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1.0 SUMMARY

The Modular Thermal Analyzer Routine (MOTAR) is a general thermal analysis routine with strong capabilities for performing thermal analysis of systems containing flowing fluids, fluid system controls (valves, heat exchangers, etc.), life support systems, and thermal radiation situations. Its modular organization permits the analysis of a very wide range of thermal problems from simple problems containing a few conduction nodes to those containing complicated flow and radiation analysis with each problem type being analyzed with peak computational efficiency and maximum ease of use.

MOTAR gives its user the ability to obtain the transient or steady state solution of a problem using either the forward differencing, mid-differencing or backward differencing finite difference solution methods. Transient and steady state analyses may be performed during the course of a single problem so that as an example, a transient analysis may be initiated at some steady state condition. In addition any number of transient and/or steady state problems may be analyzed on a given problem by applying the user logic capability on MOTAR.

Numerous options are available with MOTAR for determining time and temperature dependent thermal conductors, capacitances, and absorbed heat values. In addition to these standard options the user may supply any functional relationship desired for these elements in the user logic block. Option are available for analysis of convection and flow conductors which utilizes the results of the simultaneously performed flow analysis. Also, extensive radiation analysis capability is supplied which provides for determination of radiation interchange factors for any combination of specular and diffuse radiation. A number of thermal nodes may be combined into a single surface to greatly reduce the amount of computer time required for determining the interchange factors and calculating the net heat flow due to radiation interchange during the problem. Additional thermal analysis capabilities available as options include (1) cabin air thermal and mass balance analysis including condensation and/or evaporation from the walls (2) heat exchanger simulation ability for counterflow, crossflow, and parallel flow exchangers and (3) inline heater analysis.

A pressure/flow analysis of a fluid flow system consisting of an arbitrary tube network may be performed simultaneous with the thermal analysis so that on each iteration the thermal problem is updated based upon the latest flow conditions and vice versa. If only a pressure/flow analysis is desired with no thermal analysis this may also be performed on MOTAR. The tube/flow path methods used on previous VMSC routines for flow analysis have been replaced in MOTAR with a pressure node/tube conductor network method. Using this method the number of simultaneous equation that must be solved is reduced. Also, the user has much more flexibility as to the type of flow system that he may analyze. For instance, the user may connect any number of tubes at a junction from two to a large number, whereas previously three and only three
connections were permitted. Also, the connections need not follow any fixed pattern as before (i.e., off-center flow paths are handled automatically). The valve pressure drops are readily included in the pressure/flow balance for all types of valves with the revised method contrary to previous methods. Several options are available for obtaining friction factors and head loss values.

To enhance the pressure/flow analysis capability extensive valve and pump analysis capabilities have been included in MOTAR. The previous five valve types plus considerable additional capabilities have been simplified into three valve types. The valves have been formulated so that the control of either cooling (space radiator) or heat (solar absorber) situations may be controlled with any of the valve types. Pump options including tabulated pump curve of pump flow vs pressure drop or polynomial curves of pressure drop vs flow rate are available with accelerated methods for convergence of the pump and flow system characteristics.

The input for MOTAR has been designed to give the user a high degree of effectiveness and flexibility while maintaining an easy-to-use format. The effectiveness is accomplished by providing powerful options to the user which permit the input of large quantities of data with a single entry in the input. The flexibility is obtained by providing the user with a large number of options for each data entry. Many features were incorporated to make the routine easy to use which include the use of descriptive names to identify data blocks, the ability to omit blocks not requiring input data for a given problem, and the use of a free form input format. Several input/output options were made available to aid the user which take advantage of the magnetic tapes available on the Univac 1108 computer. Included in these were the data tape/edit capability, restart tape ability, plotting and/or starting from a previously generated history tape and the supplying of heat flux values on a tape.

The organization and programming methods applied to MOTAR achieved a high degree of computer utilization efficiency in terms of computer execution time and storage space required for a given problem. The computer time required to perform a given problem on MOTAR is approximately 40 to 50 percent that required for the currently existing widely used routines $^{14,15,24}$. The computer storage requirement for MOTAR is approximately 25 percent more than the most commonly used routines $^{14,15}$ for the most simple problems but the data storage techniques for the more complicated options should save a considerable amount of space.

* Superscripts represent the reference number for references found in Section 6.0.
INTRODUCTION

During the past eight years the Vought Missiles and Space Company (VMSC) of LTV Aerospace Corporation has been involved in the development of special purpose computer routines for the thermal analysis of systems with flowing fluid, life support components and enclosure radiation. The development of these special purpose routines was necessary to obtain the analytical capability required for the design and simulation of space radiator systems, environmental control and life support systems, and fuel cell cooling systems, since the required analytical tools didn't exist. Some of the VMSC developed routines were used for thermal simulation of the entire spacecraft for the LM ascent stage, LM decent stage, and the Apollo Block I and Block II Command Modules.

Advances in computer technology such as the advent of the Univac 1108 Fortran V computer language made possible the assembling of the previously developed specialized capabilities into a single computer routine without loss of computational efficiency. This assembly of these capabilities into a user oriented routine efficient in terms of both computer time and space was the objective of the Modular Thermalizer Routine (MOTAR) which was developed by VMSC and is described in this report.
3.0 ROUTINE ANALYTICAL METHODS

This section describes the analytical methods used in the Modular Thermal Analyzer Routine (MOTAR). MOTAR solves thermal and flow problems simultaneously for either transient or steady state temperature conditions. In either case, it solves a discrete lumped parameter finite difference user input Mathematical Model. Several methods of solution are available to the user for the transient thermal problem including explicit forward differencing, implicit mid-differencing and implicit backward differencing. Two methods are available for solution of the flow problem; namely, the direct solution method using the Gauss-Jordan elimination technique for small problems, and the successive over relaxation method for larger problems.

MOTAR contains special capabilities to enhance thermal and flow analysis. Capabilities related to thermal analysis of flowing and life support systems include the calculation of flow and convection thermal conductors using flow data, numerous options for determining heat exchanger performance, and cabin thermal and mass analysis. In addition to the normal radiation convector capability, provisions are available for determination of radiation interchange factors (Script - F) for any combination of specular and diffuse radiation and incorporation of those factors into the thermal analysis. These Script F values can be determined for infrared as well as any number of wave length bands for incoming non-infrared radiation. The pressure flow analysis is augmented with numerous options for determining friction factors, determining valve performance, and balancing the system flow rates with pump curves.

These capabilities are discussed in detail in Sections 3.1 and 3.2 which follow. Thermal analysis capabilities are discussed in 3.1 and pressure/flow analysis capabilities are discussed in Section 3.2.

3.1 THERMAL ANALYSIS

MOTAR gives its user the capability to determine the approximate solution to the differential equations which govern the transient temperature behavior in a media. This solution is obtained by approximating the non-linear partial differential equations with a set of difference equations which are solved by successively solving a set of algebraic equations. Provisions have been incorporated into the solution methods to permit the analysis of a general n-dimensional structural problem as well as problems containing radiation and convection to a fluid. Because the finite difference method evaluates equation constants at very short time intervals nonlinearities such as radiation, varying convection coefficients, and temperature dependent properties are easily approximated by linearizing over the small intervals. Numerous options are available for evaluation of these nonlinearities. Options are also available for characterizing components commonly found in flowing fluid and life support systems such as heat exchangers, fluid heaters and life support cabins.

The following sections describe the MOTAR thermal analysis capability in detail. A brief derivation of the finite difference equations is given in Section 3.1.1. The methods for solving these equations are discussed in
3.1.2 and the supporting features for evaluating the nonlinear coefficients and characterizing the special components are discussed in Section 3.1.3.

3.1.1 Finite Difference Analysis

The nonlinear partial differential equation which governs the heat conduction in a three-dimensional conducting media can be derived by use of Fourier's heat conduction equation and an energy balance on a differential element to be

\[ \rho C_p \frac{\partial T}{\partial \tau} = \frac{\partial}{\partial x} \left( k_x \frac{\partial T}{\partial x} \right) + \frac{\partial}{\partial y} \left( k_y \frac{\partial T}{\partial y} \right) + \frac{\partial}{\partial z} \left( k_z \frac{\partial T}{\partial z} \right) + q \]  

(1)

where
- \( T \) = the temperature which is a function of \( x, y, z \) and time, \( \tau \)
- \( \rho \) = density of the material
- \( C_p \) = specific heat of the material
- \( k_x, k_y, k_z \) = thermal conductivity in directions \( x, y, \) and \( z \)
- \( q \) = the heat generation per unit volume and unit time

The thermal properties, \( \rho \), \( C_p \), and \( k \), can in general be functions of temperature which makes equation (1) a second order, nonlinear partial differential equation. A general form of the boundary conditions which may be encountered is given by

\[ f_1(X_B, Y_B, Z_B, T) \left. \frac{\partial T}{\partial N} \right| _{X_B, Y_B, Z_B} = \]

\[ f_2(X_B, Y_B, Z_B, \tau, T) \cdot T(X_B, Y_B, Z_B) + f_3(X_B, Y_B, Z_B, \tau, T) \]

(2)

where \( X_B, Y_B, Z_B \) is the body surface
- \( N \) is the surface normal

When \( f_1 = 0 \), the boundary condition is that of spatially variant and time variant surface temperature. When \( f_2 = 0 \), the boundary condition is that of spatially variant and time variant surface heat flux. For \( f_1 \), \( f_2 \) and \( f_3 \) all non-zero, the equation represents a convective, radiative, or combined convective/radiative boundary condition where both the heat transfer coefficient and the sink temperature are spatially variant and time variant.

The equations defined by equations (1) and (2) have been solved for a large number of special cases 1-10 but in general approximations must
be introduced in order to solve a given problem. One such approximation which permits the general solution of equations (1) and (2) (subject to the approximation) is that of finite difference representation of the differential quantities. This permits the non-linear partial differential equation given by (1) to be written in terms of a set of linear algebraic equations which with the aid of the electronic computer can be successively solved to obtain general problem solution. This is the approach taken in MOTAR.

Using the finite difference method, the partial derivatives given by equation (1) are approximated by differences as follows:

Let

\[ \frac{\partial T}{\partial \tau} = \frac{T_{i}^{n+1} - T_{i}^{n}}{\Delta \tau} \]  

(3)

where \( T_{i}^{n+1} \) = the temperature at node \( i \) at the finite approximation of time (iteration) \( n + 1 \).

Node \( i \) is located at \( x, y, z \)

\( T_{i}^{n} \) = the temperature of node \( i \) at time \( n \)

\( \Delta \tau \) = the finite time increment

We will assume the thermal properties can be assumed constant over the small time increment, \( \Delta \tau \). Thus, the terms on the right side of equation (1) become

\[ k_{n} \frac{\partial^{2} T}{\partial N^{2}} \]

(4)

where \( N \) is either \( x, y, \) or \( z \)

We will approximate \( \frac{\partial T}{\partial N^{2}} \) by subdividing each \( N \) coordinate into a grid in space of width \( \Delta N \). The approximation is then,

\[ \frac{\partial^{2} T}{\partial N^{2}} = \frac{T_{i-\Delta n}^{m} - T_{i}^{m} - T_{i}^{m} - T_{i+\Delta n}^{m}}{\Delta N \cdot \Delta N} \quad \frac{T_{i-\Delta n}^{m} - T_{i+\Delta n}^{m}}{\Delta N \cdot \Delta N} \quad \frac{T_{i-\Delta n}^{m} - T_{i}^{m} + T_{i+\Delta n}^{m} - T_{i}^{m}}{\Delta N \cdot \Delta N} \]

(4)
Where
\[ N \] is the direction of the derivative (x, y, or z)
\[ T_{i-\Delta n}^m \] is the temperature of the node adjacent to i in the -N direction at time m
\[ T_i^m \] is the temperature of node i at time m
\[ T_{i+\Delta n}^m \] is the temperature of the node adjacent to i in the +N direction at time m
\[ \Delta N \] is the grid with in the N direction
\[ m \] is the time for evaluation of the derivative somewhere between \( r \) and \( r + \Delta r \).

If the above approximations of equations (3) and (4) are substituted into equation (1) we get
\[
\rho_i C_{pi} \left( \frac{T_{i}^{n+1} - T_{i}^n}{\Delta \tau} \right) = k_x \left[ \frac{T_{i-\Delta x}^m - T_i^m}{\Delta x^2} + \frac{T_{i+\Delta x}^m - T_i^m}{\Delta x^2} \right] + k_y \left[ \frac{T_{i-\Delta y}^m - T_i^m}{\Delta y^2} + \frac{T_{i+\Delta y}^m - T_i^m}{\Delta y^2} \right] + k_z \left[ \frac{T_{i-\Delta z}^m - T_i^m}{\Delta z^2} + \frac{T_{i+\Delta z}^m - T_i^m}{\Delta z^2} \right] + q
\]

If we multiply the above equation by the volume of node i, \( \Delta V_i \), where
\[
\Delta V_i = \Delta X \cdot \Delta Y \cdot \Delta Z
\]
We get
\[
\rho_i \Delta V_i C_{pi} \left( \frac{T_{i}^{n+1} - T_{i}^n}{\Delta \tau} \right) = k_x \Delta y \Delta z \left( \frac{T_{i-\Delta x}^m - T_i^m}{\Delta x} \right) + k_y \Delta x \Delta z \left( \frac{T_{i-\Delta y}^m - T_i^m}{\Delta y} \right) + k_z \Delta x \Delta y \left( \frac{T_{i-\Delta z}^m - T_i^m}{\Delta z} \right) + q \Delta V_i
\]
If we note that

\[ \rho_i \Delta V_i = W_i = \text{Mass of node } i \]
\[ A_y \Delta z = A_x = \text{Area for conduction in the } x \text{ direction} \]
\[ A_x \Delta z = A_y = \text{Area for conduction in the } y \text{ direction} \]
\[ A_x \Delta y = A_z = \text{Area for conduction in the } z \text{ direction} \]
\[ q_i \Delta V = Q_i^m = \text{The total heat originating at node } i \text{ at time } m \]

then we can write the above equation as

\[
W_i C_p (T_i^{n+1} - T_i^n) = \frac{K_x A_x}{\Delta x} \left( T_i^m - T_i^{m+1} \right) + \frac{K_x A_x}{\Delta x} \left( T_i^{m+1} - T_i^m \right) \\
+ \frac{K_y A_y}{\Delta y} \left( T_i^{m+1} - T_i^m \right) + \frac{K_y A_y}{\Delta y} \left( T_i^m - T_i^{m+1} \right) + \frac{K_z A_z}{\Delta z} \left( T_i^{m+1} - T_i^m \right) + \frac{K_z A_z}{\Delta z} \left( T_i^m - T_i^{m+1} \right) + Q_i^m \]

(5)

If we examine equation (5) term by term we see that the left side is the rate of heat storage required to raise the temperature of the node i mass, \( W_i \), at the rate of \( (T_i^{n+1} - T_i^n)/\Delta \tau \) and is thus the heat storage rate of node i. Each of the first six terms on the right of equation (5) represent the rate of heat transfer into node i at one of the six surfaces of the three dimensional parallelepiped from surrounding nodes. The \( kA/\Delta x \) portion of these terms represent the thermal conductance between node i and the adjacent node j. \( Q_i \) represents the total rate of heat originating at node i. Thus, the right hand side represents the total heat transfer rate into node i from its surroundings. If we define

\[ U_{ij} = \frac{kA}{\Delta x} \]
and
\[ C_i = \frac{W_i C_p}{\Delta \tau} \]

We can write equation (5) in the general form

\[
C_i \left( T_i^{n+1} - T_i^n \right) = \sum_{j=1}^{nc} U_{ij} \left( T_j^m - T_i^m \right) + Q_i^m 
\]

(6)
where \( nc \) is the number of conductances attaching node \( i \) to surrounding nodes

\[ C_i \] is the thermal capacitance of node \( i \)

\[ U_{ij} \] is the thermal conductance between nodes \( i \) and \( j \).

Equation (6) was defined in terms of conduction heat transfer only. It can be easily extended to analyze a flowing fluid. Consider fluid flowing in a tube. The energy balance on an elemental length, \( dx \), of the fluid can be used to derive the governing differential equation

\[
\begin{align*}
\dot{W}_{cp} T & \quad dx
\end{align*}
\]

\[
\frac{\partial}{\partial x} \left( \dot{W}_{cp} (T + \frac{\partial T}{\partial x} dX) \right)
\]

![Energy Stored = Energy in - energy out](image)

or

\[
\rho A_c dX C_p \frac{\partial T}{\partial \tau} = \dot{W}_{cp} T - \dot{W}_{cp} \left( T + \frac{\partial T}{\partial X} dX \right) - hPdX (T-T_t)
\]

\[
\rho A_c C_p \frac{\partial T}{\partial \tau} = -\dot{W}_{cp} \frac{\partial T}{\partial X} - hP(T-T_t)
\]

(7)

where

\( \rho \) = fluid density

\( A_c \) = Fluid flow cross sectional area

\( C_p \) = Fluid specific heat

\( \tau \) = time

\( \dot{W} \) = fluid mass flow rate down tube

\( P \) = wetted perimeter of flow passage

\( T \) = fluid temperature

\( T_t \) = tube temperature

\( h \) = convection heat transfer coefficient
If we make the following difference approximations for the partial derivatives,

\[
\frac{\partial T}{\partial r} = \frac{T^{n+1} - T^n}{\Delta r}
\]

\[
\frac{\partial T}{\partial x} = \frac{T^m - T_{x-\Delta x}}{\Delta x}
\]

substitute these into equation (7) and multiply by \(\Delta X\) we get the finite difference fluid heat balance equation for an element of length \(\Delta X\) and cross sectional area \(A_c\)

\[
\rho A_c \Delta X \left[ \frac{\Delta T}{\Delta r} \right] = -\dot{W}C_p \left[ T^{m+1} - T^m \right] - hP\Delta X \left[ T^m - T_t^m \right]
\]

or

\[
C \left[ \frac{\Delta T}{\Delta r} \right] = \dot{W}C_p \left[ T_u^m - T^m \right] + hA_t \left[ T_t^m - T^m \right]
\]

(8)

where

- \(T^{n+1}\) = fluid temperature of the node at location \(X\) at time \(r + \Delta r\)
- \(T^n\) = fluid temperature at \(X\) and time \(r\)
- \(T_u^m\) = fluid temperature of node at \(X\) and time \(r\) if \(m = n\) and \(r + \Delta r\) if \(m = n + 1\)
- \(T^m\) = fluid temperature of node at \(X\) and time \(r\) if \(m = n\) or at time \(r + \Delta r\) if \(m = n + 1\)
- \(T_t^m\) = tube temperature of tube node at \(X\) and time \(r\) if \(m = n\) or at time \(r + \Delta r\) if \(m = n + 1\)
- \(C\) = \(\dot{W}C_p\) product for the fluid node

Note that equation (8) can be cast in the same form as equation (6) with one exception. The energy represented by the \(\dot{W}C_p (T_u - T)\) term only flows one direction. That is, energy flows from the upstream fluid node but not from the downstream fluid node. Thus, if we make \(\dot{W}C_p\) a one way conductor and the \(hA\) convection conductor, equation (8) is in the form of equation (6) and we see that we can extend equation (6) to include analysis of flowing fluid and convection.
Equation (6) can also be extended to include analysis of radiation heat exchange. If we define $UA_{ij}$ by

$$UA_{ij} = \sigma \mathcal{A}_{ij} \left[ T_j^2 + T_i^2 \right]$$

where $\sigma$ = the Stephan-Baltzman Constant

$\mathcal{A}_{ij}$ = the radiation interchange factor

where in this case, $UA_{ij}$ is the heat transfer coefficient between two surfaces by radiation then radiation heat transfer analysis can be included in equation (6). Thus, with the above definitions for conductances, equation (6) is applicable for a very wide class of thermal problems which include conduction, radiation, convection and flowing fluid.

The linear algebraic equation (6) represents an approximation to the nonlinear second order partial differential equation (1). To obtain the general solution of temperature as a function of time and location in a body, equation (6) must be written for each nodal point in the body. (The shorter the distance between nodal points, the more accurate the solution.) These equations must then be solved simultaneously for values of temperature at the node locations at time $r + \Delta r$ based upon the temperature at time $r$ and the heat flow rate during the time between time $r$ and $r + \Delta r$. The time is then incremented so that $r$ becomes $r + \Delta r$ and the process repeated. Thus, the simultaneous equations are successively solved to obtain the temperature vs time for each nodal location in the problem. The approximate solution to equation (1) is then obtained in this manner.

