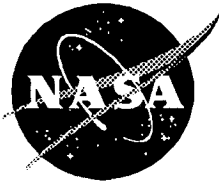


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IGNITION DYNAMICS OF A LAMINAR DIFFUSION FLAME IN THE FIELD OF A VORTEX EMBEDDED IN A SHEAR FLOW

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ABSTRACT

The role of streamwise-spanwise vorticity interactions that occur in turbulent shear flows on flame/vortex interactions is examined by means of asymptotic analysis and numerical simulation in the limit of small Mach number. An idealized model is employed to describe the interaction process. The model consists of a one-step, irreversible Arrhenius reaction between initially unmixed species occupying adjacent half-planes which are then allowed to mix and react in the presence of a streamwise vortex embedded in a shear flow. It is found that the interaction of the streamwise vortex with shear gives rise to small-scale velocity oscillations which increase in magnitude with shear strength. These oscillations give rise to regions of strong temperature gradients via viscous heating, which can lead to multiple ignition points and substantially decrease ignition times. The evolution in time of the temperature and mass-fraction fields is followed, and emphasis is placed on the ignition time and structure as a function of vortex and shear strength.

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1. INTRODUCTION

The presence of streamwise vortices is now very well established in wall-bounded shear flows as well as free shear flows either in transitional state or fully developed turbulent state. The investigations of Klebanoff, Tidstrom and Sargent (1962), Wray and Hussaini (1984), and Zang and Hussaini (1987) provide the evidence for the existence of streamwise vortices in low-speed boundary layers undergoing laminar-turbulent transition. Such vortices have been observed in the buffer region of the turbulent boundary layers by Blackwelder and Eckelmann (1979) for instance. The review of Willmarth (1975) cite some earlier observations of these phenomena. In free shear flows, the experimental studies (e.g., Lasheras and Choi (1988) and the references therein), theoretical studies (e.g., Lin and Corcos (1984) and the references cited therein), and the direct numerical simulations (e.g., Metcalf, et al. (1987) and Ashurst and Meiburg (1988)) have provided some insight into the origin and evolution of these streamwise vortices.

The evolution of a shear flow in the presence of streamwise vortices, or conversely, the dynamics of vortices stretched by shear flow is of fundamental interest in fluid mechanics. A physically and geometrically simple model of such interactions between spanwise and streamwise vorticity appears to have been first proposed by Pearson and Abernathy (1984). Their model assumes an incompressible mean flow with uniform shear which is then disturbed by the introduction of an Oseen vortex with its axis in the streamwise direction. Corcos (1988) has studied this problem by a systematic asymptotic approach with a focus and range different from that of Pearson and Abernathy. He showed that the streamwise velocity component underwent severe distortions in a region of thickness $v^{1/3}$ as a result of the streamwise vortex. These distortions were damped out in the viscous core region, which is of size $v^{1/2}$. This model, however, is restricted to the analysis of streamwise structures of turbulent non-reacting shear flows. We shall now focus our attention to reacting flows.

An important problem in the general area of non-premixed combustion is the study of chemical reactions in turbulent reacting flows. However, such flows are difficult to analyze and few theoretical studies have been conducted. One such theoretical investigation, which forms the genesis of our model and is to be described in more detail later, is that of Marble (1985), who developed a simple model problem which locally describes an established thin flame that is being wrapped up by a small scale eddy. However, there are certain important aspects, such as ignition and flame structure, which were not included within the framework of the Marble problem.

We have completed a systematic analysis of the ignition process and the subsequent flame structure of diffusion flames in vortex dominated flows using asymptotics and direct numerical simulation in the absence of a shear flow (Macaraeg, Jackson and Hussaini, 1992). We considered a constant-density, one-step, irreversible Arrhenius reaction between initially unmixed species of fuel and oxidizer occupying adjacent half-planes, which were then allowed to mix and react in the presence of a single point vortex. Using large activation energy asymptotics, particular attention was paid to the ignition regime as a function of the vortex Reynolds number. For near equal initial temperatures of the fuel and oxidizer and expanding the temperature about its inert value, it was shown that the overall ignition time decreases slightly and then asymptotes to a finite value as the vortex Reynolds number is increased from zero. For finite values of the activation energy, a direct numerical solution was used to study post-ignition events. First, a hot spot develops within the viscous core of the vortex (ignition) and progresses rapidly into a circular flame which grows in time according to a similarity rule. Next, a tribrachial flame configuration evolves at infinite distance to the right

and left of the origin. The diffusion flames emanating from this configuration then move toward and finally merge with the flame in the reacted core region. We have recently extended the ignition study to flows with counter rotating vortices (Kozusko, Macaraeg and Jackson, 1993).

The above mentioned problem of a flame interacting with a single point vortex is supposed to model certain fundamental mechanisms of turbulent diffusion flames which form the basis of many propulsion devices. Since acoustic waves are always present in these combustion systems, the role of acoustics in such flame/vortex interactions was investigated (Jackson, Macaraeg and Hussaini, 1993). The acoustic field was considered to be a spatially uniform but time dependent pressure wave of small amplitude. This pressure wave was then taken to have the sinusoidal form $P(t) = P_A \sin(\omega t + \Phi)$, where P_A is the amplitude, ω is the frequency and Φ is the phase, and was regarded as a single Fourier mode of a more general pressure wave. It was concluded that for low frequencies, ignition is accelerated or significantly delayed depending on the phase, while for moderate to high frequencies, ignition is always enhanced independent of phase. Finally, an approximation for the ignition time was found by considering an equivalent homogeneous problem in which spatial variations are ignored. This leads to the following implicit formula for the "homogeneous" ignition time t_{ig}^H , given by

$$\int_0^{t_{ig}^H} e^{P(\tau)} d\tau = t_{ig}^0,$$

where t_{ig}^0 is the ignition time in the absence of a pressure disturbance. Thus, this implicit formula relates the ignition time when pressure disturbances are absent to the homogeneous ignition time when pressure disturbances are present. It was found that this homogeneous ignition time predicts the ignition trends very well, and therefore was proposed as a good engineering approximation for obtaining the ignition times for the more complicated flow fields.

The above mentioned ignition studies have been confined to vortices evolving in an otherwise constant flow. However, shear is an important attribute of turbulent flows. Thus, the purpose of the present study is to extend the above analysis so as to investigate the effects of the interaction between a streamwise vortex and spanwise vorticity induced by the shear on ignition. We assume a simplified kinetic model consisting of a one-step, irreversible Arrhenius reaction between unmixed species occupying adjacent half-planes which are then allowed to mix and react in the presence of a streamwise vortex embedded in a shear flow. We remark here that any realistic modeling of complex kinetics will necessitate a full numerical solution. Then questions arise as to the reaction rates and their dependence on temperature and the relative importance of various reactions which entail thus rather large uncertainties. In a mathematical treatment of combustion, the kinetic model has to be necessarily simple. The one-step irreversible Arrhenius model has been extensively used with significant success in the study of low-speed combustion (e.g., Buckmaster and Ludford, 1982). This model appears to cover the essential physics of the problem. In the last decade or so, the asymptotic studies of combustion based on this model have significantly enhanced our understanding of ignition, of flame stability and of diffusion flame structure in low subsonic flows. There is as yet no reason to believe that this model will not play an equally significant role in enhancing our understanding of supersonic combustion. In any event, this idealization makes the problem amenable to asymptotic analysis and thus provides a semi-analytical solution. The results can then certainly verify and in turn be verified by full numerical simulations. An idealized model is now employed to describe the interaction process: the

streamwise vortex, assumed to be infinite in extent, interacts in time with the streamwise velocity component associated with the spanwise vorticity. Initially, the streamwise velocity is assumed to be a linear shear profile and the streamwise vortex resides along the fuel-oxidant interface. The reactants are then allowed to mix and react. Emphasis is placed on ignition time and structure. In Section 2 the basic equations and assumptions are presented. Section 3 contains the ignition analysis and results, and the conclusion is given in Section 4.

2. PROBLEM FORMULATION

In this section the problem for the time evolution of initially unmixed species occupying adjacent half-planes which are then allowed to mix and react in the presence of a vortex embedded in a shear flow (Figure 1) is formulated. We assume that the flow is independent of the downstream direction x for all time. Although it is not strictly true for any real flow, it is consistent with experimental observations that streamwise vortical structures in turbulent flows are essentially aligned with the flow and are of great streamwise extent. Since we are interested in flows with vortical motion, the basic equations are transformed into cylindrical coordinates $(y, z) \rightarrow (r, \theta)$ by the transformations $y = r \cos \theta$ and $z = r \sin \theta$. If we define g to be the radial velocity and h to be the axial velocity, i.e., $v = g \cos \theta - h \sin \theta$ and $w = g \sin \theta + h \cos \theta$, then the governing non-dimensional equations in cylindrical coordinates, neglecting all dependency in x , reduce to

$$\rho T = P, \quad (2.1a)$$

$$\rho_t + (\rho g)_r + \frac{1}{r} (\rho h)_\theta + \frac{\rho g}{r} = 0, \quad (2.1b)$$

$$\rho [u_t + g u_r + \frac{h}{r} u_\theta] = \frac{1}{\text{Re}} \nabla^2 u, \quad (2.1c)$$

$$\rho [g_t + g g_r + \frac{h}{r} g_\theta - \frac{h^2}{r}] + \frac{P_r}{\gamma M^2} = \frac{1}{\text{Re}} \left[\nabla^2 g - \frac{g}{r^2} - \frac{2}{r^2} h_\theta + \frac{1}{3} K_r \right], \quad (2.1d)$$

$$\rho [h_t + g h_r + \frac{h}{r} h_\theta + \frac{g h}{r}] + \frac{1}{\gamma M^2} \frac{P_\theta}{r} = \frac{1}{\text{Re}} \left[\nabla^2 h - \frac{h}{r^2} + \frac{2}{r^2} g_\theta + \frac{1}{3r} K_\theta \right], \quad (2.1e)$$

$$\rho [T_t + g T_r + \frac{h}{r} T_\theta] - \frac{\gamma - 1}{\gamma} [P_t + g P_r + \frac{h}{r} P_\theta] = \frac{1}{\text{Re} Pr} \nabla^2 T + \frac{(\gamma - 1) M^2}{\text{Re}} \Phi + \beta \Omega, \quad (2.1f)$$

$$\rho [F_{j,t} + g F_{j,r} + \frac{h}{r} F_{j,\theta}] = \frac{1}{\text{Re} Sc} \nabla^2 F_j - \Omega, \quad j = 1, 2, \quad (2.1g)$$

