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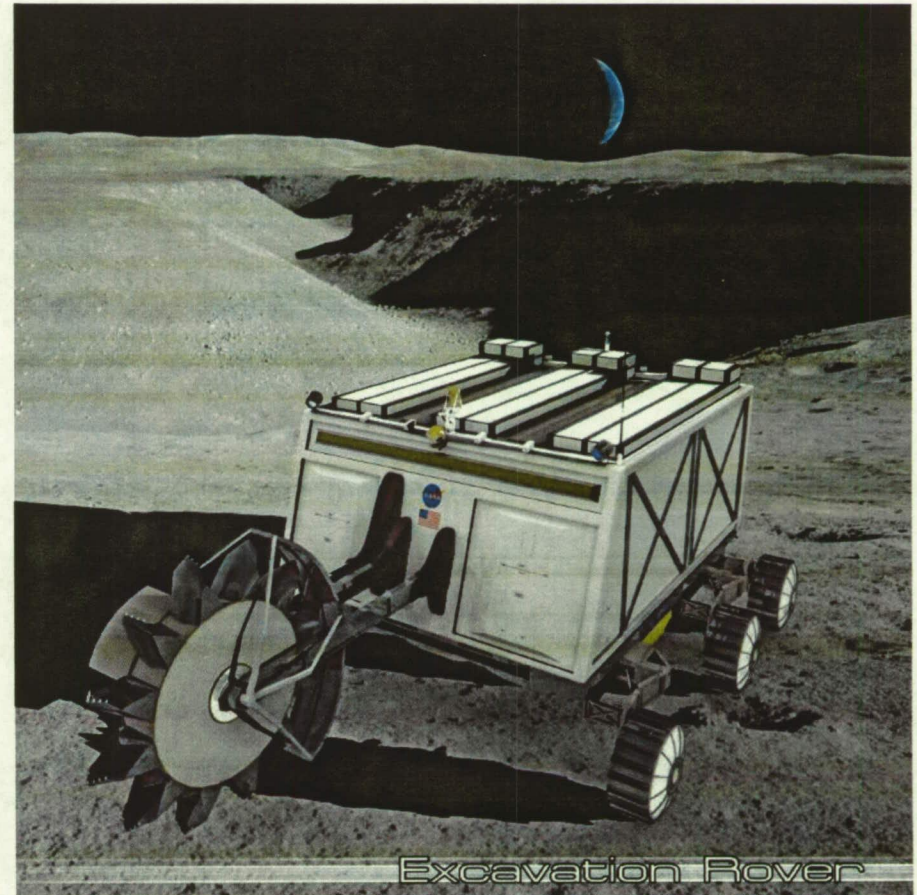


# **Development of an Integrated RVC-LWRD System for RESOLVE**



## ISRU Demonstration

- As exploration reaches new destinations, we have a greater need to live off the land
- ISRU plays a role in future mission architectures
  - Manufacture of propellants
  - Manufacture of life support consumables
  - Radiation shielding
- Since ISRU plays a key role, it would be extremely beneficial to demonstrate technology as early as possible





## NASA's Exploration Systems Architecture Study -- Final Report

### 4.2.1.2.4 Key Capabilities and Core Technologies

- Previous NASA architecture studies have included such destinations as the Moon, near-Earth asteroids, Mars, and the moons of Mars. A review of these previous studies illustrates the existence of a **common thread of key capabilities and core technologies** that are similar between destinations...
- • **ISRU**: Technologies for “living off the land” are needed to support a long-term strategy for human exploration. Key ISRU challenges include **resource identification and characterization**, excavation and extraction processes, **consumable maintenance and usage capabilities**, and advanced concepts for manufacturing other products from local resources;

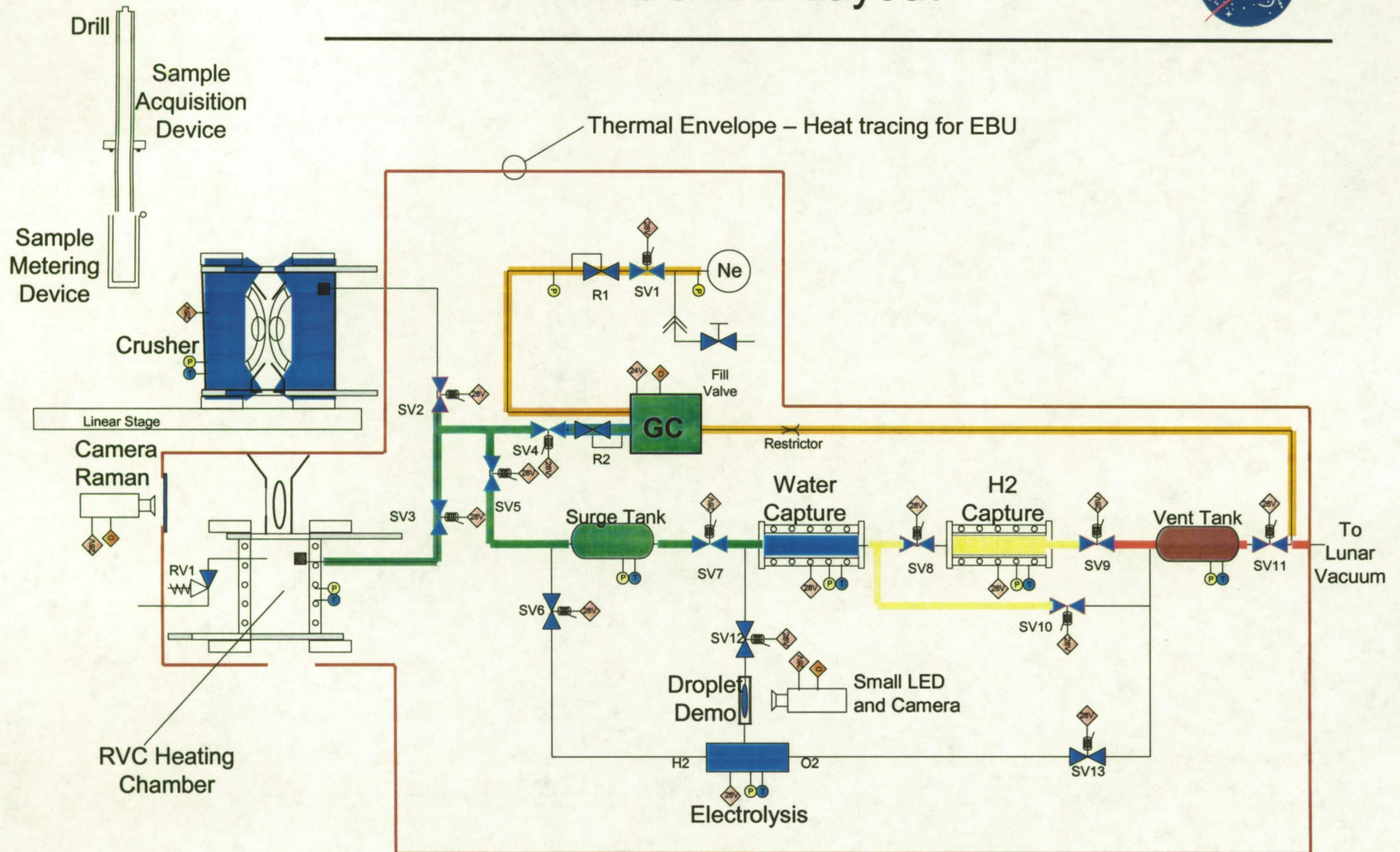


# **Brief RESOLVE Overview**



- **RESOLVE - Regolith & Environment Science and Oxygen & Lunar Volatile Extraction**
- RESOLVE incorporates 5 modules
  - EBRC (Excavation and Bulk Regolith Characterization)
  - ERPC (Environment and Regolith Physical Characterization)
  - ROE (Regolith Oxygen Extraction)
  - RVC (Regolith Volatile Characterization)
  - LWRD (Lunar Water Resource Demonstration)
- Goal – identify and quantify volatiles, demonstrate ISRU, engage the public interest in 'living off the land' technology

# RESOLVE Layout



## RESOLVE Operational Procedure



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- Evaluation of system flow
  - Loop flow
    - ☞ Increase capture efficiency, but also increase time required to run the system
  - Straight flow
    - ☞ Loss of some efficiency but decrease operational time
  - Timing of solenoid valves
    - ☞ Length of time open
    - ☞ Time between openings

# Model of system



- Model of gas moving through system to provide insight into overall operation of system
- Pressures equalize with each valve opening (assume ideal gas) and calculating resulting pressure if/when adsorption occurs

**HOW TO READ THE TABLE**

Description	LWRD Component					Mass of H2O/H2 absorbed
	Oven	Surge Tank	H2O bed	H2 Bed	Vent Tank	
Species Adsorbed (grams)			0.053566479	0.025156		
Initial Pressure (atm)	3.413663					
H2O (moles)	0.003375					
H2 (moles)	0.013403					
CO (moles)	0.000688					
SO2 (moles)	9.64E-05					
N2 (moles)	0.00158					
Total (moles)	0.000527					
Total (atm)	0.019669					
Pressure (atm)	2.275775	2.275775161				
H2O (moles)	0.00225	0.001124888				
H2 (moles)	0.004467809	0.004467809				
CO (moles)	0.000229199	0.000229199				
N2 (moles)	0.001053	0.000526511				
SO2 (moles)	0.000351	0.000175728				
Total (moles)	0.013113	0.00655628				
Initial Pressure (atm)		1.831256511	1.831256511			
H2O (moles)		0.000905168	0.00021972			
H2 (moles)		0.003595129	0.00087268			
CO (moles)		0.00043	4.47685E-05			
N2 (moles)		0.0005	6.27881E-06			
H2S (moles)		0.00042367	0.000102841			
SO2 (moles)		0.000141404	3.43243E-05			
Total (moles)		0.005275666	0.001280614			
Initial Pressure (atm)			0.714942477	0.714942		
H2O (moles)			1.01446E-05	1.18E-05		
H2 (moles)			0.000402922	0.00047		
CO (moles)			2.06699E-05	2.41E-05		
N2 (moles)			2.06699E-05	3.38E-06		
H2S (moles)			0.0005	5.54E-05		

**Annotations:**

- Oven is open to Surge tank:** Indicated by a curved arrow from the Oven column to the Surge Tank column.
- Initial values:** A bracket groups the initial values for the Oven, Surge Tank, and H2O bed columns.
- Surge tank is open to H2O Bed:** Indicated by a curved arrow from the Surge Tank column to the H2O bed column.
- Values after the vessels reach equilibrium:** A bracket groups the values for the Surge Tank, H2O bed, and H2 Bed columns.
- H2O is absorbed and H2O bed is open to H2 bed:** Indicated by a curved arrow from the H2O bed column to the H2 Bed column.
- Values after the vessels reach equilibrium:** A bracket groups the values for the H2O bed, H2 Bed, and Vent Tank columns.
- Mass of H2O/H2 absorbed:** A bracket groups the values for the H2O bed, H2 Bed, and Vent Tank columns.



