

CFD Modeling and Simulation of High Speed Reacting Flows: Theory

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Outline



- Introduction
- Governing Transport Equations
- Nondimensionalization
- Introduction to Modeling and Simulation
- Numerical Methods
- Example Applications







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Introduction: High-Speed Atmospheric Flight



Hypersonic Vehicle Applications Military (rapid response and strike on global scale) Aerospace (safer and more affordable access to space)

Civil Aviation

(point-to-point transport)

Types of Vehicle:

- Gliders (re-entry, unpowered cruise)
- Airbreathers (launch, cruise, re-entry)
- Types of Hypersonic Propulsion:
- Ramjet (RJ) / Scramjet (SJ)
- Turbine-based combined cycle (TBCC)
- Rocket-based combined cycle (RBCC)
- Air-augmented or ducted rocket (DR)
- Rocket



- Vehicle only needs to carry fuel for its propulsive needs, thereby
 - allowing for larger payloads or ...
 - lighter vehicle (less structure to support weight) or ...
 - more fuel for longer range



Hypersonic Access-to-Space Flight Trajectories



 Bernoulli's equation for a moving fluid gives rise to the *Dynamic Pressure*:

$$q_0(Pa) = \frac{\rho u^2}{2} = \frac{1}{2}\gamma p M_0^2$$

which is the kinetic component of the total pressure

• *q* is a useful aerodynamic parameter that is related to lift and drag forces of a vehicle:

$$L(N) = q_0 C_L S$$
$$D(N) = q_0 C_D S$$

- When q is too large, the structural forces and the drag can become excessive.
- When *q* is too small, the wing area required for controlled sustained flight may become too large





Mass Flow Rate and Engine Thrust

• Mass flow rate of air through the engine can also be related to the *Dynamic Pressure, q*:

$$\dot{m}_0\left(\frac{kg}{s}\right) = m_0'A_0 = \frac{2q}{u_0}A_0$$

 And since mass flow rate through the engine is related to engine net thrust (obtained from the <u>conservation of momentum</u>), we obtain:

$$F(N) = (p_e - p_0)A_e + \frac{2q}{u_0}A_0(u_e(1+f) - u_0)$$

• Specific Impulse (Isp) is a measure of how efficiently a vehicle uses its propellant to generate thrust:

$$I_{sp}(s) = \frac{F}{g \, \dot{m}_0 f}$$

• One of the most important nondimensional parameters is the *Reynolds Number*:

$$Re = \frac{2 q_0 L}{u_0 \mu_0}$$
, Natural Transition for $Re > 10^7$

- *Re* indicates to the designer whether the boundary layers are laminar, transitional, or turbulent
 - Externally, *laminar boundary layers* are preferred due to lower skin friction and wall heat transfer
 - Internally, <u>turbulent boundary layers</u> are preferred due to greater resistance to flow separation







• From the definition of total energy and static enthalpy, we have:

$$e^{t} = e + k = h - \frac{p}{\rho} + k = h^{t} - \frac{p}{\rho},$$
$$h = \sum_{\alpha} Y_{\alpha} \int_{0}^{T} dT' C p_{\alpha}(T')$$

- If we stagnate the flow such that all of *k* is absorbed into the *h*, then the flow's temperature must rise. This new temperature of the stagnated flow is called *stagnation* or total temperature*.
 - In <u>subsonic</u> flows, the kinetic energy is small, and so the static and total temperatures are about the same
 - In <u>supersonic</u> flows, the kinetic energy is large, and the ratio of static and total temperatures depends on the Mach number:

$$\frac{T_t}{T} = \left(1 + \frac{k}{h}\right) = \left(1 + \frac{\gamma - 1}{2}M^2\right)$$

- In <u>hypersonic</u> flows, the kinetic energy is >> than the enthalpy such that most of the flow's energy is in the kinetic form, e.g., at Mach 7, the kinetic energy is an order of magnitude larger than the enthalpy.
- Heating (and cooling) considerations drive material selection in high speed applications.







Simulation in ground facility



Hypersonic Research as an Aeroscience









Anderson, J. D. "Hypersonic and High Temperature Gas Dynamics" AIAA Education Series, 2006
Heiser, W. H. and Pratt, D. T. "Hypersonic Airbreathing Propulsion" AIAA Education Series,1994



- MODSIM will be increasingly relied upon for aero-propulsion system designs.
- Currently, 3-D CFD is already being used as a risk-mitigating and parameter exploration tool in design and analysis.
- CFD capabilities continue to improve via
 - More robust and efficient algorithms
 - More accurate physics models
 - Faster computers
- More so than in low speed flows, CFD is playing a critical role in scramjet development
 - Not possible to exactly reproduce hypersonic flight conditions at ground test facilities
 - CFD used to extrapolate results to flight
 - CFD used to examine test-media effects (e.g., vitiation) in ground facilities
 - Not possible to measure all relevant properties at ground test facilities
 - CFD used to "fill-in" gaps due to lack of measurements
 - CFD used to examine trends from perturbations made from a calibrated condition
 - Vehicle and engine size limited by the facility capabilities

In the future, CFD must evolve to a state capable of reliably certifying propulsion systems for flight



Conservation of Mass

$$\frac{\partial \rho}{\partial t} + \frac{\partial \rho u_k}{\partial x_k} = 0,$$

• Einstein summation notation used, i.e.,

$$\frac{\partial u_k}{\partial x_k} = \frac{\partial u_1}{\partial x_1} + \frac{\partial u_2}{\partial x_2} + \frac{\partial u_3}{\partial x_3} = \frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} + \frac{\partial w}{\partial z}.$$

• The RHS is zero except in multiphase flows, where it could contain terms describing the mass exchange between the phases.



Conservation of Species Mass

$$\frac{\partial \rho Y_{\alpha}}{\partial t} + \frac{\partial \rho u_k Y_{\alpha}}{\partial x_k} = \frac{\partial J_{\alpha k}}{\partial x_k} + \dot{\omega}_{\alpha}, \qquad \alpha = 1, 2, \dots N,$$

• Some properties

$$\sum_{\alpha} Y_{\alpha} = 1 \qquad \sum_{\alpha} J_{\alpha k} = \sum_{\alpha} Y_{\alpha} V_{\alpha k} = 0$$

- $\sum_{\alpha=1}^{N} \dot{\omega}_{\alpha} = 0.$
- Sum over all of the species recovers the conservation of mass:

$$\sum_{\alpha} \left(\frac{\partial \rho Y_{\alpha}}{\partial t} \right) + \sum_{\alpha} \left(\frac{\partial \rho u_k Y_{\alpha}}{\partial x_k} \right) = \sum_{\alpha} \left(\frac{\partial}{\partial x_k} \left(\rho Y_{\alpha} V_{\alpha k} \right) \right) + \sum_{\alpha} \left(\dot{\omega}_{\alpha} \right)$$



• Species mass production rate

$$\dot{\omega}_{\alpha} = W_{\alpha} \sum_{i=1}^{K} \left(\nu_{\alpha i}^{\prime\prime} - \nu_{\alpha i}^{\prime}\right) \left(k_{i}^{f} \prod_{\phi=1}^{N} \left[C_{\phi}\right]^{\nu_{\phi i}^{\prime}} - k_{i}^{b} \prod_{\varphi=1}^{N} \left[C_{\varphi}\right]^{\nu_{\varphi i}^{\prime\prime}}\right)$$

$$\sum_{i=1}^{N} \nu_{\alpha i}^{\prime} M_{\alpha} \longleftrightarrow \sum_{\alpha=1}^{N} \nu_{\alpha i}^{\prime\prime} M_{\alpha}, \qquad i = 1, 2, \dots K,$$

$$k_{i}^{f} = A_{i} T^{\beta_{i}} \exp\left(\frac{-E_{i}}{R_{u}T}\right),$$

$$\left[C_{\alpha}\right] = \frac{\rho Y_{\alpha}}{W_{\alpha}} = \rho Y_{\alpha} \sum_{\phi=1}^{N} \frac{Y_{\phi}}{W_{\phi}},$$

