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TABLE OF CONTENTS

P	'n	ø	e
Τ.	ч	-	v

TECHNOLOGY TEST BED REVIEW (H.V. McConnaughey)	1
ADVANCED SOLID ROCKET MOTOR PROJECT STATUS (K.D. Coates)	27
SPACE TRANSPORTATION MAIN ENGINE (J.C. Monk)	45
THE IMPACT OF TIME STEP DEFINITION ON CODE CONVERGENCE AND ROBUSTNESS (S. Venkateswaran, J.M. Weiss, and C.L. Merkle)	83
DEVELOPMENT OF CFD CODE EVALUATION CRITERIA AND A PROCEDURE FOR ASSESSING PREDICTIVE CAPABILITY AND PERFORMANCE (S.J. Lin, D.C. Chan, M.M. Sindir, and S.L. Barson)	109
COMPARISON BETWEEN THE PISO ALGORITHM AND PRECONDITIONING METHODS FOR COMPRESSIBLE FLOW (C.L. Merkle, P.E.O. Buelow, and S. Venkateswaran)	123
A COMPARISON OF ARTIFICIAL COMPRESSIBILITY AND FRACTIONAL STEP METHODS FOR INCOMPRESSIBLE FLOW COMPUTATIONS (D.C. Chan, A.D. Darian, and M.M. Sindir)	147
A STATUS OF THE ACTIVITIES OF THE NASA/MSFC PUMP STAGE TECHNOLOGY TEAM (R. Garcia, R.W. Williams, and Y. Dakhoul)	173
CFD ANALYSIS OF PUMP CONSORTIUM IMPELLER (G.C. Cheng, Y.S. Chen, and R.W. Williams)	201
CFD APPLICATIONS IN PUMP FLOWS (C. Kiris, L. Chang, and D. Kwak)	219
COMPUTATION OF THE FLOW FIELD IN A CENTRIFUGAL IMPELLER WITH SPLITTER BLADES (F.J. de Jong, SK. Choi, T.R. Govindan, and J.S. Sabnis)	245
IMPELLER TANDEM BLADE STUDY WITH GRID EMBEDDING FOR LOCAL GRID REFINEMENT (G. Bache')	259
THREE-DIMENSIONAL FLOW FIELDS INSIDE A SHROUDED INDUCER AT DESIGN AND OFF-DESIGN CONDITIONS (CFD STUDY) (C. Hah, O. Kwon, D.A. Greenwald, and R. Garcia)	289
EFFECTS OF CURVATURE AND ROTATION ON TURBULENCE IN THE NASA LOW-SPEED CENTRIFUGAL COMPRESSOR IMPELLER (J.G. Moore and J. Moore)	315
COMPUTATIONAL FLUID DYNAMIC DESIGN OF ROCKET ENGINE PUMP COMPONENTS (W.C. Chen, G.H. Prueger, D.C. Chan, and A.H. Eastland)	339

1.

The second second

	Pag
SSME HPOTP IMPELLER BACKCAVITY CFD ANALYSIS (W.W. Hsu and S.J. Lin)	36
NLS CLUTCHING BEARING CAVITY FLOW ANALYSIS (K. Tran, D.C. Chan, and A. Darian)	38
CFD ANALYSIS TO OPTIMIZE A DESIGN MODIFICATION OF BSMT (M. Ratcliff, R. Avva, and R. Williams)	41
COMBUSTION INSTABILITY ANALYSIS FOR LIQUID PROPELLANT ROCKET ENGINES (Y.M. Kim, C.P. Chen, and J.P. Ziebarth)	44
INVERSE DESIGN OF A PROPER NUMBER, SHAPES, SIZES, AND LOCATIONS OF COOLANT FLOW PASSAGES (G.S. Dulikravich)	46
NUMERICAL ANALYSIS OF THE HOT-GAS-SIDE AND COOLANT-SIDE HEAT TRANSFER IN LIQUID ROCKET ENGINE COMBUSTORS (T.S. Wang and V. Luong)	48
AN EFFICIENT AND ROBUST GRID OPTIMIZATION ALGORITHM (B.K. Soni and S. Yang)	50
ENHANCEMENTS TO THE GRIDGEN STRUCTURED GRID GENERATION SYSTEM FOR INTERNAL AND EXTERNAL FLOW APPLICATIONS (J.P. Steinbrenner and J.R. Chawner)	54
CAGI: COMPUTER AIDED GRID INTERFACE—A WORK IN PROGRESS (B.K. Soni, TY. Yu, and D. Vaughn)	57
USING ADAPTIVE GRID IN MODELING ROCKET NOZZLE FLOW (A.S. Chow and KR. Jin)	61
COMPLEX THREE-DIMENSIONAL INTERNAL FLOWS IN THE ASRM AND RSRM AFT END SEGMENTS (E.J. Reske, D.F. Billings, and J.W. Cornelison)	64
AN ANALYSIS OF THE FLOW FIELD IN THE REGION OF THE ASRM FIELD JOINTS (R.A. Dill and H.R. Whitesides)	66
EFFECT OF INCLUDING VARIABLE GAS PROPERTIES AND ENTRAINED PARTICLES IN THE FLOW ANALYSIS OF THE ASRM NOZZLE (C.D. Clayton)	68
A TWO-PHASE RESTRICTED EQUILIBRIUM MODEL FOR COMBUSTION OF METALIZED SOLID PROPELLANTS (J.S. Sabnis, F.J. de Jong, and H.J. Gibeling)	71

Page

CURRENT STATUS OF THE DEVELOPMENT OF AN IGNITION TRANSIENT MODEL FOR SOLID ROCKET MOTORS (G.D. Luke and H.A. Dwyer)	725
SRMAFTE FACILITY CHECKOUT MODEL FLOW FIELD ANALYSIS (R.A. Dill and H.R. Whitesides)	763
A COMPARATIVE STUDY OF THE EFFECTS OF INHIBITOR STUB LENGTH ON SOLID ROCKET MOTOR COMBUSTION CHAMBER PRESSURE OSCILLATIONS: RSRM AT T=80 SECONDS, PRELIMINARY RESULTS (D. Chasman, D. Burnette, J. Holt, and R. Farr)	787
OVERVIEW OF THE RELEVANT CFD WORK AT THIOKOL CORPORATION (P. Chwalowski and HT. Loh)	79 2
A STATUS OF THE ACTIVITIES OF THE NASA/MSFC COMBUSTION DEVICES TECHNOLOGY TEAM (P.K. Tucker)	807
CFD ANALYSIS OF THE STME NOZZLE FLOWFIELD (A. Krishnan, P.K. Tucker)	83
NLS NOZZLE BASE FLOW CHARACTERISTICS (J.J. Erhart)	84
HEAT TRANSFER IN ROCKET ENGINE COMBUSTION CHAMBERS AND NOZZLES (P.G. Anderson, Y.S. Chen, and R.C. Farmer)	86.
APPLICATION OF COMPUTATIONAL FLUID DYNAMICS TO THE DESIGN OF THE FILM COOLED STME SUBSCALE NOZZLE FOR THE NATIONAL LAUNCH SYSTEM (J.L. Garrett)	89
COMPUTATIONAL FLUID DYNAMICS ANALYSIS OF SPACE SHUTTLE MAIN ENGINE MULTIPLE PLUME FLOWS AT HIGH-ALTITUDE FLIGHT CONDITIONS (N.S. Dougherty, J.B. Holt, B.L. Liu, and S.L. Johnson)	92:
DIRECT NUMERICAL SIMULATION OF A COMBUSTING DROPLET WITH CONVECTION (P.Y. Liang)	94:
A NUMERICAL MODEL FOR ATOMIZATION-SPRAY COUPLING IN LIQUID ROCKET THRUST CHAMBERS (M.G. Giridharan, A. Krishnan, J.J. Lee, A.J. Przekwas, and K. Gross)	96
NUMERICAL MODELING FOR DILUTE AND DENSE SPRAYS (C.P. Chen, Y.M. Kim, H.M. Shang, J.P. Ziebarth, and T.S. Wang)	98
MODELING OF SSME FUEL PREBURNER ASI (P.Y. Liang)	101

ľ

CFD MODELING OF TURBULENT FLOWS AROUND THE SSME MAIN INJECTOR ASSEMBLY USING POROSITY FORMULATION (G.C. Cheng, Y.S. Chen, and J.H. Ruf)	
COMPUTATIONAL FLUID DYNAMICS ANALYSIS OF SSME PHASE II AND PHASE II+ PREBURNER INJECTOR ELEMENT HYDROGEN FLOW PATHS (J. H. Ruf)	••••
STME HYDROGEN MIXER STUDY (R. Blumenthal, D. Kim, and G. Bache')	•••
AN EXPERIMENTAL STUDY OF THE FLUID MECHANICS ASSOCIATED WITH POROUS WALLS. (N. Ramachandran, J. Heaman, and A. Smith)	•••
EXPERIMENTAL STUDIES OF CHARACTERISTIC COMBUSTION-DRIVEN FLOWS FOR CFD VALIDATION (R.J. Santoro, M. Moser, W. Anderson, S. Pal, H. Ryan, and C.L. Merkle)	•••
TURBINE DISK CAVITY AERODYNAMICS AND HEAT TRANSFER (B.V. Johnson and W.A. Daniels)	•••
A NUMERICAL STUDY OF TWO-DIMENSIONAL VORTEX SHEDDING FROM RECTANGULAR CYLINDERS (A.H. Hadid, M.M. Sindir, and R.I. Issa)	•••
A STATUS OF THE TURBINE TECHNOLOGY TEAM ACTIVITIES (L.W. Griffin)	•••
A CRITICAL EVALUATION OF A THREE-DIMENSIONAL NAVIER-STOKES CFD AS A TOOL TO DESIGN SUPERSONIC TURBINE STAGES (C. Hah, O. Kwon, and M. Shoemaker)	•••
NAVIER-STOKES ANALYSIS OF AN OXIDIZER TURBINE BLADE WITH TIP CLEARANCE (H.J. Gibeling and J.S. Sabnis)	•••
NUMERICAL SIMULATION OF TURBOMACHINERY FLOWS WITH ADVANCED TURBULENCE MODELS (B. Lakshminarayana, R. Kunz, J. Luo, and S. Fan)	••••
DEVELOPMENT OF A CFD CODE FOR INTERNAL FLOWS IN LIQUID FUELED ENGINES (Y. Dakhoul)	
DEVELOPMENT OF THE KIVA-II CFD CODE FOR ROCKET PROPULSION APPLICATIONS (R.V. Shannon, Jr. and A.L. Murray)	
A COMPUTATIONAL DESIGN SYSTEM FOR RAPID CFD ANALYSIS (E.P. Ascoli, S.L. Barson, M.E. DeCroix, and M.M. Sindir)	
OPTIMUM DESIGN OF NINETY DEGREE BENDS (V. Modi)	••••

	Page
A MULTIDOMAIN METHOD FOR SUBSONIC VISCOUS FLOWS (D.C. Chan and M.M. Sindir)	1427
LARGE EDDY SIMULATION OF COMPRESSIBLE TURBULENT CHANNEL FLOWS (R.A. Beddini and J.P. Ridder)	1453
TREATING CONVECTION IN SEQUENTIAL SOLVERS (W. Shyy and S. Thakur)	1469

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Current Status of the Development of an Ignition

Transient Model for Solid Rocket Motors

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An ignition transient model for solid rocket motors is currently being developed jointly by the Aerojet ASRM Division and the University of California at Davis. Though the CFD code will be general enough to predict the start transient for most solid rocket motors, the particular motive for the development of this code stems from the desire to analyze the flow field within the Advanced Solid Rocket Motor (ASRM) for the Space Shuttle with all its geometric complexity. The star grain configuration in the head end of the ASRM coupled with the multiport igniter creates a formidable problem which can only be modeled accurately using a three dimensional Navier-Stokes code if one wishes to preserve both volume and burning surface area as a function of axial position down the bore. The actual physical geometry is crucial in modeling the multiple wave interactions occurring within the combustion chamber as well as in predicting the correct amount of mass, momentum, and energy injected as a function of time and space at the propellant surface.

The primary objectives of the CFD code are to calculate the pressure rise rate, the thrust rise rate, and the maximum chamber pressure which occurs during the first second of the ASRM action time. And, more specifically, to determine the relative difference between the ignition transients produced using a single port igniter and that produced by a multiport igniter.

An implicit, three dimensional, time accurate, finite volume method is being developed to solve this problem. Current plans are to use an ADI technique, with replacement, to solve the set of analytically linearized full Navier-Stokes equations. However, to gain an understanding of which features of the code need more attention than others, and to provide an inexpensive, quick tool for studying the time accuracy of the selected solution algorithm, a one dimensional version of the code was written first. The various features of the one dimensional code were validated by comparing the numerical results to analytical results for problems where exact solutions were available. Then the one dimensional code was used to perform some sensitivity studies to help develop an understanding of the complex wave interactions occurring within the solid rocket motor.

This presentation will discuss the results obtained from the one dimensional code and the plans for the development of the 3-D code.





OBJECTIVES

- Develop Ignition Transient Model(s) to Characterize the Start Transient for Solid Rocket Motors
- Determine Relative Differences Between the Ignition Transients Produced Using Single (RSRM) and Multiport (ASRM) gniters

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- Instantaneous Pressure Rise Rate
- **Corresponding Thrust Rise Rate**
- Maximum Chamber Pressure
- Where Fins and Igniter are Located Details of Flow Field in Head End for **RSRM** and **ASRM**



THREE PART MODELING APPROACH	1. Preliminary Analysis with Existing	General 3-D Navier-Stokes Solver (CONTINUSYS Code)	 Develop 1-D "Engineering Workhorse" Ignition Transient Code 	 Bevelop ^rFull 3-D Ignition Transient Code Using Same Methodology as 1-D Code 	T.	Only 1-D Code Discussed Today
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- Provide Quick, Efficient Tool for Performing Sensitivity Studies ▲
- **Establish Bounds for Problem Through** Parametric Studies
- **Evaluate Various Numerical Schemes** Prior to Incorporation into 3-D Code
- Requiring More Attention During Development Determine Which Factors are Most Influential, of 3-D Code



	Ā	ESCRIPTION OF NUMERICAL MODEL
		Implicit, Time Dependent, Finite Volume Method
		Modular Format for Flexibility
731		Currently Contains Centered Scheme with Explicit Artificial Dissipation
		System of Equations Solved Using Alternating Direction Implicit (ADI) with Replacement (Essentially a Direct Solver for 1-D Case)
		COORDED - VENORET - NUM

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Governing Equations in Integral Form

Continuity
$$\frac{\partial}{\partial t} \iint \int \int_{v} p dv + \iint \int_{s} p \vec{u} \cdot \vec{n} dA = \iint_{A_p} \dot{r} p_p dA_p$$

X-Momentum
$$\frac{\partial}{\partial t} \iint \int \int p \vec{u} dV + \iint s p \vec{u} (\vec{u} \cdot \vec{n}) dA = -\vec{n} \iint s p dA - \iint s u dA_w - \iint s \tau_{xx} dA$$

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Energy

$$\frac{\partial}{\partial t} \int \int \int_{V} pe \, dV + \int \int_{S} [pe+P](\vec{u} \cdot \vec{n}) \, dA = \int \int_{W} q_w \, dA_w + \int \int_{S} q_x \, dA + \int \int_{A_p} \dot{r} \, p_P \, H_P \, dA_P$$

 $e = C_v T + u^2/2$ where

Equation of State

 $P = \rho RT$





Analytically Linearized Using Newton's Method

where:
$$\hat{U} \equiv \text{ primitive variable vector} = \begin{bmatrix} \rho \\ \rho e \end{bmatrix} \hat{F} \equiv \text{flux vector} = \begin{bmatrix} \rho u^2 + P \\ (\rho e + P)u \end{bmatrix}$$

$$\tilde{J} \equiv \text{Jacobian Matrix} = \begin{bmatrix} \partial \hat{F} \\ \partial \hat{U} \end{bmatrix}$$
$$\tilde{I} \land \rho_P A_P]_{\hat{I}}^{\hat{n}} = \begin{bmatrix} \hat{I} \hat{F} \\ (\rho e + P)u \end{bmatrix}$$
$$\tilde{I} \land \rho_P A_P]_{\hat{I}}^{\hat{n}} = \begin{bmatrix} \hat{I} \hat{F} \\ (\rho e + P)u \end{bmatrix}$$
$$\tilde{S} = \begin{bmatrix} I \hat{F} \rho_P A_P]_{\hat{I}}^{\hat{n}} = \begin{bmatrix} I \rho_P A_P]_{\hat{I}}^{\hat{n}} \\ \partial \hat{X} \end{bmatrix}_{\hat{I}+1/2} - \begin{bmatrix} \mu \frac{\partial u}{\partial X} \\ \partial \hat{X} \end{bmatrix}_{\hat{I}+1/2} + \begin{bmatrix} \mu \frac{\partial u}{\partial X} \\ \partial \hat{X} \end{bmatrix}_{\hat{I}+1/2} + \begin{bmatrix} \mu \frac{\partial u}{\partial X} \\ \partial \hat{X} \end{bmatrix}_{\hat{I}+1/2} + \begin{bmatrix} -k \frac{\partial T}{\partial X} \\ \partial \hat{X} \end{bmatrix}_{\hat{I}+1/2} + \begin{bmatrix} -k \frac{\partial T}{\partial X} \\ \partial \hat{X} \end{bmatrix}_{\hat{I}+1/2} + \begin{bmatrix} -k \frac{\partial T}{\partial X} \\ \partial \hat{X} \end{bmatrix}_{\hat{I}+1/2} + \begin{bmatrix} -k \frac{\partial T}{\partial X} \\ \partial \hat{X} \end{bmatrix}_{\hat{I}+1/2} + \begin{bmatrix} -k \frac{\partial T}{\partial X} \\ \partial \hat{X} \end{bmatrix}_{\hat{I}+1/2} + \begin{bmatrix} -k \frac{\partial T}{\partial X} \\ \partial \hat{X} \end{bmatrix}_{\hat{I}+1/2} + \begin{bmatrix} -k \frac{\partial T}{\partial X} \\ \partial \hat{X} \end{bmatrix}_{\hat{I}+1/2} + \begin{bmatrix} -k \frac{\partial T}{\partial X} \\ \partial \hat{X} \end{bmatrix}_{\hat{I}+1/2} + \begin{bmatrix} -k \frac{\partial T}{\partial X} \\ \partial \hat{X} \end{bmatrix}_{\hat{I}+1/2} + \begin{bmatrix} -k \frac{\partial T}{\partial X} \\ \partial \hat{X} \end{bmatrix}_{\hat{I}+1/2} + \begin{bmatrix} -k \frac{\partial T}{\partial X} \\ \partial \hat{X} \end{bmatrix}_{\hat{I}+1/2} + \begin{bmatrix} -k \frac{\partial T}{\partial X} \\ \partial \hat{X} \end{bmatrix}_{\hat{I}+1/2} + \begin{bmatrix} -k \frac{\partial T}{\partial X} \\ \partial \hat{X} \end{bmatrix}_{\hat{I}+1/2} + \begin{bmatrix} -k \frac{\partial T}{\partial X} \\ \partial \hat{X} \end{bmatrix}_{\hat{I}+1/2} + \begin{bmatrix} -k \frac{\partial T}{\partial X} \\ \partial \hat{X} \end{bmatrix}_{\hat{I}+1/2} + \begin{bmatrix} -k \frac{\partial T}{\partial X} \\ \partial \hat{X} \end{bmatrix}_{\hat{I}+1/2} + \begin{bmatrix} -k \frac{\partial T}{\partial X} \\ \partial \hat{X} \end{bmatrix}_{\hat{I}+1/2} + \begin{bmatrix} -k \frac{\partial T}{\partial X} \\ \partial \hat{X} \end{bmatrix}_{\hat{I}+1/2} + \begin{bmatrix} -k \frac{\partial T}{\partial X} \\ \partial \hat{X} \end{bmatrix}_{\hat{I}+1/2} + \begin{bmatrix} -k \frac{\partial T}{\partial X} \\ \partial \hat{X} \end{bmatrix}_{\hat{I}+1/2} + \begin{bmatrix} -k \frac{\partial T}{\partial X} \\ \partial \hat{X} \end{bmatrix}_{\hat{I}+1/2} + \begin{bmatrix} -k \frac{\partial T}{\partial X} \\ \partial \hat{X} \end{bmatrix}_{\hat{I}+1/2} + \begin{bmatrix} -k \frac{\partial T}{\partial X} \\ \partial \hat{X} \end{bmatrix}_{\hat{I}+1/2} + \begin{bmatrix} -k \frac{\partial T}{\partial X} \\ \partial \hat{X} \end{bmatrix}_{\hat{I}+1/2} + \begin{bmatrix} -k \frac{\partial T}{\partial X} \\ \partial \hat{X} \end{bmatrix}_{\hat{I}+1/2} + \begin{bmatrix} -k \frac{\partial T}{\partial X} \\ \partial \hat{X} \end{bmatrix}_{\hat{I}+1/2} + \begin{bmatrix} -k \frac{\partial T}{\partial X} \\ \partial \hat{X} \end{bmatrix}_{\hat{I}+1/2} + \begin{bmatrix} -k \frac{\partial T}{\partial X} \\ \partial \hat{X} \end{bmatrix}_{\hat{I}+1/2} + \begin{bmatrix} -k \frac{\partial T}{\partial X} \\ \partial \hat{X} \end{bmatrix}_{\hat{I}+1/2} + \begin{bmatrix} -k \frac{\partial T}{\partial X} \\ \partial \hat{X} \end{bmatrix}_{\hat{I}+1/2} + \begin{bmatrix} -k \frac{\partial T}{\partial X} \\ \partial \hat{X} \end{bmatrix}_{\hat{I}+1/2} + \begin{bmatrix} -k \frac{\partial T}{\partial X} \\ \partial \hat{X} \end{bmatrix}_{\hat{I}+1/2} + \begin{bmatrix} -k \frac{\partial T}{\partial X} \\ \partial \hat{X} \end{bmatrix}_{\hat{I}+1/2} + \begin{bmatrix} -k \frac{\partial T}{\partial X} \\ \partial \hat{X} \end{bmatrix}_{\hat{I}+1/2} + \begin{bmatrix} -k \frac{\partial T}{\partial X} \\ \partial \hat{X} \end{bmatrix}_{\hat{I}+1/2} + \begin{bmatrix} -k \frac{\partial T}{\partial X} \\ \partial \hat{X} \end{bmatrix}_{\hat{I}+1/2} + \begin{bmatrix} -k \frac{\partial T}{\partial X} \\ \partial \hat{X} \end{bmatrix}_{\hat{I}+1/2} + \begin{bmatrix} -k \frac{\partial T}{\partial X} \\ \partial \hat{X} \end{bmatrix}_{\hat{$$

Linearized Form of Discrete Equations

 $-\frac{A_{i-1}\alpha}{2} \begin{bmatrix} \overline{J}_{i-1} \\ J_{i-1} \end{bmatrix} \left(\Delta \ \widehat{U}_{i-1}^{n+1} \right) + \left\{ \frac{A_{i} \ \Delta X_{i}}{\Delta t} \begin{bmatrix} \overline{I} \\ \overline{I} \end{bmatrix} + \left(\frac{A_{i+1}\alpha - A_{i-1}\alpha}{2} \right) \begin{bmatrix} J_{i} \\ J_{i} \end{bmatrix} \right\} \left(\Delta \ \widehat{U}_{i}^{n+1} \right) + \frac{A_{i+1}\alpha}{2} \begin{bmatrix} J_{i+1} \\ J_{i+1} \end{bmatrix} \left(\Delta \ \widehat{U}_{i+1}^{n+1} \right) + \frac{A_{i+1}\alpha}{2} \begin{bmatrix} J_{i+1} \\ J_{i+1} \end{bmatrix} \left(\Delta \ \widehat{U}_{i+1}^{n+1} \right) + \frac{A_{i-1}\alpha}{2} \begin{bmatrix} J_{i+1} \\ J_{i+1} \end{bmatrix} \left(\Delta \ \widehat{U}_{i+1}^{n+1} \right) + \frac{A_{i-1}\alpha}{2} \begin{bmatrix} J_{i+1} \\ J_{i+1} \end{bmatrix} \left(\Delta \ \widehat{U}_{i+1}^{n+1} \right) + \frac{A_{i-1}\alpha}{2} \begin{bmatrix} J_{i+1} \\ J_{i+1} \end{bmatrix} \left(\Delta \ \widehat{U}_{i+1}^{n+1} \right) + \frac{A_{i-1}\alpha}{2} \begin{bmatrix} J_{i+1} \\ J_{i+1} \end{bmatrix} \left(\Delta \ \widehat{U}_{i+1}^{n+1} \right) + \frac{A_{i-1}\alpha}{2} \begin{bmatrix} J_{i+1} \\ J_{i+1} \end{bmatrix} \left(\Delta \ \widehat{U}_{i+1}^{n+1} \right) + \frac{A_{i-1}\alpha}{2} \begin{bmatrix} J_{i+1} \\ J_{i+1} \end{bmatrix} \left(\Delta \ \widehat{U}_{i+1}^{n+1} \right) + \frac{A_{i-1}\alpha}{2} \begin{bmatrix} J_{i+1} \\ J_{i+1} \end{bmatrix} \left(\Delta \ \widehat{U}_{i+1}^{n+1} \right) + \frac{A_{i-1}\alpha}{2} \begin{bmatrix} J_{i+1} \\ J_{i+1} \end{bmatrix} \left(\Delta \ \widehat{U}_{i+1}^{n+1} \right) + \frac{A_{i-1}\alpha}{2} \begin{bmatrix} J_{i+1} \\ J_{i+1} \end{bmatrix} \left(\Delta \ \widehat{U}_{i+1}^{n+1} \right) + \frac{A_{i-1}\alpha}{2} \begin{bmatrix} J_{i+1} \\ J_{i+1} \end{bmatrix} \left(\Delta \ \widehat{U}_{i+1}^{n+1} \right) + \frac{A_{i-1}\alpha}{2} \begin{bmatrix} J_{i+1} \\ J_{i+1} \end{bmatrix} \left(\Delta \ \widehat{U}_{i+1}^{n+1} \right) + \frac{A_{i-1}\alpha}{2} \begin{bmatrix} J_{i+1} \\ J_{i+1} \end{bmatrix} \left(\Delta \ \widehat{U}_{i+1}^{n+1} \right) + \frac{A_{i-1}\alpha}{2} \begin{bmatrix} J_{i+1} \\ J_{i+1} \end{bmatrix} \left(\Delta \ \widehat{U}_{i+1} \right) + \frac{A_{i+1}\alpha}{2} \begin{bmatrix} J_{i+1} \\ J_{i+1} \end{bmatrix} \left(\Delta \ \widehat{U}_{i+1} \right) + \frac{A_{i+1}\alpha}{2} \begin{bmatrix} J_{i+1} \\ J_{i+1} \end{bmatrix} \left(\Delta \ \widehat{U}_{i+1} \right) + \frac{A_{i+1}\alpha}{2} \begin{bmatrix} J_{i+1} \\ J_{i+1} \end{bmatrix} \left(\Delta \ \widehat{U}_{i+1} \right) + \frac{A_{i+1}\alpha}{2} \begin{bmatrix} J_{i+1} \\ J_{i+1} \end{bmatrix} \left(\Delta \ \widehat{U}_{i+1} \right) + \frac{A_{i+1}\alpha}{2} \begin{bmatrix} J_{i+1} \\ J_{i+1} \end{bmatrix} \left(\Delta \ \widehat{U}_{i+1} \right) + \frac{A_{i+1}\alpha}{2} \begin{bmatrix} J_{i+1} \\ J_{i+1} \end{bmatrix} \left(\Delta \ \widehat{U}_{i+1} \right) + \frac{A_{i+1}\alpha}{2} \begin{bmatrix} J_{i+1} \\ J_{i+1} \end{bmatrix} \left(\Delta \ \widehat{U}_{i+1} \right) + \frac{A_{i+1}\alpha}{2} \begin{bmatrix} J_{i+1} \\ J_{i+1} \end{bmatrix} \left(\Delta \ \widehat{U}_{i+1} \right) + \frac{A_{i+1}\alpha}{2} \begin{bmatrix} J_{i+1} \\ J_{i+1} \end{bmatrix} \left(\Delta \ \widehat{U}_{i+1} \right) + \frac{A_{i+1}\alpha}{2} \begin{bmatrix} J_{i+1} \\ J_{i+1} \end{bmatrix} \left(\Delta \ \widehat{U}_{i+1} \right) + \frac{A_{i+1}\alpha}{2} \begin{bmatrix} J_{i+1} \\ J_{i+1} \end{bmatrix} \left(\Delta \ \widehat{U}_{i+1} \right) + \frac{A_{i+1}\alpha}{2} \begin{bmatrix} J_{i+1} \\ J_{i+1} \end{bmatrix} \left(\Delta \ \widehat{U}_{i+1} \right) + \frac{A_{i+1}\alpha}{2} \begin{bmatrix} J_{i+1} \\ J_{i+1} \end{bmatrix} \left(\Delta \ \widehat{U}_{i+1} \right) + \frac{A_{i+1}\alpha}{2} \begin{bmatrix} J_{i+1} \\ J_{i+1} \end{bmatrix} \left(\Delta \ \widehat{U}_{i+1} \right) + \frac{A_{i+1}\alpha}{2} \begin{bmatrix} J_{i+1}$ $= \left[\widehat{S}_{i}^{n}\right] + \frac{A_{i-1/2}}{2} \left[\widehat{F}_{i}^{n} + \widehat{F}_{i-1}^{n}\right] - \frac{A_{i+1/2}}{2} \left[\widehat{F}_{i+1}^{n} + \widehat{F}_{i}^{n}\right]$

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Artificial Dissipation 2nd Order Terms Required to Dampen Out Oscillations Occurring at Steep Gradients

Continuity Equation:

ନ ନ୍ନାର୍କ

Momentum Equation:

$$\tau_{xx} = (\mu_R + \mu_A) \frac{\partial u}{\partial x}, \ \mu_A = \frac{\rho_u \, \Delta x}{R_e}$$

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Energy Equation:

$$q_x = -(k_R + k_A)\frac{\partial T}{\partial x}, k_A = \frac{\rho C_p u \Delta x}{P_e}$$

$$I_{x} = -(k_{R} + k_{A})\frac{\partial T}{\partial v}, k_{A} = \frac{\rho C_{p} u}{p}$$

$$a_{1} = -(k_{0} + k_{1})\frac{\partial T}{\partial T} k_{1} = \frac{\rho C_{p} t}{\delta}$$

$$q_x = -(k_R + k_A)\frac{\partial T}{\partial x}, k_A = \frac{\rho C}{\Delta C}$$

$$q_x = -(k_R + k_A) \frac{1}{\partial x}, k_A = \frac{1}{\Delta x}$$

FEATURES OF 1-D CODE

- Heat Transfer
- Friction
- Variable Area
- Mass Injection Through Side Walls



BOUNDARY CONDITIONS

- ENTRANCE BOUNDARY CONDITIONS
 - Solid Wall
- All Static Conditions Specified
- Reservoir Conditions Specified
- Solid Wall with Mass and Energy Source
- **EXIT PLANE BOUNDARY CONDITIONS** - Solid Wall
- Static Pressure Specified
- Frictionless, Constant Area Extension for Supersonic Outflow
- Linear Extrapolation for Supersonic Outflow
- SIDE WALL BOUNDARY CONDITIONS
 - Impermeable
- Specified Mass/Energy Injection Rate Burning Propellant Surface



COMPARISON	SOLUTIONS
BΥ	<u>d-</u>
VALIDATION	TO EXACT

- Fanno Flow
- Rayleigh-Line Flow
- Isentropic Nozzle Flow
- Mass Injection Through Walls of Constant Area Duct
- Shock Tube Problem





FLOW THROUGH CONSTANT AREA DUCT WITH FRICTION



FLUW INHOUGH CONSTANT AREA DUCT WITH FRICTION



ISENTROPIC FLOW THROUGH A NOZZLE NOZZLE CONFIGURATION



ISENTROPIC FLOW THROUGH A NOZZLE PRESSURE vs AXIAL POSITION



ISENTROPIC FLOW THROUGH A NOZZLE TEMPERATURE vs AXIAL POSITION





RADIAL MASS INJECTION INTO CONSTANT AREA DUCT



NALVAL MASS INJECTION INTO CONSTANT AREA DUCT











ONE DIMENSIONAL SHOCK TUBE PROBLEM PRESSURE vs AXIAL POSITION NEAR STEADY STATE, t = 835 milliseconds



ONE DIMENSIONAL SHOCK TUBE PROBLEM TEMPERATURE vs AXIAL POSITION PRIOR TO SHOCK REFLECTION, t = 0.5 milliseconds



ONE DIMENSIONAL SHOCK TUBE PROBLEM TEMPERATURE vs AXIAL POSITION AS SHOCK CONTACTS WALL, t = 1.0 milliseconds



ONE DIMENSIONAL SHOCK TUBE PROBLEM TEMPERATURE vs AXIAL POSITION NEAR STEADY STATE, t = 835 milliseconds



RELIMINARY SENSITIVITY STUDIES AXIMUM HEAD END dP/dt AS A FUNCTION OF CT LENGTH AND NOZZLE CONTRACTION RATIO	 General Results Obtained Using a Cylindrical Duct with a Closed Aft End and an Increasing Mass Flow Rate Entering at the Head End: as the Duct Length Increased, the Maximum dP/dt at the Head End Increased Closer Examination Revealed Sinusoidal Behavior Due to Complex Wave Interactions 	 General Results Obtained Using a Cylindrical Duct with a Nozzle Attached at the Aft End: as the Nozzle Contraction Ratio Increased, the Maximum dP/dt at the Head End Increased Contraction Ratio of 2.5:1 (ASRM) Produced Results within 10% of Worst Case Solid Wall
PRELIM MAXIMUM DUCT LENG	Bergers as den Bergers	A Gen Cen Be C the Be


D CODE RATE	8 (8) 80.29	1, 800
JITC1D IG AS A FLOW	— (7) 71.5t	,
THE A	(6) 62.71	75,000 psi/se
FROM OCK STI REASIN	(msec) 6 · · · (5) 53.69	900 DIS TANCE
N OF SH	TIME B (4) 44.3	AXIAL AXIA AXIA
RY RES	8 (3) 34.7	300 300 "
PRELIMINAF VERIF CONSEQUE	— (1) 14.33 ··· (2, 24.8	

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PRELIMINARY RESULTS FROM THE AJITC1D CODE DUCT LENGTH AND THE IGNITER MASS FLOW RATE MAXIMUM dP/dt AS A FUNCTION OF THE TOTAL





PRELIMINARY RESULTS FROM THE AJITC1D CODE DOWNSTREAM BOUNDARY CONDITION SPECIFIED MAXIMUM dP/dt AS A FUNCTION OF THE



L	CURRENT STATUS OF 1-D CODE	
	 ALL FEATURES OF CODE VALIDATED INDIVIDUALLY BY COMPARISONS TO EXACT ANALYTICAL SOLUTIONS 	
	BURNING SURFACE BOUNDARY CONDITION ADDED	
7	FOR IMMEDIATE PARAMETRIC STUDY TO ESTABLISH BOUNDS:	
59	SIMPLE PERCENT OF PROP. LIT VS T AND X LOGIC ADDED	
	CAN BE ADJUSTED TO MATCH SINGLE PORT RSRM DATA (LOWER LIMIT FOR ASRM)	
	WORST CASE UPPER LIMIT OBTAINED BY ALLOWING FINS TO IGNITE AS INITIAL PULSE PASSES	
I		

	FUTURE PLANS FOR 1-D CODE
	NEED FLAME SPREADING MODEL FOR "FINNED" ZONE
	DERIVE FROM RSRM DATA (LOTS OF VARIABLES)
	INCORPORATE RESULTS FROM AUBURN UNIVERSITY HEAD END COLD FLOW TEST SERIES (EXTRAPOLATION PROBLEM)
760	CALCULATE MASS ADDITION RATE USING CONTINUSYS CODE (LIMITED TO INVISCID CALCULATIONS WITH USER SUPPLIED IGNITION TEMPERATURE)
	ADD EROSIVE BURNING MODEL
	PENN STATE FUNDED FOR TEST PROGRAM
	ATTICATION AND AND AND AND AND AND AND AND AND AN

Was	PLANS FOR 3-D IGNITION TRANSIENT MODEL
• EXTE	END 1-D ADI TECHNIQUE TO 3-D
• USE TRAI	EXISTING GRID GENERATORS AND COORDINATE NSFORMATION ROUTINES
• PRO WITH	BABLY NOT FEASIBLE TO RUN FULL 3-D MODEL (EVEN 1 22 PLANES OF SYMMETRY)
Ŭ ·	OMPLICATED GEOMETRY IN HEAD END
山 •	XTREMELY LONG DOMAIN (L/D > 20)
2 •	UST CALCULATE THROUGH ENTIRE 1ST SECOND
• NEEI GEO	D TO DEVELOP TRANSITION FROM 3-D TO AXISYMMETRIC METRY
∑ •	UST PRESERVE WAVE MECHANICS



SRMAFTE Facility Checkout Model Flow Field Analysis

Richard A. Dill, ERC Incorporated Harold R. Whitesides, ERC Incorporated

Abstract

The Solid Rocket Motor Air Flow Equipment (SRMAFTE) facility was constructed for the purpose of evaluating the internal propellant, insulation, and nozzle configurations of solid propellant rocket motor designs. This makes the characterization of the facility internal flow field very important in assuring that no facility induced flow field features exist which would corrupt the model related measurements. In order to verify the design and operation of the facility, a three-dimensional computational flow field analysis was performed on the facility checkout model setup.