## User Interface – Inputs

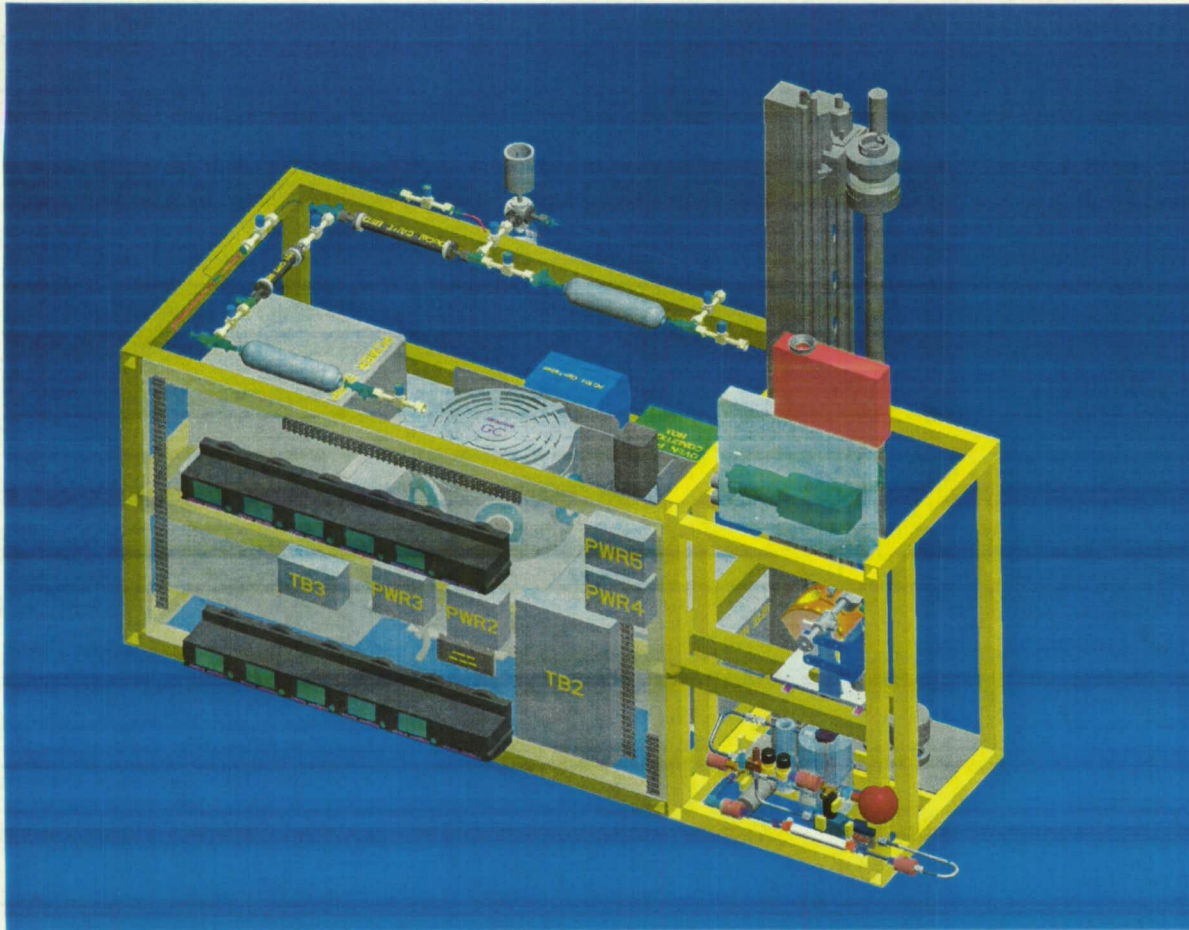
### Input Parameter Field

Parameter	Name	Value	Units	Description
<b>Options for Simulation</b>	Simulation Mode	Multiple Loops		
	Minimum H <sub>2</sub> O adsorbed	0.05	grams	If H <sub>2</sub> O adsorbed is not a constrain, this number should be large (i.e. 1e10)
	Minimum H <sub>2</sub> adsorbed	1.00E+10	grams	If H <sub>2</sub> adsorbed is not a constrain, this number should be large (i.e. 1e10)
<b>Oven</b>	Volume	200	cm <sup>3</sup>	Volume of vessel
	Temperature	423	K	Temperature of vessel
	Minimum Pressure	5	torr	Minimum pressure change to re-pressurize the vessel
<b>Surge Tank</b>	Volume	100	cm <sup>3</sup>	Volume of vessel
	Temperature	423	K	Temperature of vessel
	Minimum Pressure	5	torr	Minimum pressure change to re-pressurize the vessel
<b>Dessicant Bed</b>	Volume	20	cm <sup>3</sup>	Volume of vessel
	Temperature	298	K	Temperature of vessel
	Minimum Pressure	5	torr	Minimum pressure change to re-pressurize the vessel
	Mass of absorbant	5	gram	Mass of water absorbant
<b>Hydride Bed</b>	Volume	20	cm <sup>3</sup>	Volume of vessel
	Temperature	298	K	Temperature of vessel
	Minimum Pressure	5	torr	Minimum pressure change to re-pressurize the vessel
	Mass of absorbant	0.5	gram	Mass of metal hydride
<b>Vent Tank</b>	Volume	200	cm <sup>3</sup>	Volume of vessel
	Temperature	298	K	Temperature of vessel
	Minimum Pressure	5	torr	Minimum pressure change to re-pressurize the vessel
	H <sub>2</sub> O	900	µg/g-regolith	

Run

Clear

# Model of RESOLVE System

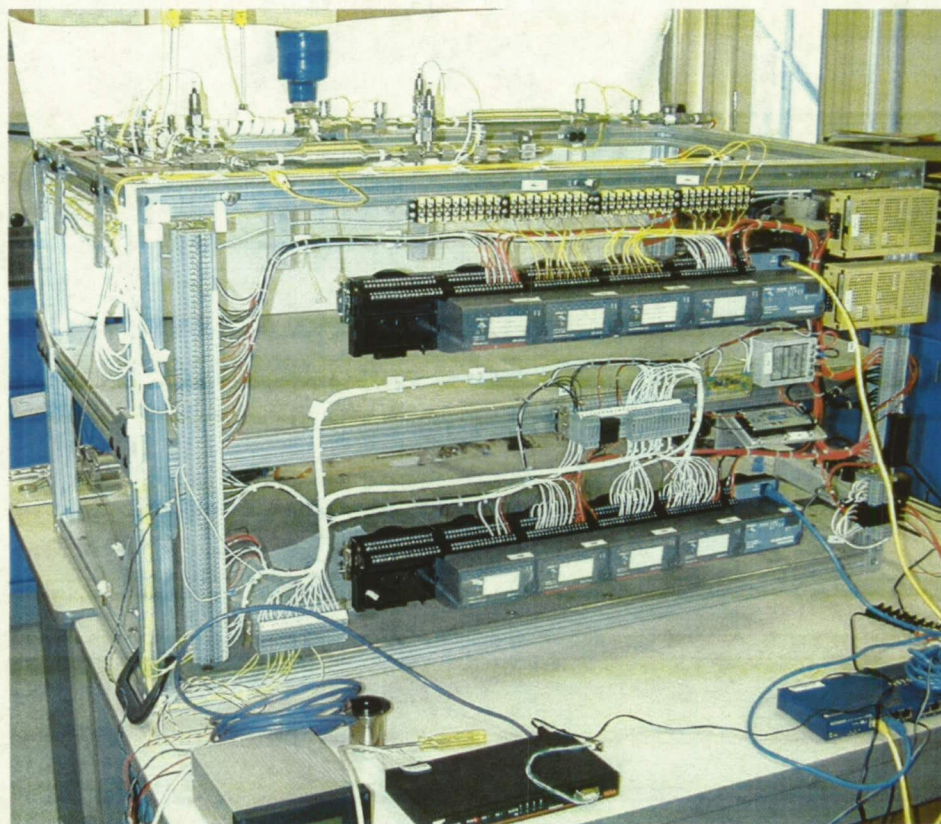


Pro-E drawings done by  
Victor Spencer - JSC

## Engineering Breadboard Unit (EBU)



- Hardware is being assembled
  - GRC – vibrofluidization oven
  - KSC – GC and LWRD
  - NORCAT – drill, crusher
  - JSC – ROE
  - JPL – CHAMP RAMAN
- First cut at an integrated system, finding the kinks
- RVC-LWRD will be integrated and tested at KSC
- Integration will be at JSC in March-April timeframe