$$\Omega = \tau Da \rho F_1 F_2 e^{-Z_e/T}, \quad (2.1h)$$

where ∇^2 is the two-dimensional Laplacian operator in cylindrical coordinates, Φ is the viscous dissipation term, and $K = g_r + g/r + h_\theta/r$. Here, (u, g, h) are the velocity components in the (x, r, θ) directions, respectively; ρ is the density; T is the temperature; P is the pressure; and F_1 and F_2 the mass fractions of the fuel and oxidizer, respectively. The chemical model is assumed to be a one-step, irreversible Arrhenius reaction. The nondimensional parameters appearing above are the Schmidt number $Sc = \nu/D$ assumed equal for both species with D the species diffusion coefficient and ν the kinematic viscosity; the Prandtl number Pr ; the Reynolds number $Re = L_v V_v / \nu$ where L_v and V_v are characteristic length and velocity scales of the vortex; the Zeldovich number $Ze = E / (R^\circ T_\infty)$ with E the dimensional activation energy and R° the universal gas constant; the Damkohler number $Da = t_d / t_c$ defined as the ratio of the characteristic diffusion time scale t_d to the characteristic chemical time scale t_c ; β the heat release per unit mass of F_1 ; γ the ratio of specific heats; the Mach number $M = V_v / a_\infty$ where a_∞ is the characteristic speed of sound; and finally $\tau = t_v / t_d$ is the ratio of the time scale of the vortex t_v to that of diffusion. The density, temperature, pressure and mass fractions are nondimensionalized by their initial values ρ_∞ , T_∞ , $P_\infty = \rho_\infty R^\circ T_\infty$ and $F_{1,\infty}$, respectively. Lengths are referred to L_v , a characteristic lengthscale of the vortex, such as the core size, and velocities are referred to V_v , the reference tangential velocity. The actual choice for these scales is given in the next section. The relevant time scale is therefore $t_v = L_v / V_v$. The system (2.1) must be solved subject to appropriate initial and boundary conditions chosen to represent a streamwise Oseen vortex evolving in a shear flow.

3. IGNITION

At time $t = 0$, the reaction rate is exactly zero owing to the product $F_1 F_2 = 0$. For $t > 0$, the fuel and oxidizer begin to mix by diffusion, as well as by convection due to the presence of the vortex, and the reaction rate is no longer zero. For small time, it can thus reasonably be assumed that the effect of the reaction on the overall flow field is small. The solution for small time in which the reaction rate term is neglected is known as the inert or chemically frozen solution, and will be denoted by the superscript I . In what follows, we only consider the case of near equal initial temperatures and small Mach numbers, and take the asymptotic limit of large Zeldovich number (for the simplified hydrogen-oxygen system $2H_2 + O_2 \rightarrow 2H_2O$ in the presence of an inert N_2 , the dimensional activation energy E lies in the range 0(7-40 kcal/mole) yielding $Ze \approx 5-20$ for T_∞ in the range 300–2000°K; e.g., Glassman, 1977; also, Drummond and Mukunda, 1988, in their numerical work on reacting mixing layers uses 7200 cal/mole). For large activation energies (and hence large Zeldovich numbers), this assumption leads to the inert solutions $T^I = \rho^I = 1 + O(Ze^{-1})$, provided that the Mach number is no larger than $Ze^{-1/2}$ so that the viscous dissipation term can be neglected to leading order. For larger Mach numbers the temperature field can no longer be considered uniform to leading order since heating must take place by means of the dissipation term. The $O(Ze^{-1})$ term is included to allow for small initial temperature differences across the interface. Thus, the leading-order inert solution corresponds to the constant density approximation prevalent in the combustion literature. As time increases, more of the combustible mixes until, at some finite time, a thermal explosion occurs characterized by significant departure from the inert. To analyze the ignition process, we determine the effect of the growing reaction rate by expanding about the inert solution as

$$T = 1 + Ze^{-1} T_1 + O(Ze^{-2}), \quad \rho = 1 + Ze^{-1} \rho_1 + O(Ze^{-2}), \quad F_j = F_j^I + O(Ze^{-1}), \quad (3.1a)$$

$$(u, g, h) = (u^I, g^I, h^I) + O(Ze^{-1}), \quad P = 1 + \gamma M^2 [P^I + O(Ze^{-1})], \quad (3.1b)$$

and take the asymptotic limit $Ze \rightarrow \infty$. The viscous dissipation term in (2.1f) in this limit is of the order $M^2 Ze$, and for a proper balance of the energy equation we set

$$M = M_0 / \sqrt{Ze}. \quad (3.2)$$

Thus, solutions are also sought in limit of small Mach numbers. A comment about the size of the Mach number and the relative importance of the viscous dissipation term in the energy equation is in order here. For typical combustion systems the Mach numbers are of the order $O(10^{-3})$, and so the role of viscous heating is negligible. Here, however, we have in mind propulsion devices in high speed flows. As such, the Mach number within the mixing region can be relatively large. For example, in their study of compressible viscous vortices, Colonius et al. (1991) report Mach numbers in the range of 0.0625 to 0.67 (the definition of their Mach number is the same as used here). In our work, we have taken $M_0 = \sqrt{Ze} M$ with M_0 lying in the range (0.3-0.7), corresponding to Mach numbers of 0.01 to 0.22, respectively, for a typical value of $Ze=10$. These values are well within physical ranges. Thus, in these flow situations, viscous heating can indeed play a major role in the ignition dynamics.

The leading-order equations are given by

$$\rho_1 + T_1 = \gamma M_0^2 P^I, \quad (3.3a)$$

$$g_r^I + \frac{1}{r} h_\theta^I + \frac{g^I}{r} = 0, \quad (3.3b)$$

$$u_t^I + g^I u_r^I + \frac{h^I}{r} u_\theta^I = \frac{1}{\text{Re}} \nabla^2 u^I, \quad (3.3c)$$

$$g_t^I + g^I g_r^I + \frac{h^I}{r} g_\theta^I - \frac{h^{I2}}{r} + P_r^I = \frac{1}{\text{Re}} \left[\nabla^2 g^I - \frac{g^I}{r^2} - \frac{2}{r^2} h_\theta^I \right], \quad (3.3d)$$

$$h_t^I + g^I h_r^I + \frac{h^I}{r} h_\theta^I + \frac{g^I h^I}{r} + \frac{1}{r} P_\theta^I = \frac{1}{\text{Re}} \left[\nabla^2 h^I - \frac{h^I}{r^2} + \frac{2}{r^2} g_\theta^I \right], \quad (3.3e)$$

$$T_{1,t} + g^I T_{1,r} + \frac{h^I}{r} T_{1,\theta} - (\gamma-1) M_0^2 P_t^I = \frac{1}{\text{Re} Pr} \nabla^2 T_1 + (\gamma-1) \frac{M_0^2}{\text{Re}} \Phi^I + \tau F_1^I F_2^I e^{T_1}, \quad (3.3f)$$

$$F_{j,t}^I + g^I F_{j,r}^I + \frac{h^I}{r} F_{j,\theta}^I = \frac{1}{\text{Re} Sc} \nabla^2 F_j^I, \quad j = 1, 2, \quad (3.3g)$$

$$\Phi^I = (h_r^I - \frac{h^I}{r})^2 + u_r^{I2} + \frac{1}{r^2} u_\theta^{I2}. \quad (3.3h)$$

where we have chosen the Damkohler number Da to be

$$Da = \frac{e^{Ze}}{\tau \beta Ze}. \quad (3.4)$$

This particular choice of the Damkohler number ensures that a distinguished limit exists, in that the reaction rate term is of the same order in a Zeldovich number expansion as the time derivative terms (see, e.g., Buckmaster and Ludford, 1982). This implies that we are looking at the fast chemistry limit and thus selects our chemical time scale.

We first see that the continuity and momentum equations (3.3b-e) are decoupled from the rest of the system and thus, will completely determine u^I , g^I , h^I and P^I . At $t = 0$, we situate a point vortex at the origin and allow it to diffuse under the action of viscosity. Then, assuming the flow in the (r, θ) plane to be axisymmetric, the induced non-dimensional flow field is given by (Lamb, 1932)

$$g^I = 0, \quad h^I = \frac{1}{r} [1 - \exp(-Re r^2 / 4 t)], \quad (3.5)$$

$$P^I(r, t) = - \int_r^\infty \frac{h^{I^2}(\bar{r}, t)}{\bar{r}} d\bar{r} \equiv - \frac{Re}{4t} \left\{ \frac{2}{\eta^2} (1 - 2e^{-\eta^2/4} + e^{-\eta^2/2}) + Ei(\eta^2/4) - Ei(\eta^2/2) \right\}, \quad (3.6)$$

where $\eta = r \sqrt{Re} / \sqrt{t}$. The solution (3.5)-(3.6) is the solution for the incompressible Oseen vortex. The velocity scale V_v has been chosen so that the corresponding potential vortex at L_v (i.e., at $r = 1$) is unity, resulting in the relationship

$$\frac{\Gamma}{2\pi L_v V_v} = 1,$$

where Γ is the circulation parameter of the vortex. This particular choice shows that

$$Re = \frac{L_v V_v}{\nu} = \frac{\Gamma}{2\pi \nu} = R_o$$

where R_o is the usual vortex Reynolds number. The streamwise velocity component u^I is found from the equation

$$u_t^I + \frac{h^I}{r} u_\theta^I = \frac{1}{Re} \nabla^2 u^I, \quad (3.7)$$

which is to be solved subject to the initial and boundary conditions,

$$u^I = k_1 + k_2 z \quad \text{at } t > 0, r \rightarrow \infty, 0 < \theta < 2\pi, \quad \text{and } t = 0, r > 0, 0 < \theta < 2\pi, \quad (3.8)$$

where k_1 is the nondimensional velocity at the centerline and k_2 is the local nondimensional shear, defined as the ratio of the time scale of the vortex to that of the shear. In this study we shall assume that $k_2 = O(1)$

so that the two time scales are comparable. At this order the streamwise vortex influences the streamwise velocity component and hence the associated spanwise vorticity, but not vice versa.

We note here that equation (3.7) has previously been considered by several authors for non-reacting flows. Pearson and Abernathy (1984), in the context of streamwise vortical structures found in turbulent boundary layers, constructed solutions which were valid for all Reynolds numbers. Corcos (1988), in the context of large scale structures found in mixing layers, has recently given an asymptotic solution in the limit of large Reynolds number. Because these authors used different notations and because these solutions are needed later for understanding certain aspects of ignition, we give below a summary of these solutions for completeness.

