

Gravity-related Issues in Boiling and Condensation

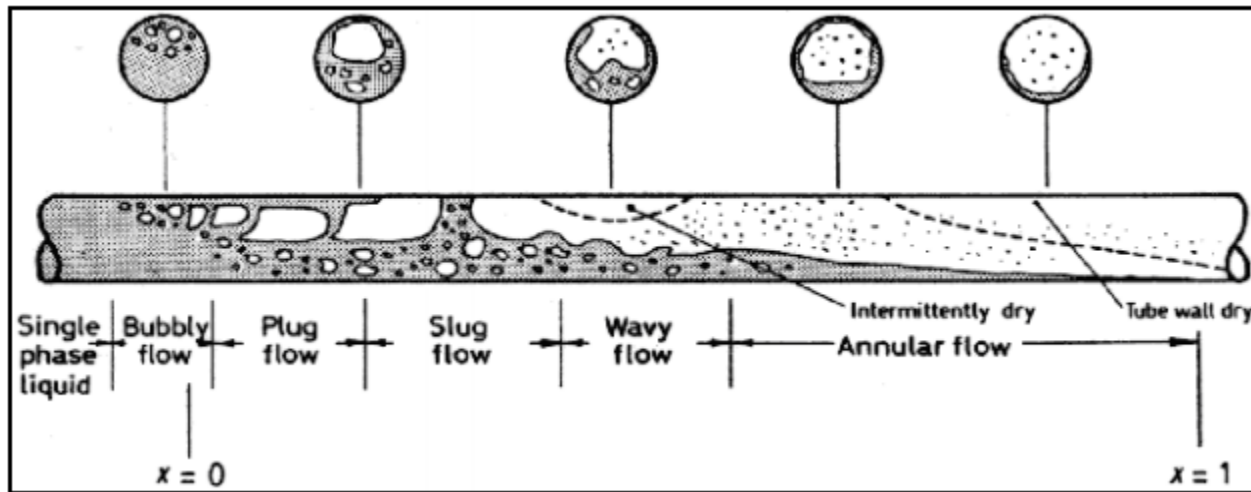
JSC Perspective

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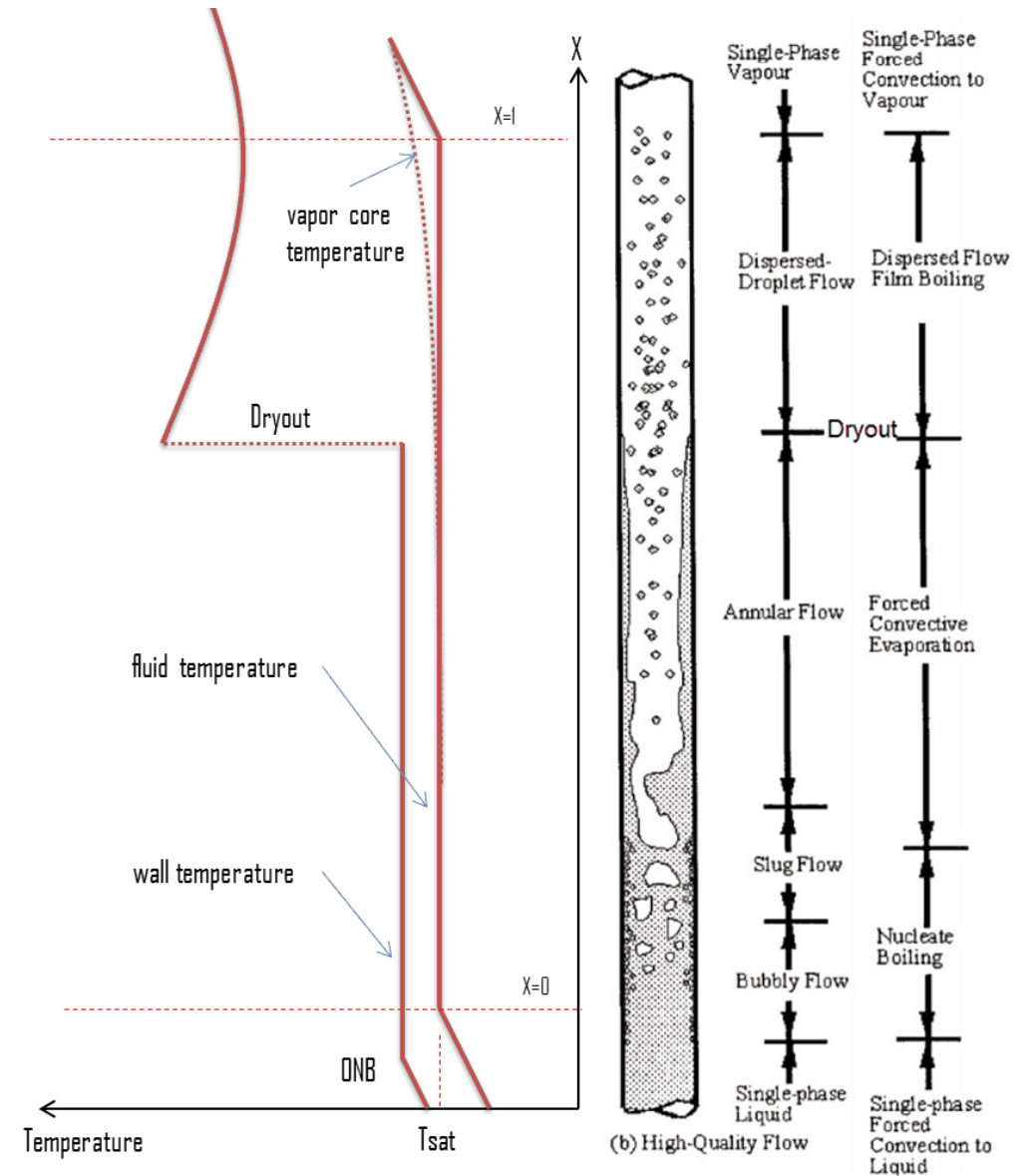
Problem Statement