As previously mentioned, the value of $m$ in equation (6) represents the point within the time increment from $r$ to $r + \Delta r$ for evaluating the flow of heat. The choice of $m$ has a significant effect on the problem solution formulation. For instance $m = n$, equation (6) becomes

$$C_i \left[ \frac{T^n_{i+1} - T^n_i}{\Delta r} \right] = \sum_{j=1}^{nc} U_{ij} \left[ T^n_j - T^n_i \right] + Q^n_i \quad i=1, NN$$

and it can be solved explicitly for $T^n_{i+1}$ in terms of known conditions at time $n$ as follows:

$$T^n_{i+1} = T^n_i + \frac{\Delta r}{C_i} \left[ \sum_{j=1}^{nc} U_{ij} \left( T^n_j - T^n_i \right) + Q^n_i \right] \quad i=1, NN$$

(9)

Here, $NN$ = the number of nodes. This is the explicit or forward-difference finite difference method.

If $m$ in equation (6) is $n + 1$, it can be re-written as
This equation represents a set of $NN$ simultaneous equations to be solved for the $T$'s and is called the implicit backward difference method. It is much more difficult to solve than equation (9) but it is more efficient than (9) for certain types of problems because it has no stability restrictions on the time increment.

Equation (9) assumes the heat transfer rates are established at the time $r$, the start of the temperature iteration whereas, equation (10) assumes the rates are established at time $r + \Delta r$. A third method assumes the heat transfer rate is some weighted average between that at $r$ and that at $r + \Delta r$. Let the net heat transfer rate $Q_{net}$ be given by

$$Q_{net} = A Q_{net}^{n+1} + [1-A] Q_{net}^n$$

Then

$$C_i \left( \frac{T_i^{n+1}-T_i^n}{\Delta r} \right) = A Q_{net}^{n+1} + [1-A] Q_{net}^n$$

and

$$C_i \left( \frac{T_i^{n+1}-T_i^n}{\Delta r} \right) = A \left( \sum_{j=1}^{nc} U_{ij} \left[ T_j^{n+1}-T_i^{n+1} \right] + Q_i^{n+1} \right)$$

$$+ (1-A) \left( \sum_{j=1}^{nc} U_{ij} \left[ T_j^{n+1}-T_i^n \right] + Q_i^n \right)$$

or

$$\left( \frac{C_i + A}{\Delta r} \sum_{j=1}^{nc} U_{ij} \right) T_i^{n+1} - \sum_{j=1}^{nc} A U_{ij} T_j^{n+1} = C_i T_i^n + A Q_i^{n+1}$$

$$+ (1-A) \left( \sum_{j=1}^{nc} U_{ij} \left[ T_j^n-T_i^n \right] + Q_i^n \right)$$

for $i = 1, NN$
Equation (11) represents the general form of the implicit equation. When \( A = 1 \) the backward difference equation given by equation (10) results. When \( A = 0 \), the forward difference equation given by (9) results. When \( A = 0.5 \) the solution method is called the implicit mid-difference.

In MOTAR, equation (9) is solved for the explicit method and equation (11) is solved for the implicit methods. Only values for \( A \) of 0.5 and greater are considered for the implicit methods because stability problems arise for values of a less than 0.5.

A discussion of the implementation of these methods is presented in the following section.

3.1.2 Temperature Solution Methods

In the previous section the nonlinear partial differential equation governing the temperature in a material was cast in the form of a set of linear algebraic equations by use of finite difference approximation. These equations are solved by MOTAR to obtain the approximate temperature vs time trace for each lump location (or the steady state temperature distribution for steady state problems). This is done by obtaining successive solutions of the equations at small increments of time with each time point solution depending on that of the previous time. Two basic methods are currently available to the MOTAR user for evaluating these transient equations depending on the point in the time interval that the flow of heat is assumed to occur. These are the explicit method wherein the heat flow rate is assumed to be that at the start of the time step and the implicit method where the heat flow can be evaluated anywhere between mean over the time step and the end of the time step. Each of the methods are discussed in more detail below. Methods for steady state analysis are also discussed.

3.1.2.1 Explicit Temperature Solution

When, in obtaining the solution to the finite difference temperature equations, the flow of heat is assumed to occur at the start of the iteration the updated temperature for each lump can be solved directly from known values of temperatures, heat fluxes, and coefficients and no simultaneous solution is required. The general form of the equation to be solved for each node is given by

\[
T_i^{n+1} = T_i^n + \frac{\Delta r}{c_i} \left( \sum_{j=1}^{nc} U_{ij}^n \left[ T_j^n - T_j^n \right] + Q_i \right) \quad i=1,NN
\]  

(12)
where \( T_{i}^{n+1} \) = the temperature of node \( i \) at iteration \( n+1 \)
\( T_{i}^{n} \) = the temperature of node \( i \) at iteration \( n \)
\( \Delta r \) = the iteration time increment
\( C = \) the lunar capacitance = \( m \cdot C_{p} \)
\( C_{p} = \) the specific heat
\( I_{ij} \) = the conductance between nodes \( i \) and \( j \)
\( n_{c} \) = the number of conductances
\( Q_{i} \) = the absorbed incident heat or the heat generated internally
\( N_{N} \) = the number of nodes

Since all times on the right side of equation (12) are known at the start of each iteration \( T_{n+1} \) can be solved directly. This is performed in MOTAR by subroutine EXPLCT and its referenced subroutines.

The values used for \( U_{ij} \) must be obtained by different methods depending on the mechanism for heat transfer, (i.e., conduction, connection, flowing fluid, etc.). The methods used in MOTAR for determining \( U_{ij} \) for heat transfer mechanisms are discussed in section 3.1.3.

Equation (12) gives a stable solution as long as the time increment, \( \Delta r \), meets the following requirement

\[
\Delta r \leq \frac{C_{i}}{\sum_{j=1}^{n_{lc}} U_{ij} + \sum_{j=1}^{n_{rc}} 4 \sum_{j=1}^{n_{rc}} A_{ij} T_{i}^{3}} \tag{13}
\]

Where \( n_{lc} = \) Number of linear conductor
\( n_{rc} = \) Number of radiation conductor

MOTAR has two options which the user may specify regarding the time increment. If option 1 is specified, the time increment will be "overridden" for those lumps having smaller maximum time increments than the problem increment. When this occurs, the maximum time increment given by equation (13) is substituted for \( \Delta r \) in equation (12), resulting in a "steady state" solution for those nodes overridden. If option 2 is specified, the entire problem will be iterated at the value of the smallest maximum time increment given by equation (13). The user may specify maximum and minimum values of the problem iteration increment for this option and if the maximum time increment of some node is below the specified minimum iteration increment the problem will be terminated.
3.1.2.2 Implicit Temperature Solution

The finite difference transient temperature equations can be formulated so that the flow of heat is assumed to occur at some point during the iteration time step other than the start. With this formulation, the set of temperature equations must be solved simultaneously as shown below.

The general form of the finite difference temperature equation assuming the rate of heat flow is evaluated at the fraction, \(A\), of the iteration is given by

\[
\left(\frac{C_i + A \sum_{j=1}^{nc} U_{ij}}{\Delta r}\right) T_i^{n+1} - \sum_{j=1}^{nc} A U_{ij} T_j^{n+1} = (1-A) \left(\sum_{j=1}^{nc} U_{ij} [T_j^n - T_i^n] + Q_i^n\right) + A Q_i^{n+1} + \frac{C_i}{\Delta r} T_i^n \quad i = 1, N \tag{14}
\]

Where the symbols are as defined in equation (12). \(A\) is the fraction of the heat flux at the end of the time step and \((1-A)\) is the fraction of the heat flux at its start; i.e., if \(A = 0.5\), the flux is the average between that at the start and that at the end of the iteration resulting in the mid-differencing technique. If \(A = 1.0\) all the heat flow is assumed to occur at the end of the iteration resulting in the backward difference method.

If we define the following,

\[
b_{ii} = \frac{C_i + A \sum_{j=1}^{nc} U_{ij}}{\Delta r}
\]

\[
b_{ij} = -A U_{ij} \quad i \neq j
\]

\[
C_i = (1-A) \sum_{j=1}^{nc} U_{ij} [T_j^n - T_i^n] + Q_i^n + A Q_i^{n+1} + \frac{C_i}{\Delta r} T_i^n
\]

we can write \(N\) equations from equation (14) for the \(N\) lumps in the problem.

\[
\sum_{j=1}^{N} b_{ij} T_j^{n+1} = C_i \quad i = 1, N
\]

This set of equations are solved for \(T_j^{n+1}\) in MOTAR at each time step using a modified version of the successive-point-overrelaxation method. The following is a summary of the procedure:
1. Assume an initial temperature array called $T$

2. Calculate time and temperature dependent constants

3. Call PRETMP

4. Calculate values of temperature from equation one lump at a time. Call this value $T_i$ for the $i$th lump. The value is then modified by the equation $T_i = T_i + ORP (T_i - T_i)$, ORP being the overrelaxation parameter. The value of $T_i$ is then compared to $T_i$. If $T_i - T_i$ is less than an input DTMXA (iteration limit) the iteration of this particular equation is temporarily suspended. The value of $T_i$ is set equal to $T_i$ following the comparison.

5. This procedure is continued until each lump's equation has been iterated until the error satisfies the tolerance; i.e., until $T_i - T_i$ is less than DTMXA for each lump, is tentatively achieved.

6. The process is repeated from step 3. As soon as the last lump satisfies the $T_i - T_i$ < DTMXA, if all equations were not iterated, the process is again begun for each lump from step 3.

The standard SOR procedure is modified in that those equations which satisfy the $|T_i - T_i| < DTMXA$ are not iterated until all equations have satisfied the relation. For some problems this procedure has some of the features of a block-iterative solution. If in a large problem a heat source is localized, the temperature change would, in an ordinary SOR method, propagate outward from the heat source in waves. With the above modification, only those equations of nodes in the immediate area of the disturbance will be iterated on the second and succeeding few iterations. After these reach the prescribed iteration limit the procedure is restarted and the number of nodes whose equations are iterated continuously increases. After a certain time subsequent to the passage of the "solution wave" through the various lumps, those lumps near the original disturbance will have reached a steady state value such that further iterations would not alter their temperature more than the prescribed limit applied to the iterations. This modification therefore intuitively leads to a fewer number of iterations, on the average.

The iteration limit, DTMXA, on the equations is assumed to be that which guarantees the error in the iteration process to be less than some specified amount. This amount of iteration error should be chosen to be well within the expected truncation error.

The selection of overrelaxation parameters, ORP, is of paramount importance to the user, in that proper selection of it can reduce run time significantly. Theoretical analyses of convergence rates for the successive overrelaxation iteration are summarized in Reference 3. For elliptic
equations with boundary conditions of the type that the function is specified constant on the boundary, a typical predicted curve of the number of iterations to solve the equation as a function of the overrelaxation parameter is as shown in the sketch below. A value of 1.4 has been found from experience to be a good first estimate.

![Sketch showing the number of iterations to solve equations as a function of the overrelaxation parameter.](image)

3.1.2.3 Steady State Solution

Two methods are available in MOTAR for determining the steady state solution for the temperature distribution in a given problem. The first method iterates the basic explicit equation, equation (12), to solution. The second method obtains the solution to the implicit equation given by equation (14). The first method results in a block iterative Sidel iteration method and the second results in a point iterative Sidel method with successive overrelaxation. The second method generally converges faster but the first requires less space and thus, can handle the largest problem.

**Explicit Steady State**

The explicit steady state method is basically the solution of equation (12) with constant boundary conditions. To accelerate the convergence the maximum time increment, \( \Delta r_{\text{max}} \), for each node given by equation (13) is substituted for \( \Delta r \) in equation (12). This results in the steady state solution for each node with its surrounding conditions on the previous iteration for each iteration for problems with no radiation. For problems with radiation this results in the largest stable change permitted.

**Implicit Steady State**

The implicit steady state method is basically the solution of equation (14) with constant boundary conditions, with \( A=1 \) and with a large
value for $\Delta r$, the time increment, so that the terms $C/\Delta r$ approach zero. This results in the equation

$$T_i - \frac{\sum U_{ij} T_j}{\sum U_{ij}} = \frac{Q_i}{\sum U_{ij}} \quad i=1,n$$

Which is solved using the iterative procedure described in section 3.1.2.2.

3.1.3 Thermal Analysis Features

This section describes some of the more significant thermal analysis features used to enhance the temperature solution methods described in Section 3.1.2. The items discussed are (1) conductor calculation methods, (2) heat exchanger analysis method, (3) cabin analysis method and (4) radiation interchange methods.

3.1.3.1 Conductor Calculation Method

The values of $U_{ij}$ in equations (12) and (14) are determined by different methods depending on the heat transfer mechanism. The methods used to determine the conductors for conduction, convection, radiation, and for fluid crossing the boundary from one node into another are described below.

**Conduction**

The conductance between two nodes for conduction heat transfer is given by:

$$U_{ij} = \frac{k A_{ij}}{\Delta x_{ij}}$$

Where $k$ = thermal conductivity of lumps i and j
$A_{ij}$ = the area for conduction between i and j
$\Delta x_{ij}$ = the conduction distance from the center of node i to the center of node j

If the thermal conductivities of nodes i and j are different, either because of different materials or variation with temperature, the conduction conductance is given by

$$U_{ij} = \frac{A_{ij}}{k_i + k_j}$$

$$\frac{\Delta x_i}{k_i} + \frac{\Delta x_j}{k_j}$$
Where

\[ \Delta X_i = \text{the conduction distance from the center of node } i \text{ to the boundary between nodes } i \text{ and } j \]

\[ \Delta X_j = \text{the conduction distance in node } j \]

\[ k_i, k_j = \text{the thermal conductivity in nodes } i \text{ and } j \text{ respectively} \]

**Convection Conductors**

The value of \( U_{ij} \) for convection between a fluid and a surface is given by

\[ U_{ij} = h A \]

Where

\( h = \text{the convection coefficient} \)

\( A = \text{the convection area} \)

Several methods are directly available in MOTAR for determining the heat transfer coefficient, \( h \).

For flow in a tube the flow regime is assured to be laminar when the Reynolds number is 2000 or less. For this regime the heat transfer coefficient is calculated by

\[
h = k \left[ 3.66 F_1 + \frac{0.0155 F_2}{\frac{R e}{D} X + 0.015 \left( \frac{1}{R e} \frac{X}{D} \right)^{1/3}} \right]
\]

(16)

Where

\( h = \text{thermal conductivity} \)

\( D = \text{hydraulic diameter to flow} \)

\( X = \text{distance from tube entrance} \)

\( Re = \text{Reynolds number} \)

\[
Re = \frac{4 \dot{m}}{\mu p}
\]

\( \dot{m} = \text{flow rate of fluid} \)

\( \mu = \text{viscosity of fluid} \)

\( p = \text{wetted perimeter of fluid flow passage} \)
\[ F_1 = \text{An input factor for modifying fully developed flow} \]
\[ F_2 = \text{An input factor for modifying developing flow} \]

Equation (16) is a curve fit obtained by VMSC to approximate the Gratz solution to flow in a tube for values of \( \frac{X}{D} \) greater than 0.001.

The convection heat transfer coefficient for flow in a tube in the transition flow regime (2000 < Re < 6400) is approximated in MOTAR by the following relation:

\[
h = \frac{K}{D} \left[ 0.116 \left( \frac{Re^{2/3}}{125} \right)(Pr)^{1/3} \right]
\]

This relation was derived by Hausen and holds only for fully developed flow.

The relation used in MOTAR to determine \( h \) for turbulent flow (Re \( \geq \) 6400) is the following:

\[
h = 0.023 \frac{K}{D} (Re)^{8}(Pr)^{1/3}
\]

A more general option available on MOTAR for determining the heat transfer coefficient is given by the relation

\[ St(Pr)^{2/3} = f(Re) \]

Where \( St = \text{ Stanton number} \)

\[ St = \frac{Nu}{Re \, Pr} = \frac{h}{Cp \, V} \]

\( V = \text{Average fluid velocity} \)

\( F(Re) = \text{An arbitrary function of Reynolds number which the user can input as a table} \)

The heat transfer coefficient is calculated by

\[
h = \frac{K}{D} \, F(Re) \, Re(Pr)^{1/3}
\]
Flow Conductors

As described in Section 3.1.1, equation (8) a flow conductor is needed to analyze the problem of a fluid flowing in a tube. The flow conductor is a one way conductor from $j$ to $i$ and is calculated by

$$ UA_{ij} = \frac{W}{C_{pi}} $$

Where

$ UA_{ij} $ = the conductance from the upstream lump

$ W $ = the mass flow rate in the tube

$ C_{pi} $ = the fluid specific heat for lump $i$

The flow rate can be input directly or it may be obtained from a flow solution which is being performed simultaneously with the temperature solution problem (Section 3.2)

Radiation Conductors

The value of the conductance between two nodes, $i$ and $j$, by radiation is given by

$$ U_{ij} = \sigma \, F \, A_{ij} \left( \frac{[T_j+T_z]^2 + [T_i+T_z]^2}{[T_j+T_z] + [T_i+T_z]} \right) $$

Where

$ \sigma $ = the Stefan-Boltzman Constant

$ F $ = the radiation interchange factor between nodes $i$ and $j$

$ T_z $ = the value for conversion to absolute temperature

This relation is obtained by assuming that the heat transfer between nodes $i$ and $j$ by radiation is proportional to the temperature difference between these nodes during the iteration time span rather than proportional to the difference in the fourth power of the temperatures. This results in the above linearized coefficient. $ \sigma $ and $ T_z $ are input values so that the user may use any system of units for his problem. $ F $ may be either input or calculated internally as described in Section 3.1.3.5.

3.1.3.2 Heat Exchanger Analysis

Four subroutines have been written to facilitate the thermal analysis of systems containing heat exchangers. These are HXNT for analysis of counter flow heat exchangers, HXPAR for parallel flow exchangers, HXCROS for cross flow
exchangers and HXEFF for any heat exchanger with an input effectiveness. These subroutines calculate the outlet temperatures of two sides based upon the inlet temperatures and heat exchanger effectiveness. The relations used for effectiveness are given by the following equations, taken from reference 17 for the first three subroutines.

**Counterflow**

\[
\epsilon = \frac{1 - e^{-\frac{UA}{(MC)_s} \left\{1 - \frac{(MC)_s}{(MC)_l}\right\}}}{1 - e^{-\frac{UA}{(MC)_l} \left\{1 - \frac{(MC)_s}{(MC)_l}\right\}}}
\]

Where \( \epsilon \) = effectiveness

\( UA \) = overall effectiveness

\( (MC)_s \) = mass, specific heat product for the side with the smallest MC

\( (MC)_l \) = mass, specific heat product for the side with the largest MC

The limiting case for this relation are:

1. When \( (MC)_s / (MC)_l = 0 \),
   \[ \epsilon = 1 - e^{-UA/(MC)_s} \]

2. When \( (MC)_s / (MC)_l = 1 \)
   \[ \epsilon = \frac{UA}{(MC)_s} \]

**Parallel Flow**

\[
\epsilon = \frac{UA}{(MC)_s} \left[1 + \frac{(MC)_s}{(MC)_l}\right]
\]

The limiting cases are

1. When \( (MC)_s / (MC)_l = 0 \),
   \[ \epsilon = 1 - e^{-UA/(MC)_s} \]
(2) When \((MC)_s/(MC)_l = 1.0\),

\[ \epsilon = \frac{1 - e^{-2 UA/(MC)_s}}{2.0} \]

**Cross Flow**

A. Both Streams Unmixed

\[ \epsilon = 1 - e^{\left[ e^{\left( \frac{UA}{(MC)_s(MC)_l} \right)} - 1 \right]} \]

Where \[ \eta = \left[ \frac{(MC)_s}{UA} \right] 0.22 \]

B. Both Streams Mixed

\[ \epsilon = \frac{UA}{(MC)_s} \frac{UA}{(MC)_s} + \frac{UA}{(MC)_s} \frac{UA}{(MC)_l} \]

C. Stream \((MC)_s\) Unmixed

\[ \epsilon = \frac{1 - e^{-\left(\frac{(MC)_s}{(MC)_l}\right)}}{1 - e^{-\left(\frac{(MC)_s}{(MC)_s}\right)}} \]

D. Stream \((MC)_l\) Unmixed

\[ \epsilon = \frac{1 - e^{-\left(\frac{(MC)_l}{(MC)_s}\right)}}{1 - e^{-\left(\frac{(MC)_l}{(MC)_l}\right)}} \]
Using the effectiveness as calculated by any of the above methods, the outlet temperatures are calculated as follows:

1. For the side with the smallest MC, \((MC)_S\):

\[
T_{outS} = T_{inS} - \epsilon (T_{inS} - T_{in})
\]

2. The outlet temperature for the side with the large MC is then calculated by

\[
T_{outL} = \left(\frac{(MC)_L}{(MC)_S}\right) (T_{inS} - T_{outS}) + T_{inL}
\]

3.1.3.3 Inline Heater Analysis

Provisions for the analysis of a fluid heater have been included in MOTAR with subroutine HEATER. This subroutine simulates an electrical heater with a control system which turns the heater on when a specified sensor lump drops below a set value and turns the heater off when the specified sensor lump rises above another set value. When the heater is on an input quantity of heat is added to the heater node.