The facility checkout model entails a straight constant diameter pipe in place of a specific solid propellant rocket motor internal component. This configuration was to provide a simple internal flow field for evaluation of any facility induced effects.

One-dimensional estimates of the checkout model flow field were available for comparison to the measurement data collected for the checkout model but the CFD results provided a comparative estimate in regions where one-dimensional estimates were not valid.

Since the facility was too large and complex to perform a complete three-dimensional analysis from end to end, the facility was divided into three major zones for analysis. 1) The header pipes, metering nozzle, nozzle exit, and diffuser. 2) The adapter chamber, transition, checkout model section, and checkout model nozzle. 3) The model nozzle exit, diffuser and muffler. The three-dimensional numerical calculation of the flow field was performed by Fluent/BFC. This code solves the full Navier-Stokes equations of fluid flow cast in a staggered grid formulation. The SIMPLER numerical algorithm is used in the solution process. The code utilizes wall functions instead of physically resolving the boundary layer and the standard k-e turbulence model is used to close the system fluid dynamic equations.

The checkout model measurement data, one-dimensional and three-dimensional estimates were compared and the design and proper operation of the facility was verified. The proper operation of the metering nozzles, adapter chamber transition, model nozzle and diffuser were verified. The one-dimensional and three-dimensional flow field estimates along with the available measurement data are compared in this presentation.

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SRMAFTE FACILITY CHECKOUT MODEL FLOW FIELD ANALYSIS

Richard A. Dill and R. Harold Whitesides ERC, Inc. **Tenth Annual CFD Working Group Meeting**

April 29, 1992

NASA/MSFC

Session 8

OBJECTIVES
 VERIFY CHECKOUT MODEL SYSTEM DESIGN AND OPERATIONAL PERFORMANCE PARAMETERS INCLUDING TWO AND 3-D EFFECTS
1) ASYMMETRIC FLOW EFFECTS CREATED BY THE MANIFOLD SYSTEM 2) METERING NOZZLE PERFORMANCE AND EXPANSION SECTION FLOW FIELD
 3) ASYMMETRIC FLOW FIELD IN THE ADAPTER CHAMBER 4) UNIFORMITY OF FLOW IN THE CHECKOUT MODEL CHAMBER
5) MODEL NOZZLE REGION FLOW FIELD 6) DIFFUSER FLOW FIELD INCLUDING SHOCKS
 COMPARE FACILITY CHECKOUT MODEL TEST DATA WITH CFD RESULTS AS VERIFICATION OF THE CFD CODE
ERC, Inc. 4/29/92

CFD METHODOLOGY	- GOVERNING EQUATIONS ARE THE 3-D ENSEMBLE-AVERAGED NAVIER STOKES EQUATIONS IN CONSERVATION FORM	- CLOSURE OF THE EQUATIONS BY THE STANDARD TWO-EQUATION $k^{-\epsilon}$ MODEL OF TURBULENCE	- WALL FUNCTIONS USED TO DETERMINE NEAR WALL GRADIENTS	- DISCRETIZATION METHOD	GOVERNING EQUATIONS ARE WRITTEN IN COMPONENT FORM USING CONTRAVARIANT VELOCITY COMPONENTS	THIS ALLOWS THE USE OF A BOUNDARY FITTED CURVILINEAR COORDINATE SYSTEM	NUMERICAL METHOD IS FINITE VOLUME BASED	STAGGERED GRID STORAGE SYSTEM IS USED	CONVECTION AND DIFFUSION FLUXES ARE APPROXIMATED USING A POWER-LAW SCHEME	TIME DERIVATIVES ARE CALCULATED USING A FULLY IMPLICIT FIRST ORDER SCHEME	- PRESSURE-VELOCITY COUPLING IS ACCOMPLISHED BY USING THE SIMPLER ALGORITHM	- SOLVER USES LINEARIZED BLOCK IMPLICIT SCHEME
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BOUNDARY CONDITION CHECKOUT MODEL HEADER PIPI	<u>IS USE</u> ES AND	<u>D FOR THE</u>) METERING NOZZLE
• INLET CONDITIONS		
STAGNATION PRESSURE (psia) STAGNATION TEMPERATURE (°R) TURBULENCE INTENSITY (%) TURBULENCE LENGTH SCALE (m)		1200 530 10 0.146
GENERAL CONDITIONS MODELED		
IDEAL GAS LAW USED RATIO OF SPECIFIC HEATS MOLECULAR WEIGHT DYNAMIC VISCOSITY (Ibm/ft-sec)		1.4 28.966 1.245x10 ⁻⁵
• EXIT CONDITION STATIC PRESSURE (neia)	•	600
		ERC, Inc. 4/29/9







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Metering Nozzle Radial Pressure Ratio Profile

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ERCI - 1/8/92

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TURBULENCE LENGTH SCALE (m) : 0.146 TURBULENCE LENGTH SCALE (m) : 0.146 • GENERAL CONDITIONS MODELED IDEAL GAS LAW USED IDEAL GAS LAW USED RATIO OF SPECIFIC HEATS RATIO OF SPECIFIC HEATS : 1.4 MOLECULAR WEIGHT : 28.966 DYNAMIC VISCOSITY (Ibm/ft-sec) : 1.245x10^5 SUPERSONIC OUTLET BOUNDARY CONDITION SUPERSONIC OUTLET BOUNDARY CONDITION
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æ	<u>3-D CHECKOUT MODEL FLOW FIELD (21X30X170) GRID</u> Profiles of W-VELOCITY	FLUENT/BFC V3.02 30 Domain
	Slices: J=15	Steady State

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BOUNDARY CONDITIONS USED FOR THE SRMAFTE DIFFUSER

INLET CONDITIONS		
STAGNATION PRESSURE (psia)		150
STAGNATION TEMPERATURE (°R)	••	530
TURBULENCE INTENSITY (%)	••	ប
TURBULENCE LENGTH SCALE (m)	••	0.108
GENERAL CONDITIONS MODELED		
IDEAL GAS LAW USED		
RATIO OF SPECIFIC HEATS	••	1.4
MOLECULAR WEIGHT	••	28.966
DYNAMIC VISCOSITY (Ibm/ft-sec)		1.245x10 ⁻⁵
EXIT CONDITION		
STATIC PRESSURE (psia)		15

ERC, Inc. 4/29/92



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	FI LIFNT, "	DEENE X. INC.
	ORIENT = Z	Z-D DOMAIN
		NIN. = 5.25557E-04
		4.48647E+00
KEY 4.41E+00 4.28E+00 5.39EE+00 3.98E+00 3.88E+00 3.88E+00 5.28E+00 2.87E+00 1.77E+00 1.177E+00 1.177E+00 1.177E+00 1.2757E+00 1.277E+00		MAX. =

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																											ORIENT = Z FI LIFNT		2-0 DOM/IN UNEWE-X. IN. J
																												R PLOT OF MACH NO. (DIMENSIONLESS)	4.48647E+00 MIN. = 5.25557E-04
1.48E+00	1.43E+00	1.38E+00	1.335+00	1.295+50	1.22.60		1 - 1 - 1 - 1 - 1 - 1 - 1 - 1 - 1 - 1 -	9.755-A1	9.256-01	8.75E-01	8.256-01	7.75E-01	7.255-01	6.72-01	6.23E-01	10-3.5	1.255-01	3.75E-01	3.25E-01	2.75E-01	2.23E-01	1.736-01	1.20-11 7.555-01	2.55E-02	.	, , ,		RASTE	MAX. =

Diffuser Performance Map



CONCLUSIONS	THE CFD ANALYSES OF THE CHECKOUT MODEL, MANIFOLD SYSTEM AND DIFFUSER CONFIRMEI THE DESIGN AND VERIFIED THAT:	1) THE FLOW CHOKES IN BOTH THE METERING AND MODEL NOZZLE AND THE MANIFOLD SYSTEM SHOULD PERFORM AS EXPECTED.	2) THE ADAPTER AND TRANSITION SECTION PERFORM WELL IN DELIVERING A UNIFORM FLOW PROFILE TO THE MODEL NOZZLE.	3) THE PREDICTED SHOCK STRUCTURE IN THE DIFFUSER INDICATES THE DESIGN SHOULD PERFORM AS EXPECTED.	
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A Comparative Study of the Effects of Inhibitor Stub Length on Solid Rocket Motor Combustion Chamber Pressure Oscillations: RSRM at T=80 Seconds, Preliminary Results

D. Chasman, D. Burnette, J. Holt Rockwell International, Space Systems Division Huntsville, Alabama 35806 R. Farr NASA Science and Engineering Laboratory George C. Marshall Space Flight Center

ABSTRACT

Results from a continuing, time-accurate computational study of the combustion gas flow inside the Space Shuttle Redesigned Solid Rocket Motor (RSRM) are presented. These CFD analyses duplicate unsteady flow effects which interact in the RSRM to produce pressure oscillations, and resulting thrust oscillations, at nominally 15, 30 and 45 Hz. Results of Navier-Stokes computations made at mean pressure and flow conditions corresponding to 80 seconds after motor ignition both with and without a protruding, rigid inhibitor at the forward joint cavity are presented here.

Previous studies by the authors have demonstrated that combustion chamber pressure oscillations in the RSRM are generated by flow/acoustic interactions which occur at the three field joint cavities [1,2,3]. Edge-tone, Hole-tone and Organ pipe-tone are all acoustic sources that play part in these interactions[4,5,6]. By constructive interference processes, the different acoustic sources interact, amplifying the pressure oscillation level at some instant during the RSRM burn (i.e. T+80 sec). This behavior is representitive of an aerodynamic whistle of Class III [7,8].

However, the question remained as to whether the cavities alone are the main acoustic generators or whether protruding inhibitors dominate the system. With this in mind, two simulations have been conducted. The first simulation represent a full scale model of the RSRM with a rigid inhibitor perturbing the flow at the forward joint, while the second simulation was conducted without an inhibitor. All other flow conditions and grain geometries were kept constant for both simulations.

Fig. 1 shows a comparison of results between the two simulations. A full-length density contour plot of the simulation with forward inhibitor is shown in Fig. 1a., while that without the inhibitor is shown in Fig. 1d.. In both plots the shear layer which developed from the burning surfaces is apparent. High density values, corresponding to areas of high pressure amplitude, appear in red.

Details of the forward field joint area are shown for both simulations in Figs. 1b. and 1e.. Both show intense, but different, shear flow activity indicative of vortex dynamics. Streamlines shown in Fig. 1c. and Fig. 1f. single out individual vortices and further illustrate the difference between the two simulations.

Fig. 2 illustrates a comparison of pressure data time histories for three points common to both simulations. It can be seen that 30 Hz oscillations are evident in the midsection of the chamber, while 15 Hz is found at both the head and aft ends, with the head end being 180 degrees out of phase with the aft end. These results indicate classic organ pipe acoustics are found in both simulations. However, there is a marked difference in the peak-to-peak amplitude of these pressure oscillations. These preliminary results show pressure amplitude in the case without the inhibitor are about 14% of total chamber pressure, while those in the case with the inhibitor are only 10% of the total pressure.

While calculated peak-to-peak pressure amplitude values are significally higher than levels measured during actual firing and flight, we feel these results can nevertheless be used for

comparative analyses of the effects of inhibitor stub height on RSRM combustion chamber acoustic pressure amplitudes. Specifically, these findings demonstrate that the inhibitors alone are not the dominant factor in amplifying combustion chamber pressure oscillations, but rather are included in secondary acoustic/flow interactions occuring at the three field joint cavities. Our results indicate that inhibitors, when present, actually act to damp such oscillations.

References

1. D., R. Farr, T. Nesman, D. Burnette, and Chasman, D., "Time-Accurate Navier-Stokes Computations of Low Speed Flow Over Cavities: No Slip vs. Blowing Walls", Fourth International Symposium on Computational Fluid Dynamics, Davis California, September 1991.

2. R. Farr, T. Nesman, Chasman, D., and D. Burnette, "Time-Accurate Navier-Stokes Computations of Pressure Oscillation in the RSRM, 80 seconds after Ignition", Fourth International Symposium on Computational Fluid Dynamics, Davis California, September 1991.

3. Burnette, D., J. M. O'Farrell, J. Holt, R. A. Farr, T. Nesman "Time Accurate Navier-Stokes Computations of Solid Rocket Motor Internal Field Joint Cavity Flows", TABES 91 Paper No. 91-269, Seventh Annual Technical and Business Exhibition and Symposium, Huntsville Alabama, May 1991.

4. Powell, A., "On The Edgetone", J. Acoust. Soc. of America, Vol. 33, No. 4, pp. 395-409, 1961.

5. Powell, A., "Nature of the Feedback Mechanism in Some Fluid Flows Producing Sound", 4th International Congress on Acoustics, No. 022, Copenhagen, Aug. 1962.

6. Rossiter, J. E., "Wind Tunnel Experiments on the Flow over Rectangular Cavities at Subsonic and Transonic Speeds", Royal Aircraft Establishment Technical Report No. 64037, October 1964.

7. Chanaud, R.C. and Powell, A., "Some Experiments Concerning the Hole and Ring Tone", J. Acoust. Soc. of America, Vol. 37, NO. 5, pp 902-911, May 1965.

8. Chanaud, R.C., "Aerodynamic Whistles", Scientific American, January 1970.

RSRM PC OSCILLATION



Space Systems Division

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Huntsville Operations

RENG001748.0



Huntsville Operations

Overview of the relevant CFD work at Thiokol Corporation

Pawel Chwalowski & Hai-Tien Loh Thiokol Corporation, M/S L63, P.O. Box 707, Brigham City, Utah 84302-0707

The use of computational fluid dynamics (CFD) in supporting rocket propulsion designs at Thiokol Corporation has the continuously increased in the past few years. An in-house developed proprietary advanced CFD code called SHARP[®] is a primary tool for many flow simulations and design analyses. The SHARP code is a time dependent, two-dimensional (2-D) axisymmetric numerical solution technique for the compressible Navier-Stokes equations. The solution technique in SHARP uses a vectorizable implicit, second order accurate in time and space, finite-volume scheme based on the following: 1) an upwind flux-difference splitting of a Roe-type approximated Riemann solver, 2) Van Leer's flux vector splitting, and 3) a fourth order artificial dissipation scheme with а preconditioning to accelerate the flow solution. Turbulence is simulated by an algebraic model, and ultimately the $k-\epsilon$ Some other capabilities of the code are 2-D two-phase model. Lagrangian particle tracking and cell blockages. Extensive development and testing been conducted on has the three-dimensional (3-D) version of the code with flow, combustion, and turbulence interactions.

The SHARP code has been applied in many areas of the solid rocket motor (SRM) design involving internal and external flow However, the internal flow analysis inside the analysis. motor and in the nozzle region are the most frequent. Usually, the results from these CFD analyses become the boundary conditions for thermal and structural computations. In the case of the internal nozzle flow calculations, SHARP computes the convective heat transfer coefficients and temperature distribution along the nozzle wall for the thermal erosion predictions, and the pressure distribution for the structural predictions. The pressure loads on the propellant grain surfaces inside the SRM obtained from SHARP are used as a boundary conditions to predict propellant grain deformation and displacement. The 2-D two-phase Lagrangian particle tracking gives the

ability to predict solid particle impingement on the exit cone. Also, SHARP prediction of the slag accumulation in the aft dome region of the SRM agrees with the actual static test data.

The emphasis in the presentation will be put on the specific applications of SHARP in SRM design.

SHock wave And Recirculation Program is a copyrighted acronym owned by Thiokol Corporation.
OVERVIEW OF THE RELEVANT CFD WORK AT THIOKOL CORPORATION

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SPACE OPERATIONS

Pawel Chwalowski

CFD Workshop

April 28, 1992

Thiokol CORPORATION SPACE OPERATIONS

AGENDA

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CFD Tools Used at Thiokol Corp.

Description of the Primary CFD Code

Applications in the Solid Rocket Motor (SRM) Design

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PHOENICS (versions 1.4 and 1.5)

subsonic flow cases (includes heat conduction, multiphase flow, -well developed and tested for many incompressible and/or reactive flow, etc.)

-works well for incompressible and/or subsonic flow

-finite volume SIMPLE scheme (Semi-Implicit Method for Pressure Linked Equation)

-exhibits problems for high speed compressible and turbulent modeling

-lacks flexibility in BFC gridding

SHARP

-developed in-house by Thiokol; considered proprietary

-2D version extensively tested and operational

-3D version in development and testing

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SHARP 2D DESCRIPTION

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Flow Modeling

2D Planar/Axisymmetric Compressible Code

2D Lagrangian Particle Tracking

Solution Algorithm

Upwind Roe Flux Difference Splitting

Upwind Van Leer's Flux Vector Splitting

Central Difference with Artificial Dissipation

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SHARP 2D DESCRIPTION (cont.)

Features

Finite Volume / Second Order Accuracy in Time

Use of Preconditioning to Accelerate Flow Solution

Cell Blockage

Baldwin-Lomax Algebraic Turbulence Model (Ultimately k-ɛ Model)

Unstructured Grid in Testing

SHARP 3D CODE

SHARP 3D in Development and Testing with Flow, Combustion, and **Turbulence Interaction**

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APPLICATIONS IN SRM DESIGN

Internal Flow Modeling

Nozzle Flow

along nozzle wall are calculated for the thermal erosion -heat transfer coefficients and temperature distribution analysis -pressure along nozzle wall is calculated for the structural analysis

-aluminum oxide particle motion is predicted and better understood

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SHARP Results Internal Flow Modeling Nozzle Flow Mach Contour Temperature Contour (K)





Temperature 3.369E+03 3.028E+03 2.687E+03 2.346E+03 2.346E+03 2.005E+03 1.664E+03
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APPLICATIONS IN SRM DESIGN (cont.)

Internal Flow Modeling (cont.)

Chamber Internal Flow

are calculated to predict propellant grain deformation -pressure loads on the propellant grain surfaces and displacement

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								<pre>propellant grain</pre>								aft segment						
g Elour								propellant grain										center segment				
Internal Flow Modelin Shutta SBM Internal	Pressure Contour Ine							propellant grain		×					802	2		center segment				

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Internal Flow Modeling Shuttle SRM Internal Flow Pressure Differential in The Slot Area Between Center And Aft	
Segments (psi)	

822.80

821.00

820.00

818.00

817.08

819.00



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SUMMARY

-efficient algorithm was developed / runs well on computer workstations

-SHARP 2D was extensively tested

-SHARP demonstrates capabilities in SRM design and flow analysis

-turbulent combustion development and testing is in progress

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N92-39250

Submitted for the CFD Workshop - 1992

A Status of the Activities of the NASA/Marshall Space Flight Center Combustion Devices Technology Team

Kevin Tucker

The Consortium for Computational Fluid Dynamics (CFD) Applications in Propulsion Technology was established to focus CFD applications in propulsion. Specific areas of effort include developing the CFD technology required to address rocket propulsion issues, validating the technology, and applying the validated technology to design problems; all under peer review by experts in the field.

The Combustion Devices Technology Team was formed to implement the above objectives in the broad area of combustion-driven flows. In an effort to bring CFD to bear in the design environment, the team has focused its efforts on the Space Transportation Main Engine nozzle. The main emphasis has been on the film cooling scheme used to cool the nozzle wall. Benchmark problems have been chosen to validate CFD film cooling capabilities. CFD simulations of the subscale nozzle (to be tested 8/92) have been made. Also, CFD predictions of the base flow resulting from this type of nozzle have been made. A status of these calculations will be presented along with future plans.



A STATUS OF THE ACTIVITIES OF THE

MSFC COMBUSTION DEVICES TECHNOLOGY TEAM

KEVIN TUCKER APRIL 29, 1992

Rational Aeronautics and Space Administration

Combustion-Driven Flow Analysis Technology

Overview

- Combustion Driven Flow Team Participants
- Background
- Programs
- STME Nozzle Film Cooling
- NLS Base Heating
- Summary.

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Combustion-Driven Flow Analysis Technology

Participants

- NASA/Marshall Space Flight Center (MSFC)
- NASA/Ames Research Center (ARC)
- NASA/Lewis Research Center (LeRC)
- Air Force (Phillips Lab)
- Aerojet
- Pratt & Whitney (P&W)

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- Rocketdyne (Rkdn)
- SECA
- Computational Fluid Dynamics (CFD) Research Corporation
- United Technology Research Center (UTRC)
- .Calspan University of Buffalo Research Center (CUBRC)
- Calspan AEDC Operations
- W. J. Shafer Associates
- Remtech
- University of Tennessee Space Institute (UTSI)
- Pennsylvania State University
- The University of Alabama (UA)
- The University of Alabama in Huntsville (UAH)

National Aeronautics and National Aeronautics and Space Administration Combu Space Administration Combu Space Administration Combu Same Administration EXAL A IS - TOM activity Identified TCA IS - Need for Improved desig - Need for Improved desig - Need for Improved desig - Need for Improved desig - Identified nine generic technology - Identified major technology - High aspect ratio coolan - Chose STME film/dump coo - Identified validation/verifica	oustion-Driven Flow Analysis Technology Background Background ssues which could benefit from enhanced analytical capabilities is methodology (engine contractors) ic in near to mid-term (CFD specialists) hnology Issues in injector, chamber, and nozzle y/development in STME TCA ant channels ant channels logy Issues with STME TCA concerns oled nozzle for team focus cation requirements for supersonic film cooling
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tional Aeronautics and ace Administration	Combustion-Driven Flow Analysis Technology
	Background
NLS Base Heating Base heating is a 	a concern on every launch vehicle
 The hydrogen-rid Dumping low database 	ch film/dump coolant causes additional complexities/concerns energy hydrogen into the base region put the program out of historica
 Resulting high Subscale tests 	n heating rate environments are based on conservative assumptions s with base and/or afterburning don't scale well
 CFD is being use 	ed to augment classical analysis and testing
 Extensive code 	validation plan has been developed

Combustion-Driven Flow Analysis Technology	Program - STME Nozzle Film Cooling	film to adequately cool the nozzle skirt elerating core flow on film integrity t which film should be injected olant/injector delivery system on performance s inition in nozzle/MCC joint area des for supersonic film cooling des as design tool for subscale (40K) nozzle ng performance in subscale nozzle des in design of fuil scale nozzle
Combu	Pr	film to ade elerating co t which film t which film olant/injecto s des for supe des as desi ng performa des in desi
National Aeronautics and Space Administration		 Issues Capability of the Effect of acc Effect of film coo Effect of film coo Environment de Task Description Validate CFD co Use validated cc Verify film coolit Use validated cc

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Combustion-Driven Flow Analysis Technology

Program - STME Nozzle Film Cooling

- Results to Date
- Film cooling benchmark calculations complete
- Analysis of film coolant network for subscale nozzle complete
- Preliminary primary injector analysis complete
- Analysis of cases from subscale test matrix underway; to be completed 8/92
- Impact
- Demonstration of CFD as a nozzle design tool successful
- Subscale secondary injector redesigned using CFD
- Confidence gained in film cooling early in subscale design
- Large film cooling analytical/test database being developed

National Aeronautics and Space Administration

Combustion-Driven Flow Analysis Technology

Film Cooling Benchmark





Combustion-Driven Flow Analysis Technology

STME Subscale Nozzle







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National Aeronautics and Space Administration	Combustion-Driven Flow Analysis lechnology
	Program - NLS Base Heating
 Issues 	
- CFD has not be	en used extensively for base environments
- Codes must be	assessed for vehicle base flows
- Decisions mus current predicti	t be made on where, how, and when CFD codes will be used to supplemen ive techniques
 Task Description 	
- Establish valid	ation plan based on physical processes involved in base heating
- Perform single	nozzle analyses for the following:
Engineerin	g models
Support for	· subscale model design and subsequent scaling
- Perform 3D/axi	symmetric clustered nozzle calculations
- Perform all noz	zzle analyses at altitudes spanning vehicle trajectory

Program - NLS Base Heating	ozzle "demonstration" calculations at low and high altitudes complete (Iculations well underway in-house and at Rocketdyne	facing step	cid plume	e nozzle	uster	-S/STME single nozzle calculations to be completed by 5/92) NLS/STME base calculation to be completed by 5/92		monstration" calculations delivered to ED64 for heat flux calculations	es are pushing computer limits; job turnaround is slow
	 Results to Date STME single nozz 	codes) - Benchmark calcu	Backward fac	MOC/Inviscid	S-1C single no	4-nozzle clust	 Preliminary NLS/9 	- Preliminary 3D NI	 Impact 	- Results of "demo	- The 3D analyses
	Program - NLS Base Heating	 Program - NLS Base Heating Results to Date STME single nozzle "demonstration" calculations at low and high altitudes complete (Program - NLS Base Heating Results to Date STME single nozzle "demonstration" calculations at low and high altitudes complete (codes) Benchmark calculations well underway in-house and at Rocketdyne 	 Program - NLS Base Heating Results to Date STME single nozzle "demonstration" calculations at low and high altitudes complete (codes) Benchmark calculations well underway in-house and at Rocketdyne Backward facing step 	 Program - NLS Base Heating Results to Date STME single nozzle "demonstration" calculations at low and high altitudes complete (codes) Benchmark calculations well underway in-house and at Rocketdyne Backward facing step MOC/Inviscid plume 	 Program - NLS Base Heating Results to Date STME single nozzle "demonstration" calculations at low and high altitudes complete (codes) Benchmark calculations well underway in-house and at Rocketdyne Backward facing step MOC/Inviscid plume S-1C single nozzle 	 Program - NLS Base Heating Results to Date STME single nozzle "demonstration" calculations at low and high altitudes complete (codes) Benchmark calculations well underway in-house and at Rocketdyne Benchmark facing step MOC/Inviscid plume S-1C single nozzle 	 Program - NLS Base Heating Results to Date STME single nozzle "demonstration" calculations at low and high altitudes complete (codes) Benchmark calculations well underway in-house and at Rocketdyne Benckward facing step Backward facing step MOC/Inviscid plume S-1C single nozzle 4-nozzle cluster Preliminary NLS/STME single nozzle calculations to be completed by 5/92 	 Program - NLS Base Heating Results to Date STME single nozzle "demonstration" calculations at low and high altitudes complete (codes) Stocedes) Benchmark calculations well underway in-house and at Rocketdyne Backward facing step MOC/Inviscid plume S-1C single nozzle 4-nozzle cluster Preliminary 3D NLS/STME base calculation to be completed by 5/92 Preliminary 3D NLS/STME base calculation to be completed by 5/92 	Program - NLS Base Heating • Results to Date • STME single nozzle "demonstration" calculations at low and high altitudes complete (codes) • Benchmark calculations well underway in-house and at Rocketdyne • Backward facing step • MOC/Inviscid plume • 4-nozzle • 4-nozzle cluster • Preliminary NLS/STME single nozzle calculations to be completed by 5/92 • Iminary 3D NLS/STME base calculation to be completed by 5/92	 Program - NLS Base Heating Results to Date STME single nozzle "demonstration" calculations at low and high altitudes complete (codes) Benchmark calculations well underway in-house and at Rocketdyne Benchmark calculations to be completed by 5/92 Preliminary 3D NLS/STME base calculation to be completed by 5/92 Impact Results of "demonstration" calculations delivered to ED64 for heat flux calculations

Rational Aeronautics and Space Administration

Combustion-Driven Flow Analysis Technology

NLS 1.5 Stage Base





Combustion-Driven Flow Analysis Technology

Backward-Facing Step Benchmark



MOREL BINKINSIBIL AND CONTONENT DESIGNATION

National Aeronautics and Space Administration **VSV**

Combustion-Driven Flow Analysis Technology

Clustered Nozzle Benchmark



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radial base pressure distribution

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Combustion-Driven Flow Analysis Technology

Summary

- Technology program geared toward STME TCA issues
- Supported by government, industry, and universities
- CFD codes being validated for and applied to NLS/STME
- CFD contributing to STME design improvements
- Usefulness of analytical tools being enhanced via technology, experience, and peer review of results
N92-32251

CFD Analysis of the STME Nozzle Flowfield

Anantha Krishnan CFD Research Corporation, Huntsville, AL and Kevin Tucker NASA MSFC, Huntsville, AL

The Space Transporter Main Engine (STME) uses a gas generator cycle to cool the nozzle wall by a film-dump of the turbine exhaust. The ability to cool the skirt is a key concern in the design of the STME. CFD calculations were undertaken to predict the film cooling effectiveness and performance sensitivities for various design configurations, operating points and inlet conditions. The results in this study were obtained for the subscale nozzle. The computations were performed using REFLEQS.

