

Role of Turbulent Prandtl Number on Heat Flux at Hypersonic Mach Numbers

X. Xiao^{*}, J. R. Edwards[†], and H. A. Hassan[‡]
North Carolina State University, Raleigh, NC 27695-7910

and

R. L. Gaffney, Jr.[§]
NASA Langley Research Center, Hampton, VA 23681-2199

A new turbulence model suited for calculating the turbulent Prandtl number as part of the solution is presented. The model is based on a set of two equations: one governing the variance of the enthalpy and the other governing its dissipation rate. These equations were derived from the exact energy equation and thus take into consideration compressibility and dissipation terms. The model is used to study two cases involving shock wave/boundary layer interaction at Mach 9.22 and Mach 5.0. In general, heat transfer prediction showed great improvement over traditional turbulence models where the turbulent Prandtl number is assumed constant. It is concluded that using a model that calculates the turbulent Prandtl number as part of the solution is the key to bridging the gap between theory and experiment for flows dominated by shock wave/boundary layer interactions.

Nomenclature

$C_b, C_{h,1}-C_{h,11}$	=	model constants
h	=	enthalpy
\tilde{h}^{n^2}	=	enthalpy variance
M	=	Mach number
k	=	turbulence kinetic energy

^{*} Research Assistant Professor, Dept. of Mechanical and Aerospace Engineering, Member AIAA

[†] Associate Professor, Dept. of Mechanical and Aerospace Engineering, Associate Fellow AIAA

[‡] Professor, Dept. of Mechanical and Aerospace Engineering, Associate Fellow AIAA.

[§] Aerospace Engineer, Hypersonic Air Breathing Propulsion Branch, Senior Member AIAA.

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P	=	pressure
Pr	=	Prandtl number
q_i	=	turbulent heat flux
S_{ij}	=	strain tensor
T	=	temperature
u_i	=	velocity
α	=	heat diffusivity
β	=	deflection angle of shock generator
ν	=	kinematic viscosity
ρ	=	density
ζ	=	enstrophy
ϵ_h	=	dissipation rate of enthalpy variance

Subscript

0	=	stagnation conditions
t	=	turbulent
w	=	wall
∞	=	free stream

I. Introduction

Present simulation of turbulent flows involving shock wave/boundary layer interaction invariably over-estimate heat flux by almost a factor of two.¹ One possible reason for such performance is a result of the fact that the turbulence models employed make use of Morkovin's hypothesis.² This hypothesis is valid for non-hypersonic Mach numbers and moderate rates of heat transfer. At hypersonic Mach numbers, high rates of heat transfer exist in regions where shock wave/boundary layer interactions are important. For such flows, temperature fluctuations, which are as important as velocity fluctuations at the higher Mach numbers, play a major role in determining the

wall heat flux and their effects must explicitly be taken into consideration. As a result, one should not expect traditional turbulence models to yield accurate results.

The goal of this investigation is to explore the role of a variable Prandtl number formulation in predicting the heat flux in flows dominated by strong shock wave/boundary layer interactions. The intended applications involve flows in the absence of combustion such as those encountered in supersonic inlets. This can be achieved by adding equations for the temperature (enthalpy) variance and its dissipation rate. Such equations can be derived from the exact Navier-Stokes equations. Traditionally, modeled equations (see, for example, Ref. 3,4) are based on the low speed energy equation where the pressure gradient term and the term responsible for energy dissipation are ignored. It is clear that such assumptions are not valid for hypersonic flows.

The approach used here is based on the procedure used in deriving the k - ζ model,⁵ in which the exact equations that governed k , the variance of velocity, and ζ , the variance of vorticity, were derived and modeled. For the variable turbulent Prandtl number, the exact equations that govern the temperature (enthalpy) variance and its dissipation rate are derived and modeled term by term. The resulting set of equations are free of damping and wall functions and are coordinate-system independent. Moreover, modeled correlations are tensorially consistent and invariant under Galilean transformation.

Two flat plate experiments were used to determine model constants. The first is the Mach (M) 9.2 experiments of Coleman and Stollery⁶, which was conducted in a hypersonic gun tunnel at Imperial College. The second is the M=8.3 experiments of Kussoy et al.⁷ which were conducted in the Ames 3.5 Foot Hypersonic Wind Tunnel Facility. This turned out to be a major undertaking because of the different instrumentations and because no accuracy estimates of heat transfer measurement were provided. In order to put things in proper perspective, it is noted that recent heat transfer measurements⁸ on an elliptic cone in the Arnold Engineering Development Center (AEDC) Tunnel B estimated uncertainties in excess of $\pm 10\%$. The model was validated by recent non-intrusive measurements by Schülein⁹ of flows involving shock wave/boundary layer interactions at M = 5. The measurements were carried out at the Ludwig Tube Facility at DLR. Oil-film interferometry techniques were used to measure skin friction while an infrared camera system was used for heat transfer measurements.

The recent measurements of Schülein were a repeat of an earlier experiment¹⁰ which did not include heat transfer measurements or skin friction measurements in the separated flow region. Calculations of the earlier experiments were carried out by Nance and Hassan¹¹ using a k - ζ two-equation and an abbreviated stress model. It was concluded

in Ref. 10 that there was a need to develop turbulence models capable of predicting the turbulent Prandtl number as part of the solution.

It is shown in this study that a variable Prandtl number formulation results in significant improvement of heat transfer predictions in the presence of shock wave/boundary layer interactions. However, the new model has insignificant influence on wall pressure and skin friction distributions.

II. Formulation of the Problem

1. Governing equations

The energy equation can be written as

$$\rho \frac{Dh}{Dt} = \frac{\partial}{\partial t} (\rho h) + \frac{\partial}{\partial x_i} (\rho u_i h) = \frac{DP}{Dt} - \frac{\partial q_i}{\partial x_i} + \phi \equiv S_h \quad (1)$$

where $q_i = -\lambda \frac{\partial T}{\partial x_i}$

$$\phi = t_{ij} \frac{\partial u_i}{\partial x_j}$$

$$t_{ij} = 2\mu S_{ij} - \frac{2}{3} \delta_{ij} \mu \frac{\partial u_m}{\partial x_m}$$

$$S_{ij} = \frac{1}{2} \left(\frac{\partial u_i}{\partial x_j} + \frac{\partial u_j}{\partial x_i} \right) \quad (2)$$

and ρ is the density, h is the enthalpy, P is the pressure, u_i is the velocity and λ and μ are the coefficients of thermal conductivity and molecular viscosity. Noting that

$$\frac{DP}{Dt} = R\rho \frac{DT}{Dt} + RT \frac{D\rho}{Dt} \quad (3)$$

and using the relation $h = C_p T$ and the conservation of mass equation, Eq. (1) can be re-written as

$$\rho \frac{Dh}{Dt} = -(\gamma - 1) \rho h \frac{\partial u_i}{\partial x_i} + \gamma \left(-\frac{\partial q_i}{\partial x_i} + \phi \right), \quad \gamma = C_p / C_v \quad (4)$$

where C_p and C_v are the specific heats at constant pressure and constant volume.

