

Stirling Analysis Comparison of Commercial VS. High-Order Methods



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Thermal Energy Conversion Branch

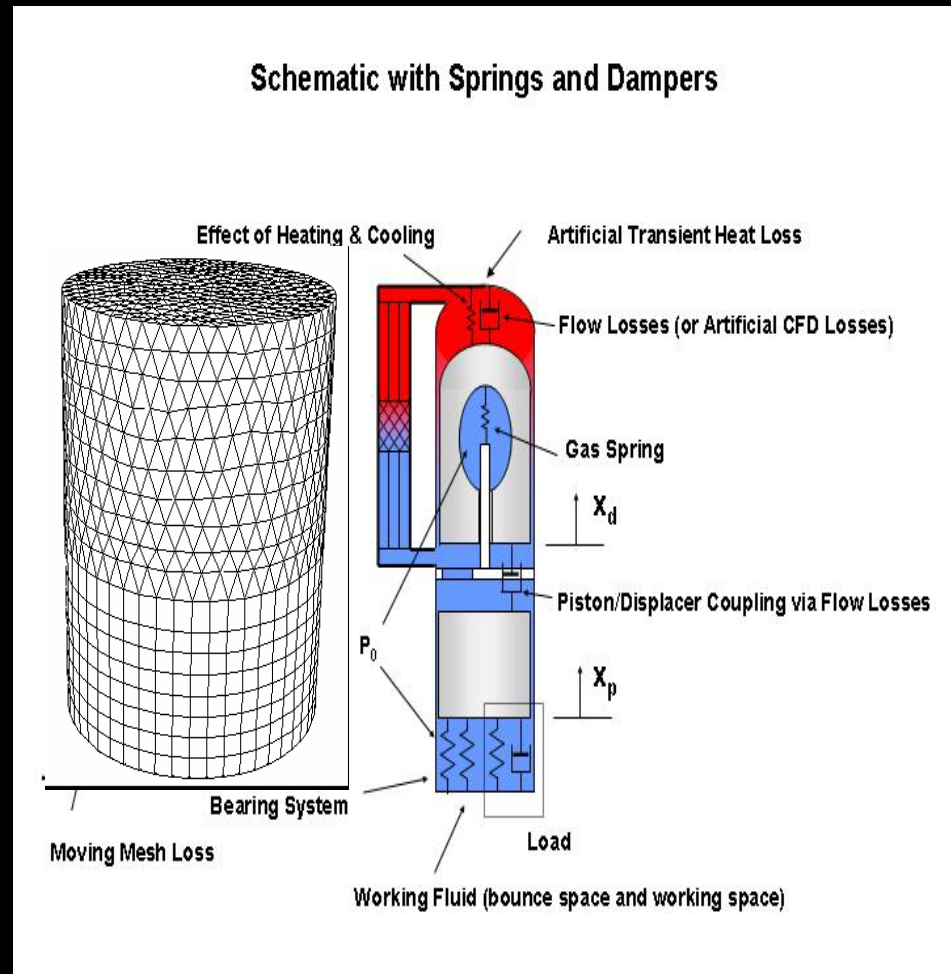
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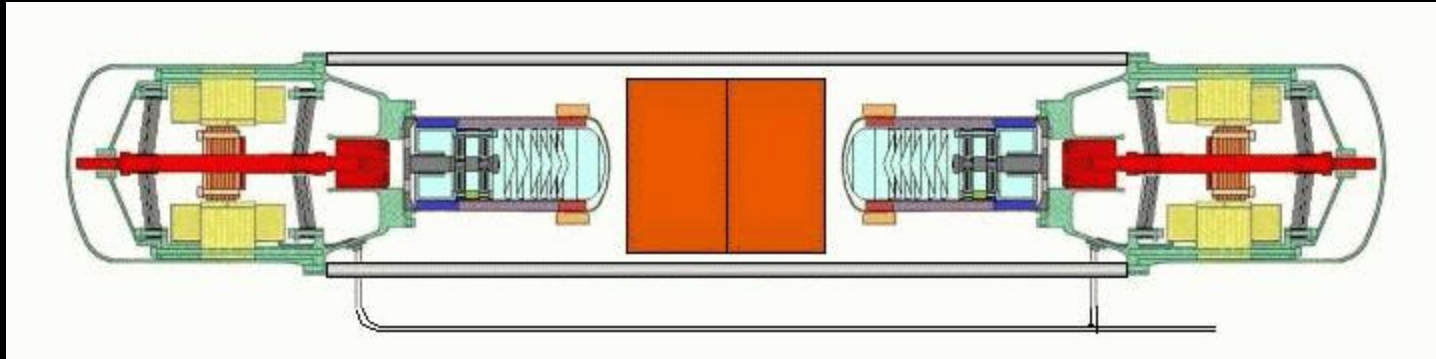
Stirling Simulation Numerical Error

- Remeshing interpolation
- Layering interpolation
- Diffusive time advance
- Low grid quality/skewness
- Sliding interface interpolation
- Artificial entropy
- Turbulence transition



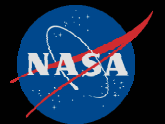
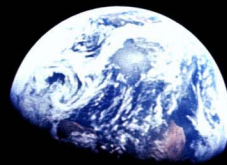
Dual Opposed Convertors

- High Efficiency – Low Mass Space Power

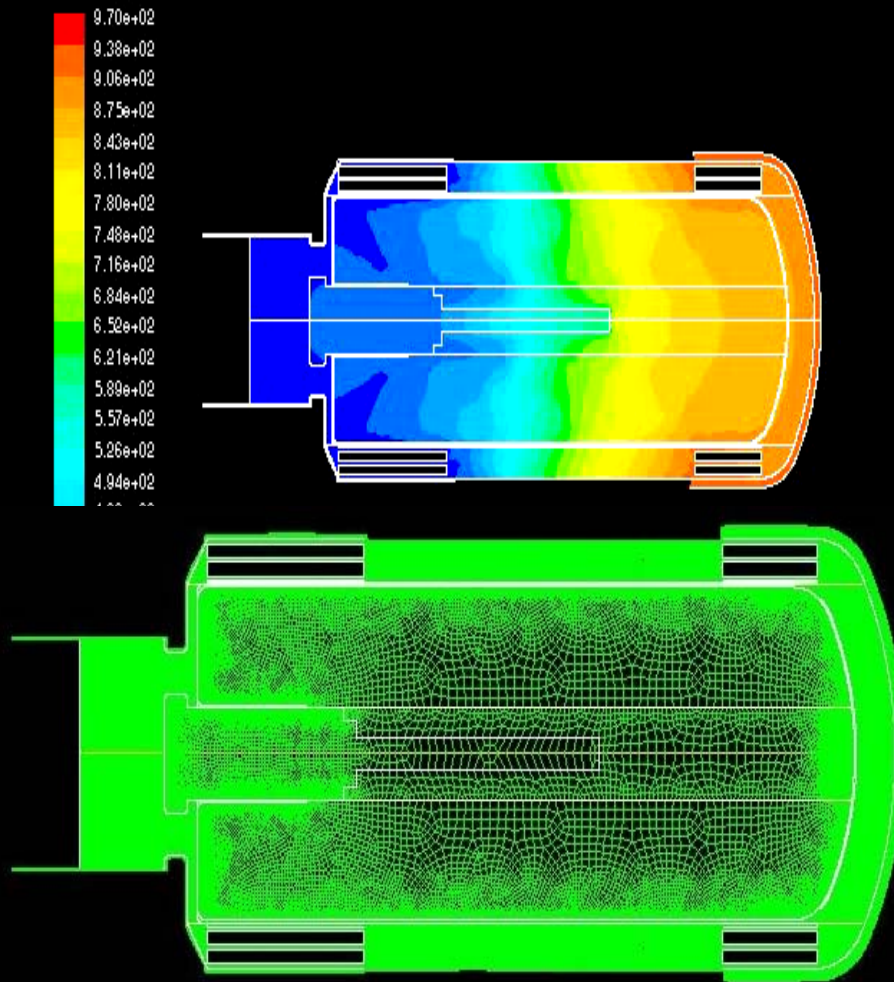


- Free Piston Geometry is Essentially Smooth

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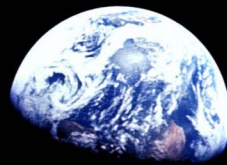


Whole Engine Simulation

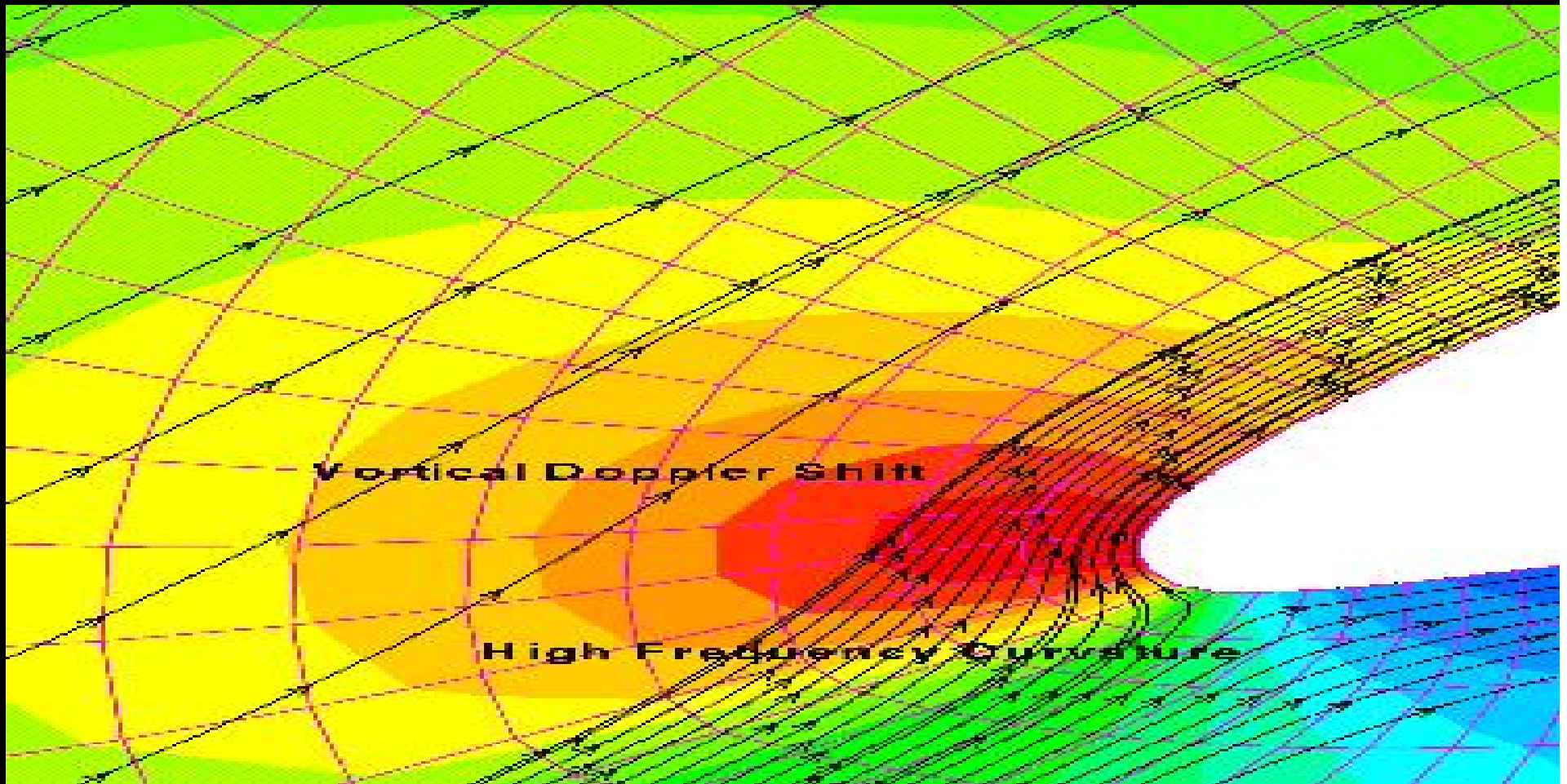


- Bounded by Walls – No need for nonreflecting B.C.
- Kolmogorov scales fairly large
- Steep thermal gradients
- No shocks/subsonic/transitioning
- High-order friendly