The computational analysis showed that a chemical equilibrium model was necessary to obtain correct predictions of the specific impulse. The frozen composition model underpredicts the ISP by about 6%. It was also observed that the coolant film was successful in maintaining the nozzle wall well below the stagnation temperature of the core flow. The effect of the coolant flow on the performance of the engine was found to be negligible. The computed heat fluxes at the wall were in good agreement with the empirical data obtained by Pratt & Whitney.

Further test data from Pratt & Whitney are forthcoming for the subscale nozzle. Calculations will be performed to determine cooling efficiencies and nozzle performance over a range of conditions and the model predictions will be compared with experimental data.

CFD Research Corporation 3325-D Triana Blvd. Huntsville, AL 35805 (205) 536-6576 FAX: (205) 536-6590	CFD ANALYSIS OF THE STME FLOWFIELD	by Anantha Krishnan CFD Research Corporation	and Kevin Tucker NASA - MSFC	Tenth Annual CFD Workshop NASA - MSFC April 28-30, 1992
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INTRODUCTION

-CFD3C

- Nozzle Wall by a Film Dump of the Turbine Exhaust. The STME Uses a Gas Generator Cycle to Cool the
- The Film Dump is Split into a Subsonic Stream and Supersonic Stream Injected at Different Locations on the Nozzle Wall.
- **Cooling Effectiveness and Performance Sensitivies** CFD Calculations were Undertaken to Predict Film for Various Design Configurations and Operating **Points**.
- The Calculations were Done for the Subscale Nozzle.

CTUXC STME SUBSCALE NOZZLE ASSEMBLY





FD METHODOLOGY	REFLEQS Code has been Adapted for Rocket Thrust Chambers	Solving for Reynolds Average Navier-Stokes Equations with	 k-ɛ Turbulence Model Chemical Equilibrium BFC Grid (210x58) Colocated Variables and Solving for Cartesian Velocity Components (strong conservation form) Implicit Solver for Skew Grids Finite Volume Discretization Validated for Large Number of Benchmark Problems (REFLEQS Validation Manual)
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Structured 210 x 58 Grid



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Area of c/s (in²)	23.469
Mach Number	0.219
Velocity (ft/sec)	1096.08
Temperature (°R)	6683.4
ure a)	9.9
Pressi (Psi.	218

Table 2. Subsonic Injector

f c/s :)	8
Area o (in ³	1.9
Mach Number	0.205
Velocity (ft/sec)	876.9
Temperature (°R)	523.9
Pressure (Psia)	59.13
Mass Flow Rate (lb/sec)	0.254

Table 3. Sonic and Supersonic Injectors

Area of c/s (in²)	2.448	1.740	2.092	1.464	2.448	1.794
Mach Number	1.0	1.454	1.0	1.454	1.0	1.503
Velocity (ft/sec)	4456.0	5277.0	4456.0	5277.0	4456.0	5423.0
Temperature (°R)	568.53	377.14	568.53	377.14	568.53	372.74
Pressure (Psia)	60.9	48.0	57.6	46.1	73.47	53.98
Mass Flow Rate (lb/sec)	1.51	1.51	1.22	1.22	1.82	1.82

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Case	Chemistry	Coolant Flow	Coolant Exit Condition
< +	Frozen Composition	Nominal	Sonic
< '. <	Equilibrium Model	Nominal	Sonic
Э.	Equilibrium Model	Nominal	Supersonic
4.	Equilibrium Model	Minimum	Sonic
5.	Equilibrium Model	Minimum	Supersonic
9 .	Equilibrium Model	Maximum	Sonic
. .	Equilibrium Model	Maximum	Supersonic
ω	Equilibrium Model	Nominal	Sonic
	(no subsonic flow)		
9.	Equilibrium Model	(no primary inje	sctor flow)
10.	Equilibrium Model	Nominal	Sonic
	(T _W =1060°R)		
11.	Equilibrium Model	Nominal	Supersonic
	(T _W =1060∘R)		

NACID SUBSCALE NOZZLE CALCULATIONS

Temperature Distribution (°K) - Frozen Composition Model

L NTOURS	378E+02	711E+03	LEVELS	378E+02	594E+02	511E+02	328E+02	015E+03	196E+03	378E+03	560E+03	7 4 1E+03	323E+03	105E+03	286E+03	468E+03	550E+03	83 1E+03	013E+03	195E+03	376E+03	558E+03	740E+03	
MP CO	IIN 2 8	IAX 3	INTOUR I	م	4	Ű	œ		1					, V	2	с Л	- - - - - - - - - - - - - - - - - - -	<u>دا</u>	(C)	M	M	M	M	•
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Temperature Distribution (°K) - Chemical Equilibrium Model

	918E+02	7 12E+03	LEVELS	918E+02	726E+02	534E+02	342E+02	Ø15E+Ø3	196E+03	377E+03	557E+03	738E+03	919E+03	100E+03	280E+03	461E+03	G42E+03	823E+03	004E+03	184E+03	3656+03	546E+03	727E+03	
XY PLANE	FMIN 2.	FMAX 3.	CONTOUR	1 2	دم 4	0	4 0	ר ד		7 1.	B 1	ں 1.	10 1.	11 2.	12 2.	13 2.	14 2.	15 2.	16 3	17 3.	18 3.	19 3.	20 3.	< X </td



NOZZLE CALCULATIONS CFD3C	Distribution (Pa) - Chemical Equilibrium Model	
BSCALE	Pressure [ANE 1 CONTOURS 1.860E+04 1.860E+04 1.462E+07 2.711E+04 6.356E+04 8.178E+04 1.000E+05 6.000E+05 8.000E+05 1.128E+05 1.128E+06 1.128E+06
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CIUXC SUBSCALE NOZZLE CALCULATIONS

Pressure Distribution (Pa) - Chemical Equilibrium Model

I 1 IN TOURS	583E+05	Z13E+05	LEVELS	922E+05	344E+05	767E+05	189E+05	611E+05	033E+05	456E+05	878E+05	300E+05	
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XY PLA Pres	FMIN	FMAX	CONTOL	, - 1	N	m	4	ហ	ഗ	7	ω	ຫ	< XO



SUBSCALE NOZZLE CALCULATIONS

Mach Number - Chemical Equilibrium Model

401E-01 602E-01 803E-01 100E+00 320E+00 540E+00 761E+00 981E+00 201E+00 641E+00 641E+00 861E+00 861E+00 081E+00 301E+00 521E+00 741E+00 1 127E-01 4 181E+00 961E+00 181E+00 201E-0 CONTOURS LEVELS XY PLANE Ч 4 0 0 - -N МАСН FMIN FMAX CONT 1234567 844



COMPUTATIONAL RESULTS FOR THE SUB-SCALE NOZZLE FILM COOLING

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ISP	407.7	434.2	433.8	434.6	434.3	433.7	433.3	434.3	435.5	432.3	431.9
Mass Flow Rate (1bm/sec)	84.67	84.67	84.67	84.38	84.38	84.98	84.98	84.42	83.16	84.67	84.67
Primary Injector Type	Nominal, Sonic	Nominal, Sonic	Nominal, Supersonic	Minimum, Sonic	Minimum, Supersonic	Maximum, Sonic	Maximum, Supersonic	Nominal, Sonic No Subsonic Flow	Subsonic Flow No Sonic Flow	Nominal, Sonic	Nominal, Supersonic
Model	Frozen Composition	Equilibrium Model	Equilibrium Model	Equilibrium Model	Equilibrium Model	Equilibrium Model	Equilibrium Model	Equilibrium Model	Equilibrium Model	Equilibrium Model Wall at 1060°R	Equilibrium Model Wall at 1060°R



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CONCLUSIONS

-CFD3C

Computations were Performed for the Subscale STME Film Cooling. The Main Conclusions of this Analysis were:

- Chemistry Needs to be Considered to Predict the ISP Correctly
- The Coolant Film is Successful in Maintaining the Nozzle Wall Well Below the Stagnation **Temperature of the Core Flow** сi N
- Computed Heat Fluxes at the Wall were in Good Agreement with (P&W) Empirical Data പ്
- The Nozzle Performance is Relatively Insensitive to the Coolant Injection 4

N92-32252

NLS Nozzle Base Flow Characteristics

J. J. Erhart Pratt & Whitney West Palm Beach, FL

ABSTRACT

The flow characteristics of the NLS nozzle base area need to be determined in order for heat transfer rates to be estimated. The objective of this work is to calculate these flow characteristics using CFD. A Full Navier-Stokes code in an axisymmetric mode using a k-& turbulent model with wall functions is applied. Calculations were completed at an altitude of 3,250 and 80,000 feet in the flight trajectory. The results show flow features which can affect vehicle design. Calibration of a 3-D case with data is underway.

NOZZLE BASE CFD ANALYSIS



Wednesday, April 29, 1992

John J. Erhart

MSFC CFD Workshop

OUTLINE



- o Motivation
- o Approach
- o Geometry and Flow Boundary Conditions
- o Results
- o Summary

MOTIVATION

Understand Base Flow Phenomena



- Parameters Influencing Transport Of Hydrogen Into Base Of Nozzle.
- o Define Typical Base Flow Environment
- Streaklines
- $^{\Box}$ H²
- Mach Number
- Pressure

APPROACH



- Simplify Geometry Single Axisymmetric Nozzle
 With Largest Base Height.
- o Two Altitudes Different Plume Shapes.



GEOMETRY & FLOW BOUNDARY CONDITIONS



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HIGH & LOW ALTITUDE – STREAKLINES

Base H₂ Concentration Function Of Nozzle Plume And Bluff Body Recirculation Interaction









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RESULTS

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 H_2

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RESULTS *Pressure*



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CONTOUR 1 0.00020 0.00060 0.00100		0.00500 0.00540 0.00580	PSF 10 ⁴







RESULTS

Mach Number – Low Altitude









Pressure – Low Altitude





SUMMARY



o H₂ Transport Into The Base Is A Function Of Configuration And Flight Conditions.

	Low Altitude	High Altitude
Recirculation Region	Stronger	Weaker
H ₂ Transport Into Base	Trace	~1 - 1.5%
Pressure	~ 13.9 PSIA	~0.2 PSIA

HEAT TRANSFER IN ROCKET ENGINE COMBUSTION CHAMBERS AND NOZZLES

P. G. Anderson^{*}, Y.S. Chen[†], and R.C. Farmer^{*}

Abstract

Complexities of liquid rocket engine heat transfer which involve the injector faceplate and regeneratively and film cooled walls are being investigated by computational analysis. A conjugate heat transfer analysis will be used to describe localized heating phenomena associated with particular injector configurations and coolant channels and film coolant dumps. These components are being analyzed, and the analyses verified with appropriate test data. Finally, the component analyses will be synthesized into an overall flowfield/heat transfer model. The FDNS code is being used to make the component analyses. Particular attention is being given to the representation of the thermodynamic properties of the fluid streams and to the method of combining the detailed models to represent overall heating. Unit flow models of specific coaxial injector elements have been developed and will be described. Film cooling simulations of film coolant flows typical of the subscale STME being experimentally studied by Pratt and Whitney have been made, and these results will be presented. Other film coolant experiments have also been simulated to verify the CFD heat transfer model being developed by SECA. The status of this entire study will be presented, and its relevance as a new design tool will be demonstrated.

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[†] Engineering Sciences, Inc., 4920 Corporate Drive, Suite K, Huntsville, AL

HEAT TRANSFER IN ROCKET ENGINE COMBUSTION CHAMBERS AND NOZZLES

P. G. Anderson, Y. S. Chen, and R. C. Farmer

SECA, Inc.

OUTLINE OF STUDY

- NAVIER-STOKES FLOW SOLVER
- TWO-EQUATION TURBULENCE MODELS WITH COMPRESSIBILITY CORRECTIONS AND WALL FUNCTION APPROACH
- HOLDEN'S TEST CASE #45
- Slot Jet Nozzle Flowfield
 Film Cooling Analysis
- GASL TEST CASE #41

• **k-EQ. CORRECTION:**
$$\frac{\partial \rho k}{\partial t} + \frac{\partial \rho k U_{j}}{\partial X_{j}} = \frac{\partial}{\partial X_{j}} \left[\left(\mu + \frac{\mu_{t}}{\sigma_{k}} \right) \frac{\partial k}{\partial X_{j}} \right] + \mu_{t} \left[\frac{\partial U_{i}}{\partial X_{j}} + \frac{\partial U_{j}}{\partial X_{j}} \right] \frac{\partial U_{i}}{\partial X_{j}} - \rho \varepsilon \left(1 + \alpha M_{t}^{2} \right)$$

•
$$\varepsilon$$
-EQ. CORRECTION:
 $\frac{\partial \rho \varepsilon}{\partial t} + \frac{\partial \rho \varepsilon U_{j}}{\partial X_{j}} = \frac{\partial}{\partial X_{j}} \left[\left(\mu + \frac{\mu_{t}}{\sigma_{\varepsilon}} \right) \frac{\partial \varepsilon}{\partial X_{j}} \right] + \frac{C_{\varepsilon^{1}}^{*} \varepsilon \mu_{t}}{k} \left[\frac{\partial U_{i}}{\partial X_{j}} + \frac{\partial U_{j}}{\partial X_{j}} \right] \frac{\partial U_{i}}{\partial X_{j}} - \rho C_{\varepsilon^{2}} \frac{\varepsilon^{2}}{k}$

where

 $\alpha = 1, \qquad M_t = \frac{k}{a^2}$

 $C_{\epsilon^{1}}^{*} = 1.44 (1 + 0.08 M^{0.25}), C_{\epsilon^{2}} = 1.92,$

 $M = \frac{V_{total}}{a}$

•

HEAT TRANSFER WALL FUNCTION:

(Integration of Near Wall Energy Balance-- Viegas et al. 1985)

Heat Flux Source Term:

$$q_{w} = [h_{w} - h - Pr_{t}(u - u_{w})^{2}/2](\tau_{w}/Pr_{t}u)$$
$$= [h_{w} - h - Pr_{t}(u - u_{w})^{2}/2](\rho u_{\tau}/Pr_{t}u^{+})$$

where

$$u^{+} = ln \left[\frac{(y^{+} + 11)^{4.02}}{(y^{+^{2}} - 7.37y^{+} + 83.3)^{0.79}} \right]_{+} 0.563 \, tan^{-1} (0.12y^{+} - 0.441) - 3.81$$

 $Pr_{t} = 0.9$

For Adiabatic Wall Boundary Condition,

$$h_{w} = h + Pr_{t} (u - u_{w})^{2} / 2$$
HOLDEN'S TEST CASE #45

SLOT JET NOZZLE (H = 0.12)

Re = 4.51×10^4 per inch

 $\lambda = 0.0945$

Mesh: 61 x 11 x 31

FILM COOLING ANALYSIS

Re = 7.00 x 10^5 / in

Mesh: 101 x 81



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HOLDEN TEST CASE 45 COULING JET NOZZLE EXIT MACH NUMBER PROFILE COMPARISONS

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HOLDEN FILM COOLING TEST CASE 45 WITH L-CORRECTED MODEL OHEAT FLUX UNIT = BTU/FT///SLC)

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HOLDEN FILM COULING TEST CASE 45 WITH TURBU INLET DATA - MODEL COMPARISONS CHEAT FLUX UNIT+= BTU/FI2/SEC)

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GASL TEST CASE #41

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Re = 1.74×10^5 per inch

M_{air} = 3.84

 $P_{air} = 5.7 psia$ $T_{air} = 2000 {}^{\circ}R$ M_{H_2} = 2.50 (Fully Developed Laminar Profile)

 $Re_{H_2} = 2.557 \times 10^4$

 $P_{H2} = 16.6 \text{ psia}$

T_{H2} = 233 °R

Mesh: 101 x 81



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- COOLING JET EXIT BOUNDARY CONDITIONS ARE IMPORTANT FOR FILM COOLING ANALYSIS
- 3-D COMPUTATION OF COOLING JET NOZZLE FLOWFIELD PROVIDES THE NEEDED JET EXIT BOUNDARY CONDITIONS
- COMPRESSIBILITY CORRECTIONS FOR TWO-EQUATION TURBULENCE MODELS ARE EFFECTIVE FOR FILM COOLING ANALYSIS

APPLICATION TO STME NOZZLE FLOW

Mesh Size: 18,000 Grid Points

40,000 Grid Points

(2nd case in progress)

Two-Equation Turbulence Model With

Compressibility Correction

Finite-Rate Chemistry

(6 Species, 9 Reaction)

Subscale Nozzle Operating Conditions:

Nozzle: Re = 2.95 x 10⁵ (Vin) Mass Flow Rate = 82.6 (Ibm/sec) Re = 2190 Psia Te = 6700 R Min = 0.225 Min = 0.225 Sonic Jet: m = 0.254 Ibm/sec; P = 59.13 Psia Sonic Jet: m = 1.51 Ibm/sec; P = 59.13 Psia

 $T_{jet} = 530$ R









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SSME MCC and Nozzle Wall Heating











N92-32254

APPLICATION OF COMPUTATIONAL FLUID DYNAMICS TO THE DESIGN OF THE FILM COOLED STME SUBSCALE NOZZLE FOR THE NATIONAL LAUNCH SYSTEM.

By

Joseph L. Garrett Government Engine and Space Propulsion Pratt and Whitney West Palm Beach, Florida

ABSTRACT

A status of CFD calculations for the STME film/dump cooled nozzle design will be presented, with an emphasis on the timely impact of CFD in the design of the sub-scale nozzle coolant system. The following aspects of the sub-scale coolant delivery system were analyzed with CFD:

- 1. Design trade study of a mechanical flow splitting device for uniform distribution of the subsonic cavity flow.
- 2. Design trade study of the subsonic cavity lip to achieve coolant film integrity.
- 3. Analysis of the primary flow interaction with the core/secondary coolant streams.

All design calculations were performed with the Generalized Aerodynamic Simulation Program (GASP), a 3-D, multi-block, generalized Navier-Stokes code capable of solving with frozen, finite-rate or equilibrium chemical kinetics.

The initial design of the subsonic cavity flow used square posts to distribute the sonic orifice jets into a uniform flow. Calculations for this design indicated that an unacceptable mal-distribution of film occurred. Design modifications involving curved and slotted posts were computed in an effort to uniformly distribute the secondary coolant flow. Analysis of these configurations showed that although the flowfield improved in uniformity, it was still unacceptable, especially at higher feed pressures. Results from these studies were then incorporated into a design that resulted in the insertion of a porous metal ring into the subsonic cavity. Subsequent water flow model studies showed that this concept was successful in uniformly distributing flow exiting the cavity.

In addition to the design of the subsonic cavity, CFD was also used to analyze the secondary coolant lip and the primary flow interaction with the core/secondary coolant streams. A series of calculations were first performed to modify the subsonic cavity lip contour. The flow over the modified lip was then computed simultaneously with the primary injectors to determine the impact of the subsonic coolant stream on the primary slot jets.

Pressure, temperature, velocity and coolant mass fraction contours will be presented for these configurations.

APPLICATION OF CFD TO THE DESIGN OF THE

FILM COOLED STME SUBSCALE NOZZLE



CFD Applications In Rocket Propulsion – NASA MSFC Presented At 10th Annual Workshop For April 29, 1992

Joseph L. Garrett Pratt & Whitney, GESP West Palm Beach, Florida

ACKNOWLEDGEMENTS



O NASA MSFC Consortium For CFD In Combustion Driven Flows.

- **O National Aerodynamic Simulation Facility For CRAY YMP Computing Resources.** 899
- ^O CRAY Research For CRAY YMP Computing Resources.

OUTLINE



- **o** Analysis Of Secondary Coolant Cavity
- **Support Of Secondary Subsonic Lip Design** 0
- Analysis Of Core/Secondary/Primary Flow Interactions 0
- o Summary

CFD CODE USED

General <u>Aerodynamic</u> Simulation Program



- 3-D, 2-D or Axisymetric
- **O Parabolized & Full Navier-Stokes**
- ^O Explicit & Implicit Time Integration
- O Finite-Rate, Frozen & Equilibrium Chemistry
- ^O Algebraic & 2–Equation Turbulence Models
- **O Memory Management Techniques**



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Geometry Orientation

Subscale Thrust Chamber Assembly





ANALYSIS OF SECONDARY COOLANT CAVITY

Curve Post Design, Low P








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SUBSCALE CORE/FILM COOLANT INTERACTION

Previous Assumptions

- o Algebraic Turbulence Model
- o Equilibrium Chemistry in the Chamber
- o Frozen Chemistry in the Interaction Region
- o Chamber $P_0 = 2250 \text{ psi}, T_0 = 6500 \text{ }^{\circ}\text{R}$
- o Injector $P_0 = 70$ psi, $T_0 = 530^{\circ}R$
- o Chamber Walls Fixed at $T = 1440^{\circ} R$
- o Injector Walls are Adiabatic







	T 535.25 R 535.25 R 535.25 R 7.536 x 10 ⁻⁴ slug/ft ³ 1.023 x 10 ⁻³ slug/ft ³	Darameter Old Slot New Slot	tinent Geometry And Inflow Conditions	Naw Slot State New Slot 0.070" 0.070" 0.070" 94.26 psi 94.26 psi 94.26 psi 94.1 psi 94.1 psi 94.1 psi 535.25 R 3100 ⁻³ slug/ft ³	OF OLD & NEW SECONI And Inflow Conditions Old Slot 0.005" 0.210 lbm/sec 70 psi 530 R 530 R	Trinent Geometry Rlip Parameter P P P P
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t Geometry And Inflow Conditions	t Geometry And Inflow Conditions	t Geometry And Inflow Conditions		DARY SLOT	OF OLD & NEW SECONI	AKIDUIN



Note: Increasing Lip Radius and Flow Rate Result in Diminishing the Impact of Vortex Mixing





Imposed Bc	undary Values For High n	ı Case	
Property	Core Inflow	Subsonic Inflow	Primary Inflow
° Po	2250 psi	94.26 psi	
т _о	6780 R	535.5 R	
Σ	0.2233	0.05	1.456
٩	2187.38 psi	94.1 psi	55.5 psi
F	6735.0 R	535.25 R	372.1 R
Ò	1.448 x 10 ⁻² slug/ft ³	1.023 x 10 ⁻³ slug/ft ³	8.677 x 10 ⁻⁴ slug/ft ³
×	1.134	1.386	1.386
۰E	84.21 lbm/sec	0.352 lbm/sec	1.773 lbm/sec









Integrity of Primary Jet Maintained

H2 Mass Fraction Contours

0.04000 0.08000 0.12000	H. 16000 H. 20000	11. 28000 11. 28000 11. 32000	U. 36000 U. 40000	U. 4400U A. 4800B A. 5200B

H. LEARTON H. ZEARTON H. ZEARTON H. ZEARTON H. 200000 H. 920000 H. 92000 H. 92000 H. 92000 H. 920000 H. 920000 H. 9200 Note: Mixing of Jet with the core Indicates Exhaust Film is Less than 50% H₂



Primary Film Layer Provides Adequate Cooling For Nozzle Skirt

STPT

Temperature Contours (R)

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Nozzle Geometry & Film Injection Produce Shock Losses

Pressure Contours (psi)





SUMMARY



- o CFD Impacted The Design Of The Secondary Cavity Coolant **Distribution System.**
- **o CFD Used To Minimize Temperature Loads On The Injector Ring.**

FUTURE WORK



O Validate GASP With Subscale Nozzle Test Data.

^O Evaluate / Enhance Fullscale Design (Scaling Methodology).

N92-32255

COMPUTATIONAL FLUID DYNAMICS ANALYSIS OF SPACE SHUTTLE MAIN ENGINE MULTIPLE PLUME FLOWS AT HIGH-ALTITUDE FLIGHT CONDITIONS

by

N. S. Dougherty, J. B. Holt, B. L. Liu and S. L. Johnson Rockwell International Space System Division Huntsville, Alabama 35806

ABSTRACT

for the Consideration of WORKSHOP FOR COMPUTATIONAL FLUID DYNAMIC APPLICATIONS IN ROCKET PROPULSION APRIL 28-30, 1992

Computational fluid dynamics (CFD) analysis is providing verification of Space Shuttle flight performance details and is being applied to Space Shuttle main engine multiple plume interaction flow field definition. Advancements in real-gas CFD methodology described herein have allowed definition of exhaust plume flow details at Mach 3.5 and 107,000 ft. The specific objective of the study includes the estimate of flow properties at oblique shocks between plumes and plume recirculation into the Orbiter base so that base heating and base pressure can be model accurately. The approach utilizes the Rockwell USA Real Gas Three-Dimensional Navier-Stokes (USARG3D) Code for the analysis. The code has multi-zonal capability to detail the geometry of the plumes and base region and utilizes finite-rate chemistry to compute the plume expansion angle and relevant flow properties at altitude correctly. Through an improved definition of the base recirculation flow properties, heating and aerodynamic design environments of the Space Shuttle Vehicle can be further updated.

Results of IRAD work in progress indicate that at this altitude the plumes intersect and produce oblique shocks. At the hottest spot of the oblique shock between Engines 2 and 3, the recovery pressure and temperature were found to be 216 psfa and 5000 °F. There the flow resembles a location of a source flow with a discriminating streamline driving hot gas back into the base. Considerable exhaust gas is forced back toward the thermal shield of the Orbiter base between Engines 2 and 3, although Engine 1 flow is aspirated. The highest base temperature at the lower center of the heat shield reaches 2500 °F. Future work is planned to integrate the base flow solution to the integrated vehicle forebody flow for a total 'nose-to-plume' solution. With the vertical tail and OMS pods effects included later, it is expected that there may be recirculation of Engine 1 flow, also.

Space Shuttle Vehicle and Exhaust Plume Flows Computational Fluid Dynamics Analysis of at High Altitude Flight Conditions

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N.S. Dougherty, J.B. Holt, B.L. Liu, and S.L. Johnson Huntsville, Alabama 35806 Space Systems Division **Rockwell International**

April 21, 1992

Work Sponsored in part by NASA Johnson Space Center



Space Systems Division Huntsville Operations



Rockwell	International	Space Systems Division
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OBJECTIVE

Huntsville Operations

remain at high altitude conditions to improve Refined definition of Space Shuttle Vehicle effects to reduce small uncertainties that airloading and base recirculation plume payload managers' margin for

the vehicle as it flies today

- will fly after 1994 with ASRM's

Rockwell International	Space Systems Division

APPROACH

Huntsville Operations

dynamics (CFD) simulations are being extended Space Shuttle ascent computational fluid to 'nose-to-plume'

Present effort: at Mach 3.5 and 107,000 ft













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Rockwell ORI International Space Systems Division

ORBITER BASE HEATING MECHANISM

Huntsville Operations





	Rockwell International	CONCLUSIONS
	Space Systems Division	Huntsville Operations
	Space Shuttle simulation cor	forebody pressures in the CFD nfirm the wind tunnel data
94.3	 Space Shuttle detail on foreb shows no adve 	CFD simulation provides much greater ody pressures and temperatures and erse effects with ASRM's
	 Space Shuttle simulation sho good agreeme pressure/temp 	Main Engine exhaust plumes CFD ws base recirculation flow details and nt with Orbiter base heat shield erature data

N92-32256

Direct Numerical Simulation of a Combusting Droplet with Convection

P. Y. Liang

CFD Technology Center, Rocketdyne Division, Rockwell International Canoga Park, California

The evaporation and combustion of a single droplet under forced and natural convection has been studied numerically from first principles using a numerical scheme that solves the time-dependent multi-phase and multi-species Navier-Stokes equations and tracks the sharp gas-liquid interface cutting across an arbitrary Eulerian grid. The flow fields both inside and outside of the droplet are resolved in a unified fashion. Additional governing equations model the inter-phase mass, energy and momentum exchange. Test cases involving iso-octane, n-hexane and n-propanol droplets show reasonable comparision with experimental data regarding parameters such as breakup mode, evaporation rate and flame stand-off distance. The partially validated code is thus readied to be applied to more demanding droplet combustion situations where substantial drop deformation render classical models inadequate.

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OBJECTIVE	
STUDY THE EVAPORATION AND COMBUSTION OF A SINGLE DROPLET UNDER FORCED AND NATURAL CONVECTION FROM FIRST PRINCIPLES	
Rockwell International Rocketdyne Division	

SIGNIFICANCE DIRECT MODELING OF BOTH DROPLET <u>AND</u> AMBIENT IN UNIFIED CFD MODEL REMOVES CONSTRAINTS DUE TO ASSUMPTIONS OF
SPHERICAL SYMMETRY
SMALL CONVECTIVE EFFECTS
LOW EVAPORATION RATE (NO BLOWING)
SHARP FLAME FRONT (INSTANTANEOUS AND COMPLETE COMBUSTION)
Rockwell International Rocketdyne Division

Control Volume Next to Droplet Surface



Governing Equations

Continuity equation integrated twice to yield

$$\dot{\mathbf{N}}_1$$
 ($\Delta \mathbf{z}$) = c $\operatorname{seln}\left(\frac{1-X_1 \operatorname{gas}}{1-X_1 \operatorname{surface}}\right)$

P

$$\hat{\mathbf{m}}_{vap} = \frac{\mathbf{c} \, \mathfrak{M}_1 \, \mathbf{A}_s}{\Delta \mathbf{z}} \ln \left(\frac{1 - \mathbf{X}_{1gas}}{1 - \mathbf{X}_1 surface} \right)$$

Assuming N_{total} ≈ N₁

Governing Equations

Final heat-up rate equation for multi-species

$$V_{\ell} \Big(c_{\ell} \, \hat{M}_1 \Big) \Big(\frac{c_{p_{1\nu}}}{\hat{M}_1} \Big) \frac{dT_{\ell}}{dt} = \frac{k \, \xi \, A_s \left(T_g - T_{\ell} \right)}{\left(\Delta z \right) \left(e^{\xi} - 1 \right)} - \frac{1}{\hat{m}_{vap}} \left(\frac{\Delta H_{vap}}{\hat{M}_1} \right)$$

where

$$\xi \equiv \frac{\dot{N}_{1} c_{p_{1}v}(\Delta z)}{k} = \frac{\dot{m}_{vap}}{A_{s}} \left(\frac{c_{p_{1}v}}{M_{1}}\right) \frac{(\Delta z)}{k}$$

Equation for single species

$$\mathbf{\hat{m}}_{vap} = \mathbf{A}_{s} \mathbf{E}_{p} \left(\mathbf{p}_{vap} - \mathbf{p} \right) \left(\frac{\mathbf{M}_{1}}{2\pi \mathbf{R} \mathbf{T}_{\ell}} \right)^{1/2}$$

Governing Equations

Energy equation integrated twice to yield

$$\dot{q}_{\ell} \left[e \dot{\dot{N}}_1 \ c_{p_1 \upsilon} \left(\Delta z \right) / k \ -1 \right] \ = \ \dot{\dot{N}}_1 \ c_{p_1 \upsilon} \left(T_g \ - \ T_\ell \right)$$

where $\dot{\mathbf{q}}_\ell$ is in turn given by

$$\dot{\mathbf{q}}_{\ell} = \frac{V_{\ell}}{A_{s}} c_{\ell} c_{p_{1\ell}} \frac{dT_{\ell}}{dt} + \dot{\mathbf{N}}_{1} \left(\Delta H_{vap} \right)$$

ARICC-ST MODELS

- FULL NAVIER-STOKES IN BOTH GAS AND LIQUID PHASES
- TWO PHASE, VOLUME-OF-FLUID, WITH SURFACE TRACKING
- VARIABLE TEMPERATURE IN BOTH PHASES

953

INTER-PHASE MASS AND HEAT TRANSFER (EVAPORATION) AND SURFACE TENSION





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Fig. 2 Bag Mode Breakup of Simulated (a & c) and Experimental (b) Droplet Due to Shock Wave Passage. (c) was done with evaporation and ignition.



955

Highlight of Problem Parameters for Combusting Droplet With Convection Simulations Table 1.