The mean energy equation follows from Eq. (1) as

$$\frac{\partial}{\partial t} (\bar{\rho} \tilde{h}) + \frac{\partial}{\partial x_i} (\bar{\rho} \tilde{h} \tilde{u}_i) = \frac{D\bar{P}}{Dt} - \frac{\partial \bar{q}_i}{\partial x_i} + \bar{\phi} - \frac{\partial}{\partial x_j} (\overline{\rho h'' u_j''}) \quad (5)$$

where

$$\bar{\phi} = \bar{t}_{ij} \frac{\partial \tilde{u}_i}{\partial x_j} + \bar{\rho} \epsilon; \quad \epsilon = \nu \zeta \quad (6)$$

where ν is the kinematic viscosity and ζ is the enstrophy.

Equation (4) was the starting point for deriving an equation for the enthalpy variance and its dissipation rate. The exact equations are given in the Appendix, while the modeled equations are:

$$\begin{aligned} \frac{\partial}{\partial t} (\rho \tilde{h}''^2 / 2) + \frac{\partial}{\partial x_j} (\bar{\rho} \tilde{u}_j \tilde{h}''^2 / 2) &= \frac{\partial}{\partial x_j} \left[\rho (\gamma \alpha + \alpha_t C_{h,2}) \frac{\partial (\tilde{h}''^2 / 2)}{\partial x_j} \right] \\ &+ 2\mu \gamma \bar{S}_{ij} \left[\frac{\partial}{\partial x_j} (q_{t,i} / \rho) + \frac{\partial}{\partial x_i} (q_{t,j} / \rho) \right] - \frac{4}{3} \mu \gamma \bar{S}_{kk} \frac{\partial}{\partial x_j} (q_{t,j} / \rho) \\ &- (\gamma - 1) \bar{\rho} \tilde{h}''^2 \frac{\partial \tilde{u}_i}{\partial x_i} - q_{t,i} \frac{\partial \tilde{h}}{\partial x_i} + 2 C_{h,4} \gamma \mu \sqrt{\tilde{h}''^2} \zeta - \bar{\rho} \epsilon_h \end{aligned} \quad (7)$$

where

$$q_{t,j} = -\bar{\rho} \alpha_t \frac{\partial \tilde{h}}{\partial x_j}$$

$$\begin{aligned}
\alpha_t &= 0.5[C_h k \tau_h + \nu_t / 0.89] \\
\tau_h &= \overline{\tilde{h}''^2} / \epsilon_h \\
\epsilon_h &= \alpha \overline{\left(\frac{\partial \tilde{h}''}{\partial x_i} \right)^2}
\end{aligned} \tag{8}$$

and where ϵ_h is the rate of dissipation of the enthalpy variance, α is the diffusivity, and

$$\nu_t = C_\mu k^2 / \nu \zeta \equiv C_\mu k \tau_k$$

is the turbulent kinematic viscosity.

The modeled equation for the dissipation of enthalpy variance is

$$\begin{aligned}
\frac{\partial}{\partial t} (\bar{\rho} \epsilon_h) + \frac{\partial}{\partial x_j} (\bar{\rho} \tilde{u}_j \epsilon_h) &= -\bar{\rho} \epsilon_h \left(C_{h,5} b_{jk} - \frac{\delta_{jk}}{3} \right) \frac{\partial \tilde{u}_j}{\partial x_k} \\
&+ C_{h,6} \bar{\rho} k \frac{\partial \sqrt{\tilde{h}''^2}}{\partial x_j} \frac{\partial \tilde{h}}{\partial x_j} + \frac{\partial}{\partial x_j} \left[(\gamma \alpha + C_{h,7} \alpha_t) \frac{\partial \epsilon_h}{\partial x_j} \right] \\
&+ C_{h,8} \frac{q_{t,j}}{\tau_h} \frac{\partial h}{\partial x_j} - \gamma \rho \epsilon_h \left[\frac{C_{h,9}}{\tau_h} + \frac{C_{h,10}}{\tau_k} \right] \\
&+ C_{h,11} \epsilon_h \left[\frac{D\rho}{Dt} + \frac{\rho}{P} \max \left(\frac{DP}{Dt}, 0.0 \right) \right]
\end{aligned} \tag{9}$$

with

$$b_{ij} = \frac{\tau_{ij}}{\bar{\rho} k} + \frac{2}{3} \delta_{ij}, \quad \tau_{ij} = -\overline{\rho u_i'' u_j''} \tag{10}$$

The constants, $C_h, \dots, C_{h,11}$ are model constants and are given in Table 1. The turbulent Prandtl number is defined as

$$Pr_t = \nu_t / \alpha_t \tag{11}$$

The choice of α_t merits further elaboration. It was indicated in Ref. 4 that experiments in simple shear flows showed that the appropriate time scale for temperature fluctuations is proportional to the arithmetic average of τ_h

and τ_k . This is the basis for the modeling indicated in Eq. 8. It should be noted that, traditionally^{3,4}, the time scale of temperature fluctuations is taken as the geometric average of τ_h and τ_k .

2. Numerical Procedure

A modification of REACTMB¹², a code that has been developed at North Carolina State University over the last several years, is used to set constants and validate the model. It employs a second order ENO upwind method based on the Low-diffusion Flux-Splitting of Edwards¹³ to discretize the inviscid fluxes while central differences are employed for the viscous and diffusion terms. Planar relaxation is used to advance the solution in time.

III. Results and Discussion

The solutions computed using the model are shown first with the data from the 15 deg ramp experiment of Coleman and Stollery. In this experiment no flow separation was indicated. The remaining comparisons will be made with Schülein two-dimensional flow measurements for deflection angles β of 10 and 14 degrees. Flow separation was observed for both of these angles.