- Lu, T. & Law, C., "Toward Accommodating Realistic Fuel Chemistry in Large-Scale Computations," *Prog. Energy Combust. Sci.*, 2009, 35, 192-215.
- Pope, S. "Small Scales, Many Species and the Manifold Challenges of Turbulent Combustion," *Proc. Combust. Inst.*, 2013, 34, 1-31.
- Princeton Summer School on Combustion https://www.princeton.edu/cefrc/combustion-summer-school/lecture-notes/



• Species molecular diffusion

$$J_{\alpha k} = -\rho Y_{\alpha} V_{\alpha k},$$

• Fick's model

$$V_{\alpha k}^{F} = -\frac{D_{\alpha}}{Y_{\alpha}} \frac{\partial Y_{\alpha}}{\partial x_{k}}$$

$$V_k^c = \sum_{\alpha} D_{\alpha} \frac{\partial Y_{\alpha}}{\partial x_k}$$

 $Le_{\alpha} = \frac{k}{\rho C p D_{\alpha}} = \frac{\kappa}{D_{\alpha}} = \frac{\text{rate of thermal diffusion}}{\text{rate of mass diffusion}},$ $Pr = \frac{C_{p}\mu}{k} = \frac{\text{rate of viscous diffusion}}{\text{rate of thermal diffusion}},$

$$D = \frac{k}{\rho C p L e} = \frac{\mu}{\rho P r L e} = \frac{\mu}{\rho S c},$$

Conservation of species mass fractions

$$\frac{\partial \rho Y_{\alpha}}{\partial t} + \frac{\partial \rho (u_k + V_k^c) Y_{\alpha}}{\partial x_k} = \frac{\partial}{\partial x_k} \left(\rho D_{\alpha} \frac{\partial Y_{\alpha}}{\partial x_k} \right) + \dot{\omega}_{\alpha}, \qquad \alpha = 1, 2, \dots N.$$



• Conservation of momentum (Navier-Stokes Eqs.)

$$\frac{\partial \rho u_i}{\partial t} + \frac{\partial \rho u_k u_i}{\partial x_k} = -\frac{\partial p}{\partial x_i} + \frac{\partial \tau_{ik}}{\partial x_k} + \rho |g| \hat{n}_i \cdot \hat{n}_g$$

• Viscous stress tensor

$$\tau_{ij} = \mu \left(\frac{\partial u_i}{\partial x_j} + \frac{\partial u_j}{\partial x_i} \right) - \frac{2}{3} \mu \frac{\partial u_k}{\partial x_k} \delta_{ij}.$$

• Pressure (EoS)

$$p = \frac{\rho R_u T}{W_{mix}} = \rho R_u T \sum_{\alpha} \frac{Y_{\alpha}}{W_{\alpha}},$$



• Total energy

$$e^{t} = e + k = h - \frac{p}{\rho} + k = h^{t} - \frac{p}{\rho} = \sum_{\alpha} h_{\alpha} Y_{\alpha} - \frac{p}{\rho} + \frac{u_{i} u_{i}}{2},$$

Conservation of total energy and heat flux vector

$$\frac{\partial \rho e^t}{\partial t} + \frac{\partial \rho u_k h^t}{\partial x_k} = \frac{\partial u_i \tau_{ik}}{\partial x_k} - \frac{\partial \dot{q}_k}{\partial x_k} + \rho u_k |g| \hat{n}_k \cdot \hat{n}_g.$$
$$\dot{q}_k = -k \frac{\partial T}{\partial x_k} + \rho \sum_{\alpha} h_{\alpha} Y_{\alpha} V_{\alpha k}.$$

• Conservation of enthalpy (typically solved for in low speed flows) $\frac{\partial \rho h}{\partial t} + \frac{\partial \rho (u_k + V_k^c) h}{\partial x_k} = \underbrace{\frac{\mathcal{D}p}{\mathcal{D}t} + \tau_{ik} \frac{\partial u_i}{\partial x_k}}_{\approx 0 \ if \ Mach < 0.3} + \frac{\partial}{\partial x_k} \left(\frac{k}{Cp} \frac{\partial h}{\partial x_k}\right) - \underbrace{\frac{\partial}{\partial x_k} \left(\frac{k}{Cp} \sum_{\alpha} \left(\frac{Le_{\alpha} - 1}{Le_{\alpha}}\right) h_{\alpha} \frac{\partial Y_{\alpha}}{\partial x_k}\right)}_{=0 \ if \ Le_{\alpha} = 1}.$

Governing Transport Equations



$$\frac{\partial \rho u_k}{\partial x_k} = 0, \qquad \qquad \boxed{\rho u A = \dot{m}}$$

$$\frac{\partial \rho(u_k + V_k^c) Y_\alpha}{\partial x_k} = \frac{\partial}{\partial x_k} \left(\rho D_\alpha \frac{\partial Y_\alpha}{\partial x_k} \right) + \dot{\omega}_\alpha, \qquad \alpha = 1, 2, \dots N.$$
$$V_k^c = \sum_\alpha D_\alpha \frac{\partial Y_\alpha}{\partial x_k}$$

$$\frac{\partial \rho u_k u_i}{\partial x_k} = -\frac{\partial p}{\partial x_i} + \frac{\partial \tau_{ik}}{\partial x_k} + \rho |g| \hat{n}_i \cdot \hat{n}_g \qquad \boxed{\rho u^2 A + pA = \mathcal{F}}$$
$$p = \frac{\rho R_u T}{W_{mix}} = \rho R_u T \sum_{\alpha} \frac{Y_{\alpha}}{W_{\alpha}}, \qquad \tau_{ij} = \mu \left(\frac{\partial u_i}{\partial x_j} + \frac{\partial u_j}{\partial x_i}\right) - \frac{2}{3} \mu \frac{\partial u_k}{\partial x_k} \delta_{ij}.$$

$$\frac{\partial \rho u_k h^t}{\partial x_k} = \frac{\partial u_i \tau_{ik}}{\partial x_k} - \frac{\partial \dot{q}_k}{\partial x_k} + \rho u_k |g| \hat{n}_k \cdot \hat{n}_g. \qquad \begin{bmatrix} h + \frac{1}{2} u^2 = h^t \\ \frac{\partial q_k}{\partial x_k} + \rho \sum_{\alpha} h_{\alpha} Y_{\alpha} V_{\alpha k}. \end{bmatrix}$$



References

Panton, R.L., Incompressible Flow, John Wiley and Sons, New York, NY, 1984.

Williams, F.A., *Combustion Theory*, The Benjamin/Cummings Publishing Company, Menlo Park, CA, 2nd ed., 1985.

Turns, S.R., An Introduction to Combustion: Concepts and Applications, McGraw Hill, 2nd ed., 2000.

Kuo, K.K., Principles of Combustion, John Wiley and Sons, Hoboken, N.J., 2nd ed., 2005.

Warnatz, J., Maas, U., and Dibble, R.W., Combustion, Springer, Berlin, Germany, 4th ed., 2006.

Poinsot, T. and Veynante, D., *Theoretical and Numerical Combustion*, R.T. Edwards, Inc., Philadelphia, PA, 2nd ed., 2005.