To examine the time evolution of the streamwise Oseen vortex in a shear flow, we define

$$u^I(r, \theta, t) = k_1 + k_2 [r \sin \theta + \hat{u}(r, \theta, t)], \quad (3.9)$$

where \hat{u} is the disturbed velocity component owing to the presence of the vortex. Upon substituting (3.9) into (3.7), \hat{u} is found to satisfy the convection-diffusion equation

$$\hat{u}_t + \frac{1}{r^2} [1 - \exp(-\text{Re} r^2/4t)] (r \cos \theta + \hat{u}_\theta) = \frac{1}{\text{Re}} \nabla^2 \hat{u}, \quad (3.10)$$

subject to homogeneous initial and boundary conditions. This equation was previously considered by Pearson and Abernathy (1984) (see their equation (14)), in the context of streamwise vortical structures found in turbulent boundary layers. They employed the similarity type variable $r^2/4t$ and defined (in our notation) $\hat{u} = \text{Real}(r F(r) e^{i\theta})$. This choice led to an equation for the complex function $F(r)$ which was solved numerically after special treatment of the regular singular point at the origin. A different approach for solving (3.10), which is perhaps more instructive, is to first transform using the similarity variable $\eta = r \sqrt{\text{Re}}/\sqrt{t}$ and then introducing the definition

$$\hat{u} = \frac{\sqrt{t}}{\sqrt{\text{Re}}} [u_e(\eta) \cos \theta + u_o(\eta) \sin \theta]; \quad (3.11)$$

this yields the coupled second-order differential equations,

$$\frac{1}{2} (u_e - \eta u_e') + \frac{\text{Re}}{\eta^2} [1 - \exp(-\eta^2/4)] (u_o + \eta) = u_e'' + \frac{1}{\eta} u_e' - \frac{1}{\eta^2} u_e, \quad (3.12a)$$

$$\frac{1}{2} (u_o - \eta u_o') - \frac{\text{Re}}{\eta^2} [1 - \exp(-\eta^2/4)] u_e = u_o'' + \frac{1}{\eta} u_o' - \frac{1}{\eta^2} u_o, \quad (3.12b)$$

subject to the boundary conditions,

$$u_e(0) = u_o(0) = u_e(\infty) = u_o(\infty) = 0. \quad (3.13)$$

Primes denote ordinary differentiation with respect to the similarity variable η , u_e is the amplitude of the even mode, and u_o is the amplitude of the odd mode. The system (3.12) depends only on the Reynolds number Re .

The coupled system (3.12) for the odd and even components subject to (3.13) represents the influence of the Oseen vortex on the streamwise velocity and is solved numerically using a 2nd-order finite difference scheme with an appropriate stretching in η . The solution to this system for a range of Reynolds numbers is given in Figure 2. As the Reynolds number increases, the number of oscillations in each of the components u_e and u_o increases while the region of oscillation moves away from the origin, thus establishing a core region. The solution difference $u_d = \eta \sin \theta + u_e \cos \theta + u_o \sin \theta$, where $u_d = \sqrt{Re}(u^I - k_1)/(k_2\sqrt{t})$, is plotted in Figure 3 for $\theta = \pm\pi/2$ and for various values of Re . From this figure the extent of the core region is seen to grow as Re increases, and this core, once established, grows like \sqrt{t} .

To investigate the solution described above for large times, let $t \rightarrow \infty$, so that $\eta \rightarrow 0$ for fixed r . Hence from (3.11) we have

$$\begin{aligned}\hat{u} &= \lim_{t \rightarrow \infty} \frac{\sqrt{t}}{\sqrt{Re}} [u_e(\eta) \cos \theta + u_o(\eta) \sin \theta] \\ &= \lim_{\eta \rightarrow 0} \frac{r}{\eta} [u_e(\eta) \cos \theta + u_o(\eta) \sin \theta] \\ &= \lim_{\eta \rightarrow 0} \frac{1}{\eta} [u_e(\eta)y + u_o(\eta)z] \\ &= a_1 y + b_1 z,\end{aligned}\tag{3.14}$$

where from (3.12) and (3.13) it is easy to show that the asymptotic behaviour as $\eta \rightarrow 0$ is

$$u_e = a_1 \eta + O(\eta^3), \quad u_o = b_1 \eta + O(\eta^3),\tag{3.15}$$

where a_1 and b_1 are found numerically and are functions of the Reynolds number Re . Substituting (3.14) into (3.9) yields

$$u^I = k_1 + k_2 [a_1 y + (1 + b_1)z].\tag{3.16}$$

Comparing (3.16) to the initial condition (3.8), the effect of the vortex is seen to be the establishment of a new equilibrium shear profile within the viscous core region. In addition, as $Re \rightarrow \infty$ the coefficients $a_1 \rightarrow 0$, $b_1 \rightarrow -1$, yielding $u^I \rightarrow k_1$; i.e., the streamwise velocity component becomes constant within the core at large vortex Reynolds numbers.

The streamwise Oseen vortex induces additional spanwise vorticity. This is seen by considering the total vorticity defined by $\underline{\omega} = \hat{e}_x \omega + \underline{\omega}'$, where ω is the streamwise vorticity component and $\underline{\omega}'$ is associated with the spanwise vorticity

$$\underline{\omega}' = \hat{e}_y \frac{\partial u}{\partial z} - \hat{e}_z \frac{\partial u}{\partial y}.\tag{3.17}$$

The magnitude of the spanwise vorticity, defined by $G = |\underline{\omega}'|$, is a function of Re and, at leading order, has the value

$$G_0 = |k_2| \left[a_1^2 + (1 + b_1)^2 \right]^{1/2}, \quad (3.18)$$

at the center of the core. Figure 4 is a plot of G_0 versus Re for $k_2 = 1$. Note that as $Re \rightarrow \infty$, $G_0 \rightarrow 0$ which implies that there are no gradients within the center of the core and thus the core is completely established. From this figure, the core is 95% established at $Re \approx 50$ which is in agreement with Figure 3 where a well defined core is clearly visible at $Re = 100$.

Even though the solution can be determined numerically for any Reynolds number, it is constructive to consider the limit as $Re \rightarrow \infty$. The leading-order solution in this limit is found by a direct asymptotic investigation of (3.7) subject to the initial and boundary conditions (3.8). In the limit $Re \rightarrow \infty$, an outer inviscid layer exists and is governed by the inviscid version of (3.7),

$$u_r^O + \frac{1}{r^2} u_\theta^O = 0, \quad (3.19)$$

where u^O denotes the streamwise velocity u^I in this outer layer. This equation is valid for $r = O(1)$ and $t \ll O(Re)$, so that the effect of a potential line vortex or an Oseen vortex on the streamwise velocity is the same. The solution found by the method of characteristics is

$$u^O = k_1 + k_2 r \sin \theta_0, \quad (3.20)$$

where θ_0 is the characteristic

$$\theta_0 = \theta - \frac{t}{r^2}. \quad (3.21)$$

As $r \rightarrow 0$, the solution (3.20) is singular indicating that the viscous terms in (3.7) must be retained. We introduce the similarity type variable

$$s = \frac{r}{\sqrt{\delta t}}, \quad (3.22)$$

where $Re^{-1} \ll \delta \ll 1$ and δ is a nondimensional parameter that will be chosen in the course of the analysis. Defining u^M to be the dependent variable u^I in the main layer, and letting

$$u^M = k_1 + k_2 \sqrt{\delta t} \tilde{u}(s, \theta), \quad (3.23)$$

we see that \tilde{u} satisfies the convection-diffusion equation

$$\frac{1}{2}(\tilde{u} - s \tilde{u}_s) + \frac{1}{\delta s^2} [1 - \exp(-Re \delta s^2/4)] \tilde{u}_\theta = \frac{1}{\delta Re} \nabla^2 \tilde{u}. \quad (3.24)$$

To facilitate matching with the outer inviscid solution (3.20), we change to a new (non-orthogonal) coordinate system in which the characteristic θ_0 is one of the coordinates. Thus, the above equation in terms of s and θ_0 becomes

$$\begin{aligned} \frac{1}{2}(\bar{u} - s \bar{u}_s) - \frac{1}{\delta s^2} \exp(-\text{Re} \delta s^2/4) \bar{u}_{\theta_0} \\ = \frac{1}{\delta \text{Re}} \left\{ \left[\frac{\partial}{\partial s} + \frac{2}{\delta s^3} \frac{\partial}{\partial \theta_0} \right]^2 + \frac{1}{s} \left[\frac{\partial}{\partial s} + \frac{2}{\delta s^3} \frac{\partial}{\partial \theta_0} \right] + \frac{1}{s^2} \frac{\partial^2}{\partial \theta_0^2} \right\} (\bar{u}). \end{aligned} \quad (3.25)$$

Balancing the viscous terms with the convection terms necessitates the choice

$$1 = \frac{1}{\delta \text{Re}} \frac{4}{\delta^2}, \quad (3.26)$$

or, in terms of δ ,

$$\delta = (4/\text{Re})^{1/3} = O(v^{1/3}), \quad (3.27)$$

which is in agreement with Corcos (1988). This layer is thicker than the inner diffusion layer of the vortex which is of the order $v^{1/2}$. For this scaling, $\exp(-\text{Re} \delta s^2/4)$ is exponentially small in the distinguished limit $\text{Re} \gg 1$, and so again the effect of a potential line vortex or an Oseen vortex is the same. In order to account for the diffusion of the vortex, an inner layer must be constructed. This is not necessary, as will be shown below, since u^M is not singular at the origin. The leading order equation in a δ -expansion is given by

$$\frac{1}{2}(\bar{u} - s \bar{u}_s) = \frac{1}{s^6} \bar{u}_{\theta_0 \theta_0}, \quad (3.28)$$

which is solved by separation of variables and matched with the outer solution (3.20) to get

$$\bar{u} = s \exp \left[\frac{-1}{3 s^6} \right] \sin \theta_0. \quad (3.29)$$

The solution in the main layer is now given by

$$u^M = k_1 + k_2 s \sqrt{\delta t} \exp \left[\frac{-1}{3 s^6} \right] \sin \theta_0. \quad (3.30)$$

The composite solution, valid in both the outer and main layers, is given by

$$u^C = k_1 + k_2 r \exp \left[\frac{-(\delta t)^3}{3 r^6} \right] \sin \left[\theta - \frac{t}{r^2} \right]. \quad (3.31)$$

To compare the asymptotic solution u^C given in (3.31) to the exact solution u^I given in (3.9), a plot of the solution difference u_d versus η for $\theta = \pm\pi/2$ with $\text{Re} = 10,000$ is shown in Figure 5, where u_d and η are defined as before. From this figure we see that the asymptotic solution is in good quantitative agreement with the exact solution shown in Figure 3c.

The magnitude of the spanwise vorticity at $O(1)$ obtained by substituting (3.31) into the definition of G and then letting $\delta \rightarrow 0$, yields

$$G_0 = \frac{2|k_2|}{\delta s^2} \exp \left[\frac{-1}{3s^6} \right] \left| \cos \left(\theta - \frac{1}{\delta s^2} \right) \right|. \quad (3.32)$$

Figure 6 is a plot of G_0 versus s for $\theta = \pi/2$, $k_2 = 1$, and $\delta = 1/5$. The limit $\text{Re} \rightarrow 0$ corresponds to $G_0 \rightarrow 0$, and so the large spikes have been created by the vortex.