3.1.3.4 Cabin Analysis

A subroutine has been written for use with MOTAR which will give the user the ability to perform thermal and mass balance analyses on cabin air systems.

The cabin heat transfer and condensation analysis involves the two-component flow of a condensable vapor and a non-condensable gas, with condensation of the vapor occurring on surfaces in contact with the fluid. Two problems of this nature have been studied extensively.

1. Condensation on, or evaporation from, a surface over which a free stream of fluid is passing. In this case, for relatively low mass transfer rates, the fluid properties are assumed to be constant.

2. Dehumidification of a confined fluid stream by a bank of tubes. In this case there is a marked change in the temperature and vapor content of the fluid, and the detailed deposition of the condensate is not of primary interest. This type of analysis is usually handled on an overall basis similar to heat exchanges effectiveness calculations.

The following additional assumptions have been made with respect to the cabin atmospheric conditions.

1. The heat of circulation in the cabin is sufficiently high that the temperature and humidity are effectively the same throughout the cabin.
2. The velocity at all points where heat transfer and/or condensation can occur is known, and is proportional to the total mass flow rate in the cabin.

These assumptions make it possible to calculate the heat and vapor balance in the cabin for the entire volume as a unit, and to solve the heat transfer and condensation equations at each node independently of the other nodes.

Cabin humidity can be determined from an overall vapor balance in the cabin. The total vapor in the cabin at the end of an iteration is:

\[ W_v = W_{v_{i-1}} + W_{v_{in}} - W_{v_{out}} - \Sigma W_{L} \]

Where
- \( W_{v_{i-1}} \) = mass of vapor in cabin at start of iteration \( i-1 \)
- \( W_{v_{in}} \) = mass of vapor flowing into cabin during iteration \( i \)
- \( W_{v_{out}} \) = mass of vapor flowing out of cabin during iteration \( i \)
- \( \Sigma W_{L} \) = mass of vapor condensed during iteration \( i-1 \)

\( W_{v_{in}} \) is determined from the known conditions of the gas flowing into the cabin.

\[ W_{v_{in}} = \dot{m}_{in} \left[ \frac{\psi_{in}}{\psi_{in} + 1} \right] \]

Where
- \( \dot{m}_{in} \) = mass flow rate into cabin
- \( \psi_{in} \) = specific humidity of gas flowing into cabin
- \( \psi_{in} \) = time increment

It is assumed that an equal volume of gas is flowing out of the cabin. Then,

\[ W_{v_{out}} = \dot{m}_{out} \left[ \frac{\psi_{c}}{\psi_{c} + 1} \right] \]

Where
- \( \psi_{c} \) = specific humidity in the cabin (at the end of the previous iteration)

and

\[ \dot{m}_{out} = \dot{m}_{in} \left[ \frac{\rho_{c}}{\rho_{in}} \right] \]

Where
- \( \rho_{c} \) = cabin density
- \( \rho_{in} \) = density of gas flowing into cabin

The condensation term \( \Sigma W_{L} \) is determined from the calculations for the individual nodes as described below. The properties of the cabin atmosphere are determined from the calculated
value of \( W \). The vapor pressure in the cabin is

\[
P_v = \frac{W_v}{V_c} \quad R_v \quad T_c
\]

Where

- \( V_c \) = cabin volume
- \( R_v \) = gas constant
- \( T_c \) = temperature of cabin gas
- \( P_v \) = vapor pressure

Assuming that the cabin pressure \( P_c \) is a constant, the gas partial pressure \( P_a \) is:

\[
P_a = P_c - P_v
\]

and

\[
W_a = \frac{P_a}{R_a \quad T_c}
\]

Where \( W_a \) = mass of non-condensible gas in the cabin.

Now the new value of specific humidity in the cabin can be determined by

\[
\psi_c = \frac{W_v}{W_a}
\]

The properties of the atmosphere can now be determined by

\[
\mu_c = \frac{X \mu_g + \psi_c \mu_v}{X + \psi_c}
\]

\[
C_{pc} = \frac{C_{pg} + \psi_c C_{pv}}{1 + \psi_c}
\]

\[
k_c = \frac{X k_g + \psi_c k_y}{X + \psi_c}
\]

\[
\rho_c = \frac{W_v + W_s}{V_c}
\]

Where

- \( \mu \) = viscosity
- \( C_p \) = specific heat
- \( k \) = thermal conductivity
- \( X \) = molecular weight ratio, \( M_v \)
- \( M_g \)
and all values are evaluated at $T_{c}^{i-1}$. Cabin temperature $T_{c}$ can be determined by a heat balance on the cabin atmosphere.

$$
T_{c} = T_{c}^{i-1} + \frac{\dot{m} \text{ in } C_{p,c} (T_{in} - T_{c}^{i-1}) - \Sigma Q_{L}}{(W_{v} + W_{a}) \text{ C}_{p,c}}
$$

Where
- $T_{c}^{i-1}$ = $T_{c}$ after previous iteration
- $T_{in}$ = temperature of gas flowing into cabin
- $\Sigma Q_{L}$ = net heat loss to cabin lumps

The heat transfer between the cabin atmosphere and the tube and structure lumps in the cabin is defined by:

$$Q_{Li} = hA_{Li} \left[ T_{c} - T_{Li} \right] \Delta r$$

Where
- $h$ = heat transfer coefficient
- $A_{Li}$ = heat transfer area of lump
- $T_{Li}$ = temperature of tube lump
- $\Delta r$ = time increment

Using the Colburn-Chilton heat transfer-mass transfer analogy, the condensation (or evaporation) at the tube lump is determined by:

$$\Delta W_{Li} = K_{m} A_{Li} \left[ P_{v} - P_{wi} \right] \Delta r$$

Where
- $W_{Li}$ = condensation on wall, lb.
- $K_{m}$ = mass transfer coefficient
- $P_{wi}$ = vapor pressure at $T_{Li}$

The latent heat addition to the lump due to this condensation is

$$\Delta Q_{\lambda} = \Delta W_{Li} \lambda$$

Where
- $\lambda$ = latent heat of vaporization (BTU/lb.)

The vapor pressure $P_{wi}$ can be determined by a relationship derived from the Clausius-Clapeyron equation and the perfect gas law (Appendix K of Reference 16)
Three methods are available for determining mass and heat transfer coefficient. For tube lumps the equations from Reference 17 for gas flowing normal to the tube axis was assumed. Three different equations are used depending on the value of the Reynolds number.

\[
\text{Nu} = 0.43 + 0.533 \left( \text{Re} \right)^{0.5} \left( \text{Pr} \right)^{0.31} \quad \text{Re} < 4000
\]

\[
\text{Nu} = 0.43 + 0.193 \left( \text{Re} \right)^{0.189} \left( \text{Pr} \right)^{0.31} \quad 4000 < \text{Re} < 40000
\]

\[
\text{Nu} = 0.43 + 0.0265 \left( \text{Re} \right)^{0.0805} \left( \text{Pr} \right)^{0.31} \quad 40000 < \text{Re} < 400000
\]

These equations were derived for an air-vapor mixture, but should be relatively accurate for other similar gases. The Nusselt and Reynolds numbers in the equations are defined using the tube diameter for the characteristic dimension, and the velocity in the Reynolds number is input at each lump and ratioed to the total cabin atmosphere flow rate.

\[
\nu_i = \frac{\nu_i \text{circ}}{\nu_\text{circ}}
\]

Where

- \( \nu_\text{circ} \) = nominal cabin atmosphere circulation rate
- \( \nu_i \) = velocity at lump at \( \nu_\text{circ} \)
- \( \text{Wc} \) = circulation rate at time of calculation

The second option assumes flat plate flow for cabin wall lumps. In this case the heat transfer coefficient, for laminar flow, varies along the plate. Hence, direction of gas flow and the location of an assumed leading edge must be assumed. The equation for flat plates from Reference is:

\[
\text{Nu} = 0.332 \left( \text{Re} \right)^{0.5} \left( \text{Pr} \right)^{1/3}
\]

Where the Nusselt and Reynolds's numbers are local values and are defined by the distance \( X \) from the assumed leading edge. For a wall lump of length \( L_i \) which is located a distance \( L_{10} \) from the assumed leading edge, the average Nusselt number can be defined as:
\[
N_u = 0.664 \ Pr^{1/3} \left[ (Re_1)^{0.5} - (Re_0)^{0.5} \right]
\]

Where
- \( N_u \) is defined by \( L_1 \)
- \( Re_0 \) is defined by \( L_i0 \)
- \( Re_1 \) is defined by \( L_i0 + L_i \)

The third option is a direct user input for convective heat transfer coefficient.

For the determination of mass transfer coefficients, the same equations as were used for heat transfer coefficient can be used with the Sherwood number substituted for Nusselt number and Schmidt number for Prandtl number. However, if the diffusion coefficient for the cabin is approximately equal to thermal diffusivity, the Sherwood number is equal to the Nusselt number and the mass transfer coefficient can be determined directly from the heat transfer coefficient. That is:

\[
Sh = Nu
\]

\[
\frac{K_mRT_gx}{D} = \frac{h_x}{k}
\]

If \( D \approx a \) then

\[
K_m = \frac{hD}{\alpha \rho p C_p RT_g}
\]

\[
K_m \approx \frac{h}{C_p P_c}
\]

This is the Lewis relationship (Reference 17). For a mixture of oxygen and water vapor characteristic values are .866 for the diffusion coefficient, \( D \), and .879 for thermal diffusivity, \( a \), so the relationship should be valid.

For cabin tube and wall lumps the values for \( \Delta Q_{L_i} \) and \( \Delta Q_{A_i} \) are added to the basic heat balance equation for these lumps. Values for \( \Delta Q_{L_i} \) are summed for all participating lumps for input to the cabin atmosphere heat balance. Values for \( \Delta W_{L_i} \) are also summed for all lumps for cabin humidity balance, and the value for total water condensed on each lump \( W_{L_i} \) is maintained.

If the rate of evaporation or condensation is high it would be possible for the cabin humidity to change significantly during a single iteration. This could lead, for example, to overestimating condensation by assuming that the humidity is constant in the calculation. A test of the approximate vapor pressure in the cabin at the end of the iteration is
made, and the condensation or evaporation at any lump is reduced, if the sign of the $\Delta W_{Li}$ term is changed. A value $W_v'$ is calculated by:

$$W_v' = W_v^{i-1} - \Sigma W_{Li}$$

and

$$P_v' = \frac{W_v'}{144 \sqrt{V_c}} R_v T_g$$

Then for each lump if

$$\frac{P_v' - P_{wi}}{P_v - P_{wi}} < 0$$

a new value of $\Delta W_{Li}$ is calculated by:

$$\Delta W_{Li} = \left[ \frac{P_v - P_{wi}}{P_v' - P_{wi}} \right]$$

The new values of $\Delta W_{Li}$ are now again summed for the new value of $\Sigma \Delta W_L$ for establishing cabin humidity for the next iteration. A test is also made to assure that $W_v'$ is never less than zero.

3.1.3.5 Radiation Interchange Analysis

Capabilities have been incorporated into MOTAR to facilitate the analysis of radiation heat transfer in an enclosure. The capabilities include the ability to:

1. Analyze diffuse and/or specular infrared radiation in an enclosure
2. Analyze diffuse and/or specular non-infrared radiation for as many wave bands as desired.
3. Consolidate several temperature nodes into a single surface to improve computational efficiency

A radiation surface is defined as a group of temperature nodes which may be assumed to have identical radiating properties, angle factors and interchange factors.

The subroutines account for the net radiation heat transfer between a number of surfaces due to emitted radiation from each surface, reflected radiation from each surface, and radiation from any number of incident sources. The reflection of the energy originally emitted by another surface or from an external source may be either diffuse, specular, or any combination of the two.
Infrared Radiation

The radiosity of a surface is defined as the flux of infrared radiation leaving that surface with a diffuse distribution (according to Lambert's Law). That energy leaving a surface which has been reflected in a specular manner does not contribute to the radiosity of that surface. The incident infrared radiosity is denoted by the symbol $H$. The reflectance $(1 - \epsilon)$ of a surface is separated into two components, the diffuse reflectance $(\rho)$, and the specular reflectance $(\rho_s)$. Here is the emittance of the surface and is equivalent to the absorptance for long wavelength radiation. With the angle factors $(F_{ij})$ defined in the normal way, there exist similar angle factors which relate the geometrical ability of surface $i$ to radiate to surface $j$ by means of a mirror-like reflection from specular surface $k$. Reference to Figure 1 indicates the method of imagery which will enable the calculation of these reflected angle factors. Here the angle factor to surface $j$ is identical with the angle factor to the image of surface $j$. Also the angle factor is limited by the ability of surface $i$ to "see" through the "window" of surface $k$. With the specular surface angle factors so defined, an interchange factor $E_{ij}$ is defined similarly to reference 18 as follows:

$$E_{ij} = \sum_k \rho_s^k F_{ij}(k) + \sum_k \sum_l (\rho_s^k)(\rho_s^l) F_{ij}(k,l) + \cdots$$

Here $F_{ij}(k)$ is the angle factor from $i$ to $j$ as seen in the specular surface $k$, $F_{ij}(k,l)$ is the angle factor from $i$ to $j$ as seen in the double specular reflection from $k$ and $l$. There are an infinite number of possible combinations of these multi-reflections. It is evident that the interchange factors account for the specularly reflected radiant flux from the reflecting surface. This portion of total leaving flux is not a component of the radiosity of that surface. The radiosity may be written

$$B_i = \epsilon_i \sigma T_i^4 + \rho_i H_i,$$

and, for $n_s$ surfaces,

$$H_i = \frac{1}{A_i} \sum_{j=1}^{n_s} B_j A_j E_{ji}$$

Now the interchange factors obey the reciprocity relation

$$A_i E_{ij} = A_j E_{ji}$$
FIGURE 1: ILLUSTRATION OF METHOD USED TO DETERMINE SPECULAR SURFACE REFLECTED VIEW FACTORS
So,
\[ H_i = \sum_j B_j E_{ij} \]  \(21\)

Substitution into the equation for \(B\) results in
\[ \sum_j (\delta_{ij} - \rho_i E_{ij}) B_j = \epsilon_i \sigma T_i^4 \]  \(22\)

This equation represents a set of linear, simultaneous, inhomogeneous algebraic equations for the unknowns \((B_j)\). The symbol \(\delta_{ij}\) is the Kronecker delta function which is 1 when \(i = j\) and is 0 when \(i \neq j\).

Note that the coefficients of \(B_j\) in equation (22) do not form a symmetric coefficient matrix since the off-diagonal terms contain \(-\rho_i E_{ij}\). This equation can be made symmetric by multiplying each equation by \(A_j / \rho_j\). This gives
\[ \sum_j \left(\frac{\delta_{ij} A_i}{\rho_i} - E_{ij} A_i \right) B_j = \frac{\epsilon_i A_i}{\rho_i} \sigma T_i^4 \]  \(23\)

Written in matrix form this equation is
\[ E B = T \]  \(24\)

Where \(E\) is a symmetric coefficient matrix. The solution is
\[ B = E^{-1} T = [e_{ij}] T \]  \(25\)

or
\[ B_i = \sum_{j=1}^{\text{ns}} e_{ij}^{-1} \frac{\epsilon_i A_j}{\rho_j} \sigma T_j^4 \]  \(26\)

The net heat transfer rate absorbed by surface \(i\) is given by
\[ Q_i = A_i \epsilon_i \left[ H_i - \sigma T_i^4 \right] \]  \(27\)

Where \(H_i\) is given from equation
\[ H_i = \frac{1}{\rho_i} \left[ B_i - \epsilon \sigma T_i^4 \right] \]
Substituting in for $H_j$ gives

$$Q_i = A_i \frac{\epsilon_i}{\rho_i} \left\{ \frac{1}{\rho_i} \left[ B_i - \epsilon_i \sigma T_i^4 \right] - \sigma T_i^4 \right\}$$

$$= \frac{A_i \epsilon_i}{\rho_i} \left\{ B_i - \left[ \rho_i + \epsilon_i \right] \sigma T_i^4 \right\} \quad (28)$$

Substituting in for $B_j$ from equation (26) into equation (28) gives

$$Q_i = \frac{A_i \epsilon_i}{\rho_i} \left\{ \sum_{J=1}^{n} \frac{e_{ij}^{-1} \epsilon_j A_j}{\rho_j} \sigma T_j^4 - \left[ \rho_i + \epsilon_i \right] \sigma T_i^4 \right\}$$

$$= \frac{A_i \epsilon_i}{\rho_i} \left\{ \sum_{\substack{J=1 \\mathrm{J \neq i}}}^{n} \frac{e_{ij}^{-1} \epsilon_j A_j}{\rho_j} \sigma T_j^4 - \left[ \rho_i + \epsilon_i \right] \frac{e_{ij}^{-1} \epsilon_i A_i}{\rho_i} \sigma T_i^4 \right\} \quad (29)$$

Since, in steady state, $Q_i = 0$, and $T_i^4 = T_j^4$ for all $i$ and $j$ we can conclude that

$$\rho_i + \epsilon_i - \frac{e_{ij}^{-1} \epsilon_i A_i}{\rho_i} = \sum_{\substack{J=1 \\mathrm{J \neq i}}}^{n} \frac{e_{ij}^{-1} \epsilon_j A_j}{\rho_j}$$

Making the above substitution in equation (29) gives

$$Q_i = \sum_{J=1}^{n} \frac{\sigma \epsilon_i \epsilon_j A_i A_j e_{ij}^{-1}}{\rho_i \rho_j} \left[ T_j^4 - T_i^4 \right] \quad (30)$$

If we define $\mathcal{F}$ as

$$\mathcal{F}_{ij} = \frac{\epsilon_i \epsilon_j A_i A_j e_{ij}^{-1}}{\rho_i \rho_j} \quad (31)$$

Then

$$Q_i = \sum_{J=1}^{n} \sigma \mathcal{F}_{ij} A_i \left[ T_j^4 - T_i^4 \right] \quad (32)$$
This equation gives the heat flux between surfaces. However, each surface can contain several nodes. The heat absorbed by for each node is determined by

\[ Q_n = \frac{A_n}{A_i} \sum_{j=1}^{ns} \sigma \mathcal{F}_{ij} A_i \left[ T_j^4 - T_n^4 \right] \]  

(33)

Where \( n = \) the node number on surface \( i \)

Prior to each iteration, the temperature of the surfaces are determined by

\[ T_i^4 = \frac{\sum_{n=1}^{nn} A_n T_n^4}{\sum_{n=1}^{nn} A_n} = \frac{\sum_{n=1}^{nn} A_n T_n^4}{A_1} \]  

(34)

Where \( nn = \) the number of nodes on surface \( i \)

Since the heat transfer rate given by equation (33) depends on the node temperature, stability considerations must be taken into account. This is handled by storing the following relation into the array containing the sum of the conductors used for time increment calculation

\[ CON_n = \frac{4 A_n}{A_i} \sigma T_n^3 \sum_{j=1}^{nc} \mathcal{F}_{ij} A_{ij} \]  

(35)

Subroutine RADIR makes the calculations necessary to obtain \( Q_n \) given by equation (33) and \( CON_n \) given by equation (35). The following is a summary of the calculations:

A. The following are performed the first time through RADIR:

1. From the user input values of \( E_{ij}, A_i, \) and \( \rho_i \), the \( E \) matrix given by equation (24) is formed. Only half of the symmetric matrix is stored to save space.
2. The \( E \) matrix is inverted in its own space to get \( E^{-1} \) with elements \( e_{ij} \).
3. The \( \mathcal{F}_{A_{ij}} \) values are determined from equation (31) and stored in the surface connections data.

B. The following calculations are performed on each temperature iterations:

1. The temperature of each surface is calculated by equation (34).
2. The heat absorbed for each node is determined using equation (33) and is added to the \( Q \) array.

