ |
| $C_{p}$ | specific heat at constant pressure, $\left[\frac{\partial h}{\partial T}\right]_{p}$, cal/gm-mole $-K$ |
| $C_{p_{d}}$ | diffusion specific heat at constant pressure, $\left[\sum_{i=1}^{N S} h_{i} \frac{\partial C_{i}}{\partial T}\right]_{p}, \text { call } g m-m o l e-K$ |
| $C_{p_{f}}$ | frozen specific heat, |
|  | $C_{p_{f}}=\sum_{i=1}^{N S} C_{i} C_{p, i}=\left[\frac{\partial h}{\partial T}-\sum_{i=1}^{N S} h_{i} \frac{\partial C_{i}}{\partial T}\right]_{p}, \text { cal } / g m-\text { mole }-K$ |
| $C_{p, i}$ | specific heat of species $i,\left(\frac{\partial h_{i}}{\partial T}\right]_{p}$, call $g m-$ mole $-K$ |
| $D_{i i}$ | coefficient of self-diffusion, $\mathrm{cm}^{2} / \mathrm{sec}$ |
| $D_{i j}$ | binary diffusion coefficient, $\mathrm{cm}^{2} / \mathrm{sec}$ |
| $E_{b, r}$ | activation energy for the backward reaction $r$, erg/gm-mole |
| $E_{f, r}$ | activation energy for the forward reaction $r$, erg/gm-mole |
| $F_{i}^{o}$ | free energy of species $i$ at 1 atm pressure (standard state), cal/gm-mole |
| $h$ | enthalpy of mixture, $\sum_{i=1}^{N S} C_{i} h_{i}$, cal/gm-mole |
| $h_{i}$ | enthalpy of species $i$, cal/gm-mole |
| $h_{i, v i b}$ | vibrational component of enthalpy of a molecular species $i$, cal/gm - mole |
| $\left(\Delta h_{i}{ }^{f}\right)_{T_{r e f}}$ | standard heat of formation of species $i$ at temperature $T_{\text {ref }}$, cal/gm-mole |
| $J_{i}^{k}$ | diffusion mass flux of species $i, \mathrm{gm} / \mathrm{cm}^{2}-\mathrm{sec}$ |
| K | total effective thermal conductivity of mixture in thermodynam ic equilibrium, $K_{f}+K_{d}$ or $K_{f}+K_{r}$, cal/cm-sec $-K$ |
| $K_{d}$ | diffusion component of thermal conductivity of mixture defined by equation (A14), cal/ $\mathrm{cm}-\mathrm{sec}-K$ |
| $K_{e}$ | thermal conductivity of electrons, cal/ $\mathrm{cm}-\mathrm{sec}-\mathrm{K}$ |
| $K_{e}^{\prime}$ | thermal conductivity of electrons due to electron-electron collisions only, cal/ cm-sec-K |
| $K_{e l}$ | component of thermal conductivity of mixture due to electron excitation, cal/ $\mathrm{cm}-\mathrm{sec}-K$ |


| $K_{f}$ | frozen thermal conductivity of mixture in thermodynamic equilibrium, $K_{\text {tr }}+K_{\text {int }}$, cal/cm-sec $-K$ |
| :---: | :---: |
| $K_{f, i}$ | frozen thermal conductivity of species $i$ in thermodynamic equilibrium, $K_{i r, i}+K_{i n t, i}$, cal/ $\mathrm{cm}-\mathrm{sec}-K$ |
| $K_{i n t}$ | internal component of frozen thermal conductivity of a mixture in thermodynam ic equilibrium, $K_{r o t}+K_{v i b}+K_{e l}$, cal/cm $-\mathrm{sec}-K$ |
| $K_{\text {int,i }}$ | internal component of the frozen thermal conductivity of species $i$ in thermodynamic equilibrium, cal/ $\mathrm{cm}-\mathrm{sec}-K$ |
| $K_{r}$ | reaction component of thermal conductivity of mixture defined by equation (A16), cal/ $\mathrm{cm}-\mathrm{sec}-K$ |
| $K_{t r}, K_{t r}{ }^{(1)}$ | translational thermal conductivity of mixture from first Chapman-Enskog approximation, $\mathrm{cal} / \mathrm{cm}-\mathrm{sec}-\mathrm{K}$ |
| $K_{\text {tr }}^{*}$ | translational thermal conductivity of mixture without contributions due to electron-heavy particle collisions, $K_{t r}-K_{e}$, cal/cm-sec-K |
| $K_{t r, i}$ | translational component of thermal conductivity of species $i$, cal/cm-sec-K |
| $K_{\text {vib }}$ | vibrational component of thermal conductivity of mixture, cal/cm-sec-K |
| $k$ | Boltzm ann's constant, $1.38 \times 10^{-16} \mathrm{erg} / \mathrm{K}$ |
| $k_{b, r}$ | backward reaction rate coefficient for reaction $r, \mathrm{~cm}^{3} / \mathrm{mole}-\mathrm{sec}$ or $\mathrm{cm}^{6} / \mathrm{mole}^{2}-\mathrm{sec}$ |
| $k_{f, r}$ | forward reaction rate coefficient for reaction $r, \mathrm{~cm}^{3} / \mathrm{mole}-\mathrm{sec}$ |
| $L e_{f, i}$ | frozen binary Lewis number, $\rho C_{p_{f}} D_{i j} / K_{f}$ |
| $L e_{r, i}$ | reactive binary Lewis number, $\rho C_{p} D_{i j} / K$ |
| $M_{i}$ | molecular weight of species $i, \mathrm{gm} / \mathrm{gm}$-mole |
| M | molecular weight of mixture, $\mathrm{gm} / \mathrm{gm}$-mole |
| $N_{\text {A }}$ | Avogadro's number, $6.0225 \times 10^{23}$ molecules/gm - mole |
| $n$ | number density, particles $/ \mathrm{cm}^{3}$ |
| $P r_{f}$ | frozen Prandtl number, $C_{p}{ }^{\mu /} K_{f}$ |
| Pr $r_{\text {r }}$ | reactive Prandtl number, $C_{p} \mu / K$ |
| $p$ | pressure, dyne/ $\mathrm{cm}^{2}$ |
| $q^{k}$ | $k$ th component of the overall heat flux vector, cal/ $\mathrm{cm}^{2}-\mathrm{sec}$ |
| $q_{e}^{k}$ | $k$ th component of the electron heat flux vector due to electronelectron collisions, cal/ $\mathrm{cm}^{2}-\mathrm{sec}$ |
| $q_{v i b}^{k}$ | $k$ th component of the vibrational heat flux vector due to molecule-molecule collisions, cal/ $\mathrm{cm}^{2}-\mathrm{sec}$ |
| $R_{\text {univ }}$ | universal gas constant, $1.987 \mathrm{cal} / \mathrm{gm}-\mathrm{mole}-\mathrm{K}$ |
| $T$ | temperature under thermodynamic equilibrium, $K$ |
| $T_{D_{b, r}}$ | characteristic reaction temperature for the backward reaction $r$, $E_{b, r} / k, K$ |


| $T_{D_{f, r}}$ | characteristic reaction temperature for the forward reaction $r$, $E_{f, r} / k, K$ |
| :---: | :---: |
| $T_{e}$ | electron temperature, $K$ |
| $T_{e l}$ | electronic excitation temperature, $K$ |
| $T_{\text {ref }}$ | reference temperature, 298.15 K |
| $T_{\text {rot }}$ | rotational temperature, $K$ |
| $T_{t r}$ | translational temperature, $K$ |
| $T_{v e}$ | vibrational-electron-electronic excitation tem perature, $K$ |
| $T_{\text {vib }}$ | vibrational temperature, $K$ |
| $t$ | time, sec |
| $V_{i}^{k}$ | $k$ th component of diffusion velocity of species $i, \mathrm{~cm} / \mathrm{sec}$ |
| $\dot{w}_{i}$ | mass rate of formation of species $i, g / \mathrm{cm}^{3}-\mathrm{sec}$ |
| $\boldsymbol{X}_{\boldsymbol{i}}$ | concentration of species $i$, moles/volume |
| $x^{k}$ | $k$ th component of general orthogonal coordinate system |
| $x_{i}$ | mole-fraction of species $i$ |
| $\alpha_{i, r}$ | stoichiometric coefficients for reactants |
| $\beta_{i, r}$ | stoichiometric coefficients for products |
| $\gamma_{j}$ | mole mass ratio of species $j, X_{j} / \rho$ |
| $\mu^{(1)}, \mu$ | viscosity of mixture from first Chapman-Enskog approximation, $\mathrm{gm} / \mathrm{cm}-\mathrm{sec}$ |
| $\mu_{i}$ | viscosity of species $i, \mathrm{gm} / \mathrm{cm}-\mathrm{sec}$ |
| $\rho$ | density of the mixture, $\mathrm{gm} / \mathrm{cm}^{3}$ |
| $\boldsymbol{\rho}_{\text {i }}$ | density of species $i, \mathrm{gm} / \mathrm{cm}^{3}$ |
| $\bar{\Omega}_{i j}^{(1,1)}$ | average collision cross section (for diffusion, viscosity, and translational, internal and reaction components of thermal conductivity) for collisions between the species $i$ and $j, \AA^{2}$; $1 \AA=10^{-8} \mathrm{~cm}$ |
| $\bar{\Omega}_{i j}^{(2,2)}$ | average collision cross section (for viscosity and translational component of thermal conductivity) for collisions between the species $i$ and $j, \AA^{2}$ |
| $\bar{\Omega}_{i j}^{(1,2)}, \bar{\Omega}_{i j}^{(1,3)}$ | average collision cross sections (for translational component of thermal conductivity) for collisions between the species $i$ and $j$, $\AA^{2}$ |

Subscripts:

| $b$ | backward reaction |
| :--- | :--- |
| $e$ | electron |
| $e l$ | electronic excitation |
| $f$ | forward reaction |
| $i$ | species $i$ |

```
j species j
p constant pressure
r rth reaction
ref reference condition
rot rotational energy mode
tr translational energy mode
ve
v
total number of species, \equiv NS
```

Abbreviations:

AOTV
NASP
NIR
$N J$

NR
NS

Aeroassisted Orbital Transfer Vehicle
National Aero-Space Plane
total number of independent reaction
sum of the reacting species ( $N S$ ) plus the number of catalytic bodies
total number of reactions
total number of species

## Chemical Kinetic Model and Reaction Rates

When chemical reactions proceed at a finite rate, the rate of production terms appear in the energy equation when formulated in terms of temperature and in the species continuity equations (refs. 13,14,15). For a multicomponent gas with $N S$ reacting chemical species and $N R$ chemical reactions, the stoichiometric relations for the overall change from reactants to products are:

$$
\begin{equation*}
\sum_{i=1}^{N J} \alpha_{i, r} X_{i} \underset{k_{b, r}}{\stackrel{k_{f, r}}{\rightleftarrows}} \sum_{i=1}^{N J} \beta_{i, r} X_{i} \tag{1}
\end{equation*}
$$

where $r=1,2, \ldots, N R$ and $N J$ is equal to the sum of the reacting species ( $N S$ ) plus the number of catalytic bodies. The quantities $\alpha_{i, r}$ and $\beta_{i, r}$ are the stoichiometric coefficients for reactants and products, respectively, and $k_{f, r}$ and $k_{b, r}$ are the forward and backward rate constants. The quantities $X_{i}$ denote the concentrations of the chemical species and catalytic bodies in moles per unit volume. The catalytic bodies ( $N J-N S$ ) may be chemical species or linear combinations of species that do not undergo a chemical change during the reaction.

The net mass rate of production of the ith species per unit volume resulting from all the reactions $N R$ may be obtained (ref. 14) from

$$
\begin{equation*}
\dot{w}_{i}=M_{i} \sum_{r=1}^{N R}\left(\frac{d X_{i}}{d t}\right)_{r}=\sum_{r=1}^{N R}\left(\frac{d \rho_{i}}{d t}\right)_{r} \tag{2a}
\end{equation*}
$$

or

$$
\begin{equation*}
\dot{w}_{i}=M_{i} \sum_{r=1}^{N R}\left(\beta_{i, r}-\alpha_{i, r}\right)\left(R_{f, r}-R_{b, r}\right) \tag{2b}
\end{equation*}
$$

where

$$
\begin{align*}
& R_{f, r}=k_{f, r} \prod_{j=1}^{N J}\left(\gamma_{j} \rho\right)^{\alpha_{j, r}}  \tag{2c}\\
& R_{b, r}=k_{b, r} \prod_{j=1}^{N J}\left(\gamma_{j} \rho\right)^{\beta_{j, r}} \tag{2d}
\end{align*}
$$

Here, the mole-mass ratio $\gamma_{j}$ is defined as

$$
\gamma_{j}= \begin{cases}\frac{X_{j}}{\rho}=\frac{C_{j}}{M_{j}} & j=1,2, \ldots, N S  \tag{2e}\\ \sum_{i=1}^{N S} Z_{(j-N S), i} \gamma_{i} & j=N S+1, \ldots, N J\end{cases}
$$

The constants $Z_{(j-N S), i}$ are determined from linear dependence of the catalytic bodies upon the $N S$ species. Values of these constants for the 11 -species air model are given in table 1 .

The reaction rates in equation (1) or equations (2c) and (2d) are expressed in the Arrhenius form as:

$$
\begin{array}{ll}
k_{f, r}=A_{f, r} T^{B_{f, r}} \exp \left(-T_{D_{f, r}} / T\right), & \frac{1}{s}\left[\frac{m o l e}{c m^{3}}\right)^{-\alpha_{r}} \\
k_{b, r}=A_{b, r} T^{B_{b, r}} \exp \left(-T_{D_{b, r}} / T\right), & \frac{1}{s}\left(\frac{m o l e}{\mathrm{~cm}^{3}}\right]^{-\beta_{r}} \tag{3b}
\end{array}
$$

where

$$
\begin{align*}
& \alpha_{r}=\sum_{i=1}^{N J} \alpha_{i, r^{-1}}  \tag{4a}\\
& \beta_{r}=\sum_{i=1}^{N J} \beta_{i, r}-1 \tag{4b}
\end{align*}
$$

and $T_{D_{f}, r}$ and $T_{D_{b, r}}$ are the characteristic reaction temperatures for the forward and backward reactions, respectively. Values for the reaction rates $k_{f, r}$ and $k_{b, r}$ are tabulated in table II for the 11-species air model. For a specified temperature, density, and species composition, equations (2) through (4) can be used to obtain the production rate of a species $i$ in a multicomponent gas by employing the catalytic body efficiencies and reaction rates from tables I and II. The first seven reactions and reaction rates in table Il are taken from reference 16 and were employed in reference 13 for the 7 species air model ( $N, O, N_{2}, O_{2}, N O, N O^{+}, e^{-}$). Reaction rates for reactions 8 through 20 of table II are taken from reference 17. Some of these reactions have been regrouped here (and in ref. 18) through the use of third bodies $\mathrm{M}_{1}$ through $\mathrm{M}_{4}$ which is similar to the approach in reference 13.

The reaction rates given in table II were originally used by Blottner (ref. 13) and Dunn and Kang (ref. 17) in the context of a single temperature assuming thermal equilibrium. One may use Park's (ref. 19) guidelines (in the context of his twotemperature model) for defining the rate controlling temperature in dissociation and electron impact ionization reactions under thermal nonequilibrium conditions. This was done in reference 20 , for example.

Park has suggested the use of a temperature weighted with the vibrational temperature to characterize dissociation reactions, based on the preferential dissociation concept. The reaction rates in Park's model are assumed to be dictated by the geometric average temperature

$$
\begin{equation*}
T_{a v}=\sqrt{T_{t r} T_{v i b}} \tag{5}
\end{equation*}
$$

and the dissociation reaction rates are given by

$$
\begin{equation*}
k_{f, r}=A_{f, r} T_{a v}^{B_{f, r}} \exp \left(-T_{D_{f, r}} / T_{a v}\right) \tag{6}
\end{equation*}
$$

Treanor and Marrone (refs. 21 and 22) have suggested a more rational (but slightly more difficult) way than Park's to account for the effect of vibrational relaxation on dissociative reactions with the preferential dissociation concept. They have suggested the use of a vibrational coupling factor (refs. 20,21, and 22) with the dissociation reaction rates obtained under the assumption of thermal equilibrium.

Recent work of Jaffe (ref. 23), based on collision theory and using methods of statistical mechanics, found no evidence of preferential weighting to any particular energy mode in obtaining the total energy available in a collision whether it is an elastic, inelastic, or reactive encounter. Jaffe found that the multi-temperature effects on the reaction rates were small for dissociation. These findings were supported by those of Moss et al. (ref. 24), who carried out flowfield analyses employing the Direct Simulation Monte Carlo (DSMC) approach. Thus, a weaker dependence of $k_{f, r}$ on $T_{v i b}$ (such as the one recently suggested by Sharma et al. (ref. 25) as $T_{a v}=T_{t r}^{0.7} T_{v i b}^{0.3}$ ) might be more realistic, especially for highly energetic flows.

It is obvious that the multi-temperature kinetic models for high energy flows based on both preferential and non-preferential dissociation assumptions employ some degree of empiricism. They exemplify the degree of uncertainty which exists in modelling the multi-temperature kinetics. Quantum mechanical studies of the type in reference 23 supplemented by non-obtrusive laser diagnostic studies would be desirable to establish these models on a sounder basis.