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Curvilinear Features



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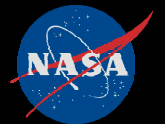
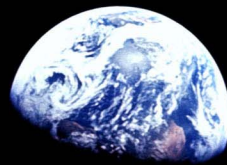


Stability Analysis

- Courant (CFL) number,
 $r = c \Delta t / \Delta x$
- Von Neumann number,
 $v = \mu \Delta t / \Delta x^2$
- Linear Viscous Burger's Equation

$$\frac{\partial u}{\partial t} + c \frac{\partial u}{\partial x} = \mu \frac{\partial^2 u}{\partial x^2}$$

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Compact Scheme 6th Order in Space

$$\alpha \left(\frac{\partial u}{\partial x} \right)_{i-1} + \left(\frac{\partial u}{\partial x} \right)_i + \alpha \left(\frac{\partial u}{\partial x} \right)_{i+1} = a \frac{u_{i+1} - u_{i-1}}{2\Delta x} + b \frac{u_{i+2} - u_{i-2}}{4\Delta x}$$

$$\alpha = 1/3, a = 14/9, b = 1/9$$

$$\alpha \left(\frac{\partial^2 u}{\partial x^2} \right)_{i-1} + \left(\frac{\partial^2 u}{\partial x^2} \right)_i + \alpha \left(\frac{\partial^2 u}{\partial x^2} \right)_{i+1} = a \frac{u_{i+1} - 2u_i + u_{i-1}}{\Delta x^2} + b \frac{u_{i+2} - 2u_i + u_{i-2}}{4\Delta x^2}$$

$$\alpha = 2/11, a = 12/11, b = 3/11$$

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Runge-Kutta 4th Order

$$R(u) = -cu_x + \mu u_{xx}$$

$$u^{(1)} = u^n + \frac{\Delta t}{2} R^n$$

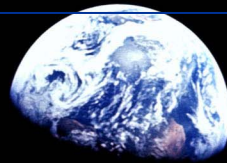
$$u^{(2)} = u^n + \frac{\Delta t}{2} R^1$$

$$u^{(3)} = u^n + \Delta t R^2$$

$$u^{(n+1)} = u^n + \frac{\Delta t}{6} (R^n + 2R^{(1)} + 2R^{(2)} + R^{(3)})$$

$$R^{(1)} = R(u^{(1)}), R^{(2)} = R(u^{(2)}), R^{(3)} = R(u^{(3)})$$

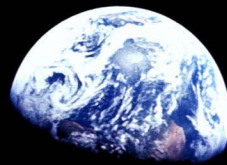
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Current Practice

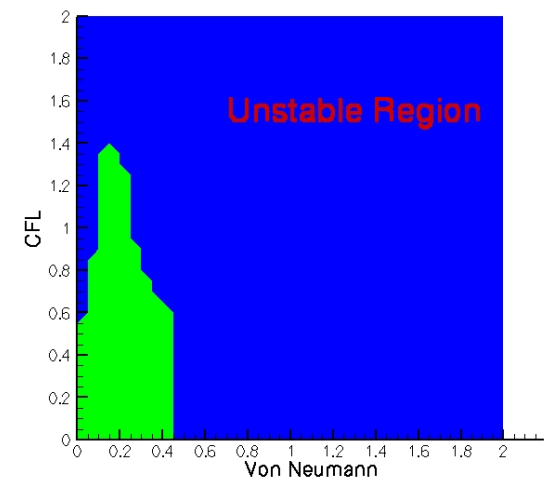
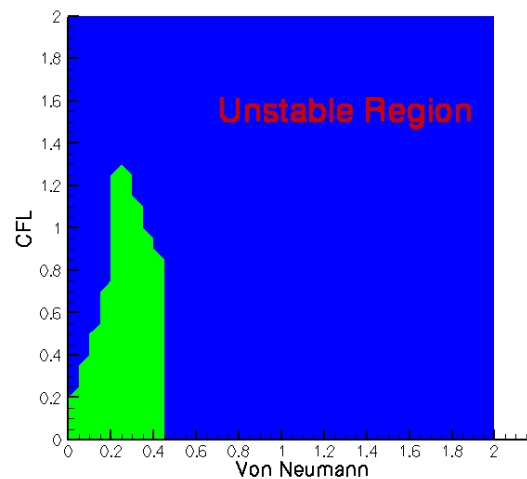
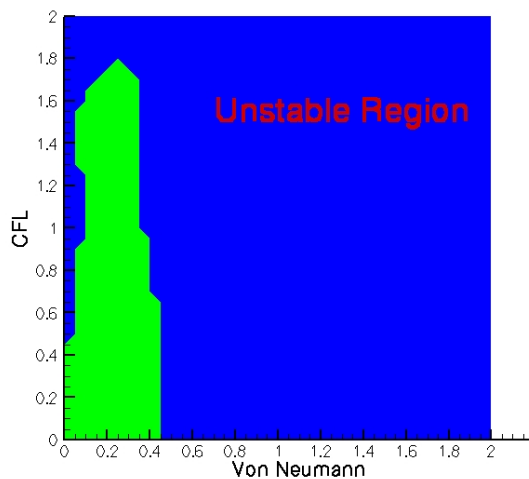
- Implicit 1st or 2nd order in time commercially
- 1st or 2nd order in space implicit
- Explicit/implicit 4th order in time academically
- Implicit 6th order compact scheme in space

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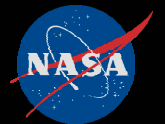


Compact Scheme Stability Range

- Domain size affects stability since implicit



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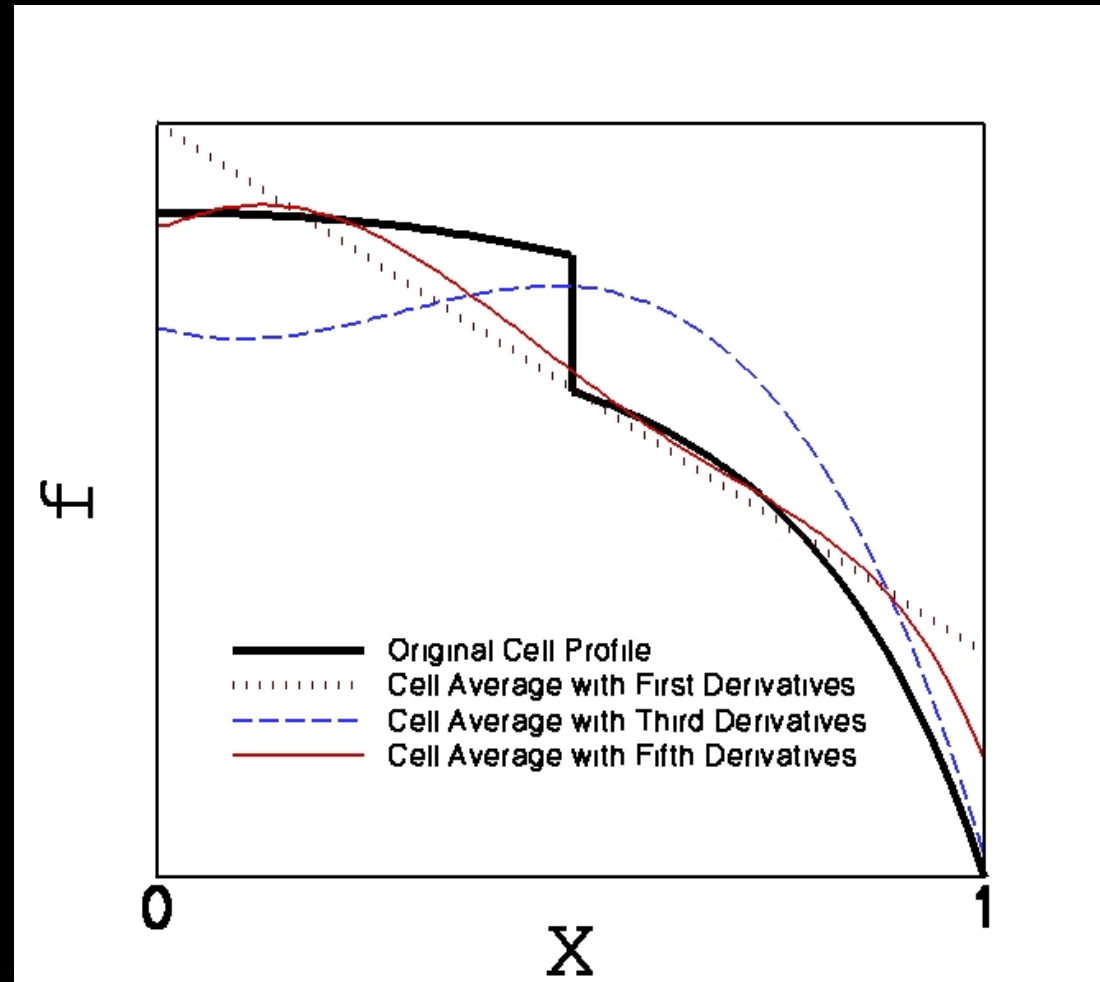
Basic UHF Technique