20

Nondimensionalization

1

- Identifies a minimum set of nondimensional groups
- Helps to identify limiting behavior of a set of equations
- Homogenizes the values of different quantities so the values are neither too small or too large
- For high speed flows it is convenient to use a combination of free stream and sonic nondimensionalization variables

$$\begin{aligned} u^* &= \frac{tc_r}{l_r}, \ x^* = \frac{x}{l_r}, \ \rho^* = \frac{\rho}{\rho_r}, \ u^*_i = \frac{u_i}{c_r}, \ T^* = \frac{T}{T_r}, \ p^* = \frac{p}{\rho_r c_r^2}, \ e^{t^*} = \frac{e^t}{c_r^2}, \ h^* = \frac{h}{c_r^2}, \\ \mu^* &= \frac{\mu}{\mu_r}, \ k^* = \frac{k}{k_r}, \ D^*_{\alpha} = \frac{D_{\alpha}}{D_r}, \ R^* = \frac{R}{R_r}, \ W^*_{\alpha} = W_{\alpha}/W_r, \end{aligned}$$

• With some reference quantities computed from other reference values:

$$c_r = \sqrt{\gamma_r R_r T_r}, \ \gamma_r = \frac{Cp_r}{Cp_r - R_r}, \ Cp_r = \sum_{\alpha} Y_{\alpha,r} Cp_{\alpha}(T_r), \ R_r = \frac{R_u}{W_r}, \ W_r = \frac{1}{\sum_{\alpha} \frac{Y_{\alpha,r}}{W_{\alpha}}},$$
$$\mu_r = \mu(T_r), \ k_r = k(T_r), \ D_r = c_r l_r,$$

Nondimensional parameters become

$$Re_{r} = \frac{\rho_{r}u_{r}l_{r}}{\mu_{r}}, \ Fr_{r} = \frac{u_{r}}{\sqrt{l_{r}|g|}}, \ M_{r} = \frac{u_{r}}{c_{r}}, \ Pr_{r} = \frac{\mu_{r}Cp_{r}}{k_{r}}, \ Le_{r} = \frac{k_{r}}{\rho_{r}Cp_{r}D_{r}}, \ Sc_{r} = Pr_{r}Le_{r},$$

Nondimensionalization



• Transport Equations for Mass, Momentum, and Energy

$$\begin{aligned} \frac{\partial \rho^*}{\partial t^*} + \frac{\partial \rho^* u_k^*}{\partial x_k^*} &= 0. \\ \frac{\partial \rho^* Y_\alpha}{\partial t^*} + \frac{\partial \rho^* (u_k^* + V_k^{c*}) Y_\alpha}{\partial x_k^*} &= \frac{\partial}{\partial x_k^*} \left(\rho^* D_\alpha^* \frac{\partial Y_\alpha}{\partial x_k^*} \right) + \frac{l_r}{\rho_r c_r} \dot{\omega}_\alpha, \\ &= \frac{\partial}{\partial x_k^*} \left(\frac{\mu^*}{S c_\alpha^*} \frac{\partial Y_\alpha}{\partial x_k^*} \right) + \frac{l_r}{\rho_r c_r} \dot{\omega}_\alpha, \qquad \alpha = 1, 2, \dots N, \end{aligned}$$

$$\frac{\partial \rho^* u_i^*}{\partial t^*} + \frac{\partial \rho^* u_k^* u_i^*}{\partial x_k^*} = -\frac{\partial p^*}{\partial x_i^*} + \frac{M_r}{Re_r} \frac{\partial}{\partial x_k^*} \left(\mu^* \left(\frac{\partial u_i^*}{\partial x_k^*} + \frac{\partial u_k^*}{\partial x_i^*} \right) - \frac{2}{3} \mu^* \frac{\partial u_j^*}{\partial x_j^*} \delta_{ik} \right) + \frac{M_r^2}{F r_r^2} \rho^* \hat{n}_i \cdot \hat{n}_g$$

$$Re >> 1 : \text{Euler Eqs.} \qquad Fr >> 1 : \text{Neglect Buoyancy}$$

$$\frac{\partial \rho^* e^{t^*}}{\partial t^*} + \frac{\partial \rho^* (u_k^* + V_k^{c^*}) h^{t^*}}{\partial x_k^*} = \frac{M_r}{Re_r} \frac{\partial}{\partial x_k^*} \left(u_i^* \left(\frac{\mu^*}{\partial x_k^*} + \frac{\partial u_k^*}{\partial x_i^*} \right) - \frac{2}{3} \mu^* \frac{\partial u_j^*}{\partial x_j^*} \delta_{ik} \right) \right)$$
$$+ \frac{M_r}{Re_r Pr_r} \frac{\partial}{\partial x_k^*} \left(\frac{\mu^*}{Pr^*} \frac{\partial h^*}{\partial x_k^*} - \frac{\mu^*}{Pr^*} \sum_{\alpha} \left(\frac{Le_{\alpha}^* - 1}{Le_{\alpha}^*} \right) h_{\alpha}^* \frac{\partial Y_{\alpha}}{\partial x_k^*} \right) + \frac{\partial \rho^* k^* V_k^{c^*}}{\partial x_k^*} + \frac{M_r^2}{Fr_r^2} \rho^* u_k^* \hat{n}_k \cdot \hat{n}_g$$

Nondimensionalization



- Nondimensional form of the species production rate
 - Difficult to implement in a solver
 - Reveals two more nondimensional groups

$$\begin{aligned} \frac{l_r}{\rho_r c_r} \dot{\omega}_{CO_2} &= x W_{CO_2}^* Da \exp\left(\frac{-Ze}{T^*}\right) \rho^{*m+n} Y_{C_x H_y}^m Y_{O_2}^n, \\ Da &= \frac{l_r}{\rho_r c_r} \frac{W_r \rho_r^{m+n} A}{W_{C_x H_y}^m W_{O_2}^n}, \ Ze = \frac{E_a}{R_u T_r}, \end{aligned}$$

- Damkohler number:
 - Da >> 1 leads to rapid reaction and near equilibrium chemical compositions.
 - Da << 1 leads to extinction
- Zeldovich number represents the nondimensional measure of the temperature sensitivity of the reaction



- One physical phenomena that can be studied using the Navier-Stokes equations is <u>turbulence</u>
 - Turbulence is multiscale, i.e., occurs over a range of length and time scales



- Turbulence complicates other physical processes through non-linear interactions, e.g., combustion
- Turbulence leads to complex flow behaviors, e.g., boundary layers.
- Range of turbulence scales is proportional to the Reynolds number
 - The range is too large to simulate numerically for engineering problems

$$\frac{\eta}{L} = Re^{-3/4}, \qquad \frac{t_{\eta}}{t_L} = Re^{-1/2},$$













- The two most common scale-reduction strategies are the time-averaging and spatial-averaging (or filtering)
 - Time-averaging gives rise to Reynolds averaged simulations (RAS)

$$\overline{f}(x) = \lim_{T \to \infty} \int_{t}^{t+T} \mathrm{d}t' f(x, t'),$$

• Filtering leads to large-eddy simulations (LES)

$$\overline{f}(x,t) = \int_{-\infty}^{+\infty} \mathrm{d}x' f(x',t) \mathcal{G}(x'-x),$$

• Favre average is useful in variable density flows and is defined as the density-weighted average. $\sim \overline{of}$

$$\widetilde{f} = \frac{\overline{\rho f}}{\overline{\rho}}.$$

- Both of the above operators
 - produce the exact same (looking) set of governing equations although the interpretation and modeling strategies vary
 - produce extra terms in the governing equations that require modeling