## Species Thermodynamic Properties and Mixture Formulas

Thermodynamic properties (i.e., $C_{p, i}$ and $h_{i}$ ) are required for each species considered in a finite-rate flowfield calculation. For calculations with chemical equilibrium, the free energies $F_{i}$ are also required. Since the multicomponent gas mixtures are considered to be mixtures of thermally perfect gases, the thermodynam ic properties for each species are calculated by using the local static temperature. Then, properties for the gas mixture are determined in terms of the individual species properties through the relations:

$$
\begin{equation*}
h=\sum_{i=1}^{N S} C_{i} h_{i} \tag{7a}
\end{equation*}
$$

with

$$
\begin{equation*}
h_{i}=\int_{298}^{T} C_{p, i} d T+\left(\Delta h_{i}^{f}\right)_{T=298 K} \tag{7b}
\end{equation*}
$$

and

$$
\begin{equation*}
C_{p_{f}}=\sum_{i=1}^{N S} C_{i} C_{p, i} \tag{8a}
\end{equation*}
$$

with

$$
\begin{equation*}
C_{p, i}=\left[\frac{\partial h_{i}}{\partial T}\right]_{p} \tag{8b}
\end{equation*}
$$

Note that $C_{p_{f}}$ for a mixture defined through equation (8a) is the 'frozen' specific heat. This definition does not account for species production or conversion due to chemical reactions. Frozen specific heat is commonly employed in defining the Prandtl and Lewis numbers $\dagger$ for a mixture and is related to the mixture enthalpy $h$ through the relation

$$
\begin{equation*}
C_{p_{f}}=\left[\frac{\partial h}{\partial T}-\sum_{i=1}^{N S} h_{i} \frac{\partial C_{i}}{\partial T}\right]_{p}=\sum_{i=1}^{N S} C_{i} C_{p, i} \tag{9}
\end{equation*}
$$

Expressions for $C_{p, i}$ using the partition function approach were obtained in reference 26 , whereas references 27 and 28 employed a virial coefficient method. The partition function formulation is quite accurate at low temperatures; however, this formulation becomes less accurate at high temperatures because of the introduction of errors from several sources such as non-rigidity of the rotor and anharmonicity of the oscillator. The virial formulation defines the potential-energy surface more accurately at higher temperatures in comparison with the partition function approach. Using the virial formulation, Browne (refs. 27 and 28) obtained the thermodynamic properties as corrections to those of the monatomic gas in terms of the first and second virial coefficients and their temperature derivatives. These data can be used to separate the contributions of different internal energy modes to the specific heat as is required in the case of multi-temperature flowfield models. For example, in a two-temperature model (refs. 19 and 20), advantage may be taken of the fact that the translational and rotational energy modes are fully excited at room temperature, and therefore, the heat capacities for these modes are independent of temperature. The combined vibrational-electronic specific heat for species $i,\left(C_{p, i}\right)_{v e}$, can then be evaluated by using the value for the total specific heat, $C_{p, i}$, evaluated at temperature $T_{v e}$ and subtracting out the constant contribution from the translational and rotational specific heats. This can be described (see fig. 2 for the various contributions) by

$$
\begin{equation*}
\left[\left(C_{p, i}\right)_{v e}\right]_{T_{v e}}=\left[C_{p, i}\right]_{T_{w e}}-\left(C_{p, i}\right)_{t r}-\left(C_{p, i}\right)_{r o t} \tag{10}
\end{equation*}
$$

The enthalpy, $h_{i}$, for a two-temperature model can be evaluated similarly, since contributions from the translational and rotational modes are linear with temperature. Therefore, the vibrational-electronic enthalpy for species $i,\left(h_{i}\right)_{v e}$, can be obtained from the specific enthalpy $h_{i}$ evaluated at temperature $T_{v e}$ and subtracting out the contribution from the translational and rotational enthalpies evaluated at $T_{v e}$ as well as the enthalpy of formation.

$$
\begin{equation*}
\left[\left(h_{i}\right)_{v e}\right]_{T_{v e}}=\left[h_{i}\right]_{T_{v e}}-\left[\left(C_{p, i}\right)_{t r}+\left(C_{p, i}\right)_{r o t}\right]\left(T_{v e}-T_{r e f}\right)-\left(\Delta h_{i}^{f}\right)_{T_{r e f}} \tag{11}
\end{equation*}
$$

[^0]The specific enthalpy from all the contributions of internal energy modes can then be obtained by adding the contributions of translational and rotational enthalpies (evaluated at the translational-rotational temperature) and the enthalpy of formation to the vibrational-electronic enthalpy as follows

$$
\begin{equation*}
h_{i}\left(T, T_{v e}\right)=\left[\left(h_{i}\right)_{v e}\right]_{T_{w}}+\left[\left(C_{p, i}\right)_{t r}+\left(C_{p, i}\right)_{r o t}\right]\left(T-T_{r e f}\right)+\left(\Delta h_{i}^{f}\right)_{T_{r f}} \tag{12}
\end{equation*}
$$

Reference 26 has provided curve fits for $C_{p, i}$ and $h_{i}$, whereas references 27 and 28 have provided tabulations of these data. Since the use of curve fits reduces the expense of computing the original functional relations, these thermodynamic properties have been curve fitted here as a function of temperature for the temperature range of $300 \mathrm{~K} \leq T \leq 30000 \mathrm{~K}$. These curve fits include those of reference 26 for the range $300 \mathrm{~K} \leq T \leq 6000 \mathrm{~K}$, and new curve fits are provided to the tabulated values of references 27 and 28 for the range $6000 \mathrm{~K} \leq T \leq 30000 \mathrm{~K}$. The following polynomial equations are employed for these curve fits:
Specific heat:

$$
\begin{equation*}
\frac{C_{p, i}}{R_{\text {univ }}}=A_{1}+A_{2} T+A_{3} T^{2}+A_{4} T^{3}+A_{5} T^{4} \tag{13}
\end{equation*}
$$

Specific enthalpy:

$$
\begin{equation*}
\frac{h_{i}}{R_{u n i v} T}=A_{1}+\frac{A_{2} T}{2}+\frac{A_{3} T^{2}}{3}+\frac{A_{4} T^{3}}{4}+\frac{A_{5} T^{4}}{5}+\frac{A_{6}}{7} \tag{14}
\end{equation*}
$$

For equilibrium calculations, the following curve fit for the free energies $F_{i}$ may be used:

$$
\begin{equation*}
\frac{F^{o_{i}}}{R_{u n i v} T}=A_{1}[1-\ln (T)]-\frac{A_{2} T}{2}-\frac{A_{3} T^{2}}{6}-\frac{A_{4} T^{3}}{12}-\frac{A_{5} T^{4}}{20}+\frac{A_{6}-A_{7}}{T} \tag{15}
\end{equation*}
$$

where $F^{o_{i}}$ is the free energy of species $i$ at 1 atm pressure (standard state).
A tabulation of the polynomial constants ( $A_{1}$ to $A_{7}$ ) for the 11 -species air model is given in table III. A least squares technique has been used for obtaining the polynomial coefficients for the five temperature ranges between 300 and 30000 K . To assure a smooth variation of thermodynamic properties over the entire temperature range, values of $A_{1}$ to $A_{7}$ should be linearly averaged across the curve-fit boundaries (i.e., $800<T<1200,5500<T<6500,14500<T<15500$, and $24500<T<25500$ ). An example subroutine which evaluates the polynomial curve fits and performs the linear averaging is presented in appendix B. This routine may be easily modified to suit the user's requirements.

It may be mentioned here that temperature, $T$, in equations (13) through (15) is in ${ }^{\circ} \mathrm{K}$. With the universal gas constant in cal/gm-mole $-K$, the specific heat and enthalpies will have the units of cal/gm-mole $-K$ and cal/gm-mole respectively. The constant $A_{6}$ in these equations is related to the heat of formation through the relation

$$
\begin{equation*}
A_{6} R_{\text {univ }}=\left(\Delta h_{i}^{f}\right)_{T=298 \mathrm{~K}} \tag{16}
\end{equation*}
$$

Figure 3 compares the values of specific heat obtained from the polynomial curve fit (eq. (13)) with the data of McBride et al. (ref. 26) and Browne (ref. 28). Values provided by Hansen (ref. 29) are also included for comparison. Hansen's values begin to deviate from those of references 26 and 28 beyond 4000 K for $\mathrm{O}_{2}$ (fig. 3(a)), beyond 8000 K for $N_{2}$ (fig. 3(b)), and beyond 6000 K for $N O$ (fig. 3(c)). This may
be due to the rigid-rotator and harmonic-oscillator partition function employed by Hansen. At higher temperatures, the population of levels corresponding to the nonparabolic regions of the potential energy curve are no longer negligible, and it becomes necessary to introduce the non-rigidity and anharmonicity corrections into the energy levels of the molecules as was done in reference 28.

## Species Transport Properties and Mixture Formulas

The transport properties required in flowfield calculations are viscosity, thermal conductivity, and diffusion coefficients. The collision cross sections required for these properties have been recomputed herein using the same molecular data used previously by Yos (refs. 7,8, and 9). The computational techniques employed in the calculations are described in references 30 and 31 which give details of the NATA (Nonequilibrium Arc Tunnel Analysis) code (ref. 32). In NATA, the average collision cross sections $\pi \bar{\Omega}_{i j}^{(l, s)}$ for the collisions between species $i$ and $j$ are calculated from basic cross section data as functions of temperature and gas composition for each pair of species in the mixture. The basic data are either in tabular form or are given as simple analytical functions of temperature or composition. NATA contains twelve methods or options for calculating the cross sections $\pi \bar{\Omega}_{i i}^{(1,1)}, \pi \bar{\Omega}_{i i}^{(2,2)}$, and $B_{i j}^{*}$ (the ratio of cross sections). The options include using the Coulomb cross section for the electrons and ions plus exponential potential (ref. 33) and Lennard-Jones (6-12) potential (ref. 34) for neutral species in high and low temperature ranges, respectively. The formulas employed in NATA to compute the transport properties from the collision cross sections are obtained from an approximation (ref. 35) to the rigorous first-order Chapman-Cowling expressions.

## Single Species Transport Properties

The viscosity $\mu_{i}$ and frozen $\dagger$ thermal conductivity $K_{f, i}$ of a gas containing a single molecular species are given, to a good approximation, by the formulas (ref. 34, Chapters VII and VIII):

$$
\begin{gather*}
\mu_{i}=\frac{5}{16} \frac{\sqrt{\pi m_{i} k T}}{\pi \bar{\Omega}_{i i}^{(2,2)}}, \quad \frac{g m}{c m-s e c}  \tag{17a}\\
=2.6693 \times 10^{-5} \frac{\pi \sqrt{M_{i} T}}{\pi \bar{\Omega}_{i i}^{(2,2)}}, \quad \frac{g m}{c m-s e c}  \tag{17b}\\
K_{f, i}=K_{t r, i}+K_{i n t, i} \tag{18a}
\end{gather*}
$$

with

$$
\begin{align*}
& K_{t r, i}=\frac{75}{64} \frac{k \sqrt{\pi k T / m_{i}}}{\pi \bar{\Omega}_{i i}^{(2,2)}}, \quad \frac{\mathrm{erg}}{c m-\sec -K}  \tag{18b}\\
& =1.9891 \times 10^{-4} \frac{\pi \sqrt{T / M_{i}}}{\pi \bar{\Omega}_{i i}^{(2,2)}}, \quad \frac{\mathrm{cal}}{c m-\sec -K}  \tag{18c}\\
& =\frac{15}{4} \frac{\mu_{i} R_{u n i v}}{M_{i}}, \quad \frac{\mathrm{cal}}{c m-\sec -K} \tag{18d}
\end{align*}
$$

+ See Appendix A for various definitions
and

$$
\begin{align*}
& K_{\text {int }, i}=\frac{3}{8}\left[\frac{C_{p, i}}{R_{\text {univ }}}-\frac{5}{2}\right] \frac{k \sqrt{\pi k T / m_{i}}}{\pi \bar{\Omega}_{i i}^{(1,1)}}, \frac{e r g}{c m-\sec -K}  \tag{18e}\\
& =6.3605 \times 10^{-5} \frac{\pi \sqrt{T / M_{i}}}{\pi \bar{\Omega}_{i i}^{(1,1)}}\left[\frac{C_{p, i}}{R_{\text {univ}}}-\frac{5}{2}\right], \frac{c a l}{c m-\sec -K}  \tag{18f}\\
& \quad=R_{\text {univ }} \frac{\mu_{i}}{M_{i}}\left[\frac{\rho D_{i i}}{\mu_{i}}\right]\left[\frac{C_{p, i}}{R_{u n i v}}-\frac{5}{2}\right], \frac{c a l}{c m-\sec -K} \tag{18~g}
\end{align*}
$$

where $K_{i r, i}$ is the translational component of the thermal conductivity and $K_{i n t, i}$ is the component of thermal conductivity resulting from the diffusion of internal excitation energy of the molecules. In equations (17a) through (18g), $m_{i}$ is the molecular mass in $g m, k$ is Boltzmann's constant $\left(1.38 \times 10^{-16} \mathrm{erg} / K\right), T$ is the gas temperature in $K$, $\pi \bar{\Omega}_{i i}^{(l, i)}$ are average collision cross-sections for the molecules in $\AA^{2}$, (where $\left.1 \AA=10^{-8} \mathrm{~cm}\right), \quad M_{i}$ is the molecular weight in $\mathrm{gm} / \mathrm{gm}$-mole, $R_{u n i v}=1.987 \mathrm{cal} / \mathrm{gm}$-mole $-K, C_{p, i}$ is the specific heat at constant pressure in cal/gm-mole $-K, \rho$ is the density in $\mathrm{gm} / \mathrm{cm}^{3}$, and $D_{i i}$ is the coefficient of self diffusion in $\mathrm{cm}^{2} / \mathrm{sec}$.

From equations (18a), (18d), and (18g), the frozen thermal conductivity may also be expressed as

$$
\begin{equation*}
K_{f, i}=\frac{R_{u n i v} \mu_{i}}{M_{i}}\left[\frac{15}{4}+\left[\frac{\rho D_{i i}}{\mu_{i}}\right]\left[\frac{C_{p, i}}{R_{\text {univ }}}-\frac{5}{2}\right]\right] \tag{19}
\end{equation*}
$$

The factor ( $\rho D_{i \ddot{u}} / \mu_{i}$ ) appearing in equations ( 18 g ) and (19) is the reciprocal Schmidt number and is related to the collision cross sections $\pi \bar{\Omega}_{i i}^{(l, l)}$ through the relation (ref. 34)

$$
\begin{equation*}
\frac{\rho D_{i i}}{\mu_{i}}=\frac{6}{5} \frac{\pi \bar{\Omega}_{i i}^{(2,2)}}{\pi \bar{\Omega}_{i i}^{(1,1)}} \tag{20}
\end{equation*}
$$

with $D_{i i}$ defined as

$$
\begin{align*}
& D_{i i}=\frac{3}{8} \frac{\sqrt{\pi m_{i} k T}}{\pi \bar{\Omega}_{i i}^{(1.1)}}\left[\frac{1}{\rho}\right),  \tag{21a}\\
=2.6280 \times 10^{-3} \frac{\pi \sqrt{T^{3} / M_{i}}}{\pi \bar{\Omega}_{i i}^{(1,1)} p}, & \frac{\mathrm{~cm}^{2}}{\mathrm{sec}} \tag{21b}
\end{align*}
$$

where $p$ is the pressure in atm. The coefficient of self-diffusion $D_{i i}$, must be regarded as somewhat artificial. It is more correct to regard it as a limiting form of the coefficient of binary diffusion. The ratio $\pi \bar{\Omega}_{i}^{(2,2)} / \pi \bar{\Omega}_{i}^{(1,1)}$ appearing in equation (20) is a very slowly varying function of temperature, $T$, and hence $\rho D_{i i} / \mu_{i}$ is very nearly constant. This factor appearing in equation (19) has a value of unity in the Eucken correction (ref. 34) and is close to 1.32 for the Lennard-Jones potential over a large temperature range (ref. 36).

The collision cross sections $\pi \bar{\Omega}_{i i}^{(l, l)}$ or $\pi \bar{\Omega}_{i j}^{(l, s)_{\ddagger}}$, in general, are the weighted

[^1]given in reference 34 and as $\bar{\Omega}(1, s)$ given in reference 31
averages of the cross sections for collisions between species i and j . These have been defined (refs. 7,8 and 9) as
\[

$$
\begin{equation*}
\pi \bar{\Omega}_{i j}^{(l, s)}=\frac{\int_{0}^{\infty} \int_{0}^{\pi} \exp \left(-\gamma^{2}\right) \gamma^{2 s+3}\left(1-\cos ^{l} \chi\right) 4 \pi \sigma_{i j} \sin \chi d \chi d \gamma}{\int_{0}^{\infty} \int_{0}^{\pi} \exp \left(-\gamma^{2}\right) \gamma^{2 s+3}\left(1-\cos ^{l} \chi\right) \sin \chi d \chi d \gamma} \tag{22}
\end{equation*}
$$

\]

where $\sigma_{i j}=\sigma_{i j}(\chi, g)$ is the differential scattering cross section for the pair $(i, j), \chi$ is the scattering angle in the center of mass system, $g$ is the relative velocity of the colliding particles, and $\gamma=\left(\left[m_{i} m_{j} / 2\left(m_{i}+m_{j}\right) k T\right]^{1 / 2}\right) g$ is the reduced velocity. For collisions between the similar species, equation (22) yields $\pi \bar{\Omega}_{i i}^{(l, l)}$ required in equations (17) and (18).

The collision cross sections $\pi \bar{\Omega}_{i i}^{(1,1)}$ and $\pi \bar{\Omega}_{i i}^{(2,2)}$ employed here are the same as those used by Yos (refs. 7,8,9). The cross sections for the neutral species $N, N_{2}, N O, O$, and $O_{2}$ were taken from the tabulations of Yun et al. (ref. 37), for temperatures up to $15,000 \mathrm{~K}$. Above $15,000 \mathrm{~K}$, the cross sections for atomic $N$ were obtained by extending Yun's calculations to $30,000 K$ using the same input data and techniques as were used in his work. The cross sections for the remaining species $N_{2}, N O, O$ and $O_{2}$ were extrapolated to roughly $30,000 \mathrm{~K}$ assuming the same temperature dependence as calculated for $N$.

For the ionized species, the calculations used effective Coulomb cross sections chosen to make the computed transport properties for a fully ionized gas agree with the correct theoretical results (ref. 38) as discussed in references 7 and 9 . The specific formulas used in the calculations are

$$
\begin{gather*}
\pi \bar{\Omega}_{e c}^{(2,2)}=1.29 Q_{c} \text { for electrons }  \tag{23a}\\
\pi \bar{\Omega}_{I l}^{(2,2)}=1.36 Z^{4} Q_{c} \text { for ions }  \tag{23b}\\
\pi \bar{\Omega}_{e e}^{(1,1)}=\pi \bar{\Omega}_{I I}^{(1,1)}=0.795 Z^{4} Q_{c} \text { for electrons and ions } \tag{23c}
\end{gather*}
$$

where $Z=1$ for singly ionized species and

$$
\begin{equation*}
Q_{c}=\frac{e^{4}}{(k T)^{2}} \ln \Lambda \tag{23d}
\end{equation*}
$$

The shielding parameter $\Lambda$ is defined as

$$
\begin{gather*}
\Lambda=\left[\frac{9(k T)^{3}}{4 \pi e^{6} n_{e}}+\frac{16(k T)^{2}}{e^{4} n_{e}^{2 / 3}}\right]^{1 / 2}  \tag{23e}\\
=\left[2.09 \times 10^{-2}\left[\frac{T^{4}}{10^{12} p_{e}}\right]+1.52\left[\frac{T^{4}}{10^{12} p_{e}}\right]^{2 / 3}\right]^{1 / 2} \tag{23f}
\end{gather*}
$$

where $T$ is the temperature in $K$ and $p_{e}=n_{e} k T$ is the electron pressure in atm . In equation (22d), $e=4.8 \times 10^{-10}$ esu is the electron charge. Equation (23) is applicable for electron pressures of the order 1 atm or below and becomes less accurate as the electron pressure increases above atmospheric (ref. 38).

In the present report, the transport properties of the ionic species are provided for a nominal electron pressure of $p_{e}=1 \mathrm{~atm}$. For any other electron pressure, it will be necessary to correct the tabulated transport properties of the ionic species according to the formula

$$
\begin{align*}
& \frac{\mu_{i}\left(p_{e}\right)}{\mu_{i}(1 \mathrm{~atm})}= \frac{K_{f, i}\left(p_{e}\right)}{K_{f, i}(1 \mathrm{~atm})}=\frac{K_{t r, i}\left(p_{e}\right)}{K_{t r, i}(1 \mathrm{~atm})}=\frac{K_{\text {int }, i}\left(p_{e}\right)}{K_{\text {int }, i}(1 \mathrm{~atm})}=\frac{\ln \Lambda(1 \mathrm{~atm})}{\ln \Lambda\left(p_{e}\right)} \\
&= \ln \left[2.09 \times 10^{-2}\left[\frac{T}{1000}\right]^{4}+1.52\left[\frac{T}{1000}\right]^{8 / 3}\right]  \tag{24a}\\
& \ln \left[2.09 \times 10^{-2}\left[\frac{T}{1000 p_{e}^{1 / 4}}\right]^{4}+1.52\left[\frac{T}{1000 p_{e}^{1 / 4}}\right]^{8 / 3}\right]
\end{align*}
$$

Similarly, the collision cross sections $\pi \bar{\Omega}_{i j}^{(l, s)}$ (for the pair of species where both are ions or electrons or a combination of the two) for any other electron pressure $p_{e}$ may be obtained from the values provided herein for $p_{e}=1 \mathrm{~atm}$ by employing the relation

$$
\begin{gather*}
\frac{\pi \bar{\Omega}_{i j}^{(l . s)}\left(p_{e}\right)}{\pi \bar{\Omega}_{i j}^{(l, s)}(1 \mathrm{~atm})}=\frac{\ln \Lambda\left(p_{e}\right)}{\ln \Lambda(1 \mathrm{~atm})} \\
=\frac{\ln \left[2.09 \times 10^{-2}\left[\frac{T}{1000 p_{e}^{1 / 4}}\right]^{4}+1.52\left[\frac{T}{1000 p_{e}^{1 / 4}}\right]^{8 / 3}\right]}{\ln \left[2.09 \times 10^{-2}\left[\frac{T}{1000}\right]^{4}+1.52\left[\frac{T}{1000}\right]^{8 / 3}\right]} \tag{24b}
\end{gather*}
$$

Equation (24b) is also applicable for $i=j$ (single species).
In calculating the contribution $K_{\text {int,i }}$ of the internal energy states to the thermal conductivity for the atomic species $N$ and $O$, the diffusion cross section $\pi \bar{\Omega}_{i i}^{(1,1)}$ in equations (18e) or ( 18 f ) has been set equal to the corresponding charge-exchange cross section for the atom and atomic ion (refs. 8 and 39). As discussed in reference 7 , this approximation allows for the effects of excitation exchange in reducing the contribution of internal energy states to the thermal conductivity in a gas of identical atoms.