# **Window Viewport for Imaging Chamber**



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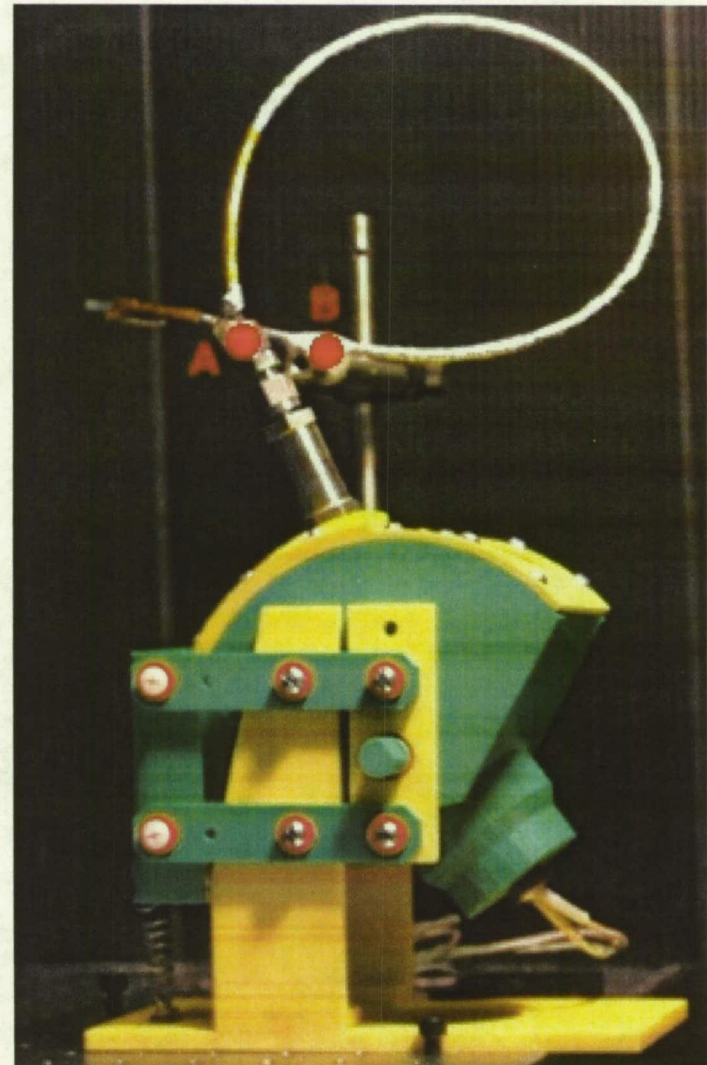
- The window for the RAMAN-CHAMP camera needs to be cleaned between samples to reduce contamination between the samples
- KSC's electrostatics group (led by Dr. Carlos Calle) has been developing dust removal techniques
- Transparent electrodes made of ITO (Indium Tin Oxide) will be placed on a sapphire window substrate, a voltage will be applied to clean the dust from the window surface
- Technology will be evaluated with real lunar soil

## Regolith Volatiles Characterization (RVC) Oven



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- Crushed regolith will be delivered through RAMAN viewing chamber into vibrofluidization oven
- Oven designed to evenly heat sample,
  - This is important for correlating the volatiles released with the temperature of the regolith
  - The temperature at which the volatiles are released will provide insight into the nature of their bonding
- GRC has done extensive testing on optimizing vibrofluidization parameters

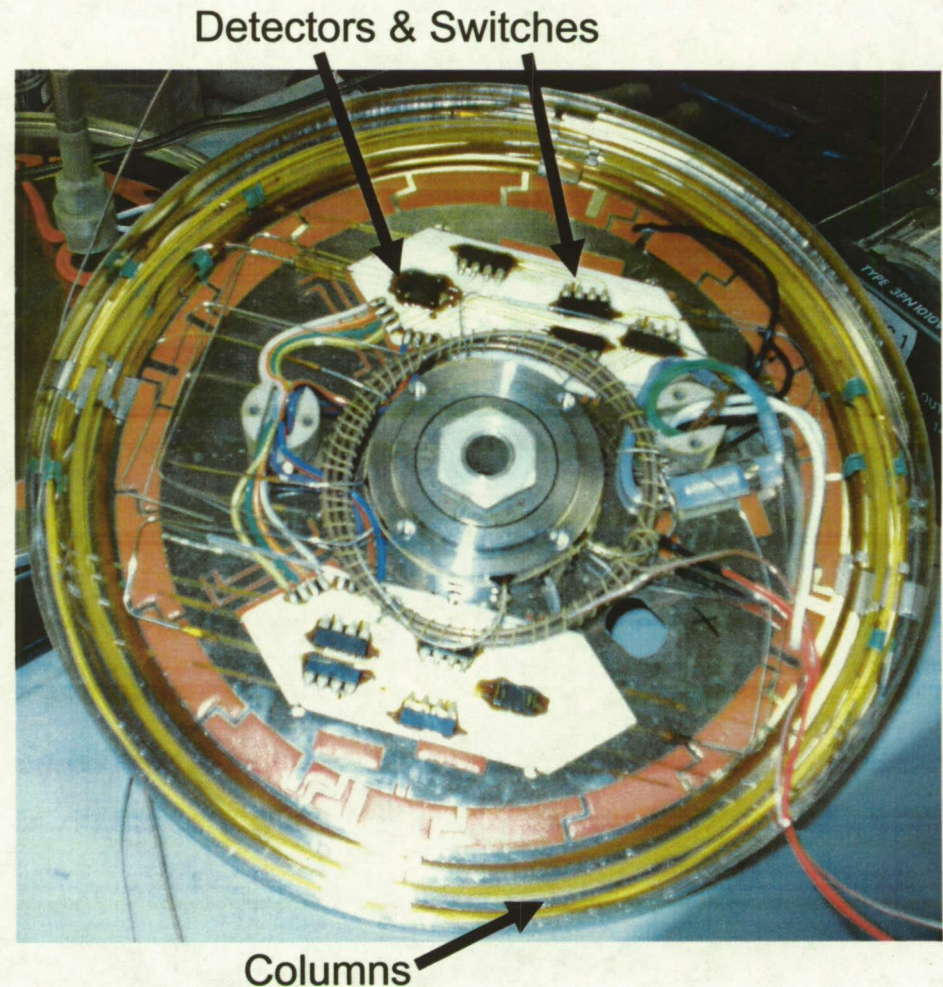


# RVC Gas Chromatograph



- COTS Siemens GC MicroSAM, converted to Neon carrier gas
- Modified in house to optimize separation and detection of  $H_2$ , He,  $H_2O$ ,  $O_2$ , CO,  $CO_2$ ,  $CH_4$ ,  $H_2S$
- Water detection was challenging but modifications and heat tracing have allowed for quantitative analysis of concentrations from 1% to 20% of vapor phase composition (current limitation of generation system)
- Water limit of detection corresponds to approximately 0.05 wt % in regolith
- Current testing
  - Optimization of flow
  - Column temperatures

## Analysis Module of GC

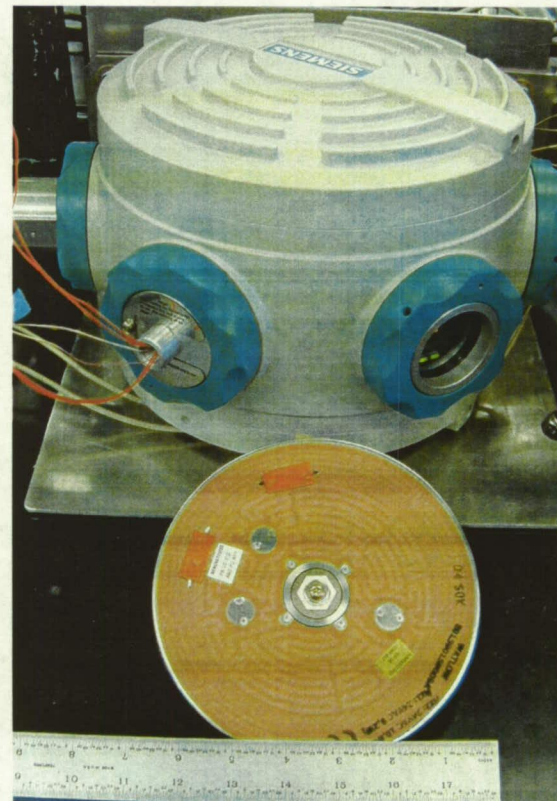
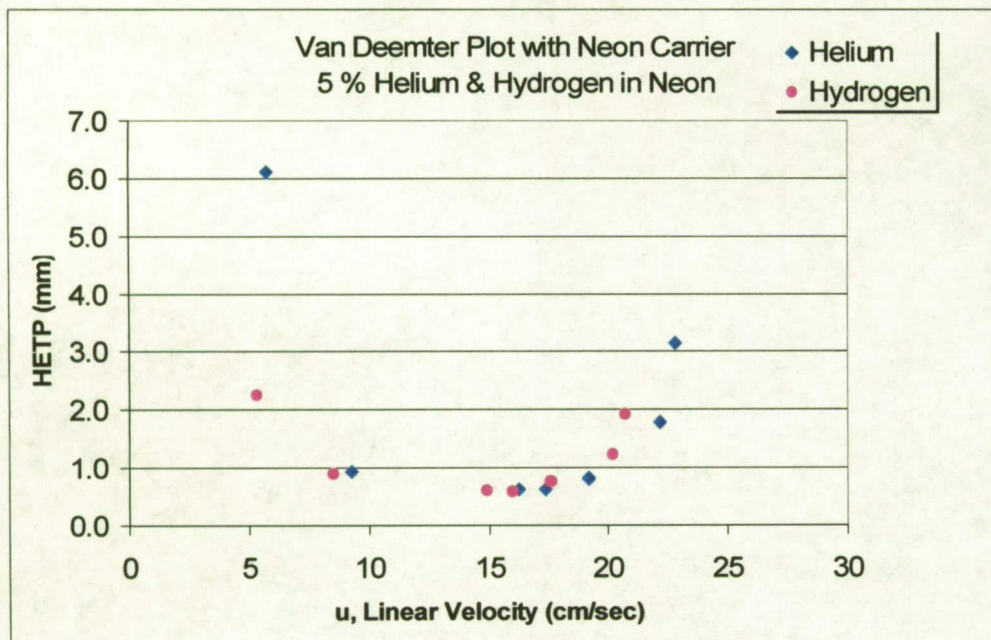