The free stream conditions for the experiments of Coleman and Stollery are: $M=9.2$, $Re=47 \times 10^6/m$, $T_o=1070K$, $T_\infty=64.5K$ and $T_w=295K$. It has been shown in Ref. 11 that use of 241×141 Cartesian grid with constant spacing in the x (flow) direction and geometric spacing in the y (normal) direction resulted in a grid resolved solution and this grid is employed in the present calculations. Values of y^+ are less than 0.2. Figures 1 and 2 compare the pressure distribution and wall heat flux for constant and variable Prandtl number calculations. As is seen from Fig. 1 the pressure distribution is essentially independent of the turbulent Prandtl number. The variable Prandtl number calculations are in good agreement with experiment in the pressure rise region and both calculations underpredict the heat flux in the recovery region. The recovery region has always been difficult to predict using Reynolds Averaged Navier-Stokes (RANS) equations. Better results are obtained when a hybrid Large Eddy Simulation/Reynolds Averaged Navier-Stokes (LES/RANS) formulation is employed¹⁴.

The experimental setup of the Schülein experiment is shown in Fig. 3. A shock generator is mounted on the upper wall and the resultant oblique shock wave interacts with the turbulent boundary layer growing on the flat plate along the lower wall. The free-stream conditions in the test section were: $M=5$, unit Reynolds number = $37 \times 10^6/m$, $T_o=410K$, $P_o=2.12$ MPa and a wall temperature of 300 ± 5 K. Three grids are used in this investigation: a coarse

151×141, medium 243×141, and fine 301×141. Results employing the medium and fine gave grid independent solutions. All results presented below employ the fine grid.

The calculations were limited to a region ahead of the point where the reflected shock impinges on the upper surface. This assumption makes it possible to use an extrapolation boundary condition at the outflow. Without this assumption, one would be forced to consider the upper wall in the calculations.

Figures 4-6 compare predictions of surface pressure, wall shear stress and wall heat flux while Figs. 7 and 8 compare temperature and velocity at $x = 376$ mm for $\beta=10$ deg. It is seen from Figs. 4 and 5 that the results are almost identical for both constant and variable turbulent Prandtl numbers. Both calculations underpredict the pressure in the separated region.

The oil-film interferometry technique cannot be used to determine the extent of the separated region. Instead, conventional oil-film visualization was used to deduce the start and end of the separated region. It is seen from Fig. 5 that the extent of separation is well predicted. However, some discrepancies are noted in predicting the wall shear stress in the recovery region. The calculations are consistent with the fact that the τ_w should decrease in the constant pressure region. As is seen from Fig. 4, measurements suggest that the pressure is approximately constant after $x=370$ mm station. It is not clear why the experiment indicates in the wall shear stress downstream of this location.

Figure 6 shows that constant Prandtl number calculations overpredict peak heating by a factor of 2. As is seen from the figure, the variable Pr_t results represent a definite improvement over constant Pr_t results. The slight oscillation in the calculated results are attributed to the fact that the shock does not lie along a grid line. The oscillations can be reduced or eliminated by increasing the numerical damping of the numerical scheme. As is seen from Fig. 9, the convergence history indicates that the small oscillations are not an indication of lack of iterative convergence.

Figures 7 and 8 show that both temperature and velocity profile are in fair good agreement with experiment. The fact that the variable Prandtl number formulation results in more realistic heat flux estimates is a direct result of the fact that temperature distribution for the variable Prandtl number is in better agreement with experiment near the wall.

Figure 10 shows a contour plot of Pr_t in the neighborhood of the separated region. In the separated region, Pr_t is about 1.0. As a result, both constant and variable Pr_t solutions yield similar results as indicated in Fig. 6. Downstream of that region, Pr_t is greater than 1, which is responsible for the reduction in the heat flux compared

with the constant Pr_t results. Outside the boundary layer, the first term in the expression for α_t is much less than $\nu_t/0.89$ and thus Pr_t asymptotes to 1.78. This has no real physical significance because the temperature is essentially constant outside the boundary layer.

Figures 11-17 compare similar predictions for the $\beta = 14$ degree case. Similar remarks can be made regarding this case. Experimental measurements show more oscillations in the data.

IV. Concluding Remarks

A new approach has been developed for calculating the turbulent Prandtl number as part of the solution. The approach is based on a two-equation model for the enthalpy variance and its dissipation rate. All of the correlations that appear in the exact equations that govern the enthalpy variance and its dissipation rate are modeled in order to ensure the incorporation of relevant physics into the model equations.

The new formulation is used to study flows characterized by shock wave/boundary layer interactions. In general heat flux calculations showed dramatic improvements while surface pressures and wall shear stress were unaffected by the variable Prandtl number formulation.

When comparing pressure, skin friction and heat flux measurements, the highest errors are associated with heat flux measurements. Despite the discrepancy between computed and measured heat flux, the key to bridging the gap between theory and experiment in flows dominated by shock wave/boundary layer interactions is to employ better measurement techniques and use variable turbulent Prandtl number formulations. It has always been difficult for RANS solutions to reproduce the correct flow behavior in the recovery regions. Hybrid LES/RANS approaches have better prediction capabilities and should be used in future investigations.

V. Acknowledgment

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VI. References

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VII. Appendix

1. Exact Equation for Enthalpy Variance:

$$\frac{\partial}{\partial t} (\overline{\rho \tilde{h}''/2}) + \frac{\partial}{\partial x_j} [\overline{\rho \tilde{u}_j \tilde{h}''/2}] = -\overline{\rho h'' u_j''} \frac{\partial \tilde{h}}{\partial x_j} - \frac{\partial}{\partial x_j} [\overline{\rho u_j'' h''/2}] + \overline{h'' S_h} \quad (1)$$

where

$$\overline{h'' S_h} = h'' \frac{Dp}{Dt} - h'' \frac{\partial \xi_i}{\partial x_i} + \overline{h'' \phi} \quad (2)$$

2. Exact Equation for the Dissipation Rate of Enthalpy Variance:

$$\begin{aligned} \rho \frac{D}{Dt} \epsilon_h + 2\rho\alpha \frac{\partial h''}{\partial x_j} \frac{\partial h''}{\partial x_k} \frac{\partial \tilde{u}_j}{\partial x_k} + 2\rho\alpha \frac{\partial u_j''}{\partial x_k} \frac{\partial h''}{\partial x_k} \frac{\partial \tilde{h}}{\partial x_j} + 2\rho\alpha u_j'' \frac{\partial h''}{\partial x_k} \frac{\partial^2 \tilde{h}}{\partial x_j \partial x_k} \\ + u_j'' \frac{\partial}{\partial x_j} \left[\overline{\rho\alpha \left(\frac{\partial h''}{\partial x_k} \right)^2} \right] + 2\rho\alpha \frac{\partial u_j''}{\partial x_k} \frac{\partial h''}{\partial x_k} \frac{\partial h''}{\partial x_j} \\ = 2\rho\alpha \frac{\partial h''}{\partial x_k} \frac{\partial}{\partial x_k} \left[\frac{S_h'}{\rho} - \frac{1}{\rho} \frac{\partial}{\partial x_j} (\overline{\rho u_j'' h''}) \right] \end{aligned} \quad (3)$$

where

$$S'_h = -\frac{\partial q_i}{\partial x_i} + \phi' \quad (4)$$

Table 1 – Model Constants

Ch	Ch,2	Ch,4	Ch,5	Ch,6	Ch,7	Ch,8	Ch,9	Ch,10	Ch,11
0.0648	0.5	- 0.4	0- 0.5	- 0.12	1.45	0.7597	0.87	0.25	0.5