The individual species viscosities and thermal conductivities computed using equations (17) and (18) have been curve fitted herein as a function of temperature by employing the following relations

$$
\begin{gather*}
\mu_{i}=e^{\left.E_{\mu_{i}} T A_{\mu_{i}}(\ln T)^{3}+B_{\mu_{i}}(\ln T)^{2}+C_{\mu_{i}} \ln T+D_{\mu_{i}}\right]}, \quad \frac{g m}{c m-\sec }  \tag{25}\\
K_{f, i}=e^{E_{\kappa_{f, i}} T^{\left[A_{\kappa_{f, i}}(\ln T)^{3}+B_{\kappa_{f, i}}(\ln T)^{2}+C_{\kappa_{f, i}} \ln T+D_{\kappa_{f, i}}\right]},} \frac{\frac{c a l}{c m-\sec -K}}{} \tag{26}
\end{gather*}
$$

The curve-fit coefficients appearing in equations (25) and (26) are given in tables IV and $V$ for the 11 chemical species. These coefficients yield values of the viscosity and frozen thermal conductivity of ionic species at a nominal electron pressure of 1 atm and should be corrected for any other electron pressure (or number density) by using equation (24a).

Figure 4 displays typical results from the viscosity curve fit (eq. (25)) of equation (17) for some of the neutral and charged species. The frozen thermal conductivity curve fit (eq. (26)) of equations (19) through (21) is shown in figure 5 for the same species. It may be noticed from these figures (and in tables IV and V) that a higher order curve is needed for the charged species because of the inflection of the viscosity
and thermal conductivity curves at low temperatures. Higher order curve fits are also needed for the thermal conductivity of the neutral molecular species.

## Transport Properties of Multicomponent Mixtures

Rigorous kinetic theory formulas which have been derived directly from a solution of the Boltzmann equation using the classical Chapman-Enskog procedure (refs. 33 and 40) are available for obtaining the transport properties of a gas mixture from the molecular constituent species. In the first Chapman-Enskog approximation, formulas for both the viscosity and translational component of thermal conductivity, $K_{t r, i}$, of a gas mixtures are of the general form

$$
\left[\mu^{(1)} \text { or } K_{t r}^{(1)}\right]_{\text {mixture }}=-\frac{\left[\begin{array}{ccccccc}
A_{11} & \cdot & \cdot & \cdot & A_{1 v} & 1 & x_{1}  \tag{27}\\
\cdot & & & \cdot & 1 & \cdot \\
\cdot & & & \cdot & 1 & \cdot \\
\cdot & & & \cdot & 1 & \cdot \\
A_{v 1} & \cdot & \cdot & \cdot & A_{v v} & \mid & x_{v} \\
- & - & - & - & - & - & - \\
x_{1} & \cdot & \cdot & \cdot & x_{v} & 1 & 0
\end{array}\right]}{\left|A_{i j}\right|}
$$

where $x_{i}$ is the mole fraction of the $i$ th species, $v(\equiv N S)$ is the total number of species present in the mixture, and the matrix elements $A_{i j}$ can be expressed in the form

$$
\begin{equation*}
A_{i j}=A_{j i}=-x_{i} x_{j} a_{i j}+\delta_{i j}\left(x_{i} A_{i}+\sum_{l=1}^{v} x_{i} x_{l} a_{i l}\right) \tag{28}
\end{equation*}
$$

where $a_{i j}=a_{j i}$ and $\delta_{i j}$ is the Kronecker delta. Elements $A_{i}$ and $a_{i j}$ are defined subsequently. The superscript 1 on $\mu$ or $K_{\text {tr }}$ indicates that equation (27) is the first Chapman-Enskog approximation for the transport property. Further details for obtaining the transport properties by employing the first Chapman-Enskog approximation are given in reference 35 . In principle, the problem of calculating the transport coefficients for a given mixture consists of two parts: first, the determination of the collision cross sections $\pi \bar{\Omega}_{i j}$ for all possible pairs of species ( $i, j$ ); and second, the evaluation of the Chapman-Enskog formulas. The amount of computation required to evaluate the mixture transport properties is greatly reduced if approximations to the complete Chapman-Enskog formulas are employed. Reference 7 has provided approximate formulas for the transport properties based on the relations developed in references 41,42 , and 43. Earlier, references 10,11 , and 44, and more recently, references 12 and 45 have also provided approximations to the Chapman-Enskog formulas. These are apparently the most satisfactory of the many simplifying approximations for the mixture viscosity and thermal conductivity which have been suggested by various authors. However, effects of the elements $A_{i j}$ in the Chapman-Enskog formula are completely neglected in Brokaw's approximation (ref. 42) so that this approximation always gives too large a value for the transport properties. In the Buddenberg-Wilke (refs. 10 and 44) and Mason-Saxena (ref. 11) formulas, the effects of these elements are accounted for by means of a single empirical constant which is assumed to be the
same for all gas mixtures. The approximation used by Peng and Pindroh (ref. 41) represents an attempt to take account of the nondiagonal elements explicitly to first order at the expense of a somewhat increased calculational effort. Armaly and Sutton (refs. 12 and 45) neglected the nondiagonal matrix elements $A_{i j}$ in a manner similar to Brokaw (ref. 42). However, they did not force the value of $A_{i j}$, defined as

$$
\begin{equation*}
A_{i j}^{*}=\frac{\bar{\Omega}_{i j}^{(2,2)}}{\bar{\Omega}_{i j}^{(1,1)}} \tag{29}
\end{equation*}
$$

to be equal to $5 / 3$ and $5 / 2$ in their approximations for viscosity and thermal conductivity, respectively. $\dagger$ They assigned different values to $A_{i j}^{*}$ for ion-atom and neutral atom-molecule interactions. From the computer time, storage, and simplicity point of view, references 10 and 11 would appear to be adequate for non-ionized gas mixtures, whereas references 12 and 45 would be useful for computing the viscosity and translational component of thermal conductivity for an ionized gas mixture.

In all the approximations to the Chapman-Enskog formulas for viscosity and translational thermal conductivity discussed thus far, the transfer of momentum or energy from one species to another by collisions has been either neglected or has been accounted for by an empirical constant. This transfer process, which is represented by the nondiagonal elements $A_{i j}$ in the Chapman-Enskog formula (eq. (27)), has the effect of making the less conductive species in the mixture carry a larger fraction of the transport. This process, therefore, reduces the overall conductivity of the mixture below the value which it would have if the transfer process were neglected.

In reference 35 , Yos obtained approximations to the Chapman-Enskog formulas which account for the effects of the above mentioned transfer process between different species. These cross sections reproduce the results of the first ChapmanEnskog formula (eqs. (27) and (28)) to within a fraction of a percent for all cases considered in reference 35 and are also simpler to use than the latter. Based on the cross sections developed by Yos (ref. 35), the following formulas may be used to compute viscosity and the translational component of thermal conductivity

$$
\begin{equation*}
\left[\mu^{(1)} \text { or } K_{t r}^{(1)}\right]=\frac{\sum_{i=1}^{N S} x_{i} /\left(A_{i}+a_{a v}\right)}{1-a_{a v} \sum_{i=1}^{N S} x_{i} /\left(A_{i}+a_{a v}\right)} \tag{30}
\end{equation*}
$$

Here, $N S$ is the number of species in the gas, $x_{i}$ is the mole fraction of the $i$ th species, and $a_{a v}$ is an average value of the nondiagonal matrix elements $a_{i j}$ contained in equation (28) which is defined as

$$
\begin{equation*}
a_{a v}=\frac{\sum_{i, j=1}^{N S} x_{i} x_{j}\left(\frac{1}{A_{i}}-\frac{1}{A_{j}}\right)^{2} a_{i j}}{\sum_{i, j=1}^{N S} x_{i} x_{j}\left(\frac{1}{A_{i}}-\frac{1}{A_{j}}\right)^{2}} \tag{31a}
\end{equation*}
$$

with

[^2]\[

$$
\begin{equation*}
A_{i}=\sum_{l=1}^{N S} x_{l} A_{i l} \tag{31b}
\end{equation*}
$$

\]

For the viscosity, the quantities $a_{i j}$ and $A_{i j}$ appearing in equations (31a) and (31b) are defined as

$$
\begin{gather*}
a_{i j}=\frac{N_{A}}{\left(M_{i}+M_{j}\right)}\left[2 \Delta_{i j}^{(1)}-\Delta_{i j}^{(2)}\right]  \tag{32a}\\
A_{i l}=\frac{N_{A}}{M_{i}} \Delta_{i l}^{(2)} \tag{32b}
\end{gather*}
$$

For translational thermal conductivity, the above quantities are defined as

$$
\begin{equation*}
a_{i j}=\left[\frac{2}{15 k}\right] \frac{M_{i} M_{j}}{\left(M_{i}+M_{j}\right)^{2}}\left[\left(\frac{33}{2}-\frac{18}{5} B_{i j}^{*}\right] \Delta_{i j}^{(1)}-4 \Delta_{i j}^{(2)}\right] \tag{33a}
\end{equation*}
$$

and
$A_{i l}=\frac{2}{15 k\left(M_{i}+M_{l}\right)^{2}}\left\{8 M_{i} M_{l} \Delta_{i l}^{(2)}+\left(M_{i}-M_{i}\right)\left[9 M_{i}-\frac{15}{2} M_{l}+\frac{18}{5} B_{i l}^{*} M_{l}\right] \Delta_{i l}^{(1)}\right\}$
In these equations, $M_{i}$ is the molecular weight of the $i$ th species, $N_{A}=6.0225 \times 10^{23}$ molecules/gm-mole is Avogadro's number, and $k=1.3805 \times 10^{-16} \mathrm{erg} / \mathrm{K}$ is Boltzman's constant. The remaining quantities are defined as

$$
\begin{gather*}
\Delta_{i j}^{(1)}=\frac{8}{3}\left[\frac{2 M_{i} M_{j}}{\pi N_{A} k T\left(M_{i}+M_{j}\right)}\right]^{1 / 2} \pi \bar{\Omega}_{i j}^{(1,1)}  \tag{34}\\
\Delta_{i j}^{(2)}=\frac{16}{5}\left[\frac{2 M_{i} M_{j}}{\pi N_{A} k T\left(M_{i}+M_{j}\right)}\right]^{1 / 2} \pi \bar{\Omega}_{i j}^{(2,2)}  \tag{35}\\
B_{i j}^{*}=\frac{5 \bar{\Omega}_{i j}^{(1,2)}-4 \bar{\Omega}_{i j}^{(i, 3)}}{\bar{\Omega}_{i j}^{(1,1)}} \tag{36}
\end{gather*}
$$

and the collision integrals $\pi \bar{\Omega}_{i j}^{(1, s)}$ are weighted averages of the cross sections defined through equation (22).

The frozen thermal conductivity $K_{f}$ employed in defining the frozen Prandtl and Lewis numbers $\dagger$ can be obtained from the modified Eucken approxim ation (ref. 43)

$$
\begin{equation*}
K_{f}=K_{t r}+K_{i n t} \tag{37}
\end{equation*}
$$

where $K_{t r}$ is the translational component of the thermal conductivity given by equations (30) to (36) and $K_{i n t}$ is the component of thermal conductivity resulting from the internal excitation energy of the molecules, defined (ref. 7) as

$$
\begin{equation*}
K_{\text {int }}=k \sum_{i=1}^{N S}\left[\frac{\left[\frac{M_{i} C_{p, i}}{k N_{A}}-\frac{5}{2}\right] x_{i}}{\left(\sum_{j=1}^{N S} x_{j} \Delta_{i j}^{(1)}\right]}\right] \tag{38}
\end{equation*}
$$

[^3]Here, $C_{p, i}$ is the specific heat at constant pressure of the $i$ th species.
The binary diffusion coefficient $D_{i j}$ needed to obtain the binary and multicomponent Lewis numbers (refs. 13, 14, and 34) is obtained from the complete first Chapman-Enskog approximation (ref. 34):

$$
\begin{equation*}
D_{i j}=\frac{\bar{D}_{i j}}{p}=\frac{k T}{p \Delta_{i j}^{(1)}}, \quad \mathrm{cm}^{2} / \mathrm{sec} \tag{39a}
\end{equation*}
$$

with

$$
\begin{equation*}
\bar{D}_{i j}=\frac{k T}{\Delta_{i j}^{(1)}}, \quad \mathrm{cm}^{2}-\mathrm{atm} / \mathrm{sec} \tag{39b}
\end{equation*}
$$

Here $p$ is the pressure in atmospheres. Equation (39b) for $\bar{D}_{i j}$ has been curve fitted in the present work by using the expression

$$
\begin{equation*}
\bar{D}_{i j}=e^{D_{\bar{D}_{i j}} T^{\left[A_{\bar{D}_{i j}}(\ln T)^{2}+B_{\bar{D}_{i j}} \ln T+C_{\bar{D}_{i j}}\right]}, \quad \mathrm{cm}^{2}-\mathrm{atm} / \mathrm{sec} .} \tag{40a}
\end{equation*}
$$

where $T$ is the temperature in $K$. The curve-fit coefficients of equation (40a) are given in table VI for the different interactions occurring in the 11 -species air model.

The values of $\bar{D}_{i j}$ obtained from equation (40a) with the curve-fit coefficients given in table VI are for a nominal electron pressure of 1 atm . If the pair of interacting species are both ions, both electrons, or any combination of the two, then $\bar{D}_{i j}$ may be corrected for any other electron pressure by employing:

$$
\begin{equation*}
\bar{D}_{i j}\left(P_{e}\right)=\bar{D}_{i j}(1 \mathrm{~atm}) \frac{\ln \left[2.09 \times 10^{-2}\left[\frac{T}{1000}\right]^{4}+1.52\left[\frac{T}{1000}\right)^{8 / 3}\right]}{\ln \left[2.09 \times 10^{-2}\left[\frac{T}{1000 p_{e}}\right]^{4}+1.52\left[\frac{T}{1000 p_{e}}\right]^{8 / 3}\right]} \tag{40b}
\end{equation*}
$$

If the approximations of references 41 through 43 are employed in place of the more exact formulas given by equations (30) through (36) $\dagger$, then the following approximate formulas for the mixture viscosity and thermal conductivity may be used (ref. 7):

$$
\begin{gather*}
\mu_{\text {mixture }}^{(1)}=\sum_{i=1}^{N S}\left[\frac{\frac{M_{i}}{N_{A}} x_{i}}{\sum_{j=1}^{N S} x_{j} \Delta_{i j}^{(2)}}\right]  \tag{41}\\
{\left[K_{i r}^{(1)}\right]_{\text {mixure }}=\frac{15}{4} k \sum_{i=1}^{N S}\left[\frac{x_{i}}{\sum_{j=1}^{N S} \alpha_{i j} x_{j} \Delta_{i j}^{(2)}}\right]} \tag{42a}
\end{gather*}
$$

where $\Delta_{i j}^{(2)}$ is given by equation (35) and $\alpha_{i j}$ is defined as

$$
\begin{equation*}
\alpha_{i j}=1+\frac{\left[1-\left(M_{i} / M_{j}\right)\right]\left[0.45-2.54\left(M_{i} / M_{j}\right)\right]}{\left[1+\left(M_{i} / M_{j}\right)\right]^{2}} \tag{42b}
\end{equation*}
$$

[^4]To obtain the viscosity $\mu$ and the translational component of thermal conductivity $K_{t r}$ of a gas mixture from either the more exact equations (30) through (36) or from the approximate relations in equations (41) through (42), the binary collision cross sections $\pi \bar{\Omega}_{i j}^{(1, s)}$ and their ratios are needed in equations (34) through (36). These cross sections, defined by equation (22), are the same as those used by Yos (refs. 7,8, and 9). In addition to the formulas given by equation (23) for the Coulomb collision integrals, the following relations are also employed:

$$
\begin{gather*}
\pi \bar{\Omega}_{e l}^{(1,1)}=0.795 Z^{4} Q_{c}  \tag{43a}\\
\pi \bar{\Omega}_{e l}^{(2,2)}=1.29 Q_{c} \tag{43b}
\end{gather*}
$$

where the subscripts $e$ and $I$ represent electrons and ions, respectively, and $Z$ and $Q_{c}$ are defined in equation (23d).

The NATA code (refs. 30,31, and 32) employed to obtain the collision cross sections, $\pi \bar{\Omega}_{i j}^{(l, s)}$, contains default provisions for estimating some cross sections if they are not specified explicitly in the built-in database or the input. The defaults are summarized as
(i) If both species are ions, then the Coulomb cross sections given by equations (23) and (43) are used.
(ii) If one species is neutral and the other ionized, then the formula

$$
\begin{equation*}
\pi \bar{\Omega}_{i j}^{(l, s)}=A^{(l, s)} T^{-0.4} \tag{44a}
\end{equation*}
$$

is employed with the constants $A^{(1, s)}$ defined in the code.
(iii) If both species are neutral and are unlike, then the cross sections are estimated using the simple mixing rule

$$
\begin{equation*}
\pi \bar{\Omega}_{i j}^{(l, s)}=\frac{1}{4}\left(\sqrt{\pi \bar{\Omega}_{i j}^{(l, s)}}+\sqrt{\pi \bar{\Omega}_{i j}^{(1, s)}}\right)^{2} \tag{44b}
\end{equation*}
$$

The built-in data in NATA specify steps for calculating the cross sections for the like-like interactions of ten species ( $e^{-}, \mathrm{N}_{2}, \mathrm{O}_{2}, \mathrm{~N}, \mathrm{O}, \mathrm{NO}, \mathrm{NO}^{+}, \mathrm{N}^{+}, \mathrm{O}^{+}$, and $\mathrm{N}_{2}^{+}$) and for those unlike interactions for which experimental or theoretical cross sections are available in the literature. The cross sections for $O_{2}^{+}$are taken to be the same as those for $N_{2}^{+}$in these calculations. NATA contains twelve methods or options for calculating $\pi \bar{\Omega}_{i j}^{(1,1)}, \pi \bar{\Omega}_{i j}^{(2,2)}$, and $B_{i j}^{*}$ which are described in detail in references 30 through 32. Note that the accuracy of the calculated transport properties is largely determined by the accuracy of the input data for the cross-section integrals. A brief discussion of the values employed in the present study is given in reference 7. Reference 46 provides a comparison between theory and experiment for the thermal conductivity of nitrogen up to temperatures of 14000 K . Fairly good agreement between the two is shown there.

Figures 6 and 7 give viscosity and frozen thermal conductivity values, respectively, obtained for equilibrium air at 1 atm by employing the presently computed collision cross sections for the constituent species. The present calculations employ equation (41) for the calculation of mixture viscosity and equations (37), (38), and (42) for the mixture frozen thermal conductivity. In addition, the collision cross sections used are nearly identical to those obtained in reference 9. The mixing laws employed for the viscosity and thermal conductivity shown in figures 6 and 7 are accurate for sub-ionization temperatures (less than 9000 K at 1 atm ) only. For ionized flows, more accurate mixing laws of the type given by equation (30) should be employed. Figures

6 and 7 also include viscosity and thermal conductivity values from other researchers for comparison. In these figures, the predictions of Peng and Pindroh (ref. 41) and Esch et al. (ref. 47) are based on the Buddenberg-Wilke (ref. 44) type of mixture law and have the same level of approximation as the present calculations. The mixture laws employed by Hansen (ref. 29) contain a somewhat lower level of approximation. In Hansen's work, the viscosity is computed by using the simple summation formula for a mixture of hard sphere molecules, whereas a linearized expression with Eucken's assumption (ref. 34) is employed for the frozen thermal conductivity. The viscosity values obtained in the present work are in good agreement (fig. 6) with the values obtained by Peng and Pindroh (ref. 41) and Esch et al. (ref. 47), presumably due to the similar mixing laws employed. Hansen's (ref. 29) predictions are lower, especially at higher temperatures. Even with the beginning of dissociation of molecular nitrogen at about 4000 K (when the dissociation of molecular oxygen is almost complete), Hansen's values of viscosity are not much different from the Sutherland's law. For the frozen thermal conductivity (fig. 7), the present values are in agreement with those obtained by Peng and Pindroh (ref. 41) up to temperatures of about 9000 K . The values obtained by Esch et al. (ref. 47) deviate from the present values beyond 6000 K . This may be due to the constant cross-sectional values employed for the ionized species in the 8000 to 15000 K temperature range in reference 47. Hansen's predictions of thermal conductivity are lower than the other data and are closer to the Sutherland values up to temperatures of about 4000 K . Again, the differences between the present computations and those of Hansen are presumably due to the somewhat more rigorous mixing laws employed herein.