## RVC-GC



- Van Deemter plot generated to optimize pressure driven flows for best separation of components

- The lower the HETP value, the better the separation on the column (height equivalent of a theoretical plate)



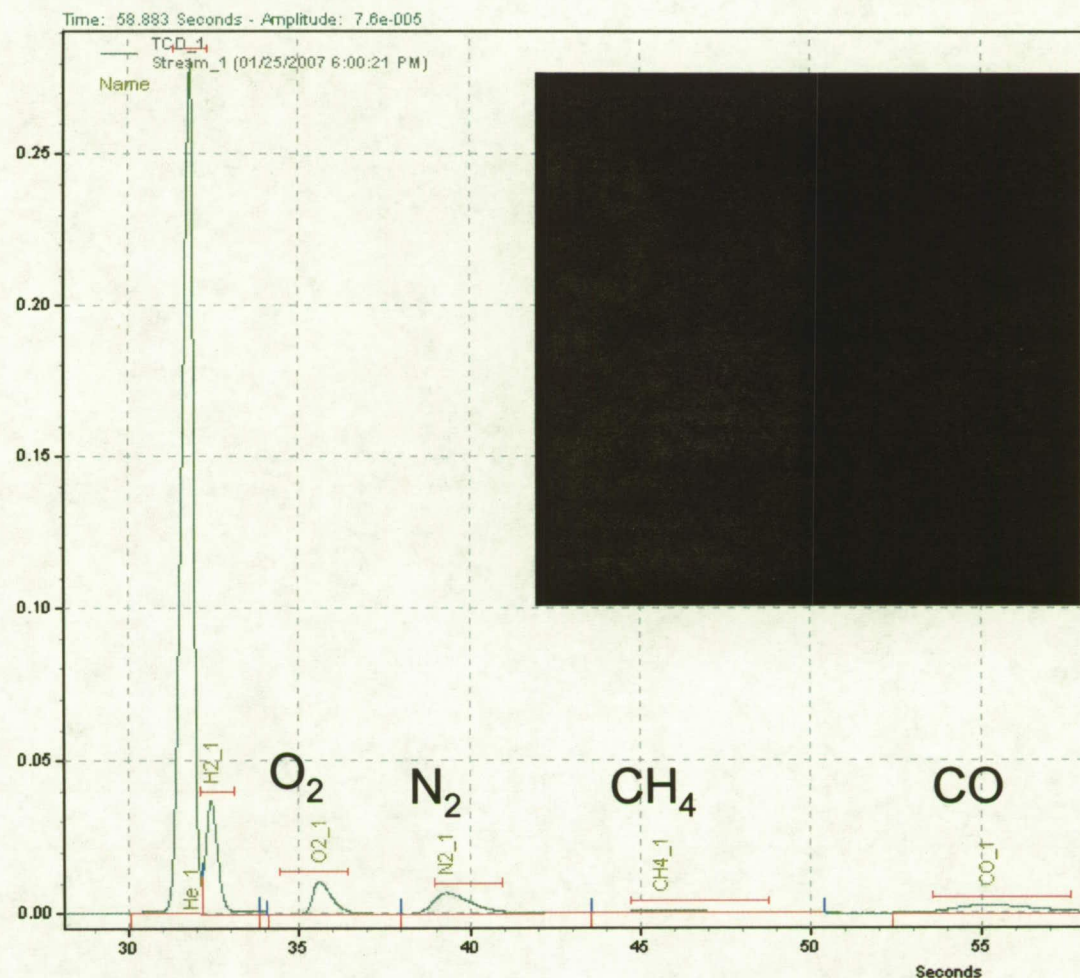
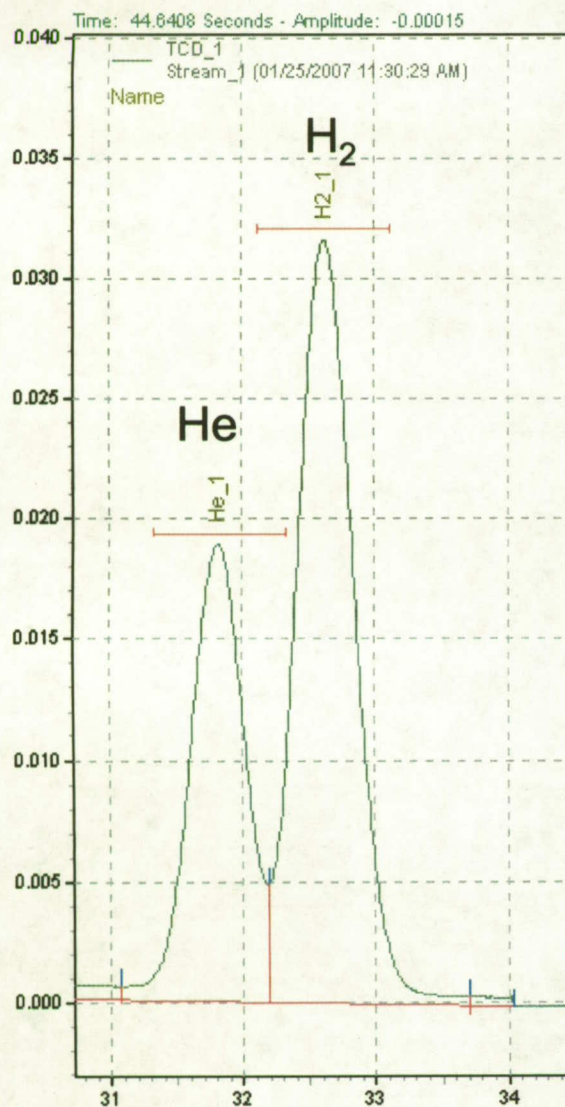
GC with  
explosion  
proof case

Analysis  
module

- MicroSAM GC (top) in factory designed case will be stripped and the analysis module (bottom) will be isolated for use in FPU

## Sample Chromatograms

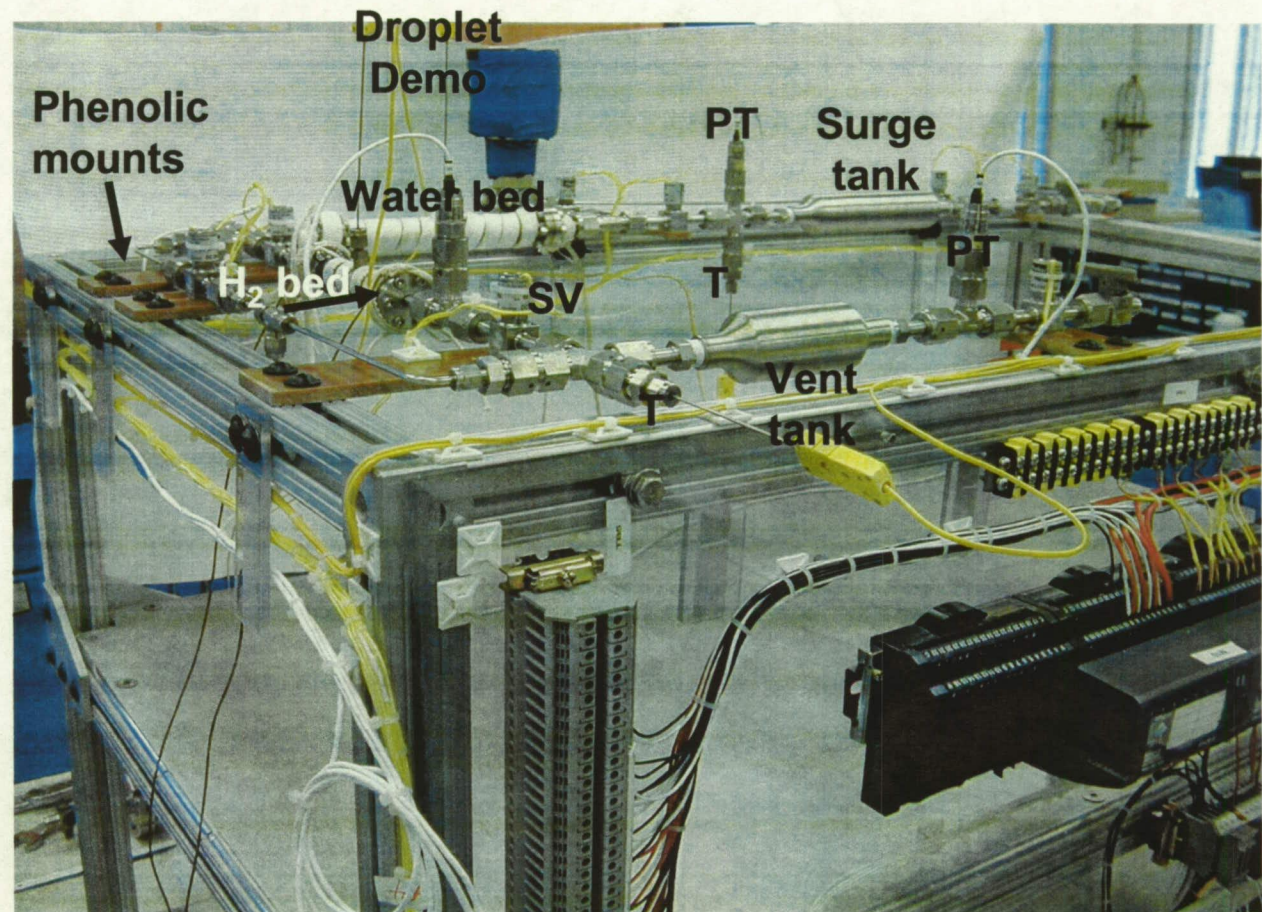
### ■ Sample containing He, H<sub>2</sub>, O<sub>2</sub>, N<sub>2</sub>, CH<sub>4</sub>, CO, H<sub>2</sub>O (inset)