Forced Convection

Natural Convection

Liquid	n-Hexane (C ₆ H ₁₄)	n-Propanol (C ₃ H ₇ OH)
MM	86.178	60.096
Surface tension (dynes/am)	14.4 (at 333 K) ,	23.04 (at 293 K)
Density (g/cc)	.521 (at 423,K)	.804 (at 293 K)
Viscosity (poise)	.21554 x 10 ^{-c} (at 342 K)	.464 x 10 ^{-c} (at 370 K)
Conductivity (ergs/am-s-K)	1.1076 × 10 ⁴ (at 342 K)	1.4255 × 10 ⁴ (at 370 K)
Vapor pressure (mtHg)	exp(15.84-2698/(T-48.78))	exp(17.54-3166/(T-80.15))
Latent heat (ergs/g)	$3.165 \times 10^9 ((1-\Gamma_r)/(1-\Gamma_{r,mef})) \cdot 375$	$6.952 \times 10^9 ((1-T_r)/(1-T_r, r_{ref}))^{375}$
	$T_r = T/T_{crit}$, $T_{crit} = 507.6$	$T_{crit}=536.7$
Initial drop diam. (cm)	.1815	.210
Initial drop temp (K)	355.0	293.0
Anbient	N	Air
Initial temp. (K)	470.0	293.0
Pressure (atm.)	13.6	S
Prandtl number	.714 .	.75 ,
Viscosity (poise)	1.925 x 10 ⁻⁴ (at 470 K)	1.813 x 10 ⁻⁴ (at 293 K)
Grid size	30 × 100	35 × 105

2

956



Fig. 3 Numerical vs Experimental Drop Diameter and Drop Center Temperature Histories in Forced Convection



Fig. 4 Numerical vs Experimental Drop Diameter Histories in Natural Convection. Dashed line is reference D²-law



Fig. 5 Flame Stand-off Distance and Drop Center Temperature vs Time in Natural Convection

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Sequence of Simulated Temperature Contours in Grey Scale Showing Initial Transient of n-Propanol Droplet Combusting with Natural Convection. (white Tmax=2500 K, black Tmin=300 K) Fig. 6







t = .110 sec

Fig.8 Close-up View of Velocity Vector Plot from n-Propanol Drop Combustion Under Natural Convection Simulation





CONCLUSIONS	
SIMULATIONS OF DEFORMING, EVAPORATING AND COMBUSTING DROPS PERFORMED WITHOUT EMPIRICAL INPUTS	
REASONABLE COMBUSTION RATE, EVAPORATION RATE AND TEMPERATURE DISTRIBUTION OBTAINED	
EFFECT OF EVAPORATION ON BREAKUP MODE REQUIRE MANY MORE PARAMETRIC STUDIES	
DETAILS OF INTERNAL RECIRCULATING FLOWFIELD REQUIRE LARGE GRID CONCENTRATION AROUND BOUNDARY LAYER	
Rockwell International Rocketdyne Division	

N92-32257

A NUMERICAL MODEL FOR ATOMIZATION-SPRAY

COUPLING IN LIQUID ROCKET THRUST CHAMBERS

by

M. G. Giridharan, A. Krishnan, J. J. Lee and A. J. Przekwas CFD Research Corporation, Hunstville, AL 35802 and

K. Gross NASA Marshall Space Flight Center, Hunstville, AL 35802

The physical process of atomization is an important consideration in the stable operation of liquid rocket engines. Many spray combustion CFD codes do not include an atomization sub-model but assume arbitrary drop size distributions, drop initial locations and velocities. It has been shown that the results of spray combustion models are extremely sensitive to the assumed droplet initial conditions. Furthurmore, the atomization process itself is a strong function of the local conditions of the liquid and gas flow. Thus it is important to account for the strong mutual coupling between the liquid phase, the spray dynamics and the gas flow. A method of coupling an atomization model with the spray model in a REFLEQS CFD code will be presented. This method is based on a novel Jet-Embedding technique in which the equations governing the liquid jet core are solved separately using the surrounding gas phase conditions. The droplet initial conditions are calculated using a stability analysis appropriate for the atomization regime of liquid jet break-up.

This novel coupling model is used to analyze the SSME fuel preburner single injector flow. Results of the diffusion flame characteristics in a single injection element will be presented. The effect of relative velocity, mixture ratio and droplet initial conditions will be shown. The predictions of present atomization model is compared with that of the widely used CICM correlation. The results are also compared with the predictions of volume-of-fluid method.

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A NUMERICAL MODEL FOR ATOMIZATION-SPRAY

COUPLING IN LIQUID ROCKET THRUST CHAMBERS

^

M.G. Giridharan, J.J. Lee, A. Krishnan and A.J. Przekwas **CFD Research Corporation**

Marshall Space Flight Center K. Gross and

10th Annual CFD Workshop NASA - MSFC April 30, 1992

OUTLINE

-CFD3C

- Introduction
- Atomization-Spray Coupling Model
- **Validation**
- Demonstration Results

967

Conclusions

INTRODUCTION



- Importance of an Atomization-Spray Coupling Model
- Two Approaches:
- Interface Capturing VOF Methodology Interface Fitting Jet-Embedding
- **Atomization Models**

968

- **Meyer's Model**
- Linear Dispersion Equation
- Spray Model
- Eulerian/Lagrangian Particle Tracking ł

Temperature Distribution in the Thrust Chamber

Ud = Vd = 25.0 m/s, Dd = 25 Microns

lsp = 318.6 seconds



Temperature Distribution in the Thrust Chamber

Ud = Vd = 25.0 m/s, Dd = 100 Microns

lsp = 313.8 seconds



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ATOMIZATION MODELS

-CFD3C

Meyers Model

- Energy Balance at the Interface

Linear Theory

- Dispersion Relationship: Growth Rate = F (λ , r, s, Re, We)



SPRAY MODEL

- Improved Version of PSI-CELL Model
- Deterministic Droplet Tracking
- Coupled Droplet Source/Sink Terms for the Gas Phase
- Droplet Boundary Conditions
- Wall Zero Normal Momentum
 - Symmetry Reflection

PR-92-15/15

COUPLING MODEL (jet-embedding technique)

echnique)

LIQUID PHASE CALCULATION:

Obtain Shape and Velocity of Intact Liquid Core



Space-MarchingTechnique

COUPLING MODEL

GAS PHASE CALCULATION:

- REFLEQS CFD Code
- Gas Phase Grid is Adapted to the Shape of the Core
- Interface Modeled as Sliding Wall

974

- Combustion Model:
- Instantaneous Chemistry Model

PR-92-15/05

FLOW CHART OF COUPLING PROCEDURE CFDRC Initial guess for gas velocity and density at the interface New gas velocity and Solve 1-D jet core density at the interface equations **Obtain local diameter** of the core and its velocity No Prepare initial conditions for the spray model, i.e., the breakup rate and droplet size Yes distribution Stop (If converged Adapt the gas phase grid to the liquid jet core shape Obtain gas phase Impose the sliding wall solution using boundary condition at the interface REFLEQS

4041-09/91 prog.

VALIDATION

-CFD3C

Experimental Data

- Low Speed Water Jet
 Experiments by Chigier (1990)
- Reynolds Number: 1460-9300
- Weber Number: 50-200
- Jet Intact Core Length from Photographs
- Drop Size (PDPA)


VALIDATION (CONTINUED)

Comparison of Predictions with Experimental Data



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SSME Preburner Flow Field

Operating Condition

idizer Fu .OX) (GI	0.1	25	1122	106	
OX OX	ŵ, kg/sec 0	u ₀ , m/sec	Po, kg/m ³	т, ∘К	

Coaxial Injection Element

















Axial Distance







Ug = 200.0 m/s, UI = 25.0 m/s, Tg = 200 K(CICM Correlation)



Temperature Distribution



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Oxygen Mass Source (gms/sec) Distribution

Ug = 200.0 m/s, UI = 25.0 m/s, Tg = 200 K

(Linear Surface Wave Model)



Temperature Distribution



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Ug = 150.0 m/s, Ul = 25.0 m/s, Tg = 200 K (CICM Model)





Passive Scalar (Hydrogen) Concentration Distribution

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CONCLUSIONS



- Developed a New Jet-Embedding Technique to Couple Atomization and Spray Models
- Predictions have been Validated with Water Jet Data
- to SSME Single Injector Flow and Could be Extended Coupling Model has been Successfully Employed to Multi-Injector Flow
- Computationally Efficient Tool for Rocket Injector Flow Analysis

Numerical Modeling for Dilute and Dense Sprays

N92-32258

C.P. Chen, Y.M. Kim, H.M. Shang, and J.P. Ziebarth University of Alabama in Huntsville

> T.S. Wang NASA Marshall Space Flight Center

Abstract

Numerical modelings of fuel-droplet spray combustion finds useful applications for the assessment of the engine performance & stability characteristics. With our ongoing studies on turbulent reacting flows, we have successfully implemented a numerical model for spray-combustion calculations. In this model, the governing gas-phase equations in Eulerian coordinate are solved by a time-marching multiple pressure correction procedure based on the operator-splitting technique. The droplet-phase equations in Lagrangian coordinate are solved by a stochastic discrete particle technique. In order to simplify the calculation procedure for the circulating droplets, the effective conductivity model is utilized. This vaporization model includes the effects of variable thermophysical properties, non-unitary Lewis number in the gas-film, the Stefan flow effect, and the effect of internal circulation and transient liquid heating. The $k - \epsilon$ models are utilized to characterize the time and length scales of the gasphase in conjunction with turbulent modulation by droplets and droplet dispersion by turbulence. This method entails random sampling of instantaneous gas flow properties and the stochastic process requires a large number of computational parcels to produce the satisfactory dispersion distributions even for rather dilute sprays.

The present study has made two major improvements in spray combustion modelings. Firstly, we have developed a probability density function approach in multidimensional space to represent a specific computational particle. Advantages of a parcel PDF tracking method is to reduce the number of computational parcels representing the spray dynamics as well as to obtain grid- independent solutions for two-phase flows. Secondly, we incorporate the TAB Taylor Analogy Breakup model for handling the dense spray effects. These breakup models is based on the reasonable assumption that atomization and drop breakup are indistinguishable processes within a dense spray near the nozzle exit. Accordingly, atomization is prescribed by injecting drops which have a characteristic size equal to the nozzle exit diameter.

Example problems include the nearly homogeneous and inhomogeneous turbulent particle dispersion, and the non-evaporating, evaporating, and burning dense sprays. Comparison with experimental data will be discussed in detail.

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NUMERICAL MODELING FOR DILUTE AND DENSE SPRAYS

Y.M. Kim, H.M. Shang, C.P. Chen, and J.P. Ziebarth University of Alabama in Huntsville

and

T.S. Wang NASA/Marshall Space Flight Center 10th Workshop for CFD Applications in Rocket Propulsion April 28-30, 1992 NASA/Marshall Space Flight Center

MOTIVATION

- To attain a prediction capability to assess the performance and the stability characteristics of liquid-fueled engines.
- To appraise the physical submodels as well as to evaluate numerical procedures for prediction of spray-combusting flows.
- To gain fundamental understanding of the effects of vaporization, swirl, initial size distribution, and droplet dispersion.
- To provide reliable distribution of drop size and velocity.
- To develop an efficient, accurate, and stable numerical model spray combustion.

APPROACH

- Stochastic Particle Tracking Technique
- Delta function stochastic separated flow(SSF) model
- Deterministic dispersion width transport(DDWT) model
 - Stochastic dispersion width transport(SDWT) model
- Incorporation of Dense Spray Effects
- Taylor analogy breakup(TAB) model.
 - Drop collision and coalescence model
- Eulerian-Lagrangian Formulation
 - Multiple pressure correction
- Non-iterative for transient calculation
- Applicable to all-speed flows

ISSUES

- Turbulene effects on droplets and turbulece modulation by droplets.
- Incorporation of dense spray effects and primary atomization model.
- Vaporization at subcritical and supercritical condition.
- Numerical accuracy, stability, and efficiency for the fast transient spray-combusting flows.

GROUP/WIDTH DISPERSION MODEL



Turbulence-induced displacement and velocity:

$$\frac{dv'_k}{dt} = \frac{u'_k - v'_k}{\tau_k}$$
$$\frac{dx'_k}{t} = v'_k$$

Particle fluctuating locations and velocities:

dt

$$k_{i} = u'_{k_{rms}} \Delta t_{ki} + (v'_{k(i-1)} - u'_{k_{rms}}) \tau_{k(i-1)} (1 - e^{\tau_{k(i-1)}})$$
$$v'_{ki} = u'_{k_{rms}} + (v'_{k(i-1)} - u'_{k_{rms}}) e^{\frac{-\Delta t_{ki}}{\tau_{k(i-1)}}}$$

`~;

 $-\Delta t_{k_1}$

Time step to interact with k^{th} eddy:

$$\sum_{i=1}^{m} \Delta t_{ki} = \Delta t_k$$

Variance of a computational particle pdf within the k^{th} eddy:

$$\sigma_k^2 = \sigma_{k-1}^2 + (\sum_{i=1}^m x'_{ki})^2$$

Normalized particle variance:

$$\hat{\tau}_{yk} = K \frac{\sigma_{yk}}{\sqrt{N}_t}$$

 $\frac{\sigma_{yk}}{\sqrt{N_t}}$ = statistical uncertainty in the mean particle position K = correction factor to account for undersampling $N_t = total$ number of computational particles

 $\sigma_{k-1} =$ existing variance of the particle pdf

Cumulative pdf distribution at any point in coordinate y:

$$P(y) = \int_{-y}^{y} \frac{1}{\sqrt{2\pi}\hat{\sigma}_{yk}} e^{\frac{-(y-y_{p})^{2}}{2\hat{\sigma}_{yk}^{2}}} dy$$

Symmetric cumulative distribution function:

$$P(y) = 0.5[erf(\frac{y-y_p}{\sqrt{2}\hat{\sigma}_{yk}}) + erf(\frac{y+y_p}{\sqrt{2}\hat{\sigma}_{yk}})]$$

Two ways to calculate the mean position of parcel:

- Deterministic Dispersion Width Transport(DDWT) model
 Stochastic Dispersion Width Transport(SDWT) model

Mean collision rate between each pair of "parcels" coexisting in a given numerical cell:

$$\nu = \frac{N_1}{Vol}\pi(r_1 + r_2)^2 \mid v_1 - v_2 \mid /N_2$$

• Probability(Poisson distribution) occuring n collisions in time Δt :

$$P_n = e^{-\overline{n}} \frac{\overline{n}^n}{n!} \quad (\overline{n} = \nu \Delta t, \quad P_o = e^{-\overline{n}} : \quad probability \quad of \quad no \quad collision)$$

• Stochastic collision sampling procedure:

$$XX < P_o \Rightarrow no \ collision$$

$$XX > P_o \Rightarrow$$
 collision (collision parameter, $b = \sqrt{YY}(r_1 + r_2)$)
 $b < b_{cr} \Rightarrow$ coalescence, $b \ge b_{cr} \Rightarrow$ grazing collision
 $b_{cr} = f(drop \ radii, \ surface \ tension, \ relative \ velocity)$
 $XX, \ YY \ : \ 1st \ and \ 2nd \ random \ number$

	Mass conservation $\rightarrow N^{n+1} = N^n \left(\frac{r^n}{r_{br}}\right)^3$	Energy conservation $\rightarrow r_{32} = \frac{r}{1 + \frac{8K}{20} + \frac{\rho_1 r^3}{\sigma} y'^2 \frac{(6K-5)}{120}}$ chi - squared distribution for product drops(rbr)	$t^n < t_{br} < t^{n+1}$: breakup	vo Extra Equations (y_p, y'_p) - $y_p \rightarrow deformation$ and $y'_p \rightarrow oscillation$ - functions of We, viscous damping time, and oscillation frequency cillation amplitude, frequency, y_p , and $y'_p \rightarrow t_{br}$	 ylor Analogy Breakup Model analogy between an oscillating & distorting drop and spring-mass system gas aerodynamic fsurface tension fliquid viscous f.
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BREAKUP MODEL

996

VALIDATION CASES

- Particle Turbulent Dispersion(Snyder et. al.) Particle Laden Turbulent Round Jet(Yuu et. al.)
- Non-Evaporating Solid-Cone Spray(Hiroyasu et. al.)
 Non-Evaporating Hollow-Cone Spray(Shearer et. al.)
 Evaporating and Burning Spray(Yokota et. al.)



Figure 1. Particle dispersion of a nearly-homogeneous flow for SSF model(5000 particles) and DDWT model.



SSF model(10,000 particles) and SDWT model(50 parcels) with various correction factors. Figure 2. Normalized particle concentration distribution of particle laden round jet for



Figure 3. Normalized particle concentration distribution of particle laden round jet for SDWT model(200 parcels) with various correction factors.



Figure 4. Normalized particle concentration distribution of particle laden round jet for SSF model(10,000 particles) and SDWT model(200 parcels).



Figure 4.22 Spray parcel distribution in a solid-cone spray (t = 3.0ms)

1002



















Figure 4.26 Spray tip penetration versus time in a hollow-cone spray

















SUMMARIES

- Efficient Particle Dispersion Modeling by DDWT and SDWT.
- Good Agreement with Experiment for Dense Spray Cases.
- Extension of SDWT to Evaporating and Burning Dense sprays.
- Implementation of Volume of Fluid(VOF) method.
- Incorporation of Supercritical Vaporization Model.

N92-32259

Modeling of SSME Fuel Preburner ASI

P. Y. Liang CFD Technology Center Rocketdyne Division, Rockwell International Corporation Canoga Park, California

The Augmented Spark Ignitor (ASI) is a LOX/H2/electrical spark system that functions as an ignition source and sustainer for stable combustion. It is used in the SSME preburner combustor, the SSME main combustion chamber, the J-1 and J-2 engines as well as proposed designs of the Space Transportation Main Engine (STME) main combustor and gas generators. In the SSME it is a long circular cylindrical chamber located along the Main Combustor centerline with a truncated conical dome at the top, which contains two oblique LOX injection ports and two spark plugs offset at 90 degrees. Hydrogen injection is through a number of nearly tangential slots downstream which creates a swirl flow intended to cool the ASI chamber walls. Past incidents of erosion of the ASI spark plugs have often led to the need for replacement of these very costly devices. Thus it is desirable to understand the complex reactive flow field within the ASI both during the initial ignition transient and during the main stage steady state combustion (no sparking).

While it is impossible to perform direct optical diagnostics to measure the internal flow field of the ASI under hot-fire conditions, recent advances in CFD-based combustion modeling have made it feasible to characterize the flow through time-accurate simulations. This paper documents an undertaking to characterize the flow of the ASI. The code consists of a marriage of the Implicit-Continuous-Eulerian/Arbitrary-Lagrangian-Eulerian (ICE-ALE) Navier-Stokes solver with the Volume-of-Fluid (VOF) methodology for tracking of two immiscible fluids with sharp discontinuities. Spray droplets are represented by discrete numerical parcels tracked in a Lagrangian fashion. Numerous physical sub-models are also incorporated to describe the processes of atomization, droplet collision, droplet breakup, evaporation, and droplet and gas phase turbulence. An equilibrium chemistry model accounting for 8 active gaseous species is also used. Taking advantage of the symmetry plane, half of the actual ASI is modeled with a 3-dimensional grid that geometrically resolves the LOX ports, the spark plug locations, and the hydrogen injection slots. The pertinent features and formulations of these submodels will be briefly described in the paper.
IR ASI		CFD 62-000-005/D2PM
IG OF SSME FUEL PREBURNE	PAK-YAN LIANG	OCKWELL INTERNATIONAL CORPORATION ROCKETDYNE DIVISION
MODELII		Rockwell International Rocketdyne Division



	SIGNIFICANCE
	EROSION AND REPLACEMENT OF ASI SPARK PLUGS EXTREMELY COSTLY
	DESIRABLE TO UNDERSTAND REACTIVE FLOWFIELD INSIDE ASI DURING IGNITION TRANSIENT AND MAIN STAGE
1016	DIAGNOSTICS WITHIN ASI VERY DIFFICULT
	MAY REPLACE ONE SPARK PLUG WITH SEEDING DEVICE FOR PLUME MEASUREMENTS IN TESTS
	Rockwell International Rocketdyne Division

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Fig. 5 Plots of droplet parcels for (a)case 2 (b)case 2 (c)case 4 1018







Fig. 2 Variation of penetration with orifice diameter; $V_g = 100 \text{ m/s}$, $V_1 = 15 \text{ m/s}$.



Fig. 3 Streamwise SMD profiles for various orifice diameters (d_j); V_g=100 m/s, V_l=15 m/s.



Fig. 4 Influence of airstream velocity on mean
 dropsize taken at 12 cm station; V₁=15 m/s,
 d₁ =1.3 mm(comp), =1.5 mm(exp).
 j₀



Fig. 1 Schematic of SSME Preburner ASI. (LOX ports are actually 90 deg. apart from spark plugs rather than being on same meridian plane as shown)



Fig. 2 Close-up Side and Top Views of ASI Dome Region



Fig. 3 Computational Grid (Partial) Across a J-plane (shown reflected across central axis to represent full chamber)



Fig. 4 Velocity Profiles In Vertical and Horizontal Cross Sectional Planes Before Ignition (t=.737 msec)



(c) temperature at k=6

Fig. 5 Transient Temperature and Velocity Fields During and Right After Ignition by Spark Plugs



(a) velocity

(b) temperature

(c) log 0₂ conc.





(a) velocity

(b) temperature

- (c) log 0₂ conc.
- Fig. 7 Velocity, Temperature and Log 0; Concentration Profiles Across k=6 Plane at Pseudo-steady State (t=4.10 msec)





Fig. 8 Log H_2^0 Concentration Profiles at t=4.10 msec



CFD MODELING OF TURBULENT FLOWS AROUND THE SSME MAIN INJECTOR ASSEMBLY USING POROSITY FORMULATION

Gary C. Cheng^{*}, Y.S. Chen[†], and Joseph H. Ruf[‡]

<u>Abstract</u>

Hot gas turbulent flow distributions around the main injector assembly of the Space Shuttle Main Engine (SSME) and LOX flow distributions through the LOX posts have great effect on the combustion phenomenon inside the main combustion chamber. An advanced computational fluid dynamics (CFD) analysis will help to provide more accurate and efficient characterization of this type of flow field. In order to design a CFD model to be an effective engineering analysis tool with good computational turn-around time (especially for 3-D flow problems) and still maintain good accuracy in describing the flow features, the concept of porosity is employed to describe the effects of blockage and drag force due to the presence of the LOX posts in the turbulent flow field around the main injector assembly of the SSME. A validated non-isotropic porosity model is developed and incorporated into an existing Navier-Stokes flow solver (FDNS). Volume and surface porosity parameters, which are based on the configurations of local LOX post clustering, will be introduced in to the governing equations, which can be written as

$$\frac{1}{J}\left(\mathbf{v}_{\mathbf{v}}\frac{\partial\rho\,\mathbf{q}}{\partial t}\right) = -\frac{\partial\mathbf{v}_{i}F_{i}}{\partial\xi_{i}} + \mathbf{v}_{\mathbf{v}}S_{\mathbf{q}} + R_{\mathbf{q}}$$

where J is the Jacobian, F_i is the sum of the convective flux and the viscous flux, v_i is the surface porosity, v_v is the volume porosity, S_q and R_q are the source and residual terms of the flow variable q, respectively. The drag force and the heat flux source due to the presence of LOX posts will be added to the residual term. 2-D numerical studies have been conducted to identify the drag coefficients of the flows both through tube banks and around the shielded posts with a wide range of Reynolds numbers. A verified model of the drag coefficients is incorporated into the FDNS flow solver. A 2-D flow study of the main injector assembly is performed to verify the proposed porosity model. A reasonable O/F ratio distribution was obtained, therefore, a 3-D CFD analysis is conducted with confidence. The 3-D CFD analysis of the SSME main injector assembly is divided into three parts, LOX dome, LOX post assembly torus, and hydrogen cavity. A 62 x 91 x 16 mesh system is constructed for the LOX dome, where a 37 x 91 x 25 grid system is employed for the torus region, and the hydrogen cavity is discretized into a 29 x 91 x 14 mesh system. The numerical study of the turbulent flow in the SSME Phase II+ power head is analyzed based on 104% power balance level, and the result will be presented in the coming CFD workshop meeting.

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CFD MODELING OF TURBULENT FLOWS WITHIN SSME MAIN INJECTOR ASSEMBLY USING A **POROSITY MODEL**

By

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AND

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NASA Contract No. NAS8-38871

- OBJECTIVE
- NUMERICAL APPROACH
- PROPOSED POROSITY MODEL
- 3-D POROSITY/CFD ANALYSIS OF PHASE II+ POWER HEAD
- CONCLUSIONS AND RECOMMENDATIONS

0	BJECTIVE
•	DEVELOPMENT OF ROBUST CFD METHODOLOGY FOR TURBULENT FLOWS IN THE ENGINE 0209
1036	VALIDATION OF A POROSITY MODEL FOR NAVIER-STOKES FLOW SOLVER
	PREDICTION OF LOCAL MASS FLOW RATE AND O/F RATIO DISTRIBUTIONS DOWNSTREAM OF THE PRIMARY FACE PLATE



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Z	UMERICAL APPROACH
	FLOW AROUND LOX POST ELEMENTS IN SIMULATED AS
	MASS FLOW RATE THROUGH POST ELEMENTS AND THROUGH POROUS PLATES ARE CALCULATED BASED ON POROSITY MODEL
1038	BENCHMARK THE MODELS FOR POROUS MEDIA
	o Flow Through Tube Banks
	o Flow Through Shielded Posts With and Without Holes
	3-D POROSITY MODEL/CFD ANALYSIS OF THREE COMPONENTS OF THE POWER HEAD (LOX DOME, LOX POST ASSEMBLY, HYDROGEN CAVITY)

DRAG COEFFICIENTS FOR FLOW THROUGH TUBE BANK

- **o** NON-SHIELDED ELEMENTS
- Re (Local Flow Reynolds no.) < 4 x 10³

 $C_d = 0.417 EXP(4.932 Re^{-0.296})$

4 x 10³ < Re < 6 x 10⁴

 $C_d = 0.647 - 0.5 \times 10^{-6} \text{ Re}$

6 x 10⁴ < Re < 10⁶

$$C_d = 0.618 + 0.491 \times 10^{-6} \text{ Re} - 6.303 \times 10^{-12} \text{ Re}^2 + 10.694 \times 10^{-18} \text{ Re}^3 - 5.2 \times 10^{-24} \text{ Re}^4$$

► Re > 10⁶

 $C_{d} = 0.2735$

SHIELDED ELEMENTS

- With Holes: $C_d = 4$.
- Without Hole: $C_d = 48$.

LOX DOME POROSITY MODEL (104% RPL)

K (Loss Coeff.)
$$\equiv \sqrt{\frac{\rho \, \Delta P}{\dot{m}^2}}$$
; $\Delta P = P_{exit} - P_{chamber}$; or $\Delta P = P_{exit} - P_{baffle}$

	m (lb/sec)	ΔP(psi)	K (ft ⁻⁴)
Non-Baffle Elements	665.105	575.07	4.14 × 10 ²
Baffle Elements	105.65	625.49	1.785 x 10 ⁴
First Three Rows	56.154	575.07	5.809 x 10 ⁴

LOX POST ASSEMBLY POROSITY MODEL (104% RPL)

Baffle	Elements	8
ents	Row #1 - #11	152
on-Baffle Eleme	Row #12	156
Ž	Row #13	135
		K (in ⁻⁴)

HYDROGEN CAVITY POROSITY MODEL (104% RPL)

	ṁ (lb/sec)	ΔP (psi)	K (ft ⁻⁴)
Primary Face Plate	6.77	251	3.578 x 10⁴
Secondary Face Plate	3.41	86	5.506 x 10 ⁴
Baffle Elements	15.25	301	8.467 x 10 ³
Non-Baffle Elements	0	251	8
BLC Holes	3.67	251	1.16 x 10 ⁵

3-D POROSITY/CFD ANALYSIS OF PHASE II+ POWER HEAD

LOX DOME

- o GRID SIZE: 62 x 91 x 16
- INLET FLOW CONDITIONS
- Static Pressure: 3670 psi
- Static Temperature: 197 °R
- Reynolds no.: 1.28 x 10⁸ ft⁻¹
- Mass Flow Rate: 826.7 lb/sec
- INCOMPRESSIBLE, SINGLE SPECIES







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MAIN INJECTOR ASSEMBLY WITH TRANSFER DUCTS

- THREE ZONES
- Zone #1: 37 x 91 x 25 (Main Injector Assembly)
- Zone #2: 10 x 21 x 17 (Fuel Transfer Duct)
- Zone #3: 10 x 15 x 15 (Oxidizer Transfer Duct)
- o INLET FLOW CONDITIONS:
- Fuel Side (Reference Conditions)

Static Pressure: 3351 psi

Static Temperature: 1666 °R

Reynolds no.: 3.17 x 10⁷ ft⁻¹

Mass Flow Rate: 77.55 lb/sec (symmetrical)

O/F Ratio: 0.8685

Oxidizer Side

Static Pressure: 3353 psi

Static Temperature: 1254 °R

Mass Flow Rate: 33.375 lb/sec (symmetrical)

O/F Ratio: 0.599

U/U_{ref}: 0.693

INCOMPRESSIBLE, ISOTHERMAL, TWO SPECIES, NON-REACTING FLOW 0



Geometry of Hot Gas Injector Assembly











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CONTOUR LEVELS -63.5 -63.5 -63.1 -63.1 -64.0 -61.5 -61.5 -61.5 -53.5

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HYDROGEN CAVITY

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- o GRID SIZE: 29 x 91 x 14
- INLET FLOW CONDITIONS
- Static Pressure: 3395 psi
- Static Temperature: 448.66 °R
- Reynolds no.: 2.52 x 10⁷ ft⁻¹
- Mass Flow Rate: 14.55 lb/sec (symmetrical) ▲
- INCOMPRESSIBLE, SINGLE SPECIES







-22.8 -19.0 -16.0 -16.0 -13.0 -1.0 -46.0 -43.0 -40.0 -37.0 -31.0 -31.0





THE O/F RATIO DISTRIBUTION ALONG THE OUTER EDGE OF THE INJECTOR FACE (NO BLC COOLANT ADDED)







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THE O/F RATIO INJECTOR FACE CWITH BLC COOLANT ADDED (FUEL SIDE) OF





	ŏ	CONCLUSIONS AND RECOMMENDATIONS	1
	ightarrow	 THE PREDICTED O/F RATIO IS CLOSE TO STOICHIOMETRIC AROUND BAFFLE ELEMENTS 	
	•	 THE RESULTS OF THIS STUDY SHOULD BE USED TO PREDICT ENGINE PERFORMANCE AND HEAT LOADS 	
1069	•	 LOCAL MASS FLOW RATE DISTRIBUTION IS DEPENDENT ON PRESSURE AND LOSS COEFFICIENT DISTRIBUTION 	
	•	 THE 3-D POROSITY/CFD ANALYSIS OF THE POWER HEAD CAN BE IMPROVED BY 	
		 KNOWING THE DISTRIBUTION OF CHAMBER PRESSURE AN OF BAFFLE ELEMENT DISCHARGE PRESSURE 	~
		 THE MEASUREMENT OF LOSS COEFFICIENTS FOR EACH COMPONENTS 	
		 USING PROPER INLET FLOW PROFILES TO THE LOX DOME 	

N92-32261

Computational Fluid Dynamics Analysis of SSME Phase II and Phase II+ Preburner Injector Element Hydrogen Flow Paths

Joseph H. Ruf

Computational Fluid Dynamics Branch

Marshall Space Flight Center, NASA

Phase II+ Space Shuttle Main Engine powerheads E0209 and E0215 degraded their Main Combustion Chamber (MCC) liners at a faster rate than is normal for phase II powerheads. One possible cause of the accelerated degradation was a reduction of coolant flow through the MCC. Hardware changes were made to the preburner fuel leg which may have reduced the resistance and, therefore, pulled some of the hydrogen from the MCC coolant leg.

The preburner injector element's hydrogen flow path changed significantly from the phase II to the II+ design. The hydrogen inlet area was reduced by 42 percent, the annulus length was shortened, and the geometry of the annulus convergence section changed. With the large reduction of inlet area, an increased resistance would normally be expected. However, a 10 percent decrease in fuel flow resistance was quoted for phase II+ preburner injector elements.

To resolve this discrepancy, a Computational Fluid Dynamics analysis was performed to determine hydrogen flow path resistances of the phase II+ fuel preburner injector elements relative to the phase II element. The analysis was performed for 104 percent RPL conditions. FDNS was implemented on axisymmetric grids with the hydrogen assumed incompressible. The analysis was performed in two steps. The first isolated the effect of the different inlet areas and the second modeled the entire injector element hydrogen flow path.

The isolated effect of the reduced inlet area was a 3. percent increased resistance for phase II+ elements. However, the entire flow path model showed no difference between phase II and II+ injector element resistances. Phase II+ annulus geometry changes compensated for the reduced inlet area such that there was no net effect on hydrogen flow path resistance.

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Computational Fluid Dynamic Analysis of SSME Phase II and Phase II+ Preburner Injector Element Hydrogen Flow Paths

Joseph H. Ruf Computational Fluid Dynamics Branch Marshall Space Flight Center



SSME Phase II and Phase II+ Preburner Injector Computational Fluid Dynamic Analysis of **Element Hydrogen Flow Paths**

- OBJECTIVE
- BACKGROUND
- APPROACH
- RESULTS

CONCLUSION

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OBJECTIVE

Analytically determine the hydrogen flow path resistance of the phase II+ preburner injector elements.

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BACKGROUND

- A number engine hardware changes were made from phase II to II+ to improve the operating environment in the SSME.
- Hot fire testing of E0209 and E0215 phase II+ engines resulted in an increased rate of main combustion chamber (MCC) liner degradation.
- resistances in the fuel flow circuit such that the coolant flow It was thought the phase II+ hardware changes altered the to the MCC was reduced.
- One area of uncertainty was the resistance of the preburner has a reduced hydrogen inlet area and a shorter hydrogen injector elements. Phase II+ preburner injector element annulus.
 - Rocketdyne guoted a 10% decrease in hydrogen flow resistance for the phase II+ element with respect to phase II.