- For a flight center, gravity-related issues in boiling and condensation take on a unique perspective
- Flight systems must be
 - highly reliable
 - developed and qualified in a cost effective manner
- Must work in 0-g and partial gravity as applicable

Gravity Effects

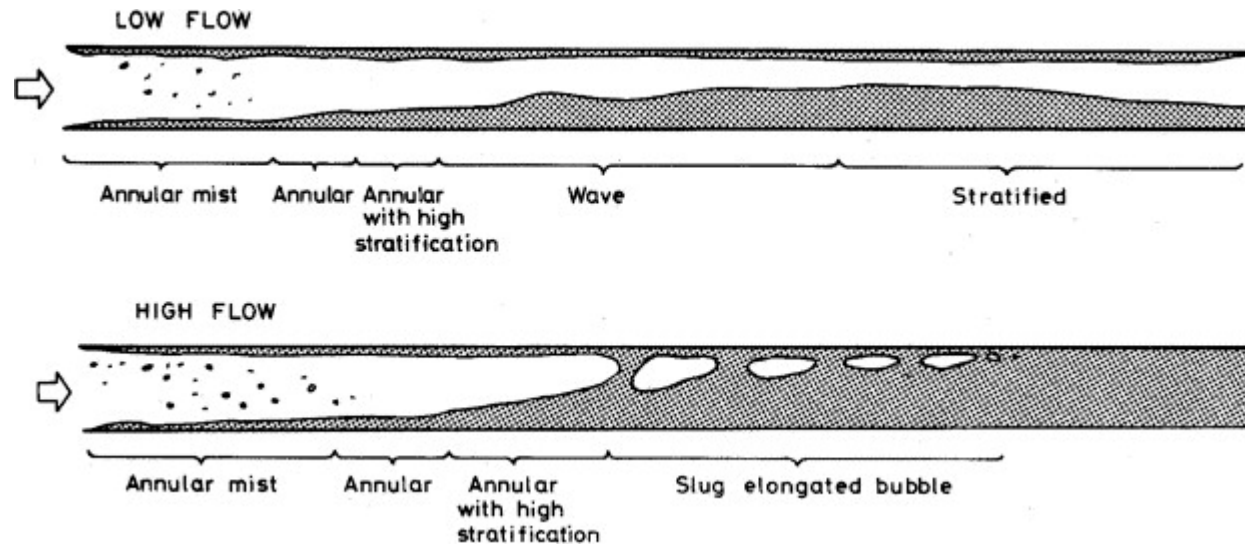


Heat transfer regions in convective boiling in a horizontal tube from Collier and Thome (1994)



Heat transfer regions in convective boiling in a vertical tube from Collier and Thome (1994)