He/H<sub>2</sub> separation (5% each in Ne)

## EBU Hardware

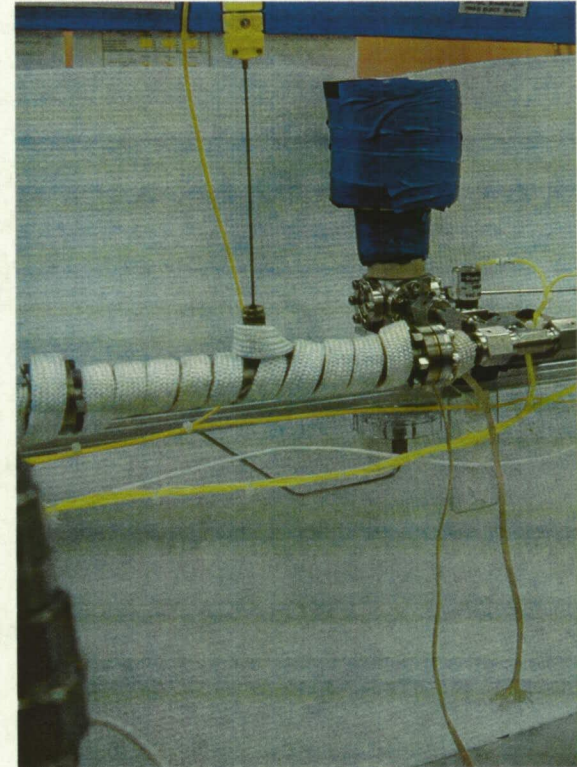
- EBU configuration laid out to allow for easy access to system
  - Wire tracing
  - Leak checks
  - Heat tracing
    - Calculations to estimate power and chose best gauge of wire have been done
- Insulation
  - Polyimide foam
  - Durablanket (ceramic fiber) high temp insulation



## Heat Tracing Challenges



- Goal – prevent condensation of water in system while capturing volatiles
- Cold spots in system would allow for condensation which would skew GC analysis of volatiles
- Thermal imaging camera will be used to analyze heat tracing
- Challenge – solenoid valves (normally closed)
  - maximum operating temp of ~100degC observed when continuously operated, only two must be continuously operated
  - In an insulated system they would overheat, however they need to be heat traced to prevent condensation
  - For FPU latching solenoid valves are preferred to avoid this problem



High temperature heat tape on water capture bed



## Water Vapor generation

- Currently Miller Nelson or in house vapor generation system used
- First cut evaluation will be done with mixed gases and injected water with no simulant
  - Preliminary tests with water and simulant indicate clumping will be a problem for vibrofluidization oven
- Goal will be to dope simulant with hydrated salts that release water vapor for analysis at elevated temperatures
- current oven design is limited to 150°C, this puts an upper bounds on the amount of water vapor we'd see in the system (VP of water at 150°C is ~70 psi)

Desorption  
temps of  
selected  
hydrated  
salts from  
STA runs

# Water Capture



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## ■ Several options explored

- LN<sub>2</sub> cold trap
  - + efficiently captures water
  - not selective, will condense other volatiles (contamination for electrolysis)
- Molecular sieves
  - + reversible water capture
  - capture based on size, not selective
- Hydrated salts
  - + selective adsorption
  - slower than LN<sub>2</sub> trap

Picture of LN<sub>2</sub>,  
molecular  
sieves and  
hydrated salts

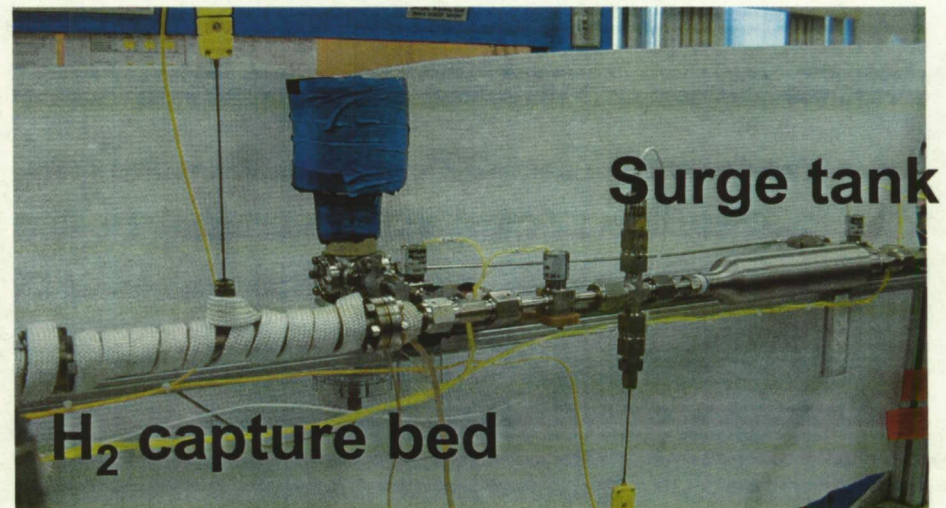
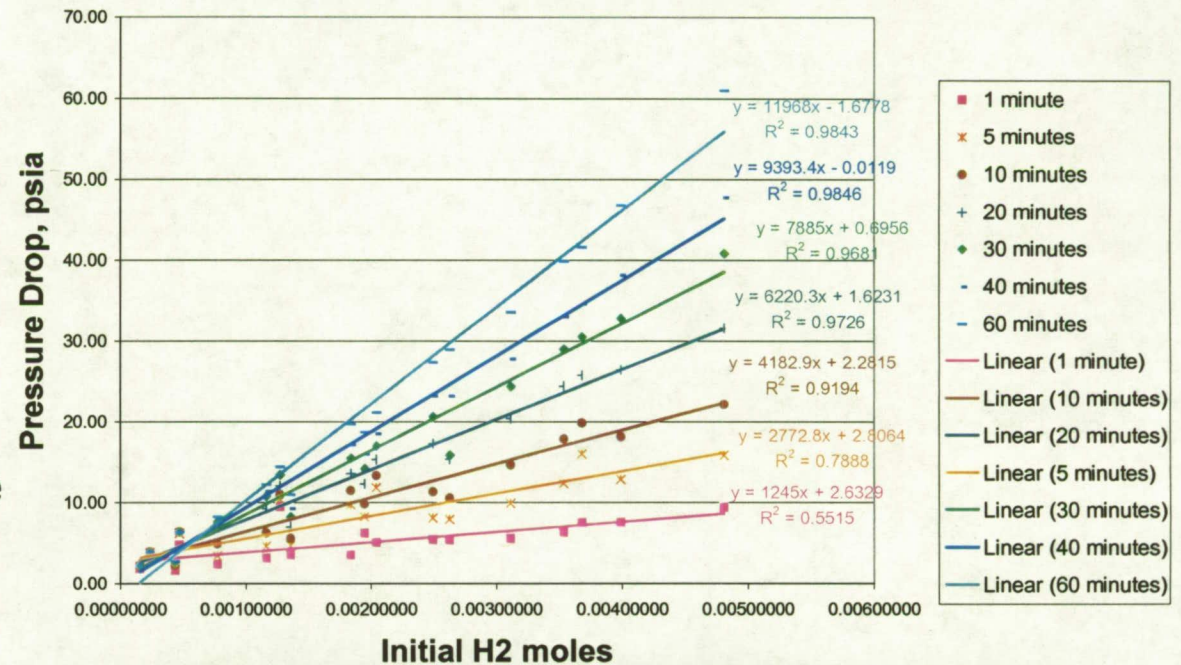
Integration with ROE – current  
system will need to capture  
~1g of water