There are 121 possible binary interactions for the dissociating air having eleven species. Therefore, 121 values of each of the collision cross sections $\pi \bar{\Omega}_{i j}^{(1,1)}, \pi \bar{\Omega}_{i j}^{(2,2)}$ and the collision cross-section ratio $B_{i j}^{*}$ are required to evaluate the transport properties. By use of the symmetrical equality, i.e. $(i, j)=(j, i)$, only 66 values of each cross section and cross-section ratio are required. These values have been curve fit in the present study as a function of temperature for a nominal electron pressure of 1 atm using the following relations

$$
\begin{align*}
& \pi \bar{\Omega}_{i j}^{(1,1)}=e^{D_{\bar{\Omega}_{i j}^{(1,1)}}} T^{\left[A_{\bar{\Omega}_{i j}^{(1,1)}}(\ln T)^{2}+B_{\bar{\Omega}_{(i j)}} \ln T+C_{\bar{\Omega}_{i j}^{(1,1)}}\right]}, \quad \AA^{2}  \tag{45}\\
& \pi \bar{\Omega}_{i j}^{(2,2)}=e^{D_{\bar{\Omega}}(2,2)} T^{\left[A_{\bar{\Omega}\left({ }_{i j}\right)}(\ln T)^{2}+B_{\overline{\Omega_{i j}}(2,2)} \ln T+C_{\bar{\Omega}(i j}\right]}, \quad \AA^{2}  \tag{46}\\
& B_{i j}^{*}=e^{\left.D_{B_{i j}} T A_{B_{i j}}(\ln T)^{2}+B_{B_{i j}}+C_{B_{i j}}\right]} \tag{47}
\end{align*}
$$

For electron pressures different from unity, the formula given by equation (24b) is used to correct the cross sections for the ionic species. No such correction is required for the cross-section-ratio parameter $B_{i j}^{*}$.

Curve-fit coefficients appearing in equations (45) through (47) are given in Table VII through IX for the various interactions in an 11 -species air model. Figure 8 illustrates some typical curve fits obtained by employing equation (40a) and equations (45) through (47) with the associated constants. The figure compares the computed values of binary diffusion coefficient, collision integrals, and collision integral ratio with the resulting curve fit for different interaction pairs of neutral and ionized species, including electrons. The collision integral ratio, $B_{i j}^{*}$, is almost constant with temperature as shown in the figure and was fitted with the lower order curve fit where possible. However, the collision integrals $\pi \bar{\Omega}_{i j}^{(l, s)}$ for the charged species pairs exhibit more complex
behavior and require higher order curve fits.
The transport properties of a multi-temperature gas mixture may be obtained by following the approaches of references 20 and 48. These references have used equations (41) and (42) for the calculation of mixture viscosity and translational thermal conductivity. The collision integrals for heavy particles in these equations are evaluated by using the heavy particle translational temperature, whereas those for electrons with any other partner are obtained by using the electron temperature. With these modifications, equations (41) and (42) can be written for an 11 -species gas mixture as

$$
\begin{align*}
& \mu_{\text {mixure }}=\sum_{i=1}^{10}\left[\frac{\frac{M_{i}}{N_{A}} x_{i}}{\sum_{j=1}^{10} x_{j} \Delta_{i j}^{(2)}(T)+x_{e} \Delta_{i e}^{(2)}\left(T_{e}\right)}\right]+\frac{\frac{M_{e}}{N_{A}} x_{e}}{\sum_{j=1}^{11} x_{j} \Delta_{e j}^{(2)}\left(T_{e}\right)}  \tag{48}\\
& \left(K_{t r}^{*}\right)_{\text {mixture }}=\frac{15}{4} k \sum_{i=1}^{10}\left[\frac{x_{i}}{\sum_{j=1}^{10} \alpha_{i j} x_{j} \Delta_{i j}^{(2)}(T)+3.54 x_{e} \Delta_{i e}^{(2)}\left(T_{e}\right)}\right] \tag{49}
\end{align*}
$$

where $\alpha_{i j}$ is still obtained from equation (42b). Note that the above definition of $K_{t r}^{*}$ does not include contributions due to electron-heavy particle and electron-electron collisions. These contributions, defined by $K_{e}$, are given later. The approach outlined here may also be used to obtain the mixture viscosity and thermal conductivity from the more exact expressions in equations (30) through (36). Equation (38) for the internal thermal conductivity needs to be modified for the multi-temperature formulation. The contributions resulting from the excitation of different internal energy modes can not be lumped together into a single term $K_{\text {int }}$ for such a formulation. Further, equation (37) no longer can be used to obtain a frozen thermal conductivity for the mixture. The relation given in equation (37) may be used to obtain a frozen thermal conductivity with only the rotational mode contributing to the internal energy at the translational temperature. In general, there are four components of the internal thermal conductivity, similar to the molecular specific heat (fig. 2). Using these components, the $k$ th component of the overall heat flux vector can be expressed as

$$
\begin{equation*}
q^{k}=-\left(K_{i r}^{*}+K_{r o l}\right) \frac{\partial T}{\partial x^{k}}-K_{v i b} \frac{\partial T_{v}}{\partial x^{k}}-K_{e l} \frac{\partial T_{e l}}{\partial x^{k}}-K_{e} \frac{\partial T_{e}}{\partial x^{k}}+\sum_{i=1}^{N S} \rho_{i} h_{i} V_{i}^{k} \tag{50a}
\end{equation*}
$$

where $K_{t r}^{*}$ is the translational thermal conductivity defined previously by equation (49) and $K_{r o l}, K_{v i b}$ and $K_{e l}$ are the rotational, vibrational, and electronic thermal conductivities, respectively, associated with these internal energy modes (ref. 49). Also, $K_{e}$ is the thermal conductivity of electrons, $T$ is the translational-rotational temperature, $T_{v}$ is the vibrational temperature, $T_{e l}$ is the electronic excitation temperature, $T_{e}$ is the electron temperature, $x^{k}$ is the $k$ th component in a general orthogonal coordinate system, and the last term is the diffusive component of the heat flux vector. Further details of the heat flux vector $q^{k}$ and other definitions are given in appendix A. Two other heat flux vectors are required in describing the conservation equations for the electron energy and the vibrational energy (ref. 48). The electron heat-flux vector $q_{e}^{k}$ and the vibrational heat-flux vector $q_{v}^{k}$ are defined in appendix $C$. The thermal conductivities required to evaluate these flux vectors are obtained from the electronelectron and molecule-molecule collisions. These thermal conductivities are also
defined in appendix $C$. In the diffusive heat flux component, $\rho_{i}, h_{i}$, and $V_{i}^{k}$ are the density, enthalpy and diffusion velocity of species $i$, respectively. For a twotemperature model, equation (50a) may be written (refs. 19 and 20) as

$$
\begin{equation*}
q^{k}=-\left(K_{i r}^{*}+K_{r o t}\right) \frac{\partial T}{\partial x^{k}}-\left(K_{v i b}+K_{e l}+K_{e}\right) \frac{\partial T_{v e}}{\partial x^{k}}+\sum_{i=1}^{N S} \rho_{i} h_{i} V_{i}^{k} \tag{50b}
\end{equation*}
$$

Different components of the internal thermal conductivity appearing in equation (50) can be evaluated from equation (38) by appropriate modifications for these components. For example, $K_{\text {rot }}$ can be obtained from

$$
\begin{equation*}
\left(K_{\text {rot }}\right)_{\substack{\text { Parcial } \\ \text { Excitaion }}}=k \sum_{i=1}^{N S}\left[\frac{\left[\frac{M_{i}}{N_{A}} \frac{C_{p, i}\left(T_{\text {rot }}\right)}{k}-\frac{5}{2}\right] x_{i}}{\sum_{j=1}^{N S} x_{j} \Delta_{i j}^{(1)}\left(T_{\text {rot }}\right)}\right] \tag{51a}
\end{equation*}
$$

for partial excitation of the rotational internal energy mode if the temperature is less than that needed to excite the vibrational energy mode (fig. 2). Values of specific heat at constant pressure, $C_{p, i}$, appearing in equation (51a) can be obtained from the curve-fit relation of equation (13) by employing the rotational temperature, $T_{\text {rot }}$, if different from the translational temperature $T$. When the vibrational mode begins to excite, the rotational mode is fully excited and equation (51a) becomes

$$
\begin{equation*}
\left(K_{\text {rot }}\right)_{\text {Exciutation }}^{\text {Fult }}=k \sum_{i=1}^{N S}\left[\frac{x_{i}}{\sum_{j=1}^{N S} x_{j} \Delta_{i j}^{(1)}\left(T_{r o t}\right)}\right] \tag{51b}
\end{equation*}
$$

Similarly, expressions for $K_{\text {vib }}$ with partial and full excitations of the vibrational energy mode may be written as

$$
\begin{equation*}
\left(K_{\text {vib }}\right)_{\text {Exariation }}^{\text {Pxion }}=k \sum_{i=1}^{N S}\left[\frac{\left[\frac{M_{i}}{N_{A}} \frac{C_{p, i}\left(T_{v i b}\right)}{k}-\frac{7}{2}\right] x_{i}}{\sum_{j=1}^{N S} x_{j} \Delta_{i j}^{(1)}\left(T_{v i b}\right)}\right] \tag{52a}
\end{equation*}
$$

and

$$
\begin{equation*}
\left(K_{v i b}\right)_{\text {Excuation }}^{\text {Full }}=k \sum_{i=1}^{N S}\left[\frac{x_{i}}{\sum_{j=1}^{N S} x_{j} \Delta_{i j}^{(1)}\left(T_{v i b}\right)}\right] \tag{52b}
\end{equation*}
$$

Once again, the value of $C_{p, i}$ appearing in equation (52a) can be obtained from the curve-fit relation of equation (13) by employing $T_{\text {vib }}$. Also, the vibrational energy mode is fully excited when the electronic contribution becomes significant (as shown in fig. 2 for the specific heat at constant pressure).

The rotational and vibrational energy modes are almost fully excited at their respective characteristic temperatures. Therefore, for rotational and vibrational temperatures greater than these characteristic temperatures, equations (51b) and (52b) can be employed to obtain $K_{\text {rot }}$ and $K_{\text {vib }}$, respectively.

Expressions for $K_{e l}$ with the excitation of electronic energy mode can be written as

$$
\begin{equation*}
K_{e l}=k \sum_{i=1}^{N S}\left[\frac{\left[\frac{M_{i}}{N_{A}} \frac{C_{p, i}\left(T_{e l}\right)}{k}-\frac{9}{2}\right] x_{i}}{\sum_{j=1}^{N S} x_{j} \Delta_{i j}^{(1)}\left(T_{e l}\right)}\right] \tag{53}
\end{equation*}
$$

In equation (53), higher electronic degeneracy levels begin to contribute to $K_{e l}$ (and $C_{p, i}$, etc.) as the characteristic temperatures for the electronic excitation of those degeneracy levels are reached.

Finally, the thermal conductivity for free electrons, $K_{e}$, appearing in equation (50) may be obtained from the modified form of equation (42)

$$
\begin{equation*}
K_{e}=\frac{15}{4} \frac{k x_{e}}{\sum_{j=1}^{N S} 1.45 x_{j} \Delta_{e j}^{(2)}\left(T_{e}\right)} \tag{54}
\end{equation*}
$$

This thermal conductivity results from the collisions between electrons and other species, including other electrons.

## Concluding Remarks

The present work provides the reaction rate coefficients and thermodynamic and transport properties for an 11 -species air model which are needed in an alyzing the high energy flow environment of currently proposed and future hypersonic vehicles. Approximate and more exact formulas have been provided for computing the properties of partially ionized gas mixtures in chemical and thermal nonequilibrium around such vehicles.

The work presented here uses the best estimates of available data needed to compute properties of the 11 -species air model. However, there is need for improved data, especially for air in thermochemical nonequilibrium. There is also some degree of uncertainty about reaction rate coefficients at high temperatures. Both the theoretical and experimental bases of the multi-temperature kinetic models need to be strengthened. The virial coefficient approach as compared to the partition function analysis for obtaining the thermodynamic properties at higher temperatures appears sufficient but needs further verification. For transport properties, the input data for obtaining the collision cross sections at high temperatures are not adequate.

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## Appendix A

## Heat Flux, Frozen and Reactive Prandtl and Lewis Numbers, and Associated Definitions

The $k$ th component of overall heat flux vector $q^{k}$ for the dissociating and ionizing 11-species air model in a multi-temperature formulation can be expressed as $\dagger$

$$
\begin{equation*}
q^{k}=-\left(K_{i r}^{*}+K_{r o t}\right) \frac{\partial T}{\partial x^{k}}-K_{v i b} \frac{\partial T_{v}}{\partial x^{k}}-K_{e l} \frac{\partial T_{e l}}{\partial x^{k}}-K_{e} \frac{\partial T_{e}}{\partial x^{k}}+\sum_{i=1}^{n 1} \rho_{i} h_{i} V_{i}^{k} \tag{A1}
\end{equation*}
$$

where the various symbols are explained in the main text after equation (50a). For thermal equilibrium conditions, equation (A1) may be written as

$$
\begin{equation*}
q^{k}=-\left(K_{i r}^{*}+K_{r o l}+K_{v i b}+K_{a l}+K_{a}\right) \frac{\partial T}{\partial x^{k}}+\sum_{i=1}^{11} \rho_{i} h_{i} V_{i}^{k} \tag{A2}
\end{equation*}
$$

or,

$$
\begin{equation*}
q^{k}=-K_{f} \frac{\partial T}{\partial x^{k}}+\sum_{i=1}^{11} \rho_{i} h_{i} V_{i}^{k} \tag{A3}
\end{equation*}
$$

with

$$
\begin{equation*}
K_{f}=\left(K_{i r}^{*}+K_{e}\right)+K_{i n t} \tag{A4}
\end{equation*}
$$

and

$$
\begin{equation*}
K_{i n t}=K_{r o t}+K_{v i b}+K_{a l} \tag{A5}
\end{equation*}
$$

It may also be noted that under thermal equilibrium conditions

$$
\begin{equation*}
K_{t r}=K_{t r}^{*}+K_{s} \tag{A6}
\end{equation*}
$$

where $K_{t r}$ is given by equation (42), $K_{\text {tr }}^{*}$ is obtained from equation (49) and $K_{\text {e }}$ is evaluated from equation (54). The last term in equations (A1), (A2) and (A3) represents the diffusion contribution to the heat flux vector. The diffusion mass flux of species $i, J_{i}^{k}$, is related to the diffusion velocity $V_{i}^{k}$ through the relation

$$
\begin{equation*}
J_{i}^{k}=\rho_{i} V_{i}^{k} \tag{A7}
\end{equation*}
$$

and for the case of binary diffusion may be expressed as (ref. 50)

$$
\begin{equation*}
J_{i}^{k}=-\rho D_{i j} \frac{\partial C_{i}}{\partial x^{k}} \tag{A8}
\end{equation*}
$$

when the species $i$ diffuses into any other species $j$. Here, $C_{i}$ is the mass fraction of species $i$ and $D_{i j}$ is the binary diffusion coefficient. Using relation (A7) and (A8), equation (A3) can be written as

$$
\begin{equation*}
q^{k}=-K_{f} \frac{\partial T}{\partial x^{k}}-\rho \sum_{i=1}^{11} D_{i j} h_{i} \frac{\partial C_{i}}{\partial x^{k}} \tag{A9}
\end{equation*}
$$

or,

$$
\begin{equation*}
q^{k}=-K_{f} \frac{\partial T}{\partial x^{k}}-\left[\rho \sum_{i=1}^{11} D_{i j} h_{i} \frac{\partial C_{i}}{\partial T}\right) \frac{\partial T}{\partial x^{k}} \tag{A10}
\end{equation*}
$$

[^5]or,
\[

$$
\begin{equation*}
q^{k}=-K \frac{\partial T}{\partial x^{k}} \tag{A11}
\end{equation*}
$$

\]

where $K$ is the total effective thermal conductivity defined as

$$
\begin{equation*}
K=K_{f}+\rho \sum_{i=1}^{11} D_{i j} h_{i} \frac{\partial C_{i}}{\partial T} \tag{A12}
\end{equation*}
$$

or,

$$
\begin{equation*}
K=K_{f}+K_{d} \tag{A13}
\end{equation*}
$$

with the diffusion contribution to the thermal conductivity, $K_{d}$, defined as

$$
\begin{equation*}
K_{d}=\rho \sum_{i=1}^{11} D_{i j} h_{i} \frac{\partial C_{i}}{\partial T} \tag{A14}
\end{equation*}
$$

An alternate definition of the total thermal conductivity, $K$, is given in reference 7 as

$$
\begin{equation*}
K=K_{f}+K_{r} \tag{A15}
\end{equation*}
$$

where $K_{r}$ is the reaction thermal conductivity $\dagger$ defined as

$$
\begin{equation*}
K_{r}=k \sum_{l=1}^{N I R}\left[\frac{\left(\Delta h_{l} / R_{\text {univ}} T\right)^{2}}{\sum_{i=1}^{N S}\left[\left(\beta_{i, l}-\alpha_{i, l}\right) / x_{i}\right] \sum_{j=1}^{N S}\left[\left(\beta_{i, l}-\alpha_{i, l}\right) x_{j}-\left(\beta_{j, l}-\alpha_{j, l}\right) x_{i}\right] \Delta_{i j}^{(1)}}\right] \tag{A16}
\end{equation*}
$$

where $k$ is the Boltzmann constant, NIR is the total number of independent reactions in the system, NS is the total number of species in the system, $\Delta h_{l}=\sum_{i=1}^{N S}\left(\beta_{i, l}-\alpha_{i, l}\right) h_{i}$ is the heat of reaction per $g m$-mole for the $l$ th reaction, $x_{i}$ is the mole fraction of species $i, \Delta_{i j}^{(1)}$ is defined through equation (34), and $\alpha_{i, l}$ and $\beta_{i, l}$ are the stoichiometric coefficients for reactants and products in the reaction given by equation (1). The thermal conductivities $K_{d}$ given by equation (A14) and $K_{r}$, given by equation (A16) are equivalent.

Similar to relations (A12) and (A13), the total specific heat at constant pressure may be defined as

$$
\begin{equation*}
C_{p}=\left[\frac{\partial h}{\partial T}\right]_{p} \tag{A17}
\end{equation*}
$$

or, from equation (9),

$$
\begin{equation*}
C_{p}=C_{p_{f}}+\left[\sum_{i=1}^{11} h_{i} \frac{\partial C_{i}}{\partial T}\right]_{p} \tag{A18}
\end{equation*}
$$

or,

$$
\begin{equation*}
C_{p}=C_{p_{f}}+C_{P_{d}} \tag{A19}
\end{equation*}
$$

with

$$
\begin{equation*}
C_{P_{d}}=\left[\sum_{i=1}^{11} h_{i} \frac{\partial C_{i}}{\partial T}\right]_{p} \tag{A20}
\end{equation*}
$$

[^6]where $C_{p_{d}}$ is the diffusion contribution to the specific heat at constant pressure.
Using the various definitions for the thermal conductivity and the specific heats at constant pressure, the frozen and reactive Prandtl and Lewis numbers usually employed in dimensionless heat flux calculations may now be defined. $\dagger$

Generally, the frozen values of specific heat at constant pressure and thermal conductivities are employed in flowfield calculations. Associated heat flux from these calculations is, accordingly, expressed in terms of the frozen Prandtl and Lewis numbers. Alternately, one may also use total values of specific heat at constant pressure and thermal conductivity in flowfield computations. In this case, the heat flux may be expressed in terms of the reactive Prandtl and Lewis numbers. However, the total values of $C_{p}$ and $K$ as well as the reactive Prandtl and Lewis numbers can be used only with calculations involving thermal equilibrium. This is obvious from the definitions of $K$ and $C_{p}$ given by equations (A13) and (A19), respectively.

The frozen Prandtl number and Lewis numbers are defined as

$$
\begin{gather*}
P r_{f}=C_{p_{f}} \mu / K_{f}  \tag{A21}\\
L e_{f, i}=\rho C_{p_{f}} D_{i j} / K_{f} \tag{A22}
\end{gather*}
$$

where $C_{p_{f}}$ and $K_{f}$ are defined by equations (9) and (37), respectively. Generally, the subscript $f$ is not used in the literature to denote the frozen Prandtl and Lewis numbers as is done here.