The routine utilizes data used for obtaining \( \mathcal{F}_{A_{ij}} \) in step A as working space for step B, thus, maximizing space utilization.
Radiation from External Source

As with the infrared radiation, the solar (or any other non-infrared radiation) interchange factor is defined by

\[ E_{ij}^* = F_{ij} + \sum_k \rho_k^s F_{ij}(k) + \sum_k \sum_l \rho_l^s \rho_k^S F_{ij}(k,l) + \ldots \]

Where \( \rho_k^s \) is the solar specular reflectance of surface \( k \)

\( F_{ij}(k) \) is the angle factor from \( i \) to \( j \) as seen in the specular surface

\( F_{ij}(k,l) \) is the angle factor from \( i \) to \( j \) as seen in a double specular reflection from \( j \) to \( l \) back to \( i \)

The interchange factors as defined above accounts for the specularly flux reflected from the surface. Thus, since the specular component of the flux is assumed to go directly from surface \( i \) to surface \( j \) by the interchange factor, \( E_{ij} \), this portion of the total flux is not a component of the radiatity for the intermediate surfaces (\( k \) and \( l \) above). The radiatity of surface \( i \) is given by

\[ B_i^* = \rho_i^* H_i^* \]  

Where \( B_i^* \) is the radocity (energy leaving)

\( H_i^* \) is the incident energy

\( \rho_i^* \) is the diffuse reflectance

The energy incident upon a surface is given by

\[ H_i = \sum_{J=1}^{ns} B_j^* E_{ij}^* + S_i \]  

Where \( S_i \) is the energy directly incident on surface \( i \) from an external source

Substituting equation (36) into (37), multiplying by \( A_i/\rho_i^* \) and simplifying gives the following relation for the radocity

\[ \begin{bmatrix} A_i - E_{ij}^* A_i \end{bmatrix} B_i^* + \sum_{J=1}^{n} E_{ij}^* A_i B_j^* = S_i A_i \quad i=1, n \]  

(38)
This set of n equations can be written in matrix form as

\[ E^* B^* = S \]  
(39)

Note that the equations are written so that \( E^* \) is a symmetric matrix, which has the solution for \( B^* \)

\[ B^* = E^{*-1} S \]  
(40)

Where \([e_{ij}^{*}]^{-1}\) is the \(ij\)th element of the inverse of the \(E^*\) matrix.

The heat flux absorbed by the \(i\)th surface is given by

\[ \frac{Q_i^*}{A_i} = \alpha H_i \]  
(41)

But from equation (36)

\[ H_i = \frac{B_i}{\rho^*} \]  
(42)

Combining equations (40), (41), and (42) gives

\[ Q_i^* = \sum_{j=1}^{n} e_{ij}^{* -1} \frac{a_i}{\rho^*_i} A_j A_i S_j \]  
(43)

If we define

\[ \mathcal{F}_{ij}^* = e_{ij}^{* -1} \frac{a_i}{\rho^*_i} A_j \]  
(44)

Then the absorbed heat flux is given by

\[ Q_i^* = \sum_{j=1}^{n} \mathcal{F}_{ij}^* A_i S_j \]  
(45)

Equation (45) gives the heat absorbed by each surface. However, each surface may contain several temperature nodes. The absorbed heat for each node is given by

\[ Q_n^* = \frac{A_n}{A_i} Q_i^* \]  
(46)

Where \(A_n\) is the area of the node.
Subroutine RADSOL was written to make necessary calculations to obtain $Q_{n}^{*}$ given by equation (46). The following is a summary of the calculations:

A. The following calculations are made the first time through RADSOL:

1. From the user input values of $E_{ij}^{*}$, $p_{ij}^{*}$, and $A_{i}$, the $E^{*}$ matrix given by equation (39) is formed. Only one half is stored since $E^{*}$ is symmetric.
2. The $E^{*}$ matrix is inverted in its own space to get $E^{*-1}$ with elements, $e_{ij}^{*-1}$.
3. The $f_{ij}^{*}A_{i}$ values are determined from equation (44) and stored in the surface connections data.

B. The following calculations are performed on each temperature iteration:

1. The heat flux absorbed by each node is calculated by
   \[ Q_{i}^{*} = \frac{1}{A_{i}} \sum_{j=1}^{n} f_{ij}^{*}A_{i}S_{j} \]
2. The net heat absorbed by this wave length radiation is calculated for each temperature node on each surface by
   \[ Q_{n}^{*} = A_{n} \frac{Q_{i}^{*}}{A_{i}} \]
This quantity of absorbed heat is added to the $Q$ array for node $n$.

Note that the user may specify subroutine RADSOL for as many bands of non-infrared radiation is desired. A single call is required for each band.

3.2 PRESSURE - FLOW ANALYSIS

Provisions have been included in MOTAR for the pressured flow balance analysis of a flow system which contains a network of interconnected tubes including any combination of series/parallel flow. The effect of valves may be included in the pressure/flow analysis and the overall system pressure drop and flow rate may balanced with input pump pressure and flow characteristics.

3.2.1 Overall Model Description

The model used to mathematically describe a flow network consists of pressure "nodes" at tube junction and flow "conductors" for the tubes connecting the pressure nodes. The flow conductors for each tube is calculated as the reciprocal of the sum of the flow resistance of temperature fluid lumps in each tube. The conductor/node network method for describing the flow system was chosen over that previously used because of the computational advantages and the flexibility it gives the user. The computational advantages come from the fact that the number of equations which must be
solved simultaneously are reduced from the number of tubes to the number of nodes between tubes. The method is more flexible because there are no restrictions on the number of tubes which can be connected at a junction.

For analysis purposes each flow network is divided into two levels. These are the "system" and any number of "subsystems". This subdivision is made to divide the network into those portions not requiring simultaneous equation solution (the system) and those requiring the solution to a set of equations (the subsystem). Also tied to the concepts of system and subsystem are the two basic classes of valves in MOTAR. These are (1) valves which dictate a given flow split based upon their position and (2) valves which dictate a resistance to flow based upon their position (class). Class 1 valves were devised for use in the system where no pressure balance is obtained and Class 2 valves were devised for use with the subsystem where the valve pressure drop is included in the pressure/flow balance.

Consider Figure 2 to help illustrate the meaning of system and subsystem. In Figure 2 (a) if valve VI is of the specified flow split type (class 1) then, the system consists of tubes 1, 2, 11, 12, 18, and 19. This is because the flow in each of these tubes is defined by the flow in tube 1 (the inlet) and the valve position. Two subsystems exist for this example which are those requiring a pressure balance. One consists of tubes 3 thru 10; the other consists of tubes 13 thru 17. In this example, if valve VI were of the pressure drop type (class 2) then the system would be tubes 1 and 19 and one subsystem would exist consisting of tubes 2 thru 18.

Figure 2(b) shows an example in which no subsystem is required. If the valves VI and V2 are both Class 1 (flow splitting) then all tubes are in the system and no subsystem exists. If valve VI is class 2, then valve V2 must also be Class 2 and tubes 2 thru 6 belong to the subsystem. If VI is Class 1 and V2 is Class 2, then all tubes are in the system except 3 and 4 which are in the subsystem.

The sections that follow give a detailed description of the analytical methods for (1) determining the conductor values for each tube, (2) determining the conductor values for valves, (3) determining network solutions, and (4) balancing system pressure drop and flow with pump flow characteristics.

3.2.2 Tube Conductor Determination

The value of the flow conductor is determined for each tube by first calculating the flow resistance for each temperature fluid lump contained in the tube, summing these resistances up to obtain the flow resistance of the tube and inverting the tube resistance to get the conductance. Flow conductance is defined by the relationship

$$\dot{W}_{ij} = G_{ij} [P_i - P_j] \quad (47)$$

Where

- $\dot{W}_{ij}$ = flow rate between pressure nodes i and j
- $G_{ij}$ = flow conductance between nodes i and j
- $P_i$ = pressure at pressure node i
- $P_j$ = pressure at pressure node j
Figure 2: Illustration of System and Subsystem Concept

(A) Numbers are tube numbers
V1 = Valve No. 1

(B)
The flow resistance for each lump is then

\[ R_k = \frac{1}{G} = \frac{\Delta P_k}{\dot{W}} \]

Where \( R_k \) = flow resistance for lump \( k \)
\( \Delta P_k \) = pressure drop for lump \( k \)

But \( \Delta P_k \) is given by

\[ \Delta P_k = f_k f_{fc} \frac{L_k}{D_k} + k \frac{\dot{W}^2}{2g_c \rho_k A^2} \quad (48) \]

Where \( f_k \) = the friction factor for lump \( k \)
\( f_{fc} \) = the friction factor coefficient
\( L_k \) = the lump length for lump \( k \)
\( D_k \) = the lump hydraulic diameter for lump \( k \)
\( k \) = the dynamic head losses for lump \( k \)
\( \dot{W} \) = the flow rate
\( g_c \) = the gravitational constant
\( \rho_k \) = the fluid density for lump \( k \)
\( A \) = the flow area

The flow resistance is then given by

\[ R_k = f_k f_{fc} \frac{L_k}{D_k} + k \frac{\dot{W}}{2g_c \rho_k A^2} \quad (49) \]

Two options are available for obtaining the friction factor, \( f_k \). These are (1) it is calculated internally and (2) it is calculated internally for laminar flow but is obtained from a table of \( f \) vs Re (where Re is the Reynold's number) for transition and turbulent flow. For the first option the internal calculations for the three flow regimes are:

- **Laminar Regime**: \( Re_k \leq 2000 \).

\[ f_k = \frac{64}{Re_k} \quad (50) \]

Where \( f_k \) = friction factor for lump \( k \)
\( Re_k \) = Reynolds number for lump \( k \)
Transition Regime: $2000 < \text{Re}_k < 4000$

\[
f_k = 0.2086082052 - 0.1868265324 \left( \frac{\text{Re}_k}{1000} \right) + 0.06236703785 \left( \frac{\text{Re}_k}{1000} \right)^2 - 0.0065545818 \left( \frac{\text{Re}_k}{1000} \right)^3
\]  

(51)

Turbulent Regime: $\text{Re}_k \geq 4000$

\[
f_k = 0.316 \left( \frac{\text{Re}_k}{1000} \right)^{0.25}
\]  

(52)

Equation (51) for the transition regime is a curve fit between the laminar and turbulent regimes which was derived to match the two curves in a continuous manner. It is merely an arbitrary curve in this undefined region. A curve of the friction factor VS Reynolds number given by the above relations is shown in Figure 3.

The second option for friction factor uses equation (50) for the laminar regime and a user input curve of $f_k$ vs Re for the other regimes. The options available for input of the dynamic head loss, $\zeta$, include (1) an input constant or (2) a tabulated curve of $\zeta$ vs Re.

To obtain the conductance for each tube, the flow resistances for all the lumps in the tube are added and then inverted. That is,

\[
G_{ij} = \frac{1}{\sum_k R_k}
\]  

(53)

3.2.3 Valve Analysis

As discussed in Section 3.2.1 two classes of valves are available in MOTAR. For Class 1 valves the valve position dictates directly the friction of the incoming flow distributed to the valve outlet branches. For Class 2 valves the valve position and pressure drop characteristics define the flow resistance for the valve branches. These resistances are added to the other flow resistance of the tubes to obtain the overall tube conductance prior to solving for the flow rate.

A number of valve types are available to the user for both classes of valves which are:

1. Rate limited
2. Polynomial (replaces the polynomial)
3. Shut-off proportioning
FIGURE 3  Friction Factor vs Reynolds Number
These valves types differ in the relationship between the sensor and the valve position as described below.

3.2.3.1 Valve Position Determination

Described below are the methods used in the routine to obtain the valve position. The following section will describe the use of the valve position to obtain flow split and pressure drop information.

**Rate Limited Valve**

The valve position for the rate limited valve is obtained by an approximate integration of the valve rate of movement, \( \dot{X} \). \( \dot{X} \) depends on the temperature difference between the valve control set point temperature and the sensor temperature as shown in Figure 4. With this characteristic, the valve has no movement as long as the valve temperature error, \( \Delta T \), is within the dead band. Outside the dead band, the velocity of the valve increases linearly as the error increases to a maximum rate, \( \dot{X}_{\text{max}} \). The dead band, rate of velocity increase, \( d\dot{X}/d(\Delta T) \), and the maximum velocity are controlled by user input.

The relations used to obtain the valve positions are as follows:

\[
X^{i+1} = X^i + (\dot{X}^{i+1}) (\Delta r)
\]

Where

\( X^{i+1} = \) valve position at iteration \( i+1 \)

\( X^i = \) valve position at iteration \( i \)

\( \dot{X}^{i+1} = \) valve velocity at iteration \( i+1 \)

\( \Delta r = \) the problem time increment

The valve position is limited by

\( X_{\text{min}} \leq X^{i+1} \leq X_{\text{max}} \)

Where \( X_{\text{min}} \) and \( X_{\text{max}} \) are input limits on the valve position.

The valve velocity, \( \dot{X}^{x+1} \), in equation (54) is given by:

\[
\dot{X}^{i+1} = 0 \text{ if } |T_{\text{sen}} - T_{\text{set}}| \leq T_{\text{db}}
\]

Where

\( T_{\text{sen}} = \) Sensor lump temperature
Valve Position, $X = X_0 + \dot{X}$ (Time Increment) $0 < X < 1.0$

Figure 4  Rate Limited Valve Operation
Polynomial Valve

The polynomial valve determines the steady state valve position as a forth degree polynomial function of the temperature error between the sensor lump and the set point. A valve time constant is then applied to determine how far between the previous position and the new steady state position the valve will move. The steady state position, \( X_{ss} \), is given by

\[
X_{ss} = A_0 + A_1 \Delta T + A_2 \Delta T^2 + A_3 \Delta T^3 + A_4 \Delta T^4
\]

Where \( \Delta T = T_{sen} - T_{set} \)

\( T_{sen} \) = the sensor lump temperature
\( T_{set} \) = the set point temperature
\( A_0, A_1, A_2, A_3, A_4 \) = input constants

The valve position, \( X^{i+1} \), is then determined by

\[
X^{i+1} = X_{ss} + (X^i - X_{ss}) e^{-\Delta r/r_c}
\]

Where \( X^{i+1} \) = valve position at iteration \( i+1 \)
\( X^i \) = valve position at iteration \( i \)
\( \Delta r \) = problem time increment
\( r_c \) = valve time constant
Note that this valve combines the capabilities of the polynomial valve and the proportioning valve described in Reference 12. If one desires to eliminate the effect of the time constant (and thus, give the valve an instantaneous response), a valve for \( r_c \) should be input which is small compared to the time increment, \( \Delta r \). Also, either a constant value or a temperature lump number may be specified for the set point to permit the use of the value for proportioning between two sides.

**Shut-off Valve**

Two types of shut-off valves are available. For the first, the valve position decreases from \( X_{\text{max}} \) to \( X_{\text{min}} \) when the temperature of the sensor lump drops below the specified "off" temperature \( T_{\text{off}} \) and increased from \( X_{\text{min}} \) to \( X_{\text{max}} \) when the sensor lump exceeds a second specified temperature, \( T_{\text{on}} \). \( T_{\text{on}} \) must be greater than \( T_{\text{off}} \). The second type of shut-off valve works in reverse to the first. The valve position increases from \( X_{\text{min}} \) to \( X_{\text{max}} \) when the sensor temperature drops below the specified \( T_{\text{on}} \) and decreases from \( X_{\text{max}} \) to \( X_{\text{min}} \) when the sensor lump increases above the off temperature, \( T_{\text{off}} \). For the second type, \( T_{\text{off}} \) must be greater than \( T_{\text{on}} \).

### 3.2.3.2 Flow Split and Pressure Characteristic Determination

For the Class 1 valves the valve position as determined by the methods described in Section 3.2.3.1 will determine the flow split directly between two outlet tubes. (Two are required for class 1). The flow rate is given by

\[
\begin{align*}
\dot{W}_1 &= X \dot{W}_{\text{in}} \\
\dot{W}_2 &= (1.-X) \dot{W}_{\text{in}} 
\end{align*}
\]

Where

- \( \dot{W}_{\text{in}} \) = flow rate into the valve
- \( \dot{W}_1 \) = flow rate out side 1
- \( \dot{W}_2 \) = flow rate out side 2

For the Class 2 valves, the position is used to determine the valve resistance to flow. The valve pressure drop on one side is assumed to be...
given by

\[ \Delta P = E \left( \frac{W}{X} \right)^2 \]  

(56)

Where 
- \( E \) is an input constant
- \( W \) is the flow through one side of the valve
- \( X \) is the valve position (fraction of total possible distance)

Since flow resistance is \( \Delta P/W \), the valve flow resistance is given by

\[ R_v = \frac{E \dot{W}}{X^2} \]  

(57)

This value of flow resistance is calculated and added to the other flow resistances of the tube prior to performing the operation in equation (53) to find the tube conductor.

Class 2 valves may be either one way or two way - i.e., there may be one tube or two tubes at the outlet. If only one tube exists on the valve outlet the flow resistance is calculated using equation (57) above. If a second tube exists, the resistance on side 2 is given by

\[ R_{v2} = \frac{E_2 \dot{W}_2}{(1 - X)^2} \]  

(58)

3.2.4 Pressure-Flow Network Solution

After the flow conductor values have been obtained by the methods described in Sections 3.2.2 and 3.2.3 a set of simultaneous equations are set up and solved for each subsystem. This set of equations are obtained by conservation of mass at each pressure node. This gives as many equations as there are nodes in the subsystem.

For any node \( i \) the conservation equation can be written as follows.

\[ \sum W_{\text{out}} - \sum W_{\text{in}} = 0 \]  

(59)

Let \( W_{\text{in}} = W_i \)

and \[ \sum W_{\text{out}} = \sum_{J=1}^{nc} G_{ij} [P_j - P_i] \]  

(60)
Then equation (59) becomes

\[ \sum_{j=1}^{n} G_{ij} [P_j - P_i] - W_i = 0 \quad i = 1, n \]  

(60)

Where

- \( G_{ij} \) = flow conductor between pressure nodes \( i \) and \( j \)
- \( P_i \) = pressure at node \( i \)
- \( P_j \) = pressure at node \( j \)
- \( W_i \) = flow rate added at node \( i \)
- \( N \) = number of pressure nodes in the subsystem

The above equation can be written as a set of simultaneous equations in \( P \) and solved for all pressures. One pressure in the system must be specified. The set of equation can be written in Matrix form (assuming \( P_n \) is the specified pressure):

\[ GP = C \]  

(61)

Where

\[
G = \begin{bmatrix}
\sum G_{1j} & -G_{12} & -G_{13} & \ldots & \\
-G_{21} & \sum G_{2j} & -G_{23} & \ldots & \\
\vdots & \vdots & \ddots & \ddots & \\
-G_{n-1,1} & -G_{n-1,2} & \ldots & \sum G_{n-1,j}
\end{bmatrix}
\]

\[
P = \begin{bmatrix}
P_1 \\
P_2 \\
\vdots \\
P_{n-1}
\end{bmatrix}
\]
The above equations are solved for pressures at each point in the system and flow rates are then calculated for each tube (conductor) by:

\[
\begin{bmatrix}
W_1 + G_{1n} P_n \\
W_2 + G_{2n} P_n \\
\vdots \\
W_{n-1} + G_{n-1} P_n
\end{bmatrix}
\]

Specified Pressure (Doesn't have to be the last one)

Two methods of solution are available in MOTAR for solving the set of equations given by equation (61). These are the Gauss-Jordon reduction method, which is a direct solution method and the Seidel stationary point iteration method with successive overrelaxation which is an iterative method. The user may specify which of the two methods to be used. Normally, for the typical problem the direct method would be used. However, for extremely large problems where the direct method proves unsatisfactory, the iterative method may be an improvement.

Since the flow conductors are functions of the flow rate, the set of equations given by (61) are solved numerous times on each temperature iteration with a new set of \(G_{ij}\) values for each solution. The iteration process continues until the change in the flow rates is within some user specified tolerance before proceeding to the next iteration.

3.2.5 Pump and System Pressure - Flow Matching

Concurrent with iterating the system flow equation to solution on each iteration, the overall system pressure drop and flow rate must be matched to a pump characteristic. Several types of pump characteristics
are available to the user as options. These are (1) The system flow rate may be specified as a constant, (2) it may be specified as a known function of time, (3) the pressure drop may be specified as a function of the flow rate in a tabular form and (4) the pressure drop may be specified as a function of flow rate with a fourth degree polynomial curve.

The first two options require no balancing of the pump with the system. Balancing is required for options (3) and (4) and iterative procedures have been devised to obtain the solution of the pump curve to the system characteristics with as few passes as possible through the system pressure/flow balancing loop for these options. The procedures used for these options are described below.