PHASE II+ INVESTIGATION

SIMPLIFTED REGISTANCE/FLOW MODEL SCHEMATIC:





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APPROACH

- Quantify the change in resistance/delta P with a comparative analysis of phase II and II+ elements.
 - phase II preburner injector element hydrogen flow delta P is 400 psi.
- preburner injector elements are similar in both phase II and II+. Modeled the fuel preburner injector elements; oxidizer and fuel
- Performed axisymetric CFD analysis (FDNS) of the hydrogen flow path of phase II and II+ elements at 104% RPL conditions
 - Assumptions:
- incompressible flow
- rows of inlet holes modeled as equivalent area circumferential channels 0
 - LOX flow not modeled



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APPROACH, cont.

- Analysis done in two steps
- quantify the effect of reduced inlet area
- quantify effect of entire hydrogen flow path
- Specified mass flow rate and inlet pressure; resistance \sim delta P.
- Performed grid independency study





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RESULTS

- Effect of inlet area
- phase II delta P = 529 psi
- phase II+ delta P = 545 psi $\Delta = + 3\%$
- Full hardware geometry
- phase II delta P = 406 psi
- $\Delta = -0.25\%$ phase ll+ delta P = 405 psi
- Phase II calculated pressure drop matched well with accepted value (406 vs. 400 psi).
- Majority of the flow passes through the holes closest to the exit.



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CONCLUSION

No net effect of phase II+ hardware changes on preburner injector element hydrogen resistance/delta P.

N92-32262

STME HYDROGEN MIXER STUDY

Rob Blumenthal Dongmoon Kim George Bache'

ABSTRACT

The hydrogen mixer for the STME is used to mix cold hydrogen bypass flow with warm hydrogen coolant chamber gas, which is then fed to the injectors. It is very important to have a uniform fuel temperature at the injectors in order to minimize mixture ratio problems due to the fuel density variations. In addition, the fuel at the injector has certain total pressure requirements. In order to achieve these objectives, the hydrogen mixer must provide a thoroughly mixed fluid with a minimum pressure loss. The AEROVISC CFD code was used to analyze the STME hydrogen mixer, and proved to be an effective tool in optimizing the mixer design. AEROVISC, which solves the Reynolds Stress-Averaged Navier-Stokes equations in primitive variable form, was used to assess the effectiveness of different mixer designs. Through a parametric study of mixer design variables, an optimal design was selected which minimized mixed fuel temperature variation and fuel mixer pressure loss. The use of CFD in the design process of the STME hydrogen mixer was effective in achieving an optimal mixer design while reducing the amount of hardware testing.

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STME HYDROGEN MIXER STUDY

TENTH ANNUAL WORKSHOP FOR CFD APPLICATIONS IN ROCKET PROPULSION

NASA MARSHALL SPACE FLIGHT CENTER

Robert F. Blumenthal Dongmoon Kim George Bache' April 30, 1992



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WHY IS MIXING IMPORTANT?

- Equal ΔP Across Each Injector Element Which Therefore Require Uniform Hydrogen Density in Order to Have Equal H₂ Flow Rate to Each Element Injector Elements All Designed With Identical Metering Orifice Areas and
- A Uniform Mixture Ratio Injector Core Delivers Highest ISP Performance •
- Uniform H₂ Density (Mixture Ratio) Is Dependent on the Performance of the Hydrogen Mixer
- Uniform Temperature Implies Uniform Density

MODELING ISSUES

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- DISCRETE COLD INLET HOLES
- HOT GAS INLET ASSUMES UNIFORM FLOW ACROSS PASSAGE
- 3-D WEDGE
- COMPRESSIBLE FLOW
- GAS PROPERTIES BASED ON MIXED TEMPERATURE
- STANDARD K-e TURBULENCE MODEL
- ADIABATIC WALLS
- EXIT PLANE AT BEGINNING OF DIFFUSER SECTION
- GRID SIZE 97 X 19 X 16



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STME HYDROGEN MIXER

Cold Hydrogen Inlet Hole Size Varied to Determine Effect on Mixing

Wedge Angle [Deg]	1.45	0.96	0.70
A _{CTOT} [in ²]	3.22	3.22	3.22
D _C [in]	0.091	0.074	0.063
о Х	495	749	1033
NCNOM	500	750	1000

Cold Hydrogen Inlet Holes Are Staggered With Respect to the Mixing Channel Centerline





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EXIT PLANE TEMPERATURE DEPENDENT ON COLD HYDROGEN INLET HOLE SIZE

NC-500 HOLES



NC=750 HOLES



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NC-1000 HOLES



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TOTAL TEMPERATURE VARIATION VS. L/DH NC=500. 750. 1000 H0LES





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COLD HYDROGEN INLET HOLE SIZE RESULTS

∆P _T [Psi]	116.9	95.3	93.3
∆T _T [°R]	174.5	98.7	126.2
σ _Τ [°R]	56.9	33.1	44.2
T _{TAVE} [°R]	204.0	203.6	205.5
N N	500	750	1000

 T_{TAVE} = Mass-Averaged Value of Total Temperature at Exit Plane = Total Temperature Range at Model Exit Plane ΔT_T

= Net Total Pressure Recovery (Prexit - Prhinlet) ΔP_{T} = Standard Deviation of Temperature at Exit Plane 91

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DETREMINE EFFECTS ON TOTAL TEMPERATURE AND PRESSURE COLD HYDROGEN INLET FLOW ANGLE WAS VARIED TO



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EXIT PLANE TEMPERATURE DEPENDENT ON COLD HYDROGEN FLOW ANGLE

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NC= 750 HOLES

THETA=26.5 DEG

2.500E+02 2.450E+02 2.400E+02 2.350E+02 2.300E+02 2.250E+02 2.200E+02 2.150E+02 2.100E+02 2.0506+02 2.000E+02 1.9506+02 1.900E+02 1.850E+02

TTOTAL



THETA=0 DEG

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THETA=45 DEG

THETA=33.7 DEG

1.600E+02

1.7506+02 1.700E+02 1.650E+02 1.600E+02

1.550E+02

1.500E+02

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AEROJET TOTAL PRESSURE VARIATION VS. L/DH 26.5, 33.7, 45 DEG FLOW ANGLE=0.



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TOTAL TEMPERATURE VARIATION VS. L/DH DEG FLOW ANGLE=0. 26.5. 33.7. 45





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COLD HYDROGEN INLET FLOW ANGLE RESULTS

CI	ANG [DEG]	T _{TAVE} [°R]	σ _T ["R]	∆T _T [°R]	ΔP _T [Psi]
RONA	0	203.6	33.1	98.7	95.3
L PAC	26.5	199.2	17.8	58.5	11.4
e is	33.7	199.3	11.8	42.4	-9.5
	42.0	198.8	8.1	24.3	-58.3
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 T_{TAVE} = Mass-Averaged Value of Total Temperature at Exit Plane = Total Temperature Range at Model Exit Plane ΔT_{T}

= Net Total Pressure Recovery (P_{TEXIT} - P_{THINLET}) ΔP_T = Standard Deviation of Temperature at Exit Plane Δ_{T}

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FUTURE WORK

- Examine Other Configurations
- Swirled Injection
- Smaller Mixing Channel Area
- Inline Cold Hydrogen Inlet Holes
- Modifying Position of Cold Hydrogen Inlet Holes With Respect to the Mixing Channel Centerline
- Provide Design Requirements for Experimental Cold Flow Hardware
- Support Cold Flow Testing
- Analyze Cold Flow Data and Validate Aerovisc Predictive Capability
- Use Validated Model to Design Flight Mixer

N92-32263

AN EXPERIMENTAL STUDY OF THE FLUID MECHANICS ASSOCIATED WITH POROUS WALLS (AIAA 92-0769)

N. Ramachandran, Universities Space Research Association, J. Heaman, A. Smith, NASA Marshall Space Flight Center, Huntsville, Al 35812

ABSTRACT

The fluid mechanics of air exiting from a porous material is investigated. The experiments are filter rating dependent, as porous walls with filter ratings differing by about three orders of magnitude are studied. The flow behavior is investigated for its spatial and temporal stability. The results from the investigation are related to jet behavior in at least one of the following (1) Jet coalescence effects with increasing flow rate, (2) Jet field categories: decay with increasing distance from the porous wall, (3) Jet field temporal turbulence characteristics and (4) Single jet turbulence characteristics. The measurements show that coalescence effects cause jet development and this development stage can be traced by measuring the pseudoturbulence (spatial velocity variations) at any flow rate. The pseudoturbulence variation with increasing mass flow reveals an initial increasing trend followed by a leveling trend, both of which are directly proportional to the filter rating. Α critical velocity begins this leveling trend and represents the onset of fully developed jetting action in the flow field. A correlation is developed to predict the onset of fully developed jets in the flow emerging from a porous wall. The data further show, that the fully developed jet dimensions are independent of the filter rating, thus providing a length scale for this type of flow field (1 Individual jet characteristics provide another unifying trend with mm). similar velocity decay behavior with distance; however, the respective turbulence magnitudes show vast differences between jets from the same Measurement of the flow decay with distance from the porous wall sample. show that the higher spatial frequency components of the jet field dissipate Flow turbulence intensity faster than the low frequency components. measurements show an out of phase behavior with the velocity field and are generally found to increase as the distance from the wall is increased.





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RELEVANT LITERATURE

REPARTS

 Dunlap, R., and Willoughby, P. G.: Cold Flow Study Test Report. United Technologies, Chemical Systems Division, 1989.

2. MacPhult, D.: ARC R & M 1376, Accondutical Research Council. England, 1939. yon Bohl, D.: Dus Verhulten paralleler Luitstrahlen, Ingemeur Archiv, Vol. 11, 4, 1940, p 295. Correlin, S.: Investigation of the Behavior of Parallel Two-Dimensional Air Jets, ACR 21(2) NACA, 1944.

 Murgan, P. G.: The Stability of Flow through Porous Screen, Journal of the Royal Aeronautical Society, Vol. 64, 1960, pp. 359-362. Bradshaw, P.: The Effect of Wind-Tunnel Screens on Nonunully Two-Dimensional Boundary Layers, Journal of Fluid Mechanics, Vol. 22, 1965.

7, Schubauer, G. M.: Journal of the Asconautical Sciences, $V \in \{1, 1, 2, 3\}$

Pimenta, M., and Motifar, R.: Stability of Rlow through Place.
 Plates: Coulement Jeta Effect, ALAA Journal, Vol. 12, 10, 1974.

 Traineau, J. C., Hervat, P., and Kuentzmann, P.: Coid-Flux Simulation of a Two-Dimensional Nuzzleies Solid Rocket Mutor. Presented at the ALAA/ASME/SAE/ASEE 22nd Joint Propulsion Conference, Huntswille, Alabana, ALAA/86-1447, June 16-13, 1936.

10. Lubbe, J., and Hervat, P., Private communication.

11. Dunlap, R., et al.: Private Communication.

 Tong, K. and Knight, C. J.: Flow around an Isolated Porous Tube with Nonuniform Walt Thickness, ALAA Journal, Vol. 17, No. 11, 1979, pp. 1262-1263.

 Collins, R., E.: Flow of Fluids through Porous Muterials, Reinhold Publishing Corp., NY, 1561. Beddini, R. A.: Contribution to ERCI Fourth Quarterly Progress Report, NASS-38070, 1991.

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OTHER CATEGORIES q. RESULTS

2. Jet field turbulence characteristics. 1. Jet field decay with distance from the surface.

3. Single jet turbulence durnacteristics.

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N92-32264

"Experimental Studies of Characteristic Combustion-Driven Flows for CFD Validation"

R. J. Santoro, M. Moser, W. Anderson, S. Pal, H. Ryan and C. L. Merkle Propulsion Engineering Research Center The Pennsylvania State University University Park, PA 16802

A series of rocket-related studies intended to develop a suitable data base for validation of CFD models of characteristic combustion-driven flows has been undertaken at the Propulsion Engineering Research Center at Penn State. Included are studies of coaxial and impinging jet injectors as well as chamber wall heat transfer effects. The objective of these studies is to provide fundamental understanding and benchmark quality data for phenomena important to rocket combustion under well-characterized conditions. Diagnostic techniques utilized in these studies emphasize determinations of velocity, temperature, spray and droplet characteristics and combustion zone distribution. Since laser diagnostic approaches are favored, the development of an optically accessible rocket chamber has been a high priority in the initial phase of the project. During the design phase for this chamber, the advice and input of the CFD modeling community were actively sought through presentations and written surveys. Based on this procedure, a suitable uni-element rocket chamber has been fabricated and is presently under preliminary testing. Results of these tests, as well as the survey findings leading to the chamber design, was presented.

In particular, laser-induced fluorescence imaging results for hydroxyl radicals have been obtained. These experiments were conducted using gaseous hydrogen/gaseous oxygen propellants in the optically accessible uni-element rocket chamber. Heat transfer studies demonstrated the effectiveness of the curtain window purge needed to protect the optical surfaces. These results also demonstrated the capability to determine wall heat transfer rates in the present rocket test chamber. Measurements indicated that heat transfer rates were approximately an order of magnitude smaller than observed in actual rocket chambers. If larger propellant flow rates are utilized, this difference should be further narrowed.

Related results from impinging jet studies under non-combusting conditions revealed several trends regarding drop size and liquid sheet breakup. The general experimental observation that breakup length increases with increasing jet velocity and decreasing impingement angle is in agreement with previous studies. However, this trend is opposite to predictions derived from linear stability-based analysis of liquid sheet atomization. However, drop size predictions for linear stability-based analysis reproduced the observed trend of decreasing drop size with increasing jet velocity and increasing impingement angle.

Experimental Studies of Characteristic Combustion-Driven Flows for CFD Validation

R. J. Santoro, M. Moser, W. Anderson, S. Pal, H Ryan, and C. L. Merkle

The Propulsion Engineering Research Center The Pennsylvania State University University Park, PA 16802

Workshop for Computational Fluid Dynamic (CFD) Applications in Rocket Propulsion

April 28-30, 1992

OUTLINE

- CFD Validation Optically Accessible Rocket
- Heat Transfer Measurements
- Impinging Jet Studies
- Summary
- Future Work

CFD VALIDATION - OPTICALLY ACCESSIBLE ROCKET M. Moser, S. Pal, R. Santoro, C. Merkle

OBJECTIVE

To Provide Benchmark-Quality Data for CFD Code Validation for Combustion-Driven Flows

Obtain Fundamental Data Under Realistic and Well Characterized Conditions

APPROACH

Emphasize Uni-element Coaxial Injectors

Obtain Fundamental Data Under Well Characterized and Realistic Conditions

Pressure Combustion zone Mean Velocity Turbulence Intensity Species Droplet Size and Velocity

Employ Non-Intrusive Advanced Diagnostics

Laser Induced Fluorescence Raman Spectroscopy Laser Velocimetry Flow Visualization Phase Doppler Particle Analyzer Polarization Ratio Raman Spectroscopy

Closely Integrate CFD Objectives Into Experimental Program

Experiment Design Measured Quantities Boundary Condition Specification

SUMMARY OF SURVEY RESULTS

• Square Geometry Is Acceptable

Initially Axisymmetric Approximation Suitable Eventually 3-d Verification Required

- Chamber Mach Number Need Not Be Matched to Actual Rocket Conditions
- Recirculation Effect In Uni-Element Chamber Can Be Accommodated If Suitable Measurements Are Available
- Measurements And Boundary Conditions Nearly Everything Is Important

Typically All Parameters Rate 1 Or 2 On Scale Of 5

Responses From:

MSFC Aerojet Rocketdyne CFDRC

OPTICALLY ACCESSIBLE ROCKET



- Two Inch Square Cross-section
- Variable Length 6-12 Inches
- Two Inch Diameter Quartz Windows For Viewing
- Slot Windows For Laser Access
- Injector Design Is Modular



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RESULTS

- Rocket Chamber Has Been Checked Out To 400 psi Chamber Pressure
- Window Purges Effectiveness Tested With Heat Flux Gages
- Quartz Windows Tested To 200 psi For Four Second Firings
- Shadowgraph Photograph Obtained
- 2-D Laser Induced Fluorescence Image Of OH Obtained





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HEAT TRANSFER MEASUREMENTS S. Pal, C. Merkle

Objective:

- Demonstrate Capability
- Test Effectiveness Of Window Purge



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WINDOW PURGE COMPARISON



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OBJECTIVES

- Characterize Spray Phenomena Associated With Impinging Jet Injectors
- Breakup Length
- Drop Size Periodic Structures
- Investigate Sensitivity of Spray Characteristics to Geometric and Operational Parameters
- Jet Velocity Orifice Diameter
- Impingement Angle Pre-Impingement Length Orifice Length
- Compare Experimental Results with Theoretical Models of Sheet Breakup and Drop Formation
- Linear Growth of Surface Waves Due to Aerodynamic Forces



Impinging Jet Injector System





$$U_j = 6.4 \text{ m/s}$$

 $2\theta = 60^{\circ}$

 $U_j = 18.5 \text{ m/s}$ $2\theta = 60^{\circ}$





$$U_j = 6.4 \text{ m/s}$$

 $2\theta = 80^{\circ}$

 $U_j = 18.5 \text{ m/s}$ $2\theta = 80^{\circ}$





SUMMARY

- Experimental Results Were Compared with Predictions From Linear Aerodynamic Instability Derived Model
- Breakup Length Predictions Oppose Observed Trends 1
 - Drop Size Predictions Reproduce Observed Trend and Agree Within Factor of 2 1
- General Appearance Favors Impact Wave Breakup Mechanism
- Orifice L/D Has No Significant Effect on Spray Characteristics
- Pre-Impingement Length Has Measurable Effect on Breakup Length and Drop Size

SUMMARY

- Successful Firings of Optically Accessible Rocket Test Chamber Achieved
- Shadowgraph of Combustion Zone Obtained
- Preliminary Two-Dimensional OH Imaging Results
 Obtained
- Wall Heat Transfer Rate Measurement Capability Demonstrated
- Fundamental Studies of Impinging Sprays Are Elucidating Basic Atomization Mechanisms
FUTURE WORK

- Semi-Quantitative Measurement of Relative OH Concentration
- Velocimetry (initially single point measurements, eventually 2-D velocimetry measurements)
- Raman Spectroscopy

ACKNOWLEDGEMENTS

The CFD Validation Studies Are Supported By The Marshall Space Flight Center Under Contract NAS8-38862

the Impinging Jet Studies Are Supported by The Air Force Office Of Scientific Research Under Grant AFOSR-91-0336

N92-32265

TURBINE DISK CAVITY AERODYNAMICS AND HEAT TRANSFER

B. V. Johnson W. A. Daniels United Technologies Research Center East Hartford, CT 06108

Experiments were conducted to define the nature of the aerodynamics and heat transfer for the flow within the disk cavities and blade attachments of a large-scale model, simulating the SSME turbopump drive turbines. These experiments of the aerodynamic driving mechanisms explored the following: (1) flow between the main gas path and the disk cavities, (2) coolant flow injected into the disk cavities, (3) coolant density, (4) leakage flows through the seal between blades, and (5) the role that each of these various flows has in determining the adiabatic recovery temperature at all of the critical locations within the cavities. The model and the test apparatus provide close geometrical and aerodynamic simulation of all the two-stage cavity flow regions for the SSME High Pressure Fuel Turbopump and the ability to simulate the sources and sinks for each cavity flow.

Carbon dioxide was used as a trace gas for constant density experiments or as the simulated "heavy gas" coolant. Gas samples were withdrawn at selected locations on the rotating and stationary surfaces in the fore and aft cavity and the interstage seal regions of the two stage system. The gas samples were used to determine the fraction of gas at a location which originates from each of three coolant injection locations or four gas path locations. Samples were also withdrawn at selected locations in the blade shank regions.

A parametric series of experiments was conducted with constant density fluids and an exploratory series of experiments was conducted with CO_2 as the simulated coolant. Experimental results showed (1) the variation of coolant distribution on the cavity and disk surfaces as a function of coolant flow ratio, (2) the effects on the coolant distribution for changes in the coolant inlet distributions, and (3) increased mixing of coolant with the ingested gas when a heavy gas (density ratio equal 1.5) was used as the coolant.

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TURBINE DISK CAVITY AERODYNAMICS AND HEAT TRANSFER

Contract NAS8-37462

B.V. Johnson W.A. Daniels Tenth Workshop for Computational Fluid Dynamic Applications in Rocket Propulsion

UNITED TECHNOLOGIES RESEARCH

April 30, 1992





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GAS SOURCES AND EXITS



Pressure/CO₂ taps on rotating components Pressure/CO₂ taps on stationary components

O Pressure/CO₂ taps in passages

Thermocouples



SSME TURBINE DISK CAVITY MODEL



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MODEL IN INTERNAL FLOW FACILITY

MODEL SEAL REGION AND GAS SOURCE/EXIT LOCATIONS











COOLANT DISTRIBUTION ON ROTOR

Region IV: Aft Cavity & Rotor 2 Coolant: Air



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COOLANT DISTRIBUTION ON STATIONARY WALL

Region IV: Aft Cavity & Rotor 2 Coolant: Air



COOLANT DISTRIBUTION ON ROTOR

Region IV: Aft Cavity & Rotor 2 Coolant: CO2



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COOLANT DISTRIBUTION ON STATIONARY WALL

Region IV: Aft Cavity & Rotor 2 Coolant: CO2



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82

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86

5

B10

RESULTS/CONCLUSIONS

Constant Density

- Coolant flows approximately one-half free disk entrainment rate provide full purge of cavity $(\phi > 80\% \text{ below blade shanks})$
- rate $(\phi > 90\%)$ for coolant flows 1/4 design flow Coolant concentration on rotor surface high
- Cavity walls have largest variation of ϕ with coolant flow rate

RESULTS/SPECULATION

Variable Density (Exploratory Experiments with CO₂)

- Density ratio has strong effect
- Coolant concentration on rotor decreased from constant density results at comparable weight flow or volume flow rates. 1
- Coolant concentration on aft cavity wall decrease significantly from constant density results at comparable flow rates. I
- rotating flow with higher gas densities at low radii. Decreased coolant concentration attributed to increased mixing and probable instability of

N92-32266

A Numerical Study of Two-Dimensional Vortex Shedding From Rectangular Cylinders

A. H. Hadid, M. M. Sindir CFD Technology Center Rockwell International/Rocketdyne Division Canoga Park., California R. I. Issa Department of Mineral Resources Engineering Imperial College of Science Technology and Medicine, London, SW7, 2BP, England

An efficient time-marching, non iterative calculation method is used to analyze timedependent flows around rectangular cylinders. The turbulent flow in the wake region of a square section cylinder is analyzed using an anisotropic k- ε model. Initiation and subsequent development of the vortex shedding phenomenon is naturally captured once a perturbation is introduced in the flow. Transient calculations using standard eddy-viscosity and an anisotropic k- ε models averaged over an integral number of cycles to get the fluctuating energy (organized and turbulent) are compared with experimental data. It is shown that the anisotropic k- ε model resolves the anisotropy of the Reynolds stresses and give mean energy distribution closer to the experiment than the standard k-e model.

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 AN EFFICIENT TIME-ACCURATE CALCULATIONAL METHOD IS USED TO PREDICT THE 2D TRANSIENT VORTEX SHEDDING MOTION BEHIND A SQUARE OBSTACLE THE SEPARATED TURBULENT FLOW BEHIND THE OBSTACLE IS MODELED USING AN ANISOTROPIC ke TURBULENCE MODEL COMPARISONS WITH EXPERIMENTAL RESULTS SHOW REASONABLE AGREEMENT AND RIGHT TRENDS 		OVERVIEW
 THE SEPARATED TURBULENT FLOW BEHIND THE OBSTACLE IS MODELED USING AN ANISOTROPIC k-e TURBULENCE MODEL COMPARISONS WITH EXPERIMENTAL RESULTS SHOW REASONABLE AGREEMENT AND RIGHT TRENDS 	•	AN EFFICIENT TIME-ACCURATE CALCULATIONAL METHOD IS USED TO PREDICT THE 2D TRANSIENT VORTEX SHEDDING MOTION BEHIND A SQUARE OBSTACLE
COMPARISONS WITH EXPERIMENTAL RESULTS SHOW REASONABLE AGREEMENT AND RIGHT TRENDS	•	THE SEPARATED TURBULENT FLOW BEHIND THE OBSTACLE IS MODELED USING AN ANISOTROPIC k-€ TURBULENCE MODEL
	•	COMPARISONS WITH EXPERIMENTAL RESULTS SHOW REASONABLE AGREEMENT AND RIGHT TRENDS
Bockwell International		
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	INTRODUCTION (CONTD.)
•	STANDARD k-€ MODELS TEND TO DAMP PERIODIC SHEDDING MOTION UNDERPREDICTING THE STROUHAL NUMBER
•	FOR A SUCCESSFUL SIMULATION OF TRANSIENT TURBULENT FLOWS A RELIABLE TIME ACCURATE NUMERICAL PROCEDURE AND A GOOD TURBULENCE MODELS ARE NEEDED
•	AN EFFICIENT NON-ITERATIVE TIME ACCURATE NUMERICAL SCHEME BASED ON THE "PISO" METHODOLOGY IS EMPLOYED TO ANALYZE THE TRANSIENT VORTEX SHEDDING FLOW
•	TURBULENCE IS MODELLED BY USING THE ANISOTROPIC k-ε TURBULENCE MODEL
Rockwell Rocketdyne	nternational Division



"PISO" NUMERICAL PROCEDURE (CONTD.)	A MINIMUM OF TWO-CORRECTOR STAGES ARE NECESSARY FOR MANY PRACTICAL PURPOSES	• METHOD IS ESSENTIALLY NON-ITERATIVE WHERE THE SOLTION PROCESS IS SPLIT INTO A SERIES OF STEPS WHEREBY OPERATINS ON PRESSURE ARE DECOUPLED FROM THOSE ON VELOCITY AT EACH TIME STEP IN A SERIES OF CORRECTOR STEPS			Rockwell International Rocketdyne Division
					K







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NISIZIMA USED THIS MODEL TO STUDY FULLY DEVELOPED TURBULENT SQUARE DUCT FLOW WHERE DEVIATIONS OF THE REYNOLDS STRESSES FROM ITS ISOTROPIC EDDY-VISCOSITY PLAYS A CENTRAL ROLE	YOSHIZAWA SHOWED FOR THE SIMPLE ASYMMETRIC CHANNEL FLOW BETWEEN A ROUGH AND A SMOOTH WALLS THE NONCOINC- IDENCE OF THE LOCATION OF ZERO SHEAR AND MAXIMUM VELOCITY	MYONG AND KASAGI USED THE MODEL FOR FULLY DEVELOPED TURBULENT CHANNEL FLOW WHITH C ₇₁ AND C ₇₂ OPTIMIZED TO REPRODUCE THE ANISOTROPY OF TURBULENT INTENSITIES	IN THE PRESENT STUDY THE MODEL CONSTANTS C ₇ 1, C ₇₂ AND C ₇₃ WERE OPTIMIZED TO 0.01, 0.01 AND 0.001 RESPECTIVELY TO SATISFY THE REALIZABILITY CONSTRAIN	WALL FUNCTIONS WERE USED TO BRIDGE THE NEAR OBSTACLE WALL REGION
•	•	•	•	٠



RESULTS AND DISCUSSIONS (CONTD.)	 CALCULATIONS CAPTURED THE VORTEX SHEDDING PHENOMENON	 COMPUTATIONAL DOMAIN WAS RESOLVED BY 75X40 CELLS WITH	AN OPTIMIZED TIME STEP OF 0.001 sec. WAS CHOSEN IN THE	kwell International
	AFTER EXPLICITLY PERTURBING THE FLOW AT THE INLET	CLUSTERING AT THE OBSTACLE WALLS	CALCULATIONS	Materiana Division




















 DISCUSSION RESULTS OF MEAN KINETIC ENERGY SHOW k-E MODEL PREDICTS A BETTER TREND THA MODEL THE IMPROVED TREND IS MANILY DUE TO TURBULENT ENERGY CONTRIBUTION AS SH STRESSES CONTOURS THE IMPROVED TREND IS MANILY DUE TO TURBULENT ENERGY CONTRIBUTION AS SH STRESSES CONTOURS LENGTH OF RECIRCULATION ZONE BEHIND LOCATION OF THE MAXIMUM FLUCTUATIN USING THE ANISOTROPIC MODEL



N92-32267

Submitted for the CFD Workshop -- 1992

A Status of the Turbine Technology Team Activities

Lisa W. Griffin

A Status of the activities of the Turbine Technology Team of the Consortium for Computational Fluid Dynamics (CFD) Application in Propulsion Technology is presented. The team consists of members from the government, industry, and universities. The goal of this team is to demonstrate the benefits to the turbine design process attainable through the application of CFD. This goal is to be achieved by enhancing and validating turbine design tools for improved loading and flowfield definition and loss prediction, and transferring the advanced technology to the turbine design process.

In order to demonstrate the advantages of using CFD early in the design phase, the Space Transportation Main Engine (STME) turbines for the National Launch System (NLS) were chosen on which to focus the team's efforts. The Turbine Team activities run parallel to the STME design work.

Work during the past year has centered on transferring technology obtained through the team's Generic Gas Generator Turbine Program (reported on in the 1990 workshop) to the STME LOX turbine design point. A preliminary baseline design was analyzed through CFD, and areas requiring refinement to eliminate local overspeeds and separations were found. An improved baseline design has been finalized. The team is currently comparing results from five team members (Aerojet, NASA/Ames Research Center, NASA/Lewis Research Center, Pratt & Whitney, and Scientific Research Associates). These solutions will be compared to data to be obtained in the Marshall Space Flight Center Turbine Airflow Facility. Interrogation of these solutions are also in progress to determine high loss locations and to provide guidance for developing and/or implementing concepts to control these losses.