# Hydrogen Capture

## Pressure Drop vs. Initial H2 moles

### ■ Metal hydrides explored

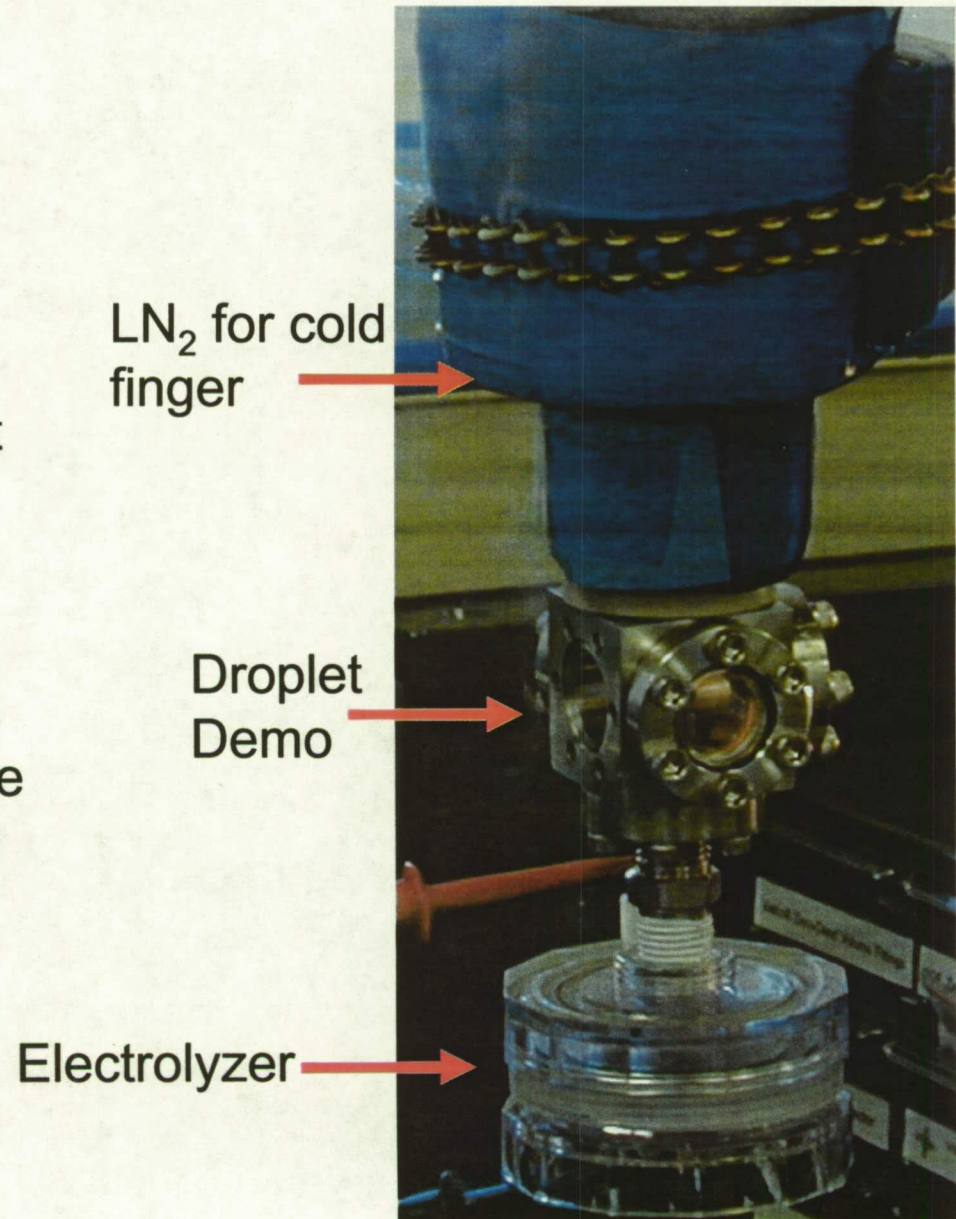
- ZrNi most stable of evaluated hydrides in air, least susceptible to contamination
- Equilibrium vapor pressure vs desorption temperature trade off explored for ZrNi
- Kinetics of ZrNi outweigh the slightly higher equilibrium vapor pressure at elevated temperatures, adsorption performed  $\sim 160^{\circ}\text{C}$



# Water Droplet Demo and Electrolysis



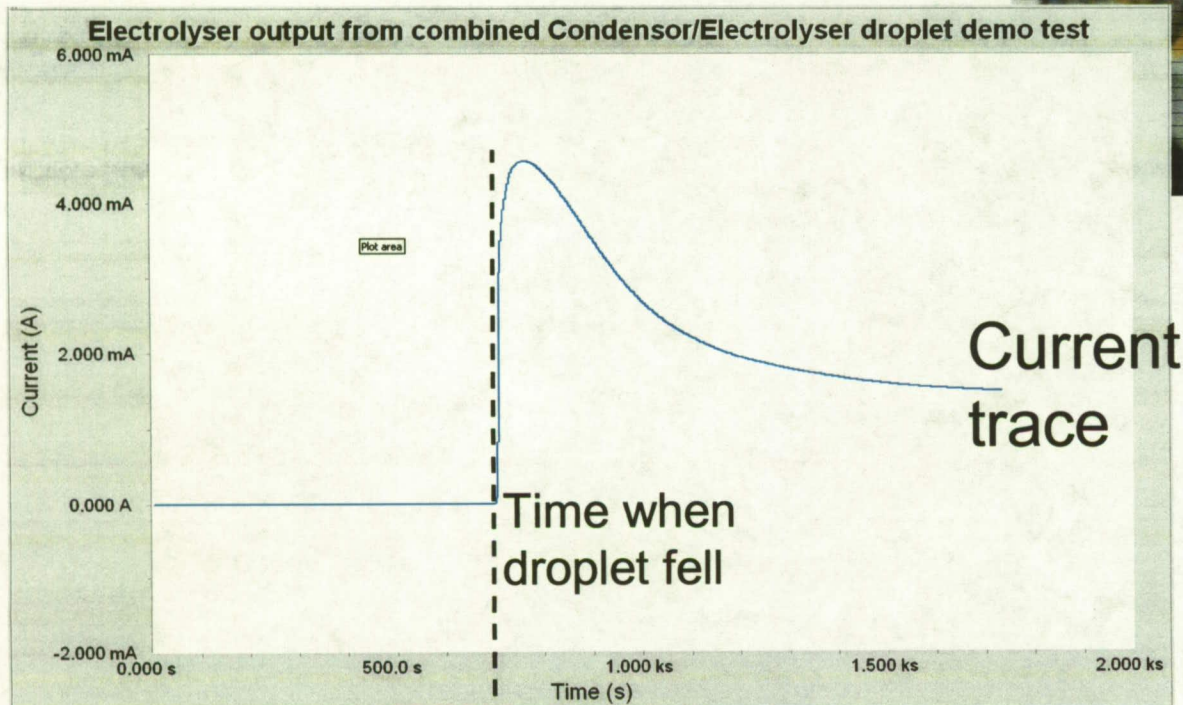
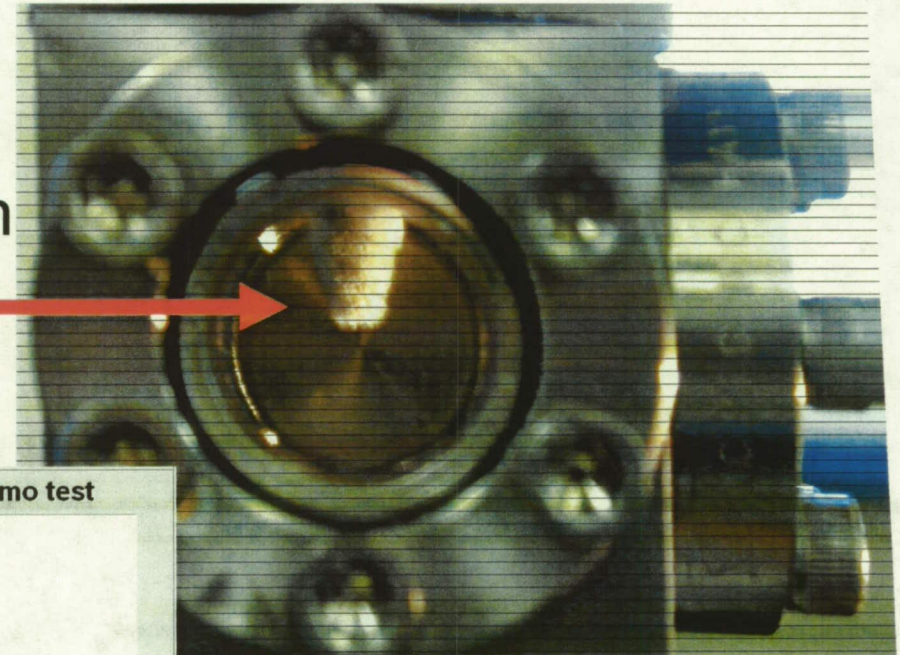
- Currently  $\text{LN}_2$  used to cool cold finger for water condensation
- Droplet demo tested, when the cold finger is warmed a droplet will form on the tip of the condenser and fall into the electrolyzer
- Electrolyzer records an increase in current corresponding to the time the droplet fell