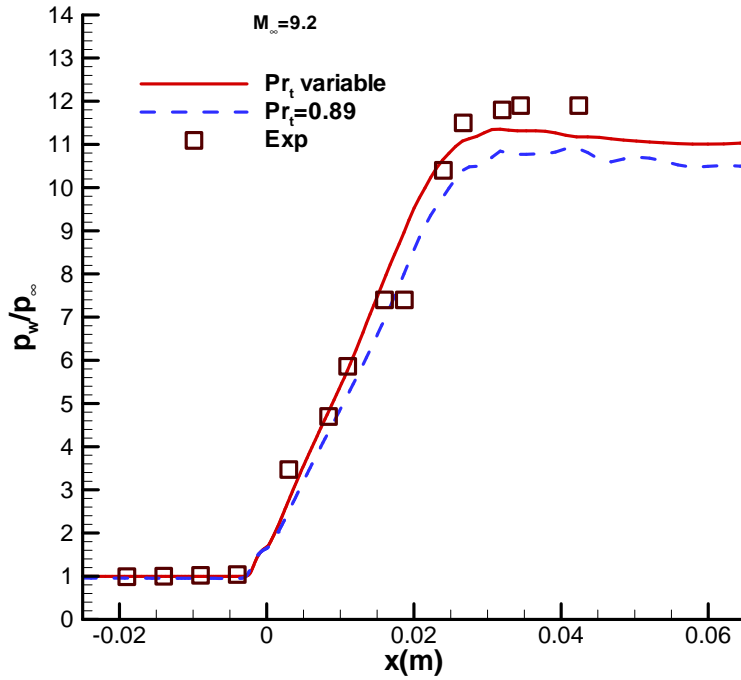


Fig.1 Computed and measured pressure distribution, 15 deg ramp

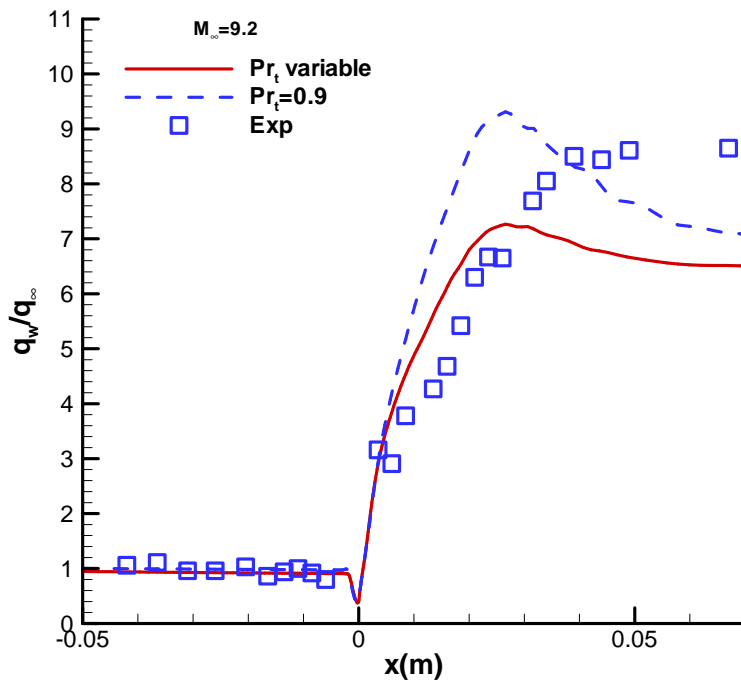


Fig.2 Computed and measured heat flux, 15 deg ramp

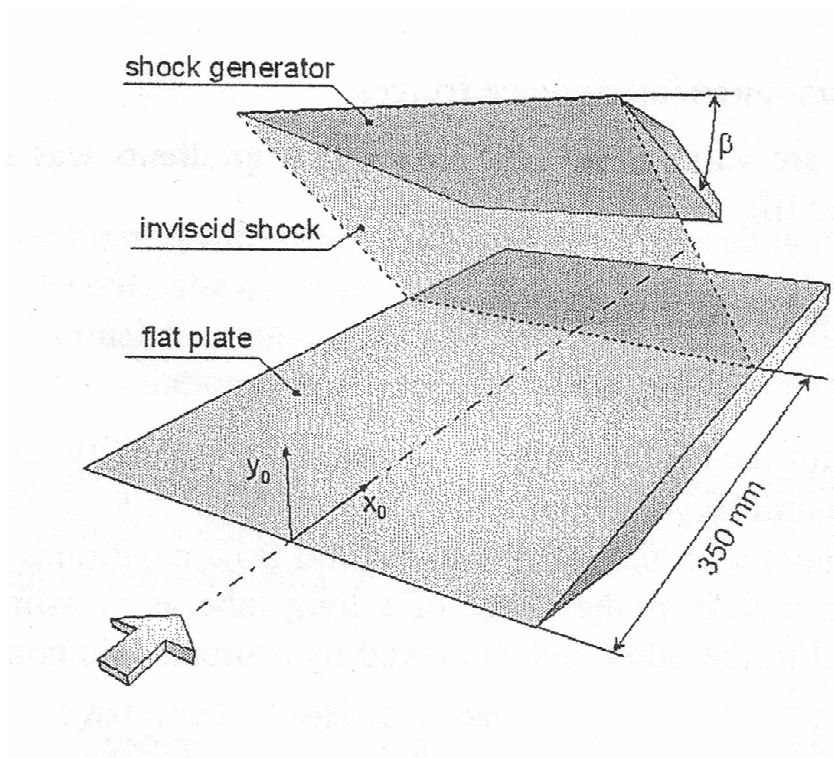


Fig.3 Schematic of shock-wave/boundary layer interaction experiment.