The reactive Prandtl and Lewis numbers are defined by employing the total values of $C_{p}$ and $K$ as

$$
\begin{gather*}
P r_{r}=C_{p} \mu / K  \tag{A23}\\
L e_{r, i}=\rho C_{p} D_{i j} / K \tag{A24}
\end{gather*}
$$

where $C_{p}$ and $K$ are defined through equations (A18) and (A13) or (A15), respectively. Reference 29 gives definitions of the reactive Prandtl and Lewis numbers with $K$ defined through use of equation (A15) and employs no subscripts on $\operatorname{Pr}$ or Le. The frozen values defined through equations (A21) and (A22) are denoted as partial values in reference 29 and are denoted as $P r^{\prime}$ and $L e^{\prime}$ there.

[^7]
## Appendix B

## Sample Program to Evaluate Thermodynamic Properties From Polynomial Curve-

 FitsThis appendix lists a sample Fortran subroutine which evaluates the species specific heats and enthalpies for an 11 -species air model using polynomial curve fits as functions of temperature. Five temperature ranges are used for each species for temperatures between 300 K and 30000 K . Properties evaluated near the temperature range boundaries are smoothed by linearly averaging the polynomial coefficients to assure continuous derivatives. The subroutine may be easily modified for different needs.

## SUBROUTINE THERMO(T.CPI,HI)

C Computes enthalpy and specific heat for 11 species by
C approximating polynomials. Polynomial coefficients are stored in
C arrays A1 to A6 and are linearly averaged at the temperature range C boundaries.
C
C input: T temperature, K
C output: CPI specific heats of the species, $\mathrm{cal} / \mathrm{gm}-\mathrm{mole}-\mathrm{K}$
C HI enthalpies of the species, cal/gm-mole
DIMENSION A1(11,5),A2(11,5),A3(11,5),A4(11,5),A5(11,5),A6(11,5)
DIMENSION P(6),COEF (11,5,6)
DIMENSION CPI(11),HI(11)
EQUIVALENCE (Al,COEF)
C Universal gas constant, cal/gm-mole-K
DATA UNIR / 1.987/
C
C Coefficients are input for five temperature ranges
C
$K=4$
$\mathrm{L}=5$
IF(T.GT.15500.)GO TO 20
$K=3$
$\mathrm{L}=4$
IF(T.GT.5500)GOTO 30
$K=2$
$\mathrm{L}=3$
IF(T.GT.:200.)GO TO 40
$K=1$
$\mathrm{L}=2$
$\mathrm{PA}=1.0$
$\mathrm{PB}=0.0$
IF(T.LE.300.)GO TO 50

```
        \(\mathrm{PB}=(1 . / 400) *.(\mathrm{~T}-800\).
        \(\mathrm{PA}=1.0-\mathrm{PB}\)
        GO TO 50
    40 CONTINUE
        \(\mathrm{PA}=1.0\)
        \(\mathrm{PB}=0.0\)
        IF(T.LE.5500.)GO TO 50
        \(\mathrm{PB}=(1 . / 1000) *.(\mathrm{~T}-5500\).
        \(\mathrm{PA}=1.0-\mathrm{PB}\)
        GO TO 50
    20 CONTINUE
        \(\mathrm{PA}=0.0\)
        \(\mathrm{PB}=1.0\)
        IF(T.GE.25500.)GO TO 50
        \(\mathrm{PA}=1.0\)
        \(\mathrm{PB}=0.0\)
        IF(T.LE.24500.)GO TO 50
        \(\mathrm{PB}=0.001^{*}\) (T-24500.)
        \(\mathrm{PA}=1.0-\mathrm{PB}\)
        GO TO 50
    30 CONTINUE
    \(\mathrm{PA}=0.0\)
    \(\mathrm{PB}=1.0\)
    IF(T.GE.15500.)GO TO 50
    \(\mathrm{PA}=1.0\)
    \(\mathrm{PB}=0.0\)
    IF(T.LE.14500.)GO TO 50
    PB=0.001*(T-14500.)
    \(\mathrm{PA}=1.0-\mathrm{PB}\)
50 CONTINUE
C
    \(\mathrm{T} 2=\mathrm{T} * \mathrm{~T}\)
    \(\mathrm{T} 3=\mathrm{T} 2 * \mathrm{~T}\)
    T4 = T3*T
    TOV \(=1.0 / \mathrm{T}\)
C Compute properties for 11 species
    DO \(65 \mathrm{I}=1,11\)
    DO \(60 \mathrm{~J}=1,6\)
\(60 \mathrm{P}(\mathrm{J})=\mathrm{PA} \mathrm{C}^{\operatorname{COEF}}(\mathrm{I}, \mathrm{K}, \mathrm{J})+\mathrm{PB}{ }^{*} \operatorname{COEF}(\mathrm{I}, \mathrm{L}, \mathrm{J})\)
    \(\mathrm{HI}(\mathrm{I})=\mathrm{UNIR} * \mathrm{~T} *(\mathrm{P}(1)+0.5 * \mathrm{P}(2) * \mathrm{~T}+\mathrm{P}(3) * \mathrm{~T} 2 / 3 .+0.25 * \mathrm{P}(4) * \mathrm{~T} 3\)
    \(1+0.2 * \mathrm{P}(5) * \mathrm{~T} 4+\mathrm{P}(6) * \mathrm{TOV})\)
    \(\mathrm{CPI}(\mathrm{I})=\operatorname{UNIR} *(\mathrm{P}(1)+\mathrm{P}(2) * \mathrm{~T}+\mathrm{P}(3) * T 2+\mathrm{P}(4) * \mathrm{~T} 3+\mathrm{P}(5) * \mathrm{~T} 4)\)
65 CONTINUE
    RETURN
    END
```


## Appendix C

## Electron and Vibrational Heat Fluxes and Associated Thermal Conductivities for Flows with Thermal Nonequilibrium

Electron and vibrational heat fluxes are required in the electron energy and vibrational energy conservation equations in a multi-temperature gas model (refs. 20 and 46). The $k$ th component of heat flux vector $q_{a}^{k}$ resulting from the collisions between electrons only is given by

$$
\begin{equation*}
q_{a}^{k}=-K_{e}^{\prime} \frac{\partial T_{e}}{\partial x^{k}}+\rho_{e} h_{e} V_{e}^{k} \tag{C1}
\end{equation*}
$$

where $\rho_{e}\left(=m_{e} n_{e}\right)$ is the density and $h_{e}\left(=(5 / 2) k T_{d} / m_{e}\right)$ is the enthalpy of electrons, $m_{e}$ is the electron mass, $\dagger n_{e}$ is the electron number density, $k$ is Boltzmann's constant, $V_{e}^{k}$ is the $k$ th component of electron diffusion velocity and $K_{e}^{\prime}$ is the thermal conductivity of electrons resulting from collisions between electrons only. In a flowfield analysis, the diffusion velocity $V_{l}^{k}$ is generally obtained from the electron concentration gradient by using the relation

$$
\begin{equation*}
V_{e}^{k}=-D_{e j} \frac{\partial \ln \left(C_{e}\right)}{\partial x^{k}} \tag{C2}
\end{equation*}
$$

where $D_{c j}$ is the binary diffusion coefficient of electrons diffusing into the species $j$ and $C_{e}$ is the electron mass fraction.

The thermal conductivity $K_{f}^{\prime}$ (appearing in equation (C1)) due to collisions between electrons only may be obtained from $K$. (defined through equation (54)) by employing the relation

$$
\begin{equation*}
K_{e}^{\prime}=K_{e}\left[\frac{x_{e} \Delta_{e}^{(2)}\left(T_{e}\right)}{\sum_{j=1}^{11} x_{j} \Delta_{e j}^{(2)}\left(T_{e}\right)}\right] \tag{C3}
\end{equation*}
$$

The $k$ th component of vibrational heat flux vector $q_{v}^{k}$ (obtained from moleculemolecule collisions only) may be written as

$$
\begin{equation*}
q_{v i b}^{k}=-K_{v i b}^{\prime} \frac{\partial T_{v i b}}{\partial x^{k}}+\sum_{i=\text { moleccules }} \rho_{i} h_{i, v i b} V_{i}^{k} \tag{C4}
\end{equation*}
$$

where $h_{i, v i b}$ is the vibrational component of enthalpy of the molecules, $V_{i}^{k}$ is the $k$ th component of diffusion velocity of the molecules, and $K_{\text {vib }}^{\prime}$ is the thermal conductivity due to the collisions between molecules only.

Referring to Fig. 2, $h_{i, \text { wib }}$ for the partially excited vibrational energy mode may be obtained from

$$
\begin{equation*}
\left[h_{i, v i b}\right]_{T_{v i b}}=\left[h_{i}\right]_{\text {vib }}-\left[\left(C_{p, i}\right)_{r r}+\left(C_{p, i}\right)_{r o t}\right]\left(T_{v i b}-T_{r e f}\right)-\left(\Delta h_{i}{ }^{f}\right)_{T_{r e f}} \tag{C5}
\end{equation*}
$$

In equation ( C 5 ), the vibrational component of enthalpy for species $i$ is obtained by using the curve-fit relation of equation (14) for the specific enthalpy $h_{i}$ evaluated at temperature $T_{\text {vib }}$ and subtracting out the contributions from the translational and rotational enthalpies evaluated at $T_{\text {vib }}$ as well as the enthalpy of formation. Equation (C5)

[^8]can be employed up to the characteristic vibrational temperature $\Theta_{i, \text { vib }}$ for the species $i$, i.e., for $T_{\text {vib }} \leq \Theta_{i \text {,vib }}$. For higher temperatures ( $~_{\text {vib }}>\Theta_{i, \text { vib }}$ ), the vibrational energy mode is fully excited and $h_{i, v i b}$ can be obtained from
\[

$$
\begin{equation*}
\left[h_{i, v i b}\right] T_{\text {wib }}=R_{\text {univ }} T_{v i b} / M_{i} \tag{C6}
\end{equation*}
$$

\]

The thermal conductivity $K_{\text {vib }}^{\prime}$ (also known as the $V-V$ thermal conductivity) in equation (C4) is obtained from the overall vibrational thermal conductivity $K_{\text {vib }}$ (defined in equation (52)) by considering the contribution of molecule-molecule collisions only.

$$
\begin{equation*}
K_{v i b}^{\prime}=K_{v i b} \sum_{i=\text { molecules }}\left[\frac{\sum_{j=\text { molecules }} x_{j} \Delta_{i j}^{(2)}\left(T_{v i b)}\right.}{\sum_{j=1}^{10} x_{j} \Delta_{i j}^{(2)}\left(T_{v i b)}+x_{i} \Delta_{i e^{(2)}}^{(2)}\left(T_{a}\right)\right.}\right] \tag{C7}
\end{equation*}
$$

$$
-34-
$$

Table I. Third Body Efficiences Relative to Argon

| Catalytic Bodies | $\mathrm{Z}_{(j-N S), i}$ | Efficiences relative to argon of |  |  |  |  |  |  |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
|  |  | $\mathrm{O}_{2}$ | $\begin{gathered} N_{2} \\ 2 \end{gathered}$ | $\begin{array}{r} N \\ 3 \end{array}$ | $\begin{aligned} & 0 \\ & 4 \end{aligned}$ | $\begin{gathered} \text { NO } \\ 5 \end{gathered}$ | $\begin{gathered} \mathrm{NO}^{+} \\ 6 \end{gathered}$ | $\begin{gathered} O_{2}^{+} \\ 7 \end{gathered}$ | $\begin{gathered} N_{2}^{+} \\ 8 \end{gathered}$ | $\begin{gathered} O^{+} \\ 9 \end{gathered}$ | $\begin{gathered} N^{+} \\ 10 \end{gathered}$ |
| $\mathrm{M}_{1}$ | 1,i | 9 | 2 | 25 | 1 | 1 | 0 | 0 | 0 | 0 | 0 |
| $\mathrm{M}_{2}$ | 2,i | 1 | 2.5 | 1 | 0 | 1 | 0 | 0 | 0 | 0 | 0 |
| $\mathrm{M}_{3}$ | 3,i | 1 | 1 | 20 | 20 | 20 | 0 | 0 | 0 | 0 | 0 |
| $\mathrm{M}_{4}$ | 4,i | 4 | 1 | 0 | 0 | 0 | 0 | 0 | 0 | 0 | 0 |
| $e^{-}$ | 5,i | 0 | 0 | 0 | 0 | 0 | 1 | 1 | 1 | 1 | 1 |

Table II. Chemical Reactions and Rate Coefficients

| No.t | Reaction | Forward rate coefficient. $k_{f, r}$ $\mathrm{cm}^{3} /$ mole-sec | Backward rate coefficient, $k_{b, r}$. $\mathrm{cm}^{3} /$ mole - sec or $\mathrm{cm}^{6} / \mathrm{mole}^{2}-\mathrm{sec}$ | $\begin{aligned} & \text { Third body } \\ & M \end{aligned}$ |
| :---: | :---: | :---: | :---: | :---: |
| 1 | $O_{2}+M_{1} \rightleftarrows 2 O+M_{1}$ | $3.61 \times 10^{18} T^{-1.0} \exp \left(-5.94 \times 10^{4} / T\right)$ | $3.01 \times 10^{15} T^{-0.5}$ | $\mathrm{O}, \mathrm{N}, \mathrm{O}_{2}, \mathrm{~N}_{2}, \mathrm{NO}$ |
| 2 | $N_{2}+M_{2} \rightleftarrows 2 N+M_{2}$ | $1.92 \times 10^{17} T^{-0.5} \exp \left(-1.131 \times 10^{5} / T\right)$ | $1.09 \times 10^{16} \mathrm{~T}^{-0.5}$ | O. $O_{2,} N_{2}, N O$ |
| 3 | $N_{2}+N \rightleftarrows 2 N+N$ | $4.15 \times 10^{22} T^{-1.5} \exp \left(-1.31 \times 10^{5} / T\right)$ | $2.32 \times 10^{21} T^{-1.5}$ |  |
| 4 | $\mathrm{NO}+\mathrm{M}_{3} \rightleftarrows \mathrm{~N}+\mathrm{O}+\mathrm{M}_{3}$ | $3.97 \times 10^{20} T^{-1.5} \exp \left(-7.56 \times 10^{4} / T\right)$ | $1.01 \times 10^{20} T^{-1.5}$ | $\mathrm{O}, \mathrm{N}, \mathrm{O}_{2}, \mathrm{~N}_{2}, \mathrm{NO}$ |
| 5 | $\mathrm{NO}+\mathrm{O} \rightleftarrows \mathrm{O}_{2}+\mathrm{N}$ | $3.18 \times 10^{9} T^{1.0} \exp \left(-1.97 \times 10^{4} / T\right)$ | $9.63 \times 10^{11} T^{0.5} \exp \left(-3.6 \times 10^{3} / T\right)$ |  |
| 6 | $\mathrm{N}_{2}+\mathrm{O} \rightleftarrows \mathrm{NO}+\mathrm{N}$ | $6.75 \times 10^{13} \exp \left(-3.75 \times 10^{4} / T\right)$ | $1.5 \times 10^{13}$ |  |
| 7 | $N+O \rightleftarrows \mathrm{NO}^{+}+\mathrm{e}^{-}$ | $9.03 \times 10^{9} T^{0.5} \exp \left(-3.24 \times 10^{4} / T\right)$ | $1.80 \times 10^{19} T^{-1.0}$ |  |
| 8 | $O+e^{-} \rightleftarrows O^{+}+e^{-}+e^{-}$ | $(3.6 \pm 1.2) \times 10^{31} T^{-291} \exp \left(-1.58 \times 10^{5} / T\right)$ | $(2.2 \pm 0.7) \times 10^{40} T^{-4.5}$ |  |
| 9 | $N+e^{-} \rightleftarrows N^{+}+e^{-}+e^{-}$ | $(1.1 \pm 0.4) \times 10^{33} T^{-3.14} \exp \left(-1.69 \times 10^{5} / T\right)$ | $(2.2 \pm 0.7) \times 10^{40} \mathrm{~T}^{-4.5}$ |  |
| 10 | $O+O \rightleftarrows O_{2}+e^{-}$ | $(1.6 \pm 0.4) \times 10^{17} T^{-0.98} \exp \left(-8.08 \times 10^{4} / T\right)$ | $(8.02 \pm 2.0) \times 10^{21} T^{-1.5}$ |  |
| 11 | $O_{+}^{+} O_{2}^{+} \rightleftarrows O_{2+} O^{+}$ | $2.92 \times 10^{18} T^{-1.11} \exp \left(-2.8 \times 10^{4} / T\right)$ | $7.8 \times 10^{11} T^{0.5}$ |  |
| 12 | $N_{2}+N^{+} \rightleftarrows N+N_{2}^{+}$ | $2.02 \times 10^{11} T^{0.81} \exp \left(-1.3 \times 10^{4} / T\right)$ | $7.8 \times 10^{11} T^{0.5}$ |  |
| 13 | $N+N \rightleftarrows N_{2}^{+}+e^{-}$ | $(1.4 \pm 0.3) \times 10^{13} \exp \left(-6.78 \times 10^{4} / T\right)$ | $(1.5 \pm 0.5) \times 10^{22} T^{-1.5}$ |  |
| 14 | $\mathrm{O}_{2}+\mathrm{N}_{2} \rightleftarrows \mathrm{NO}+\mathrm{NO}^{+}+\mathrm{e}^{-}$ | $1.38 \times 10^{20} T^{-1.84} \exp \left(1.41 \times 10^{5} / T\right)$ | $1.0 \times 10^{24} T^{-2.5}$ |  |
| 15 | $N \mathrm{O}+\mathrm{M}_{4} \rightleftarrows \mathrm{NO}^{+}+\mathrm{e}^{-}+\mathrm{M}_{4}$ | $2.2 \times 10^{15} T^{-0.35} \exp \left(-1.08 \times 10^{5} / T\right)$ | $2.2 \times 10^{26} T^{-2.5}$ | $O_{2}, N_{2}$ |
| 16 | $\mathrm{O}+\mathrm{NO}^{+} \rightleftarrows \mathrm{NO}+\mathrm{O}^{+}$ | $3.63 \times 10^{15} T^{-0.6} \exp \left(-5.08 \times 10^{4} / T\right)$ | $1.5 \times 10^{13}$ |  |
| 17 | $\mathrm{N}_{2}+\mathrm{O}^{+} \rightleftarrows \mathrm{O}+\mathrm{N}^{+}$ | $3.4 \times 10^{19} T^{-20} \exp \left(-2.3 \times 10^{4} / T\right)$ | $2.48 \times 10^{19} T^{-2.2}$ |  |
| 18 | $\mathrm{N+NO}{ }^{+} \rightleftarrows \mathrm{NO}+\mathrm{N}^{+}$ | $1.0 \times 10^{19} T^{-0.93} \exp \left(-6.1 \times 10^{4} / T\right)$ | $4.8 \times 10^{14}$ |  |
| 19 | $\mathrm{O}_{2}+\mathrm{NO}^{+} \rightleftarrows \mathrm{NO}+\mathrm{O}_{2}$ | $1.8 \times 10^{15} T^{0.17} \exp \left(-3.3 \times 10^{4} / T\right)$ | $1.8 \times 10^{13} T^{0.5}$ |  |
| 20 | $\mathrm{O}+\mathrm{NO}^{+} \rightleftarrows \mathrm{O}_{2}+\mathrm{N}^{+}$ | $1.34 \times 10^{13} T^{0.31} \exp \left(-7.727 \times 10^{4} / T\right)$ | $1.0 \times 10^{14}$ |  |