• LES (or RAS) equations are:

$$\begin{split} \frac{\partial \overline{\rho}}{\partial t} &+ \frac{\partial \overline{\rho} \widetilde{u}_k}{\partial x_k} = 0, \\ \overline{p} = \overline{\rho} \widetilde{RT} = \overline{\rho} \sum_{\alpha} \frac{Ru}{W_{\alpha}} \widetilde{Y}_{\alpha} \widetilde{T} + \underbrace{\overline{\rho}} \sum_{\alpha} \frac{Ru}{W_{\alpha}} (\widetilde{Y}_{\alpha} T - \widetilde{Y}_{\alpha} \widetilde{T}) \\ \underbrace{\partial \overline{\rho} \widetilde{Y}_{\alpha}}{\partial t} &+ \frac{\partial \overline{\rho} (\widetilde{u}_k + \widehat{V}_k^c) \widetilde{Y}_{\alpha}}{\partial x_k} = \frac{\partial}{\partial x_k} \left(\frac{\widehat{\mu}}{\widehat{S} c_{\alpha}} \frac{\partial \widetilde{Y}_{\alpha}}{\partial x_k} \right) + \dot{\omega}_{\alpha} (\overline{p}, \widetilde{Y}_{\alpha}, \widetilde{T}) \\ &- \underbrace{\frac{\partial}{\partial x_k} \left(\overline{\rho} \widetilde{u}_k \widetilde{Y}_{\alpha} - \overline{\rho} \widetilde{u}_k \widetilde{Y}_{\alpha} \right)}_{\text{Turbulence Subgrid Flux}} + \underbrace{\left(\frac{\dot{\omega}_{\alpha} (p, Y_{\alpha}, T) - \dot{\omega}_{\alpha} (\overline{p}, \widetilde{Y}_{\alpha}, \widetilde{T}) \right)}_{\text{Turbulence Chemistry Interaction (TCI)}}, \\ & \frac{\partial \overline{\rho} \widetilde{u}_i}{\partial t} + \frac{\partial \overline{\rho} \widetilde{u}_k \widetilde{u}_i}{\partial x_k} = -\frac{\partial \overline{p}}{\partial x_i} + \frac{M_r}{Re_r} \frac{\partial}{\partial x_k} \left(\widehat{\mu} \left(\frac{\partial \widetilde{u}_i}{\partial x_k} + \frac{\partial \widetilde{u}_k}{\partial x_i} \right) - \frac{2}{3} \widehat{\mu} \frac{\partial \widetilde{u}_j}{\partial x_j} \delta_{ik} \right) - \underbrace{\frac{\partial}{\partial x_k} \left(\overline{\rho} \widetilde{u}_k \widetilde{u}_i - \overline{\rho} \widetilde{u}_k \widetilde{u}_i \right)}_{\text{Turbulence Subgrid Stress}} \end{split}$$

$$\frac{\partial \overline{\rho} \widetilde{e^t}}{\partial t} + \frac{\partial \overline{\rho} (\widetilde{u}_k + \widehat{V}_k^c) \widetilde{h^t}}{\partial x_k} = \frac{M_r}{Re_r} \frac{\partial}{\partial x_k} \left(\widetilde{u}_i \left(\widehat{\mu} \left(\frac{\partial \widetilde{u}_i}{\partial x_k} + \frac{\partial \widetilde{u}_k}{\partial x_i} \right) - \frac{2}{3} \widehat{\mu} \frac{\partial \widetilde{u}_j}{\partial x_j} \delta_{ik} \right) \right) + \underbrace{\frac{M_r}{Re_r} \frac{\partial}{\partial x_k} \left(\overline{u_i \tau_{ik}} - \widetilde{u}_k \overline{\tau_{ik}} \right)}_{\text{Output}}$$

Velocity-Shear Stress Correlation

27

$$+\frac{M_{r}}{Re_{r}Pr_{r}}\frac{\partial}{\partial x_{k}}\left(\frac{\widehat{\mu}}{\widehat{Pr}}\frac{\partial\widetilde{h}}{\partial x_{k}}-\frac{\widehat{\mu}}{\widehat{Pr}}\sum_{\alpha}\left(\frac{\widehat{Le}_{\alpha}-1}{\widehat{Le}_{\alpha}}\right)\widetilde{h}_{\alpha}\frac{\partial\widetilde{Y}_{\alpha}}{\partial x_{k}}\right)+\frac{\partial\overline{\rho}(\widetilde{k}+k)\widehat{V}_{k}^{c}}{\partial x_{k}}$$
$$-\frac{\partial}{\partial x_{k}}\left(\overline{\rho}\widetilde{u_{k}h}-\overline{\rho}\widetilde{u_{k}h}\right) -\frac{\partial}{\partial x_{k}}\left(\overline{\rho}\widetilde{u_{k}}\frac{u_{i}u_{i}}{2}-\overline{\rho}\widetilde{u}_{k}\frac{\widetilde{u_{i}u_{i}}}{2}\right)$$

Turbulence Subgrid Enthalpy Flux Turbulence Subgrid Kinetic Energy Flux



• With the commonly found definitions

$$\tau(a,b) = \widetilde{a \, b} - \widetilde{a} \, \widetilde{b},$$

$$\tau(a,b,c) = \widetilde{a \, b \, c} - \widetilde{a} \tau(b,c) - \widetilde{b} \tau(a,c) - \widetilde{c} \tau(a,b) - \widetilde{a} \, \widetilde{b} \, \widetilde{c},$$

• The unclosed terms can be written as

$$\widetilde{\rho u_k Y_\alpha} - \overline{\rho} \widetilde{u_k} \widetilde{Y_\alpha} = \overline{\rho} \tau(u_k, Y_\alpha), \\
\widetilde{\rho u_k u_i} - \overline{\rho} \widetilde{u_k} \widetilde{u_i} = \overline{\rho} \tau(u_k, u_i), \\
\widetilde{\rho u_k h} - \overline{\rho} \widetilde{u_k} \widetilde{h} = \overline{\rho} \tau(u_k, h), \\
\widetilde{\rho u_k} \underbrace{\widetilde{u_i u_i}}_2 - \overline{\rho} \widetilde{u_k} \underbrace{\widetilde{u_i u_i}}_2 = \frac{1}{2} \overline{\rho} \tau(u_k, u_i, u_i) - \overline{\rho} \widetilde{u_i} \tau(u_k, u_i).$$

- We either have to represent the above terms as functions of the variables we are solving for or derive the transport equations and solve for them
- If we derive the transport equation for any one of the above unclosed terms we'll find that additional, yet higher order terms appear in those equations. This is referred to as the closure problem.



$$\overline{\rho}\tau(u_k, u_i) - \frac{1}{3}\overline{\rho}\tau(u_j, u_j)\delta_{ik} = -\mu_t \left(\frac{\partial \widetilde{u}_i}{\partial x_k} + \frac{\partial \widetilde{u}_k}{\partial x_i}\right) - \frac{2}{3}\mu_t \frac{\partial \widetilde{u}_j}{\partial x_j}\delta_{ik},$$
$$\overline{\rho}\tau(u_k, Y_\alpha) = -\frac{\mu_t}{Sc_t}\frac{\partial \widetilde{Y}_\alpha}{\partial x_k},$$
$$\overline{\rho}\tau(u_k, h) = -\frac{\mu_t}{Pr_t}\frac{\partial \widetilde{h}}{\partial x_k},$$
$$\frac{1}{2}\overline{\rho}\tau(u_k, u_i, u_i) = -\frac{\mu_t}{\sigma_k}\frac{\partial k}{\partial x_k}$$

In general

- any correlations between molecular transport properties and transported quantities are neglected
- the scalar-temperature correlations in the EoS are typically neglected
- In engineering applications
 - turbulence-chemistry interactions are often neglected
- So how do we obtain turbulence subgrid viscosity?