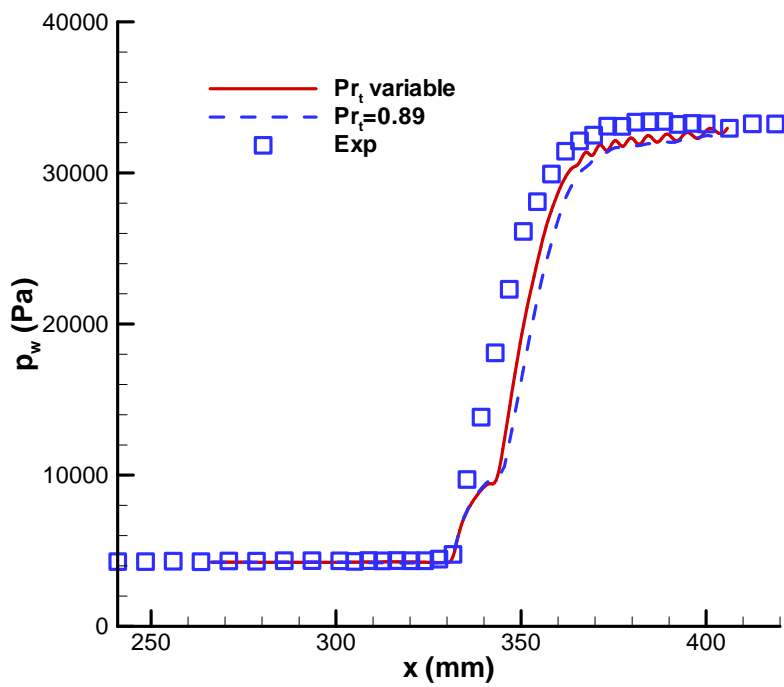


Fig.4 Computed and measured wall pressure, $\beta=10$ deg

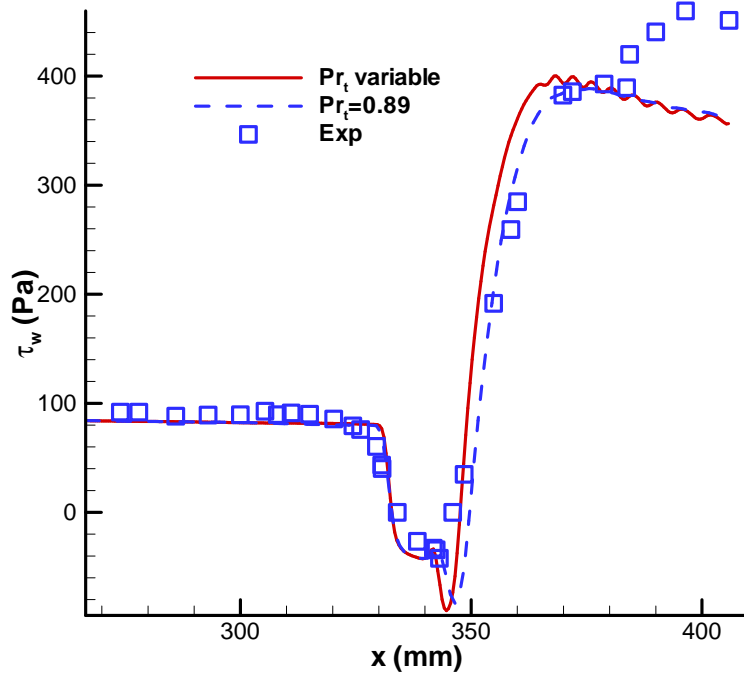


Fig. 5 Computed and measured wall shear stress, $\beta=10$ deg

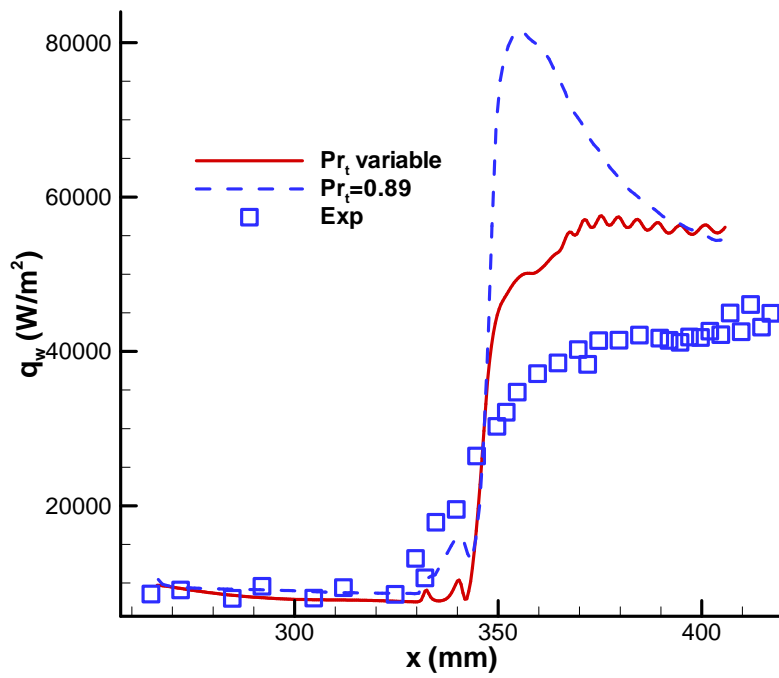


Fig.6 Computed and measured wall heat flux, $\beta=10$ deg

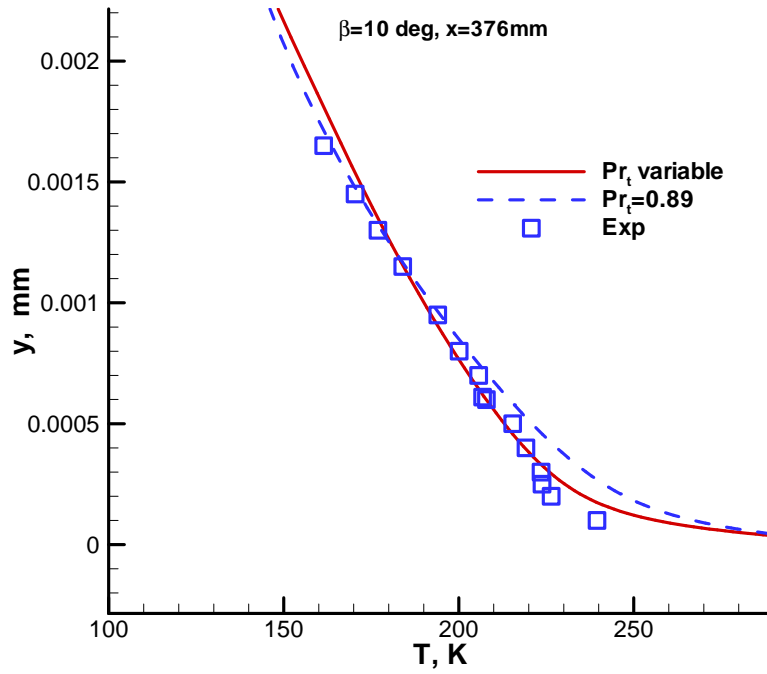