[^9]Table III. Constants for Polynomial Curve-fits of Thermodynamic Properties $(300 \mathrm{~K} \leq \mathrm{T} \leq 30000 \mathrm{~K}) \dagger$
Species $A_{1} \quad A_{2} \quad A_{3} \quad A_{4} \quad A_{5}$

| $N_{2}$ | $0.36748 E+01$ | $-0.12081 E-02$ | 0.23240E-05 | -0.63218E-09 | $-0.22577 E-12$ | $-0.10612 E+04$ | $0.23580 E+01$ |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
|  | $0.28963 E+01$ | 0.15155E-02 | $-0.57235 E-06$ | 0.99807E-10 | $-0.65224 E-14$ | $-0.90586 E+03$ | $0.61615 E+01$ |
|  | $0.37270 E+01$ | $0.46840 \mathrm{E}-03$ | $-0.11400 E-06$ | 0.11540E-10 | $-0.32930 E$ | .10430E + 04 | $0.12940 E+01$ |
|  | $0.96377 E+01$ | $-0.25728 E-02$ | 0.33020E-06 | -0.14315E-10 | 0.20333E-15 | $-0.10430 E+04$ | $-0.37587 E+02$ |
|  | $-0.51681 E+01$ | 0.23337E-02 | $-0.12953 E-06$ | 0.27872E-11 | $-0.21360 E-16$ | $-0.10430 E+04$ | $0.66217 E+02$ |
| $O_{2}$ | $0.36256 E+0$ | $-0.18782 E-02$ | 05 | $-0.67635 E$ |  |  | 43 |
|  | $0.36219 E+01$ | $0.73618 E-03$ | -0.19652E-06 | 0.36202E-10 | -0.28946E | .12020E + 04 | $0.36151 E+01$ |
|  | $0.37210 E+01$ | $0.42540 E-03$ | $-0.28350 E-07$ | 0.60500E-12 | -0.51860E | $-0.10440 E+04$ | $0.32540 E+01$ |
|  | $0.34867 E+01$ | $0.52384 E-03$ | $-0.39123 E-07$ | $0.10094 E-11$ | $-0.88718 E-17$ | $-0.10440 E+04$ | $0.48179 E+01$ |
|  | $0.39620 E+01$ | $0.39446 E-03$ | $-0.29506 E-07$ | $0.73975 E-12$ | 0.64209E-17 | . 10 | 0.13 |
| $N$ | $0.25031 E+01$ | $-0.21800 E-04$ | 205E-07 | $-0.56476 E-10$ | 0.20999 | $0.56099 E+05$ | 0.41676 |
|  | $0.24503 E+01$ | 0.10661 E-03 | $-0.74653 E-07$ | $0.18797 E-10$ | -0.10260E-14 | $0.56116 E+05$ | $0.44488 E+01$ |
|  | $0.27480 E+01$ | $-0.39090 E-03$ | 0.13380E-06 | $-0.11910 E-10$ | 0.33690 E-15 | $0.56090 E+05$ | $0.28720 E+01$ |
|  | $-0.12280 E+01$ | 0.19268E-02 | $-0.24370 E-06$ | 0.12193E-10 | $-0.19918 E-15$ | $0.56090 E+05$ | $0.28469 E+02$ |
|  | $0.15520 E+02$ | $-0.38858 E-02$ | 0.32288E-06 | $-0.96053 E-11$ | 0.95472E-16 | $0.56090 E+05$ | $-0.88120 E+02$ |
| 0 | $0.29464 E+01$ | $-0.16382 E-02$ | 0.24210E-05 | $-0.16028 E-08$ | $0.38907 E-12$ | $0.29148 E+05$ | . $29640 E+01$ |
|  | $0.25421 E+01$ | $-0.27551 E-04$ | $-0.31028 E-08$ | $0.45511 E-11$ | $-0.43680 E-15$ | $0.29231 E+05$ | 01 |
|  | $0.25460 E+01$ | $-0.59520 E-04$ | 0.27010E-07 | $-0.27980 E-11$ | 0.93800E-16 | $0.29150 E+05$ | $0.50490 E+01$ |
|  | -0.97871E-02 | $0.12450 \mathrm{E}-02$ | $-0.16154 E-06$ | 0.80380E-11 | $-0.12624 E-15$ | $0.29150 E+05$ | $0.21711 E+02$ |
|  | $0.16428 E+02$ | $-0.39313 E-02$ | 0.29840E-06 | $-0.81613 E-11$ | 0.75004E-16 | $0.29150 E+05$ | $-0.94358 E+02$ |
| No | $0.40459 E+01$ | $-0.34182 E-02$ | 0.79819E-05 | -0.61139E-08 | 0.15919E-11 | $0.97454 E+04$ | $0.29975 E+01$ |
|  | 0.31890 E + 01 | $0.13382 E-02$ | $-0.52899 E-06$ | $0.95919 E-10$ | $-0.64848 E-14$ | $0.98283 E+04$ | $0.67458 E+01$ |
|  | $0.38450 E+01$ | $0.25210 E-03$ | $-0.26580 E-07$ | $0.21620 E-11$ | $-0.63810 E-16$ | $0.97640 E+04$ | $32120 E+01$ |
|  | $0.43309 E+0$ | $-0.58086 E-04$ | 0.28059E-07 | $-0.15694 E-11$ | 0.24104E-16 | $0.97640 E+04$ | $0.10735 E+00$ |
|  | $0.23507 E+01$ | $0.58643 E-03$ | $-0.31316 E-07$ | $0.60495 E-12$ | -0.40557E-17 | $0.97640 E+04$ | $0.14026 E+02$ |
| NO* | $0.36685 E+01$ | -0.11545E-02 | 0.21756E-05 | -0.48227E-09 | -0.27848E-12 | $0.11803 E+06$ | $0.31779 E+01$ |
|  | $0.28886 E+01$ | 0.15217E-02 | -0.57531E-06 | $0.10051 E-09$ | -0.66044E-14 | $0.11819 E+06$ | $0.70027 E+01$ |
|  | $0.22142 E+01$ | 0.17761E-02 | -0.43039E-06 | $0.41738 E-10$ | -0.12829E-14 | $0.11819 E+06$ | $0.11268 E+02$ |
|  | $-0.33240 E+01$ | 0.24420E-02 | 0.19057E-06 | 0.68580E-11 | $-0.99112 E-16$ | $0.11819 E+06$ | $0.51864 E+02$ |
|  | $-0.43488 E+01$ | 0.24012E-02 | -0.14460E-06 | $0.33813 E-11$ | $-0.28255 E-16$ | $0.11819 E+06$ | $0.60082 E+02$ |
| $e^{-}$ | $0.25000 E+01$ | $0.00000 E+00$ | $0.00000 E+00$ | 0.00000E + 00 | $0.00000 E+00$ | $-0.74538 E+03$ | $-0.11734 E+02$ |
|  | $0.25000 E+01$ | $0.00000 E+00$ | $0.00000 E+00$ | $0.00000 E+00$ | $0.00000 E+00$ | $-0.74538 E+03$ | $-0.11734 E+02$ |
|  | $0.25080 E+01$ | $-0.63320 E-05$ | $0.13640 E-08$ | $-0.10940 E-12$ | 0.29340E-17 | $-0.74500 E+03$ | 0.12080E + 02 |
|  | $0.25001 E+01$ | $-0.31128 E-09$ | $0.35721 E-13$ | $-0.16037 E-17$ | $0.25071 E-22$ | $-0.74500 E+03$ | $-0.11734 E+02$ |
|  | $0.25001 E+01$ | $0.30158 E-09$ | $-0.22620 E-13$ | $0.66734 E-18$ | $-0.68917 E-23$ | $-0.74500 E+03$ | $-0.11734 E+02$ |
| $N^{+}$ | $0.27270 E+01$ | -0.28200E-03 | 0.11050E-06 | -0.15510E-10 | 0.78470E-15 | $0.22540 E+06$ | $0.36450 E+01$ |
|  | $0.27270 E+01$ | $-0.28200 E-03$ | 0.11050E-06 | $-0.15510 E-10$ | 0.78470E-15 | $0.22540 E+06$ | $0.36450 E+01$ |
|  | $0.24990 E+01$ | $-0.37250 E-05$ | $0.11470 E-07$ | $-0.11020 E-11$ | 0.30780E-16 | $0.22540 E+06$ | $0.49500 E+01$ |
|  | $0.23856 E+01$ | $0.83495 E-04$ | $-0.58815 E-08$ | $0.18850 E-12$ | $-0.16120 E-17$ | $0.22540 E+06$ | $0.56462 E+01$ |
|  | $0.22286 E+01$ | 0.12458E-03 | $-0.87636 E-08$ | $0.26204 E-12$ | $-0.21674 E-17$ | 0.22540 | 0.6781 |


|  | $0.24985 E+01$ | $0.11411 E-04$ | $-0.29761 E-07$ | $0.32247 E-10$ | $-0.12376 E-13$ | $0.18795 E+06$ | $0.43864 E+01$ |
| :---: | ---: | ---: | ---: | ---: | ---: | ---: | ---: |
| $O^{+}$ | $0.25061 E+01$ | $-0.14464 E-04$ | $0.12446 E-07$ | $-0.46858 E-11$ | $0.65549 E-15$ | $0.18795 E+06$ | $0.43480 E+01$ |
|  | $0.29440 E+01$ | $-0.41080 E-03$ | $0.91560 E-07$ | $-0.58480 E-11$ | $0.11900 E-15$ | $0.18790 E+06$ | $0.17500 E+01$ |
|  | $0.12784 E+01$ | $0.40866 E-03$ | $-0.21731 E-07$ | $0.33252 E-12$ | $0.63160 E-18$ | $0.18790 E+06$ | $0.12761 E+02$ |
|  | $0.12889 E+01$ | $0.43343 E-03$ | $-0.26758 E-07$ | $0.62159 E-12$ | $-0.45131 E-17$ | $0.18790 E+06$ | $0.12604 E+02$ |
|  |  |  |  |  |  |  |  |
|  | $0.33970 E+01$ | $0.45250 E-03$ | $0.12720 E-06$ | $-0.38790 E-10$ | $0.24590 E-14$ | $0.18260 E+06$ | $0.42050 E+01$ |
| $N_{2}^{+}$ | $0.33970 E+01$ | $0.45250 E-03$ | $0.12720 E-06$ | $-0.38790 E-10$ | $0.24590 E-14$ | $0.18260 E+06$ | $0.42050 E+01$ |
|  | $0.33780 E+01$ | $0.86290 E-03$ | $-0.12760 E-06$ | $0.80870 E-11$ | $-0.18800 E-15$ | $0.18260 E+06$ | $0.40730 E+01$ |
|  | $0.43942 E+01$ | $0.18868 E-03$ | $-0.71272 E-08$ | $-0.17511 E-12$ | $0.67176 E-17$ | $0.18260 E+06$ | $-0.23693 E+01$ |
|  | $0.39493 E+01$ | $0.36795 E-03$ | $-0.26910 E-07$ | $0.67110 E-12$ | $-0.58244 E-17$ | $0.18260 E+06$ | $0.65472 E+00$ |
|  |  |  |  |  |  |  |  |
|  | $0.32430 E+01$ | $0.11740 E-02$ | $-0.39000 E-06$ | $0.54370 E-10$ | $-0.23920 E-14$ | $0.14000 E+06$ | $0.59250 E+01$ |
|  | $0.32430 E+01$ | $0.11740 E-02$ | $-0.39000 E-06$ | $0.54370 E-10$ | $-0.23920 E-14$ | $0.14000 E+06$ | $0.59250 E+01$ |
| $O_{2}$ | $0.51690 E+01$ | $-0.36200 E-03$ | $0.20410 E-06$ | $-0.13000 E-10$ | $0.24940 E-15$ | $0.14000 E+06$ | $-0.52960 E+01$ |
|  | $-0.28017 E+00$ | $0.16674 E-02$ | $-0.12107 E-06$ | $0.32113 E-11$ | $-0.28349 E-16$ | $0.14000 E+06$ | $0.31013 E+02$ |
|  | $0.20445 E+01$ | $0.10313 E-02$ | $-0.74046 E-07$ | $0.19257 E-11$ | $-0.17461 E-16$ | $0.14000 E+06$ | $0.14310 E+02$ |

$\dagger$ There are five rows of constants provided for each species which correspond to the following five temperature ranges, respectively.

$$
\begin{gathered}
300 \mathrm{~K} \leq \mathrm{T} \leq 1000 \mathrm{~K} \\
1000 \mathrm{~K} \leq \mathrm{T} \leq 6000 \mathrm{~K} \\
6000 \mathrm{~K} \leq \mathrm{T} \leq 15000 \mathrm{~K} \\
15000 \mathrm{~K} \leq \mathrm{T} \leq 25000 \mathrm{~K} \\
25000 \mathrm{~K} \leq \mathrm{T} \leq 30000 \mathrm{~K}
\end{gathered}
$$

For temperatures less than 300 K (which may arise in the freestream for certain flight trajectories (refs. 15,52 )), the specific heats of $O, \mathrm{O}_{2}, \mathrm{~N}$, and $\mathrm{N}_{2}$ are practically constant. For such cases, the specific enthalpy may be obtained from the relation:

$$
h_{i}=C_{p, i}\left(T-T_{r e f}\right)+\left(\Delta h_{i}^{\prime}\right)_{T_{r e f}}
$$

with $T_{\mathrm{ref}}=298 \mathrm{~K}$ and $C_{p, 0}=5.44 \mathrm{cal} / \mathrm{gm}-$ mole $-K, C_{p, 0}=7.00 \mathrm{cal} / \mathrm{gm}-\mathrm{mole}-K, C_{p, N}=4.97 \mathrm{cal} / \mathrm{gm}-\mathrm{mole}-\mathrm{K}$, $C_{p, N_{2}}=6.96 \mathrm{cal} / \mathrm{gm}-$ mole $-K$.

## Table IV. Constants for Viscosity $\dagger$ Curve-Fits $(1000 \mathrm{~K} \leq \mathrm{T} \leq 30000 \mathrm{~K}) \dagger \dagger$

|  |  | $B_{\mu_{i}}$ |  | $C_{\mu_{i}}$ | $D_{\mu_{i}}$ |
| :--- | :--- | :--- | ---: | ---: | ---: |
| Species $\ddagger$ | $A_{\mu_{i}}$ |  | $E_{\mu_{i}}$ |  |  |
|  |  |  |  |  |  |
| $N_{2}$ | 0.0 | 0.0 | 0.0203 | 0.4329 | -11.8153 |
| $O_{2}$ | 0.0 | 0.0 | 0.0484 | -0.1455 | -8.9231 |
| $N$ | 0.0 | 0.0 | 0.0120 | 0.5930 | -12.3805 |
| 0 | 0.0 | 0.0 | 0.0205 | 0.4257 | -11.5803 |
| $N O$ | 0.0 | 0.0 | 0.0452 | -0.0609 | -9.4596 |
| $N O^{+}$ | 0.0913 | -3.3178 | 45.1426 | -270.3948 | 586.3300 |
| $e^{-}$ | 0.0899 | -3.2731 | 44.5782 | -267.2522 | 574.4149 |
| $N^{+}$ | 0.0895 | -3.2573 | 44.3511 | -265.8276 | 576.1313 |
| $O^{+}$ | 0.0912 | -3.3154 | 45.1290 | -270.4211 | 586.2903 |
| $N_{2}^{+}$ | 0.0897 | -3.2618 | 44.4079 | -266.1462 | 577.1449 |
| $O_{2}^{+}$ | 0.0908 | -3.3020 | 44.9511 | -269.3877 | 584.4130 |

$\dagger$ Viscosity is obtained in $\mathrm{gm} / \mathrm{cm}-\mathrm{sec}$
$\dagger \dagger$ For temperatures less than 1000 K , Sutherland's viscosity law for air may be used for all species.
$\ddagger$ The ionic species viscosities given here are for an electron pressure of 1 atm . For different electron pressures, these values should be corrected by the formula given in equation (24a) in the main text.

Table V. Constants for Frozen Thermal Conductivity $\dagger$ Curve-Fits ( $1000 \mathrm{~K} \leq \mathrm{T} \leq 30000 \mathrm{~K}$ ) $\dagger^{\dagger}$

| Species $\ddagger$ | $A_{K_{f, i}}$ | $B_{K_{f, i}}$ | $C_{K_{f, i}}$ | $D_{K_{f, i}}$ | $E_{K_{f, i}}$ |
| :--- | :--- | :--- | ---: | ---: | ---: |
|  |  |  |  |  |  |
| $N_{2}$ | 0.0418 | -1.2720 | 14.4571 | -71.9660 | 122.5745 |
| $O_{2}$ | 0.0776 | -2.5007 | 30.1390 | -160.1758 | 307.3634 |
| $N$ | 0.0 | 0.0 | 0.0169 | 0.5373 | -12.8682 |
| $O$ | 0.0 | 0.0 | 0.0319 | 0.2485 | -11.6657 |
| $N O$ | 0.0263 | -0.8130 | 9.4203 | -47.6841 | 79.4139 |
| $N O^{+}$ | 0.0 | 0.0431 | -0.5477 | 2.1912 | -17.8610 |
| $e^{-}$ | 0.0908 | -3.3046 | 44.9877 | -269.6002 | 588.9412 |
| $N^{+}$ | 0.1023 | -3.6925 | 49.8997 | -297.1291 | 641.3168 |
| $O^{+}$ | 0.0534 | -2.0710 | 29.9141 | -188.4951 | 421.3914 |
| $N_{2}^{+}$ | 0.0918 | -3.3760 | 46.2945 | -278.4425 | 604.2017 |
| $O_{2}^{+}$ | -0.0125 | 0.1276 | 2.5428 | -37.7507 | 111.8110 |

$\dagger$ Thermal conductivity is obtained in call $\mathrm{cm}-\mathrm{sec}-\mathrm{K}$
$\dagger \dagger$ For temperatures lower than 1000 K , Sutherland's law for thermal conductivity of air may be used for each species.
$\ddagger$ The ionic species frozen thermal conductivities given here are for an electron pressure of 1 atm. For different electron pressure, these values should be corrected by employing the formula given in equation (24a) in the main text.