- Anyone getting started with LES should probably read:
 - Pope, S. B., "Ten Questions Concerning the Large-Eddy Simulation of Turbulent Flows," New J. Phys., 2004, 6, 35.
- To get us started the most common model for the subgrid viscosity is the Smagorinsky model:

$$\begin{split} \mu_t &= \overline{\rho} C_s^2 \Delta_L^2 |S|, \\ |\widehat{S}| &= \sqrt{2 \widehat{S}_{ij} \widehat{S}_{ij}}, \\ \widehat{S}_{ij} &= \frac{1}{2} \left(\frac{\partial \widetilde{u}_i}{\partial x_j} + \frac{\partial \widetilde{u}_j}{\partial x_i} \right), \end{split}$$

~2.2.2

- One of the major advancements in LES is the use of scale similarity to develop the dynamic procedure to estimate the model coefficients. $\overline{\rho \widetilde{u}_i \widetilde{u}_j} - \frac{\overline{\rho \widetilde{u}_i}}{\overline{\rho \widetilde{u}_j}} =$
 - Germano identity:



 Assuming that the Smagorinsky model is applicable at both LES and test filter scales we have:

$$\overline{\overline{\rho}}\mathcal{T}(u_i, u_j) - \frac{1}{3}\overline{\overline{\rho}}\mathcal{T}(u_k, u_k)\delta_{ij} = -\overline{\overline{\rho}}C_s^2\Delta_G^2|\widehat{\widehat{S}}|(2\widehat{\widehat{S}}_{ij} - \frac{2}{3}\widehat{\widehat{S}}_{kk}\delta_{ij}),$$
$$\overline{\overline{\rho}\tau(u_i, u_j)} - \frac{1}{3}\overline{\overline{\rho}\tau(u_k, u_k)}\delta_{ij} = -\overline{\overline{\rho}}C_s^2\Delta_L^2|\widehat{S}|(2\widehat{S}_{ij} - \frac{2}{3}\widehat{S}_{kk}\delta_{ij}),$$

$$|\widehat{\widehat{S}}| = \sqrt{2\widehat{\widehat{S}}_{ij}\widehat{\widehat{S}}_{ij}},$$

$$\widehat{\widehat{S}}_{ij} = \frac{1}{2} \left(\frac{\partial \widetilde{\widetilde{u}}_i}{\partial x_j} + \frac{\partial \widetilde{\widetilde{u}}_j}{\partial x_i} \right) = \frac{1}{2} \left(\frac{\partial}{\partial x_j} \left(\frac{\overline{\rho} \widetilde{u}_i}{\overline{\rho}} \right) + \frac{\partial}{\partial x_i} \left(\frac{\overline{\rho} \widetilde{u}_j}{\overline{\rho}} \right) \right) \approx \frac{1}{2} \left(\frac{\partial \widetilde{u}_i}{\partial x_j} + \frac{\partial \widetilde{u}_j}{\partial x_i} \right),$$

• Substituting above into the Germano identity

$$L_{ij} - \frac{1}{3}L_{kk}\delta_{ij} = C_s^2 M_{ij} = C_s^2 \left(\overline{\rho}\Delta_L^2 |\widehat{S}| (2\widehat{S}_{ij} - \frac{2}{3}\widehat{S}_{kk}\delta_{ij}) - \overline{\rho}(\kappa\Delta_L)^2 |\widehat{\widehat{S}}| (2\widehat{\widehat{S}}_{ij} - \frac{2}{3}\widehat{\widehat{S}}_{kk}\delta_{ij}) \right),$$



- Shaping the Future of Aerospace
- The dynamic procedure relies on minimizing the "square" of the error tensor, which represents the difference between resolved and modeled subgrid stresses

$$E_{ij} = L_{ij} - \frac{1}{3}L_{kk}\delta_{ij} - C_s^2 M_{ij},$$

$$-M_{ij}$$

$$\frac{dE_{ij}E_{ij}}{dC_s^2} = 0, \Rightarrow 2E_{ij}\frac{dE_{ij}}{dC_s^2} = 0, \Rightarrow L_{ij}M_{ij} - \frac{1}{3}L_{kk}M_{ij}\delta_{ij} - C_s^2 M_{ij}M_{ij} = 0,$$

$$C_s^2 = \frac{L_{ij}M_{ij} - \frac{1}{3}L_{kk}M_{ij}\delta_{ij}}{M_{ij}M_{ij}} = \left[\frac{L_{ij}M_{ij}}{M_{ij}M_{ij}}\right].$$

- We can apply this procedure in a similar fashion to any model coefficient, with the caveat that
 - We need to "test-filter" the resolved field with a filter width greater than the filter scale
 - Additional care must be taken to ensure that Cs is not ill posed



 Another common model for the subgrid viscosity is one utilizing the one equation model for the subgrid kinetic energy

$$u_t = \overline{\rho} C_k \Delta_L \sqrt{k}.$$

- The value of the model constant may be computed using the dynamic procedure
- The unclosed form of the subgrid kinetic energy equation is

$$\frac{\partial \overline{\rho}k}{\partial t} + \frac{\partial \overline{\rho}\widetilde{u}_i k}{\partial x_i} = \frac{\partial}{\partial x_i} \left(\widehat{\mu} \frac{\partial k}{\partial x_i} \right) - \overline{\rho}\tau(u_i, u_j) \frac{\partial \widetilde{u}_i}{\partial x_j} - \overline{\rho}\epsilon - \frac{1}{2} \frac{\partial \overline{\rho}\tau(u_j, u_i, u_i)}{\partial x_j} - \left(\overline{u_i} \frac{\partial p}{\partial x_i} - \widetilde{u}_i \frac{\partial \overline{p}}{\partial x_i} \right),$$

• Following closures are commonly used:

$$\begin{aligned} -\overline{\rho}\tau(u_i, u_j)\frac{\partial \widetilde{u}_i}{\partial x_j} &= \left(2\mu_t \left(\widehat{S}_{ij} - \frac{1}{3}\frac{\partial \widetilde{u}_k}{\partial x_k}\delta_{ij}\right) - \frac{2}{3}k\delta_{ij}\right)\frac{\partial \widetilde{u}_i}{\partial x_j} \\ -\overline{\rho}\epsilon &= -C_D\overline{\rho}\frac{k^{3/2}}{\Delta_L}, \\ -\frac{1}{2}\frac{\partial\overline{\rho}\tau(u_j, u_i, u_i)}{\partial x_j} &= \frac{\partial}{\partial x_j}\left(\frac{\mu_t}{\sigma_k}\frac{\partial k}{\partial x_j}\right), \end{aligned}$$

• The velocity-pressure gradient correlation is often neglected, but ...