With g^I , h^I and u^I now known, the following equations can be solved for T_1 and F_j^I

$$T_{1,t} + \frac{h^I}{r} T_{1,\theta} = \frac{1}{\text{Re} Pr} \nabla^2 T_1 + (\gamma - 1) M_o^2 [P_t^I + \frac{1}{\text{Re}} \Phi^I] + \tau F_1^I F_2^I e^{T_1}, \quad (3.33)$$

$$F_{j,t}^I + \frac{h^I}{r} F_{j,\theta}^I = \frac{1}{\text{Re} Sc} \nabla^2 F_j^I, \quad j = 1, 2. \quad (3.34)$$

Note that the right hand side of the equation for the temperature is the sum of three terms: the diffusion term, the term due to compressible effects, and the reaction term, respectively. The appropriate boundary and initial conditions are given by

$$T_1 = 0, F_1^I = 1, F_2^I = 0 \quad \text{at } t = 0, r > 0, 0 < \theta < \pi, \quad \text{and } t > 0, r \rightarrow \infty, 0 < \theta < \pi, \quad (3.35a)$$

$$T_1 = \beta_T, F_1^I = 0, F_2^I = \phi^{-1} \quad \text{at } t = 0, r > 0, \pi < \theta < 2\pi, \quad \text{and } t > 0, r \rightarrow \infty, \pi < \theta < 2\pi, \quad (3.35b)$$

where ϕ is the equivalence ratio defined as the ratio of the initial mass fraction of the fuel $F_{1,\infty}$ to the initial mass fraction of the oxidizer $F_{2,\infty}$, and β_T is the parameter which allows for small initial temperature differences across the interface. If $\phi = 1$, the mixture is said to be stoichiometric; if $\phi > 1$ it is fuel rich; and if $\phi < 1$, it is fuel lean. Also, if β_T is less than zero, the oxidizer (species 2) is relatively cold compared to the fuel (species 1); and if β_T is greater than zero, it is relatively hot. As t increases, the solution for T_1 becomes unbounded at some finite time (t_{ig}) and location (y_{ig}, z_{ig}). This characterizes the ignition regime. Finally, with T_1 determined, the density perturbation ρ_1 can be found from (3.3a).

The case $M_o = 0$ was discussed in the Introduction. Thus, the goal is to examine the influence of the compressible term in (3.33) on ignition. However, it is instructive to first investigate its influence on the temperature field in the absence of chemistry. We do this in the next section. The following section then contains numerical results when chemistry is included.

3.1. Nonreacting Case

In this section we investigate the influence of the compressible term in (3.33) on the temperature field in the absence of chemistry. Since an exact solution of (3.33) with $\tau = 0$ is not possible, we shall examine the equation in the limit $Re \gg 1$. In this limit an outer inviscid layer exists and is governed by the inviscid version of (3.33) for the outer variable T_1^O . Transforming to the (r, θ_0, t) characteristic coordinate system, where θ_0 is given in (3.21), the temperature equation (3.33) becomes to leading order

$$T_{1,t}^O = \frac{1}{RePr} \left\{ \left[\frac{\partial}{\partial r} + \frac{2t}{r^3} \frac{\partial}{\partial \theta_0} \right]^2 + \frac{1}{r} \left[\frac{\partial}{\partial r} + \frac{2t}{r^3} \frac{\partial}{\partial \theta_0} \right] + \frac{1}{r^2} \frac{\partial^2}{\partial \theta_0^2} \right\} (T_1^O) \\ + \frac{\gamma-1}{Re} M_o^2 \left[\frac{4}{r^4} + k_2^2 \left\{ \left[\tilde{u}_r + \frac{2t}{r^3} \tilde{u}_{\theta_0} \right]^2 + \frac{1}{r^2} \tilde{u}_{\theta_0}^2 \right\} \right] + O(Re^{-2}), \quad (3.36)$$

where $\tilde{u} = r \sin \theta_0$ and we have made use of the leading order outer solutions $h^I = 1/r + est$ and $P^I = -1/(2r^2) + est$, where est means exponentially small terms in Re , valid for $t \ll O(Re)$. The leading order solution in a large Reynolds number expansion can be shown to be

$$T_1^O = \frac{\gamma-1}{Re} M_o^2 \left\{ \frac{4t}{r^4} + k_2^2 \left[t + \frac{t^2}{r^2} \sin(2\theta_0) + \frac{4t^3}{3r^4} \cos^2 \theta_0 \right] \right\} + O(Re^{-2}). \quad (3.37)$$

Note that the terms in the brackets are associated with the streamwise vortex and with the spanwise vorticity. In the absence of the spanwise vorticity (i.e., $k_2 = 0$), the first term is positive showing that the effect of compressibility is to heat the outer region of the viscous core. With T_1^O known, the density in the outer layer can be determined from (3.3a).

As $r \rightarrow 0$, the solution (3.37) becomes singular so that the viscous terms in (3.33) must be retained. Transforming to the (s, θ_0, t) coordinate system, where s is defined in (3.22) and $\theta_0 = \theta - 1/\delta s^2$, the temperature equation (3.33) in the main layer becomes

$$T_{1,t}^M - \frac{s}{2t} T_{1,s}^M = \frac{1}{\delta RePr t} \left\{ \left[\frac{\partial}{\partial s} + \frac{2}{\delta s^3} \frac{\partial}{\partial \theta_0} \right]^2 + \frac{1}{s} \left[\frac{\partial}{\partial s} + \frac{2}{\delta s^3} \frac{\partial}{\partial \theta_0} \right] + \frac{1}{s^2} \frac{\partial^2}{\partial \theta_0^2} \right\} (T_1^M) \\ + \frac{\gamma-1}{Re} M_o^2 \left[\frac{4}{\delta^2 t^2 s^4} + k_2^2 \left\{ \left[\tilde{u}_s + \frac{2}{\delta s^3} \tilde{u}_{\theta_0} \right]^2 + \frac{1}{s^2} \tilde{u}_{\theta_0}^2 \right\} \right], \quad (3.38)$$

where, to leading order in δ ,

$$\tilde{u} = s \exp \left[\frac{-1}{3s^6} \right] \sin \theta_0 + O(\delta). \quad (3.39)$$

To determine the proper expansion in the main layer and the appropriate matching condition as $s \rightarrow \infty$, we first expand the outer solution (3.37) as $r \rightarrow 0$, yielding

$$T_1^O \approx (\gamma-1) M_o^2 \left\{ \frac{\delta}{t s^4} \left[1 + \frac{k_2^2 t^2}{3} \cos^2 \theta_0 \right] + \frac{\delta^2 k_2^2 t}{4 s^2} \sin(2\theta_0) + \frac{\delta^3 k_2^2 t}{4} \right\} + \dots \quad (3.40)$$

We now expand T_1^M as

$$T_1^M = \delta f_1 + \delta^2 f_2 + \dots, \quad (3.41)$$

as $\delta \rightarrow 0$. Substituting the above expansion into (3.38) gives the following problem at leading order:

$$f_{1,t} - \frac{s}{2t} f_{1,s} = \frac{1}{Pr t s^6} f_{1\theta_0\theta_0} + (\gamma - 1) M_o^2 \left\{ \frac{1}{t^2 s^4} + \frac{k_2^2}{s^4} \exp \left[\frac{-2}{3 s^6} \right] \cos^2 \theta_0 \right\}. \quad (3.42)$$

The appropriate solution that matches with the outer solution (3.40) can be verified to be

$$f_1 = \frac{(\gamma - 1) M_o^2}{t s^4} + \frac{\gamma - 1}{4} M_o^2 k_2^2 t f_{11}(s, \theta_0), \quad (3.43a)$$

$$f_{11} = s^2 \left\{ 1 - \exp \left[\frac{-2}{3 s^6} \right] + \frac{Pr}{(2 - Pr)} \left\{ \exp \left[\frac{-2}{3 s^6} \right] - \exp \left[\frac{-4}{3 Pr s^6} \right] \right\} \cos(2\theta_0) \right\}, \quad (3.43b)$$

which decays as $s \rightarrow \infty$. The first term of f_1 is associated with the streamwise vortex while f_{11} is associated with the spanwise vorticity. As mentioned above, the leading order term f_1 is positive showing that the effect of compressibility is to heat the outer region of the viscous core. Since we are primarily interested in the influence of the spanwise vorticity, we plot in Figure 7 a graph of f_{11} as a function of s for $Pr = 1$, $\theta = \pi/2$, and (a) $\delta = 1/5$ and (b) $\delta = 1/8$. Note that the graph decays exponentially as $s \rightarrow \infty$, quadratically as $s \rightarrow 0$, and is positive and oscillates for $s \approx O(1)$. Also, the number of oscillations increases as δ decreases but stays within some temperature envelope. Thus the effect of the streamwise vortex is to introduce positive temperature fluctuations in the main layer which are damped out in the inner viscous layer. This result will have important implications in the ignition regime when chemistry is included, and will be brought out in the next section. The density can now be determined from (3.3a), and is given by

$$\rho_1^M = -\frac{\gamma M_o^2}{2 s^2 t \delta} - \delta f_1 + \dots \quad (3.44)$$

As $s \rightarrow 0$, T_1^M and ρ_1^M become singular suggesting that an inner viscous layer is present. To determine the proper scalings, we see from the expansion (3.44) for the density that the second order term is of the same order as the leading order term when $s \rightarrow 0$, yielding the balance $s = O(\text{Re}^{-1/3})$. This suggests the new variable for the inner layer

$$r = \frac{\xi}{\sqrt{\text{Re}}}, \quad (3.45)$$

which is the size of the viscous core. Expanding the temperature and density in the main layer in terms of the inner variable and taking the limit $\text{Re} \rightarrow \infty$, the proper expansion for the inner variables are

$$T_1^I = \text{Re} \hat{T}, \quad \rho_1^I = \text{Re} \hat{\rho}, \quad (3.46)$$

where the superscript indicates variables in the inner layer. The leading order equations in a Reynolds number expansion are given by

$$\hat{p} + \hat{T} = \gamma M_o^2 \hat{P} \quad (3.47a)$$

$$\hat{T}_t - (\gamma - 1) M_o^2 \hat{P}_{0,t} = \frac{1}{Pr} \left(\hat{T}_{\xi\xi} + \frac{\hat{T}_\xi}{\xi} \right) + (\gamma - 1) M_o^2 \left(\hat{h}_{0,\xi} - \frac{\hat{h}_0}{\xi} \right)^2, \quad (3.47b)$$

where

$$h_0 = \text{Re}^{1/2} \hat{h}_0(\xi, t), \quad P_0 = \text{Re} \hat{P}_0(\xi, t); \quad (3.48)$$

\hat{h}_0 and \hat{P}_0 can be found from (3.5) and (3.6). This system is axisymmetric and is to be solved subject to appropriate matching conditions as $\xi \rightarrow \infty$. We do not solve this system here, but rather note that the variables are bounded at the origin. Furthermore, this system is equivalent to that considered by Colonius et al. (1991) if we rewrite their system in our notation, and so we refer the interested reader to that paper for further details.