Table VI. Constants for Diffusion Coefficient $\dagger$ Curve-Fits

| No. $\dagger \dagger$ | Interaction Pair (i-j) | $A_{\bar{D}_{\text {ij }}}$ | ${ }^{B_{\bar{D}}{ }^{\text {j }}}$ | $C_{\bar{D}_{i j}}$ | $D_{\bar{D}_{i j}}$ | Temperature Range, $\mathrm{K} \ddagger$ |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| 1 | $N_{2}-N_{2}$ | 0.0 | 0.0112 | 1.6182 | -11.3091 |  |
| 2 | $\mathrm{O}_{2}-\mathrm{N}_{2}$ | 0.0 | 0.0465 | 0.9271 | -8.1137 |  |
| 3 | $\mathrm{O}_{2}-\mathrm{O}_{2}$ | 0.0 | 0.0410 | 1.0023 | -8.3597 |  |
| 4 | $\mathrm{N}-\mathrm{N}_{2}$ | 0.0 | 0.0195 | 1.4880 | -10.3654 |  |
| 5 | $\mathrm{N}-\mathrm{O}_{2}$ | 0.0 | 0.0179 | 1.4848 | -10.2810 |  |
| 6 | $N-N$ | 0.0 | 0.0033 | 1.5572 | -11.1616 |  |
| 7 | $\mathrm{O}-\mathrm{N}_{2}$ | 0.0 | 0.0140 | 1.5824 | -10.8819 |  |
| 8 | $\mathrm{O}-\mathrm{O}_{2}$ | 0.0 | 0.0226 | 1.3700 | -9.6631 |  |
| 9 | O-N | 0.0 | -0.0048 | 1.9195 | -11.9261 |  |
| 10 | O-O | 0.0 | 0.0034 | 1.5572 | -11.1729 |  |
| 11 | $\mathrm{NO}-\mathrm{N}_{2}$ | 0.0 | 0.0291 | 1.2676 | -9.6878 |  |
| 12 | $\mathrm{NO}-\mathrm{O}_{2}$ | 0.0 | 0.0438 | 0.9647 | -8.2380 |  |
| 13 | $N O-N$ | 0.0 | 0.0185 | 1.4882 | -10.3301 |  |
| 14 | NO-O | 0.0 | 0.0179 | 1.4848 | -10.3155 |  |
| 15 | $\mathrm{NO}-\mathrm{NO}$ | 0.0 | 0.0364 | 1.1176 | -8.9695 |  |
| 16 | $\mathrm{NO}^{+}-\mathrm{N}_{2}$ | 0.0 | 0.0 | 1.9000 | -13.3343 |  |
| 17 | $\mathrm{NO}^{+}-\mathrm{O}_{2}$ | 0.0 | 0.0 | 1.9001 | -13.3677 |  |
| 18 | $\mathrm{NO}^{+}-\mathrm{N}$ | 0.0 | 0.0 | 1.8999 | -13.1254 |  |
| 19 | $\mathrm{NO}^{+}-\mathrm{O}$ | 0.0 | 0.0 | 1.9000 | -13.1701 |  |
| 20 | $\mathrm{NO}^{+}-\mathrm{NO}$ | 0.0 | 0.0047 | 1.5552 | -11.3713 |  |
| 21 | $\mathrm{NO}^{+}-\mathrm{NO}^{+}$ | -0.1251 | 3.5135 | -29.7280 | 74.1550 |  |
| 22 | $e^{-}-N_{2}$ | -0.1147 | 2.8945 | -23.0085 | 65.9815 |  |
| 23 | $e^{-}-O_{2}$ | -0.0241 | 0.3464 | 0.1136 | -1.3848 | 1000-9000 |
|  |  | -0.0029 | 0.0856 | 0.6655 | -0.8205 | 9000-30000 |
| 24 | $e^{-}-N$ | 0.0 | 0.0 | 1.5000 | -2.9987 |  |
| 25 | $e^{-}-0$ | 0.0581 | -1.5975 | 15.4508 | -40.7370 |  |
| 26 | $e^{-}-N O$ | 0.2202 | -5.2261 | 42.0630 | -106.0937 | 1000-8000 |
|  |  | 0.2871 | -8.3759 | 82.8802 | -267.0227 | 8000-30000 |
| 27 | $e^{-}-\mathrm{NO}^{+}$ | -0.1251 | 3.5134 | -29.7272 | 79.2610 |  |
| 28 | $e^{-}-e^{-}$ | -0.1251 | 3.5136 | -29.7290 | 79.6126 |  |
| 29 | $N^{+}-N_{2}$ | 0.0 | 0.0 | 1.9000 | -13.1144 |  |
| 30 | $\mathrm{N}^{+}-\mathrm{O}_{2}$ | 0.0 | 0.0 | 1.9000 | -13.1357 |  |
| 31 | $N^{+}-N$ | 0.0 | 0.0033 | 1.5572 | -11.1616 |  |
| 32 | $N^{+}-\mathrm{O}$ | 0.0 | 0.0 | 1.9000 | -13.0028 |  |
| 33 | $\mathrm{N}^{+}-\mathrm{NO}$ | 0.0 | 0.0 | 1.8999 | -13.1254 |  |
| 34 | $\mathrm{N}^{+}-\mathrm{NO}^{+}$ | -0.1251 | 3.5135 | -29.7285 | 74.3825 |  |
| 35 | $N^{+}-e^{-}$ | -0.1251 | 3.5134 | -29.7272 | 79.2611 |  |
| 36 | $N^{+}-N^{+}$ | -0.1251 | 3.5134 | -29.7274 | 74.5342 |  |
| 37 | $\mathrm{O}^{+}-\mathrm{N}_{2}$ | 0.0 | 0.0 | 1.9000 | -13.1578 |  |
| 38 | $\mathrm{O}^{+}-\mathrm{O}_{2}$ | 0.0 | 0.0 | 1.9000 | -13.1810 |  |
| 39 | $O^{+}-N$ | 0.0 | 0.0 | 1.9000 | -13.0028 |  |
| 40 | $\mathrm{O}^{+}-\mathrm{O}$ | 0.0 | 0.0034 | 1.5572 | -11.1729 |  |
| 41 | $\mathrm{O}^{+}-\mathrm{NO}$ | 0.0 | 0.0 | 1.9000 | -13.1701 |  |
| 42 | $\mathrm{O}^{+}-\mathrm{NO}^{+}$ | -0.1251 | 3.5133 | -29.7268 | 74.3330 |  |
| 43 | $\mathrm{O}^{+}-\mathrm{e}^{-}$ | -0.1251 | 3.5134 | -29.7274 | 79.2616 |  |


| 44 | $O^{+}-N^{+}$ | -0.1251 | 3.5134 | -29.7275 | 74.5023 |
| :--- | :--- | :--- | :--- | ---: | ---: |
| 45 | $O^{+}-O^{+}$ | -0.1251 | 3.5134 | -29.7277 | 74.4687 |
| 46 | $N_{2}^{+}-N_{2}$ | 0.0 | 0.0 | 1.9000 | -13.3173 |
| 47 | $N_{2}^{+}-O_{2}$ | 0.0 | 0.0 | 1.9000 | -13.3495 |
| 48 | $N_{2}^{+}-N$ | 0.0 | 0.0 | 1.9000 | -13.1144 |
| 49 | $N_{2}^{+}-O$ | 0.0 | 0.0 | 1.9000 | -13.1578 |
| 50 | $N_{2}^{+}-N O$ | 0.0 | 0.0 | 1.9000 | -13.3343 |
| 51 | $N_{2}^{+}-N O^{+}$ | -0.1251 | 3.5134 | -29.7279 | 74.1721 |
| 52 | $N_{2}^{+}-e^{-}$ | -0.1251 | 3.5134 | -29.7273 | 79.2613 |
| 53 | $N_{2}^{+}-N^{+}$ | -0.1251 | 3.5135 | -29.7288 | 74.3947 |
| 54 | $N_{2}^{+}-O^{+}$ | -0.1251 | 3.5133 | -29.7269 | 74.3453 |
| 55 | $N_{2}^{+}-N_{2}^{+}$ | -0.1251 | 3.5135 | -29.7282 | 74.1899 |
| 56 | $O_{2}^{+}-N_{2}$ | 0.0 | 0.0 | 1.9000 | -13.3173 |
| 57 | $O_{2}^{+}-O_{2}$ | 0.0 | 0.0 | 1.9000 | -13.3495 |
| 58 | $O_{2}^{+}-N$ | 0.0 | 0.0 | 1.9000 | -13.1144 |
| 59 | $O_{2}^{+}-O$ | 0.0 | 0.0 | 1.9000 | -13.1578 |
| 60 | $O_{2}^{+}-N O$ | 0.0 | 0.0 | 1.9000 | -13.3343 |
| 61 | $O_{2}^{+}-N O^{+}$ | -0.1251 | 3.5134 | -29.7279 | 74.1721 |
| 62 | $O_{2}^{+}-e^{-}$ | -0.1251 | 3.5134 | -29.7273 | 79.2613 |
| 63 | $O_{2}^{+}-N^{+}$ | -0.1251 | 3.5135 | -29.7288 | 74.3947 |
| 64 | $O_{2}^{+}-O^{+}$ | -0.1251 | 3.5133 | -29.7269 | 74.3453 |
| 65 | $O_{2}^{+}-N_{2}^{+}$ | -0.1251 | 3.5135 | -29.7282 | 74.1899 |
| 66 | $O_{2}^{+}-O_{2}^{+}$ | -0.1251 | 3.5135 | -29.7282 | 74.1899 |

$\dagger$ Diffusion coefficients are obtained in $\mathrm{cm}^{2}-\mathrm{atm} / \mathrm{sec}$. Diffusion coefficients obtained from these curvefits are for an electron pressure of 1 atm . For different electron pressures, the cross sections should be corrected by the formula given in the main text when the interacting pair of species are both ions or electrons or a combination of the two. Note that diffusion coefficients for $N_{2}^{+}$and $O_{2}^{+}$are taken to be the same.
$\dagger \dagger$ Cross section Nos. 1-15 are used in a 5 -species air model and Nos. $1-28$ in a 7 -species model.
$\ddagger$ The temperature range for all curve fits is $1000 \leq \mathrm{T} \leq 30000 \mathrm{~K}$, except where noted.

Table VII. Curve-Fit Constants for Collision Cross-Section, $\bar{\Omega}_{i j}^{(1,1)} \dagger$

| No. $\dagger \dagger$ | $\begin{aligned} & \hline \text { Interaction } \\ & \text { Pair (i-j) } \\ & \hline \end{aligned}$ | $A_{\bar{\Omega}_{i j}^{(1,1)}}$ | $B_{\bar{\Omega}_{i j}^{(1,1)}}$ | $C_{\bar{\Omega}_{(i j}^{(1,1)}}$ | $D_{\bar{\Omega}_{i j}^{(1,1)}}$ | Temperature Range, $\mathrm{K} \ddagger$ |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| 1 | $N_{2}-N_{2}$ | 0.0 | -0.0112 | -0.1182 | 4.8464 |  |
| 2 | $\mathrm{O}_{2}-\mathrm{N}_{2}$ | 0.0 | -0.0465 | 0.5729 | 1.6185 |  |
| 3 | $\mathrm{O}_{2}-\mathrm{O}_{2}$ | 0.0 | -0.0410 | 0.4977 | 1.8302 |  |
| 4 | $\mathrm{N}-\mathrm{N}_{2}$ | 0.0 | -0.0194 | 0.0119 | 4.1055 |  |
| 5 | $\mathrm{N}-\mathrm{O}_{2}$ | 0.0 | -0.0179 | 0.0152 | 3.9996 |  |
| 6 | $N-N$ | 0.0 | -0.0033 | -0.0572 | 5.0452 |  |
| 7 | $\mathrm{O}-\mathrm{N}_{2}$ | 0.0 | -0.0139 | -0.0825 | 4.5785 |  |
| 8 | $\mathrm{O}-\mathrm{O}_{2}$ | 0.0 | -0.0226 | 0.1300 | 3.3363 |  |
| 9 | $0-N$ | 0.0 | 0.0048 | -0.4195 | 5.7774 |  |
| 10 | O-O | 0.0 | -0.0034 | -0.0572 | 4.9901 |  |
| 11 | $\mathrm{NO}-\mathrm{N}_{2}$ | 0.0 | -0.0291 | 0.2324 | 3.2082 |  |
| 12 | $\mathrm{NO}-\mathrm{O}_{2}$ | 0.0 | -0.0438 | 0.5352 | 1.7252 |  |
| 13 | NO-N | 0.0 | -0.0185 | 0.0118 | 4.0590 |  |
| 14 | $\mathrm{NO}-\mathrm{O}$ | 0.0 | -0.0179 | 0.0152 | 3.9996 |  |
| 15 | $N O-N O$ | 0.0 | -0.0364 | 0.3825 | 2.4718 |  |
| 16 | $\mathrm{NO}^{+}-\mathrm{N}_{2}$ | 0.0 | 0.0 | -0.4000 | 6.8543 |  |
| 17 | $\mathrm{NO}^{+}-\mathrm{O}_{2}$ | 0.0 | 0.0 | -0.4000 | 6.8543 |  |
| 18 | $\mathrm{NO}^{+}-\mathrm{N}$ | 0.0 | 0.0 | -0.4000 | 6.8543 |  |
| 19 | $\mathrm{NO}^{+}-\mathrm{O}$ | 0.0 | 0.0 | -0.4000 | 6.8543 |  |
| 20 | $\mathrm{NO}^{+}-\mathrm{NO}$ | 0.0 | -0.0047 | -0.0551 | 4.8737 |  |
| 21 | $\mathrm{NO}^{+}-\mathrm{NO}^{+}$ | 0.1251 | -3.5134 | 31.2277 | -80.6515 |  |
| 22 | $e^{-}-N_{2}$ | 0.1147 | -2.8945 | 24.5080 | -67.3691 |  |
| 23 | $e^{-}-\mathrm{O}_{2}$ | 0.0241 | -0.3467 | 1.3887 | -0.0110 | 1000-9000 |
|  |  | 0.0025 | -0.0742 | 0.7235 | -0.2116 | 9000-30000 |
| 24 | $e^{-}-N$ | 0.0 | 0.0 | 0.0 | 1.6094 |  |
| 25 | $e^{-}-0$ | 0.0164 | -0.2431 | 1.1231 | -1.5561 | 1000-9000 |
|  |  | -0.2027 | 5.6428 | -51.5646 | 155.6091 | 9000-30000 |
| 26 | $e^{-}-N O$ | -0.2202 | 5.2265 | -40.5659 | 104.7126 | 1000-8000 |
|  |  | -0.2871 | 8.3757 | -81.3787 | 265.6292 | 8000-30000 |
| 27 | $e^{-}-N O^{+}$ | 0.1251 | -3.5134 | 31.2277 | -80.6515 |  |
| 28 | $e^{-}-e^{-}$ | 0.1251 | -3.5134 | 31.2277 | -80.6515 |  |
| 29 | $\mathrm{N}^{+}-\mathrm{N}_{2}$ | 0.0 | 0.0 | -0.4000 | 6.8543 |  |
| 30 | $\mathrm{N}^{+}-\mathrm{O}_{2}$ | 0.0 | 0.0 | -0.4000 | 6.8543 |  |
| 31 | $N^{+}-N$ | 0.0 | -0.0033 | -0.0572 | 5.0452 |  |
| 32 | $N^{+}-\mathrm{O}$ | 0.0 | 0.0 | -0.4000 | 6.8543 |  |
| 33 | $\mathrm{N}^{+}-\mathrm{NO}$ | 0.0 | 0.0 | -0.4000 | 6.8543 |  |
| 34 | $\mathrm{N}^{+}-\mathrm{NO}^{+}$ | 0.1251 | -3.5134 | 31.2277 | -80.6515 |  |
| 35 | $N^{+}-e^{-}$ | 0.1251 | -3.5134 | 31.2277 | -80.6515 |  |
| 36 | $N^{+}-N^{+}$ | 0.1251 | -3.5134 | 31.2277 | -80.6515 |  |
| 37 | $\mathrm{O}^{+}-\mathrm{N}_{2}$ | 0.0 | 0.0 | -0.4000 | 6.8543 |  |
| 38 | $\mathrm{O}^{+}-\mathrm{O}_{2}$ | 0.0 | 0.0 | -0.4000 | 6.8543 |  |
| 39 | $\mathrm{O}^{+}-\mathrm{N}$ | 0.0 | 0.0 | -0.4000 | 6.8543 |  |
| 40 | $O^{+}-0$ | 0.0 | -0.0034 | -0.0572 | 4.9901 |  |
| 41 | $\mathrm{O}^{+}-\mathrm{NO}$ | 0.0 | 0.0 | -0.4000 | 6.8543 |  |
| 42 | $\mathrm{O}^{+}-\mathrm{NO}^{+}$ | 0.1251 | -3.5134 | 31.2277 | -80.6515 |  |


| 43 | $O^{+}-e^{-}$ | 0.1251 | -3.5134 | 31.2277 | -80.6515 |
| :--- | :--- | :--- | :--- | :--- | ---: |
| 44 | $O^{+}-N^{+}$ | 0.1251 | -3.5134 | 31.2277 | -80.6515 |
| 45 | $O^{+}-O^{+}$ | 0.1251 | -3.5134 | 31.2277 | -80.6515 |
| 46 | $N_{2}^{+}-N_{2}$ | 0.0 | 0.0 | -0.4000 | 6.8543 |
| 47 | $N_{2}^{+}-O_{2}$ | 0.0 | 0.0 | -0.4000 | 6.8543 |
| 48 | $N_{2}^{+}-N$ | 0.0 | 0.0 | -0.4000 | 6.8543 |
| 49 | $N_{2}^{+}-O$ | 0.0 | 0.0 | -0.4000 | 6.8543 |
| 50 | $N_{2}^{+}-N O$ | 0.0 | 0.0 | -0.4000 | 6.8543 |
| 51 | $N_{2}^{+}-N O^{+}$ | 0.1251 | -3.5134 | 31.2277 | -80.6515 |
| 52 | $N_{2}^{+}-e^{-}$ | 0.1251 | -3.5134 | 31.2277 | -80.6515 |
| 53 | $N_{2}^{+}-N^{+}$ | 0.1251 | -3.5134 | 31.2277 | -80.6515 |
| 54 | $N_{2}^{+}-O^{+}$ | 0.1251 | -3.5134 | 31.2277 | -80.6515 |
| 55 | $N_{2}^{+}-N_{2}^{+}$ | 0.1251 | -3.5134 | 31.2277 | -80.6515 |
| 56 | $O_{2}^{+}-N_{2}$ | 0.0 | 0.0 | -0.4000 | 6.8543 |
| 57 | $O_{2}^{+}-O_{2}$ | 0.0 | 0.0 | -0.4000 | 6.8543 |
| 58 | $O_{2}^{+}-N$ | 0.0 | 0.0 | -0.4000 | 6.8543 |
| 59 | $O_{2}^{+}-O$ | 0.0 | 0.0 | -0.4000 | 6.8543 |
| 60 | $O_{2}^{+}-N O$ | 0.0 | 0.0 | -0.4000 | 6.8543 |
| 61 | $O_{2}^{+}-N O^{+}$ | 0.1251 | -3.5134 | 31.2277 | -80.6515 |
| 62 | $O_{2}^{+}-e^{-}$ | 0.1251 | -3.5134 | 31.2277 | -80.6515 |
| 63 | $O_{2}^{+}-N^{+}$ | 0.1251 | -3.5134 | 31.2277 | -80.6515 |
| 64 | $O_{2}^{+}-O^{+}$ | 0.1251 | -3.5134 | 31.2277 | -80.6515 |
| 65 | $O_{2}^{+}-N_{2}^{+}$ | 0.1251 | -3.5134 | 31.2277 | -80.6515 |
| 66 | $O_{2}^{+}-O_{2}^{+}$ | 0.1251 | -3.5134 | 31.2277 | -80.6515 |

$\dagger$ Cross sections are obtained in $\AA^{2} ; 1 \AA^{2}=10^{-16} \mathrm{~cm}^{2}$. Collision cross sections obtained from these curve-fits are for an electron pressure of 1 atm . For different electron pressures, the cross sections should be corrected by the formula given in the main text when the interacting pair of species are both ions or electrons or a combination of the two. Note that cross sections for $N_{2}$ and $O_{2}^{+}$are taken to be the same.
$\dagger \dagger$ Cross section Nos. 1-15 are used in a 5 -species air model and Nos. 1-28 in a 7 -species model.
$\ddagger$ The temperature range for all curve fits is $1000 \leq T \leq 30000 \mathrm{~K}$, except where noted.