# Water Droplet - Electrolyzer

Ice formation on  
cold finger in  
droplet demo





## Electrolyzer

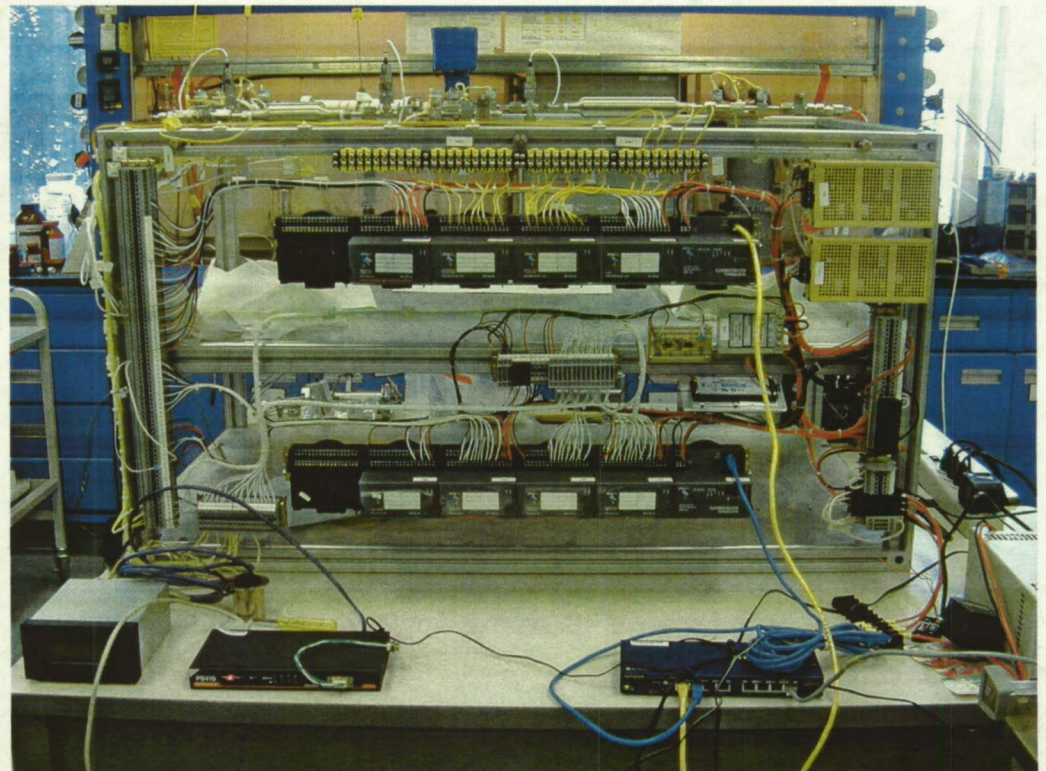
- Trade off between designing for a drop vs 1g of water

Pictures of initial  
electrolyzer  
designs and  
testing with  
40uL in dry cell

# Computer Control



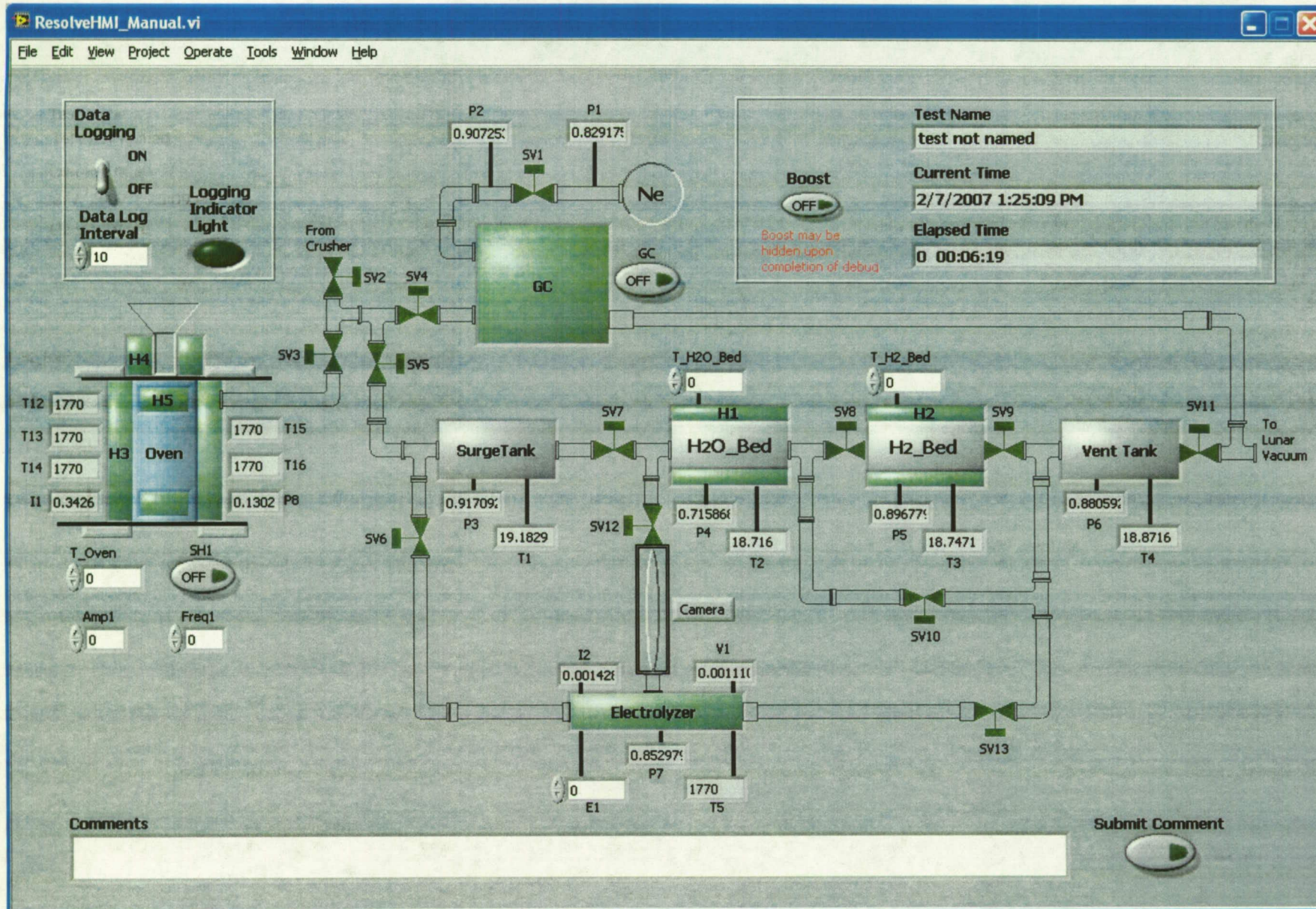
- Documentation has been placed into Microstation (CAD)
- Manual interface is operational and supporting initial testing and data recording
- Process of integrating shaker control software into our system control software
- Next steps
  - Working on heater control loops
  - To integrate system into rover we will need to go to compact fieldpoint (\$) or Xiphos (\$\$\$)
  - Flow charts for automated processes are being constructed



# Manual Control Interface



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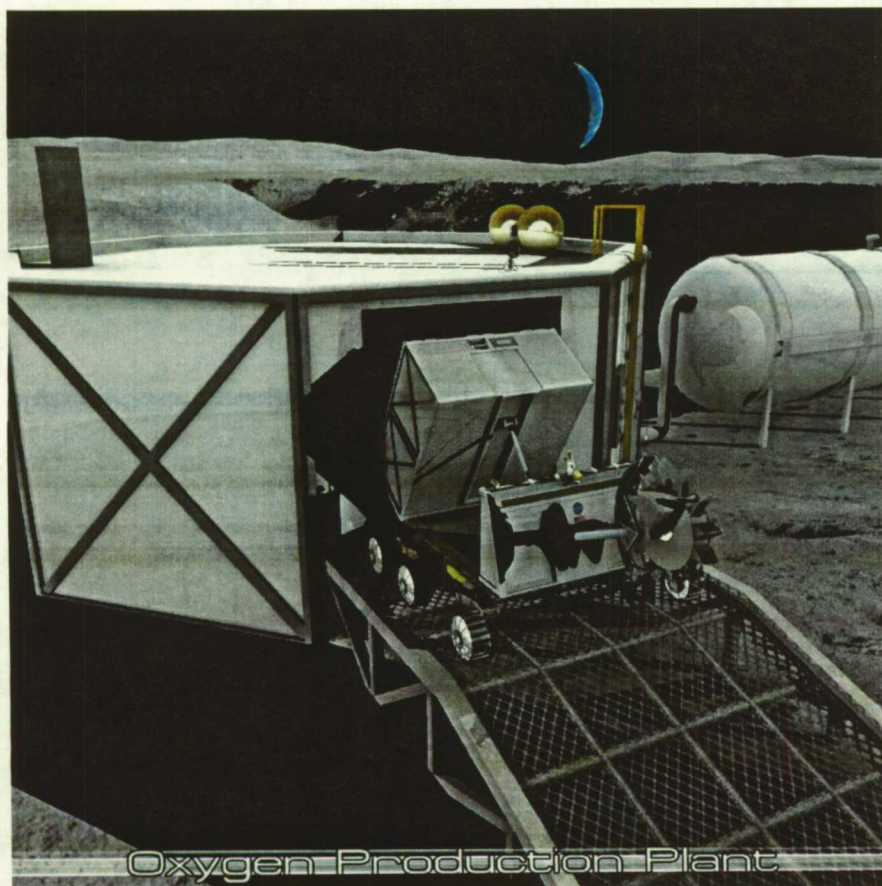
## Conclusion

- EBU integration currently in progress
- Future goals and changes required for FPU identified
- Current RESOLVE goals of volatile characterization and demonstration of ISRU will be met with the EBU and optimized for FPU