3.2. Reacting Case

When chemical effects are included, the system (3.33)-(3.34) with boundary conditions (3.35) describes the ignition regime which must be solved numerically. The numerical scheme utilized here is described in Macaraeg et al. (1992). A small nonzero initial time is assumed in order to avoid nonphysical initial transients which may lead to early ignition. For the cases which follow, k_1 is assumed to be zero, so that the imposed shear is symmetric about the origin. Emphasis will be placed on the effects of the shear strength parameter k_2 , so the other parameters will be held fixed. Here, we set $\beta_T = 0$ and $\phi = Pr = 1$.

We begin the numerical computations by first setting $\tau = 0$ in (3.33). This allows a qualitative comparison between the numerically generated solution and the asymptotic solution derived in the previous section. To this end, recall that the asymptotic solution indicates that the introduction of streamwise shear gives rise to oscillations in the velocity field as well as the temperature field via the dissipation function. Shown in Figure 8 are contour plots and cross-section cuts of T_1 and TU for $\text{Re} = 50$, $k_2 = 1$ and $M_o = 0.7$. The quantity TU is computed by subtracting the numerical solution corresponding to $M_o = 0$ from T_1 . Thus, TU is proportional to f_{11} of the previous section and highlights the underlying oscillating temperature field. The cross-section plots of T_1 and TU versus z , taken through the vortex center, show that the overall temperature perturbation has a single temperature peak in the center, whereas the temperature due to spanwise vorticity has multiple peaks, even though their magnitude is small at this low shear strength. If the strength of the shear is increased, the magnitude of these oscillations increases by k_2^2 , as can be seen in Figure 9 which displays plots of TU for three values of the shear strength parameter k_2 . This trend was predicted earlier by the outer asymptotic solution obtained in (3.43), which indicates a proportionality with k_2^2 . Also given are the corresponding cross-sections of the streamwise velocity component. Note that the magnitude and number of oscillations increases with increasing shear, again consistent with the asymptotic solution derived in the previous section. Figure 10 depicts contours and cross-sections of T_1 for the same conditions of Figure 9. Note that the temperature perturbation, T_1 , becomes dominated by the spanwise vorticity for high values of shear.

The multiple temperature peaks appearing for high shear values can have a dramatic effect on ignition when chemistry is added. To illustrate this we show in Figure 11 contours and cross-section plots of the temperature perturbation for $Re = 10$, $M_o = 0.316$ and two values of the shear strength parameter k_2 . For $k_2 = 1$, there is a single hot spot located in the vortex center, while for high shear ($k_2 = 20$) there are two ignition points, located in the main layer of the viscous core. The evolution in time of this double ignition point is shown in Figure 12. Note that the temperature perturbation is strongly sheared, which gives rise to multiple ignition points at a later time.

The influence of the streamwise shear on the ignition time is shown in Figure 13, where the maximum temperature perturbation over the entire spatial domain is plotted against time. We note here that for weak shear ($k_2 = 1$), the ignition time is comparable to that obtained by Linan and Crespo (1976) in which diffusion is the only mechanism present for mixing. Also, the ignition location is at the center of the vortex, consistent with previous results (Macaraeg et al., 1992). As the strength of the shear increases, the ignition time decreases indicating that mixing is enhanced owing to the presence of streamwise shear. In addition, the ignition location no longer resides in the viscous core, but now multiple ignition points occur and are located in the outer region of the core. This phenomena is due to the large temperature perturbations induced by the interaction process between the streamwise and spanwise vorticity described in the previous section.

4. CONCLUSIONS

The problem of a flame interacting with a vortex is assumed to model certain fundamental mechanisms of turbulent diffusion flames which form the basis of many propulsion devices. Streamwise shear, which can be present due to large scale structures within the flow field or can be introduced as a mixing enhancement technique, is always present in these combustion systems, so that it is important to study the role of shear in such flame/vortex interactions. An unexplored fundamental problem of turbulent reacting flows is thus the evolution of a shear flow in the presence of streamwise vortices, or conversely, the dynamics of vortices stretched by shear flow. This problem is examined by means of asymptotic analysis and numerical simulation in the limit of small Mach number. An idealized model is employed to describe the interaction process which, among other assumptions, neglects spatial variations in the streamwise direction. The model then consists of a one-step, irreversible Arrhenius reaction between initially unmixed species occupying adjacent half-planes which are then allowed to mix and react in the presence of a streamwise vortex embedded in a shear flow.

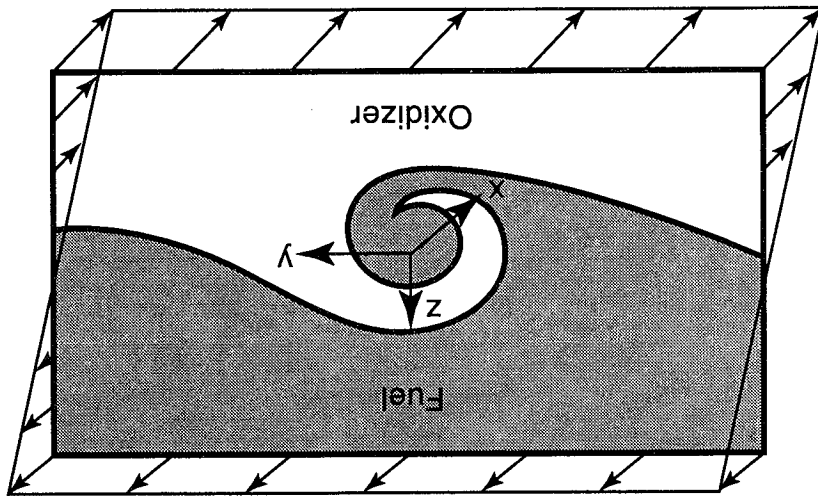
It is shown that the effect of shear is to give rise to oscillations in the velocity field, which produces localized regions of high temperature gradients via viscous heating. As the strength of the shear is increased, these high temperature gradients give rise to multiple ignition points while substantially decreasing the overall ignition times. This results in the enhancement of mixing brought about by the linear shear associated with the spanwise vorticity.

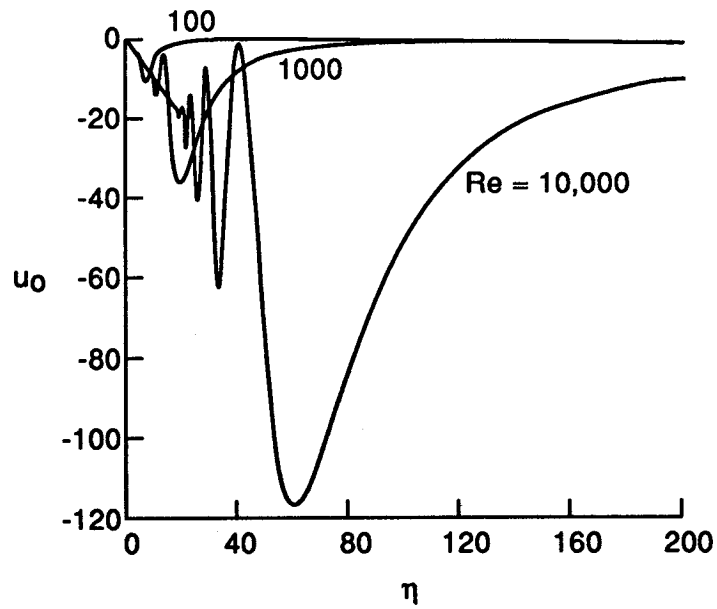
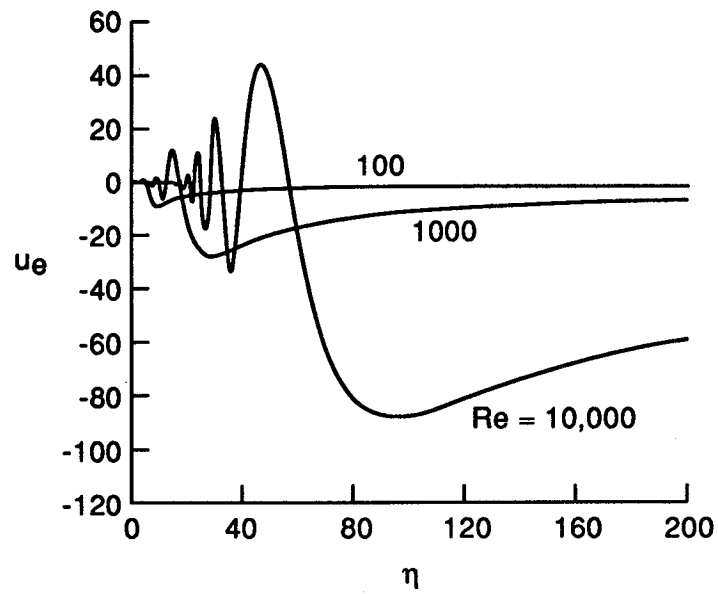
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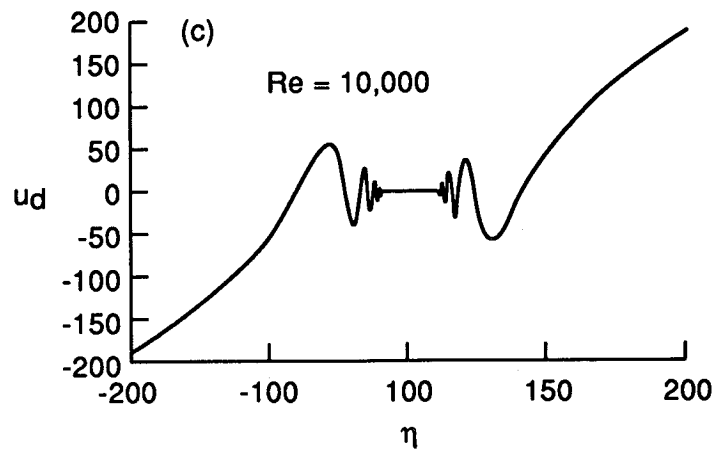
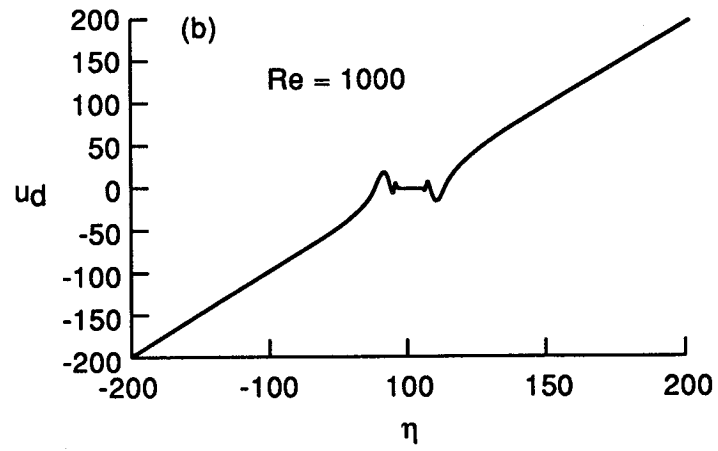
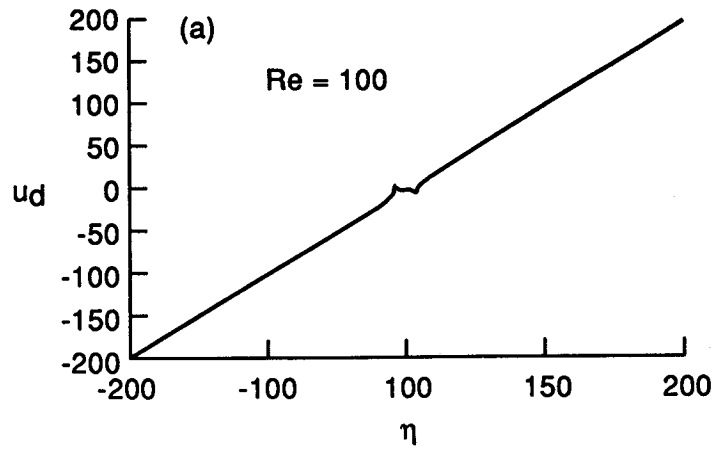
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1. Schematic of reactants present in a vortex field with shear.