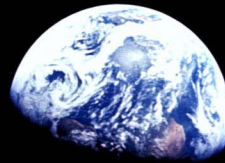
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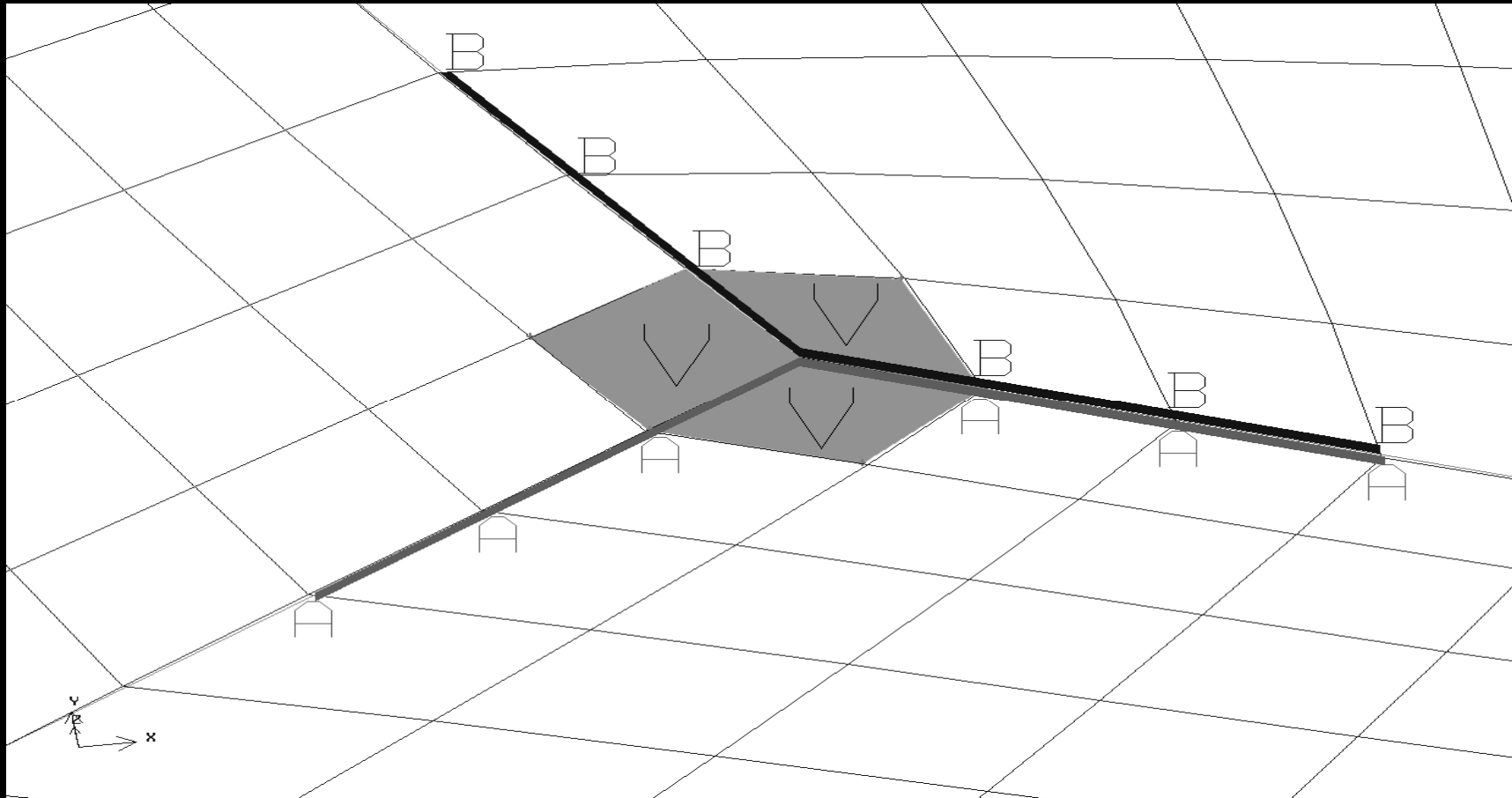
Derivatives of Cell Averages



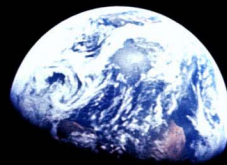
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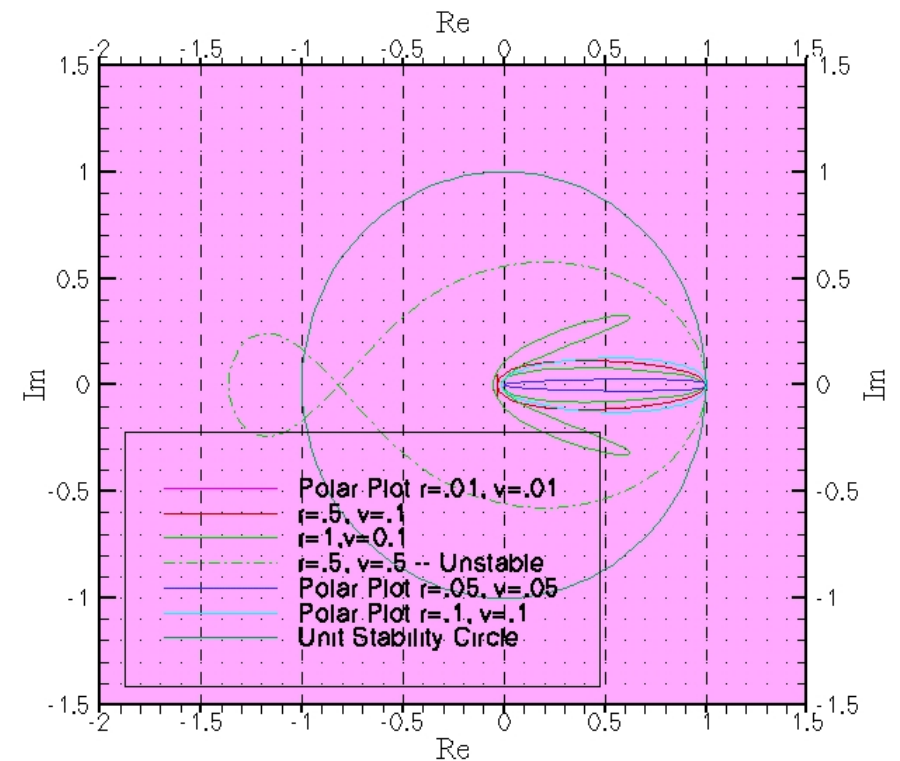
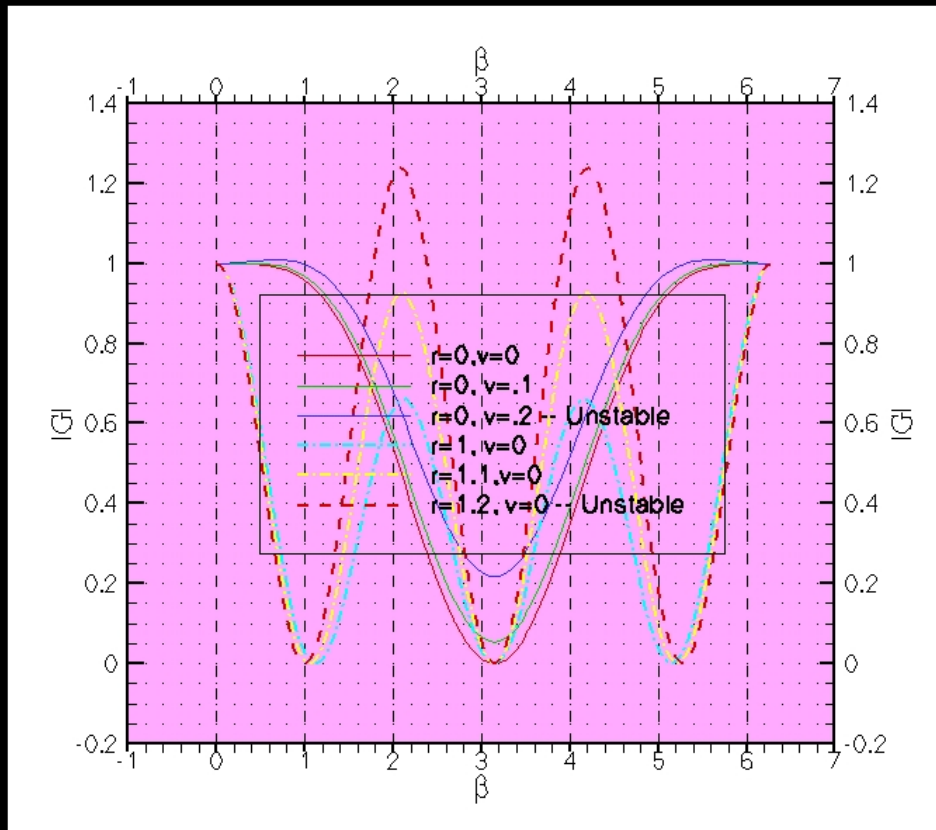
Grid Singularity Resolution



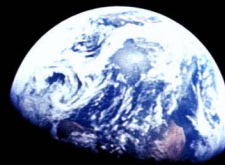
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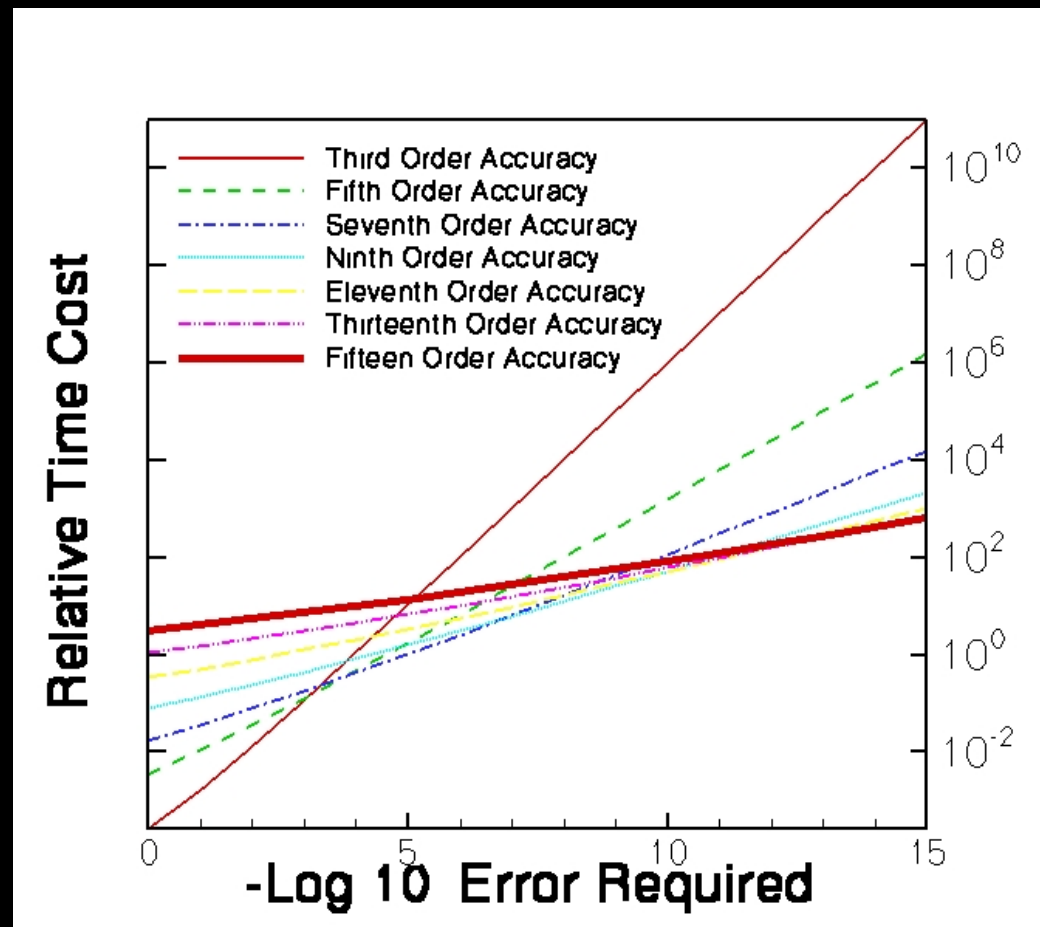
C4o0 Linear Viscous Burger's Equation