A Summary of the Activities of the NASA/MSFC Turbine Technology Team

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Z	National Ae	Space Admi

A Summary of the Activities of the NASA/MSFC Turbine Technology Team

Overview

- Structure/Objectives
- Turbine Team Participants
- Program Overview
- Code Development/Enhancement
- Validation Experiments
- Advanced Hardware Development
- Subsonic Turbine Development Program
- Background
- Gas Generator Oxidizer Turbine (GGOT)
- New Programs
- Volute Development
- Supersonic Turbine Development
- Summary

Reference and Space Administration

A Summary of the Activities of the NASA/MSFC Turbine Technology Team

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A Summary of the Activities of the NASA/MSFC **Furbine Technology Team**

Participants

- NASA Marshall Space Flight Center (MSFC)
- NASA Ames Research Center (ARC)
- NASA Lewis Research Center (LeRC)
- Aerojet
- Pratt and Whitney (P&W)
- Rocketdyne (RKDN)
- Calspan University of Buffalo Research Center (CUBRC)
- Rotodata
- Scientific Research Associates (SRA)
- SECA
- United Technologies Research Center (UTRC)
- Carnegie Mellon University (CMU)
- Pennsylvania State University (PSU)
- The University of Alabama (UA)
- The University of Alabama in Huntsville (UAH)
- Virginia Polytechnic Institute (VPI)

VSV	tional Aeronautics and	
2	Natio	Space

A Summary of the Activities of the NASA/MSFC **Furbine Technology Team**

Program Overview

- Code Development/Enhancement
- · Rotor/Stator Interaction (NASA/ARC)
- 3D Navier-Stokes Code for Volutes (NASA/LeRC)
- Validation of 3D Unsteady Rotor/Stator Interaction Code ROTOR3 (P&W)
- Enhancement and Validation of ROTOR3 for Supersonic Turbines (RKDN)
- Turbulence Modeling (PSU)
- Validation Experiments
- 3D Rotor Heat Transfer (UTRC)
- Unsteady Interrow Aerodynamics (P&W)
- SSME HPFTP Fuel Turbine
- -- Baseline Aerodynamics (MSFC)
- -- Baseline Unsteady Aerodynamics/Heat Transfer (CUBRC)
- -- Smooth Blades (MSFC)
- -- Circumferential Exit ΔP (MSFC)
- -- ATD (MSFC)

Rational Aeronautics and Space Administration

A Summary of the Activities of the NASA/MSFC Turbine Technology Team

Program Overview

- Advanced Hardware Development
- Subsonic Turbine Development
- Volute Development
- Supersonic Turbine Development

 A Summary of the Activities of the NA Turbine Technology Team Subsonic Turbine Development Prog Background Subsonic Turbine design point resulting any sis tools on the STME fuel turbine design point resulting to the concept developed T) design T) design<th></th>	
 Antional Aeronautics and Space Administration Focused flow an Generator (G³ Advanced Turt Advanced an unt Beduced pa Increased ef Analyses in ov Axial gap selec Improved eff Beduced bla Besign concept ir Coused flow ana Oxidizer Turbin 	

	National Aeronautics and Space Administration	TURBINE FLOW ANALYSIS TECHNOI	LOGY
		Background	
		Aerodynamic Design Approach	
		Previous State -of - the-Art	G ^a T Design
	General Description	70/30 Work Split Nominal Annulus Height	50/50 Work Split Increased Annulus Height
1213	Blade Turning	135°	160°
	Fluid Acceleration	0.9	1.6
	Max Blade Mach Numb	Jr. 1.32	0.87
	Efficiency	Base	+10 percent
	Airfoil Count	Base	-55 percent

BASELINE GGGT AERODYNAMIC DESIGN Calculated Streamlines - Midspan



CONSORTIUM FOR CFD APPLICATION IN PROPULSION TECHNOLOGY

Turbine Stage Technology Team-Baseline GGGT aerodynamic analyses



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	Reference and Reference and	A Summary of the Activities of the NASA/MSFC
	Space Administration	Turbine Technology Team
		Subsonic Turbine Development Program GGOT
	 Phase I Task Des 	sription
	- Development o	preliminary baseline design (P&W)
	- Analyses of pre	iminary design (P&W, NASA/ARC, and NASA/LeRC)
	- Modification of	oreliminary design (P&W)
12	- Analysis of mot	ified design (P&W, NASA/ARC, NASA/LeRC, SRA, and Aerojet)
217	- Development o	final baseline design (P&W)
	- Comparisons o	CFD solutions
	- Experimental e	aluation of baseline design (MSFC)
	 Phase II Task Das 	
	- Internorate has	dina reculte for regione of loccae
	- Develonment o	concents to control losses
	Parametric s	udies with CFD
	- Development of	advanced design
	- Detailed analys	ss of advanced design
	- Experimental er	aluation of advanced design



Downstream Separation Eliminated 3D Flow Analysis Shows Baseline GAS GENERATOR OXIDIZER TURBINE (GGOT) DESIGN 00 0 Е **3D Flow Analysis Shows Separation** Streaklines Downstream of Rotor Downstream of Rotor **Preliminary** 00 ≙ Ш 1219

URBINE BASELINE DESIGN	Blade Losses	Baseline Design Philosophy Secondary Leakage Control Studies 3D Navier-Stokes Analyses, Steady & Unsteady
OXIDIZER TECHNOLOGY T Concerns / Potential Weaknesses	Vane Losses	Secondary Addressed in Philosophy

GGOT ROTOR - TIP LEAKAGE FLOW



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2.053E+00

1.842E+Ø0

1.846E+09

1.737E+00 1.631E+ØØ

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6.830E-01 7.875E-01 6.820E-01 5.765E-Ø1 4.710E-01 3.855E-Ø1

2.600E-01



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GGOT ROTOR - PRESSURE LOSS COEFFICIENT CONTOURS

A Summary of the Activities of the NASA/MSFC Turbine Technology Team	New Program - Volute Development	signed using existing database and limited analysis utes out of experience base e diffuser/volute) esign considered for cost and weight ute dataset non-existent	ne volutes with existing design methodology olutes for design and off-design conditions on of baseline volutes on GGOT for code validation control and side load reduction concepts with CFD f improved designs ation of improved volutes on advanced concepts GGOT
Rational Aeronautics and Space Administration		 Issues Volutes traditionally desi STME LOX turbine volut High Mach number High swirl (discharge Vaneless diffuser des Benchmark quality volu 	 Task Descriptions Design of three baselin Analysis of baseline vo Experimental evaluatio Evelopment of loss co Development of loss co - Parametric studies v - Detailed analysis of - Experimental evalua

• • 1225	Antional Aeronautics and National Aeronautics and Space Administration - High Iosses and blads - Durability requirer - Low confidence ir - Low confidence ir - Low confidence ir - Supersonic turbine da - Supersonic turbine da - Design baseline turbi - Analysis of baseline turbi - Experimental evaluat expansion - Development of adva	A Summary of the Activities of the NASA/MSFC Turbine Technology Team New Program - Supersonic Turbine Development e excitations found in supersonic turbines nents require special attention paid to unsteady loadings and shock interactions the understanding of unsteady loadings and shock interactions the understanding of unsteady loadings and shock interactions the understanding of unsteady loadings the understanding of unsteady loadings the understanding of unsteady loadings the understanding of unsteady loadings the understanding of unsteady loadings of the understanding of unsteady loadings the
	Parametric studies	of candidate concepts to control losses and interactions
	Detailed analyses	of advanced design
	Experimental eval	lation of advanced design

	National Aeronautics and Space Administration	A Summary of the Activities of the NASA/MSFC Turbine Technology Team
-		Summary
	 Team of governmen design and analys 	t, industry, and university experts in place and focused on relevant turbine is issues
	 Codes and models 5 	re being developed and enhanced to address complex flows in turbines
1226	 Unique experimenta of turbine analysis 	l data is being taken to provide information for thorough calibration/validation tools
	 Team activities have design 	been coordinated and focused on demonstration of CFD tools for turbine

N92-32268

A CRITICAL EVALUATION OF A THREE-DIMENSIONAL NAVIER-STOKES CFD AS A TOOL TO DESIGN SUPERSONIC TURBINE STAGES

C. HAH, O. KWON, AND M. SHOEMAKER NASA LEWIS RESEARCH CENTER 21000 BROOKPARK ROAD, CLEVELAND, OHIO

Three-dimensional flow phenomena in a supersonic turbine blade row have been studied numerically to evaluate CFD as a tool to design supersonic turbine stages.

The details of the three-dimensional flow structure inside the supersonic turbine blade row and the overall aerodynamic performance at design and off-design conditions are analyzed and the results are compared between the experimental data and the numerical results. A CRITICAL EVALUATION OF A THREE-DIMENSIONAL NAVIER-STOKES CFD AS A TOOL TO DESIGN SUPERSONIC TURBINE STAGES

C. HAH, O. KWON, AND M. SHOEMAKER NASA LEWIS RESEARCH CENTER 21000 BROOKPARK ROAD, CLEVELAND, OHIO

SUPERSONIC TURBINE STAGE

COMMONLY USED IN SPACE ENGINES

DESIGN IS BASED ON 2-D METHOD

VERY LOW EFFICIENCY

FLOWS INSIDE SUPERSONIC TURBINE



OBJECTIVES

UNDERSTAND DETAILED FLOW STRUCTURE

INVESTIGATE LOSS MECHANISM

DEVELOP 3-D DESIGN METHOD

FLOWS INSIDE SUPERSONIC TURBINE





STARTED FLOW

UNSTARTED FLOW

OVERALL APPROACHES

APPLY 3-D NAVIER-STOKES CODE

VERIFY FOR STARTING MACH #, FLOW SEPARATION

EVALUATE CURRENT CAPABILITY


..... ----------**** ----Į -e e da e fa 1 -----1 1 -Ŧ F ŧ • -t.....

COMPUTATIONAL GRID



COMPARISON FOR UNSTARTED FLOW

CALCULATED

MEASURED

1235



COMPARISON FOR STARTED FLOW

CALCULATED







1237



SHOCK-INDUCED VORTEX

MERIDIONAL VELOCITY VECTORS



CONCLUSIONS

3-D VISCOUS CFD CAPTURES MOST FLOW STRUCTURE

CAN BE USED FOR DESIGN APPLICATION

NEEDS HIGH QUALITY DATA FOR VERIFICATION

N92-32269

NAVIER-STOKES ANALYSIS OF AN OXIDIZER TURBINE BLADE WITH TIP CLEARANCE[†]

Howard J. Gibeling Jayant S. Sabnis^{*} Scientific Research Associates, Inc. Glastonbury, CT

ABSTRACT

The Gas Generator Oxidizer Turbine (GGOT) Blade is being analyzed by various investigators under the NASA MSFC sponsored Turbine Stage Technology Team design effort. The present work concentrates on the tip clearance region flow and associated losses; however, flow details for the passage region are also obtained in the simulations. The present calculations simulate the rotor blade row in a rotating reference frame with the appropriate coriolis and centrifugal acceleration terms included in the momentum equations. The upstream computational boundary is located about one axial chord from the blade leading edge. The boundary conditions at this location have been determined by Pratt & Whitney using an Euler analysis without the vanes to obtain approximately the same flow profiles at the rotor as were obtained with the Euler stage analysis including the vanes. Inflow boundary layer profiles are then constructed assuming the skin friction coefficient at both the hub and the casing. The downstream computational boundary is located about one axial chord from the blade trailing edge, and the circumferentially averaged static pressure at this location was also obtained from the P&W Euler analysis.

Results have been obtained for the 3-D baseline GGOT geometry at the full scale design Reynolds number. Details of the clearance region flow behavior and blade pressure distributions have been computed. The spanwise variation in blade loading distributions are shown, and circumferentially averaged spanwise distributions of total pressure, total temperature, Mach number and flow angle are shown at several axial stations. The spanwise variation of relative total pressure loss shows a region of high loss in the region near the casing. Particle traces in the near tip region show vortical behavior of the fluid which passes through the clearance region and exits at the downstream edge of the gap. Future work will include collaboration with the P&W design team to identify design changes which may reduce clearance flow losses.

[†] Work supported under NASA MSFC Contract NAS8-38865.

[®] Currently at United Technologies Research Center, East Hartford, CT.

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SUPPORTED BY

NASA MARSHALL SPACE FLIGHT CENTER

CONTRACT NAS8-38865

Scientific Research Associates



GGOT SIMULATION SUMMARY

UTILIZE SRA GMINT CODE

- GENERAL NON-RECTANGULAR BLOCK STRUCTURE
- · SINGLE GRID
- FULL NAVIER-STOKES EQUATIONS
- NO-SLIP WALL BOUNDARY EQUATIONS WITH SUBLAYER RESOLUTION
- IMPLICIT LINEARIZED BLOCK SOLVER (ADI)



Scientific Research Associates

GGOT SIMULATION FLOW PARAMETERS

- SUPPLIED BY P&W DESIGN TEAM
- **CIRCUMFERENTIALLY AVERAGED SPANWISE DISTRIBUTIONS** FROM EULER CODE
- UPSTREAM AXIAL MASS FLUX
- UPSTREAM TOTAL TEMPERATURE
- UPSTREAM FLOW ANGLES
- DOWNSTREAM STATIC PRESSURE

HUB AND CASING ENDWALL BOUNDARY LAYER PROFILES CONSTRUCTED WITH ASSUMED $C_{f} = 0.002$























Blade Surface Pressure (9.2% span) Baseline GGOT with Clearance



Scientific Research Associates





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Blade Surface Pressure (90% span) Baseline GGOT with Clearance



Circumferentially Averaged Variables Total Pressure Loss Across Blade
















PARTICLE TRACES

BASELINE GGOT WITH TIP CLEARANCE Traces originating at 90% Span - Inflow Vieu

> Scientific Research Associates



CONCLUSIONS AND FUTURE WORK

- CLEARANCE FLOW DETAILS PREDICTED
- **BLADE PRESSURE DISTRIBUTIONS BLOCKAGE EFFECTS**
- · SPANWISE VARIATION OF TOTAL PRESSURE LOSS
- FURTHER ANALYSIS OF DATA NECESSARY
- TIP CLEARANCE FLOW BEHAVIOR
- SECONDARY FLOW BEHAVIOR
- COORDINATION WITH PRATT AND WHITNEY DESIGN EFFORT

Scientific Research Associates

N92-32270

NUMERICAL SIMULATION OF TURBOMACHINERY FLOWS WITH ADVANCED TURBULENCE MODELS

B. Lakshminarayana, R. Kunz, J. Luo, S. Fan The Pennsylvania State University

A three dimensional full Navier-Stokes (FNS) code is used to simulate complex turbomachinery flows. The code incorporates an explicit multistep scheme and solves a conservative form of the density averaged continuity, momentum and energy equations in body fitted coordinates. Rotation terms are included for the computation of rotor flows. A compressible low-Reynolds number form of the k- ϵ turbulence model, and a q- ω model and an algebraic Reynolds stress model have been incorporated in a fully coupled manner to approximate Reynolds stresses.

The code is used to predict viscous flow field in a backswept transonic centrifugal compressor for which laser two focus data is available. The tip clearance flow, and curvature and rotation induced secondary flows are captured to good accuracy. Solutions which incorporate Reynolds stress model show significant, though not dramatic, differences in predicted secondary flows, wall shear stress and performance parameters, when compared to the k- ϵ solution.

The code is also utilized to simulate the tip clearance flow in a cascade. An embedded H-grid topology was utilized to resolve the flow physics in the gap. The data and predictions were performed with and without tip clearance, endwall, wall motion. Additionally, both Euler and Navier-Stokes computations were performed. The results indicate that the Navier-Stokes code captures the flow physics accurately, including tip vortex strength, trajectory, loading and interaction of tip clearance flow with the secondary flow.

The code has also been used to predict the two dimensional viscous and thermal flow field in a transonic turbine nozzle with 75° turning, $M_1 = 015$, $M_2 = 0.7$ to 1.11, Re = 0.5 - 2 x 10⁶, and T_o = 415°K. Good agreement is obtained for pressure distribution, wake and surface heat transfer.

The code has been extended to include unsteady Euler solution for predicting the unsteady flow through a cascade due to incoming wakes, simulating rotor-stator interaction. Unsteady characteristic boundary conditions are specified at inlet and exit. The predicted unsteady surface pressure distribution, unsteady lift and moment, pressure wave propagation in a flat plate due to an incoming gust compares well with the analytical theories and earlier computations. This code will be integrated with a boundary layer code to capture the unsteady viscous flow and heat transfer.

NUMERICAL SIMULATION OF TURBOMACHINERY FLOWS WITH ADVANCED TURBULENCE MODELS

B. Lakshminarayana, R. Kunz, J. Luo, S. Fan The Pennsylvania State University

- 1. Introduction
- 2. Technique and Turbulence Models
- 3. Computation of Transonic Centrifugal Compressor Flow Field
- 4. Computation of Tip Clearance Flows in Cascades
- 5. Computation of Aerothermal Field in a Transonic Nozzle
- 6. Simulation of Rotor/Stator Interaction
- 7. Conclusions

		GOV	FRNING EC (Cart	UAT esiar	TONS (1			
			$\frac{\partial Q}{\partial t} = -\left(\frac{\partial E}{\partial x} + \frac{\partial F}{\partial y} + \frac{\partial G}{\partial z}\right)$	$+\left(\frac{\partial E_v}{\partial x}+\right)$	$\frac{\partial F_v}{\partial y} + \frac{\partial G_v}{\partial z} + S$			
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•	telative velociti	és, co	nstant rotation r	ate ab	out x axis, @.	Avei	aged quantities.	
•	nergy, $e_0 = \varepsilon + \frac{q^2}{2}$.	$\frac{\omega^2 r^2}{2}$, ro	othalpy constant	along	streamlines fo	r inv	iscid steady state.	

Governing Equations - Turbulence Model

• Density-averaged low-Re number k-E, conservative form :

$$\tilde{c}_{n} = \frac{\partial \hat{\Omega}}{\partial x} + \left(\frac{\partial \hat{E}}{\partial \xi} + \frac{\partial \hat{E}}{\partial n}\right) = \left(\frac{\partial \hat{E}}{\partial \xi} + \frac{\partial \hat{E}}{\partial n}\right) + \hat{S}$$
$$\tilde{c}_{n} = \frac{1}{2} \frac{1}{pu_{i}u_{i}}, \quad \tilde{c}_{n} = \frac{\sqrt{pu_{i}^{2}}}{p}, \quad \mu_{i} = \frac{C_{\mu}f_{\mu}\overline{\rho}}{\tilde{c}},$$

$$\widehat{Q} = \frac{1}{J} \left(\frac{\overline{\rho \cdot k}}{\rho \cdot \varepsilon} \right) \widehat{E}_{\varepsilon} = \frac{1}{J} \left(\frac{\overline{\rho \cdot k \cdot U}}{\rho \cdot \varepsilon \cdot U} \right) \widehat{F}_{\varepsilon} = \frac{1}{J} \left(\frac{\overline{\rho \cdot k \cdot V}}{\rho \cdot \varepsilon \cdot V} \right) \widehat{S} = \frac{1}{J} \left(C_{1} f_{1} P - C_{2} f_{2} \overline{\rho \varepsilon} \right) \widehat{E}_{k} + \varepsilon \right)$$

.

$$\widehat{E}_{\star} = \frac{1}{J} \begin{pmatrix} \left[\mu_{1} + \frac{\mu_{t}}{Pr_{k}} \right] \left[\left(\nabla \xi \cdot \nabla \xi \right)^{2\widetilde{K}} + \left(\nabla \xi \cdot \nabla \eta \right)^{2\widetilde{K}} \\ \left[\mu_{1} + \frac{\mu_{t}}{Pr_{k}} \right] \left[\left(\nabla \eta \cdot \nabla \xi \right)^{2\widetilde{K}} + \left(\nabla \eta \cdot \nabla \eta \right)^{2\widetilde{K}} \\ \left[\mu_{1} + \frac{\mu_{t}}{Pr_{k}} \right] \left[\left(\nabla \eta \cdot \nabla \xi \right)^{2\widetilde{K}} + \left(\nabla \eta \cdot \nabla \eta \right)^{2\widetilde{K}} \\ \left[\mu_{1} + \frac{\mu_{t}}{Pr_{k}} \right] \left[\left(\nabla \eta \cdot \nabla \xi \right)^{2\widetilde{K}} + \left(\nabla \eta \cdot \nabla \eta \right)^{2\widetilde{K}} \\ \left[\mu_{1} + \frac{\mu_{t}}{Pr_{k}} \right] \left[\left(\nabla \eta \cdot \nabla \xi \right)^{2\widetilde{K}} + \left(\nabla \eta \cdot \nabla \eta \right)^{2\widetilde{K}} \\ \left[\mu_{1} + \frac{\mu_{t}}{Pr_{k}} \right] \left[\left(\nabla \eta \cdot \nabla \xi \right)^{2\widetilde{K}} + \left(\nabla \eta \cdot \nabla \eta \right)^{2\widetilde{K}} \\ \left[\mu_{1} + \frac{\mu_{t}}{Pr_{k}} \right] \left[\left(\nabla \eta \cdot \nabla \xi \right)^{2\widetilde{K}} + \left(\nabla \eta \cdot \nabla \eta \right)^{2\widetilde{K}} \\ \left[\mu_{1} + \frac{\mu_{t}}{Pr_{k}} \right] \left[\left(\nabla \eta \cdot \nabla \xi \right)^{2\widetilde{K}} + \left(\nabla \eta \cdot \nabla \eta \right)^{2\widetilde{K}} \\ \left[\mu_{1} + \frac{\mu_{t}}{Pr_{k}} \right] \left[\left(\nabla \eta \cdot \nabla \xi \right)^{2\widetilde{K}} + \left(\nabla \eta \cdot \nabla \eta \right)^{2\widetilde{K}} \\ \left[\mu_{1} + \frac{\mu_{t}}{Pr_{k}} \right] \left[\left(\nabla \eta \cdot \nabla \xi \right)^{2\widetilde{K}} + \left(\nabla \eta \cdot \nabla \eta \right)^{2\widetilde{K}} \\ \left[\mu_{1} + \frac{\mu_{t}}{Pr_{k}} \right] \left[\left(\nabla \eta \cdot \nabla \xi \right)^{2\widetilde{K}} + \left(\nabla \eta \cdot \nabla \eta \right)^{2\widetilde{K}} \\ \left[\mu_{1} + \frac{\mu_{t}}{Pr_{k}} \right] \left[\left(\nabla \eta \cdot \nabla \xi \right)^{2\widetilde{K}} + \left(\nabla \eta \cdot \nabla \eta \right)^{2\widetilde{K}} \\ \left[\nabla \eta \cdot \nabla \xi \right]^{2\widetilde{K}} + \left(\nabla \eta \cdot \nabla \eta \right)^{2\widetilde{K}} \\ \left[\nabla \eta \cdot \nabla \xi \right]^{2\widetilde{K}} + \left(\nabla \eta \cdot \nabla \eta \right)^{2\widetilde{K}} \\ \left[\nabla \eta \cdot \nabla \xi \right]^{2\widetilde{K}} + \left(\nabla \eta \cdot \nabla \eta \right)^{2\widetilde{K}} \\ \left[\nabla \eta \cdot \nabla \xi \right]^{2\widetilde{K}} + \left(\nabla \eta \cdot \nabla \eta \right)^{2\widetilde{K}} \\ \left[\nabla \eta \cdot \nabla \xi \right]^{2\widetilde{K}} + \left(\nabla \eta \cdot \nabla \eta \right)^{2\widetilde{K}} \\ \left[\nabla \eta \cdot \nabla \xi \right]^{2\widetilde{K}} + \left(\nabla \eta \cdot \nabla \eta \right)^{2\widetilde{K}} \\ \left[\nabla \eta \cdot \nabla \xi \right]^{2\widetilde{K}} + \left(\nabla \eta \cdot \nabla \eta \right)^{2\widetilde{K}} \\ \left[\nabla \eta \cdot \nabla \xi \right]^{2\widetilde{K}} + \left(\nabla \eta \cdot \nabla \eta \right)^{2\widetilde{K}} \\ \left[\nabla \eta \cdot \nabla \xi \right]^{2\widetilde{K}} + \left(\nabla \eta \cdot \nabla \eta \right)^{2\widetilde{K}} \\ \left[\nabla \eta \cdot \nabla \eta \right]^{2\widetilde{K}} + \left(\nabla \eta \cdot \nabla \eta \right)^{2\widetilde{K}} \\ \left[\nabla \eta \cdot \nabla \eta \right]^{2\widetilde{K}} + \left(\nabla \eta \cdot \nabla \eta \right)^{2\widetilde{K}} + \left(\nabla \eta \cdot \nabla \eta \right)^{2\widetilde{K} + \left(\nabla \eta \cdot \nabla \eta \right)^{2\widetilde{K}} \\ \left[\nabla \eta \cdot \nabla \eta \right]^{2\widetilde{K} + \left(\nabla \eta \cdot \nabla \eta \right)^{2\widetilde{K} + \left(\nabla \eta \cdot \nabla \eta \right)^{2$$

Coakley's q- ω model

•
$$q=\sqrt{k}, \omega=\epsilon/k$$

• $\mu_t=c_{\mu}f_{\mu}\rho q^2/\omega$
 $c_{\mu}=0.09$
 $f_{\mu}=1-\exp(-\alpha R)$
 $\alpha=0.02$
 $R=\frac{qy}{v}$

• q-equation

$$\frac{\partial(\rho q)}{\partial t} + \frac{\partial(\rho q u_j)}{\partial x_j} = \frac{\partial}{\partial x_j} [(\mu + \mu_t / \Pr_q) \frac{\partial q}{\partial x_j}] + \frac{1}{2} (c_\mu f_\mu \frac{S}{\omega^2} - \frac{2}{3} \frac{f_\mu}{\omega} - 1) \rho \omega q$$

$$S = \left(\frac{\partial u_{i}}{\partial x_{j}} + \frac{\partial u_{j}}{\partial x_{i}}\right) \frac{\partial u_{i}}{\partial x_{j}} - \frac{2}{3} \left(\frac{\partial u_{k}}{\partial x_{k}}\right)^{2}$$

$$Pr_{q} = 2.0$$

ω-equation

$$\frac{\partial(\rho\omega)}{\partial t} + \frac{\partial(\rho\omega u_j)}{\partial x_j} = \frac{\partial}{\partial x_j} [(\mu + \mu_t / \Pr_{\omega}) \frac{\partial\omega}{\partial x_j}] + [c_1(c_{\mu} \frac{S}{\omega^2} - \frac{2}{3} \frac{f_{\mu}}{\omega}) - c_2]\rho\omega^2$$

In the fully turbulent region $[Y^+ = 0(10^2)]$, a compressible extension to the high Reynolds number form of the ARSM due to Galmes and Lakshminarayana (1984) is adopted:

$$-\overline{\rho u_i'' u_j''} = -\frac{2}{.3} \delta_{ij} \rho k - \rho k T_{ij}$$

where

$$T_{ij} = \frac{R_{ij}(2-C_2)/2 + (P_{ij} - 2P\delta_{ij}/3)(1-C_2)}{P + \rho \varepsilon (C_1 - 1)},$$
$$R_{ik} = -2\omega_p (\varepsilon_{ipj} \overline{\rho u_k'' u_j''} - \varepsilon_{kpj} \overline{\rho u_i'' u_j''})$$

$$P_{ij} = \left(-\overline{\rho u_i'' u_k''} \frac{\partial u_j}{\partial x_k} - \overline{\rho u_j'' u_k''} \frac{\partial u_i}{\partial x_k}\right), \ 2P = P_{ii}$$

where $C_1 = 1.5, C_2 = 0.6$.

In the fully turbulent region $[Y^* = 0(10^2)]$, a compressible extension to the high Reynolds number form of the ARSM due to Galmes and Lakshminarayana (1984) is adopted:

$$-\overline{\rho u_i'' u_j''} = -\frac{2}{3} \delta_{ij} \rho k - \rho k T_{ij}$$

where

$$T_{ij} = \frac{R_{ij}(2-C_2)/2 + (P_{ij} - 2P\delta_{ij}/3)(1-C_2)}{P + \rho \epsilon (C_1 - 1)},$$

$$R_{ik} = -2\omega_p (e_{ipj} \overline{\rho u_k'' u_j''} - e_{kpj} \overline{\rho u_i'' u_j''})$$

$$P_{ij} = \left(-\overline{\rho u_i'' u_k''} \frac{\partial u_j}{\partial x_k} - \overline{\rho u_j'' u_k''} \frac{\partial u_i}{\partial x_k}\right), \ 2P = P_{ii}$$

where $C_1 = 1.5$, $C_2 = 0.6$.

RKCC Code

- Explicit Multistage, Conservative, Compressible Formulation
- .Generalized Coordinates; 2-D, 3-D, Unsteady; ----> Turbomachinery (Rotation Periodic B.C.)
- .Coupled Compressible Low-Reynolds-Number K-ε Model, q-ω Model, ARSM Model
- .FNS + Full Turbulent KE Production Term
- .IRS for 2-D
- .Finite Diff (Flux Evaluation = Cell Vertex Finite
 Volume)
- **.**Characteristic B.C.'s, Embedded H Mesh, Tip Clearance Topologies for Turbomachinery Application
- Eigenvalue & Local Velocity Scaling of Artificial Dissipation







1285 *C*-7



Figure 3 Qualitative representation of physical phenomena contributing to the formation of the wake flow region. a) Representative sketch adapted from Eckardt (1976) and b) computed normalized relative helicity at 68 % chord.



Figure 4 Meridional velocity profiles at L2F data acquisition Plane IV. Comparison of solutions using three turbulence models : low Reynolds number k- ε model (solid), k- ε /ARS model, R_{ij} = 0 (long dash), k- ε /ARS model, R_{ij} \neq 0 (short dash).



Figure 5 Near wall relative radial and crossflow velocity profiles at 90 % chord. a) midspan on suction surface, b) midspan on pressure surface, c) mid passage on hub. Comparison of solutions using three turbulence models : low Reynolds number k- ϵ model

(square), k- ϵ /ARS model, R_{ij} = 0 (circle), k- ϵ /ARS model, R_{ij} \neq 0 (triangle). W₃ is the radial component (+ towards tip), W₂ is the relative circumferential component (+ towards pressure surface)







Figure 7. Views of computat nomenclature a) Detail of leading (three-dimensional grid.







Figure 9 Contours of dynamic pressure (Pq²/2, in percent of inlet dynamic head) at outlet measurement plane. a) Experimental. b) Navier-Stokes. c) Euler.



Figure 10 Comparison of computed and measured spanwise distribution of mass-weighted, pitchwise averaged outlet flow angle. Measured values (symbols), Navier-Stokes (solid line), Euler (short dash line).

Figure 11 Comparison of computed and measured spanwise distribution of blade normal force coefficient. Measured values (symbols), Navier-Stokes, embedded H-grid (solid line), Navier-Stokes, "pinched" standard H-grid (long dash line), Euler (short dash line).

1292









Figure 14 Contours of flow angle at outlet measurement plane for Experiment C, $\tau/c = 0.04$. a) Measured. b) Predicted. c) Comparison of computed and measured spanwise distribution of mass-weighted, pitchwise averaged outlet flow angle for Experiment C, $\tau/c = 0.04$. Measured values (symbols), Navier-Stokes (line).



Figure 15













Figure 19. Mach no. contour for above case



Figure 20 Blade heat transfer $(M_{2is}=0.93, P_{01}=0.915 \text{ Bar}, M_1 = 0.15)$ $Tu_{\infty}=1\%, T_{01}=403K, \text{ Re}_{2}\approx 600,000)$



Figure 21 Computation Grid for a Flat Plate Cascade



Figure 22 Unsteady Blade Surface Pressure Jump a) Amplitude, b) Phase Angle



Figure 23 Unsteady Blade Pressure for a Flat Plate Cascade (at zero steady incidence) with an Incoming Moving Wake (Runga-Kutta Explicit Technique, M=0.7)



Figure 24 Vector plot of unsteady velocities (mean components is subtracted)

CONCLUSIONS RKCC

•3D CODE WITH K-e/ARSM MODEL, GOOD ACCELERATION PROPERTIES AND OPTIMUM ARTIFICIAL DISSIPATION HAS BEEN CODED, VALIDATED AND USED EXTENSIVELY TO PREDICT VISCOUS FLOW FIELD IN SUPERSONIC CASCADE, SUBSONIC CASCADES, LOW SPEED COMPRESSOR, EVOLUTION OF TIP CLEARANCE FLOW, HIGH SPEED CENTRIFUGAL COMPRESSOR FLOW FIELD.

•3D CODE IS PRESENTLY EXTENDED TO INCLUDE TIME ACCURATE SOLUTION ROTOR/STATOR INTERACTION EFFECTS.

•TURBULENCE MODEL SOURCE TERMS DO NOT AFFECT THE STABILITY OF THE NUMERICAL SCHEME - CONTRARY TO THAT GENERALLY PERCEIVED.

•IMPLICIT TREATMENT OF TURBULENCE SOURCE TERM DID NOT IMPROVE CONVERGENCE RATE.

•NO ADVANTAGE IS NUMERICALLY COUPLING THE GOVERNING EQUATION AND K-e MODEL.

•NEAR WALL TURBULENCE PHYSICS AND THE EFFECT OF ROTATION AND COMPRESSIBILITY PREDICTED ACCURATELY.

•THE EFFECT OF ROTATION AND ENDWALL SECONDARY FLOW IN THE NEAR WAKE, AND EFFECT OF ROTATION ON 3D BLADE BOUNDARY LAYERS ARE CAPTURED ACCURATELY.

•THE SPANWISE DISTRIBUTION OF LOSSES IS PREDICTED WELL AWAY FROM THE ENDWALLS, BUT ONLY FAIR PREDICTION IS ACHIEVED IN THE ENDWALL REGION.

•STAGE PRESSURE RISE, MERIODIONAL VELOCITIES IN A CENTRIFUGAL COMPRESSOR IS PREDICTED TO ENGINEERING ACCURACY. THE CRITICAL ELEMENT IS GRID, FOLLOWED BY TURBULENCE MODELLING.

•THE "PINCHED" H GRID IS THE MOST APPROPRIATE GRID TO USE IN THE TIP CLEARANCE REGION.

•THE CODE ACCURATELY CAPTURES SHOCK WAVE/BOUNDARY LAYER INTERACTION IN A CASCADE, WITH THE EXCEPTION OF REFLECTED WAVES FROM THE SUCTION SURFACE; SHOCK LOSSES ARE PREDICTED WELL.

N92-32271

ABSTRACT

DEVELOPMENT OF A CFD CODE FOR INTERNAL FLOWS IN LIQUID FUILED ENGINES

SUBMITTED TO

WORKSHOP FOR COMPUTATIONAL FLUID DYNAMIC APPLICATIONS IN ROCKET PROPULSION

To support the design efforts of engines in which liquid propellants are used, one is often required to analyze incompressible, two-dimensional or axisymmetric flows within ducts and cavities with rotating walls and complicated geometries. The steadystate solution is of interest in most cases.

This code is intended to provide a tool for efficient CFD analysis of such flow problems, taking advantage of the artificial compressibility concept and the Beam-Warming numerical scheme modified for second order accurate, implicit boundary conditions. These concepts ensure a stable, robust, and accurate algorithm due to the reduced speed of sound and the accuracy of the boundary conditions.

The code is dedicated only to two-dimensional or axisymmetric flows with or without swirl. Three-dimensional computation is excluded to increase efficiency and speed.

This paper briefly presents the theory of the code, as well as several benchmark applications with comparison to well known analytical solutions. In all these test cases, the code produced remarkably accurate results.

