



Incorporation of Condensation Heat Transfer in a Flow Network Code

Miranda Anthony & Alok Majumdar NASA/Marshall Space Flight Center Huntsville, Alabama



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Introduction



- Pure water is distilled from waste water in International Space Station
- Distillation assembly consists of evaporator, compressor and condenser
- Vapor is periodically purged from the condenser to avoid vapor accumulation
- Purged vapor is condensed in a tube by coolant water prior to entering purge pump
- The paper presents a condensation model of purged vapor in a tube







Inner Tube Diameter = 0.125 inch Outer Tube Diameter = 1 inch Length = 4 inches Material is Titanium

Calculate the Quality and Heat Transfer Properties of the Water as it Condenses in the Pipe

Model consists of 2 Boundary Nodes and 28 Internal Nodes and Models Conduction through the Tube Wall





Generalized Fluid System Simulation Program







GFSSP Finite Volume Method

- Finite Volume Method is based on conservation principle of Thermo-Fluid Dynamics
- In Classical Thermodynamics we analyze a single control volume
- In Finite Volume Method, flow domain is discretized into multiple control volumes and a <u>simultaneous</u> analysis is performed
- Finite Volume Method can be classified into two categories:
 - Navier-Stokes Solution (Commonly known as CFD)
 - Network Flow Solution (NFS)





GFSSP Finite Volume Method





Network Flow Solution (NFS)

Navier-Stokes Solution (CFD)





GFSSP Process Flow Diagram

Solver & Property









GFSSP Solution Scheme

SASS : Simultaneous Adjustment with Successive Substitution

Approach : Solve simultaneously when equations are strongly coupled and non-linear

Advantage : Superior convergence characteristics with affordable computer memory





Condensation Heat Transfer







Heat transfer correlations



Akers, et al, 1959 – Annular Correlation Boyko and Kruzhulin, 1967 – Annular Correlation Chato, 1962 – Stratified Correlation Soliman, et al, 1968 – Generalized Correlation

Chose Soliman correlation for its stability and generality



Annular Condensation



Stratified Condensation



Soliman Correlation for Heat Transfer Coefficient for Annular Flow Condensation

$$h = 0.036 \operatorname{Pr}^{0.65} F_0^{0.5} \left[\frac{k_l \rho_l^{0.5}}{\mu_l} \right]$$

 $F_0 = F_f + F_m \pm F_a$

$$F_{f} = 0.045 \operatorname{Re}_{T}^{-0.2} \left[\frac{\pi^{2} \rho_{\nu} D^{4}}{8W_{T}^{2}} \right] \left[x^{1.8} + 5.70 \left(\frac{\mu_{l}}{\mu_{\nu}} \right)^{0.0523} (1-x)^{0.470} x^{1.33} \left(\frac{\rho_{\nu}}{\rho_{l}} \right)^{0.261} + 8.11 \left(\frac{\mu_{l}}{\mu_{\nu}} \right)^{0.105} (1-x)^{0.940} x^{.860} \left(\frac{\rho_{\nu}}{\rho_{l}} \right)^{0.522} \right]$$

$$F_{m} = 0.5 \left(D \frac{dx}{dz} \right) \left[\frac{\pi^{2} \rho_{\nu} D^{4}}{8W_{T}^{2}} \right] \left[2 \left(1-x \right) \left(\frac{\rho_{\nu}}{\rho_{l}} \right)^{2/3} + \left(\frac{1}{x} - 3 + 2x \right) \left(\frac{\rho_{\nu}}{\rho_{l}} \right)^{4/3} + \left(2x - 1 + \beta x \right) \left(\frac{\rho_{\nu}}{\rho_{l}} \right)^{1/3} + \left(2\beta - \frac{\beta}{x} - \beta x \right) \left(\frac{\rho_{\nu}}{\rho_{l}} \right)^{5/3} + 2 \left(1 - x - \beta + \beta x \right) \left(\frac{\rho_{\nu}}{\rho_{l}} \right) \right]$$

$$F = 0$$

F_f: Effect of two-phase friction

F_m: Effect of momentum changes in the flow

F_a: Effect of axial gravitational field on the wall shear stress





Solid-to-fluid heat transfer













Quality Comparison for Different Tube Grid Resolution (Soliman Correlation)







Outer Wall Temperature Comparison for Different Tube Grid Resolution (Soliman Correlation)





Conclusions



- A condensation heat transfer model was successfully incorporated in a general purpose flow network code
- The numerical model considers solid-to-fluid heat transfer
- Soliman et al's correlation of condensation heat transfer is recommended due to its generality and stability





References & Acknowledgements

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Acknowledgement:

Authors would like to acknowledge Mr. Bruce Tiller and Mr. Richard Schunk of MSFC for their suggestions and comments