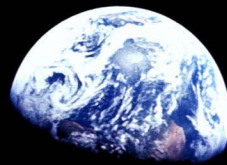
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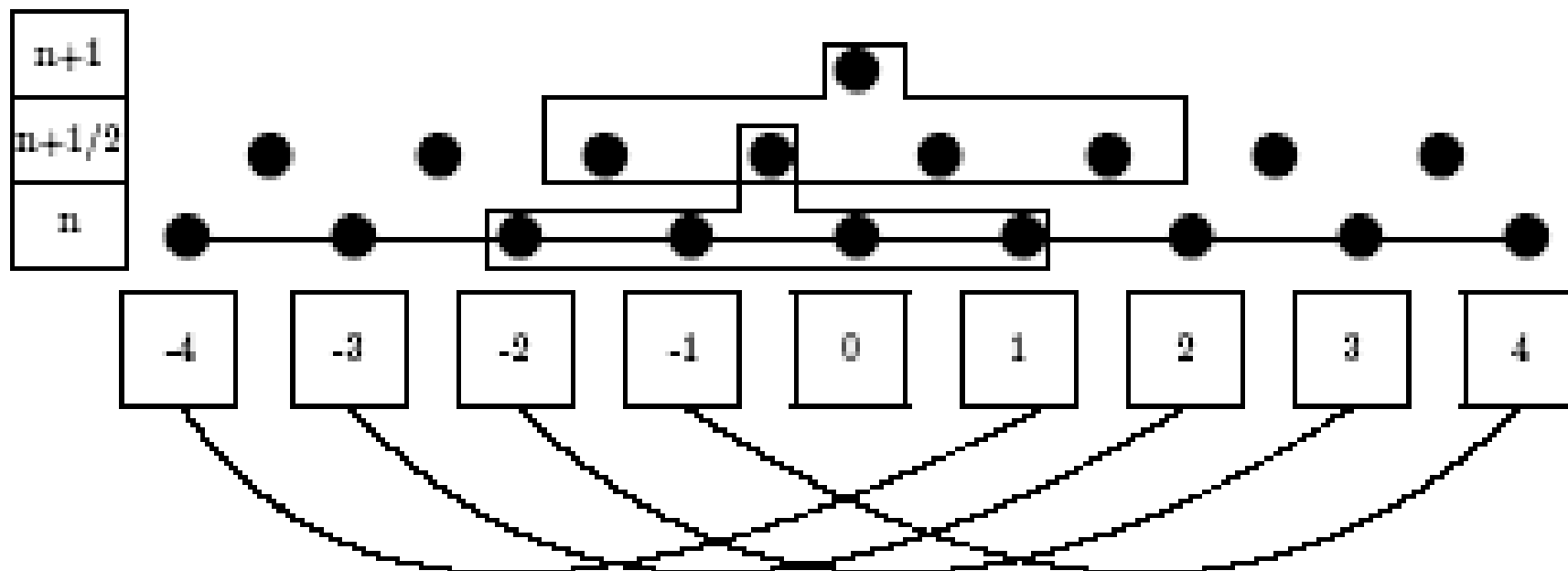
Efficiency Improves with Accuracy



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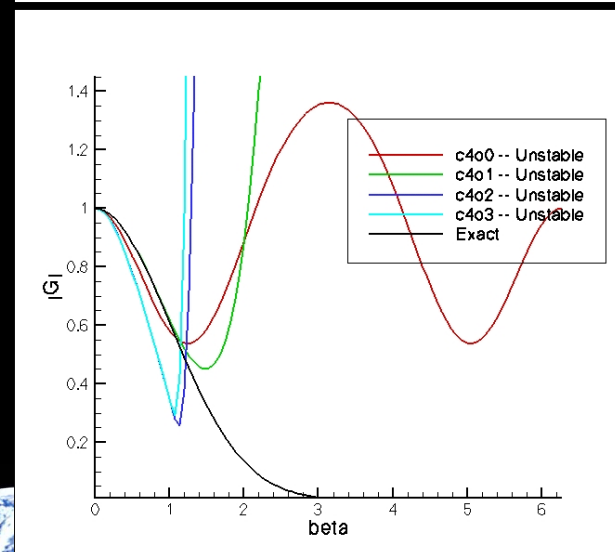
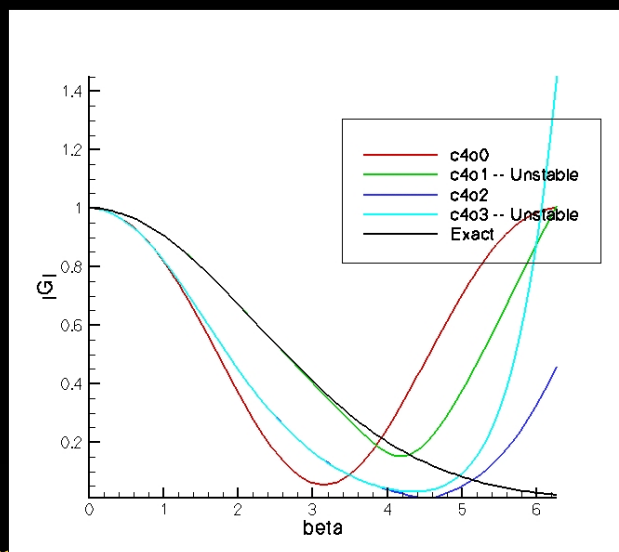
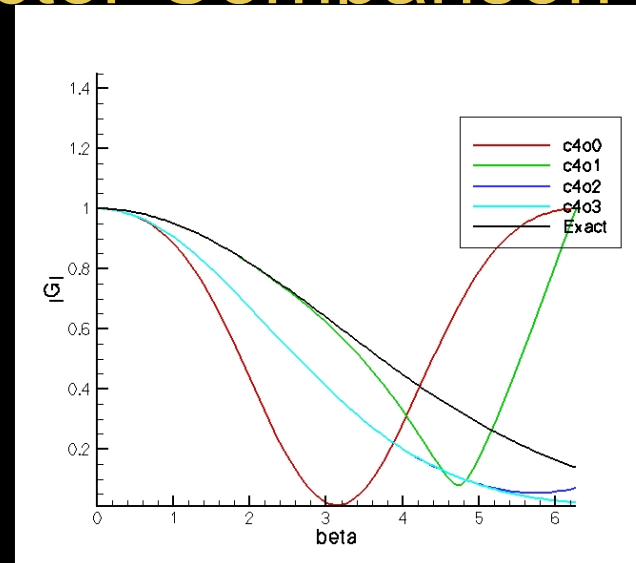
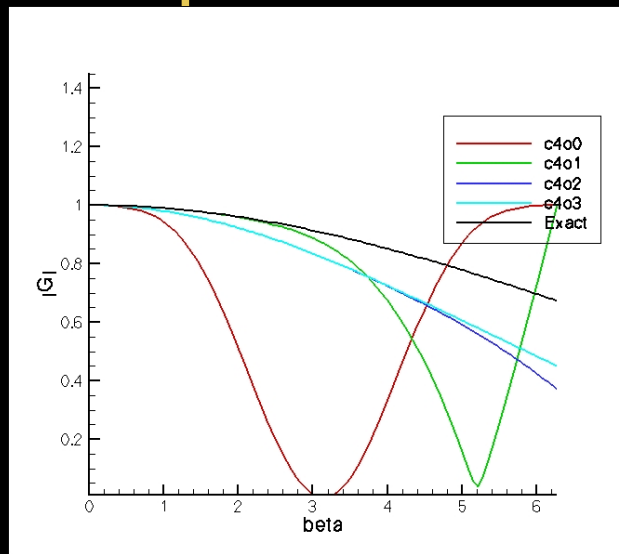
Computational Domain Schematic



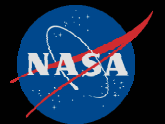
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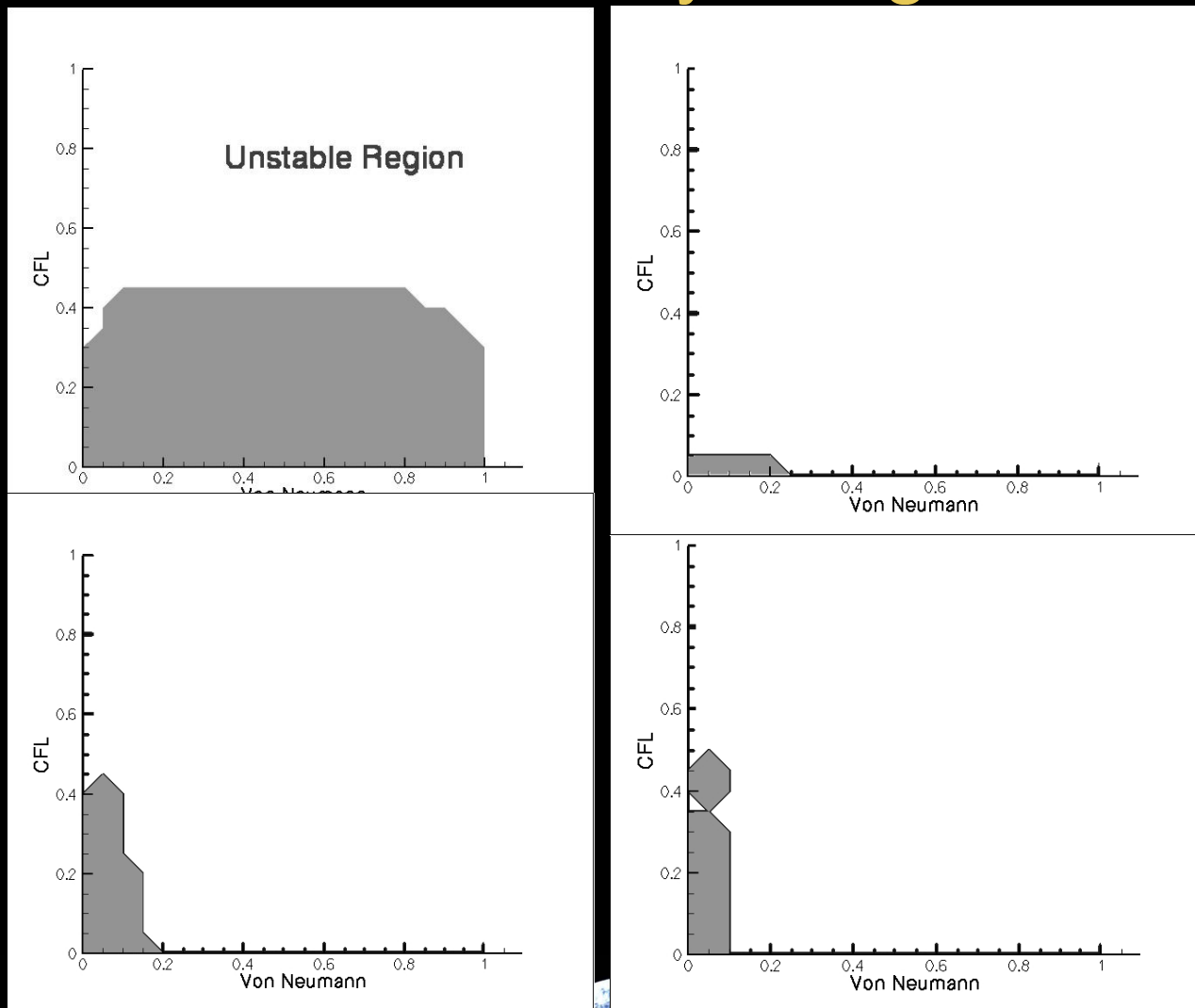
Amplification Factor Comparison