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Sverdrup

The Tenth Workshop for CFD Applications in Rocket Propulsion **MSFC April 1992**

Presented to

Sverdrup Technology **Youssef Dakhoul**

By

DEVELOPMENT OF A CFD CODE

FOR INTERNAL FLOWS

IN LIQUID FUELED ENGINES



NS	to support design effort	inced methods uces speed of sound Improves stability le Robust	ode with minimum overhead ith or without swirl, Incompressible	No chemistry No 3D computation	Sverdrup
MOTIVATIO	CFD Analysis of cavity flows required	Desire to use the most recent and adva Artificial compressibility Redu Beam-Warming method Stable	Desire to develop a specific-purpose co 2D, Planer, Axisymmetric, wi	No temperature computation No compressible flow	

1310

TECHNICAL OBJECTIVES

- Develop a CFD code for internal flows in liquid fueled engines
- Valid for 2D planer and axisymmetric flows with or without swirl
- Use the Artificial Compressibility Concept
- Use The Beam-Warming scheme with implicit boundary conditions
- Test the laminar capability of the code
- Add a suitable turbulence model
- Test the turbulent capability of the code

Sverdrup

Sverdrup ----

$$Q = \begin{bmatrix} p \\ u \\ v \\ w \end{bmatrix}$$

$$E = \begin{bmatrix} p \\ uu + p/p - v(2u_x) \\ uv - v(u_y + v_x) \\ uw - v(u_y + v_x) \end{bmatrix}$$

$$E = \begin{bmatrix} p \\ uv - v(u_y + v_x) \\ uv - v(u_y + v_x) \\ vv + p/p - v(2v_y) \\ vv - v(w_y - w/y) \end{bmatrix}$$

$$H = \frac{1}{y} \begin{bmatrix} p \\ uv - v(u_y + v_x) \\ uv - v(u_y - v(2v_y - 2w/y) \\ vv - v(2v_y - 2w/y) \end{bmatrix}$$

Governing Equations

 $Q_t + E_x + F_y + \alpha H = 0$

Nondimensionalization

 $Q_{t^{\circ}}^{*}+E_{x^{\circ}}^{*}+F_{y^{\circ}}^{*}+\alpha H^{*}=0$

$$Q^{*} = \begin{bmatrix} p^{*} \\ u^{*} \\ v^{*} \\ w^{*} \end{bmatrix}$$

$$E^{*} = \begin{bmatrix} \mu^{*} \\ u^{*}u^{*} + p^{*} - \frac{p^{*}}{R^{*}}(2u^{*}_{s}, + v^{*}_{s}) \\ u^{*}w^{*} - \frac{p^{*}}{R^{*}}(u^{*}_{s}, + v^{*}_{s}) \end{bmatrix}$$

$$E^{*} = \begin{bmatrix} \beta^{*}u^{*} \\ u^{*}w^{*} - \frac{p^{*}}{R^{*}}(u^{*}_{s}, + v^{*}_{s}) \\ u^{*}w^{*} - \frac{p^{*}}{R^{*}}(u^{*}_{s}, + v^{*}_{s}) \end{bmatrix}$$

$$H^{*} = \frac{1}{y^{*}} \begin{bmatrix} \beta^{*}v^{*} \\ u^{*}v^{*} - \frac{p^{*}}{R^{*}}(u^{*}_{s}, - u^{*}/y^{*}) \\ v^{*}v^{*} - \frac{p^{*}}{R^{*}}(u^{*}_{s}, - u^{*}/y^{*}) \end{bmatrix}$$

$$u^{*} = \frac{u}{V^{*}} \quad t^{*} = \frac{t}{t_{ref}} \quad p^{*} = \frac{p}{\rho_{ref}}y^{*} \quad s^{*} = \frac{\beta}{v^{*}_{ref}} \quad v^{*} = \frac{\nu}{v_{ref}} \quad \rho^{*} = \frac{\rho}{\rho_{ref}} = 1$$

$$\rho_{ref} = \rho = \text{fluid density} \quad t_{ref} = x_{ref}/v_{ref} \quad R_{e} = x_{ref}v_{ref}/v_{ref}$$

- Sverdrup

Transformation

 $Q_t + \mathcal{E}_{\xi} + \mathcal{F}_{\eta} + \alpha \mathcal{H} = 0$

$$Q = \frac{1}{J} \begin{bmatrix} p \\ u \\ v \\ w \end{bmatrix} \qquad \mathcal{E} = \frac{1}{J} \begin{bmatrix} \beta(\xi_{x}u + \xi_{y}v) \\ \xi_{z}(u^{2} + p) + \xi_{y}uv - \frac{p}{R_{z}}(a_{1}u_{\xi} + a_{2}u_{\eta} + a_{3}v_{\xi} + a_{4}v_{\eta}) \\ \xi_{z}uv + \xi_{y}(v^{2} + p) - \frac{p}{R_{z}}(a_{5}u_{\xi} + a_{6}u_{\eta} + a_{1}uv) \\ \xi_{z}uw + \xi_{y}vw - \frac{p}{R_{z}}(a_{5}w_{\xi} + a_{1}uv) + a_{1}uv) \end{bmatrix}$$

$$\mathcal{F} = \frac{1}{J} \begin{bmatrix} \beta(\eta_{z}u + \eta_{y}v) \\ \eta_{z}uv + \eta_{y}(v^{2} + p) - \frac{p}{R_{z}}(b_{3}u_{\xi} + b_{6}u_{\eta} + b_{7}v_{\xi} + b_{8}v_{\eta}) \\ \eta_{z}uv + \eta_{y}vw - \frac{p}{R_{z}}(b_{3}w_{\xi} + b_{1}uw + b_{1}v_{0}) \end{bmatrix}$$

$$\mathcal{H} = \frac{1}{J} \begin{bmatrix} \beta v \\ uv - \frac{p}{R_{z}}(c_{1}u_{\xi} + c_{2}u_{\eta} + c_{3}v_{\xi} + c_{4}v_{\eta}) \\ uv - \frac{p}{R_{z}}(c_{3}w_{\xi} + c_{6}v_{\eta} + c_{7}v) \end{bmatrix}$$

- Sverdrup -

Flux Jacobians

 $Q_t + \mathcal{E}_{\xi} + \mathcal{F}_{\eta} + \alpha \mathcal{H} = 0$

·····								
0 0 0	$\frac{\xi_x u + \xi_y v -}{J \kappa_a} (a_0 J_{\xi} + a_{10} J_{\eta} + a_{11} J)$	0	0	$\frac{\eta_{x}u+\eta_{y}v-}{JR_{a}}(b_{9}J_{\xi}+b_{10}J_{\eta}+b_{11}J)$		0	-2w	$\frac{2v-}{7\ddot{h}_{a}(c_{s}J_{\xi}+c_{a}J_{\eta}+c_{7}J)}$
$\frac{\xi_y \beta}{\xi_y u -} \frac{\xi_y \beta}{\frac{\gamma K_u}{2} (a_3 J_{\xi} + a_4 J_{\eta})}$ $\frac{\xi_z u + 2\xi_y v -}{\frac{\gamma K_c}{2} (a_7 J_{\xi} + a_8 J_{\eta})}$	a s	$\frac{\eta_y u - \eta_y u}{J \kappa} (b_3 J_{\xi} + b_4 J_n)$	$\frac{\eta_x u + 2\eta_y v - \frac{1}{J_{R_a}} (b_T J_{\xi} + b_B J_\eta)}{\frac{1}{2} R_a}$	1 ^N W	Ø	$\frac{u-J_{K}}{JK}(c_3J_{\xi}+c_4J_n)$	$\frac{v-}{k_c}(c_5J_{\xi}+c_6J_{\eta}+c_7J)$	2 <i>w</i>
$\begin{array}{c c} 0 & \xi_x \beta \\ \xi_x & 2\xi_x u + \xi_y v - \\ \xi_y & \frac{1}{2} \frac{1}{k} \left(a_1 J_\xi + a_2 J_\eta \right) \\ \xi_y & \xi_x v - \\ \xi_y & \frac{1}{2} \frac{1}{k} \left(a_5 J_\xi + a_6 J_\eta \right) \end{array}$	0 = {\$z^w}	$\eta_x \frac{2\eta_x u + \eta_y v -}{\frac{\gamma_x}{1/4} (b_1 J_\xi + b_2 J_\eta)}$	$\frac{\eta_{y}}{J\frac{\mu}{L}(b_{5}J_{\xi}+b_{6}J_{n})}$	<i>m</i> [±] μ	0	$\frac{v-}{JK}(c_1J_{\xi}+c_2J_{\eta})$	0	0
11				-	<u>_</u>	0	0	
<u>30</u>		<u>85</u> 80						
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-						بارد. ت	-	

- Sverdrup

The Beam-Warming Method

$$\left[I + \Delta t \left(\frac{\partial}{\partial \xi} \mathcal{A}^{n} + \frac{\partial}{\partial \eta} \mathcal{B}^{n} + \alpha \mathcal{C}^{n}\right) - I \epsilon_{imp}^{2} J^{-1} \left(\delta_{\xi}^{2} + \delta_{\eta}^{2}\right) J\right] \delta \mathcal{Q}^{n+1} = \Delta \mathcal{Q}^{n} - \epsilon_{exp}^{4} J^{-1} \left(\delta_{\xi}^{4} + \delta_{\eta}^{4}\right) J \mathcal{Q}^{n}$$

where I is the 4×4 unit matrix, and:

$$\delta Q^{n+1} = Q^{n+1} - Q^n$$
$$\Delta Q^n = -\Delta t \left[\mathcal{E}_{\xi}^n + \mathcal{F}_{\eta}^n + \alpha \mathcal{H}^n \right]$$

$$\delta_{\xi}^{2} f = f_{i-1} - 2f_{i} + f_{n+1}^{n} + c$$

 $\delta_{\xi}^{4}f = f_{i-2} - 4f_{i-1} + 6f_{i} - 4f_{i+1} + f_{i+2}$

Sverdrup

The first step is:

$$I + \Delta t \left(\frac{\partial}{\partial \xi} \mathcal{A}^{n}\right) - I \epsilon_{imp}^{2} J^{-1} \delta_{\xi}^{2} J \int \delta Q^{*} = \Delta Q^{n} - \epsilon_{exp}^{4} J^{-1} \left(\delta_{\xi}^{4} + \delta_{\eta}^{4}\right) J Q^{n}$$

which is solved for δQ^*

and the second step is:

$$I + \Delta t \left(\frac{\partial}{\partial \eta} \mathcal{B}^{n} + \alpha \mathcal{C}^{n}\right) - I \epsilon_{imp}^{2} J^{-1} \delta_{\eta}^{2} J \int \delta \mathcal{Q}^{n+1} = \delta \mathcal{Q}^{*}$$

which is solved for δQ^{n+1} at all nodes.

- Sverdrup

•		[\$ <u>0</u> ;]		q,	Note that the existence of the 'o' matrices prevents
•		5 Q3 5 Q3		d2 d3	the block matrix from being tridiagonal.
•	0 •	έQ		d.	These 'o' matrices are associated with domain e as well as east and west edges of blocked-out are
	• • • • • • • •	δQ [*] mar	·····	dimar].	They appear because one-sided, second-order- accurate differencing was used at these edges.

PIPE FLOW

GRID 81 × 31 NODES













SLIDE BLOCK FLOW Pressure contours (Pascal)

CONTOUR LEVELS 5000001.0 5000001.0 10000001.0 2000001.0 2000001.0 2000001.0 55000001.0 65500001.0 7500000.0 88000001.0 7500000.0 88000001.0 7500000.0 88000001.0 7500000.0 88000001.0 7500000.0 88000001.0 7500000.0 88000001.0 7500000.0 88000001.0 7500000.0 88000001.0 7500000.0 88000000.0 7500000.0 88000000.0 75000000.0 75000000.0 7500000.0 75000000.0 75000000.0 75000000.0 75000000.0 7500000.0 7500000.0 7500000.0 75000000.0 75000000.0 75000000.0 75000000.0 7500000.0 7500000.0 7500000.0 7500000.0 75000000.0 7500000.0 7500000.0 7500000.0 7500000.0 7500000.0 7500000.0 7500000.0 7500000.0 7500000.0 7500000.0 7500000.0 7500000.0 7500000.0 750000.0 750000.0 750000.0 750000.0 75000000.0 75000000.0 7500000.0 75000000.0 75000000.0 7500000.0 7500000.0 75000000.0 75000000.0 75000000.0 75000000.0 75000000.0 7500000000000000000000000000000000000	

750000.0





Wedge Flow



TWO CONCENTRIC CYLINDERS GRID 61 x 21 NODES



Initial Pressure Field = 0.0 Initial Velocity Field = 0.0









Two Concentric Cylinders



TAYLOR VORTICES GRID 101 × 31 NODES



TAVLOR VORTICES Swirl Velocity Contours (m/sec)



	894298842985
83	

TRVLOR VORTICES PRESSURE CONTOURS (Pascal)



TAMLOR VORTICES NORMALIZED STREAM FUNCIIUN







DRIVEN CAVITY FLOW GRID 51 × 51

DRIVEN CAUITY FLOW PARTICLE TRACES









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CAUTUR SAGE IS OF POOR QUALITY





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Preburner Pump Cavity
ATD PREBURNER DISCHARGE CAVITY Grid 138 x 120



ATD PREBURNER DISCHARGE CAUITY Relative Pressure Contours (psi)



RTD PREBURNER DISCHARGE CAUITY Swirl Velocity Contours (fps)





ATD PREBURNER PUMP CAUITY





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N92-32272

Development of the KIVA-II CFD Code for Rocket Propulsion Applications

by Robert V. Shannon Jr. and Alvin L. Murray

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Due to the existence of liquid, solid, and hybrid rocket motors a need exists for a fluid dynamics code which can solve for both the Navier-Stokes equations in multi-dimensions as well for liquid and solid particle motion within the gas flow domain. This type of CFD code must couple the gas and particle motion so that the effects of one upon the other can begin to be understood. Disciplines such as the evaluation of solid motor performance as well as nozzle erosion predictions for solid motors have a great need for the type of information that this type of computer code can provide. In addition, it is difficult to accurately simulate liquid motor combustion chamber flows without solving for the liquid oxidizer droplet motion, breakup, and evaporation coupled with the reacting gas flow.

The KIVA-II code, originally developed at Los Alamos National Laboratories to solve fluid dynamics problems in internal combustion engines, has been developed to solve rocket propulsion type flows. This work was supported by the NASA Solid Propulsion Integrity Program. The objective of the work performed was to develop this CFD code so that both liquid and solid particle motion could be simulated for arbitrary geometry and for high speed as well as low speed reacting flows.

Modification of the KIVA-II gas flow algorithm involved: incorporating independently specifiable supersonic and subsonic inflows and outflows, symmetric as well as periodic boundary conditions, the capability to use generalized single or multi-specie thermodynamic data and transport coefficients and allowing the user to specify arbitrary wall temperature/ heat flux distributions. Major modifications to the algorithms involving both convection and diffusion were successfully performed and results have been compared with some available experimental data on nozzle flows to verify these modifications.

Modification of the algorithms governing particle motion involved: incorporation of multispecie particle types, generalized liquid property thermodynamic data, options which prevent or allow particle evaporation, a generalized particle injection algorithm, simulation of particle elastic or inelastic collisions with solid boundaries, periodic or symmetric particle boundary conditions at boundaries which are not inflow, outflow, or wall boundaries, and incorporation of a particle drag model which allows for both Reynolds and Mach number effects on particle drag coefficients.

This new CFD code has been shown to successfully solve rocket propulsion flows as well as rocket propulsion flows with entrained particles for several different rocket nozzles, submerged and otherwise. Verification of this new CFD code continues by comparing results to experimental data as well as to predictions of other CFD codes. This program is proving to be a valuable tool in the prediction of rocket propulsion flows.

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Aerotherm Corporation Huntsville, Alabama

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Development of the KIVA-II CFD Code for Rocket Propulsion Applications	Original KIVA-II Code - General Information	 KIVA-II code originally issued in May 1989 Approx. 14000 source lines including routines for plotting Authored by A.A. Amsden, P.J. O'Rourke, T.D. Butler Two-equation turbulence k-e model Kinetic and/or equilibrium chemical reaction modeling Stochastic particle technique for liquid sprays Initial and boundary conditions written specifically for IC engine calculations 	
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Original KIVA-II Code - General Information	 Some boundary conditions inappropriate for high-speed flow problems Subsonic inflow boundary conditions not coupled with the overall pressure field solution Fuel spray was single component but modeling for droplet collisions and aerodynamic breakup was incorporated. 	Arende of order of or
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- Approx. 30000 source lines not including routines for plotting
 - Multiple inflow/outflows allowed
- Symmetric as well as periodic boundary conditions allowed
- Advection routines were recast in a form which directly computes the fluxes before using them
- modynamic data. Alternatively, an equilibrium gas mixture can Thermodynamic data input will allow for multiple species therbe modeled by a single Mollier table.
- Species transport property data is independently specified allowing for fewer points in regions where these quantities do not vary much. Viscosity, specific heats, and conductivity may all vary with pressure as well as temperature.

KIVA-IIG Code - General Changes Gas Flows

- Multiple wall types may be specified allowing the user to have a wall temperature distribution in his/her flowfield calculation.
- **Conjugate Residual Method used for calculating the pressure** and temperature fields now includes boundary condition specifications.

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Motion
Parcel
Changes
General
Code -
KIVA-IIG

- Multiple particle species available
- Generalized liquid property thermodynamic data
- **Option to prevent or allow particle evaporation for each particle** type
- Generalized particle injection algorithm which makes each simulated injector independent of all other injectors as far as injector characteristics
- Simulation of particle elastic or inelastic collisions with solid boundaries
- Periodic or symmetric particle boundary conditions at fluid boundaries
- 3 different particle drag models available

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PLANAR NOZZLE GRID

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PLANAR NOZZLE PRESSURE CONTOURS

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PLANAR NOZZLE TEMPERATURE CONTOURS



PLANAR NOZZLE MACH NUMBER CONTOURS



or Test Case	Kelvin lynes/cm² = 58 atm ecies was modeled by a single Mol- odynamic data for the equilibrium	Aerotherm Corporation
Two Inch Moto	 Chamber temperature 3564 F Chamber pressure 5.9(10)⁷ d The gas mixture of many specifier table representing thermomixture. Nozzle geometry is unusual. 	1362





TWO INCH MOTOR NOZZLE TEST CASE

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CALCULATED MACH CONTOURS

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 Chamber temperature 3564 Kelvin Chamber temperature 3564 Kelvin Chamber pressure 5.1(10)⁷ dynes/cm² = 50 atm The gas mixture of many species was modeled by a single Mollier table representing thermodynamic data for the equilibrium mixture. 10 micron particles "injected" into the flowfield. Injected particle density was 3.94 grams/cm³. Crowe-Hermsen modified drag model used. Gas-particle momentum and energy coupled 	 Chamber temperature 3564 Kelvin Chamber pressure 5.1(10)⁷ dynes/cm² = 50 atm The gas mixture of many species was modeled by a single Mollier table representing thermodynamic data for the equilibrium mixture. 10 micron particles "injected" into the flowfield. Injected particle density was 3.94 grams/cm³. Crowe-Hermsen modified drag model used. Gas-particle momentum and energy coupled 		MNASA Motor Test Nozzle Flowfield Analysis
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 Gas-particle momentum and energy coupled 	Gas-particle momentum and energy coupled	٠	Crowe-Hermsen modified drag model used.
		٠	Gas-particle momentum and energy coupled

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MNASA MOTOR TEST CONFIGURATION



Reference Thiokol Report TWR-60115

KIVA - IIG FLOWFIELD GRID





MNASA MOTOR PRESSURE FIELD









PARCEL VELOCITY CHRONOLOGY





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PARCEL VELOCITY CHRONOLOGY

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PARCEL VELOCITY CHRONOLOGY



Aerotherm Corporation A Subsidiary of DynCorp PARCEL VELOCITY CHRONOLOGY $T = 5.73(10)^{-3}$ sec $T = 5.72(10)^{-3} sec$ $T = 5.7(10)^{-3}$ sec

MNASA MOTOR 10 MICRON PARTICLE TREJECTORIES



Summary

- A new finite volume 2D/3D Navier-Stokes CFD code has been
 - developed by using the KIVA-II code as the starting point.
- Demonstration of this new code has been shown with promising results and verification with experimental data will continue.
 - Particle motion has been verified for low particle Reynolds num-

bers and demonstrated for typical solid rocket motor flowfields.

N92-32273

A Computational Design System for Rapid CFD Analysis

E.P. Ascoli, S.L. Barson, M.E. DeCroix, and M.M. Sindir CFD Technology Center Rockwell International, Rocketdyne Division Canoga Park, California

Effective application of computational fluid dynamics (CFD) in the engineering environment requires that key design and analysis tools be integrated to the greatest extent possible. A computational design system (CDS) is described in which these tools are integrated in a modular fashion. This CDS ties together four key areas of computational analysis; description of geometry, grid generation, computational codes, and postprocessing. Common input and output formats and necessary translators are established to facilitate data transfer between the four key areas and to enhance system modularity. Advances made in three key areas are described.

Significant progress has been made toward integration of geometry definition systems with CFD grid generation tools. Geometric data have successfully been passed from the Catia CAD and Patran CAE systems to the Rockwell Automated Grid Generation System (RAGGS). The IGES standard was employed in each case. The CFD Pump Consortium impeller geometry is used to illustrate that a reasonable level of integration is achievable for complex geometries.

While many CFD grid generators are available in the public domain, their capabilities vary widely. An effort is underway to systematically review available codes, identify those most applicable, and integrate them into the CDS described. Seven grid generation codes are currently being reviewed according to previously defined evaluation criteria described herein.

Postprocessing tools are being developed, reviewed, and integrated into the CDS as well. Engineering data extraction tools are being developed to be completely consistent with existing code methodologies and to remain completely modular. Tools for data visualization have advanced noticeably over the last few years. These are being reviewed and integrated into the CDS.

Integration of improved CFD analysis tools through integration with the Rocketdyne CDS has made a significant positive impact in the use of CFD for engineering design problems. Complex geometries are now analyzed on a frequent basis and with far greater ease.

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CFD 82-030-013/D2/SLB



NASA Marshall Space Flight Center

Workshop for Computational Fluid Dynamic **Applications in Rocket Propulsion**

April 28-30, 1992

E.P. Ascoli, S.L. Barson, M.E. DeCroix, and M.M. Sindir

Rockwell International, Rocketdyne Division

A COMPUTATIONAL DESIGN SYSTEM

FOR RAPID CFD ANALYSIS

GRATION OF CFD TOOLS NEEDED FOR EFFICIENT	PPLICATION IN ENGINEERING ENVIRONMENT
NTEGRA	APPLI

- APPLICATION OF CFD IN ENGINEERING CYCLE REQUIRES:
- INTEGRATION WITH EXISTING TOOLS AND PROCEDURES
 - USE FOR MULTIPLE LEVELS OF ANALYSIS
 RAPID TURNAROUND PARAMETRICS
 - FINAL DETAIL DESIGN ANALYSIS
- **PAST EMPHASIS ON FLOW SOLVER DEVELOPMENT OUTPACED THAT OF "PERIPHERAL" TOOLS**
- PRE- AND POST-PROCESSING CAN TAKE MORE THAN 50% **OF TOTAL CYCLE TIME**
- TOOL INTERFACES OFTEN POOR OR COMPLETELY LACKING



COMPUTATIONAL DESIGN SYSTEM INTEGRATES ANALYTICAL TOOLS FOR EFFICIENT USE
 TIES TOGETHER FOUR KEY AREAS OF COMPUTATIONAL ANALYSIS GEOMETRIC DESCRIPTION - MATHEMATICAL REPRESENTATION OF HARDWARE GEOMETRY
 GRID GENERATION - DISCRETIZATION OF FLOW DOMAIN COMPUTATIONAL CODES - ANALYTICAL SOLUTION POST-PROCESSING - REDUCTION, ORGANIZATION, AND PRESENTATION OF ANALYTICAL DATA
 ESTABLISHES COMMON INPUT/OUTPUT FORMATS AND NECESSARY TRANSLATORS
 MODULAR APPROACH ALLOWS USE OF MOST APPROPRIATE TOOL FOR EACH APPLICATION
Rockwell International Rocketdyne Division





ADVANCES MADE TOWARD IMPROVED AND

UNIFIED SET OF CFD TOOLS

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MANY GRID GENERATION CODES CURRENTLY AVAILABLE DEVELOP EVALUATION CRITERIA / SCORING GUIDELINES NEED EXISTS TO CONDUCT SYSTEMATIC REVIEW OF **GRID GENERATION CODES CURRENTLY AVAILABLE** DIFFERENT APPROACHES AND CODE FEATURES **GRID GENERATORS REVIEWED** IDENTIFY MOST APPROPRIATE CODE(S) THREE PHASES TO FINAL SELECTION **IDENTIFY CANDIDATE CODES PRELIMINARY EVALUATION** INTEGRATE WITH RACES FINAL EVALUATION PRE-SCREEN BACKGROUND OBJECTIVE APPROACH Rockwell International Rocketdyne Division •

CFD 92-030-020/02/SLB

SEVEN GRID GENE	ERATION CODES REVIEWED
• ICEM (CDC)	 EXTENSIVE CAD CAPABILITY THIRD PARTY SOURCE
· IGB (NASA LEWIS)	 TEMPLATE TYPE FOR TURBINE BLADES NOT A GENERAL PURPOSE CODE
• EAGLEVIEW (MSU)	 EAGLE BASED GRID GENERATION NEW INTERACTIVE INTERFACE
· GENIE (MSU)	 FIRST GENERATION INTERACTIVE CODE BEST SUITED FOR 2-D AND LIMITED 3-D
GRIDGEN (GENERAL DYNAMICS)	 INTERACTIVE GENERAL PURPOSE CODE HIGHLY RATED IN INDUSTRY
 PATRAN (PDA ENGINEERING) 	 LIMITED AS CFD GRID GENERATOR THIRD PARTY SOURCE
• RAGGS (ROCKWELL, NAA)	 INTERACTIVE GENERAL PURPOSE CODE DEVELOPING PRODUCT
Rockwell International Rockeddyne Division	

CFD 92-030-022/02/SLB **EVALUATION CRITERIA ESTABLISHED** SURFACE AND VOLUME GRID CAPABILITIES METHODOLOGIES AVAILABLE (e.g., ALGEBRAIC, ELLIPTIC, HYPERBOLIC) ACCURACY WITH SURFACE DEFINITION INTERFACES (INPUT AND OUTPUT) **FIVE MAIN CATEGORIES** AS TRANSLATED TO GG **GRID TYPES SUPPORTED CREATION CAPABILITY** SURFACE ACCURACY **GEOMETRY DEFINITION** AS CREATED IN GG H-, C-, O-TYPES FAN (DEGENERATE) MULTIZONE PERIODIC Rockwell International Rocketdyne Division



CFD 92-030-024/D2/SLB



DEVELOPMENT AND INTEGRATION OF OBJECTIVE: PROVIDE / DEVELOP CONSISTENT VARIOUS FLOW SOLVER METHODOLOGIES **DEVELOP GENERAL ENGINEERING DATA** REVIEW, SELECT, AND INTEGRATE DATA **POSTPROCESSING MUST ACCOUNT FOR** POSTPROCESSORS ENGINEERING DATA EXTRACTION SET OF POSTPROCESSING TOOLS EXTRACTION CAPABILITY VISUALIZATION CODES DATA VISUALIZATION APPROACH







ORIGINAL PAGE IS OF POOR QUALITY



	COMPUTATIONAL DESIGN SYSTEM SIGNIFICANTLY ENHANCES CFD ANALYSIS CAPABILITY
	 GOOD PROGRESS IN INITIAL PHASE BASIC CAPABILITY IN PLACE IMMEDIATE POSITIVE IMPACT
1306	 FURTHER INTEGRATION EFFORTS REQUIRED GEOMETRY INTERFACES INTERNAL TRANSLATORS INTERDISCIPLINARY TRANSLATORS
	 EXTENDED DATABASE CAPABILITY ESSENTIAL DATA STORAGE, ORGANIZATION, AND RETRIEVAL SIMPLIFY TRANSLATOR ISSUES
	Rockwell International Rocketdyne Division

N92-32274

OPTIMUM DESIGN OF NINETY DEGREE BENDS

Vijay Modi Department of Mechanical Engineering Columbia University

Abstract

An algorithm for the optimum design of an internal flow component to obtain the maximum pressure rise is presented. Maximum pressure rise in a duct with simultaneous turning and diffusion is shown to be related the control of flow separation on the passage walls. Such a flow is usually associated with downstream conditions that are desirable in turbomachinery and propulsion applications to ensure low loss and stable performance. The algorithm requires the solution of an "adjoint" problem in addition to the "direct" equations governing the flow in a body, which in the present analysis are assumed to be the laminar Navier-Stokes equations. Earlier studies have usually addressed such problems for the case of inviscid and/or irrotational flow. These assumptions may not be valid in flows that undergo sharp turning resulting in strong secondary flows and possibly and recirculating regions. The theoretical framework and separating computational algorithms presented in this study are for the steady Navier-Stokes equations.

A novel procedure is developed for the numerical solution of the adjoint equations. This procedure is coupled with a direct solver in a design iteration loop, that provides a new shape with a higher pressure rise. This procedure is first validated for the design of optimum plane in two-dimensional flow. The direct Navier-Stokes and the diffusers equations are solved using a finite volume formulation for "adjoint" spatial discretization in an artificial compressibility framework. The discretized equations are integrated using explicit Runge-Kutta time steps to obtain steady-state solutions. It is found that the computational work required to solve the "adjoint" problem is of the same order as that required to solve the direct problem. It is also found that the procedure converges within about ten iterations, and in addition, the number of design iterations are not sensitive to the grid used for the calculations. This is a significant computational advantage over heuristic design procedures based on point by point sensitivity analysis where the work increases with the refinement of the grid.

A simplified version of the above approach is then utilized to design ninety degree diffusing bends. The bend inlet is square with intermediate and exit cross-sections constrained to be rectangular. The location of bend walls is then determined in order to obtain the maximum pressure rise through the bend. Calculations were carried out for a mean radius ratio at inlet of 2.5 and Reynolds numbers varying from 100 to 500. While at this stage laminar flow is assumed it is shown that a similar approach can be conceived for turbulent flows.

OPTIMUM DESIGN OF NINETY DEGREE BENDS

Vijay Modi, Assistant Professor Hayri Cabuk, Post Doctoral Research Associate Jian-Chun Huan, Graduate Student Richard Quadracci, Graduate Student

Department of Mechanical Engineering, Columbia University, New York, New York 10027

MOTIVATION

- # How to shape internal flow passages
- # Combined turning and diffusing flow
- # Maximize pressure rise
- # Can not assume inviscid or 2-D flow

OBJECTIVES

- # Develop theoretical framework laminar 3-D
- # Develop Navier-Stokes and Adjoint solvers
- # Validate Navier-Stokes solver

(Laminar 90 degree bend, Taylor et al. 1982)

Validate Optimization Approach on

2-D straight diffusers

Apply to the design of ninety degree bends



$$u_{i,i} = 0$$

 $u_{j}u_{i,j} = -p_{,i}^{*} + \nu u_{i,jj}$, $p^{*} = p/\rho$

No slip BC on Γ_M

Dirichlet BC for u_i at Γ_I and Γ_O

$$J(\Gamma_{\boldsymbol{M}}) = \int_{\Gamma_{\boldsymbol{I}}} p^* u_i n_i ds + \int_{\Gamma_{\boldsymbol{O}}} p^* u_i n_i ds$$



 $[u_i^{\varepsilon}, p^{\varepsilon}] \equiv$ Solution to NS in Ω_{ε}

 $u_i^{\epsilon} = u_i + \epsilon \phi_i$ $p^{\epsilon} = p^* + \epsilon \pi$

 $\phi_{i,i}=0$

 $u_j\phi_{i,j} + \phi_j u_{i,j} = -\pi_{,i} + \nu\phi_{i,jj}$

$$\phi_i = 0 \quad ext{on} \quad (\Gamma - \Gamma_M)$$



$$u_{i}^{\varepsilon}]_{P_{\varepsilon}} = u_{i}^{\varepsilon}]_{P} + \epsilon \rho \left(\frac{\partial u_{i}^{\varepsilon}}{\partial n}\right)_{P} + O(\epsilon^{2})$$
$$= u_{i}]_{P} + \epsilon \phi_{i}]_{P} + \epsilon \rho \left(\frac{\partial u_{i}}{\partial n}\right)_{P} + O(\epsilon^{2})$$

$$\phi_i = -
ho\left(rac{\partial u_i}{\partial n}
ight) \qquad ext{ on } \Gamma_M.$$

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$$J(\Gamma_{M_{\epsilon}}) - J(\Gamma_{M}) = \epsilon \delta J + O(\epsilon^{2})$$

$$\delta J = \int_{\Gamma_I} \pi u_i n_i ds + \int_{\Gamma_O} \pi u_i n_i ds$$

$$z_{i,i} = 0$$
 in Ω

$$u z_{i,jj} + u_j (z_{i,j} + z_{j,i}) - r_{,i} = 0 \quad \text{in } \Omega$$
 $z_i = u_i \quad \text{on } \Gamma$

$$\delta J = \nu \int_{\Gamma_M} \rho(s) \left(\frac{\partial u_i}{\partial n}\right) \left(\frac{\partial z_i}{\partial n}\right) ds$$

$$\rho(s) = \omega(s) \left(\frac{\partial u_i}{\partial n}\right) \left(\frac{\partial z_i}{\partial n}\right)$$

Our "Adjoint" equation:

$$\nu z_{i,jj} + u_j(z_{i,j} + z_{j,i}) - r_{,i} = 0 \qquad \text{in } \Omega$$

$$w_{i} = \frac{1}{2} (z_{i} - u_{i})$$
$$q = \frac{1}{2} (r - p^{*} + (1/2)u_{j}^{2} - 2u_{j}w_{j})$$

Pironneau's "Adjoint" equation:

$$w_{i,i} = 0$$
 in Ω

$$\delta J = \nu \int_{\Gamma_{M}} \rho(s) \left(\frac{\partial u_{i}}{\partial n}\right) \left(\frac{\partial u_{i}}{\partial n} + 2\frac{\partial w_{i}}{\partial n}\right) ds$$

$$\frac{dw}{dt} = w(\text{const}) + \cdots$$

NAVIER-STOKES SOLVER

 $p_t = -\beta^2 u_{i,i}$ $u_{i,t} + u_j u_{i,j} = -p_{,i} + \nu u_{i,jj}$

- a) Artificial Compressibility
- b) Runge-Kutta Time Integration
- c) Finite Volume Discretization
- d) Artificial Dissipation
- e) Local Time Stepping
- e) Implicit Residual Smoothing



Figure 4: Geometry of a circular bend with square cross section.