3.2.5.1 Tabular Pump Curve Solution

The matching of a tabulated pump pressure rise/flow characteristic to the system pressure drop/flow characteristic is accomplished by the following procedure. See Figure 5 to aid in following the procedure.

Step 1: The initial flow rate, \( W_1 \), at the system inlet is established either from user input on the first iteration or the system flow of the previous iteration for subsequent iterations.

Step 2: Using \( \dot{W}_1 \), a solution to the flow network is obtained using the methods described in sections 3.2.2, 3.2.3 and 3.2.4. Following this solution, \( \Delta P_1 \) is available establishing point 1 on the true system characteristic curve shown in Figure 5.

Step 3: The constants which describe the straight line approximation for the system pressure/flow characteristic is established. (line 0 to 1 for the first pass, line 1 to 2 for the second pass, etc.)

\[
\Delta P_s = C \dot{W}_s + D
\]
Second Approximation To System

Third Approximation To System

First Approximation To System

Figure 5 System/Pump Curve Solution
(a) For the first pass,

$$C = \frac{\Delta P_1}{W_1}$$

$$D = 0$$

(b) For the second and subsequent pass on a given iteration,

$$C = \frac{\Delta P_2 - \Delta P_1}{W_2 - W_1}$$

$$D = \Delta P_1 - \left[ \frac{\Delta P_2 - \Delta P_1}{W_2 - W_1} \right] W_1$$

Where $\Delta P_2$ and $W_2$ are the values for the last solution on the system characteristic (point 2 on Figure 5 for the third pass).

$\Delta P_1$ and $W_1$ are the values for the next to the last solution on the system characteristic (point 1 for the third pass).

Step 4: The solution to the approximate system characteristic and the tabulated pump characteristic is determined by the following iterative procedure

(a) Start with $W_a = W_1$

(b) Determine $\Delta P_a$ by interpolating the pump curve at $W_a$

(c) Determine the flow rate given by the approximate system characteristic at $\Delta P_a, W_b$

$$W_b = \frac{\Delta P_a - D}{C}$$

Where constants $C$ and $D$ were obtained in Step 3.
(d) Determine the approximate solution, \( W_c \) by

\[ W_c = \frac{W_a + W_b}{2} \]

(e) Check the tolerance:

Is \( (W_c - W_a) < .001 \, W_a \)

(f) If the inequality does not hold, set \( W_a = W_c \)
and repeat b thru f. If the inequality does hold
\( W_c \) is the solution between the pump curve and
the latest approximate to the system characteristic
and

\[ W_{si} = W_c \]

Step 5: Check the following tolerance

\[ |W_1 - W_{s1}| = E \]

If \( E < .001 \times W_1 \), then \( W_{s1} \) and \( \Delta P \), are the solution.
If the tolerance is not met, repeat steps 2 thru 5 using
the latest flow rate, \( W_{s1} \) as \( W_1 \) and find \( W_{s2}, W_{s3} \) etc.
until \( W_{sf} \), the final solution is located.

3.2.5.2 Polynomial Pump Curve Solution
When the user describes the pump curve with a polynomial curve
fit, the pump characteristic is described by the relation

\[ \Delta P_p = A_0 + A_1 W + A_2 W^2 + A_3 W^3 + A_4 W^4 \]

When this option is used, the procedure for matching the pump characteristic
described above to the system characteristic is identical to that described
in Section 3.2.5.1 for the tabulated pump characteristic except Step 4 is
replaced with the following Step 4A:
Step 4A: Set up the equation for $\dot{W}_S$ and solve.

(a) Set up the equation

Since:
\[ \Delta P_p - \Delta P_s = 0 \]

\[ \Delta P_s = C W_s + D \quad (C \text{ and } D \text{ are obtained from Step 3, equation (64 or 65))} \]

\[ \Delta P_p = A_0 + A_1 W_p + A_2 W_p^2 + A_3 W_p^3 + A_4 W_p^4 \]

Then the equation for $\dot{W}_S$ is

\[ (A_0 - D) + (A_1 - C) W_s + A_2 W_s^2 + A_3 W_s^3 + A_4 W_s^4 = 0 \]

(b) Solve the equation for $W_s$ using the Newton-Raphson Method of solution for a fourth order polynomial

The remaining steps are identical to that given in Section 3.2.5.1.
4.0 ROUTINE OPERATIONAL DESCRIPTION

This section describes the nature of the MOTAR computer routine. The operation of MOTAR is divisible into three phases. These are: (1) the preprocessing phase which includes the reading of input data, the assembling of computer generated subroutines, and processing the input data into a compressed data tape, (2) the compilation phase in which the computer generated and user assembled subroutine are compiled and (3) the processing phase during which the compressed data tape is read and the desired computation are made. A schematic of the overall flow of the MOTAR routine is given in Figure 6. This three phase procedure was devised (1) to permit the tailoring of the main temperature calculation subroutines to conform with the requirements of the data in the most efficient manner and (2) to permit the user to perform logical operations and call user subroutines in the input data.

A description of the three phases including a summary of the subroutines used in each phase is given in the following subsections. A listing of all subroutines is provided in Appendix D.

4.1 PREPROCESSING PHASE

During the preprocessing phase of MOTAR the following tasks are performed:

(1) A data tape is generated and/or edited when the user so requests.

(2) The input data, which is input in a free field format, is read from cards or the final data tape, processed for more efficient use by the computer and stored on a compressed data tape.

(3) The user logic supplied in the $PRETEMP, $POSTTEMP, $CENTRAL, and $OUTPUT is read and written in a form compatible with the Fortran compiler.

(4) The symbolic logic for the transient and steady state temperature calculation subroutine is generated in a form compatible with the FORTRAN compiler.

A brief summary of the elements used during the preprocessing phase is given below:

STEPL Specifies the overlay structure of the preprocessing phase. Elements NTWRK, SUBFLW, SUBCRV, OPBLOK, and GETCOM overlayed. MAIN is designated as the Main preprocessing phase routine.

MAIN The driving routine for the preprocessing phase. It calls on subroutines SUBA and SUBB to generate a data tape, read input and write a compressed
PRE-PROCESSING PHASE

START

READ INPUT DATA

COMPilation PHASE

READ COMpressed DATA TAPE

COMPILE COMPUTER AND USER GENERATED SUBROUTINES

PROCESSING PHASE

OUTPUT OPERATIONS

PRESSURE/FLOW CALCULATIONS

TEMPERATURE CALCULATIONS

PRE-TEMPERATURE OPERATIONS

REQUIRED OPTIONAL SUBROUTINES

POST-TEMPERATURE OPERATIONS

END

FIGURE 6: MOTAR ORGANIZATION
data tape, read user logic and write it in required symbolic form and generate temperature solution subroutines corresponding to the requirements of the input data. They call on the following subroutines to perform this: EDIT, COLCHK, NTWRK, SUBFLW, SUBCRV, PRETEMP, CENTRL, PSTTMP, SOUT, ISUBA, KRVS, GENOUT, GETCON, BLOCK. These are described below.

A) EDIT
Places the user input data on a magnetic tape and performs edits to previously generated magnetic tapes. Calls EXIT if an error occurs.

B) COLCHK
Reads and writes data cards, skips blank columns and locates delimiters.

C) NTWRK
Reads and processes the $NETWORK data. Calls the following subroutines to handle different types of data:

1) COLCHK - (Described above)
2) INTMP - Reads and processes INITIAL TEMPERATURE data
3) CAPHT - Reads and processes +CAPACITANCE and +ABSORBED HEAT data
4) SUBCON - Reads and processes 'CONDUCTION' conductor data
5) SUBRAD - Reads and processes 'RADIATION' conductor data
6) SUBCNV - Reads and processes 'CONVECTION' conductor data

D) SUBFLW
Reads and processes $FLOW SYSTEMS data

E) SUBCRV
Reads $CURVES data and writes it on a drum for subsequent processing

F) CENTRAL
(Entry point to OPBLOK) Reads user logic in $CENTRAL block and writes it on a drum for subsequent processing

G) PREOP
(Entry point to OPBLOK) Reads user logic in $PRETEMP block and writes it on a drum for subsequent processing
H) POSTOP  (Entry point to OPBLOK) Reads user logic in $POSTTEMP block and writes it on a drum for subsequent processing

I) SUBOUT  (Entry point to OPBLOK) Reads user logic in $OUTPUT block and writes it on a drum for subsequent processing

J) KRVS     Process $CURVES data which was read by subroutine SUBCRV

K) GETCON   Rearranges conductor connections data for the implicit temperature routines when required

L) BLOCK    Writes computer generated and user logic elements in a form expected by the Fortran compiler

Other subroutines called during the preprocessing phase are described below:

EXIT       Terminates the job

NODENO     Reads in node numbers for all MOTAR options including multiple input options

SUBI       Reads in integers

SUBF       Reads in real numbers

SUBS       Converts arguments from a field data character to an integer by means of an Alpha-numeric search

ORDER      Orders blocks of data in an array so that one element of the block is in either ascending or decending order from block to block.

CONDNO     Reads in conductor numbers and connected nodes including Multiple input options

GENOUT     List an array of mixed mode numbers

GENR       (Entry point to GENOUT) Lists an array of real numbers

GENI       (Entry point to GENOUT) Lists an array of integers

4.2 COMPILATION PHASE

During the compilation phase, a compilation is performed on as many as six subroutines which were setup during the preprocessing phase and any other subroutines which the user may desire to supply. The six subroutines which will normally require compilation are tabulated below:
### 4.3 PROCESSING PHASE

During the processing phase the following operations are performed:

1. The compressed data generated during the preprocessing phase or from a dump tape is read into core

2. The $CENTRAL logic is executed. Included in the $CENTRAL logic are the calls to temperature solution subroutines

3. The specified temperature solution is performed including the following operations:
   - Prior to each temperature iteration, the $PRETEMP logic is executed
   - Following each temperature iteration but prior to pressure/flow balance on the flow systems the $POSTTEMP operations are performed
   - The pressure/flow balance is performed when required
   - The plot tape is written on the plot interval
   - The normal output is performed on the output interval. In addition, the $OUTPUT operations are performed.
Two types of subroutines are employed during the processing phase: (1) Those specifically designed for user calls in the four operation blocks and (2) those designed for internal program use. The user subroutines are described in detail in Appendix A. The subroutines designed for internal program use are summarized below.

**STEP2**

The main routine for the processing phase of MOTAR. It reads the compressed data tape, performs the $CENTRAL user logic and calls one or more of the following temperatures: EXPLCT, EXPSS, IMPLCT, IMPSS. The first pair or the second pair may occur in the same problem.

**EXPLCT**

Temperature solution subroutines which are assembled during the preprocessing phase. (See Appendix A for a description of the use.) These subroutines call on a number of additional subroutines which:

a) Calculate the temperature network elements based upon various user options

b) Perform the $PRETEMP, $POSTTEMP, and $OUTPUT user logic

c) Performs temperature and pressure/flow calculations

d) Writes plot and dump tape

**EXPSS**

**IMPLCT**

**IMPSS**

Table I and II illustrate the possible call statements in the order that they occur for subroutines EXPLCT and IMPLCT. Only those calls needed will actually exist for a given problem. A brief description of each subroutine is given below:

**TEMP2**

Determines the time dependent temperatures by curve linear interpolation

**PFCS**

Obtains a pressure/flow balance for the input flow systems. Also calculates valve positions and pressure drop characteristics and balances the system flow with the pump flow.

**INITL**

Prints out initial flow rates, pressures, temperatures, capacitances, heat storage rates, thermal conductances, and time increments. Also calls PRINTS to write the initial values on the history tape.

**CAPAC1**

Performs linear interpolations to obtain capacitance as a function of time.

**CAPAC2**

Performs linear interpolations versus time and multiplies the values times constants to obtain capacitance values.
TABLE I
LISTING OF CALL STATEMENTS IN SUBROUTINE EXPLCT

Common and Equivalence Tables

CALL TEMP2
CALL PFCS
CALL INITL
ITER = 0
100 CALL CAPAC1
CALL CAPAC2
CALL CAPAC3
CALL CAPAC4
CALL CAPAC5
CALL CAPAC6
CALL CONDF1
CALL CONDV
CALL COND2
CALL COND3
CALL COND4
CALL COND5
CALL RADTN
CALL ABSHT1
CALL ABSHT2
CALL ABSHT3
CALL ABSHT4
CALL ABSHT5
CALL PRETMP
CALL KNODF
CALL KOND
CALL RADT
CALL DTAU1
CALL TEMP1
TIME = TIME + TINC
ITER = ITER + 1
CALL TEMP2
CALL POSTMP
CALL PFCS
CALL PRINTS
Go to 100
\} Writes dump tape
RETURN
END
TABLE II
LISTING OF CALLS IN SUBROUTINE IMPLCT.

Common and equivalence tables

<table>
<thead>
<tr>
<th>CALL</th>
<th>Description</th>
</tr>
</thead>
<tbody>
<tr>
<td>TEMP2</td>
<td></td>
</tr>
<tr>
<td>PFCS</td>
<td></td>
</tr>
<tr>
<td>INITL</td>
<td></td>
</tr>
<tr>
<td>100 TIMEØ  = TIME</td>
<td></td>
</tr>
<tr>
<td>TIME = TIME + ALPHA * TINC</td>
<td></td>
</tr>
<tr>
<td>CALL CAPAC1</td>
<td></td>
</tr>
<tr>
<td>CALL CAPAC2</td>
<td></td>
</tr>
<tr>
<td>CALL CAPAC3</td>
<td></td>
</tr>
<tr>
<td>CALL CAPAC4</td>
<td></td>
</tr>
<tr>
<td>CALL CAPAC5</td>
<td></td>
</tr>
<tr>
<td>CALL CAPAC6</td>
<td></td>
</tr>
<tr>
<td>TIME = TIMEØ</td>
<td></td>
</tr>
<tr>
<td>CALL ABSHT 1</td>
<td></td>
</tr>
<tr>
<td>CALL ABSHT 2</td>
<td></td>
</tr>
<tr>
<td>CALL ABSHT 3</td>
<td></td>
</tr>
<tr>
<td>CALL ABSHT 4</td>
<td></td>
</tr>
<tr>
<td>CALL ABSHT 5</td>
<td></td>
</tr>
<tr>
<td>CALL IRHS</td>
<td></td>
</tr>
<tr>
<td>TIME = TIME + TINC</td>
<td></td>
</tr>
<tr>
<td>ITER = ITER + 1</td>
<td></td>
</tr>
<tr>
<td>CALL TEMP 2</td>
<td></td>
</tr>
<tr>
<td>CALL TEMP 1</td>
<td></td>
</tr>
<tr>
<td>CALL POSTOP</td>
<td></td>
</tr>
<tr>
<td>CALL PFCS</td>
<td></td>
</tr>
<tr>
<td>CALL PRINTS</td>
<td></td>
</tr>
<tr>
<td>G0 TO 100</td>
<td></td>
</tr>
</tbody>
</table>

Write dump tape

RETURN
END
CAPAC3 Obtains the capacitance of each node of this type by interpolating a time-dependent curve, a temperature dependent curve and obtaining the product of the two values and then multiplying the results by an input constant.

CAPAC4 Obtains the capacitance of each node of this type by interpolating a temperature dependent curve and multiplying it by an input constant.

CAPAC5 Obtains the capacitance of each node of this type by interpolating two temperature dependent curves, finding the product of the two values and multiplying the results by a constant.

CAPAC6 Obtains capacitance as a function of time and two temperature dependent curves.

CONDF1 Calculates the flow conductors for all options.

CONDV Calculates the convection conductors for all options.

COND2 Obtains conductance as a function of time.

COND3 Obtains the conductance by interpolating a temperature dependent curve with mean temperature between the two nodes connected and multiplying the result by a constant.

COND4 Obtains the conductance between two nodes, one with temperature dependent properties, and one without.

COND5 Obtains the conductance between two nodes, both with temperature dependent properties.

RADTN Calculates the linearized conductance due to radiation for a constant $\sigma A$.

ABSHT1 Supplies constant absorbed heat values to nodes.

ABSHT2 Supplies time dependent absorbed heat values to nodes.

ABSHT3 Obtains absorbed heat by interpolating a time dependent curve and multiplying by a constant.

ABSHT4 Obtains absorbed heat as the product of a time dependent curve, a temperature dependent curve and a constant.
<table>
<thead>
<tr>
<th>Code</th>
<th>Description</th>
</tr>
</thead>
<tbody>
<tr>
<td>ABSHT5</td>
<td>Obtains absorbed heat as the product of a temperature dependent curve and a constant</td>
</tr>
<tr>
<td>PRETMP</td>
<td>Performs user logic specified by the user in the $PRETEMP$ operation block</td>
</tr>
<tr>
<td>KONDF</td>
<td>Calculates the net heat flow to each node through flow conductors (one way) and add the quantity to the Q array. Also adds the conductance values for each node to the DTAU array for future calculation of time increments.</td>
</tr>
<tr>
<td>KOND</td>
<td>Calculates the net heat flow to each node through the normal two way conductors and adds it to the Q array. Also adds the conductance values for each node in the DTAU array for future calculation of time increments.</td>
</tr>
<tr>
<td>RADC</td>
<td>Calculates the net heat flow to each node due to radiation conductors and adds the values to the Q array. Also adds the required constant to the DTAU array for calculating time increments.</td>
</tr>
<tr>
<td>DTAU1</td>
<td>Calculates the convergent time increment for each node and applies the appropriate limits depending upon the option.</td>
</tr>
<tr>
<td>DTAU2</td>
<td>Calculates new temperatures using the explicit method.</td>
</tr>
<tr>
<td>TEMPI</td>
<td>Calculates new temperatures using the implicit method.</td>
</tr>
<tr>
<td>POSTMP</td>
<td>Performs user logic specified by the user in the $POST TEMP$ operation blank.</td>
</tr>
<tr>
<td>PRINTS</td>
<td>Performs normal output, checkout print, writes history tape and calculates incrementing time values.</td>
</tr>
</tbody>
</table>
5.0 PROGRAM USAGE DESCRIPTION

MOTAR can be used to predict the transient or steady state temperature behavior in a system including the effects of conduction, convection, and/or radiation; to predict the pressure and flow rate for a network of tubes containing a flowing fluid for any combination of series and parallel flow; to perform any general mathematical operation by supplying the required logic to the user programming blocks including calls to the appropriate MOTAR library subroutines, or any combination of these three uses. The following is the sequence of events or steps that the user must follow in performing a thermal and/or flow analysis:

1. Mathematical models must be constructed
2. The values describing the elements of the models must be established and input into MOTAR in the proper format.
3. The job must then be submitted to run on the computer system of interest following proper preparation for that system.
4. The answers are then received for evaluation by the user.

In developing MOTAR every effort was made to permit its user to complete the above tasks with a maximum of effectiveness and a minimum of effort. The input format was designed to be as powerful as possible while remaining flexible and easy to use. The output was also designed to be flexible, giving the user the ability to choose any of the many available output options or to make his own output format when desired. Extensive error messages and checkout printing should aid the user in checking out new data decks. Extensive plotting of the output with a minimum requirement of input is available which should also add to the user effectiveness. Many other input/output options are included in MOTAR which take advantage of the available input/output devices on the NASA computer system. Included in these are the dump and restart options, the data tape and edit options, the start from the history tape options, and flux curves on tape.

5.1 MATHEMATICAL MODEL BUILDING

The first step in performing a thermal or flow-pressure analysis using MOTAR is that of building a mathematical model. The intent of this section is to describe the nature of the thermal and flow models needed for input into MOTAR.

5.1.1 Thermal Models

A mathematical model of the thermal problem must be constructed by the user so that the elements of equation (6) (Section 3.1.1) can be identified for input to MOTAR. The equation is repeated for clarity:

\[
\frac{C_i (T_{i\text{r}+1} - T_i^n)}{\Delta \tau} = \left[ \sum_{j=1}^{nc} U_{ij} (T_j - T_i) + Q_i \right]_m, \quad i=1,N
\]
where

\[ C_i = \text{the thermal capacitance of node i} \]
\[ W_i = \text{the weight of lump i} \]
\[ C_{pi} = \text{the specific heat of lump i} \]
\[ T_i^{n+1} = \text{temperature of lump i at iteration } N + 1 \]
\[ T_i^n = \text{temperature of lump i at iteration } n \]
\[ \Delta \tau = \text{the iteration time increment} \]
\[ U_{ij} = \text{the overall thermal conductance between nodes i and j} \]
\[ Q_i = \text{the heat rate absorbed or generated by node i} \]
\[ nc = \text{the number of thermal connections} \]
\[ m = \text{the time between that corresponding to iteration } n \text{ and that corresponding to iteration } n + 1 \text{ for evaluation of the heat flow to the node (i.e., the right side of the equation)} \]
\[ N = \text{number of nodes} \]

The primary elements that must be identified for input are:

1. Identification numbers for each node, i
2. Initial Temperatures for the nodes, Ti
3. Thermal Capacitances for the nodes, Ci
4. Absorbed or generated heat fluxes for nodes where applicable, Qi
5. Identification numbers for the conductors and nodes connected, i and j
6. Conductor Values Uij, whether for conducting, convection, radiation, or flowing fluid heat transfer

The thermal model of a body is constructed by subdividing it into a number of small elements of volume. By the finite difference method of solution the mass of each element is assumed to be concentrated at that nodal point which lies within the volume of the element. The temperature which is calculated represents the temperature of the point mass. Care must be taken in the subdivision of a body into its volume elements. The size of the volume elements or "lumps" must be small enough to give a sufficiently
accurate temperature distribution in the body. However, if it is excessively small a severe computer time requirement may occur. Thus, an "optimum" size is desired. A detailed discussion on the recommended practices for thermal model building will not be attempted here. Instead, the reader is referred to References 1 and 13.