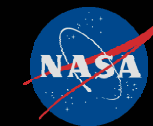
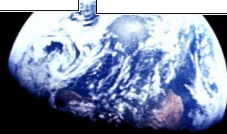
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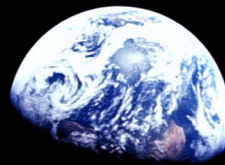
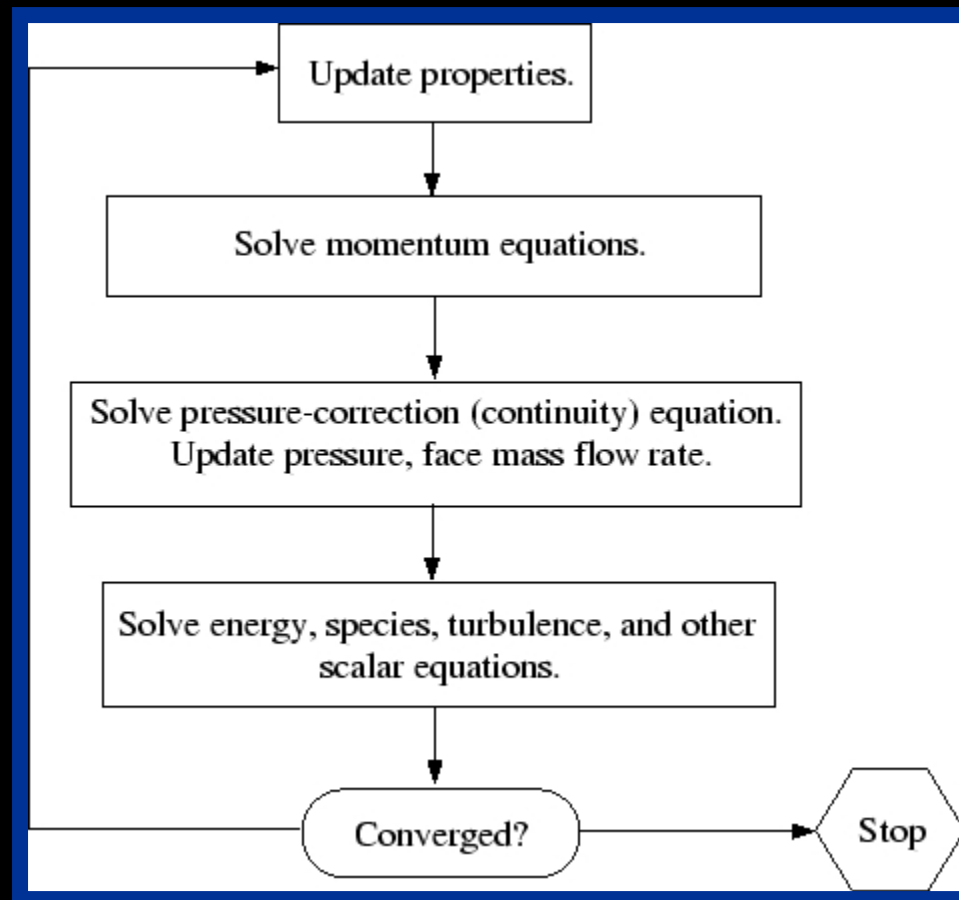
UHF Stability Range



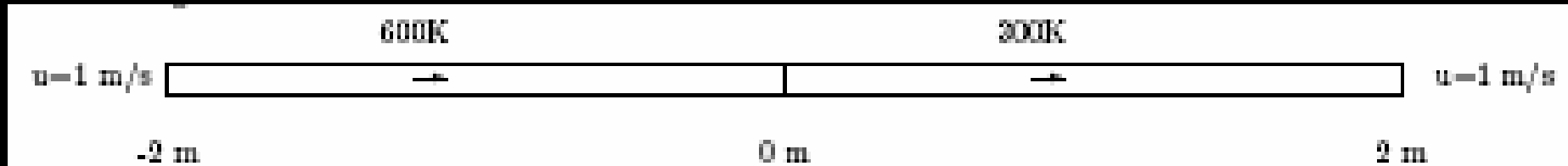
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Overview of Segregated Solution



Heat Transfer Test



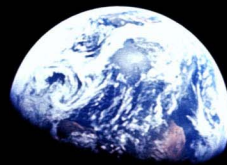
$$\frac{\partial E_t}{\partial t} + \frac{\partial}{\partial x} \left((\rho C_v T + p)u - \frac{4}{3} \mu u_x + q_x \right) = 0$$

Reduces to:

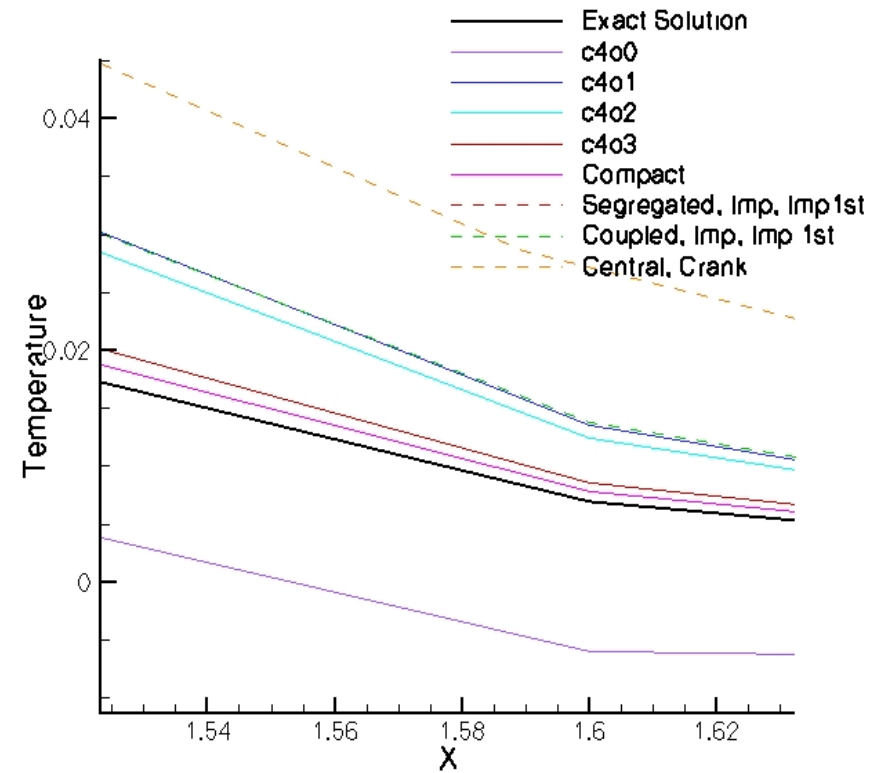
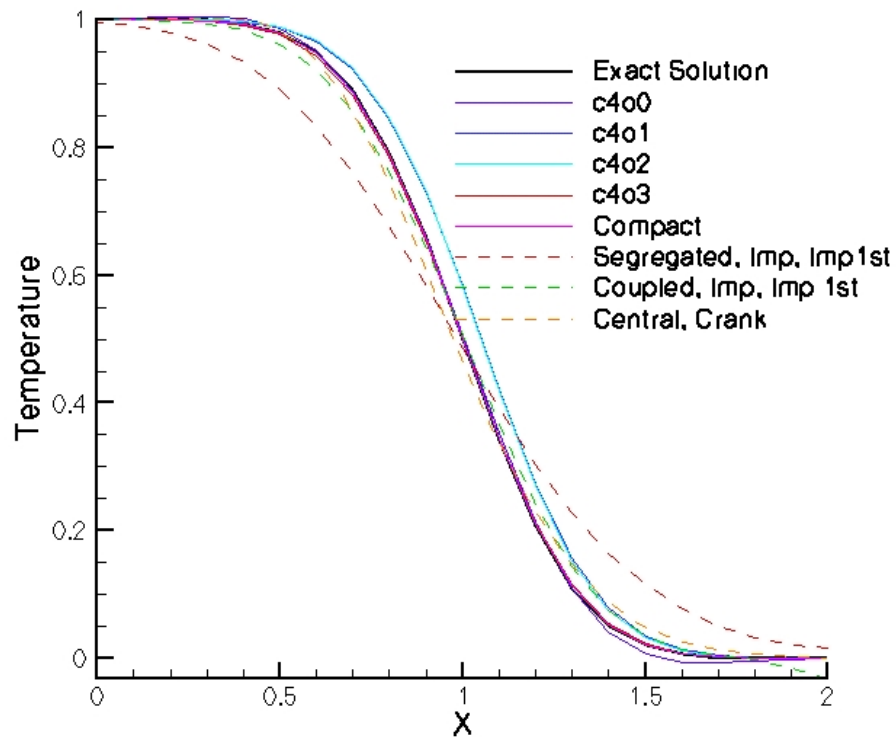
$$\frac{\partial T}{\partial t} + u \frac{\partial T}{\partial x} = \alpha \frac{\partial^2 T}{\partial x^2},$$

$$\alpha = \frac{k}{\rho C_p}$$

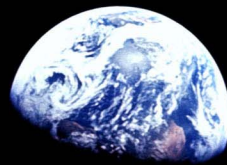
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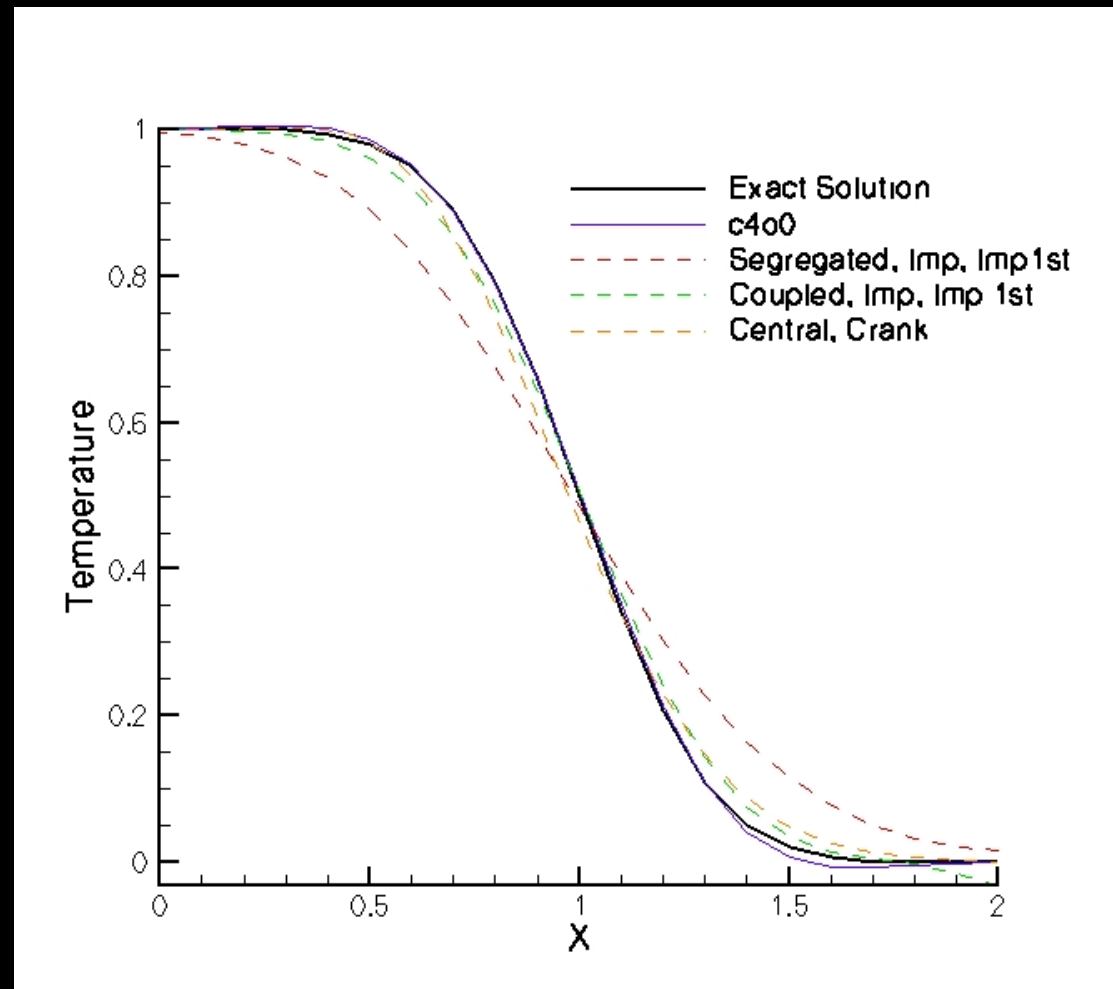
Comparison of Commercial & Advanced