 Wilcox proposed a compressible correction for high speed flows which can be readily adopted to LES

$$\begin{split} \left(\overline{u_i \frac{\partial p}{\partial x_i}} - \widetilde{u}_i \frac{\partial \overline{p}}{\partial x_i}\right) &= \overline{(\widetilde{u}_i + u_i'') \left(\frac{\partial \overline{p}}{\partial x_i} + \frac{\partial p'}{\partial x_i}\right)} - \widetilde{u}_i \frac{\partial \overline{p}}{\partial x_i} \\ &= \overline{u_i''} \frac{\partial \overline{p}}{\partial x_i} - \overline{p' \frac{\partial u_i''}{\partial x_i}} + \frac{\partial \overline{u_i''p'}}{\partial x_i}, \end{split}$$

- where the last three terms are the pressure work, dilatation, and diffusion
- The compressible correction is then

$$\begin{aligned} \overline{u_i''} \frac{\partial \overline{p}}{\partial x_i} &= \frac{M_t k}{\overline{\rho} \epsilon} \tau(u_i, u_j) \frac{\partial \overline{\rho}}{\partial x_j} \frac{\partial \overline{p}}{\partial x_i}, \\ \overline{p'} \frac{\partial u_i''}{\partial x_i} &= \alpha_2 M_t \overline{\rho} \tau(u_i, u_j) \frac{\partial \widetilde{u}_i}{\partial x_j} - \alpha_3 M_t^2 \overline{\rho} \epsilon, \\ \frac{\partial \overline{u_i'' p'}}{\partial x_i} &= 0, \end{aligned}$$

• where subgrid turbulence Mach number is $M_t = \sqrt{2k/\widetilde{u}_i\widetilde{u}_i}$



• Final form of the turbulent subgrid kinetic energy transport equation



• with M_t=0 the conventional incompressible model is recovered.

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Numerical Methods



- Physical domain discretization (i.e., grid/mesh type):
 - Structured: Cartesian, Generalized Curvilinear Coordinates, Overset
 - Unstructured (hex, tets, prisms, pyramids)
- Equation discretization:
 - Finite Difference (typically only used on structured meshes) (arbitrary order)
 - Finite Volume (cell-centered, cell-vertex, staggered) (typically 2nd order)
 - Finite Element : Discontinuous Galerkin (DG) (high order)
 - Spectral or Pseudo-Spectral (high order)
- Time discretization: \(\lambda\)
 - Explicit: Runge-Kutta, Predictor-Corrector (e.g., MacCormack), Backward Euler, etc.
 - Implicit: Runge-Kutta, Dual Time-Stepping, ADI, DAF, LU, Sundials, Hypre
- Numerical Approach:
 - Pressure projection : Rhie-Chow (typically for "weakly" compressible reacting flows)
 - Density-based (stiff at low Mach numbers)
- - Local Time-Stepping
 - Multigrid
 - Preconditioning (physical and numerical)
 - Parallelization (MPI, OMP, GPU)

Book available on Science Direct Blazek, J., Computational Fluid Dynamics: Principles and Applications, Elsevier, **2005** 38

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• Finite volume scheme in generalized curvilinear coordinates

$$\frac{\partial \mathbf{Q}}{\partial t} + \frac{\partial \mathbf{E}}{\partial x} + \frac{\partial \mathbf{F}}{\partial y} + \frac{\partial \mathbf{G}}{\partial z} = \mathbf{S}$$

$$\iiint_{V} \frac{\partial \mathbf{Q}}{\partial t} dV + \iiint_{V} \left(\frac{\partial \mathbf{E}}{\partial x} + \frac{\partial \mathbf{F}}{\partial y} + \frac{\partial \mathbf{G}}{\partial z}\right) dV = \iiint_{V} \mathbf{S} dV$$
Applying the divergence theorem to the flux terms

$$\frac{\partial}{\partial t} \iiint_V \mathbf{Q} dV + \oint_S \left(\mathbf{E} dS_x + \mathbf{F} dS_y + \mathbf{G} dS_z \right) dV = \iiint_V \mathbf{S} dV$$



Coordinates transformation

$$\xi = \xi(x, y, z)$$

$$\eta = \eta(x, y, z)$$

$$\zeta = \zeta(x, y, z)$$







$$J = \det \left| \frac{\partial(\xi, \eta, \zeta)}{\partial(x, y, z)} \right| = \det \left| \begin{pmatrix} \xi_x & \xi_y & \zeta_z \\ \eta_x & \eta_y & \eta_z \\ \zeta_x & \zeta_y & \zeta_z \end{pmatrix} \right| = \det \left| \begin{pmatrix} x_\xi & x_\eta & x_\zeta \\ y_\xi & y_\eta & y_\zeta \\ z_\xi & z_\eta & z_\zeta \end{pmatrix}^{-1} \right|$$
$$= \frac{1}{x_\xi (y_\eta z_\zeta - y_\zeta z_\eta) - x_\eta (y_\xi z_\zeta - y_\zeta z_\xi) + x_\zeta (y_\xi z_\eta - y_\eta z_\xi)}$$

40



• Transformed governing equation in conservative form

$$\begin{aligned} \frac{\partial \bar{\mathbf{Q}}}{\partial t} + \frac{\partial \bar{\mathbf{E}}}{\partial \xi} + \frac{\partial \bar{\mathbf{F}}}{\partial \eta} + \frac{\partial \bar{\mathbf{G}}}{\partial \zeta} &= \bar{\mathbf{S}} \\ \bar{\mathbf{Q}} &= \frac{\mathbf{Q}}{J} \\ \bar{\mathbf{E}} &= \frac{1}{J} (\xi_x \mathbf{E} + \xi_y \mathbf{F} + \xi_z \mathbf{G}) \\ \bar{\mathbf{F}} &= \frac{1}{J} (\eta_x \mathbf{E} + \eta_y \mathbf{F} + \eta_z \mathbf{G}) \\ \bar{\mathbf{G}} &= \frac{1}{J} (\zeta_x \mathbf{E} + \zeta_y \mathbf{F} + \zeta_z \mathbf{G}) \\ \bar{\mathbf{G}} &= \frac{1}{J} (\zeta_x \mathbf{E} + \zeta_y \mathbf{F} + \zeta_z \mathbf{G}) \end{aligned} \qquad \mathbf{Q} = \frac{1}{J} \begin{bmatrix} \bar{\rho} \\ \bar{\rho} \widetilde{Y}_1 \\ \vdots \\ \bar{\rho} \widetilde{Y}_2 \\ \vdots \\ \bar{\rho} \widetilde{Y}_N \\ \bar{\rho} \widetilde{u} \\ \bar{\rho} \widetilde{v} \\ \bar{\rho} \widetilde{w} \end{bmatrix}$$