Gravity Effects



Condensation in a horizontal tube from Liebenberg and Meyer 2006

0-g System Options

- Full scale testing in 0-g
- Gravity independent systems tested in 1-g
 - small channel surface tension dominated flows
 - high velocity inertia dominated flows
- Scaled testing in 0-g

Gravity Independence

- Surface tension dominance $Bo < 1$

$$Bo = \frac{(d/2)^2}{\sigma/[g(\rho_f - \rho_g)]}$$

- where σ is the surface tension of the fluid
 - g is the acceleration of gravity
 - ρ_f and ρ_g are the liquid and gas phase densities
- $Bo \leq 1$ means that a vapor bubble growing quasi-statically will completely fill a horizontal liquid-filled tube before growing axially

Reinarts, T. R., Ungar, E. K., and Butler, C. D., "Adiabatic Two-Phase Pressure Drop in Microgravity: TEMP2A-3 Flight Experiment Measurements and Comparison with Predictions," presented at the 33rd AIAA Aerospace Sciences Meeting & Exhibit, Reno, NV, January 9-12, 1995, AIAA 95-0635

Gravity Independence

- Inertia dominated flows (high annular) $Fr > 1$

$$Fr = \sqrt{\frac{\rho_g}{(\rho_f - \rho_g)}} \frac{u_{sg}}{\sqrt{d g}}$$

- u_{sg} is the vapor superficial velocity

Taitel, Y., and Dukler, A. E., 1976, "A Model for Predicting Flow Regime Transitions in Horizontal and Near Horizontal Gas-Liquid Flow," AIChE Journal, Vol. 22, no. 1, pp. 47-55

Gravity Independence

- Are small Bond number and/or large Froude number sufficient for gravity independence?
 - There will be low quality regions where Froude number is small
 - Bond number will be irrelevant for champagne bubbles
- A good topic for further study

Scaling in 0-g

- Testing full scale systems in 0-g is difficult
- 0-g testing usually requires geometrical scaling and a change in working fluid
- What are the proper scaling parameters?
 - Case can be made to include ρ_f/ρ_g , We_g , Re_f , Re_g , and X , the Martinelli parameter
- A good topic for further study

Partial Gravity Boiling and Condensation

- Scaling is critical
 - Flying experiments on partial-g aircraft almost always involves a fluid substitution
 - Gravity is just another parameter
- What are the proper scaling parameters?
 - Case can be made to include Fr , ρ_f/ρ_g , We_g , Re_f , Re_g , and X
- A good topic for further study
 - Might involve partial-g aircraft experiments for proof
- These should be the last partial-g experiments required

Conclusion

- Development of zero and partial gravity flight systems requires extensive testing
- Zero-g aircraft testing for 0-g systems
 - Safety concerns usually require fluid substitution
 - +/- 0.01 g is a spec, not a guarantee
 - <30 seconds of 0-g time is problematic
- Partial gravity aircraft testing for partial-g systems
 - ~30 seconds of partial time is problematic
- Testing recommendations should come from an understanding of the physics

Backup

1-g Behavior of Bubbles in Vertical Tube

- Bond number is the relevant dimensionless group

- $$Bo = \frac{(d/2)^2 g (\rho_f - \rho_g)}{\sigma}$$

- where

- r = tube diameter
- g = gravitational acceleration
- ρ_f = liquid density
- ρ_g = vapor density
- σ = surface tension

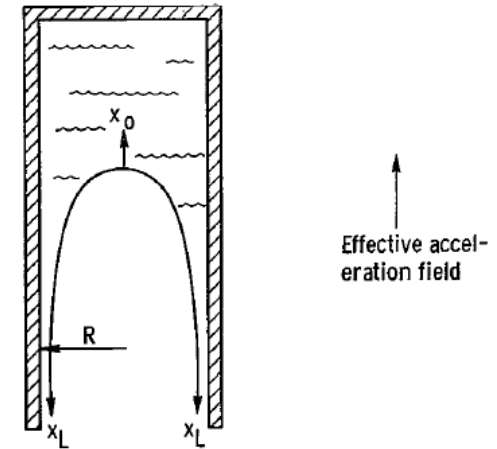


Figure 1. - Interface profile under imposed acceleration directed perpendicular from vapor to liquid phase (where x_D is vapor penetration displacement and x_L is leading-edge displacement).

- From the literature at $Bo < 0.84$ the liquid/vapor interface would be stable
- For $Bo > 0.84$ counterflow can occur