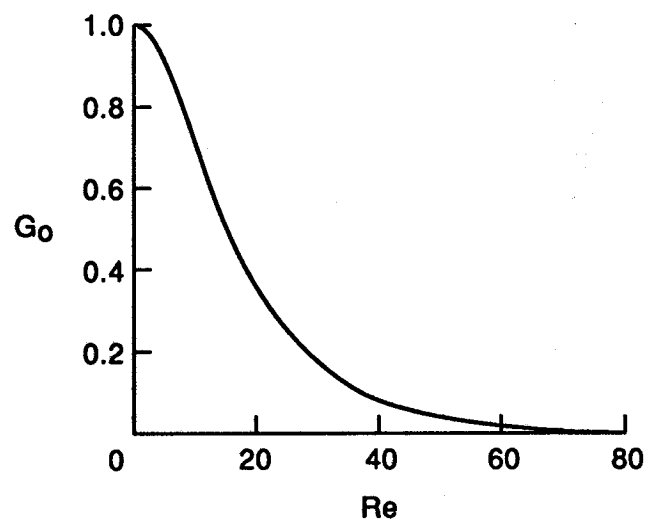




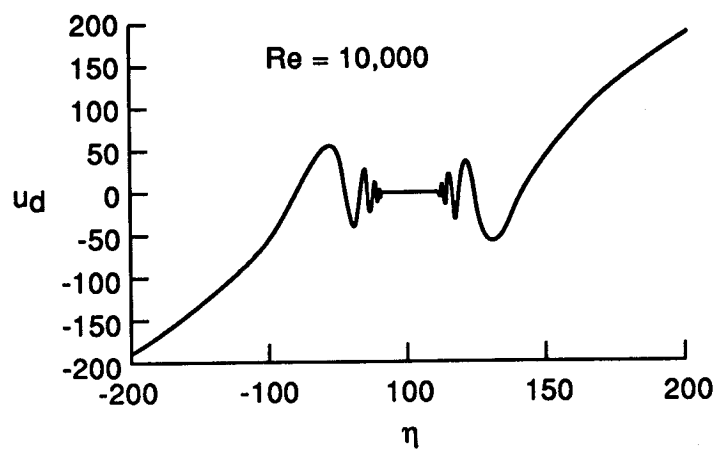
2. Plot of (a) u_e versus η for various values of the Reynolds number Re .



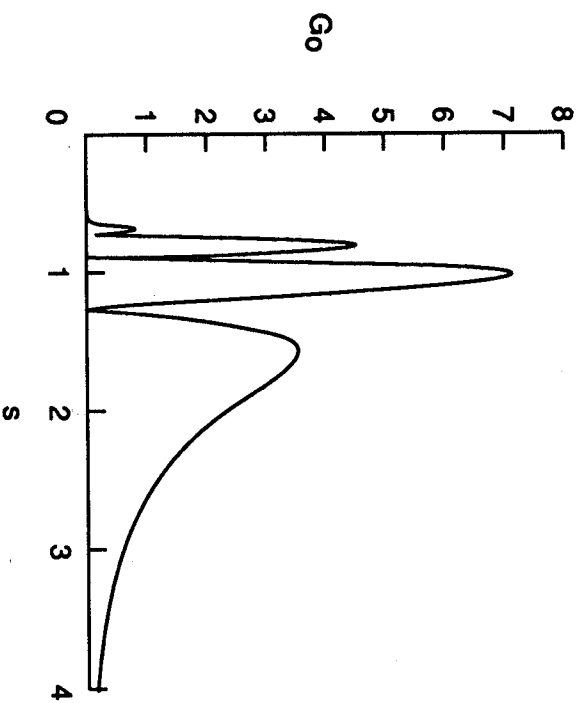
3. Plot of the solution difference u_d versus η for $\Theta = \pm\pi/2$ and various values of the Reynolds number Re .



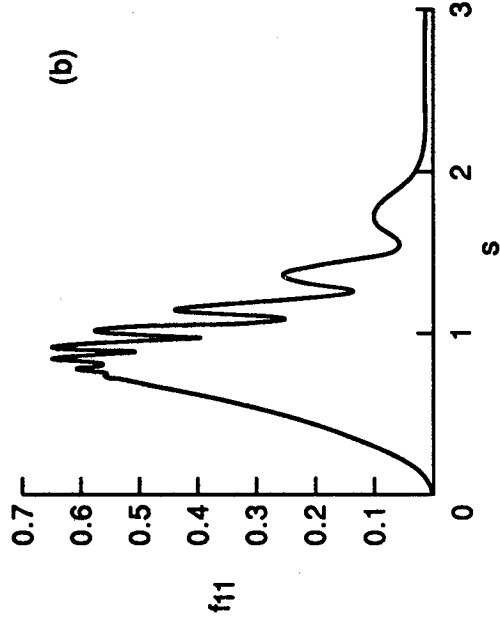
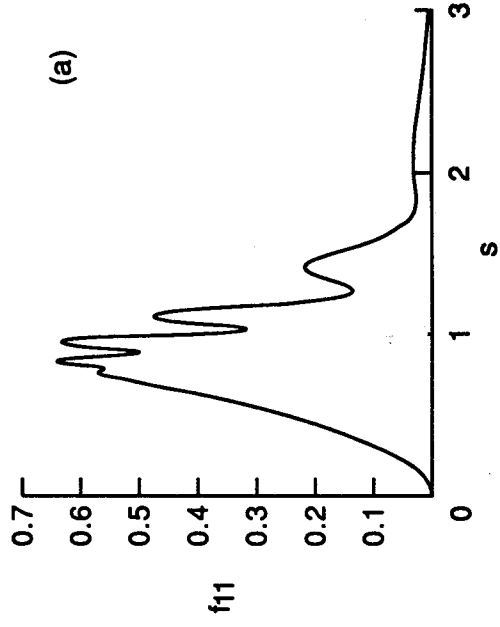
4. Plot of G_0 versus the Reynolds number Re for $k_2 = 1$.



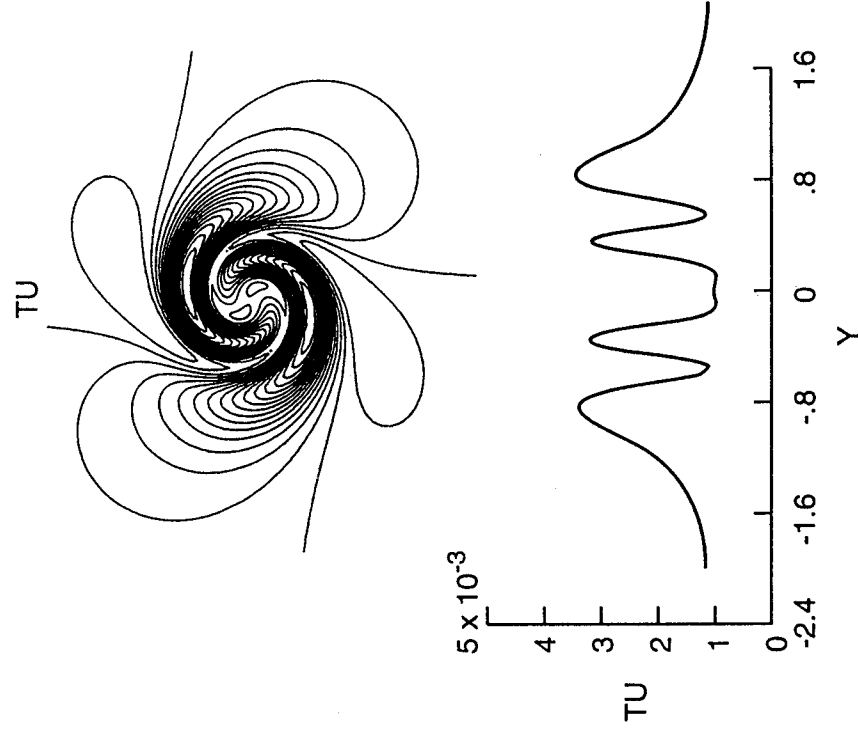
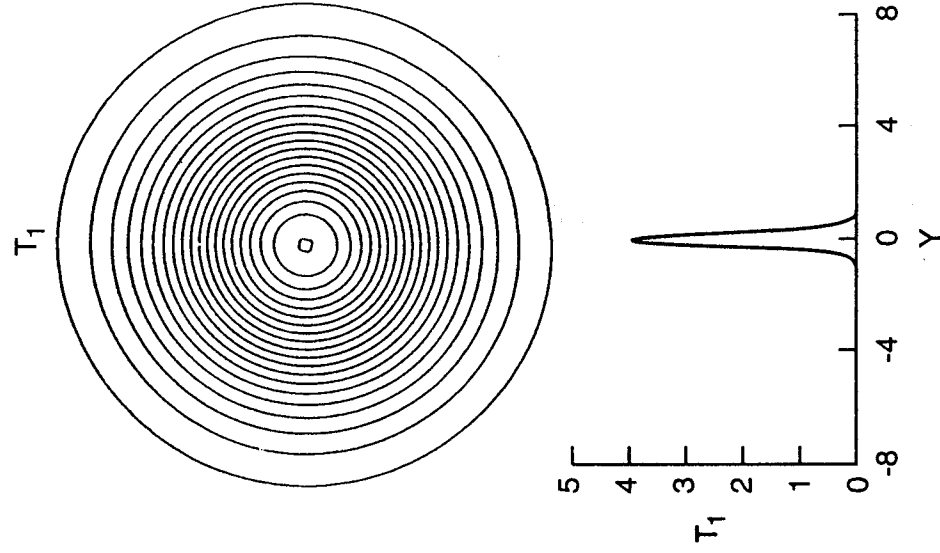
5. Plot of the solution difference u_d versus η for $\Theta = \pm\pi/2$ and $\text{Re} = 10,000$.