An example showing the method of subdividing a body into lumps and identifying the network elements whose values must be input into MOTAR is shown in Figure 7. Figure 7(a) shows an extended fin with a base temperature, $T_b$, and convecting to an ambient temperature, $T_a$. Solar energy is incident on the fin from location $l_1$ to the end of the fin, $l_2$. Figure 7(b) shows one possible nodal breakdown for building a thermal model. It consists of 5 nodes which have been arbitrarily numbered representing equal volumes bounded by the fin temperature and the air temperature with absorbed heat on the last three nodes. Figure 7(c) shows the thermal network of the fin for the nodal breakdown of Figure 7(b). Identified on the network are the elements whose values must be input. The T's represent the node temperature, C's represent the node thermal capacitances, Q's represent the node absorbed heats, and the G's represent the conductance values between nodes which have also been arbitrarily numbered. The capacitances are calculated by

$$C(I) = (\rho)(VOL)(C_p)$$

where

$C(I)$ = capacitance of node I

$\rho$ = Density of node I

$VOL$ = the volume of node I

Note that the boundary nodes, #6 and #7, have no capacitances since their temperatures are specified. The conductances for G(1) through G(5) are calculated by the relation for conduction which is

$$G(I) = \frac{kA}{\Delta x}$$

where

$k$ = thermal conductivity

$A$ = area for conduction

$\Delta x$ = the conduction distance

Those for G(6) through G(10) are calculated by the relation for convection which is

$$G(I) = hA$$

where

$h$ = convection coefficient

$A$ = area for convection
Figure 7: Example Thermal Mathematical Model
The absorbed heat for nodes 3 through 5 is calculated by

\[ Q(1) = \alpha_s A Q_{\text{solar}} \]

where

- \( Q_{\text{solar}} \) = Incident solar energy per unit area of the fin
- \( A \) = Area of incident solar heat
- \( \alpha_s \) = Absorptivity of the fin surface to the incident heat

The input values for T's defining the initial and boundary temperature for the problem complete the identification of the elements for the problem.

5.1.2 Fluid Flow Models

A flow problem may be analyzed with MOTAR, either simultaneously with a thermal analysis, so that the flow solution is continually updated based on the thermal conditions or, the flow problem may be analyzed separately without any thermal analysis. To perform a flow analysis, the user must input a mathematical model of the flow system. The flow system is assumed to consist of a set of interconnected tubes such as the example shown in Figure 8(a) which consists of two radiator panels, each containing four tubes and connected so that they flow in parallel.

For clarity the following definitions are made at this point:

1. A tube is any single length of pipe between two pressure nodes. A tube "contains" fluid temperature nodes and may contain as many of these as desired.

2. A pressure node is located at each end of a tube. As many tubes as desired may be connected at a node junction and a node must exist at the junctions of two flow pipes.

We must make a mathematical model to describe the information of equation (60) to the computer. The information required consists of

1. Identification of the pressure node numbers
2. Identification of the tube numbers and the two pressure nodes connected by tube
3. The fluid temperature nodes contained in each tube
4. The flow geometry for each temperature fluid nodes
5. The number of "head losses" such for items such as orifices
6. Fluid property information
Figure 8  Example Flow System Mathematical Model
The fluid flow mathematical model may be described as a network equivalent to an electrical resistor network. For instance, the flow system shown in Figure 8(a) can be described by the resistance network shown in Figure 8(b). In building a flow model the user may either build a resistance/node network as—shown in Figure 8(b)—or simply superimpose the identifying numbers on a schematic of the flow system as shown in Figure 8(a). In either case the identifying numbers and connection information is readily available if the identifying numbers are placed on the schematic. If one adds the fluid temperature numbers to the information shown for each tube, the information for items 1, 2, and 3 above can be read directly from the schematic. Items 4, 5, and 6 must be obtained from knowledge about the system geometry and materials.

5.2 INPUT DESCRIPTION

The input for MOTAR has been designed to give the user a high degree of effectiveness and flexibility while maintaining an easy-to-use format. The effectiveness is accomplished by providing powerful options to the user which permit the input of large quantities of data with a single entry in the input. The flexibility is obtained by providing the user with a large number of options for each data entry. Many features were incorporated to make the routine easy to use which include the use of descriptive names to identify data blocks, the ability to omit blocks not requiring input data for a given problem, and the use of a free form input format. This format permits data to be input in any column between 2 and 74 (inclusive) with data values separated by delimiters.

5.2.1 General Input Requirements

The user input for MOTAR consists of three parameter cards and 7 major input data blocks with each being identified by a $ followed by its title. Some of the 7 blocks contain subordinate blocks which are identified by a + followed by the block title. Some of these subordinate blocks contain additional subordinate blocks which are identified by enclosing the block name between two apostrophies. In addition to the 7 input blocks, three additional data cards are required. The first supplies information regarding the method for data input (cards, tape, tape with data edits, etc) and information identifying whether the run is to be implicit or explicit. The second card supplies time information and the third supplies input/output option information and tolerance information for implicit runs.

A list of the possible input blocks including the major blocks and all the subordinate blocks is shown in Table III. Only those blocks required to supply information need be input. If a block is empty its block title need not be input. Also shown in Table III are three parameter cards and their location relative to the 7 Data Block. Parameter Card No. 1 is located immediately following the XQT STEP1 card and thus is the very first data card. Parameter cards no. 2 and 3 are located immediately following the XQT STEP2 Card and thus, are the very last data input cards prior to the EOF card. While all of the seven major data blocks may be input either on cards or on tape, the three parameter cards must all be input as cards and must always be supplied regardless of the type of run.
### TABLE III
SUMMARY OF MOTAR INPUT DATA

<table>
<thead>
<tr>
<th>7g XQT STEP 1</th>
</tr>
</thead>
<tbody>
<tr>
<td>PARAMETER CARD 1</td>
</tr>
<tr>
<td>$ NETWORK DATA</td>
</tr>
<tr>
<td>+ INITIAL TEMPERATURES</td>
</tr>
<tr>
<td>+ CAPACITANCE</td>
</tr>
<tr>
<td>+ CONDUCTORS</td>
</tr>
<tr>
<td>'CONDUCTION'</td>
</tr>
<tr>
<td>'RADIATION'</td>
</tr>
<tr>
<td>'CONVECTION'</td>
</tr>
<tr>
<td>'FLOW'</td>
</tr>
<tr>
<td>+ ABSORBED HEAT DATA</td>
</tr>
<tr>
<td>$ FLOW SYSTEMS</td>
</tr>
<tr>
<td>+ SYSTEM XX (CODE XX)</td>
</tr>
<tr>
<td>'PARAMETER'</td>
</tr>
<tr>
<td>'FLOW NETWORK'</td>
</tr>
<tr>
<td>'SUB-NETWORK = 1'</td>
</tr>
<tr>
<td>'SUB-NETWORK = N'</td>
</tr>
<tr>
<td>'FLUID LUMP DATA'</td>
</tr>
<tr>
<td>'PUMP'</td>
</tr>
<tr>
<td>'VALVES'</td>
</tr>
<tr>
<td>+ SYSTEM XXX (CODE XXX)</td>
</tr>
<tr>
<td>'PARAMETER'</td>
</tr>
<tr>
<td>$ CURVES</td>
</tr>
<tr>
<td>$ CENTRAL</td>
</tr>
<tr>
<td>$ PRETEMP</td>
</tr>
<tr>
<td>$ POSTTEMP</td>
</tr>
<tr>
<td>$ OUTPUT</td>
</tr>
<tr>
<td>$ END</td>
</tr>
<tr>
<td>7g FOR, K STEP2</td>
</tr>
<tr>
<td>7g FOR, K TEMPTR</td>
</tr>
<tr>
<td>7g FOR, K PRETMP</td>
</tr>
<tr>
<td>7g FOR, K PSTTMP</td>
</tr>
<tr>
<td>7g FOR, K OUTPUT</td>
</tr>
<tr>
<td>7g FOR, K TEMPSS</td>
</tr>
<tr>
<td>7g XUT STEP 2</td>
</tr>
<tr>
<td>PARAMETER CARD 3</td>
</tr>
<tr>
<td>PARAMETER CARD 3</td>
</tr>
<tr>
<td>7g EOF</td>
</tr>
</tbody>
</table>
The general rules for MOTAR input which apply for the seven input data blocks are listed below:

1. The input for any item-including data in blocks or block headings can be written in free form in any columns between 2 and 74 inclusive.

2. All blank spaces in the input are ignored. Thus, a blank card is also ignored.

3. A comment containing any character can be written on any card between an asterisk and column 74. Everything between the asterisk and column 74 will be read and written out. The comment should not extend into column 75 since this column is used for continuation. Columns 1 and 76 thru 80 are reserved for Edit. The asterisk for comments should not occur in column 1.

4. A "data group"* can be continued on the following card by any non-zero entry in column 75. This entry will cause the data group on the card prior to the asterisk (if one exists) to be continued on the next card.

5. Several data groups may be entered on a single card if separated by a slash (/). For example three initial temperatures (each being a single data group) might be put on one card as follows:

   \[1 = 90. / 5 = 100. \ 7 = 97.5\]

6. Any system of units can be used for a given problem but all input items must be in consistent units. This required the following values be input in the problem units: (1) the temperature for the input units at absolute zero and the Stephan-Boltzman constant for thermal radiation analyses and (2) the gravitational constant \((g_c)\) for flow-pressure analysis.

7. The seven data blocks may be input in any order. All subordinate blocks may be input in any order as long as they are input under their main heading.

* A "data group" is defined as a group of data which must be input in a specified order. For instance, the input required for a conductor would be a data group consisting of the conductor number, the two nodes connected and the value of the conductance.
8. The heading or title for each data block or subordinate block is entered with the proper delimeter (\$ or +, or ') followed by the block title or at least the first three letters of the title (May be input in any column between 2 and 74 inclusive).

9. Any block or subordinate block not required can be omitted including its heading card if it supplies no information.

10. Numbers may be input as integers or real numbers. The real numbers may be input in pure decimal form such as 3.54 or in exponential form such as 3.76E-10 where the exponent is -10. As with all other input, blanks in numbers are ignored so that 3. 54 would be read 3.54. Also, the user may input as many significant figures as desired and the computer will pick up to the maximum digit capability of the machine.

The input requirements for the parameter cards, the 7 major data blocks, and their subordinate blocks, are described in the following subsections.

5.2.2 Parametric Data Card

Three parametric data cards must be supplied on each MOTAR run to supply data edit information, time information, input/output codes and implicit run information. Unlike the seven data blocks, these cards must always be supplied and the data must be entered in a fixed format. The location of the parameter cards relative to the other input data and system setup cards is shown in Table III. A description of the input for each of the three parameter cards is given below:

<table>
<thead>
<tr>
<th>PARAMETER CARD NO. 1</th>
</tr>
</thead>
<tbody>
<tr>
<td>COLUMNS</td>
</tr>
<tr>
<td>1-5</td>
</tr>
<tr>
<td>6-10</td>
</tr>
</tbody>
</table>

<table>
<thead>
<tr>
<th>PARAMETER CARD NO 2</th>
</tr>
</thead>
<tbody>
<tr>
<td>COLUMNS</td>
</tr>
<tr>
<td>1-10</td>
</tr>
</tbody>
</table>

75
<table>
<thead>
<tr>
<th>COLUMNS</th>
<th>NOMENCLATURES</th>
<th>FORMAT</th>
<th>DESCRIPTION</th>
</tr>
</thead>
<tbody>
<tr>
<td>11-20</td>
<td>TINCMN</td>
<td>F10.0</td>
<td>Minimum stable time increment for the No Overriding Option. TINCMN must be 0 for the Override or Floating Option.*</td>
</tr>
<tr>
<td>21-30</td>
<td>TINC</td>
<td>F10.0</td>
<td>Problem Time Increment</td>
</tr>
<tr>
<td>31-40</td>
<td>STIME</td>
<td>F10.0</td>
<td>Problem Stop Time</td>
</tr>
<tr>
<td>41-50</td>
<td>WINC</td>
<td>F10.0</td>
<td>Print Interval</td>
</tr>
<tr>
<td>51-60</td>
<td>PINC</td>
<td>F10.0</td>
<td>Plot Interval. If 0, no plotting will occur</td>
</tr>
<tr>
<td>61-70</td>
<td>TMPTIM</td>
<td>F10.0</td>
<td>Time that history tape will be read for initial temperatures, flow rates and value position. If 0, will be set to TIME.</td>
</tr>
<tr>
<td>71-80</td>
<td>DQTIME</td>
<td>F10.0</td>
<td>Time scale shift for flux curves. DQTIME is added to the problem time prior to interpolating flux curves.</td>
</tr>
</tbody>
</table>

**PARAMETER CARD NO. 3**

<table>
<thead>
<tr>
<th>COLUMNS</th>
<th>NOMENCLATURES</th>
<th>FORMAT</th>
<th>DESCRIPTION</th>
</tr>
</thead>
<tbody>
<tr>
<td>1-5</td>
<td>RTIME</td>
<td>F 5.0</td>
<td>Computer Time in minutes requested for run if 0., will be set to 5.</td>
</tr>
<tr>
<td>6-7</td>
<td>ISTART</td>
<td>I2</td>
<td>= 0, This problem is not being restarted Data must be supplied for starting problem</td>
</tr>
<tr>
<td></td>
<td></td>
<td></td>
<td>≠ 0, This problem is being restarted Restart data is supplied on Unit L</td>
</tr>
<tr>
<td>8-9</td>
<td>NEWTMP</td>
<td>I2</td>
<td>= 0, The history tape will not be read to obtain initial conditions</td>
</tr>
<tr>
<td></td>
<td></td>
<td></td>
<td>≠ 0, The history tape, Unit H, will be read at TMPTIM (Card 2) to obtain initial conditions</td>
</tr>
<tr>
<td>10-11</td>
<td>NFLXCD</td>
<td>I2</td>
<td>= 0, No incident heat curves will be supplied on separate flux tape</td>
</tr>
<tr>
<td></td>
<td></td>
<td></td>
<td>≠ 0, Some of the incident heat curves will be supplied on Unit E</td>
</tr>
<tr>
<td>12-13</td>
<td>NCKOUT</td>
<td>I2</td>
<td>= 0, No checkout print will be given</td>
</tr>
<tr>
<td></td>
<td></td>
<td></td>
<td>≠ 0; A checkout print will be given</td>
</tr>
<tr>
<td>14-15</td>
<td></td>
<td>Blank</td>
<td></td>
</tr>
<tr>
<td>16-20</td>
<td>MXPASS</td>
<td>I5</td>
<td>Maximum number of Gauss-Siedel iterations permitted on each iteration for solution to temperature equations. If = 0, set to 100</td>
</tr>
</tbody>
</table>

* See Page A-5
<table>
<thead>
<tr>
<th>COLUMNS</th>
<th>NOMENCLATURES</th>
<th>FORMAT</th>
<th>DESCRIPTION</th>
</tr>
</thead>
<tbody>
<tr>
<td>21-25</td>
<td>ALPHA</td>
<td>F5.5</td>
<td>Point within the iteration for evaluation of heat flux on implicit runs. If ALPHA = 1.0, backward difference occurs; if ALPHA = 0.5, mid difference occurs; if ALPHA = 0 it is set to 1.0; if ALPHA &lt; 0.5 it is set to 0.5.</td>
</tr>
<tr>
<td>26-30</td>
<td>DTMXA</td>
<td>F5.5</td>
<td>Temperature Solution Tolerance. A solution is reached when all temperatures change less than DTMXA on a given iteration. When =0, set to 0.01</td>
</tr>
<tr>
<td>31-35</td>
<td>ORP</td>
<td>F5.4</td>
<td>Overrelaxation parameter for implicit solution. Set to 1.0 if 0.</td>
</tr>
<tr>
<td>36-45</td>
<td>SSTEST</td>
<td>F10.9</td>
<td>Steady state test. Steady state is reached when all temperatures change less than SSTEST on a given iteration; if SSTEST = 0.0, it is set to 0.0001</td>
</tr>
<tr>
<td>46-55</td>
<td>IPASS</td>
<td>I10</td>
<td>Maximum number of iterations permitted to reach steady state; if IPASS = 0, it is set to 10000.</td>
</tr>
</tbody>
</table>
5.2.3 Network Data Block

The "NETWORK DATA" block contains the information required to describe the thermal network. The information is input in four subordinate blocks with the conductor block containing four additional subordinate blocks as shown in Table III. The following subordinate blocks are continued in the NETWORK DATA block:

\[
\text{\$ NETWORK DATA} \\
+ \text{INITIAL TEMPERATURES} \\
+ \text{CAPACITANCES} \\
+ \text{CONDUCTORS} \\
\quad \text{'CONDUCTION'} \\
\quad \text{'FLOW'} \\
\quad \text{'RADIATION'} \\
\quad \text{'CONVECTION'} \\
+ \text{ABSORBED HEATS}
\]

The blocks headed by + may be input in any order and those enclosed in apostrophes may be in any order but must all be contained in the conductor block. Any block or subordinate block not required may be omitted. A description of the input requirements and options for each of the blocks is described below.

5.2.3.1 Initial Temperatures

The initial temperatures are supplied in the block headed by:

+ INITIAL TEMPERATURE

The format for input of the initial temperatures is an integer, or a group of integers, representing node numbers followed by an equal sign followed by the specification of the initial temperature. Thus, the numbers on the left side of the equal specify node numbers and numbers on the right side specify temperatures. Several options are available for both sides.

The option for specifying the node numbers on the left of the equal sign are described below.

OPTION 1: Single input

The input format is:

\[
\text{NN} = \text{TI}
\]

where NN = The node number

TI = the node initial temperature

If NN is a negative integer the node is a boundary and no calculation will be made to change the temperature. Thus, it will remain at the initial value, TI throughout the problem. If an integer is supplied instead of a real number, it specifies a time dependent curve which describes the temperature of node NN as
a function of time.

OPTION 2: Multiple input separated by commas

The input format is:

N1, N2, ---, NN = TI

where N1, N2, ---NN = the node numbers with initial temperature, TI

As many node numbers as desired by be supplied in this manner (see Section 5.2.1 for rules on continuation cards, etc.). The node numbers, N1, N2 ---NN, may be input in any random order.

OPTION 3: Input of a group of sequential nodes

The input format is:

N1 thru N2 = TI

where N1 is the starting node number of the group

N2 is the final node number of the group

This option means all nodes between and including N1 and N2 are assigned a value of TI. N1 may be either smaller than, larger than, or equal to N2. It may be an integer or real as described on Option No. 1.

OPTION 4: Input of a group of nodes with equal spacing between the numbers

The input format is:

N1 thru N2 by N3 = TI

where N1 = the starting node number of the group

N2 = the final node number of the group

N3 = the integer spacing for the numbers between the starting and final numbers

Using Option 4, N2-N1 must be an integer multiple of N3.

Some illustrative examples of the input for the initial temperatures are shown in Table IV.