Fig. 7 Computed and measured temperature profile at $x=376$ mm, $\beta=10$ deg

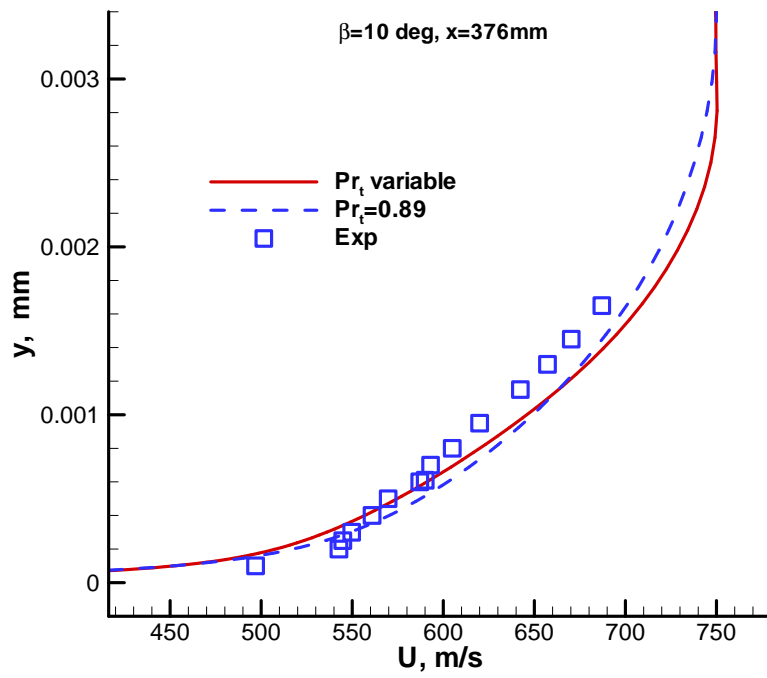


Fig. 8 Computed and measured velocity profile at $x=376$ mm, $\beta=10$ deg

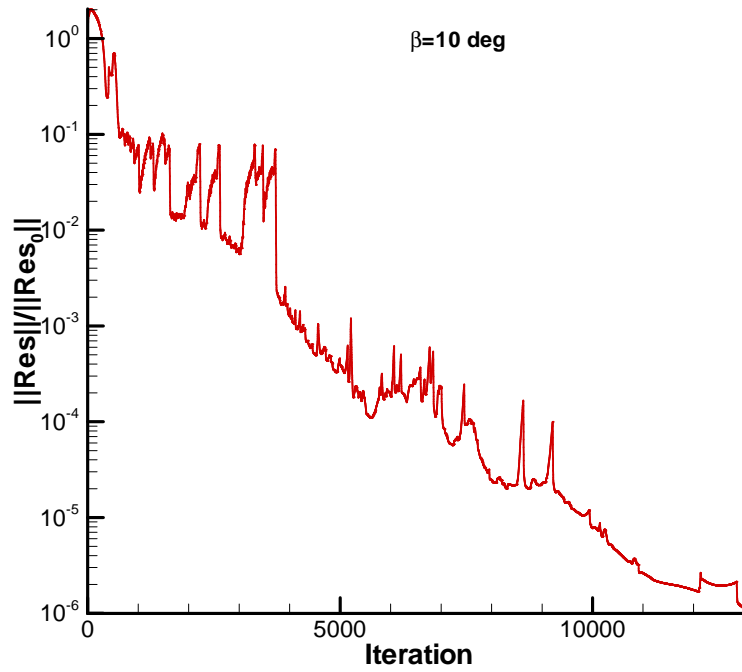


Fig.9 Convergence history, $\beta=10$ deg

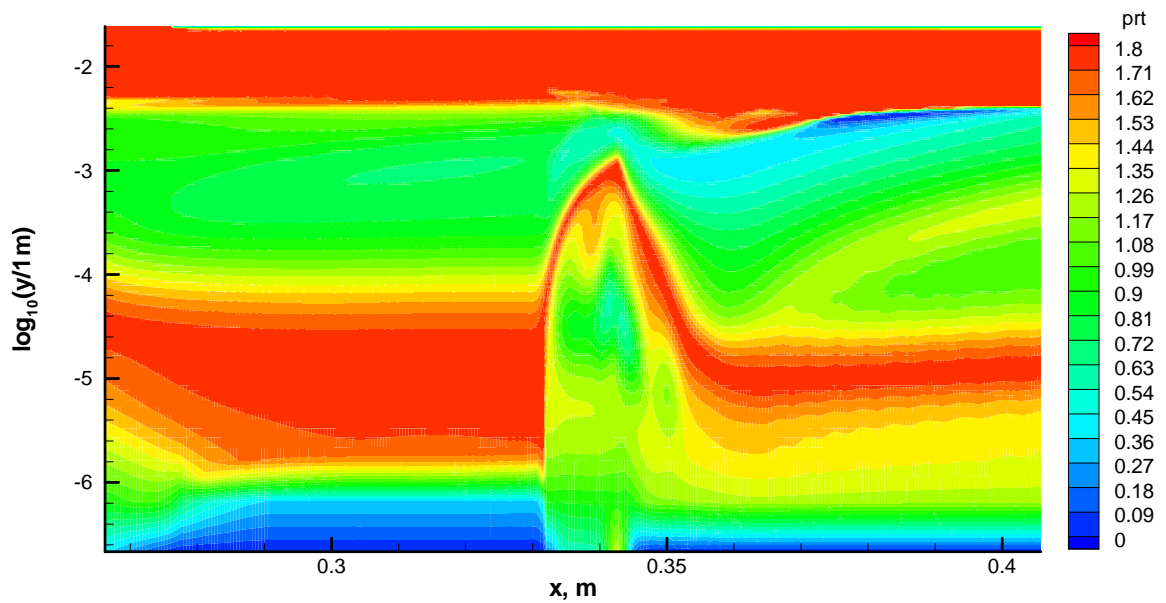


Fig.10 Contours of turbulent Prandtl number, $\beta=10$ deg