Figure 5: Streamwise velocities in a bend: a) $\Theta = 30$ degrees, b) $\Theta = 60$ degrees, c) $\Theta = 77.5$ degrees.

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ADJOINT EQUATION SOLVER

$$r_{t}^{*} = -\beta^{2} z_{i,i}$$

$$z_{i,t} = \nu z_{i,jj} + u_{j}(z_{i,j} + z_{j,i}) - \frac{1}{2} (z_{k} z_{k})_{,i} - r_{,i}^{*}$$

MESH GENERATION

Thompson et al.

 $x_{\xi\xi} + x_{\eta\eta} = 0$

 $y_{\xi\xi} + y_{\eta\eta} = 0$



Boundary Conditions

- # No-slip bc on the walls
- # Zero normal derivatives at exit
- # Streamwise velocity component is specified at entrance
- # Zero normal derivatives for remaining velocities at entrance
- # Typical bc's at symettry planes
- # Zero second derivatives for pressure (a computational bc)



Diffuser Profile History



Re=200, 61 by 31 grid

 $\bigcirc : N=1$ $\sqcap : N=2$ $\triangle : N=5$ * : N=10

Skin Friction History



Re=200, 61 by 31 grid

$$\bigcirc : N=1$$
$$\sqcap : N=2$$
$$\triangle : N=5$$
$$* : N=10$$

Pressure Rise History



Re=200, 61 by 31 grid

- \bigcirc : Area-averaged pressure rise
- \triangle : Flow-averaged pressure rise

$$C_p \equiv \frac{\text{Actual Pressure Rise}}{\text{Ideal Pressure Rise}}$$



\bigcirc : Optimal diffusers

 \triangle : Straight diverging diffusers

Separating Initial Profile



Re=100, 31 by 11 grid

 $\bigcirc : N=1$ $\Box : N=2$ $\triangle : N=3$ $\diamond : N=4$ * : N=11

Grid Study



Re=200 ○: 31 by 16 □: 61 by 31

* : 121 by 61



The error in the location of the optimal diffuser profile corresponding to a 2 percent error in the total pressure rise. The optimum shape lies between the high and low y-values shown in the graph (Re=500, grid size is 61 by 21, and $L/W_1=3$).


Sketch of the inlet header



Figure 3: A representative section of a three-dimensional diffuser. Flow enters at upstream boundary Γ_I and exits at downstream boundary Γ_O . The walls to be shaped are Γ_M .

ISSUES

Geometry Constraints

In general: Move walls by $\epsilon \rho(s)$ along the normal direction, everywhere

New shape may not satisfy

- specified mean passage location
- specified cross-sectional shape
- overall system geometry
- **#** Present Work
 - No correction on side walls $(z = 0, z = z_{max})$
 - Apply mid-plane $(z = z_{max}/2)$ correction to all z locations
 - Hence all cross-sections are rectangular
- # Laminar flow results (Re < 500)

Governing Equations:

$$u_{i,i} = 0$$
$$u_j u_{i,j} = -p_{,i} + \nu u_{i,jj}$$

Design Objective:

Maximize Static Pressure Rise

$$J = \int_{\Gamma_I} p \, ds + \int_{\Gamma_O} p \, ds$$

Cabuk and Modi, 1990

$$\left(\frac{\partial u}{\partial n}\right)_{\rm wall} = 0$$

$$\left(\frac{\partial u}{\partial n}\right)_{\rm wall} = \epsilon$$

1418

DESIGN ALGORITHM

- 1: Choose an initial shape.
- 2: Generate the computational grid.
- 3: Solve the N-S equations.
- 4: Compute shear stress on the walls.
- 5: Compare wall shear stress to target distribution and determine the amount of boundary movement $\rho(s)$.
- 6: Update the shape.
- 7: Go to step (2)

$$\rho(s) = \omega(s) \left[\left(\frac{\partial u}{\partial n} \right)_{\text{wall}} - \left(\frac{\partial u}{\partial n} \right)_{\text{target}} \right]$$

Iteration History (Re=200)



Dashed Curve : N=1 \bigcirc : N=8 \triangle : N=2 \diamond : N=5



Wall shear stress along the outer wall, Re=100

 \bigcirc : Optimum diffusing bend

 \triangle : Elliptic diffusing bend Dashed Curve : Target distribution



Wall shear stress along the inner wall, Re=100

 \bigcirc : Optimum diffusing bend

 \triangle : Elliptic diffusing bend Dashed Curve : Target distribution Pressure rise along the header (Re=100)



Arclength along the bend

 \bigcirc : Optimum header \triangle : Elliptic header

Optimum Shapes





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Performance = f(shape)

Possible Applications:

- 90 Degree Bend
- Turn Around Ducts
- Transition Ducts
- S-shaped Ducts
- Straight or Curved Diffusers
- Turbine Blades
- Engine Inlets
- Turning Vanes

CONCLUSIONS

Theory

- # Theoretical Framework for Design with Navier-Stokes equations
- # Determine $\rho(s)$ from Direct+Adjoint or from Direct alone

Computational

- # Direct and Adjoint Solvers Validated for Plane Diffusers
- # Design of 90 degree Bend with Specified Cross-section, Max. Δp
- # Number of Design Cycles < 10
- # "Flow" Interpretation of Adjoint Problem

<u>Future Plan</u>

- # Apply to 3-D turbulent flow
- # Specify mean line, vary cross-section
- # Other objectives : Min. Distortion

1426

A Multi-Domain Method for Subsonic Viscous Flows Daniel C. Chan and Munir M. Sindir CFD Technology Center Rocketdyne Division, Rockwell International Corporation Canoga Park, California

We have developed a Schwarz type domain decomposition method for a pressure base, two- and three-dimensional Navier-Stokes solver. This technique allows one to partition a flow path, which can be characterized by complex geometry and/or complicated flow physics, into smaller sub-domains according to the local geometric simplicity or estimated flow scales. We can, then, sweep the sub-domains in some order and solve the Navier-Stokes equations using as boundary conditions, along the domain interfaces, the Dirichlet conditions which are taken from the most recent update of the solution in the adjacent neighboring domains. With this technique, one can minimize the adverse effects caused by grid skewness and the stiffness problem caused by disparate flow scales.

This code has been successfully applied to complicated engineering problems and the results are presented as separate papers in this conference. Here, we report the results of a few fundamental flow cases to demonstrate that a judicious use of the multi-domain method can offer a significant convergence acceleration over the traditional one-domain method. This method can be extended to exploit the architecture of a parallel computer to further improve the speed.

A MULTI-DOMAIN METHOD FOR SUBSONIC **VISCOUS FLOWS**

ROCKETDYNE DIVISION, ROCKWELL INTERNATIONAL DANIEL C. CHAN AND MUNIR M. SINDIR CFD TECHNOLOGY CENTER B√

PRESENTED AT THE NASA MARSHALL SPACE FLIGHT CENTER TENTH WORKSHOP FOR COMPUTATIONAL FLUID DYNAMIC APPLICATIONS IN ROCKET PROPULSION APRIL 28-30, 1992

AGENDA

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- MOTIVATION
- APPROACH
- FUNDAMENTAL TEST CASES
- RESULTS
- CONCLUSIONS



MOTIVATION

- OPTIMIZE THE DESIGN OF ROCKET ENGINE COMPONENTS
 CONSISTENCY AND ACCURACY
 RAPID TURN AROUND
- CHALLENGES
- COMPLEX FLOW PATH GEOMETRY
 - COMPLICATED FLOW PHYSICS
- DISPARATE FLOW SCALES STRONG COMPONENTS INTERACTIONS
- OPTIMIZE THE DESIGN OF A ROCKET PUMP
 FLANGE-TO-FLANGE ANALYSIS

APPROACH

PARTITION A COMPLEX FLOW PATH ACCORDING TO GEOMETRIC CONSTRAINTS SIMPLIFY GRID GENERATION PROCESS

- INTERACTIVE COMPONENTS

 LACK OF WELL-DEFINED BOUNDARY CONDITIONS
 - LOCALIZED POCKET OF RECIRCULATING FLOW FLOW SCALES

NUMERICAL ISSUES

- TRANSFER OF INFORMATION ACROSS INTERFACE ACCURACY AND STABILITY
- - GRID TOPOLOGY
 SIMPLY CONNECTED
 MULTIPLY CONNECTED
 MULTIPLY CONNECTED
 DATA MANAGEMENT
 NEAREST NEIGHBORS
- INTERFACIAL CONNECTIVITIES

HARDWARE ISSUES

- VECTOR LENGTH CORE MEMORY
 - - PARALLELISM



MULTI-DOMAIN PATCHING ALGORITHM

SCHWARZ APPROACH

- SWEEP THE SUB-DOMAINS IN A SEQUENTIAL ORDERAPPLY DIRICHLET CONDITION ALONG DOMAIN INTERFACESUSE MOST RECENT SOLUTION FROM THE NEIGHBORING
- DOMAINS
- NO MAJOR MODIFICATION TO BASIC NAVIER-STOKES SOLVER

 - NOT TIME ACCURATE STABILITY COULD DEPEND ON INITIAL CONDITION

GREEN'S FUNCTION APPROACH

- FOR LINEAR DIFFERENTIAL OPERATORS ONLY

 - STRONG DOMAIN COUPLING MORE WORK PER TIME STEP
 - TIME ACCURATE
 - FULLY PARALLEI



FLOW OVER A HALF CIRCLE SINGLE AND FOUR DOMAIN GRID TOPOLOGY

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FLOW OVER A HALF CIRCLE SINGLE AND FOUR DOMAIN FLOW SOLUTION (Re=100)

SINGLE DOMAIN



FOUR DOMAINS



GREEN'S FUNCTION MULTI-DOMAIN ALGORITHM ONE-DIMENSIONAL HELMHOLTZ EQUATION FORMULATION PULICANI, 1988

GOVERNING EQUATION AND BOUNDARY CONDITIONS 11.1 $\langle \cdot \cdot \rangle_{\mathcal{F}}$ 11"(~)_

$$f(x) - \sigma U(x) = f(x), \quad x \in \Omega = [-1;1]$$

 $U(-1) = g^{-}$ and $U(1) = g^{+}$

ANALYTICAL SOLUTION

for $f(x) = -2AC^{2}(\tanh Cx)(1 - \tanh^{2} Cx) - \sigma U_{e}(x)$ $U_{e}(x) = A \tanh Cx + B$ where, $A = 0.5, B = 0.5, C = 20, \sigma = 100$



GREEN'S FUNCTION MULTI-DOMAIN ALGORITHM ONE-DIMENSIONAL HELMHOLTZ EQUATION FORMULATION PULICANI, 1988

- PARTITION INTO TWO DOMAINS
- SECOND ORDER BACKWARD DIFFERENCING FOR **CENTRAL DIFFERENCING FOR INTERIOR NODES**
 - **BOUNDARY NODES**





GREEN'S FUNCTION MULTI-DOMAIN ALGORITHM

SEEK THE SOLUTION IN A FORM OF

$$U^{j} = \overline{U}^{j} + \lambda_{1j}U_{1}^{j} + \lambda_{2j}U_{2}^{j}$$
 where, $j = 1,...J$ number of subdomain

$$(\overline{U}^{j})^{"} - \sigma \overline{U}^{j} = f$$
 with $\overline{U}^{j}(x^{j-1}) = 0$ and $\overline{U}^{j}(x^{j}) = 0$

$$(\overline{U}^{j})^{"} - \sigma \overline{U}^{j} = 0$$
 with $\overline{U}^{j}(x^{j-1}) = -i + 2$ and $\overline{U}^{j}(x^{j}) = i - 1$

$$(\overline{U}^{j})^{"} - \sigma \overline{U}^{j}_{i} = 0$$
 with $\overline{U}^{j}_{i}(x^{j-1}) = -i + 2$ and $\overline{U}^{j}_{i}(x^{j}) = i - 1$

$$i = 1, 2$$

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CONTINUITY AT DOMAIN INTERFACE REQUIRE

$$U^{j}(x^{j}) = U^{j+1}(x^{j})$$
$$\frac{d}{dx}U^{j}(x^{j}) = \frac{d}{dx}U^{j+1}(x^{j})$$



ONE-DIMENSIONAL HELMHOLTZ EQUATION WITH 31 POINTS IN EACH DOMAIN, INTERFACE AT X=0



ONE-DIMENSIONAL HELMHOLTZ EQUATION WITH 5 POINTS IN FIRST DOMAIN, 51 POINTS IN SECOND INTERFACE AT X=-0.1



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ONE-DIMENSIONAL HELMHOLTZ EQUATION WITH 5 POINTS IN FIRST DOMAIN, 61 POINTS IN SECOND INTERFACE AT X=-0.4



FUNDAMENTAL TEST CASES

LAMINAR BACKWARD FACING STEP

- ARMALY, DURST, PEREIRA AND SCHONUNG, 1983
- TWO-DIMENSIONAL ANALYSIS FOR REYNOLDS NUMBER RANGING FROM 50 TO 1,500
- THREE-DIMENSIONAL ANALYSIS FOR REYNOLDS NUMBER OF 1,000
 - TWO COMPUTATIONAL DOMAINS
- PARABOLIC VELOCITY PROFILE IMPOSED AT INLET PLANE LOCATED AT FOUR STEP HEIGHTS UPSTREAM OF EXPANSION PREDICTED REATTACHMENT LENGTHS COMPARED WITH
 - **EXPERIMENTAL MEASUREMENTS**

LAMINAR DRIVEN CAVITY FLOW

- GHIA, GHIA AND SHIN, 1982
- TWO-DIMENSIONAL ANALYSIS FOR REYNOLDS NUMBER RANGING FROM 1 TO 10.000
 - TWO AND FOUR COMPUTATIONAL DOMAINS
 - INITIALIZE WITH STAGNATING CONDITION



2-D LAMINAR BACKWARD FACING STEP PREDICTED STREAMLINE AT DIFFERENT REYNOLDS NUMBERS

Re=100

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Re=1,000





2-D LAMINAR BACKWARD FACING STEP REATTACHMENT LENGTHS AT DIFFERENT REYNOLDS NUMBERS



2-D DRIVEN CAVITY FLOW TOPOLOGY AT DIFFERENT REYNOLDS NUMBERS





CPU TIME REQUIREMENT FOR FOUR AND SINGLE DOMAIN COMPUTATIONS USING 161X161 POINTS **2-D DRIVEN CAVITY** COMPUTAT



CRAY CPU TIME (SEC.)









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2-D CAVITY WITH AN ORIFICE CPU TIME REQUIREMENT FOR TWO AND SINGLE DOMAIN COMPUTATIONS USING 1500 POINTS



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SUMMARY

- MODELING OF COMPLEX FLOW PATHS
 GEOMETRIC COMPLEXITY
 POTENTIAL FOR COMPONENTS COUPLING
- OFFER CONVERGENCE ACCELERATION
- GROUP DISPARATE FLOW SCALE
 USE CORE MEMORY
 USE APPROPRIATE VECTOR LENGTH

EXPLOIT PARALLEL COMPUTER ARCHITECTURE • CONCURRENT COMPUTATION OF SUB-DOMAINS **ON DIFFERENT CPU'S**


N92-32276

LARGE EDDY SIMULATION OF COMPRESSIBLE TURBULENT CHANNEL FLOWS*

Robert A. Beddini and Jeffrey P. Ridder Department of Aeronautical and Astronautical Engineering, MC 236 University of Illinois at Urbana-Champaign Urbana, Illinois 61801

Statement of Problem: The development of turbulence within rocket propulsion chamber flows remains a difficult problem to predict. Within solid propellant rockets, for example, the flow can exhibit multiple regions of transition to turbulence, and is susceptible to various modes of aeroacoustic interaction, potentially associated with instability of the combustion/flowfield process.

Objective: To formulate, develop and validate a large eddy simulation (LES) method for compressible channel flows. Additionally, to assess the potential and limitations of the method with regard to predicting flows of interest in realistic systems.

Approach: The LES method separates the resolvable scale motions from the unresolvable (subgrid) scales by applying a spatial filter to the compressible Navier-Stokes equations. The subgrid-scale Reynolds terms are modeled using a compressible extension of an existing incompressible model for wall bounded flows. The equations are solved numerically using a modified four-step Runge-Kutta procedure in time and second or fourth-order finite differences in space.

Results and Conclusions¹: The method has been validated by simulating a low Reynolds number ($Re_b \approx 5400$), low Mach number ($M_c \approx 0.3$) turbulent Poiseuille flow. Various statistical comparisons are made with incompressible experimental and direct simulation data at similar Reynolds numbers, including higher-order statistics and spatial correlations. The results compare favorably with the incompressible data.

A high subsonic Mach number ($M_c \approx 0.3$) turbulent Poiseuille flow is also simulated for comparison with the low Mach number results at nominally constant Reynolds number. The mean velocity profile is seen to depart from the low Mach number profile, corresponding to an expected dependence of the mean density and temperature profiles on Mach number. The turbulence velocity statistics are found to be reasonably independent of Mach number. Pressure fluctuation statistics are also found to scale with the wall shear stress independently of Mach number, although normalized density and temperature fluctuations increase substantially with Mach number. The density and temperature fluctuations, although small in magnitude, are observed not to be isobarically related.

The current simulations have validated the algorithm in the incompressible limit and have demonstrated the ability of the method to simulate high subsonic Mach number flows. The principal impediment in application of the method to practical, high Reynolds number chamber flow problems is the large CPU time requirement of the calculations. At present, this bottleneck is caused in large part by resolution requirements for the turbulence-producing "streaks" in the viscous wall layer. Improvements in the subgrid-scale modeling could greatly reduce CPU requirements, leading to more rapid engineering use.

^{*} Research supported by NASA Marshall Space Flight Center under grant NGT- 50363.

¹ Ridder, J.P.: Large Eddy Simulation Of Compressible Channel Flow, Ph.D. Thesis, U. of Illinois at Urbana-Champaign, January, 1992.

LARGE EDDY SIMULATION OF COMPRESSIBLE CHANNEL FLOWS* Robert A. Beddini Jeffrey P. Ridder	Aerothermal Simulations Laboratory Department of Aeronautical and Astronautical Engineering University of Illinois at Urbana–Champaign	CFD Applications in Rocket Propulsion NASA / MSFC Huntsville, AL April 28-30, 1992	Research sponsored by NASA under grant NGT-50383, and by the National Center for Supercomputing Applications, University of Illinois at Urbana–Champaign	University of Illinois at Urbana - Champaign / Aerothermal Simulations Lab
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- TRANSITION TO TURBULENCE WITHIN THE CHAMBER. SOLID PROPULSION INTERNAL FLOWS UNDERGO
- TRANSITIONAL FLOW AND NEAR-SURFACE TURBULENCE HAVE BEEN SHOWN IN PRIOR STUDIES TO AFFECT PROPELLANT COMBUSTION (EROSIVE BURNING & ACOUSTIC RESPONSE).
- FLOW DEVELOPMENT WITH LARGE SURFACE INJECTION **TURBULENCE MODELS IN PREDICTING TRANSITIONAL** PRIOR STUDIES HAVE SHOWN INADEQUACIES IN RATES
- REQUIRED SUBSTANTIAL PARAMETER ADJUSTMENT BOTH k-e AND FULL REYNOLDS STRESS MODELS FOR SIMPLEST INTERNAL FLOWS
 - EFFECTS OF NEAR WALL "PSEUDOTURBULENCE" DIFFICULT TO MODEL.

OBJECTIVES

- FORMULATE AND DEVELOP LARGE-EDDY SIMULATION (LES) METHOD FOR COMPRESSIBLE CHAMBER FLOWS.
- COMPRESSIBLE TURBULENT FLOWS HAVE BEEN NO PRIOR SIMULATIONS OF WALL BOUNDED REPORTED.
- DIRECT SIMULATIONS OF TURBULENT CHANNEL FLOW AT VALIDATE MODEL & METHOD BY COMPARISON WITH LOW REYNOLDS NUMBERS.

1456

ASSESS PRACTICALITY AND LIMITATIONS OF LES METHOD FOR PROBLEMATIC FLOWS. ACTUAL SOLIT RICKET FLOW









 APPLICATION OF SIMULATIONS AT PRESENT. UNRESOLVED (SUBGRID) SCALES OF TURBULENCE MUST BE EMPIRICALLY MODELLED. (THERE IS NO ALTERNATIVE IF VERY LARGE REYNOLDS NUMBERS ARE CONSIDERED.) 	 ADVANTAG ADVANTAG LES APJ SCALE SCAN SCAN<th>GES PROACH RESOLVES 3-D TIME-DEPENDENT LARGE MOTIONS WHICH NATURALLY EXIST IN BERS. IDICATE POTENTIAL VORTEX/ACOUSTIC ACTIONS. ACTIONS. ROVIDE TURBULENT LENGTH SCALE MATION NEEDED IN OTHER TURBULENCE LS. ICAL ASSUMPTIONS CONFINED TO SMALLER LS. ICAL ASSUMPTIONS CONFINED TO SMALLER SCALES – PRESUMED MORE "UNIVERSAL". ITAGES TAGES TAGES SCALES – PRESUMED MORE "UNIVERSAL". SCALES – PRESUMED MORE "UNIVERSAL". SCALES – PRESUMED MORE "UNIVERSAL". SCALES – PRESUMED MORE "UNIVERSAL". SCALES – PRESUMED MORE TURBULENCE SCALES – PRESUMED MORE TURBULENCE TAGES TAGES SCALES – PRESUMED MORE TURBULENCE SCALES – PRESUMED MORE TURBULENCE TAGES TAGES DERED.)</th>	GES PROACH RESOLVES 3-D TIME-DEPENDENT LARGE MOTIONS WHICH NATURALLY EXIST IN BERS. IDICATE POTENTIAL VORTEX/ACOUSTIC ACTIONS. ACTIONS. ROVIDE TURBULENT LENGTH SCALE MATION NEEDED IN OTHER TURBULENCE LS. ICAL ASSUMPTIONS CONFINED TO SMALLER LS. ICAL ASSUMPTIONS CONFINED TO SMALLER SCALES – PRESUMED MORE "UNIVERSAL". ITAGES TAGES TAGES SCALES – PRESUMED MORE "UNIVERSAL". SCALES – PRESUMED MORE "UNIVERSAL". SCALES – PRESUMED MORE "UNIVERSAL". SCALES – PRESUMED MORE "UNIVERSAL". SCALES – PRESUMED MORE TURBULENCE SCALES – PRESUMED MORE TURBULENCE TAGES TAGES SCALES – PRESUMED MORE TURBULENCE SCALES – PRESUMED MORE TURBULENCE TAGES TAGES DERED.)
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APPROACH

University of Illinois at Urbana - Champaign / Aerothermal Simulations Lab

	APPROACH - METHOD
•	EQUATIONS: 3-D TIME-DEPENDENT COMPRESSIBLE NAVIER- STOKES, FILTERED IN SPACE AND FAVRE AVERAGED.
•	SUBGRID REYNOLDS STRESSES AND HEAT FLUX MODELLED USING SMAGORINSKY MODEL (cf MOIN &KIM, '83).
•	NUMERICAL METHOD:
	METHOD DOES NOT ASSUME PERIODIC (SPECTRAL) DECOMPOSITION IN ANY DIRECTION.
	 SECOND AND FOURTH ORDER CENTRAL DIFFERENCES IN SPACE ASSESSED.
	 MODIFIED FOURTH-ORDER TIME DIFFERENCING SCHEME DEVELOPED FOR CELL Re>10. RESULTS IN 40% DECREASE IN CPU TIME.
	 CODE WELL VECTORIZED – 150 MFLOPS ON CRAY Y/MP.

	APPLICATION CONDITIONS
	 POISEUILLE FLOW - Re~ 5400 (BASED ON AV. U AND HEIGHT) THOUGH NOT REQUIRED, PERIODIC BC'S IN ON LENGTH
	AND DEPTH BOUNDARIES WERE USED TO COMPARE WITH PRIOR STUDIES.
	• Mach No. UF 0.3 USED TO VALIDATE METROU AND ASSESS SUBGRID PARAMETERS
14	 Mach No. OF 0.7 USED TO ASSESS COMPRESSIBLE FLOW EFFECTS W/O ADDITIONAL SHOCK CAPTURING DISSIPATION TERMS.
60	 GRID RESOLUTION EFFECTS ASSESSED – BASELINE GRID WAS 32 L x 90 H x 80 D. (=> 4 MW MEMORY REQUIREMENT).
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RESULTS (HIGH Mach No.)

- MEAN DENSITY GRADIENT IN NEAR WALL REGION, BUT AS EXPECTED. MEAN VELOCITY PROFILE AFFECTED BY FOLLOWS CROCCO SCALING.
- SCALE WELL WITH MEAN VELOCITY AT THIS SUBSONIC **REYNOLDS STRESSES AND PRESSURE FLUCTUATIONS** MACH NUMBER.
- RMS TEMPERATURE AND DENSITY FLUCTUATIONS FOUND TO SCALE NEARLY AS M² , BUT ARE NOT ISOBARICALLY RELATED.





RESOLVED REYNOLDS SHEAR STRESS COMPARISON



RESOLVED RMS PRESSURE AND TEMPERATURE FLUCTUATIONS



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	SUMMARY/CONCLUSIONS
٠	LES METHOD FOR WALL-BOUNDED COMPRESSIBLE FLOWS DEVELOPED AND VALIDATED.
•	FEASIBILITY OF LES SIMULATIONS FOR MORE COMPLEX FLOWS INDICATED PROVIDING MEAN FLOW IS NOMINALLY TWO-D.
•	FAVORABLE COMPARISON WITH DIRECT SIMULATION RESULTS AND EXPERIMENTAL DATA AT LOW MACH NO.
	• IMPROVEMENTS REQUIRED IN SUBGRID MODELING.
	 SCALE UP TO VERY-LARGE Re OTHERWIZE LIMITED BY RESOLUTION OF NEAR WALL STREAKS

	SUMMARY/CONCLUSIONS (2)
1468	 PRESSURE FLUCTUATION SPECTRA OBTAINED - POTENTIAL FEEDBACK TO PROPELLANT RESPONSE. WHY DO DIRECT AND LES METHODS UNDERPREDICT PRESSURE FLUCTUATIONS? LENGTH-SCALE DATA OBTAINED - COULD PROVIDE INFORMATION TO TURBULENCE MODELS FOR OTHER APPLICATIONS. LENGATH-SCALE DATA OBTAINED - COULD PROVIDE INFORMATION TO TURBULENCE MODELS FOR OTHER APPLICATIONS. NORMALIZED REYNOLDS STRESSES AND PRESSURE FLUCTUATIONS NEARLY INDEPENDENT OF MACH NO. NORMALIZED TEMPERATURE AND DENSITY FLUCTUATIONS VARY NEARLY AS M² => ARE THESE ACCOUNTED FOR IN HOT WIRE DATA REDUCTION??
·	
	University of Illinois at Urbana - Champaign / Aerothermal Simulations Lab

N92-32277

Treating Convection in Sequential Solvers

Wei Shyy

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The treatment of the convection terms in the sequential solver, a standard procedure found in virtually all pressure based algorithms, to compute the flow problems with sharp gradients and source terms is investigated. Both scalar model problem and one-dimensional gas dynamics equations have been used to study the various issues involved. Different approaches including the use of nonlinear filtering technique and the adoption of TVD type schemes have been investigated. Special treatments of the source terms such as pressure gradients and heat release have also been devised, yielding insight and improved accuracy of the numerical procedure adopted.

A Proposed Hierarchy of Test Problems

1. Nonlinear scalar wave equation to study capturing of sharp gradient

2. 1-D gas dynamics in a tube _____

(a) to study coupling among u, v, p and ρ



(b) to study interaction with B.C.s and among waves



(c) to study formation and propagation of acoustic and entropy waves



3. 1-D Combusting Flow in a Duct

- to study effect of chemical heat release and its impact on acoustic and entropy waves.
- to study propagation and interaction of nonlinear waves in pressure, thermal and convective fields.
- to understand the longitudinal combustion instability and to devise active control strategy



4. Multidimensional Problems

For a numerical scheme two features control its performance : Amplification factor ______ numerical damping Phase angle ______ numerical dispersion Problems of convection treatment : First order upwind scheme ______ excessive damping dispersion problem suppressed Higher order schemes ______ no excessive damping dispersion problem appears

- Nonlinear filtering
- TVD type approach with source term treatment and artificial compression



Backward Euler time stepping scheme :



1473

Point : A highly dispersive scheme may become a good one if dispersive problems in high wave number can be fixed; or better yet, to make constructive use of these wiggles

A possibility : Nonlinear Filtering

Key elements :

- * maintains conservation laws
- * utilizes standard schemes as basis
- * attempts to eliminate wiggles a posteriori (a geometric approach)
- * effective only for short wavelength oscillations $(2\Delta \text{ and } 4\Delta)$ & hence can check the filtering effectiveness via grid refinement

Define

--- Energy Content



--- Area Content

$$A = \sum_{j}^{N} \phi_{j}$$

--- Goal :

- * minimize E
- * maintain A 1474







16 Δ sine wave is only slightly altered after first filtering. Further application has no effect. E=0.999





 $Re = 10^4$ time step = 600

Euler Equations as a Simultaneous System

$$\frac{\partial U}{\partial t} + \frac{\partial F(U)}{\partial x} = 0$$

$$U = \begin{bmatrix} \rho \\ m \\ E \end{bmatrix}, \qquad F = \begin{bmatrix} m \\ m^2/\rho + p \\ (E + p)m/\rho \end{bmatrix}$$

Can also write

$$\frac{\partial U}{\partial t} + A(U)\frac{\partial U}{\partial x} = 0, \qquad A(U) = \frac{\partial F(U)}{\partial U}$$

Speed of sound

$$c = \sqrt{\frac{\partial p}{\partial \rho}} = \sqrt{\gamma \frac{p}{\rho}}$$

The eigenvalues of Jacobian matrix are

$$(a^{1},a^{2},a^{3}) = (u-c, u, u+c)$$

Sequential Approach with Coordinated Chracteristics

$$\frac{\partial \rho}{\partial t} + \frac{\partial [\rho u]}{\partial x} = 0$$

$$\frac{\partial m}{\partial t} + \frac{\partial [mu]}{\partial x} = -\frac{\partial p}{\partial x}$$

$$\frac{\partial E}{\partial t} + \frac{\partial [Eu]}{\partial x} = -\frac{\partial (pu)}{\partial x}$$

Pressure terms : source terms

The local characteristic speed : convection speed

$$a_{j+1/2} = \frac{1}{2} (u_j + u_{j+1})$$

(same for all equations)

Special Source Term Treatment

Conservation law with a source term $\Psi(u)$

$$u_{\iota} + f(u)_{z} = \psi(u)$$

Examples:

Method I - MacCormack's explicit predictor-corrector method

Method II : Operator splitting (Strang's time-splitting)

$$U^{n+1} = S_{\psi}(k/2) S_{f}(k) S_{\psi}(k/2) U^{n}$$

where S_f represents the numerical solution operator for the system $u_i + f(u)_x = 0$

and S_{ψ} is the numerical solution operator for the ODE $u_{t} = \psi(u)$



a) First-order upwind and second-order Lax-Wendroff schemes.



(b) Harten's TVD scheme ($\delta = 0$).

Density profiles using the simultaneous solution approach using different schemes.











The standard shock tube (open-ended) problem: density and energy profiles using sequential approach with source term treatment, for different values of δ .

THE RESONANT PIPE PROBLEM

SIMULTANEOUS SOLVER



Conclusions

- For sequential solvers, coordination of propagation speed among equations requires extra care.
- Can apply modern TVD type schemes with source term treatment to improve accuracy.
- Can utilize nonlinear filtering techniques to eliminate dispersion problems.
- Several test problems have been investigated; results show promise.

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