5.2.3.2 Thermal Capacitances

The thermal capacitances for the temperature nodes are input in the block headed by:
TABLE IV
EXAMPLES OF INPUT FOR INITIAL TEMPERATURES

+ INITIAL TEMPERATURES

1 = 50  * Node 1 is initially at temperature = 50.
-3 = -459.69  * Node 3 is a boundary at -459.69
2, 4, 5 = 75.  * Nodes 2, 4, and 5 initially at 75.
6 = 11  * Node 6 temp supplied on curve 11.
7 = 62. / 8 = 43. / 9 = 77  * Initial temperature of nodes 7, 8, and 9 all supplied on the same card.
10 thru 19 = 102.  * Nodes 10 thru 19 all have initial temps of 102.
51 thru 55 = 21  * Temperature vs. time for nodes 51 thru 55 supplied on curve 21.
40, 42 thru 45, 74 = 100.  * Initial temperatures of node 40, 42 thru 45, and 47 are 100.
22 thru 38 by 2 = 57.  * Temps for even nodes between 22 and 38.
20, 21 thru 39 by 2, 56 thru 60 = 66.  * Temps for node 20, odd nodes between 21 and 39 and 56 thru 60 = 66.
which is subordinate to the NETWORK DATA block. The format for input of the thermal capacitance is specification of the node numbers on the left of an equal and specification of the capacitance on the right of the equal. The options for specifying the node numbers are the same as those for the initial temperatures described in section 5.2.3.1. The values for capacitance are specified to the right of the equal in either one, two or three values. Any of the values (whether one, two or three values are supplied) may be integers or real numbers (containing decimals). When integer values are supplied, each identifies a tabulated curve to be interpolated during the run. An integer for the first value to the right of the equal identifies a curve which is a function of time. Integers for the second and/or third values indicate curves to be interpolated as a function of the node temperature. Any combination of one, two, or three numbers, any of which may be real or integers, may be input. In the preprocessing phase (problem setup) all real numbers are multiplied together. In the processing phase (the problem analysis) real values are obtained from the curves identified by integers and multiplied times the constant values to obtain capacitances on each iteration.

Some examples for capacitance input are shown in Table V.

5.2.3.3 Thermal Conductors

Thermal conductors are input in a block headed by

+ CONDUCTORS

which is contained in the higher level $ NETWORK DATA block. The + CONDUCTORS blocks data is contained in four subordinate blocks headed by 'CONDUCTION', 'CONVECTION', 'FLOW', and 'RADIATION', each containing the input for the type of conductor indicated by its descriptive heading. Some of the general rules which apply to conductors are:

1. A conductor number must be unique regardless of the type of conductor. That is, a conductor number used in one block cannot again be used in that block or any of the other three blocks.

2. Conductor numbers do not have to be input in any particular order. Also, they do not have to be numbered sequentially although sequential numbering is most efficient from a space utilization standpoint.

3. The four conductor subordinate blocks may be input in any order as long as they are within the + 'CONDUCTOR' heading.

4. The headings for each of the conductor subordinate block consists of their name enclosed in quotations as follows:

(a) 'CONDUCTION'
(b) 'CONVECTION'
(c) 'FLOW'
(d) 'RADIATION'

The nine general rules previously given for input also apply.

The input format for the conductors consists of connection identification numbers (conductor numbers, and nodes connected) on the left side of the equal and specifications for determining the conductor value on the right of the equal. The options for specifying connections identification
### TABLE V
EXAMPLES OF CAPACITANCE INPUT

<table>
<thead>
<tr>
<th>Capacitances</th>
<th>Capacitances</th>
</tr>
</thead>
<tbody>
<tr>
<td>1</td>
<td>= .35</td>
</tr>
<tr>
<td>1,12,13</td>
<td>= .47, .06, .53</td>
</tr>
<tr>
<td>3 THRU 10</td>
<td>= .61, .27</td>
</tr>
<tr>
<td>12</td>
<td>= .32, 62.4, 22</td>
</tr>
<tr>
<td>13 THRU 17 BY 2</td>
<td>= .32, 12, 22</td>
</tr>
<tr>
<td>14 THRU 18 BY 2</td>
<td>= .07, 12, .5</td>
</tr>
<tr>
<td>19 THRU 25, 31 THRU 35</td>
<td>= .57, 12</td>
</tr>
<tr>
<td>26 THRU 30</td>
<td>= 41, .06, 70</td>
</tr>
<tr>
<td>36</td>
<td>= 41, 5.3</td>
</tr>
<tr>
<td>37</td>
<td>= 51</td>
</tr>
<tr>
<td>38</td>
<td>= 61, 12, 22</td>
</tr>
<tr>
<td>39</td>
<td>= 61, 12, .76</td>
</tr>
<tr>
<td>40</td>
<td>= 61, 70, .22</td>
</tr>
<tr>
<td>41</td>
<td>= 61, 12</td>
</tr>
</tbody>
</table>

In the comments above,

- \( C(N) \) = Capacitance of node \( N \)
- \( \text{CURVE}(M,T(N)) \) = the interpolated value of curve \( M \) at the temperature of node \( N \)
- \( \text{CURVE}(M,\text{TIME}) \) = the interpolated value of curve \( M \) at the problem time
- \( \times \) = indicates multiplication
are the same for all four conductor blocks and are similar to those for specifying node numbers in the + INITIAL TEMPERATURE block except the numbers are input in groups of 3. These three numbers are conductor number, node connected, node connected. The options for specifying the conductors values are numerous and vary depending on which of the four subordinates blocks the input is in. The various options for connections identification and connection value specification are described below:

Conductor Connections Identifications
The connections identification for the conductors are input on the left of an input equal sign and they identify the conductor number and nodes connected. The options are the same for these identifiers (left side of the equal) for all blocks subordinate to the +CONDUCTOR heading. The options for connection identifications are described below:

OPTION 1: Single connection input
The input format is:
\[ NC, N1, N2 = VALUE \]
Where \( NC \) = the conductor number
\( N1, N2 \) = Nodes connected
\( VALUE \) = The specified value of the conductor (many options are available depending on the type of conductor)

The order of input of \( N1 \) and \( N2 \) is important for the 'FLOW' block and 'CONVECTION' block.

OPTION 2: Multiple input separated by commas
The input format is:
\[ NC1, N11, N21, NC2, N12, N22, \ldots, NCn, N1n, N2n = VALUE \]
Where \( NC1, NC2, \ldots, NCn \) = Conductor numbers
\( N11, N12 \) = First set of nodes connected
\[ \vdots \]
\( N1n, N2n \) = nth set of nodes connected

Any option for determining \( VALUE \) may be used which is available in the input block under consideration.

OPTION 3: Input of a group of sequentially incremented connections
The input format is:
\[ NC1, N11, N21 \text{ THRU } NCn, N1n, N2n = VALUE \]
Where \( N_C1 = \) the starting conductor number
\( N_l1 = \) the starting node number for side 1
\( N_21 = \) the starting node number for side 2
\( N_Cn = \) the final conductor number
\( N_ln = \) the final node number for side 1
\( N_2n = \) the final node number for side 2

For this option, \( N_Cn - N_C1 \) must equal \( N_ln - N_l1 \) and \( N_2n - N_21 \). All the options available for VALUE are applicable here.

**OPTION 4: Input of a group of connections sequentially incremented by an input integer**

The input format is:

\[ N_C1, N_l1, N_21 \text{ THRU } N_Cn, N_ln, N_2n \text{ BY } I_C, I_l, I_2 = \text{ VALUE} \]

Where \( N_C1 = \) the starting conductor number
\( N_l1 = \) the starting node number on side 1
\( N_21 = \) the starting node number on side 2
\( N_Cn = \) the final conductor number
\( N_ln = \) the final node number on side 1
\( N_2n = \) the final node number on side 2
\( I_C = \) the increment for the conductor numbers
\( I_l = \) the increment for the node numbers or side 1
\( I_2 = \) the increment for the node numbers on side 2

For this option, the following relations must hold:

\[ \frac{N_Cn - N_C1}{I_C} = \frac{N_ln - N_l1}{I_l} = \frac{N_2n - N_21}{I_2} \]

When \( I_x = 0 \), \( N_xn \) must equal \( N_xl \) for the nodes connected

**'CONDUCTION' BLOCK**

Numer options are available specifying the conduction conductor values or methods for determining their values. These specifications are input on the right of the equal sign with any of the connections identification options discussed above on its left. The options for conduction input are described below.

**OPTION 1: Constant Conductor**

The input format is:

\[ NC, N_l, N_2 = \text{ CONST} \]

Where \( NC, N_l, N_2 = \) Connections identification input by any of the available options
\( \text{CONST} = \) the constant value of the conductance

**OPTION 2: Conduction in homogeneous material which is tem-**
perature dependent. Input by a temperature dependent curve with a constant multiplier. The input format is:

$$NC, N1, N2 = AX, NK(TM)$$

Where $NC, N1, N2$ = connections identifications input by any available option

$AX$ = the constant portion of the conductance typically $A/X$, where $A$ = conduction area and $X$ = distance

$NK(TM)$ = a temperature dependent curve number which is interpolated with temperature $TM$. Normally this is a thermal conductivity curve

$TM$ = Mean temperature between $T(N1)$ and $T(N2)$

$$TM = \frac{T(N1) + T(N2)}{2.0}$$

OPTION 3: Conduction in non-homogeneous material where one material is temperature dependent and one is not.

(A) $N1$ is the node containing temperature dependent thermal conductivity.

The input format is:

$$NC, N1, N2 = AX1, NK(TM), KAX2$$

Where $NC, N1, N2$ = connections identification input by any of the available options

$AX1$ = $A/X$ for node $N1$

$NK(TM)$ = thermal conductivity curve for the materials of node $N1$ interpolated on each iteration at the temperature of $N1$

$KAX2$ = the constant value of $KA/X$ for node $N2$

The conductance for each iteration is obtained by

$$U(NC) = \frac{1}{\frac{1}{AX1 K(TM1)} + \frac{1}{KAX2}}$$

(B) $N2$ is the node containing temperature dependent thermal conductivity

The input format is:
\[ NC,N1,N2 = KAX1,AX2,NK(TN2) \]

Where \( NC,N1,N2 \) = Connections identification input by any of the available options

- \( KAX1 = \) The constant value for conductance, \( KA/X \) for node 1
- \( AX2 = \) A/X for node N2
- \( NK(TN2) = \) the thermal conductivity curve number for the material of node N2 interpolated at temperature of node N2

OPTION 4: Conduction is a non-homogeneous material with that of both nodes being temperature dependent

The input format is:

\[ NC,N1,N2 = AX1,NK(TN1),AX2,NK(TN2) \]

Where \( NC,N1,N2 \) = Connections identifications input by any of the available options

- \( AX1 = \) A/X for node N1
- \( NK(TN1) = \) the thermal conductivity curve number of node 1. Material interpolated at temperature \( TN1 \)
- \( AX2 = \) A/X for node N2
- \( NK(TN2) = \) the thermal conductivity curve number of node 2. Material which is interpolated at temperature

The conductance is determined on each iteration when using this option by:

\[
U(NC) = \frac{1}{(AX1)k(TN1)} + \frac{1}{(AX2)k(TN2)}
\]

OPTION 5: Conductance is a function of time

The input format is:

\[ NC,N1,N2 = NKAX (TIME) \]

Where \( NC,N1,N2 \) = connections identification input by any of the available options

- \( NKAX(TIME) = \) An integer specifying the value of the conductance as a function of TIME

Some examples of the 5 options for specifying the conductance values for conduction are given in Table VI.
TABLE VI
EXAMPLES OF CONDUCTION INPUT

'CONDUCTION'

1,5,6=1.3 * CONDUCTOR NO.1 HAS A CONSTANT VALUE OF 1.3

2,6,7=.8,62 * A/X=0.8;K INTERPOLATED AT (T(6)+T(7))/2. ON
* EACH ITERATION; CONDUCTANCE = KA/X

5,7,8=.19,62,11. * A/X(7)=.19,K(7)=CURVE(62,T(7))),
* KA/X(8)=11.

7,20,21=11,.19,62 * KA/X(20)=11.,A/X(21)=.19,K(21)=CURVE
* (62,T(21))

6,,7,20=.19,62,.31,72 * A/X(7)=.19,K(7)=CURVE(62,T(7))A/X(20)=.31,
* K(20)=CURVE(72,T(20))

9,21,8=11 * CONDUCTANCE NO 9 GIVEN AS FUNCTION OF TIME
* ON CURVE 11

In the above

A = Area for conduction
K = Thermal conductivity
X = Conduction Distance
CURVE(M,T(N)) = Interpolation of tabulated curve no. M at the
temperature of node N,T(N)
'CONVECTION' Block

The options which are available for determining conductor values for convection heat transfer are primarily options for determining the convection heat transfer coefficient, h, since the conductor values is hA, A being the constant heat transfer area for convection. A is input as a constant value for all the convection options. As described in Section 3.1.3.1 options available for calculating h are (repeated here for clarity)

Option 1: h for flow in a tube

(A) LAMINAR FLOW (Re < 2000)

\[ h = \frac{k}{D} \left( 3.66 \cdot F_1 + \frac{0.0155 \cdot F_2}{\text{Re} \cdot \text{Pr}^{1/3}} \cdot \frac{1}{D} + 0.015 \cdot \frac{1}{\text{Re} \cdot \text{Pr}^{1/3}} \cdot \frac{1}{D} \right) \]

(B) TRANSITION FLOW (2000 < Re < 6400)

\[ h = \frac{k}{D} \left( 0.116 \cdot (\text{Re}^{2/3} - 125) \cdot (\text{Pr})^{1/3} \right) \]

(C) TURBULENT FLOW (Re ≥ 6400)

\[ h = 0.023 \cdot \frac{k}{D} \cdot \text{Re}^{0.8} \cdot (\text{Pr})^{1/3} \]

Option 2: St Pr^{2/3} = f(Re) or Nu = f(Re) Re Pr^{1/3}

\[ h = \frac{k}{D} [f(\text{Re}) \cdot \text{Re} \cdot \text{Pr}^{1/3}] \]

Option 3: Heat transfer coefficient is a function of flow rate

\[ h = f(\dot{w}) \]

Option 4: Heat Transfer Coefficient is a function of time

\[ h = f(t) \]

The nomenclature for the above equations is as follows:

h = the convection heat transfer coefficient

k = the thermal conductivity of the fluid

D = the hydraulic diameter of the flow passage
\[
\begin{align*}
x &= \text{the flow length from the start of the tube} \\
Re &= \text{Reynolds number} \\
Pr &= \text{Prandtl's number} \\
F_1 &= \text{Laminar Flow fully developed factor (input)} \\
F_2 &= \text{Laminar Flow entry length factor (input)} \\
f(Re) &= \text{A tabulated curve of } \frac{ST(Pr)^{2/3}}{Re} \text{ vs } Re \text{ or } \frac{NU/(Re Pr^{1/3})}{Re} \text{ vs } Re \\
f(t) &= \text{A tabulated curve of } h \text{ vs time}
\end{align*}
\]

The MOTAR input for the convection block is headed by the input of 'CONVECTION'. The information needed for the various options is described below.

Input for Option 1:

\[
\begin{align*}
\text{NC, NF, NT} &= \text{AHT, NTUBE, F1, F2}
\end{align*}
\]

where

\[
\begin{align*}
\text{NC} &= \text{Conductor number} \\
\text{NF} &= \text{fluid lump number} \\
\text{NT} &= \text{tube lump number} \\
\text{AHT} &= \text{Area for heat transfer} \\
\text{NTUBE} &= \text{tube number for finding flow rate and fluid properties} \\
\text{F1} &= \text{Laminar fully developed factor} \\
\text{F2} &= \text{Laminar entry length factor}
\end{align*}
\]

The values for F1 and F2 are assumed to be 1.0 if they are omitted.

Input for Option 2:

\[
\begin{align*}
\text{NC, NF, NT} &= \text{AHT, TUBE, CURVE (Re, ST Pr^{2/3})}
\end{align*}
\]

Where symbols are the same as above except

\[
\text{CURVE}(\text{Re, ST Pr}^{2/3}) = \text{a type 4 curve number which gives } \text{STPR}^{2/3} \text{ as a function of } \text{Re (See Section 5.2.4 for curve data description).}
\]
St = Stanton number
Re = Reynolds number

Input for Option 3:
NC, NF, NT = AHT, TUBE, CURVE (\(\dot{w},h\))
Where symbols are the same as for Option 1 except

\[ \text{CURVE (}\dot{w},h) = \text{a type 3 curve number of a curve which} \]
\[ \text{gives } h \text{ as a function of } \dot{w} \text{ in the tube} \]
\[ h = \text{heat transfer coefficient} \]
\[ \dot{w} = \text{flow rate of fluid in the tube} \]

Input for Option 4:
NC, NF, NT = AHT, CURVE (t,h)
Where symbols are the same as those for Option 1 except

\[ \text{CURVE (t,h) = A type 1 curve number of a curve which} \]
\[ \text{gives } h \text{ as a function of } t \]
\[ h = \text{heat transfer coefficient} \]
\[ t = \text{time} \]

All of the options previously described for group input of the connections identification (NC, NF, NT) are applicable to convection conductor input.

'FLOW' Block

The inputs to define the flow conductor connections and methods for their calculations are supplied in the conductor subordinate block headed by 'FLOW'. Flow conductors are "one-way" conductors designed to simulate the flow of fluid in a tube. The conductors can be utilized in other applications however. The flow conductor is calculated by

\[ U_{ij} = \dot{w}_i C_{pj} \]

Where \( U_{ij} = \) the conductance from node i to node j (but not back the other direction)
\( \dot{w}_i = \) the fluid flow rate
\( C_{pj} = \) the fluid specific heat
The input for flow conductors is the same as for the other conductors on the left of the equal sign. That is, the same options apply for the connections identification input. The input which specifies the options and values to be used in calculating conductor values is supplied on the right of the equal. It consists of four input values: KODEF, FVALUE, KODEC, CVALUE as follows:

\[ NC, NFL, NTL = \text{KODEF, FVALUE, KODEC, CVALUE} \]

Where

- NC = conductor number
- NFL = fluid lump number
- NTL = tube lump number
- KODEF = fluid flow code
- FVALUE = value or location of the value of flow rate
- KODEC = specific heat code
- CVALUE = value or location of the value for specific heat

The method for determining the flow rate is specified by KODEF and FVALUE. The flow options are described in the tabulation below:

<table>
<thead>
<tr>
<th>KODEF</th>
<th>FVALUE</th>
</tr>
</thead>
<tbody>
<tr>
<td>1</td>
<td>Constant value specifying the flow rate</td>
</tr>
<tr>
<td>2</td>
<td>Curve number of a curve which supplies flow as a function of time</td>
</tr>
<tr>
<td>3</td>
<td>Tube number in flow network data from which flow can be obtained</td>
</tr>
</tbody>
</table>

The method for determining the specific heat is specified by the values of KODEC and CVALUE. The various options are described in the tabulation below:

<table>
<thead>
<tr>
<th>KODEC</th>
<th>CVALUE</th>
</tr>
</thead>
<tbody>
<tr>
<td>1</td>
<td>Constant value for the specific heat</td>
</tr>
<tr>
<td>2</td>
<td>Curve number of a curve which gives specific heat as a function of temperature of NFL</td>
</tr>
<tr>
<td>3</td>
<td>Flow system number from which the fluid data can be found</td>
</tr>
</tbody>
</table>

Any combination of KODEF/FVALUE can be used with any combination of the KODEC/CVALUE.
'RADIATION' block

The radiation conductor connections and values are specified in the conductor subordinate block headed by

```
"RADIATION"
TZERO=-XXX.XX (XX = numbers)
SIGMA=XX.XX
```

Where

- **TZERO** = the temperature at absolute zero for the problem temperature scale (always negative or zero)
- **SIGMA** = the Stefan-Boltzman constant in the problem units

The conductor inputs consists of the connections identifications on the left of the equal sign and specifications to identify values of FA on the right of the equal. The options for the connections are the same as all the other conductor options and have been previously discussed in this section. The options for specifying the values for FA are described below.

**Option 1: Constant FA**

Input format:

```
NC, N1, N2 = FA_{12}
```

Where

- **NC** = Conductor number
- **N1, N2** = Nodes connected
- **FA_{12}** = FA value between nodes 1 and 2 (constant)

**Option 2: Constant A with temperature dependent supplied on a curve**

Input format:

```
NC, N1, N2 = A_{1}, NF_{12}(T(N1))
```

Where

- **A_{1}** = radiator area for N1
- **NF_{12}(T(N1))** = temperature dependent curve which supplies F from N1 to N2 as a function of T(N1)

**Option 3: Curve of FA as a function of time**

Input format:

```
NC, N1, N2 = NFA_{12}(TIME)
```
Where \( NFA_{12}(\text{TIME}) \) = a curve number which supplies FA as a function of time

The \( FA_{12} \) is determined by one of the three options above. The conductance is then determined by

\[
U_{12} = (\sigma)(FA_{12})\left[\left(T_1 - T\text{ZERO}\right)^2 + \left(T_2 - T\text{ZERO}\right)^2\right] \\
\left[\left(T_1 - T\text{ZERO}\right) + \left(T_2 - T\text{ZERO}\right)\right]
\]

5.2.3.4 Absorbed Heats

Absorbed and/or internally generated heat for each node is input in the block headed by:

```
+ ABSORBED HEAT
```

This block is subordinate to the $ NETWORK DATA block. The general format for the input consists of (1) the identification of the node numbers on the left of an input equal sign and (2) specification of the option to be used to obtain the absorbed heat for the node on the right of an equal. The options available for identification of node numbers on the left of the equal are the same as those for initial temperatures as discussed in section 5.2.3.1.