 $\frac{\overline{\rho}\widetilde{e}^t}{\overline{\rho}k}$

Numerical Methods



42

- Time integration
 - Explicit

$$\begin{split} \Delta \bar{\mathbf{Q}} &= \bar{\mathbf{Q}}^{n+1} - \bar{\mathbf{Q}}^n = \Delta t \left(-\frac{\partial \bar{\mathbf{E}}}{\partial \xi} \right|^n - \frac{\partial \bar{\mathbf{F}}}{\partial \eta} \right|^n - \frac{\partial \bar{\mathbf{G}}}{\partial \zeta} \right|^n + \bar{\mathbf{S}}^n \right) \\ \cdot \text{Implicit} &= \bar{\mathbf{E}}^{n+1} = \bar{\mathbf{E}}^n + \frac{\partial \bar{\mathbf{E}}}{\partial \bar{\mathbf{Q}}} \Delta t + \mathcal{O}(\Delta t^2) \\ \bar{\mathbf{E}}^{n+1} &= \bar{\mathbf{E}}^n + \frac{\partial \bar{\mathbf{E}}}{\partial \bar{\mathbf{Q}}} \frac{\partial \bar{\mathbf{Q}}}{\partial t} \Delta t + \mathcal{O}(\Delta t^2) \\ \bar{\mathbf{E}}^{n+1} &= \bar{\mathbf{E}}^n + \frac{\partial \bar{\mathbf{E}}}{\partial \bar{\mathbf{Q}}} \left(\frac{\bar{\mathbf{Q}}^{n+1} - \bar{\mathbf{Q}}^n}{\Delta t} + \mathcal{O}(\Delta t) \right) \Delta t + \mathcal{O}(\Delta t^2) \\ \bar{\mathbf{E}}^{n+1} &= \bar{\mathbf{E}}^n + \frac{\partial \bar{\mathbf{E}}}{\partial \bar{\mathbf{Q}}} \left(\frac{\bar{\mathbf{Q}}}{\Delta t} + \mathcal{O}(\Delta t) \right) \Delta t + \mathcal{O}(\Delta t^2) \\ &= \bar{\mathbf{E}}^{n+1} = \bar{\mathbf{E}}^n + \frac{\partial \bar{\mathbf{E}}}{\partial \bar{\mathbf{Q}}} \Delta \bar{\mathbf{Q}} + \mathcal{O}(\Delta t^2) \\ &= \left(\frac{1}{\Delta t} - \frac{\partial}{\partial \xi} \frac{\partial \bar{\mathbf{E}}}{\partial \bar{\mathbf{Q}}} \right|^n - \frac{\partial}{\partial \eta} \frac{\partial \bar{\mathbf{F}}}{\partial \bar{\mathbf{Q}}} \right|^n - \frac{\partial}{\partial \zeta} \frac{\partial \bar{\mathbf{G}}}{\partial \bar{\mathbf{Q}}} \right|^n + \frac{\partial \bar{\mathbf{S}}}{\partial \bar{\mathbf{Q}}} \right|^n - \bar{\mathbf{S}}^n \right) = -\mathbf{R}^n_{\mathbf{Q}} \\ &= - \left(\frac{\partial \bar{\mathbf{E}}}{\partial \xi} \right|^n + \frac{\partial \bar{\mathbf{F}}}{\partial \eta} \bigg|^n + \frac{\partial \bar{\mathbf{G}}}{\partial \zeta} \bigg|^n - \bar{\mathbf{S}}^n \right) = -\mathbf{R}^n_{\mathbf{Q}} \\ \end{array}$$

Numerical Methods



- Discretization of Convective Fluxes
 - Central
 - Flux-vector splitting
 - Flux-difference splitting
 - TVD



- General spatial discretization for fluxes at cell faces (cell centered scheme)
 - Average of fluxes from adjacent cells

$$\mathbf{E}\,\Delta S)_{I+1/2,J} \approx \frac{1}{2} \big(\mathbf{E}(\mathbf{Q}_{I,J}) + \mathbf{E}(\mathbf{Q}_{I+1,J}) \big) \Delta S_{I+1/2,J}$$

Average of variables to cell face

$$(\mathbf{E}\,\Delta S)_{I+1/2,J} \approx \mathbf{E}(\mathbf{Q}_{I+1/2,J})\Delta S_{I+1/2,J} \qquad \mathbf{Q}_{I+1/2,J} = \frac{1}{2}(\mathbf{Q}_{I,J} + \mathbf{Q}_{I+1,J})$$

• Flux reconstruction from quantities interpolated to left and right side of the face $(\mathbf{E}\Delta S)_{I+1/2,J} \approx f_{Flux}(\mathbf{Q}_L, \mathbf{Q}_R, \Delta S_{I+1/2,J})$ $\mathbf{Q}_L = f_{Interp}(\dots, \mathbf{Q}_{I-1,J}, \mathbf{Q}_{I,J}, \dots)$ $\mathbf{Q}_R = f_{Interp}(\dots, \mathbf{Q}_{I,J}, \mathbf{Q}_{I+1,J}, \dots)$



Verification

- Richardson extrapolation and Grid Convergence Index (GCI)
- Method of Manufactured Solutions (strong verification)
- Comparisons with exact solutions of canonical problems (numerical methods)
- Comparisons with DNS (for modeling)
- Uncertainty Quantification (sensitivities)
- Comparisons with Experiments (weak verification)
- Richardson extrapolation and Grid Convergence Index (GCI)

$$Error = f(\Delta) - f^{exact} = C\Delta^{p} + H.O.T$$

$$Diff(2\Delta, \Delta) = f(2\Delta) - f(\Delta) = C\Delta^{p}(2^{p} - 1)$$

$$Error = C^{*} \frac{Diff(2\Delta, \Delta)}{2^{p} - 1}$$

Safety Factor
(1.25 for p=1, 3 for p=2)



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CFD Modeling and Simulation of High Speed Reacting Flows: Applications

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Outline



- Example Applications
 - (Re)Introduction to Problem Space
 - External Aero of Hypersonic Vehicles
 - Facility Nozzle Simulations for Ground Experimentation
 - Component Simulations
 - Scale Resolving (LES) Simulations vs. Reynolds Average Simulations (RAS)





- VULCAN-CFD is a hybrid Structured/Unstructured 3-D compressible flow solver
 - Solves the Reynolds-averaged or spatially filtered (LES) equations governing thermal equilibrium/non-equilibrium gases with chemical reactions
 - Supports any combination of FNS and/or PNS solution procedures
 - Parallelized via domain decomposition using portable MPI libraries
 - Currently supports 36 boundary conditions
 - Arbitrary C0 and non-C0 block to block connectivity supported
 - Variety of turbulence closure models (LEVMs, ARSM, hybrid RAS/LES, dynamic SGS closures)
 - Generalized chemistry treatment (finite rate with allowances for arbitrary reaction orders and pressure-dependent kinetics, CARM)
 - Collaborative development environment with continuous regression testing
 - Portable to a wide class of Unix/Linux architectures
 - Suite of post-processing tools specific to high-speed propulsion
- VULCAN-CFD is available to US Nationals (Export Controlled) and a reasonable level of support is offered as well
 - VULCAN-CFD is used extensively by government, industry and academia for external and internal hypersonic flow analysis
 - On the order of 10 new requests per year are processed





Simulation in ground facility



Current Coupled Numerical-Experimental Approach









Simulation in ground facility



External Aero of Hypersonic Flight Vehicles





External Aero of Hypersonic Flight Vehicles









Simulation in ground facility







Injector Geometries







- High quality grids are as important as turbulence modeling selection
 - Hex elements are most efficient and accurate
 - Grid alignment with shock features desired but in practice only achievable for the vehicle bow shock
 - Orthogonality and uniformity (gradual stretch rates of less then 10-15%) preferred
- Awareness of general flow features and their resolution requirements is needed (matter of experience)
 - Near-wall resolution requirements for wall-resolved (y+ < 1) vs. wall-modeled (y+ ~ 20) simulations
 - Increased grid densities near shear layers





Contours of the Mach number through the centerline of the strut injector obtained on coarse, medium, and fine meshes





1D profiles of total pressure and mixing efficiency vs. distance

- Order of accuracy (rate of convergence)
 - One for the mixing efficiency
 - ~1.5 for the total pressure recovery
- Error bars represent the Grid Convergence Index (GCI) obtained using the Richardson Extrapolation:

$$Error = C^* \frac{Diff(2\Delta, \Delta)}{2^p - 1}$$
Safety Factor
(1.25 for p=1, 3 for p=2)

 Mixing efficiency appears more sensitive to the grid resolution than other 1D quantities (e.g., total pressure, Mach, thrust potential)





Strut











- Strut injectors induce largest decrease in the Mach number and largest increase in the vorticity (or circulation) and turbulence kinetic energy (TKE)
- Ramp and flushwall injectors induce comparable levels of vorticity and TKE
- TKE is comparable among the three injectors in the far field

Reduction in the Mach number is a result of both the viscous drag on the injector bodies (for the strut and ramp) and the induced shock waves. What about injector mixing performance?