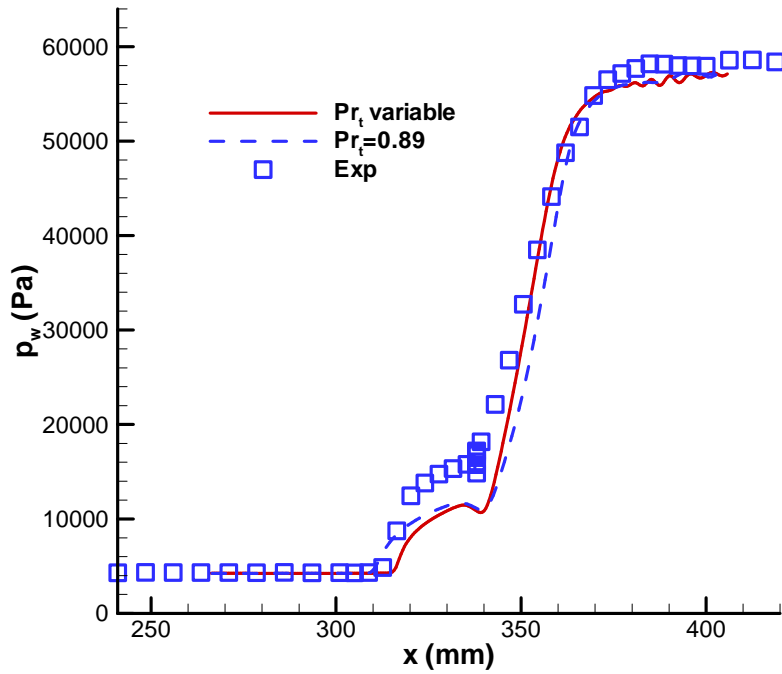


Fig.11 Computed and measured wall pressure, $\beta=14$ deg

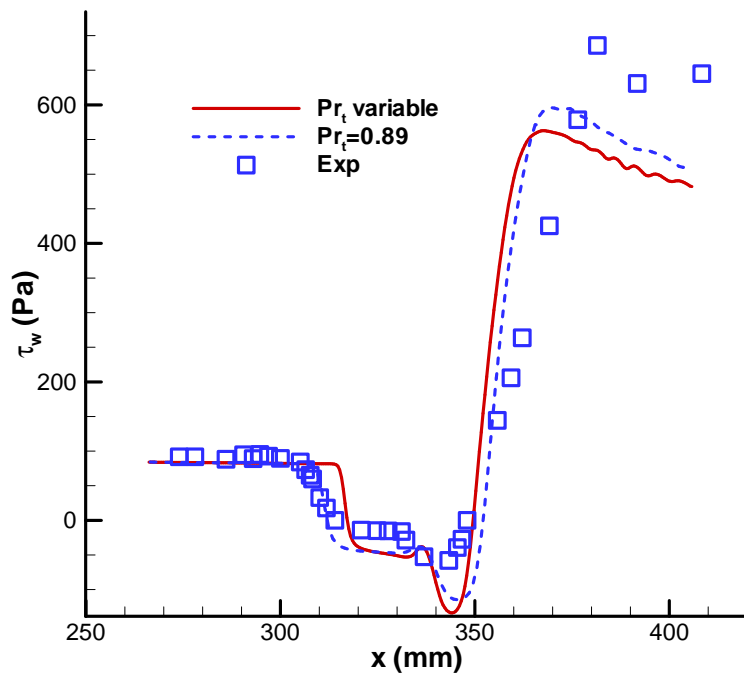


Fig.12 Computed and measured wall shear stress, $\beta=14$ deg

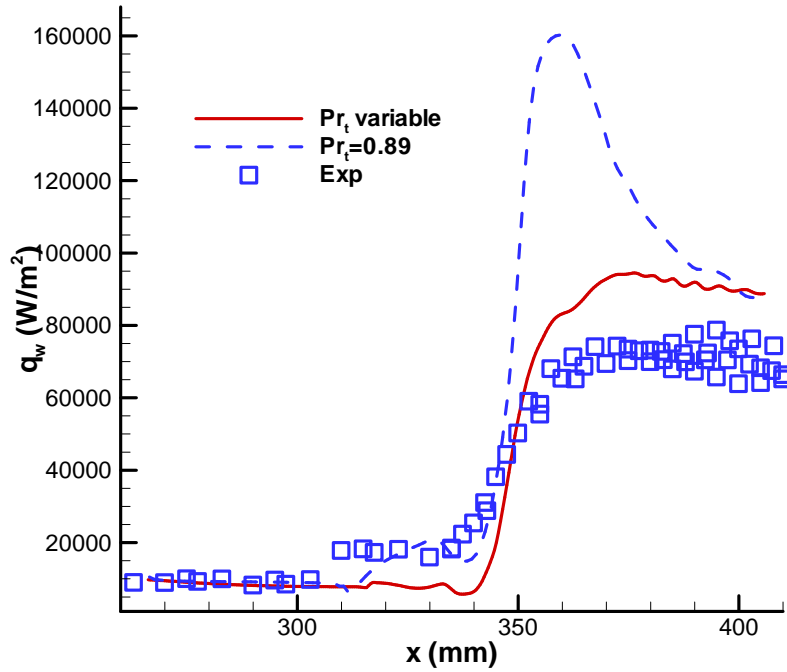


Fig.13 Computed and measured wall heat flux, $\beta=14$ deg

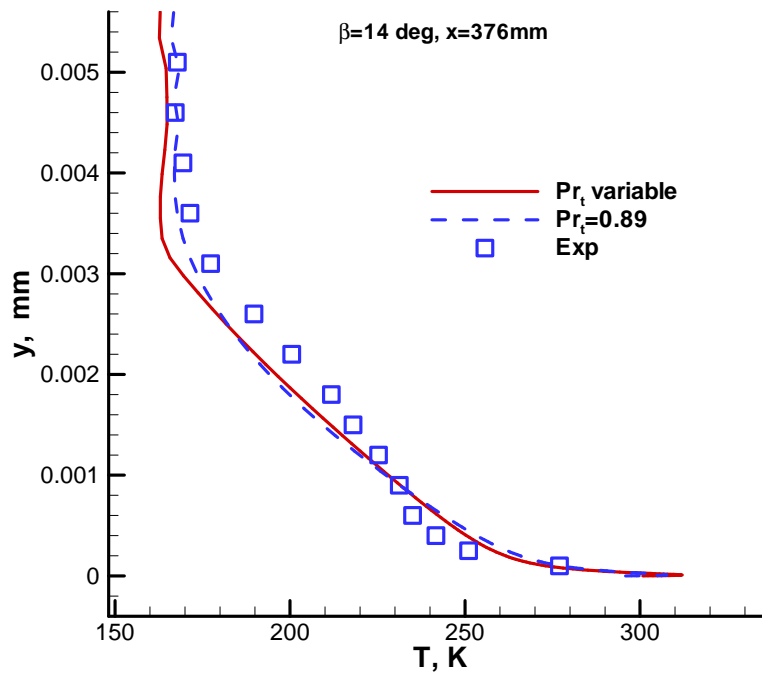