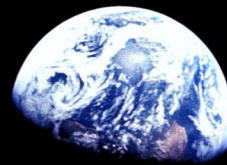
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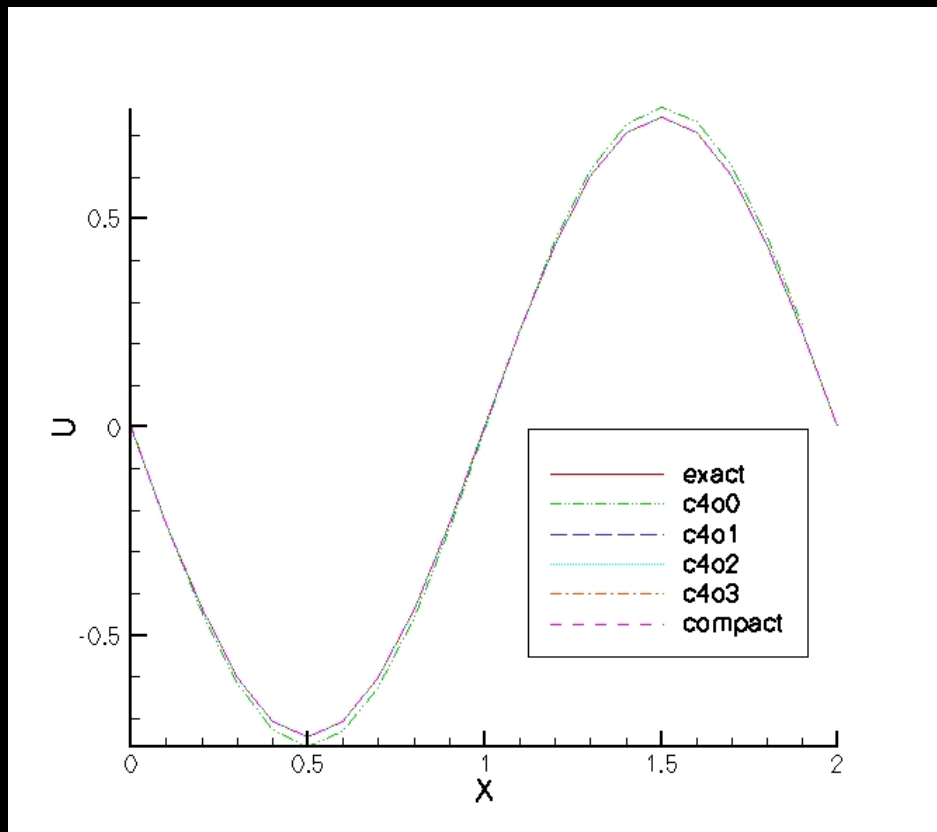
Commercial Comparison



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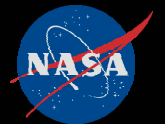
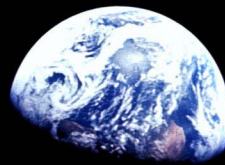


Turbulence Transition Efficiency

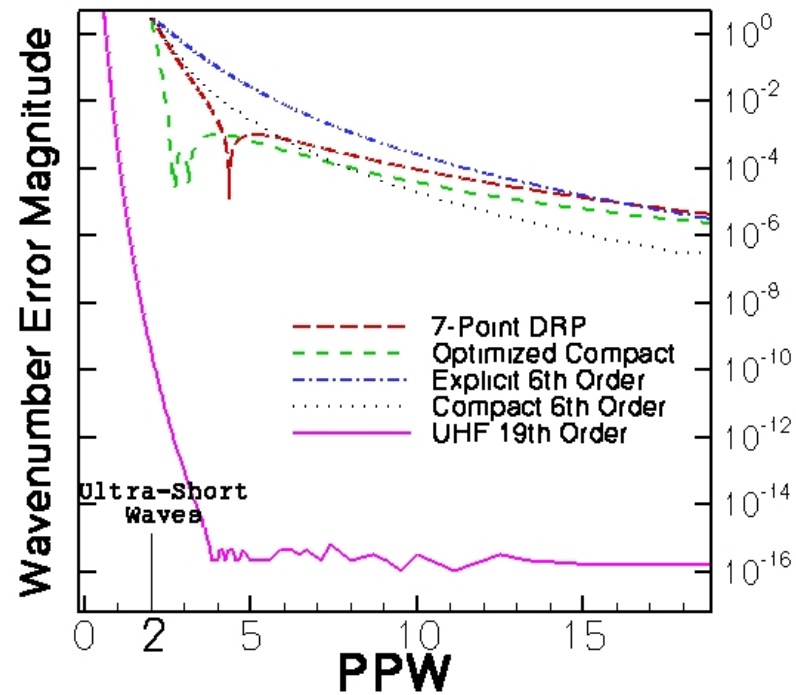


| Method | Spacing | Error |
|---------|---------|--------------------------|
| c4o0 | .1 | $2.54299 \cdot 10^{-2}$ |
| c4o0 | .2 | $4.27963 \cdot 10^{-2}$ |
| c4o0 | .4 | $4.68577 \cdot 10^{-2}$ |
| c4o1 | .1 | $3.11163 \cdot 10^{-6}$ |
| c4o1 | .2 | $2.96551 \cdot 10^{-5}$ |
| c4o1 | .4 | $8.4702 \cdot 10^{-4}$ |
| c4o2 | .1 | $1.0178 \cdot 10^{-10}$ |
| c4o2 | .2 | $3.1935 \cdot 10^{-9}$ |
| c4o2 | .4 | $6.41079 \cdot 10^{-8}$ |
| c4o3 | .1 | $3.44169 \cdot 10^{-15}$ |
| c4o3 | .2 | $2.27818 \cdot 10^{-12}$ |
| c4o3 | .4 | $3.12925 \cdot 10^{-11}$ |
| compact | .1 | $1.0993 \cdot 10^{-6}$ |
| compact | .2 | $7.10999 \cdot 10^{-5}$ |
| compact | .4 | $5.31245 \cdot 10^{-2}$ |

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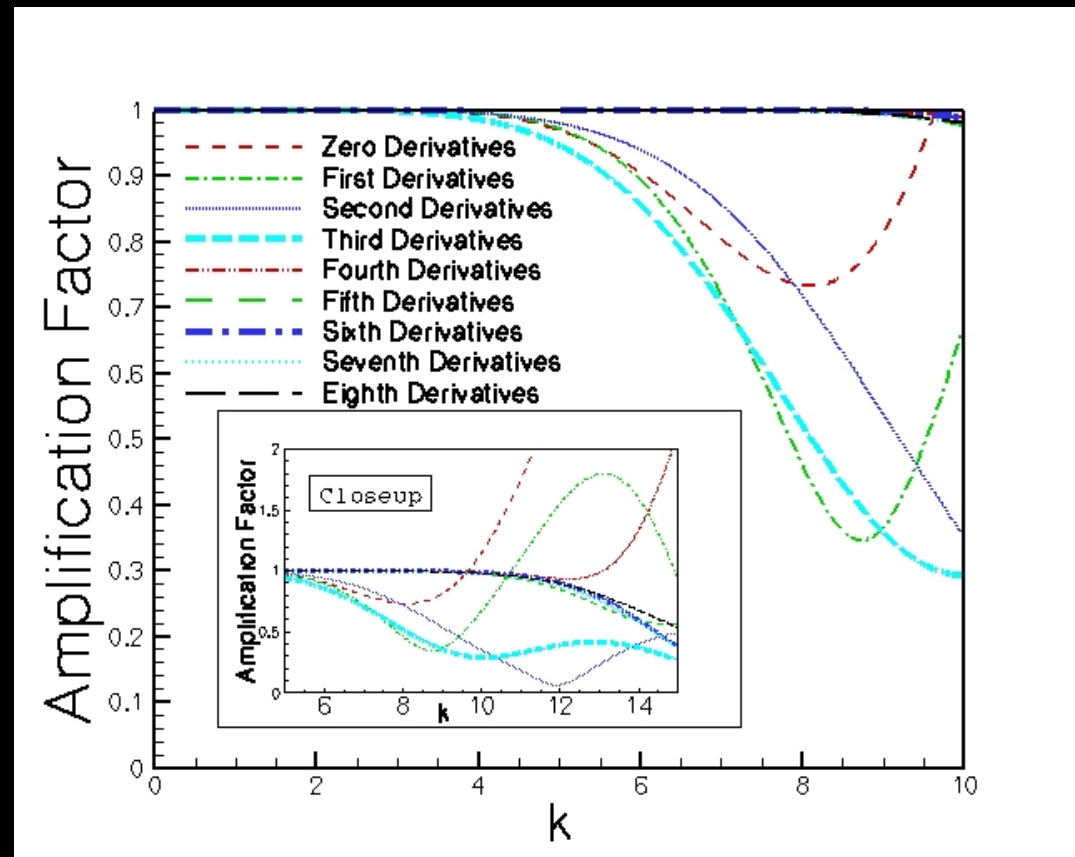
Points per Kolmogorov Wavelength