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One-Dimensional Integrated Quantities





- Strut Injectors
 - have highest mixing efficiency but also the largest total pressure loss (smallest recovery)
 - exhibit rapid mixing in the strut wake region x=0 to 3
- Ramp Injectors
 - despite comparable vortical and TKE features, exhibit better mixing than the flushwall ...
 - albeit at the expense of the lower total pressure recovery
- Flushwall
 - have lowest mixing, highest total pressure recovery, and ...
 - highest specific thrust potential? (least total pressure loss + largest momentum flux ratio)



- Injector flat plate was numerically "flown" along a constant-Q ascent trajectory from subsonic to Mach 16 free stream conditions
- As the Mach number increases the skin friction decreases but heat flux increases (heat flux predictions typically require y+ < 0.1)
- Numerically-induced boundary layer transition can be observed
- Flow transition is one of the hardest phenomena to predict accurately (trips)



Cross-Stream PLIF and CFI: Strut Injector





X=0.5 z 🗸





Turbulent Simulation



Laminar Simulation





Simulation in ground facility







Major flow features of supersonic flow over cavity.

Nominal Test Conditions	
Mach	2.92
Total Temperature	258K
Total Pressure	0.69MPa
Freestream Unit Re	6.7x10 ⁷ /m



Microsecond spark shadowgraph. Settles, et al. (1980)





visual clarity.









Instantaneous snapshots of velocity with data locations highlighted





Shear layer velocity profiles shifted to emphasize growth rate.



Grid Refinement



71





Simulation in ground facility


Cavity-Based Flameholder Application





Nominal Conditions	Case 1	Case 2	Case 3
Facility Mach No.	2.0 [2.0 [2.0 [
Facility T _o [K]	589.0 [589.0 1	589.0 (
Facility P _o [kPa]	483.0 [483.0 [483.0 (
C2H4 Flow Rate [SLPM]	0.0	56.0 [99.0 (
C2H4 T _o [K]	N/A (310.0 [310.0 (





Sensitivity to RAS Turbulence/Mixing Model





Hybrid RAS/LES Sensitivity to SGS Closures









Propulsion-airframe integrated scramjet

KR/LH02072001



Question: Don't we have enough practical design experience and physics knowledge to build robust devices?

Answer: Most designers and experienced staff think so ... until there are unforeseen difficulties that require detailed (beyond what relevant experiments can provide) understanding of complex multiphysics interactions.

How should CFD be used:

- At the least, CFD analysis offers a risk-mitigating strategy that can
 potentially confirm and/or raise questions about some design well before
 difficulties are encountered
 - Current state-of-the-art allows CFD to be used effectively in this context because only qualitative accuracy is required
- At the most, CFD analysis will be the only tool available and used to evaluate a particular design's performance. This can occur if the experimental and/or design space for practical device are beyond our current capability and experience.



- Current SoA for CFD analysis of high-speed propulsion flow paths are Reynolds-Averaged Simulations
 - All scales of turbulence are modeled \rightarrow often leading source of uncertainty
 - Boussinesq approximation with LEVM
 - Gradient diffusion assumption with constant Pr_t and Sc_t
 - Turbulence-Chemistry interactions neglected (or crudely modeled)
 - Modeling strategy is relatively mature with only "evolutionary" improvements documented over the past 15-20 years → Current focus is primarily on UQ
 - Even vehicle-scale simulations (or matrices of simulations) are computationally affordable for problems of programmatic interest on current supercomputers (typically 1-2 weeks to solution)
- Scale-Resolved Simulations (LES) have the potential to substantially reduce turbulence model uncertainty (for some models)
 - Only the smaller turbulence scales are modeled (larger scales resolved)
 - Model form uncertainty (related to turbulence) can be reduced with grid resolution
 - Computational cost about 100 times that of above RAS



- Continue to leverage RAS capabilities in design and analysis of high-speed reacting flows while systematically investigating modeling sensitivities on a caseby-case basis
 - Higher-order closures for the Reynolds stress tensor may prove beneficial for the shock-dominated internal flows prevalent in high speed propulsion devices
- Utilize LES (keeping large computational costs in mind):
 - to improve understanding of physical interactions (universities are doing this)
 - to investigate impact of unsteady effects
 - for cases (configurations and operating conditions) exhibiting high sensitivities
 - for isolated key flight conditions near operability bounds (we need to know these)
 - to reduce model-form uncertainty with RAS
- Improvements in predictive fidelity of LES over RAS must still be demonstrated
 - Are current LES SGS models sufficient for simulations of highly compressible flows?
 - Can we utilize LES as "truth" when experiments are unavailable?
- Questions?

RAS continues to be the dominant tool for high-speed reacting flow analysis



Shaping the Future of Aerospace









- <u>Branch Mission</u>: perform multidisciplinary research to develop advanced technology for hypersonic airbreathing propulsion systems for aerospace vehicles. Focus on airframe-integrated engine concepts having high performance over a wide Mach range.
- **Physics Model Development**: develop, implement, and validate Computational Fluid Dynamics (CFD) models for the design, prediction and assessment of the performance of hypersonic air-breathing propulsion systems and system components.
- **Numerical Methods and Code Development**: develop and implement enhanced numerical methods appropriate for the simulation of highly compressible flows with shocks and finite-rate chemistry.
- **Code Application**: provide state-of-the-art hypersonic airbreathing propulsion system design, analysis, and optimization capability in support of NASA's high speed full-scale vision vehicle development, subscale flight demonstrators, and associated ground tests
- **Experimental Airbreathing Propulsion**: develop and apply state-of-the-art hypersonic airbreathing propulsion test techniques for the NASA Langley Scramjet Test Complex and advance facility flight simulation capabilities. Develop comprehensive development, demonstration and verification test plans for national flight demo programs utilizing the national test infrastructure and capability.
- Vehicle Configuration Development & Optimization: design, development and optimization of ramjet/scramjet flowpaths for a given vehicle and mission, flowpath/engine performance analysis and operability assessments, design and analysis tool development, and the projection of ground test data assessments to the requisite flight environments.
- Flight Test: PI role on flight experiments and support major flight demonstrations, develop flight test approach, ensure science and/or demonstration objectives are met, develop flowpath and subsystem requirements to ensure operability and performance goals/requirements are met, develop measurement and instrumentation requirements.

Scramjet Propulsion System





KR/LH02072001

Scramjet Propulsion System





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HIFiRE2 Direct Connect Rig (HDCR) Experiment





Sounding rocket used for HIFIRE flight



HDCR combustor experimental rig



HDCR combustor mold line.

- Tested in the NASA LaRC Arc-Heated Scramjet Test
 Facility [10] in support of HIFiRE flight experiment
- Primary test objectives included developing fuel splits for:
 - Sufficient unstart margin
 - Successful dual-mode transition
 - Scram-mode operation at $\phi > 0.7$
- Employed 144 static pressure ports and 19 surface thermocouples
- Data collected at numerous test points spanning simulated flight Mach numbers 5.84-8.0

HIFiRE2 Direct Connect Rig (HDCR) Experiment





Current RAS appear to correctly model the heat release in the flowpath since the heat release is responsible for the pressure rise

HIFiRE2 Direct Combustor Rig (HDCR)





The position of the leading shock shifts downstream from the primary injector after transition from dual to scram mode

87

HIFiRE2 Direct Combustor Rig (HDCR)





Contours of the normalized heat release rate suggest dominance of subsonic combustion for dual mode operation and supersonic combustion for scram mode

HIFiRE Direct Combustor Rig (HDCR)





Flame index contours are consistent with the normalized heat release rate suggesting dominance of subsonic combustion for dual mode operation and supersonic combustion for scram mode

Injector Testing for Hypervelocity Mixing







Carbon Matrix Composite (CMC) Panel Testing for Scramjets:







Toward Predictive Use of CFD for Design and Development of Propulsion Devices