Fig.14 Computed and measured temperature profile, at $x=376$ mm, $\beta=14$ deg

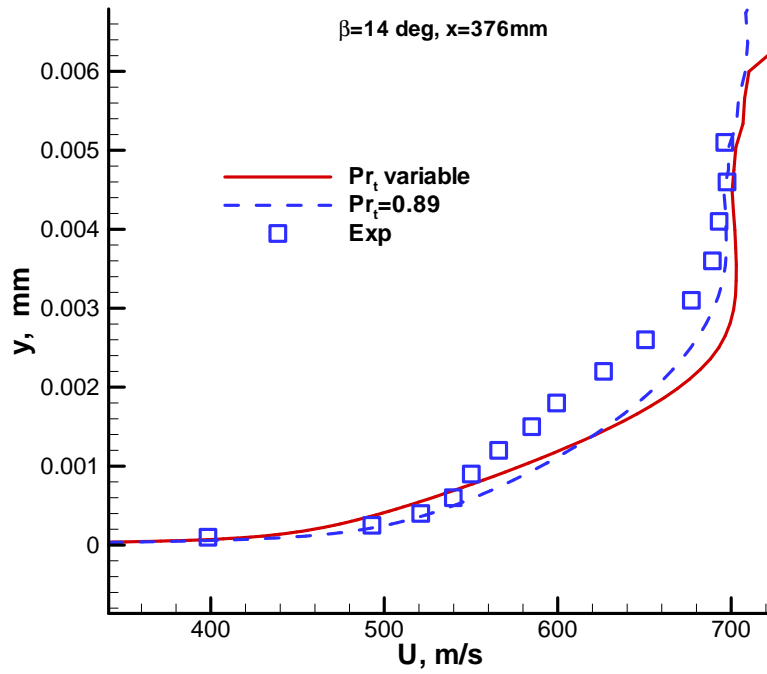


Fig.15 Computed and measured velocity profile, at $x=376$ mm, $\beta=14$ deg

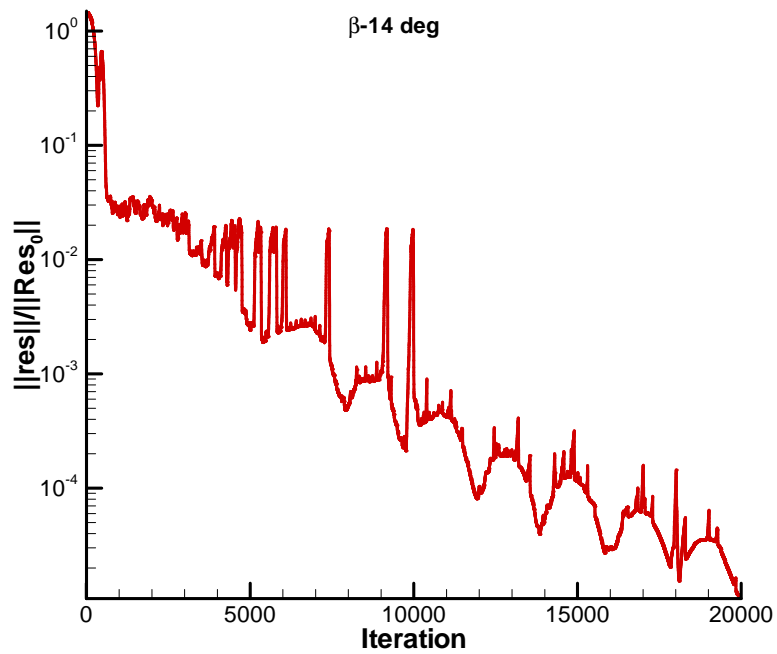


Fig.16 Convergence history, $\beta=14$ deg

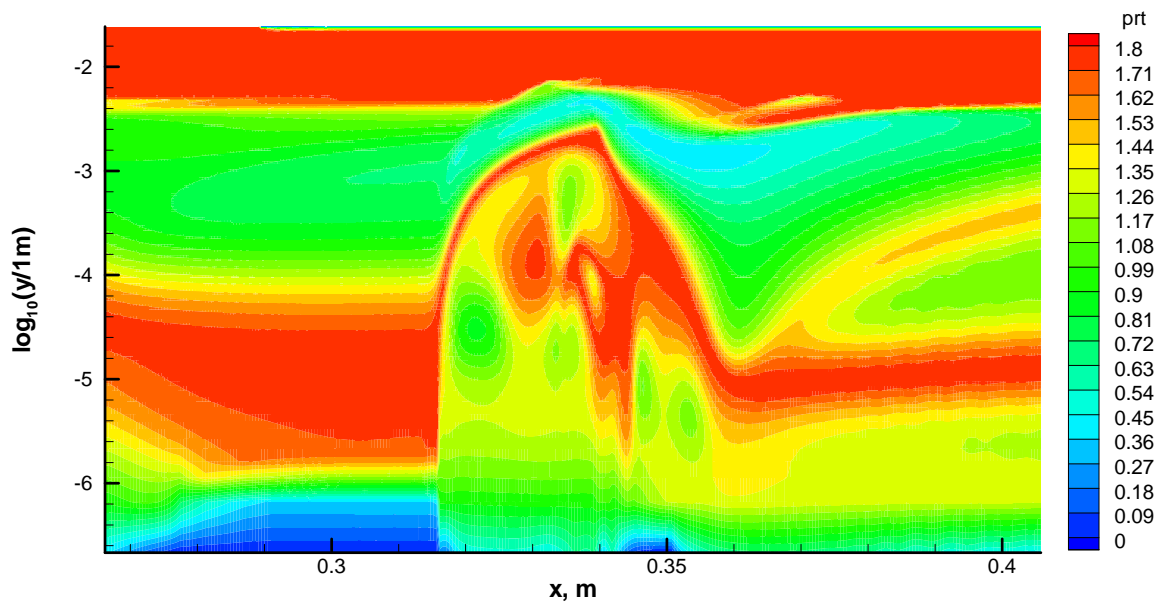


Fig.17 Contours of turbulent Prandtl number, $\beta=14$ deg