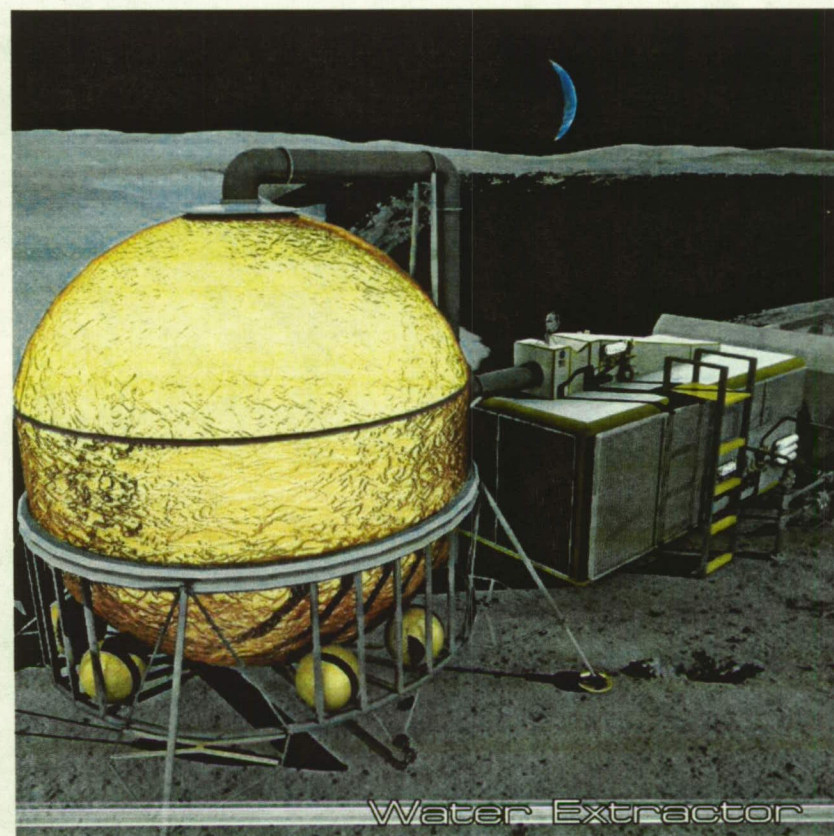




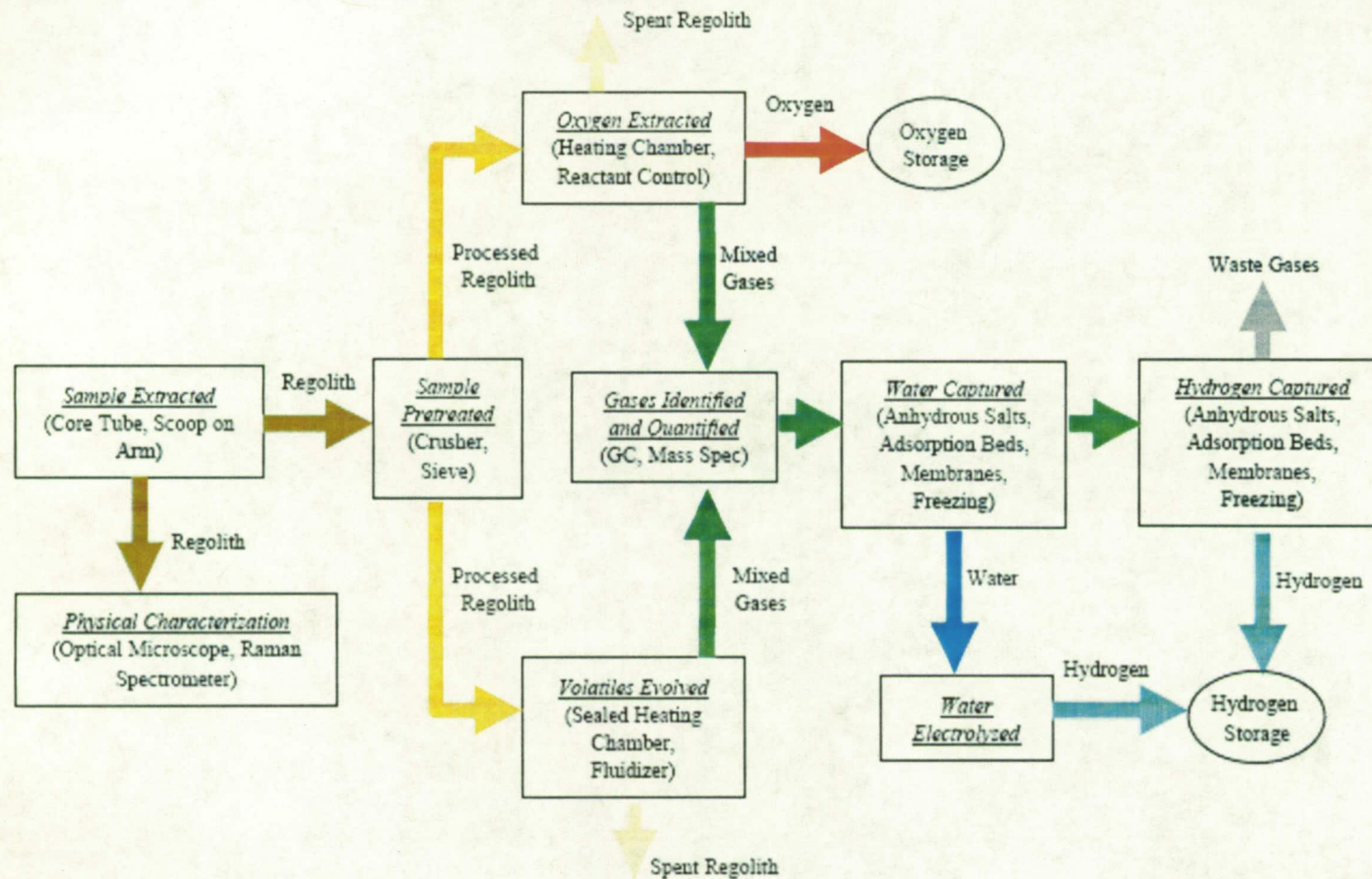
- **Key Functional Requirements and GR&As** The following key functional requirements and GR&As were used for the study, with emphasis placed on ensuring that the architecture approach was consistent with the Cycle 3 ESAS architecture and mission assumptions.
- ISRU: Capable of utilizing locally produced propellants.
- This initial strategy corresponds to the “pointer” location shown in **Figure 4-54** (which appears later in the report in **Section 4.3.5, Lunar Surface Traffic Model**), and serves as a starting point for the analysis of outpost deployment strategies. A number of key a
  - Precursor missions have accomplished the following tasks:
    - • Demonstrated ISRU technologies such as O<sub>2</sub> production, H<sub>2</sub>/H<sub>2</sub>O extraction, and excavation of regolith; and
    - • Developed an enhanced lunar gravity potential model.

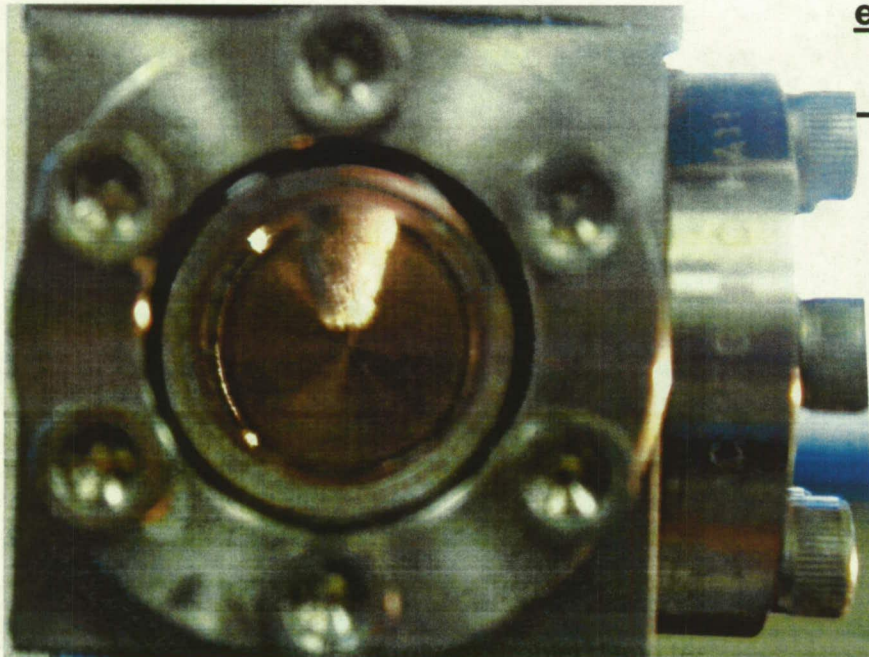


Oxygen Production Plant

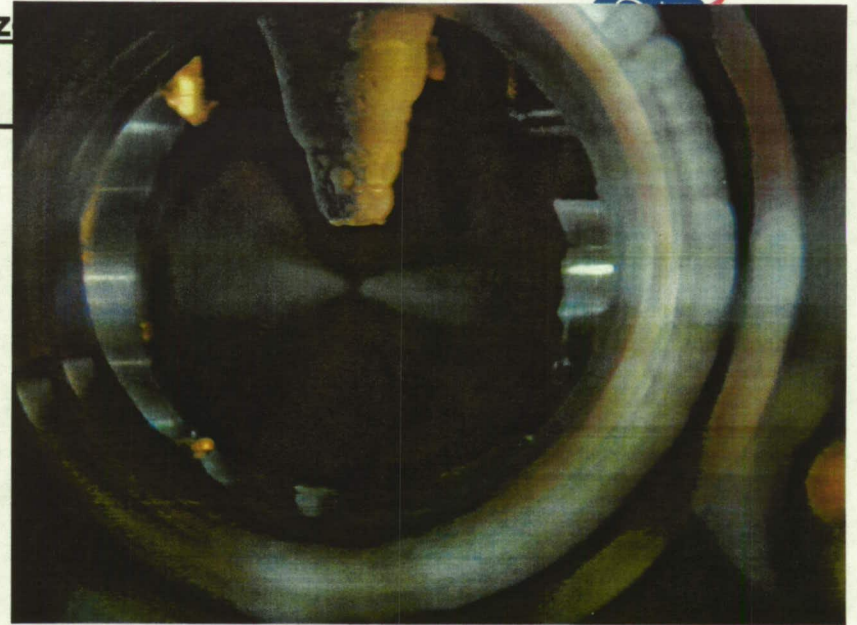


Water Extractor





electrolyz



Electrolyser output from combined Condensor/Electrolyser droplet demo tes