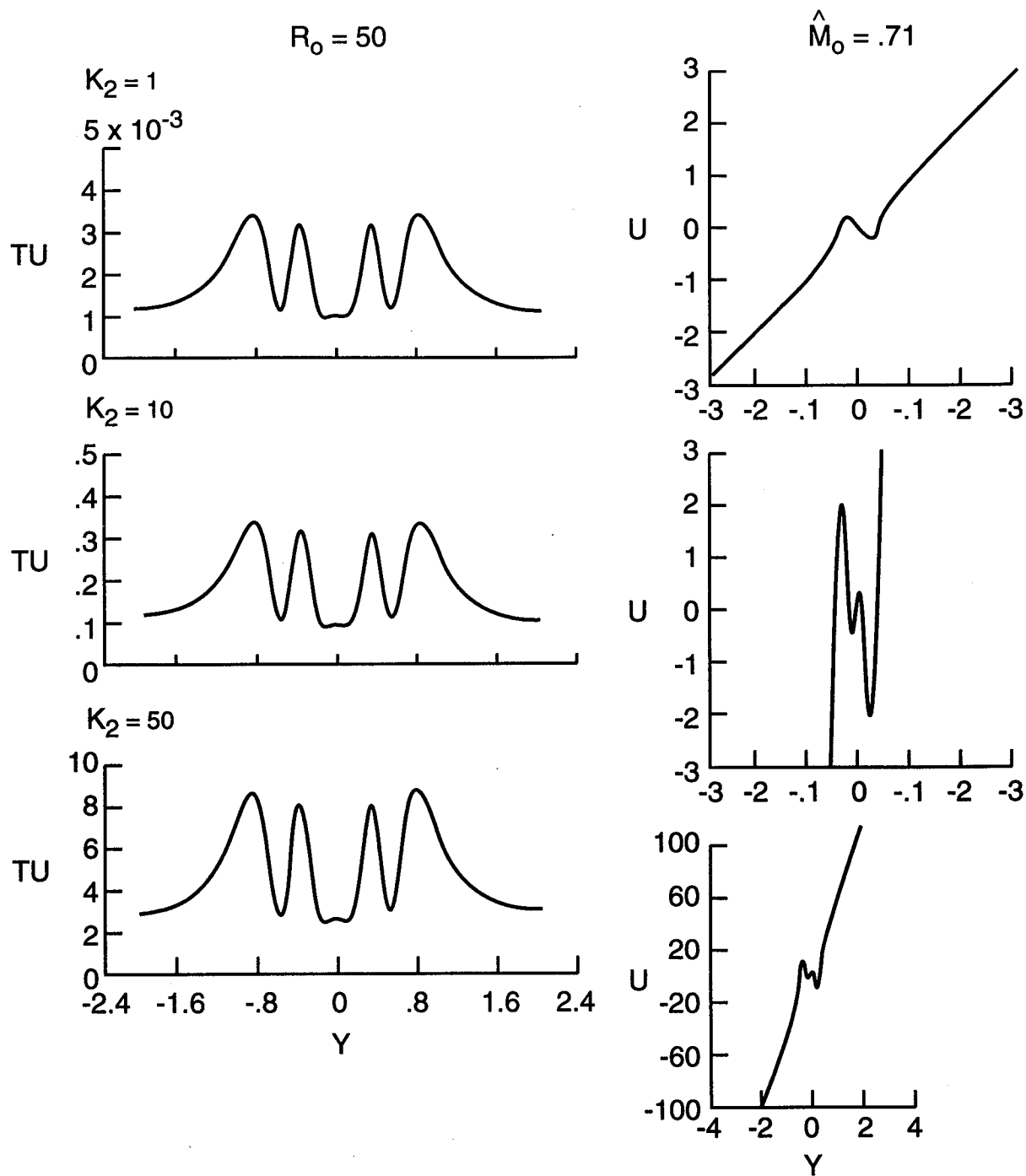
6. Plot of G_0 versus s for $\Theta = \pi/2$, $k_2 = 1$ and $\delta = 1/5$.



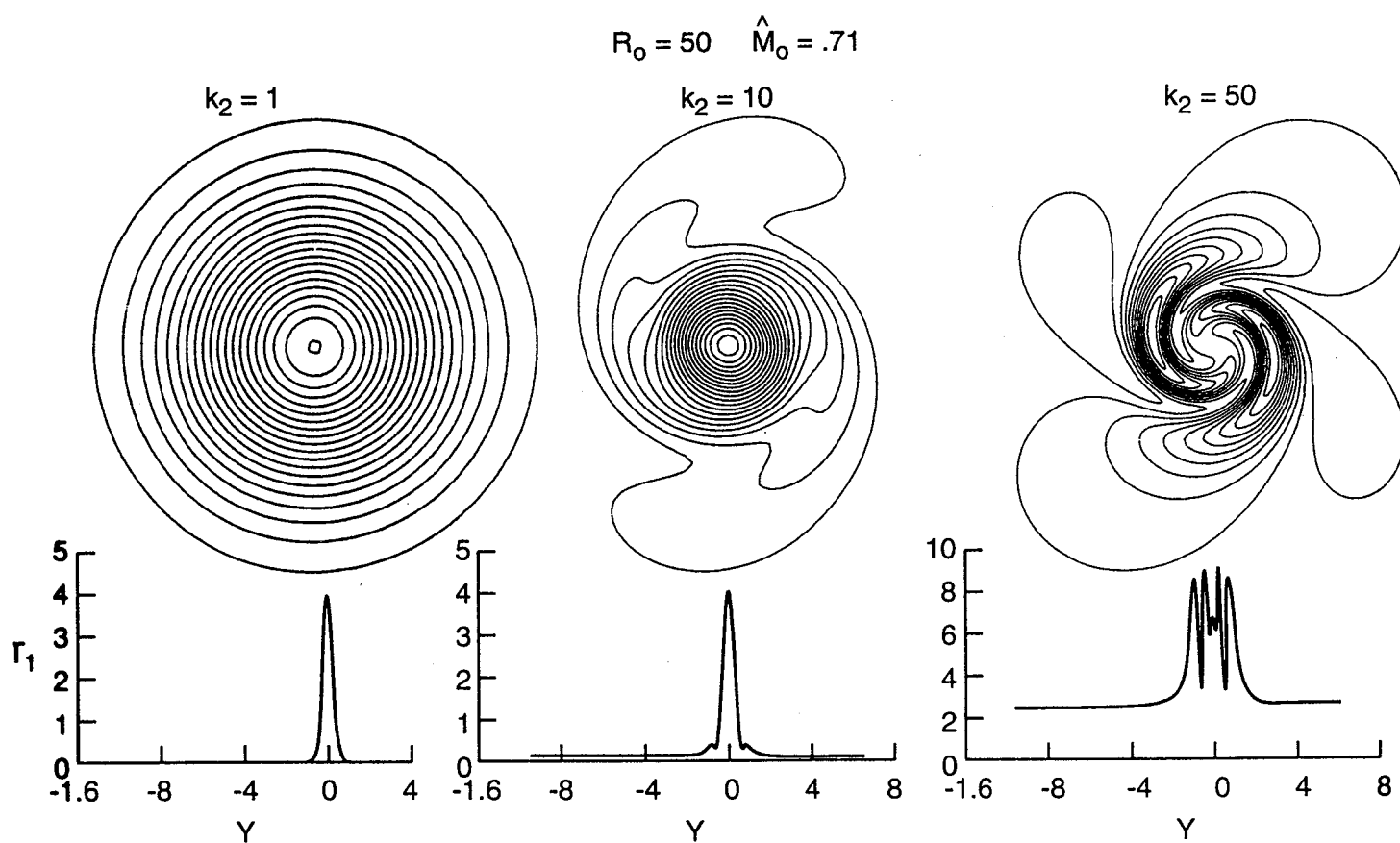
7. Plot of f_{11} as a function of s with $Pr = 1$, $\Theta = \pi/2$ and for (a) $\delta = 1/5$ and $\delta = 1/8$.



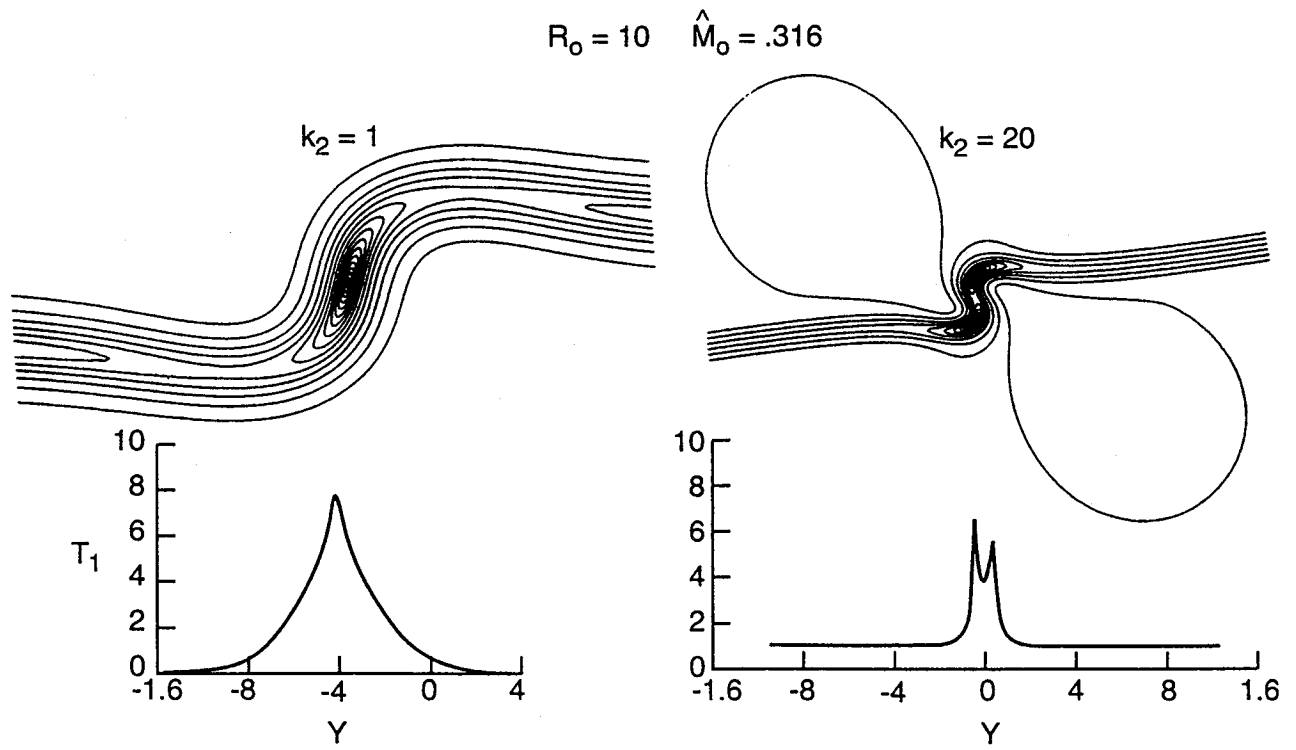
8. Contours and associated vertical cuts at the vortex center of the temperature perturbation (T_1) and the temperature perturbation associated with the spanwise vortex (TU). (No chemistry) $Re = 50$, $k_2 = 1$, $M_0 = 0.71$.