Table VIII. Curve-Fit Constants for Collision Cross-Section, $\bar{\Omega}_{i j}^{(2,2)} \dagger$

| $\overline{\text { No. } \dagger \dagger}$ | $\begin{gathered} \hline \text { Interaction } \\ \text { Pair (i-j) } \\ \hline \end{gathered}$ | ${ }^{A} \bar{\Omega}^{(1,2}{ }^{(2)}$ | ${ }^{B} \bar{\Omega}^{(i j 2)}$ | $C_{\bar{\Omega}_{i j}^{(2,2)}}$ | $\bar{D}_{\bar{\Omega}^{(i j, 2)}}$ | $\begin{gathered} \hline \text { Temperature } \\ \text { Range, } \mathrm{K} \ddagger \\ \hline \end{gathered}$ |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| 1 | $\mathrm{N}_{2}-\mathrm{N}_{2}$ | 0.0 | -0.0203 | 0.0683 | 4.0900 |  |
| 2 | $\mathrm{O}_{2}-\mathrm{N}_{2}$ | 0.0 | -0.0558 | 0.7590 | 0.8955 |  |
| 3 | $\mathrm{O}_{2}-\mathrm{O}_{2}$ | 0.0 | -0.0485 | 0.6475 | 1.2607 |  |
| 4 | $N-N_{2}$ | 0.0 | -0.0190 | 0.0239 | 4.1782 |  |
| 5 | $\mathrm{N}-\mathrm{O}_{2}$ | 0.0 | -0.0203 | 0.0730 | 3.8818 |  |
| 6 | $N-N$ | 0.0 | -0.0118 | -0.0960 | 4.3252 |  |
| 7 | $\mathrm{O}-\mathrm{N}_{2}$ | 0.0 | -0.0169 | -0.0143 | 4.4195 |  |
| 8 | $\mathrm{O}-\mathrm{O}_{2}$ | 0.0 | -0.0247 | 0.1783 | 3.2517 |  |
| 9 | $0-N$ | 0.0 | 0.0065 | -0.4467 | 6.0426 |  |
| 10 | O-O | 0.0 | -0.0207 | 0.0780 | 3.5658 |  |
| 11 | $\mathrm{NO}-\mathrm{N}_{2}$ | 0.0 | -0.0385 | 0.4226 | 2.4507 |  |
| 12 | $\mathrm{NO}-\mathrm{O}_{2}$ | 0.0 | -0.0522 | 0.7045 | 1.0738 |  |
| 13 | NO-N | 0.0 | -0.0196 | 0.0478 | 4.0321 |  |
| 14 | NO-O | 0.0 | -0.0203 | 0.0730 | 3.8818 |  |
| 15 | NO-NO | 0.0 | -0.0453 | 0.5624 | 1.7669 |  |
| 16 | $\mathrm{NO}^{+}-\mathrm{N}_{2}$ | 0.0 | 0.0 | -0.4000 | 6.7760 |  |
| 17 | $\mathrm{NO}^{+}-\mathrm{O}_{2}$ | 0.0 | 0.0 | -0.4000 | 6.7760 |  |
| 18 | $\mathrm{NO}^{+}-\mathrm{N}$ | 0.0 | 0.0 | -0.4000 | 6.7760 |  |
| 19 | $\mathrm{NO}^{+}-\mathrm{O}$ | 0.0 | 0.0 | -0.4000 | 6.7760 |  |
| 20 | $\mathrm{NO}^{+}-\mathrm{NO}$ | 0.0 | 0.0 | -0.4000 | 6.7760 |  |
| 21 | $\mathrm{NO}^{+}-\mathrm{NO}^{+}$ | 0.1251 | -3.5135 | 31.2281 | -80.1163 |  |
| 22 | $e^{-}-N_{2}$ | 0.1147 | -2.8945 | 24.5080 | -67.3691 |  |
| 23 | $e^{-}-\mathrm{O}_{2}$ | 0.0241 | -0.3467 | 1.3887 | -0.0110 | 1000-9000 |
|  |  | 0.0025 | -0.0742 | 0.7235 | -0.2116 | 9000-30000 |
| 24 | $e^{-}-N$ | 0.0 | 0.0 | 0.0 | 1.6094 |  |
| 25 | $e^{-}-0$ | 0.0164 | -0.2431 | 1.1231 | -1.5561 | 1000-9000 |
|  |  | -0.2027 | 5.6428 | -51.5646 | 155.6091 | 9000-30000 |
| 26 | $e^{-}-N O$ | -0.2202 | 5.2265 | -40.5659 | 104.7126 | 1000-8000 |
|  |  | -0.2871 | 8.3757 | -81.3787 | 265.6292 | 8000-30000 |
| 27 | $e^{-}-\mathrm{NO}^{+}$ | 0.1251 | -3.5134 | 31.2274 | -80.1684 |  |
| 28 | $e^{-}-e^{-}$ | 0.1251 | -3.5134 | 31.2274 | -80.1684 |  |
| 29 | $N^{+}-N_{2}$ | 0.0 | 0.0 | -0.4000 | 6.7760 |  |
| 30 | $\mathrm{N}^{+}-\mathrm{O}_{2}$ | 0.0 | 0.0 | -0.4000 | 6.7760 |  |
| 31 | $N^{+}-N$ | 0.0 | 0.0 | -0.4146 | 6.9078 |  |
| 32 | $N^{+}-0$ | 0.0 | 0.0 | -0.4000 | 6.7760 |  |
| 33 | $N^{+}-\mathrm{NO}$ | 0.0 | 0.0 | -0.4000 | 6.7760 |  |
| 34 | $\mathrm{N}^{+}-\mathrm{NO}^{+}$ | 0.1251 | -3.5135 | 31.2281 | -80.1163 |  |
| 35 | $N^{+}-e^{-}$ | 0.1251 | -3.5134 | 31.2274 | -80.1684 |  |
| 36 | $N^{+}-N^{+}$ | 0.1251 | -3.5135 | 31.2281 | -80.1163 |  |
| 37 | $\mathrm{O}^{+}-\mathrm{N}_{2}$ | 0.0 | 0.0 | -0.4000 | 6.7760 |  |
| 38 | $\mathrm{O}^{+}-\mathrm{O}_{2}$ | 0.0 | 0.0 | -0.4000 | 6.7760 |  |
| 39 | $\mathrm{O}^{+}-\mathrm{N}$ | 0.0 | 0.0 | -0.4000 | 6.7760 |  |
| 40 | $\mathrm{O}^{+}-\mathrm{O}$ | 0.0 | 0.0 | -0.4235 | 6.7787 |  |
| 41 | $\mathrm{O}^{+}-\mathrm{NO}$ | 0.0 | 0.0 | -0.4000 | 6.7760 |  |
| 42 | $\mathrm{O}^{+}-\mathrm{NO}^{+}$ | 0.1251 | -3.5135 | 31.2281 | -80.1163 |  |


| 43 | $O^{+}-e^{-}$ | 0.1251 | -3.5134 | 31.2274 | -80.1684 |
| :--- | :--- | :--- | :--- | :--- | ---: |
| 44 | $O^{+}-N^{+}$ | 0.1251 | -3.5135 | 31.2281 | -80.1163 |
| 45 | $O^{+}-O^{+}$ | 0.1251 | -3.5135 | 31.2281 | -80.1163 |
| 46 | $N_{2}^{+}-N_{2}$ | 0.0 | 0.0 | -0.4000 | 6.7760 |
| 47 | $N_{2}^{+}-O_{2}$ | 0.0 | 0.0 | -0.4000 | 6.7760 |
| 48 | $N_{2}^{+}-N$ | 0.0 | 0.0 | -0.4000 | 6.7760 |
| 49 | $N_{2}^{+}-O$ | 0.0 | 0.0 | -0.4000 | 6.7760 |
| 50 | $N_{2}^{+}-N O$ | 0.0 | -0.4000 | 6.7760 |  |
| 51 | $N_{2}^{+}-N O^{+}$ | 0.1251 | -3.5135 | 31.2281 | -80.1163 |
| 52 | $N_{2}^{+}-e^{-}$ | 0.1251 | -3.5134 | 31.2274 | -80.1684 |
| 53 | $N_{2}^{+}-N^{+}$ | 0.1251 | -3.5135 | 31.2281 | -80.1163 |
| 54 | $N_{2}^{+}-O^{+}$ | 0.1251 | -3.5135 | 31.2281 | -80.1163 |
| 55 | $N_{2}^{+}-N_{2}^{+}$ | 0.0 | 0.0 | -0.4000 | -80.1163 |
| 56 | $O_{2}^{+}-N_{2}$ | 0.0 | 0.0 | -0.4000 | 6.7760 |
| 57 | $O_{2}^{+}-O_{2}$ | 0.0 | 0.0 | -0.4000 | 6.7760 |
| 58 | $O_{2}^{+}-N$ | 0.0 | -0.4000 | 6.7760 |  |
| 59 | $O_{2}^{+}-O$ | 0.1251 | -3.5135 | -0.4000 | 6.7760 |
| 60 | $O_{2}^{+}-N O$ | 0.1251 | -3.5135 | 31.2281 | -80.1163 |
| 61 | $O_{2}^{+}-N O^{+}$ | 0.1251 | -3.5135 | 31.2281 | -80.1163 |
| 62 | $O_{2}^{+}-e^{-}$ | 0.1251 | -3.5135 | 31.2281 | -80.1163 |
| 63 | $O_{2}^{+}-N^{+}$ | 0.1251 | -3.5135 | 31.2281 | -80.1163 |
| 64 | $O_{2}^{+}-O^{+}$ | 0.1251 | -3.5135 | 31.2281 | -80.1163 |
| 65 | $O_{2}^{+}-N_{2}^{+}$ |  |  |  |  |
| 66 | $O_{2}^{+}-O_{2}^{+}$ |  |  |  |  |

$\dagger$ Cross sections are obtained in $\AA^{2} ; 1 \AA^{2}=10^{-16} \mathrm{~cm}^{2}$. Collision cross sections obtained from these curve-fits are for an electron pressure of 1 atm . For different electron pressures, the cross sections should be corrected by the formula given in the main text when the interacting pair of species are both ions or electrons or a combination of the two. Note that cross sections for $N_{2}^{+}$and $O_{2}^{+}$are taken to be the same.
$\dagger+$ Cross section Nos. 1-15 are used in a 5 -species air model and Nos. 1-28 in a 7 -species model.
$\ddagger$ The temperature range for all curve fits is $1000 \leq T \leq 30000 \mathrm{~K}$, except where noted.

Table IX. Curve-Fit Constants for Collision Cross-Section Ratio, $B_{i j}^{*} \dagger$ ( $1000 \mathrm{~K} \leq \mathrm{T} \leq 30000 \mathrm{~K}$ )

| N0.1 | Interaction Pair (i-j) | $A_{B_{i j}}$ | $B_{B_{i j}}$ | $C_{B_{i j}}$ | $D_{B_{i j}}$ |
| :---: | :---: | :---: | :---: | :---: | :---: |
| 1 | $N_{2}-N_{2}$ | 0.0 | -0.0073 | 0.1444 | -0.5625 |
| 2 | $\mathrm{O}_{2}-\mathrm{N}_{2}$ | 0.0 | -0.0019 | 0.0602 | -0.2175 |
| 3 | $\mathrm{O}_{2}-\mathrm{O}_{2}$ | 0.0 | 0.0001 | 0.0181 | -0.0306 |
| 4 | $\mathrm{N}-\mathrm{N}_{2}$ | 0.0 | 0.0043 | -0.0494 | 0.2850 |
| 5 | $\mathrm{N}-\mathrm{O}_{2}$ | 0.0 | 0.0033 | -0.0366 | 0.2332 |
| 6 | $N-N$ | 0.0 | 0.0002 | 0.0002 | 0.0537 |
| 7 | $\mathrm{O}-\mathrm{N}_{2}$ | 0.0 | 0.0042 | -0.0471 | 0.2747 |
| 8 | $\mathrm{O}-\mathrm{O}_{2}$ | 0.0 | 0.0024 | -0.0245 | 0.1808 |
| 9 | $0-N$ | 0.0 | 0.0147 | -0.2628 | 1.2943 |
| 10 | O-O | 0.0 | 0.0002 | 0.0 | 0.0549 |
| 11 | $\mathrm{NO}-\mathrm{N}_{2}$ | 0.0 | -0.0045 | 0.1010 | -0.3872 |
| 12 | $\mathrm{NO}-\mathrm{O}_{2}$ | 0.0 | -0.0010 | 0.0410 | -0.1312 |
| 13 | $N O-N$ | 0.0 | 0.0038 | -0.0425 | 0.2574 |
| 14 | NO-O | 0.0 | 0.0033 | -0.0366 | 0.2332 |
| 15 | NO-NO | 0.0 | -0.0027 | 0.0700 | -0.2553 |
| 16 | $\mathrm{NO}^{+}-\mathrm{N}_{2}$ | 0.0 | 0.0 | 0.0 | 0.1933 |
| 17 | $\mathrm{NO}^{+}-\mathrm{O}_{2}$ | 0.0 | 0.0 | 0.0 | 0.1933 |
| 18 | $\mathrm{NO}^{+}-\mathrm{N}$ | 0.0 | 0.0 | 0.0 | 0.1933 |
| 19 | $\mathrm{NO}^{+}-\mathrm{O}$ | 0.0 | 0.0 | 0.0 | 0.1933 |
| 20 | $\mathrm{NO}^{+}-\mathrm{NO}$ | 0.0 | 0.0003 | -0.0006 | 0.0632 |
| 21 | $\mathrm{NO}^{+}-\mathrm{NO}^{+}$ | 0.0 | 0.0 | 0.0 | 0.4463 |
| 22 | $e^{-}-N_{2}$ | 0.0 | 0.0 | 0.0 | 0.0 |
| 23 | $e^{-}-\mathrm{O}_{2}$ | 0.0 | 0.0 | 0.0 | 0.0 |
| 24 | $e^{-}-N$ | 0.0 | 0.0 | 0.0 | 0.0 |
| 25 | $e^{-}-0$ | 0.0 | 0.0 | 0.0 | 0.0 |
| 26 | $e^{-}-N O$ | 0.0 | 0.0 | 0.0 | 0.0 |
| 27 | $e^{-}-\mathrm{NO}^{+}$ | 0.0 | 0.0 | 0.0 | 0.4463 |
| 28 | $e^{-}-e^{-}$ | 0.0 | 0.0 | 0.0 | 0.4463 |
| 29 | $\mathrm{N}^{+}-N_{2}$ | 0.0 | 0.0 | 0.0 | 0.1933 |
| 30 | $\mathrm{N}^{+}-\mathrm{O}_{2}$ | 0.0 | 0.0 | 0.0 | 0.1933 |
| 31 | $N^{+}-N$ | 0.0 | 0.0002 | 0.0002 | 0.0537 |
| 32 | $N^{+}-\mathrm{O}$ | 0.0 | 0.0 | 0.0 | 0.1933 |
| 33 | $N^{+}-\mathrm{NO}$ | 0.0 | 0.0 | 0.0 | 0.1933 |
| 34 | $\mathrm{N}^{+}-\mathrm{NO}^{+}$ | 0.0 | 0.0 | 0.0 | 0.4463 |
| 35 | $N^{+}-e^{-}$ | 0.0 | 0.0 | 0.0 | 0.4463 |
| 36 | $N^{+}-N^{+}$ | 0.0 | 0.0 | 0.0 | 0.4463 |
| 37 | $\mathrm{O}^{+}-\mathrm{N}_{2}$ | 0.0 | 0.0 | 0.0 | 0.1933 |
| 38 | $\mathrm{O}^{+}-\mathrm{O}_{2}$ | 0.0 | 0.0 | 0.0 | 0.1933 |
| 39 | $O^{+}-N$ | 0.0 | 0.0 | 0.0 | 0.1933 |
| 40 | $O^{+}-0$ | 0.0 | 0.0002 | 0.0 | 0.0549 |
| 41 | $\mathrm{O}^{-}-\mathrm{NO}$ | 0.0 | 0.0 | 0.0 | 0.1933 |
| 42 | $\mathrm{O}^{+}-\mathrm{NO}^{+}$ | 0.0 | 0.0 | 0.0 | 0.4463 |
| 43 | $\mathrm{O}^{+}-e^{-}$ | 0.0 | 0.0 | 0.0 | 0.4463 |
| 44 | $\mathrm{O}^{+}-\mathrm{N}^{+}$ | 0.0 | 0.0 | 0.0 | 0.4463 |


| 45 | $O^{+}-O^{+}$ | 0.0 | 0.0 | 0.0 | 0.4463 |
| :--- | :--- | :--- | :--- | :--- | :--- |
| 46 | $N_{2}^{+}-N_{2}$ | 0.0 | 0.0 | 0.0 | 0.1933 |
| 47 | $N_{2}^{+}-O_{2}$ | 0.0 | 0.0 | 0.0 | 0.1933 |
| 48 | $N_{2}^{+}-N^{+}$ | 0.0 | 0.0 | 0.0 | 0.1933 |
| 49 | $N_{2}^{+}-O$ | 0.0 | 0.0 | 0.0 | 0.1933 |
| 50 | $N_{2}^{+}-N O$ | 0.0 | 0.0 | 0.0 | 0.1933 |
| 51 | $N_{2}^{+}-N O^{+}$ | 0.0 | 0.0 | 0.0 | 0.4463 |
| 52 | $N_{2}^{+}-e^{-}$ | 0.0 | 0.0 | 0.0 | 0.4463 |
| 53 | $N_{2}^{+}-N^{+}$ | 0.0 | 0.0 | 0.0 | 0.4463 |
| 54 | $N_{2}^{+}-O^{+}$ | 0.0 | 0.0 | 0.0 | 0.4463 |
| 55 | $N_{2}^{+}-N_{2}^{+}$ | 0.0 | 0.0 | 0.0 | 0.4463 |
| 56 | $O_{2}^{+}-N_{2}$ | 0.0 | 0.0 | 0.0 | 0.1933 |
| 57 | $O_{2}^{+}-O_{2}$ | 0.0 | 0.0 | 0.0 | 0.1933 |
| 58 | $O_{2}^{+}-N^{2}$ | 0.0 | 0.0 | 0.0 | 0.1933 |
| 59 | $O_{2}^{+}-O$ | 0.0 | 0.0 | 0.0 | 0.1933 |
| 60 | $O_{2}^{+}-N O$ | 0.0 | 0.0 | 0.0 | 0.1933 |
| 61 | $O_{2}^{+}-N O^{+}$ | 0.0 | 0.0 | 0.0 | 0.4463 |
| 62 | $O_{2}^{+}-e^{-}$ | 0.0 | 0.0 | 0.0 | 0.4463 |
| 63 | $O_{2}^{+}-N^{+}$ | 0.0 | 0.0 | 0.0 | 0.4463 |
| 64 | $O_{2}^{+}-O^{+}$ | 0.0 | 0.0 | 0.0 | 0.4463 |
| 65 | $O_{2}^{+}-N_{2}^{+}$ | 0.0 | 0.0 | 0.0 | 0.4463 |
| 66 | $O_{2}^{+}-O_{2}^{+}$ | 0.0 | 0.0 | 0.0 | 0.4463 |
|  |  |  |  |  |  |

$\dagger$ The collision cross section ratios are dimensionless parameters and are valid as given for all electron pressures.
$\dagger \dagger$ Cross section Nos. 1-15 are used in a 5 -species air model and Nos. 1-28 in a 7 -species model.

| Regions with chemical and thermal nonequilibrium |  |
| :---: | :--- |
| Region | Aerothermal phenomenon |
| (A) | Chemical and thermal equilibrium |
| (B) | Chemical nonequilibrium <br> with thermal equilibrium |
| (C) |  |
| Chemical and thermal |  |
| nonequilibrium |  |


Figure 1. Flight stagnation region air chemistry (adapted from ref. 5)

Figure 2. Specific heats of monatomic and diatomic nitrogen with contributions from the excitation of different energy modes.


(b) Diatomic nitrogen.
Figure 3. Continued.

(c) Nitric oxide.
Figure 3. Concluded.

(a) Diatomic oxygen.
Figure 4. Curve fit to the viscosity values obtained by employing the collision cross sections based on the data of Yos (ref. 32).

Figure 4. Continued.

(c) Ionized nitric oxide.
Figure 4. Continued.

(d) Electron.
Figure 4. Concluded.




[^10]
(c) Ionized nitric oxide.

Figure 5. Continued.

(d) Electron.
Figure 5. Concluded.


Figure 6. Comparison of the viscosity of equilibrium air at 1 atmosphere.


Figure 7. Comparison of the frozen thermal conductivity of equilibrium air at 1 atmosphere.
Computed:

- $\pi \bar{\Omega}_{i j}^{(1,1)}$
$-(2,2)$

Figure 8. Curve fit to the computed values of collision integrals, collision integral ratio, and binary diffusion coefficient obtained by employing
the data of Yos (ref. 32)
a) Neutral-neutral molecular interaction: $\mathrm{O}_{2} \leftrightarrow \mathrm{O}_{2}$

(c) Ion-ion molecular interaction: $\mathrm{NO}^{+} \leftrightarrow \mathrm{NO}^{+}$
Figure 8. Continued.
Computed:
$\circ \triangleleft \square \diamond \mid$



(e) Electron-electron interaction: $e^{-} \leftrightarrow e^{-}$
Figure 8. Concluded.



[^0]:    $\dagger$ See Appendix A for the various definitions.

[^1]:    $\ddagger$ The collision cross sections designated here as $\pi \bar{\Omega}_{i j}^{(l, s)}$ are the same as $\pi \sigma^{2} \Omega_{i j}^{(l, s)^{*}}$

[^2]:    + With $A^{*}=5 / 3$ and $5 / 2, A_{i j}$ becomes identically equal to zero in the Chapman-Enskog formula.

[^3]:    + See Appendix A for various definitions

[^4]:    + The approximations of references 41 through 43 may be valid only for the range of conditions for which they have been developed and not for general application because of the very approximate analysis of the nondiagonal matrix elements $A_{i j}$ of equation (27).

[^5]:    $\Varangle$ Here we have used the sign convention that the heat flux vector is positive in the normal direction away from the surface.

[^6]:    + The formula for $K r$ given here already includes the effects of ambipolar diffusion (ref. 51) on the reaction conductivity of an ionized gas.

[^7]:    $\dagger$ Dr. Ken Sutton of NASA Langley Research Center provided these definitions in an unpublished memo.

[^8]:    $\dagger$ Electron mass $m_{e}$ is related to the electron molecular weight $M_{e}$ through the relation $m_{e}=M_{e} / N_{A}$, where $N_{A}=6.02 \times 10^{23}$ molecules/gm-mole is the Avogadro's number.

[^9]:    $\dagger$ Reactions and reaction rates for Nos. 1-7 are from Blottner's (ref. 13) 7-species chemical model and Nos. 8-20 are from reference 17.

[^10]:    (b) Diatomic nitrogen.

    Figure 5. Continued.