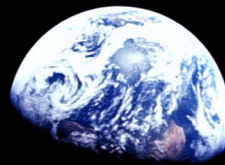
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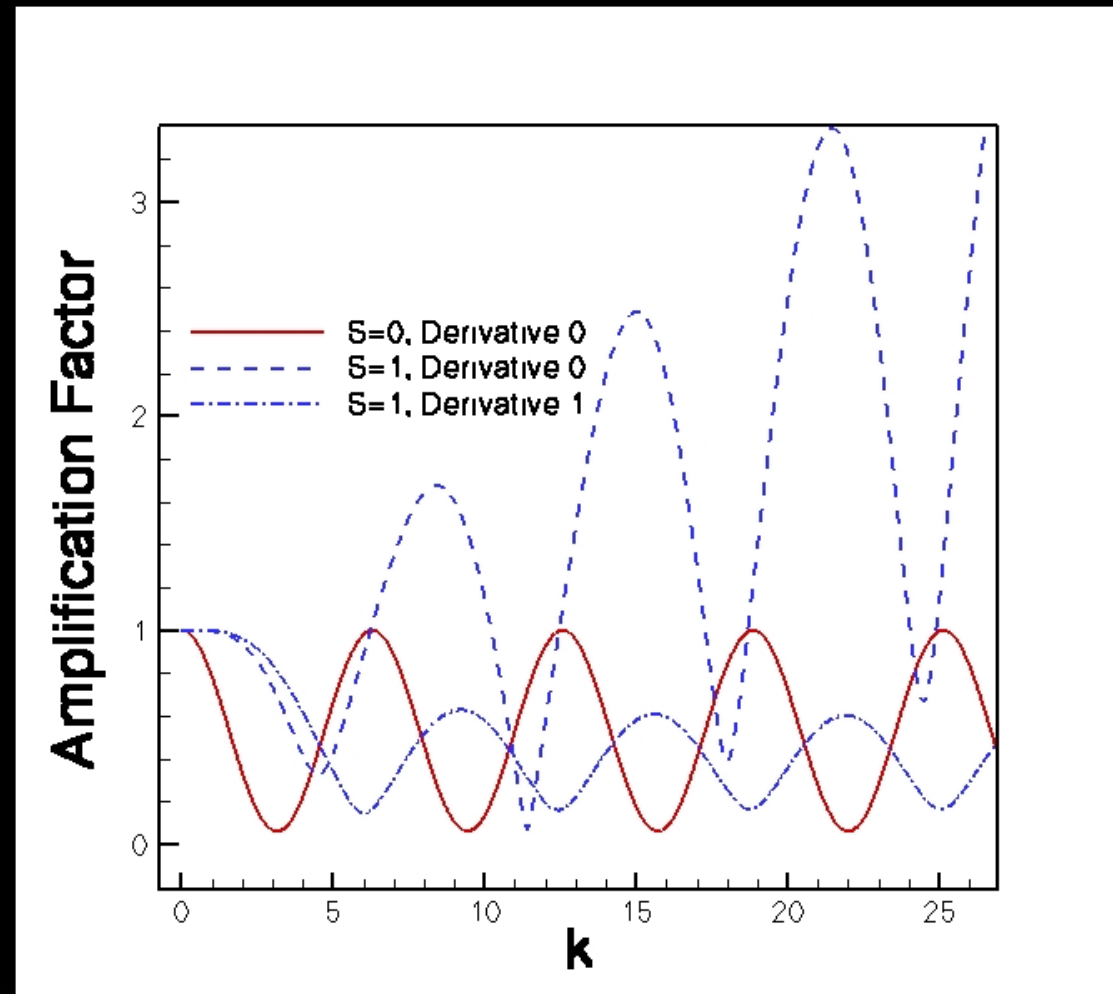
Wave Equation Amplification



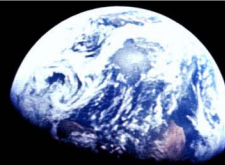
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Aliased Frequency Amplification



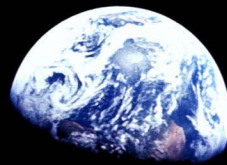
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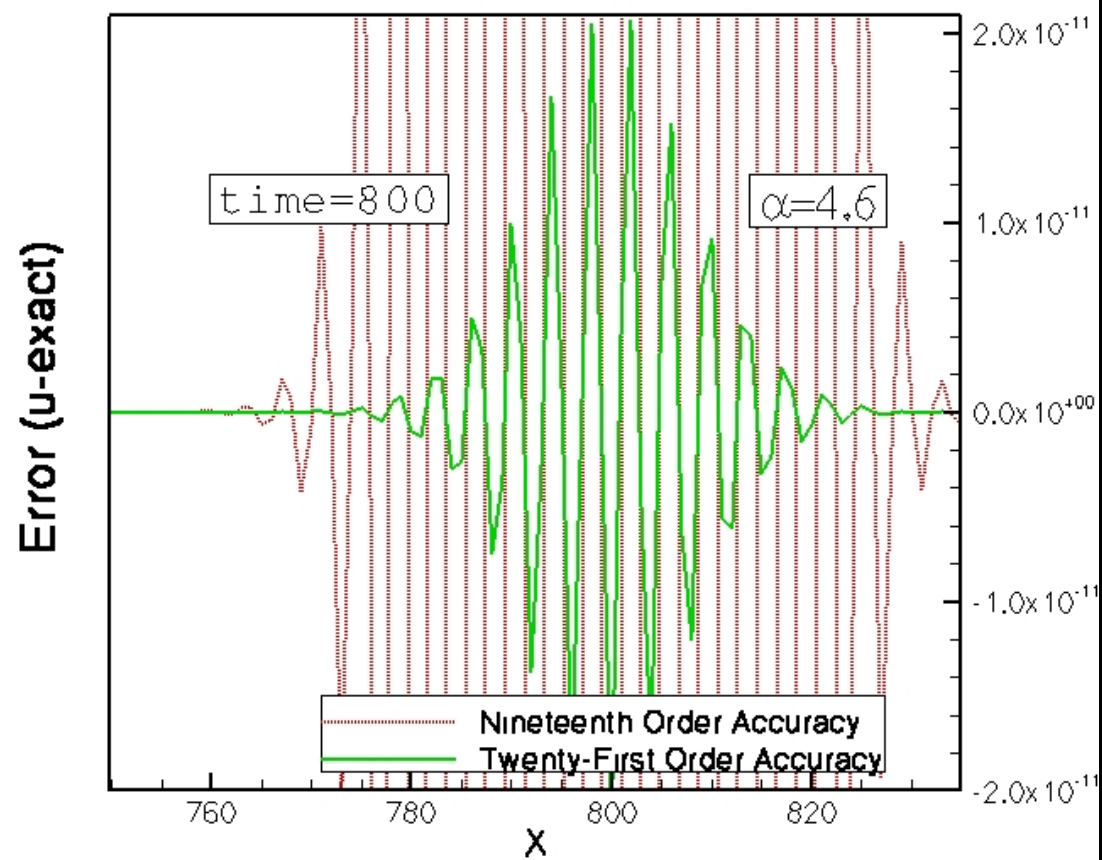


Conclusions

- Low Reynold's number, wall bounded flow allows economical use of large eddy simulation for turbulent transition modeling
- UHF and Compact comparable at conjugate heat transfer
- UHF much better for turbulence modeling
- Modern methods much more efficient than those currently available commercially

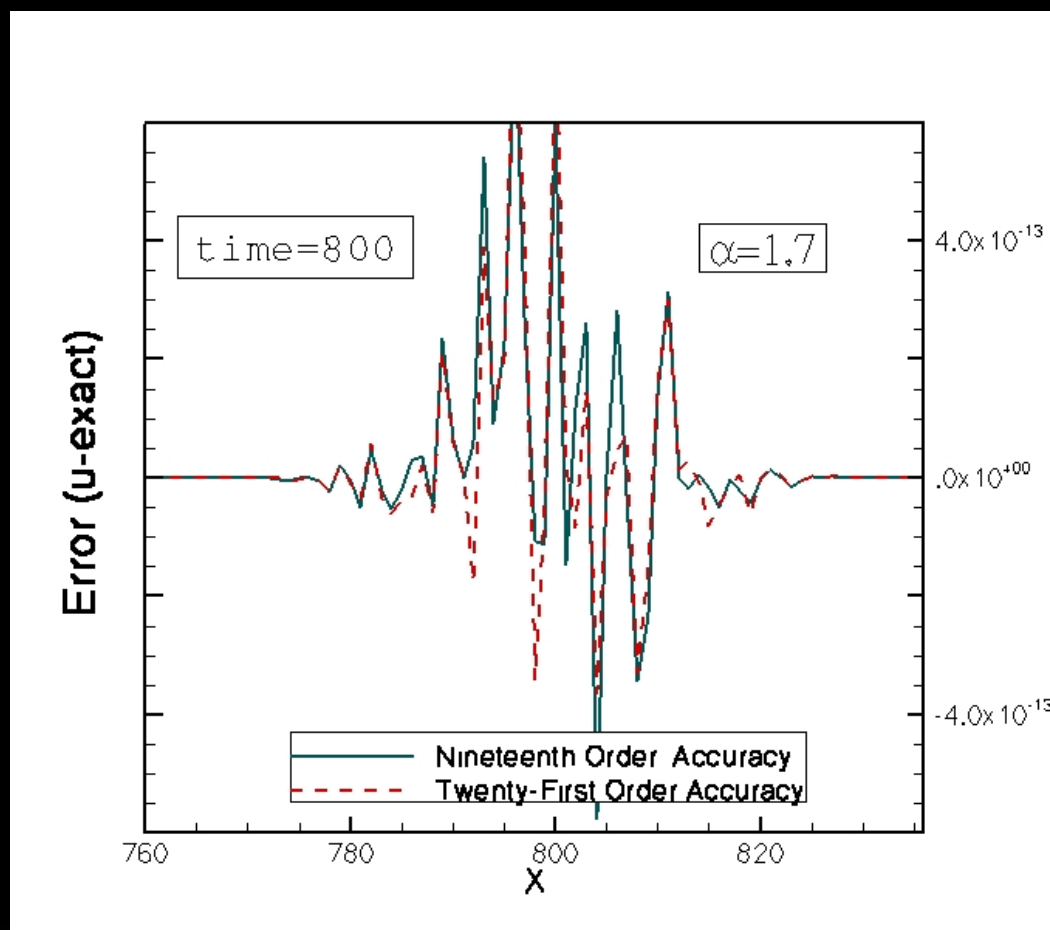
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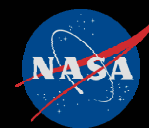


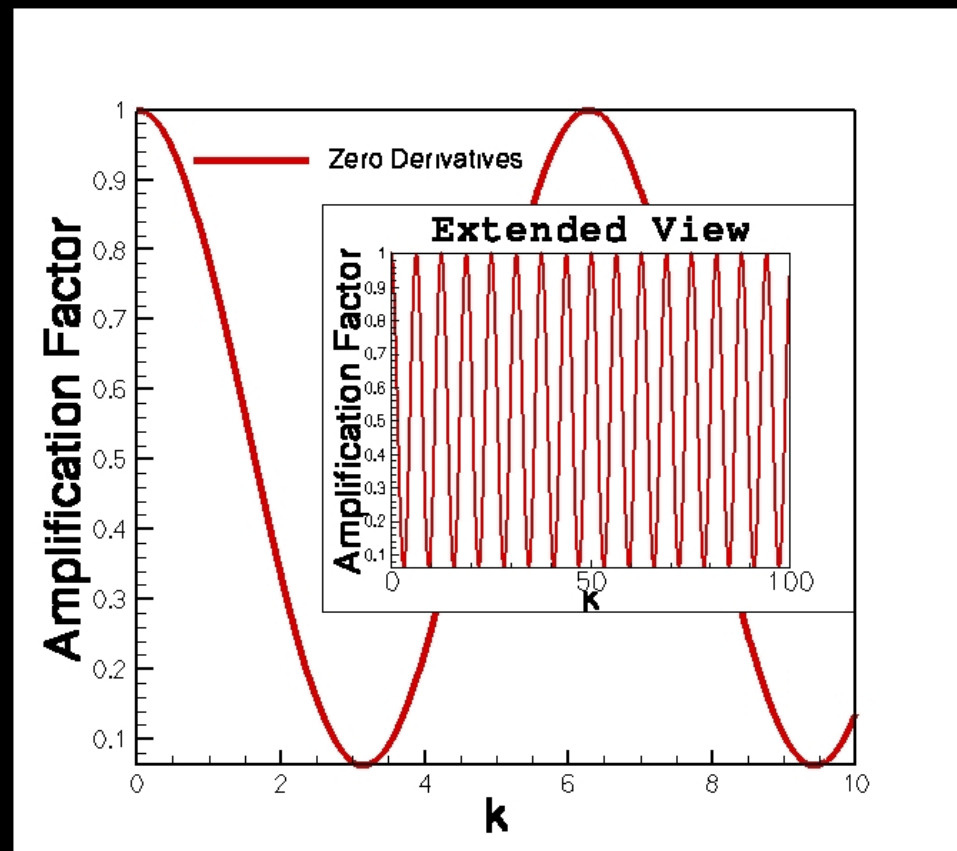
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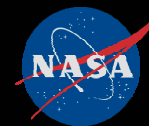