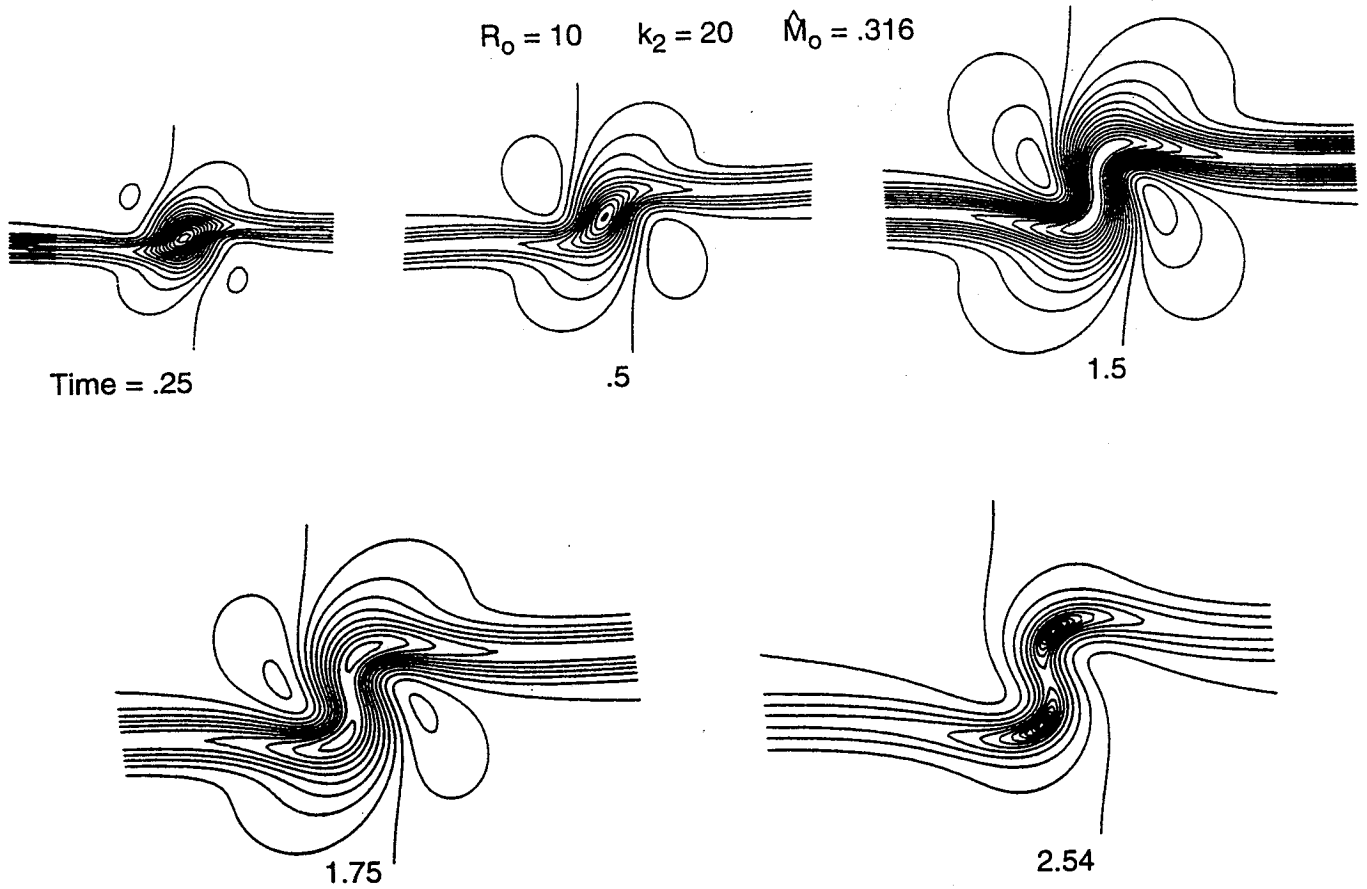
9. Vertical cuts at the vortex center of temperature perturbation due to the spanwise vorticity (TU) and streamwise velocity (U), for varying shear strengths. (No chemistry) $Re = 50$, $M_0 = 0.71$.



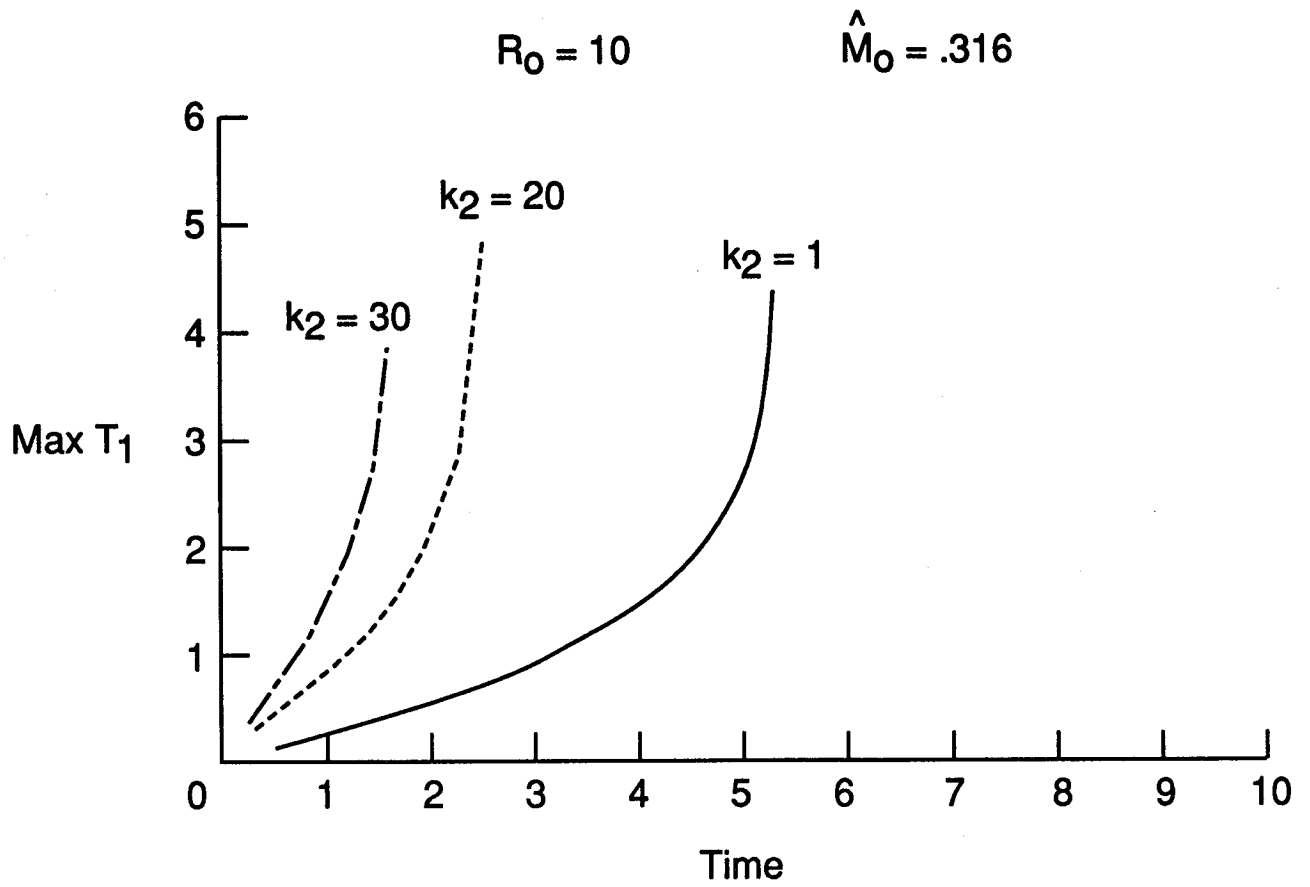
10. Contours and vertical cuts at the vortex center of the temperature perturbation (T_1) for increasing shear strengths. (No chemistry) $T_1 = 50$, $M_0 = 0.71$.



11. Contours and vertical cuts of the temperature perturbation (T_1) at ignition for increasing values of shear. $Re = 10$, $M_0 = 0.316$.



12. Contours of the temperature perturbation (T_1) evolution from early time to ignition.
 $Re = 10$, $M_0 = 0.316$, $k_2 = 20$.



13. Plot of the maximum temperature perturbation (T_1) versus time for various shear strengths. $Re = 10$, $M_0 = 0.316$.

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13. ABSTRACT (Maximum 200 words) The role of streamwise-spanwise vorticity interactions that occur in turbulent shear flows on flame/vortex interactions is examined by means of asymptotic analysis and numerical simulation in the limit of small Mach number. An idealized model is employed to describe the interaction process. The model consists of a one-step, irreversible Arrhenius reaction between initially unmixed species occupying adjacent half-planes which are then allowed to mix and react in the presence of a streamwise vortex embedded in a shear flow. It is found that the interaction of the streamwise vortex with shear gives rise to small-scale velocity oscillations which increase in magnitude with shear strength. These oscillations give rise to regions of strong temperature gradients via viscous heating, which can lead to multiple ignition points and substantially decrease ignition times. The evolution in time of the temperature and mass-fraction fields is followed, and emphasis is placed on the ignition time and structure as a function of vortex and shear strength.				
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