

Rotating Reverse Osmosis for Wastewater Reuse

Richard M. Lueptow*, Yeomin Yoon, Cynthia Pederson

Department of Mechanical Engineering, Northwestern University, 2145 Sheridan Road,
Evanston, IL, 60208, USA

*Email: r-lueptow@northwestern.edu, Telephone: 1-847-491-4265, Fax: 1-847-491-3915

Background: Reverse osmosis (RO) has long been in use as a physical membrane separation technology, and it may be useful for wastewater reuse for long-term space missions. However, concentration polarization decreases the flux of solvent through the membrane and the rejection of contaminants as a result of an increase in the solute concentration near the membrane surface. Urea, sodium chloride, and detergent (Geroon TC-42) are major contaminants in spacecraft wastewater. In addition, numerous organic contaminants such as 2-(2-butoxyethoxy) ethanol, caprolactam, 2-propanol, formaldehyde, and methanol have also been found at low concentrations in condensate collected from the cabin of the spacecraft. As the length of space missions increases and wastewater is reclaimed for use as potable water, it is necessary to remove all of these contaminants.

Objectives: Our previous work established the concept of a low-pressure rotating reverse osmosis membrane system. The rotation of the cylindrical RO filter produces shear and Taylor vortices in the annulus of the device that decrease the concentration polarization and fouling commonly seen with conventional RO filtration techniques. A mathematical model based on the film theory and the solution-diffusion model agrees well with the experimental results obtained using this first generation prototype. However, based on the model, the filtrate flux and contaminant rejection depend strongly on the transmembrane pressure. Therefore, the goal of our current work is to improve the flux of the device by increasing the transmembrane pressure by a factor of 3 to 4. In addition, the rejections for a wider variety of inorganic and organic compounds typically found in space mission wastewater are measured.

Rejection of Target Contaminants by Selected Membranes: Flat sheet samples of commercially available reverse osmosis, low pressure RO (LPRO), and nanofiltration (NF) membranes have been tested using a dead-end stirred-cell to remove conventional wastewater contaminants (sodium chloride, urea, and ammonium carbonate) and organic contaminants found in spacecraft condensate. By combining experimental rejection results for various compounds with a model based on the size and electrostatic exclusion properties of the membranes, the pore sizes of the membranes are estimated to be 0.33 nm for RO, 0.34 nm for LPRO, and 0.44 nm for NF membranes. The rejections for both organic and inorganic compounds for these membranes are shown in Figure 1. The rejections of 2-(2-butoxyethoxy) ethanol (BEE) and caprolactam are approximately 80% for the RO and LPRO membranes, because their molecular weights/molecular radii, 162 Da/0.32 nm for BEE and 113 Da/0.28 nm for caprolactam, are large enough to be rejected due to size exclusion. The rejection of these compounds is also relatively high (over 60 %) for the NF membrane. The rejection of ionic compounds is also high (over 80 %) for all membranes due to electrostatic exclusion effects. The rejection of 2-propanol is lower than that of NaCl even though these compounds have similar molecular weights due to electrostatic exclusion of the ionic compound. Urea, formaldehyde, and methanol rejections are quite low because the molecules are small and uncharged. As a result, they are difficult to reject

by size exclusion or by electrostatic exclusion. Furthermore, the rejection of urea is substantially lower than 2-propanol even though they have the same molecular weight of 60.1 Da. This is because the molecular radius of urea (0.18 nm) is smaller than that of 2-propanol (0.26 nm).

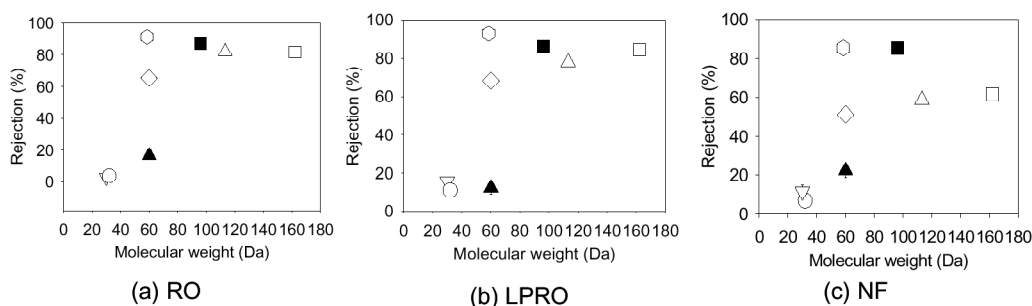


Figure 1. Rejection of different compounds for RO, LPRO, and NF. Operating conditions: • P=800 kPa; stirring speed=400 rpm; feed concentration=1 mM; recovery=60 %. (a) RO (AK), (b) LPRO (ESPA), and (c) NF (ESNA) (•; urea; •; ammonium carbonate; ◯, sodium chloride; •; methanol; •; 2-(2-butoxyethoxy) ethanol; •; caprolactam; •; formaldehyde; •; 2-propanol).

Rotating Reverse Osmosis: A second generation rotating reverse osmosis system has been designed and fabricated to function at a much higher transmembrane pressure than the original system. The new device operates at 500 psi (3450 kPa) compared to the first generation prototype that operated at 150 psi (1035 kPa). The second generation prototype and fluid circuit (Figure 2a) have also been designed so that testing can be conducted for much longer time periods: tests lasting 4 weeks or more compared to a maximum of a 6-hour test conducted with the first-generation prototype.

Preliminary three day tests exhibit high flux (Figure 2b) and high rejection (over 70 % for NaCl, 80 % for $(\text{NH}_4)_2\text{CO}_3$, 97 % for detergent) for the duration of the experiment while maintaining a high recovery ranging from 75 to 90 %. This recovery is significantly higher than the average of recovery of 25 % for typical spiral wound RO systems, a property that is particularly advantageous for maximum water recovery. The second generation device exhibits a flux four times greater than that of the first generation prototype primarily due to the higher operating pressure. These experiments are the first step in the validation of rotating reverse osmosis at high transmembrane pressures over long time periods.

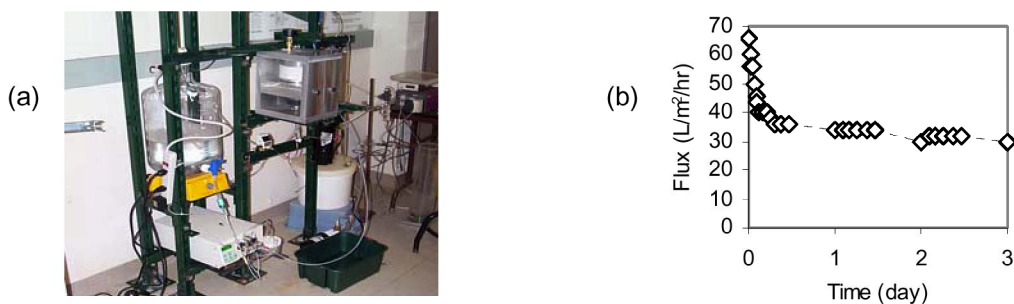


Figure 2. (a) Photograph of second generation rotating reverse osmosis filter and fluid circuit and (b) Flux as a function of time for a 3 day experiment. Operating conditions: LPRO (ESPA); • P=500 psi; rotation rate=90 rpm; recovery=75 to 90 %; wastewater composed of NaCl (1,000 mg/L), $(\text{NH}_4)_2\text{CO}_3$ (3,429 mg/L), and detergent (2,000 mg/L).

Funded by NASA.