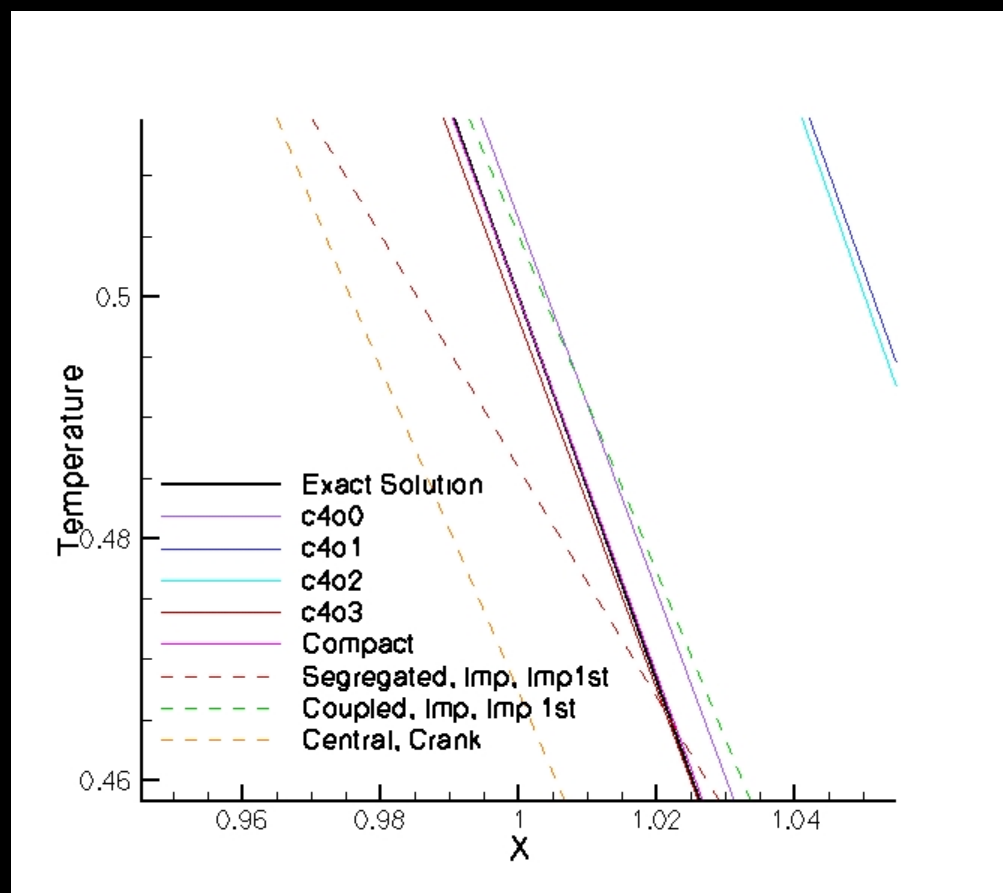
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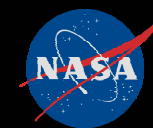


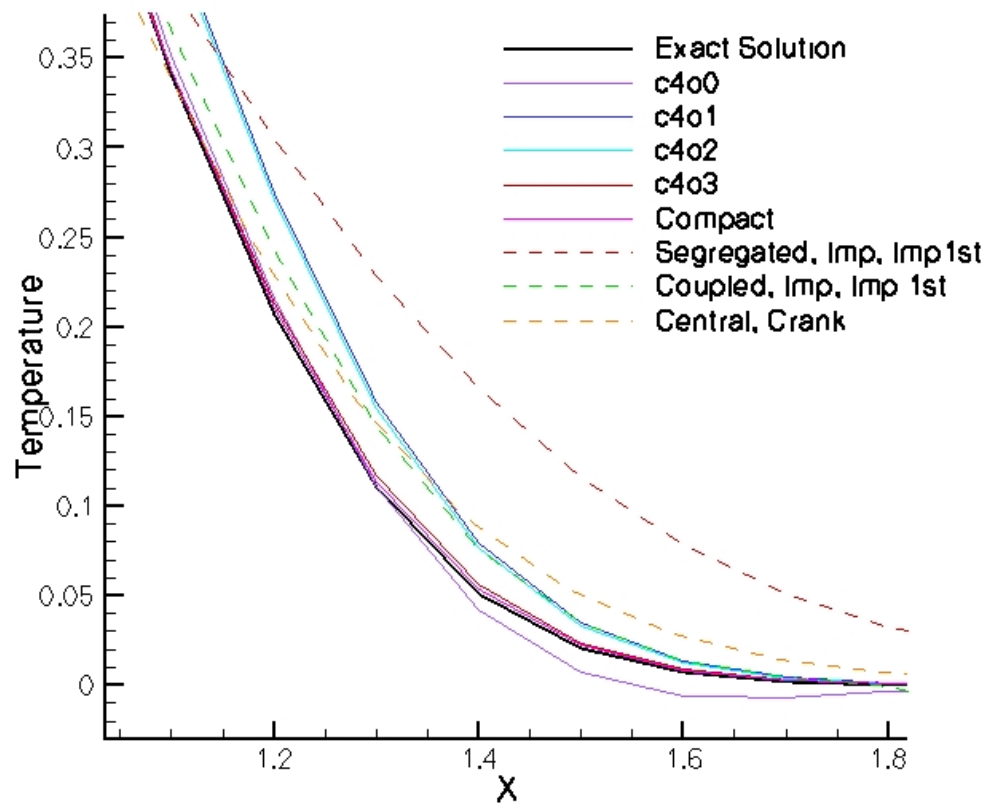
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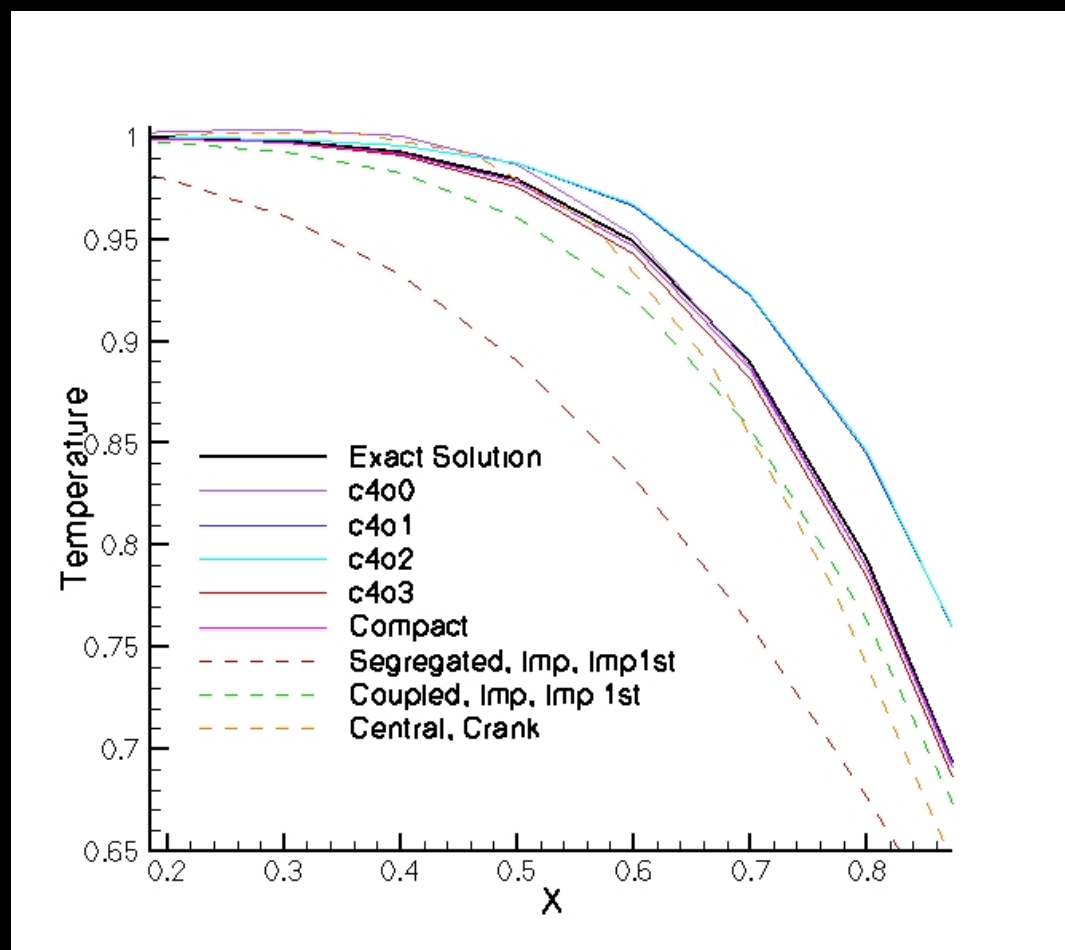
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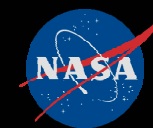


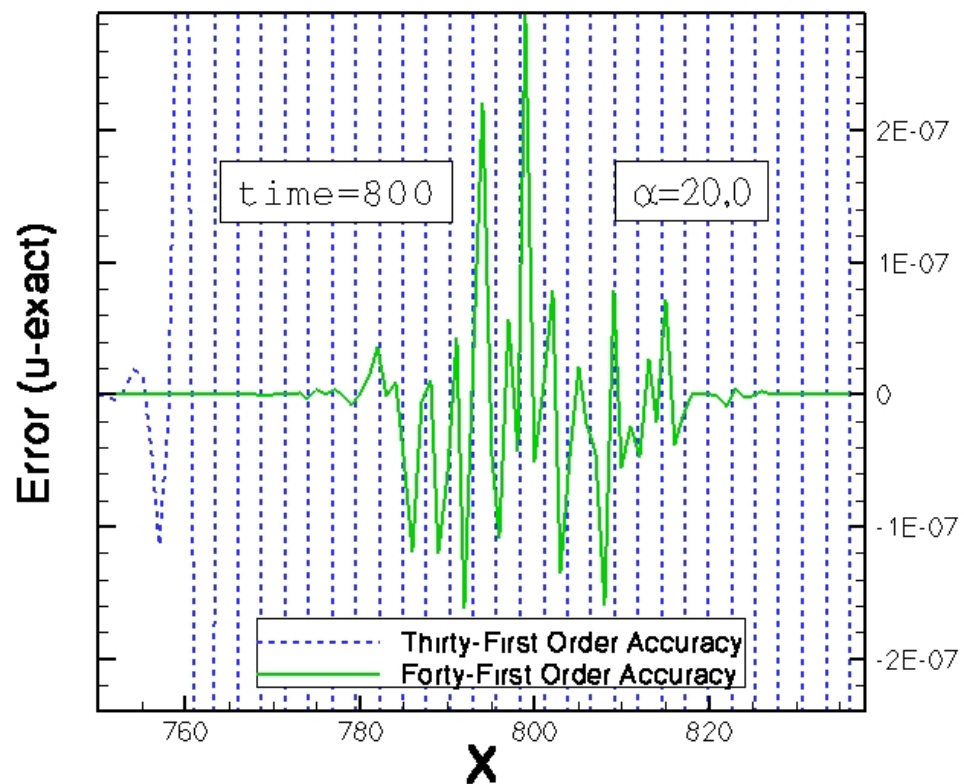
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