The methods for calculating absorbed heat are specified to the right of the equal sign by either one, two or three numbers separated by commas. The first number may be either real or integer. An integer specifies a time dependent curve number which is interpolated on each iteration. A real number is simply a multiplier for other values if others exist. The second number may also be input as a real number or an integer. An integer for the second number specifies a temperature dependent curve number which is interpolated at the node temperature on each iteration. A real number for the second number is a constant multiplier. The third number, if it exists, must be a real constant and is a multiplier.

The format for specifying the absorbed heat using the various available options are described below.

Option No. 1: Absorbed heat is one constant, two constants or three constants

The input format is

```
NN = QI, ALP,A
```

where \( NN \) = the identification of node numbers by any available option discussed in section 5.2.3.1.

\( QI,ALP,A \) = input real constants which are multiplied together to obtain absorbed heat. The second and third constants are optional; i.e., there may be one, two, or three constants.
Option No. 2: The absorbed heat is a function of time with or without constant multipliers

The input format is

\[ NN = NQI(TIME), ALP, A \]

Where

\[ NN \quad \text{The identification of node numbers by any available option} \]
\[ NQI(TIME) \quad \text{an integer specifying a curve number of a time dependent variable} \]
\[ ALP, A \quad \text{Input real constants, and are both optional; i.e., either zero, one, or two real constants may be input} \]

The absorbed heat is determined on each iteration by interpolating the NQI curve and multiplying the value by ALP and A.

Option No. 3: The absorbed heat is a function of temperature with or without constant multipliers.

The input format is

\[ NN = QI, NALP(T(NN)), A \]

Where

\[ NN \quad \text{The identification of node numbers by any available option} \]
\[ NALP(T(NN)) \quad \text{An integer specifying a curve number of a temperature dependent curve} \]
\[ QI, A \quad \text{Input real constants, } A \text{ is optional but, } QI \text{ must be supplied (May be 1.0 if not needed)} \]

The absorbed heat for nodes NN are determined by interpolating curve NALP at temperature of node NN on each iteration, multiplying the value by QI and by A if available.

Option No. 4: The absorbed heat is a function of both temperature and time with or without a constant multiplier.

The input format is

\[ NN = NQI(TIME), NALP(T(NN)), A \]
Where  

NN = The identification of node numbers by any of the available options

NQI(TIME) = An integer specifying a curve number of a curve of a time dependent variable

NALP(T(NN)) = An integer specifying a curve number of a curve of a temperature dependent variable

A = An optional real multiplier

The absorbed heat is determined by interpolating curve NQI at time and NALP at the temperature of node NN on each iteration, multiplying the interpolated values and multiplying this product by A if it is available.

The absorbed heat calculated by any of the above options is added to that already calculated by some other means. Thus, a user may specify as many absorbed heat curves as required.
5.2.4 Flow System Data

If the problem being analyzed by MOTAR requires a pressure/flow analysis, the data needed to describe the flow system is input in the block headed by the title,

$ FLOW SYSTEMS

The input values in this block may be in any system of units, but the units must be consistent throughout both the thermal and fluid portions of the problem. In order to permit this, the user must supply the gravitational constant immediately following the heading as follows:

GC = 32.174

or GC = 3.2174E1 (For feet and seconds)

Table VII gives values of GC for various units of length and time. The $FLOW SYSTEMS block data is contained in the following subordinate blocks:

$ FLOW SYSTEMS

+ SYSTEM = 1 (KODE 1)
  'PARAMETER'
  'FLOW NETWORK'
  'SUBNETWORK = 1'
  ...
  ...
  ...
  'SUBNETWORK = NSN'
  'FLUID LUMP DATA'
  'PUMP'
  'VALVES'
+ SYSTEM = 2 (KODE 2)
  'PARAMETER'
  'FLOW NETWORK'
  'SUBNETWORK = 1'
  ...
  ...
  ...
  'SUBNETWORK = NSN'
  'FLUID LUMP DATA'
  'PUMP'
  'VALVES'
+ SYSTEM = 3
  ...
  ...
  etc.
TABLE VII  VALUE OF GC FOR VARIOUS PROBLEM UNITS

<table>
<thead>
<tr>
<th>UNITS</th>
<th>GC</th>
</tr>
</thead>
<tbody>
<tr>
<td></td>
<td></td>
</tr>
<tr>
<td>MASS</td>
<td>FORCE</td>
</tr>
<tr>
<td>LB</td>
<td>LBm</td>
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<tr>
<td>GRAM</td>
<td>dyne</td>
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<td></td>
<td></td>
</tr>
<tr>
<td>KILOGRAM</td>
<td>Newton</td>
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</tbody>
</table>
The $FLOW SYSTEM$ block may be omitted if no flow analysis is required.

A flow system is defined here as a single set of interconnected tubes which contain a fluid which can be described by a single set of properties. Any number of flow systems may be analyzed in the same problem but each required a separate set of data headed by the card

```
+ SYSTEM = SN (KODE)
```

Where SN = an integer describing the system number

KODE = a code indicating whether the system is one phase flow or two phase flow

The system number must be unique for each system but consecutive numbering isn't required. For the current version of MOTAR, the two phase flow capability is not included and thus, KODE is always a value of 1. Four subordinate blocks are always required for each system. These blocks, which are 'PARAMETERS', 'FLOW NETWORK', 'FLUID LUMP DATA', and 'PUMP' supply information which is always required to define a system. The 'VALVES' and the 'SUBNETWORK' blocks are included only when they supply additional information. The input required for each of the flow systems subordinate blocks is described below.

5.2.4.1 Parameters

The parameters block must be supplied for each flow system. This block is headed by the card

```
'PARAMETERS'
```

and contains the following information:

1. Specification of the following fluid properties:
   (a) thermal conductivity
   (b) density
   (c) viscosity
   (d) specific heat
2. The node number and pressure value of the reference pressure node.
3. Parameter values describing the characteristics for the pressure-flow solution.
4. When a numerical solution rather than the direct solution for the pressure equations desired, a solution tolerance is required. This also a key input indicating a numerical solution is desired.

The above items are input by supplying a variable name on the left of an equal and the specification of its value on the right. The following is a description of the variable names

**Fluid Properties**

KT : Fluid Thermal Conductivity
RO : Fluid Density
MU : Fluid Viscosity
CP : Specific Heat

The value for each of the fluid properties may be specified as a constant by supplying a real value or it may be specified as a temperature dependant curve by supplying the value as an integer. The integer value must be the curve number. For example, if all the values were constant they would be specified as,

\[
\text{KT} = 0.25 / \text{RO} = 67. / \text{MU} = 0.137 / \text{CP} = 0.31
\]

If instead, the thermal conductivity and viscosity were supplied by a temperature dependent curve, the values would be supplied by,

\[
\text{KT} = 32 / \text{RO} = 67. / \text{MU} = 42 / \text{CP} = 0.31
\]

These values must always be supplied for each system.

Reference Pressure Specification
The pressure at the pump inlet node for a closed system or for the system outlet for an open system must be specified. This is supplied in the following format:

\[
P(\text{NN}) = \text{VALUE}
\]

Where \( \text{NN} \) = an integer representing the pressure node number

\( \text{VALUE} \) = a real value representing the pressure value of the node

For example:

\[
P(10) = 14.7
\]

indicates pressure node number 10 is the reference pressure node number with a value of 14.7.

Pressure-Flow Solution Parameters
Four optional variables may be supplied by the user in the 'PROPERTIES' block to define certain characteristics of the solution. These are described below:

MPASS: An integer specifying the number of temperature iterations between balancing of the pressures and flow rate. It is set to one if not supplied.

MXPASS: The maximum number of tries to balance the pressures and flow rates for each iteration. Routine sets to 100 if it is not supplied.
TOL: The tolerance for terminating the pressure/flow balance. When the fraction of change of the flow rates in all the tubes is within TOL, the solution is reached. If TOL is not supplied, it is set to 0.001.

A: An averaging factor to help improve the convergence rate for flow systems that are very nonlinear - i.e., system with turbulent flow or head losses. It must be a value greater than 0.0 and less than 1.0. The averaging factor is applied to each tube flow rate following each pass through the pressure/flow balancing loop as follows:

\[ \dot{W}_{\text{new}} = A \dot{W}_{\text{new}} + (1.-A) \dot{W}_{\text{old}} \]

If A is not supplied, it is set to 0.7.

FLOW: The initial system total flow rate.

EPS: The tolerance for interactive solution of the pressure flow linear simultaneous equations.

Numerical Solution for Pressure Equations

For each pass through the pressure-flow balance loop on each temperature iteration, a set of linear simultaneous equations are set up for each subnetwork. If the variable EPS is not supplied in the properties data, the solution to these equations is obtained using the Gauss-Jordan Elimination procedure. If the variable EPS is supplied, the equations are solved using Gauss-Siedel iterative method. The solution is then terminated when the change in pressure from one Gauss-Siedel iteration to the next is within EPS for all pressure nodes in the subsystem.

5.2.4.2 Flow Network and Subnetworks

The pressure/flow network is described by the flow network blocks and its corresponding subnetwork blocks for each flow system. The flow model consists of the pressure nodes, the flow tubes connecting the nodes and the fluid temperature nodes in each tube. (See sections 3.2.1 and 5.1.2 for descriptions of networks, subnetworks and model building methods). For the current version of the routine, the system network consists only of the inlet tube, the outlet tube and any other tubes in series with the inlet and outlet. The remainder of the system is contained in the subnetworks. Each subnetwork contains a set of interconnected tubes and are separated by network tubes.

The input requirements for each tube are the same whether the tube is defined in the network or subnetwork. The input format is as follows for each tube:

\[ NT, NP1, NP2 = (NF1, NF2 \ldots NFN) \]
Where  NT = the tube number

NP1 = the pressure node on the upstream side of NT
NP2 = the pressure node on the downstream side of NT

NFL --- NFN = all the fluid temperature node numbers contained in tube NT. If the user desires to control the conductor in the programming blocks, a blank or zero can be input between the ( ).

The heading card for the network data is,

'FLOW NETWORK'

The heading card for the subnetwork data is,

'SUBNETWORK = NSN'
GIN = NG
NSPR = NN

Where  NSN = subnetwork number (must be unique)

NG = tube number for the tube carrying flow into the subnetwork

NN = the pressure node number at the subnetwork

5.2.4.3 Fluid Lump Data

The flow characteristics for each fluid temperature node contained in the system are supplied in the subordinate block headed by,

'FLUID LUMP DATA'

The following information is supplied for each fluid lump:

1. Fluid wetted perimeter
2. Fluid flow cross sectional area (perpendicular) to the direction of flow
3. Fluid lump length
4. Method for calculating friction factor
5. Number of velocity head losses
6. Friction factor coefficient

The input format for the fluid lump data is:

NFL = WP, CSA, FLL, FFM, NKL, FFC

Where  NFL = the fluid lump number (integer)
WP = the wetted perimeter for NFL (real)
CSA = the cross sectional area for NFL (real)
FLL = the fluid lump length for NFL (real)
FFM = the friction factor method (integer)
NKL = the number of head losses (integer or real)
FFC = the friction factor coefficient (real)

The following options are available for FFM, NKL and FFC:

- If FFM = 0 or not supplied, the friction factor is calculated internally for the full range of Reynolds numbers using equations 50, 51, and 52.

- If FFM ≠ 0, the friction factor is calculated internally for laminar flow using equation (50). FFM is then a curve number for a curve of friction factor VS Reynolds number which is interpolated at values of Reynolds numbers above 2000.

- If NKL = 0 or not supplied, the head loss is 0.0

- If NKL = a real constant, that is the value of the head loss

- If NKL = a non-zero integer, it is then a curve number of a curve of head losses VS Reynolds number

- If FFC = 0, or not supplied, FFC = 1.0

- If FFC = a non-zero real number, then FFC = the real number.

FFC is applied to the friction factor in equation (49).

Several group input options are available for specifying the fluid lump numbers, NFL, on the left of the equal. These include:

1. Random fluid lump numbers separated by commas:
   NFL1, NFL2, - - - NFLN=WP, CSA, FLL, FFM, NKL, FFC

2. A number of lumps separated by a constant increment:
   NFL1 THRU NFLn BY INC = WP, CSA, FLL, FFM - - -

   Where NFL1 is the starting fluid lump number of the group
   NFLn is the ending fluid lump number of the group
   INC is the increment between lump numbers. (If the increment is 1, the BY INC may be omitted)

3. Any combination of (1) and (2) above. This includes multiple inputs of option (2) separated by commas.
5.2.4.4 Pump Data

The total flow rate entering each flow system is specified in the pump data which is headed by the heading:

'PUMP'

This block must always be supplied for each system. Four options are available for specifying the entering flow rate in the 'PUMP' block. These are:

1. Constant entering flow rate
2. Entering flow rate a function of time
3. Flow rate a function of pump pressure rise as specified by a tabulated curve
4. Pump pressure rise a function of flow rate as specified by a polynomial curve

A description of the input for these options is given below.

OPTION 1 : Constant Entering Flow Rate

The input format is:

NT1, LNS, VALUE

Where
- NT1 - An integer specifying the first (entering) tube in the system
- LNS - An integer specifying the last (exiting) pressure node in the system
- VALUE - A real number specifying the value of the flow rate

OPTION 2 : Entering Flow Rate A Function of Time

The input format is:

NT1, LNS, NCURVE

Where
- NTL - An integer specifying the tube with entering flow
- LNS - An integer specifying the last (exiting) pressure node in the system
- NCURVE - An integer specifying a time dependent (Type 1) flow rate curve

OPTION 3 : Flow Rate A Function of System Pressure Rise Specified by Tabulated Curve

The input format is:

NT1, LNS, NCURVE
Where

\[ \text{NT1} = \text{An integer specifying the tube with entering flow} \]

\[ \text{LNS} = \text{An integer specifying the last (existing) pressure node in the system} \]

\[ \text{NCURVE} = \text{An integer specifying a curve number of a curve of flow rate vs pressure rise (Type 5 curve)} \]

**OPTION 4**: Pump Pressure Rise A Polynomial Function of Flow Rate

The input format is:

\[ \text{NT1}, \text{LNS}, \text{AO}, \text{A1}, \text{A2}, \text{A3}, \text{A4} \]

Where

\[ \text{NT1} = \text{An integer specifying the tube with entering flow} \]

\[ \text{LNS} = \text{An integer specifying the last (existing) pressure node in the system} \]

\[ \text{AO}, \text{A1}, \text{A2}, \text{A3}, \text{A4} = \text{Curve fit constants for describing the pump curve} \]

Using this option, the pump pressure rise is given by:

\[ \Delta P = A_0 + A_1 W + A_2 W^2 + A_3 W^3 + A_4 W^4 \]

Where \( W \) = the flow rate

5.2.4.5 **Valve Data**

The input data required for each valve in a system is supplied in the valve subordinate block headed by;

'VALVES'

Three types of valves are currently available to the user. These types are identified by the following numbers:

**Type 1** - Rate Limited Valve: The valve rate of movement is proportional to the sensed temperature error up to a maximum movement rate.

**Type 2** - Polynomial Valve: The valve steady state position is a polynomial curve fit of the sensed error. A time constant may be input if a time lag is desired.

**Type 3** - Switching Valve: The valve position is either the maximum position. On side one, the valve position is the maximum when the sensor temperature is above T1. Side two is the minimum when the sensor temperature drops below T2, side one position goes to the minimum and side two to the maximum.
Any of the above three types may be either one sided or two sided valves. Also, the set point may be either a constant value or a temperature lump number for Types 1 and 2. Thus, either types one or two may be used as (1) a single sided bypass valve for a cooling situation (radiator), (2) a single sided bypass valve for a heating situation (solar absorber for instance) or (3) a proportioning valve. Type 3 valves may be used as an on-off shut off valve, an off-on shut off valve, or a switching valve.

The general input format for each valve type consists of three integers on the left of an equal with 13 values on the right for rate limited, 17 values on the right for polynomial. and 11 values on the right for switching valves. The input values on the left are supplied in the following order:

1 - Valve Number: May be any unique integer number for identification.

2 - Valve Class Code: (See Section 3.2.1 and 3.2.3 for description of Class) Only Class 2 valves are available for the current routine configuration. Thus, the valve class must be the integer 2.

3 - Valve Type: 1 for bypass valve, 2 for polynomial valve, 3 for switching valve.

The input values on the right are described below for each of the three valve types.

**Bypass Valve**

The list of variables on the right of the equal must be supplied in the following order:

1 - **Entering Tube Number**: The tube number of the tube supplying the flow to the valve.

2 - **Exiting Tube Number On Side 1**: The tube number of the tube leaving the valve on the side to be opened when the sensed temperature error becomes positive. If the valve is one sided and the characteristics of side 2 is desired (for instance, for a solar absorber bypass) this variable should be input as 0.

3 - **Exiting Tube Number on Side 2**: The tube number of the tube leaving the valve on the side to be opened when the sensed temperature error becomes negative. If the valve is one sided and the characteristics of the side 1 is desired (for instance, a radiator bypass) this variable should be set to 0.
4 - Initial Valve Position For Side One, X1 : (Should be between X1max and X1min.) The side 2 initial position is (1.0 - X1).

5 - Valve Operating Mode: If = 1, the valve operates normally if = 0, the valve does not operate but remains in its initial input position, X1.

6 - Minimum Position for Side One, X1min : Must be greater than 0.0. The maximum position for side 2 will be calculated by X2max = (1.0 - X1min). X1min must be less than X1max.

7 - Maximum Position for Side One, X1max : Must be less than 1.0 and greater than X1min. The minimum value for side 2 will be calculated by (1.0 - X1max).

8 - Sensor Lump For Side One or Set Point For Side 2 : If this variable is input as an integer it identifies the side one sensor lump to be controlled to (a) the set point or (b) sensor lump supplied for side 2 (next input). If this variable is input as a real number, it represents a set point to which the side 2 sensor lump will be controlled.

9 - Sensor Lump For Side 2 or Set Point For Side 1 : If this variable is input as an integer it identifies the side two sensor lump to be controlled to (a) the set point or (b) sensor lump temperature on side one (previous input). If this variable is a real number it represents a set point to which side 1 sensor lump will be controlled.

10 - Dead Band: The dead band as defined in Section 3.2.3.1 and Figure 4.

11 - Rate Factor: The valve rate factor as defined by Figure 4 and Section 3.2.3.1.

12 - Rate Limit : The valve rate limit as define by Figure 4 and Section 3.2.3.1.

13 - Geometric Factor : (For a valve class code of 2 only) The value of the variable E where ΔP valve = E (W 2/x^2) (See section 3.2.3.2)
Polynomial Valve

The list of variables to the right of the equal must be supplied in the following order:

1 - **Entering Tube Number**: The tube number of the tube supplying the flow to the valve.

2 - **Exiting Tube Number on Side 1**: The tube number of the tube leaving the valve on the side to be opened when the sensed temperature error becomes positive. If the valve is one sided and the characteristics of side 2 is desired (for instance, for a solar absorber bypass) this variable should be input as 0.

3 - **Exiting Tube Number on Side 2**: The tube number of the tube leaving the valve on the side to be opened when the sensed temperature error becomes negative. If the valve is one sided and the characteristics of the side 1 is desired (for instance, a radiator bypass) this variable should be set to 0.

4 - **Initial Valve Position For Side One, X1**: (Should be between \(X_{1\text{max}}\) and \(X_{1\text{min}}\).) The side 2 initial position is \((1.0 - X1)\).

5 - **Valve Operating Mode**: If = 1, the valve operates normally; if = 0, the valve does not operate but remains in its initial input position, \(X1\).

6 - **Minimum Position for Side One, X1min**: Must be greater than 0.0. The maximum position for side 2 will be calculated by \(X_{2\text{max}} = (1.0 - X_{1\text{min}})\). \(X_{1\text{min}}\) must be less than \(X_{1\text{max}}\).

7 - **Maximum Position for Side One, X1max**: Must be less than 1.0 and greater than \(X_{1\text{min}}\). The minimum value for side 2 will be calculated by \((1.0 - X_{1\text{max}})\).

8 - **Sensor Lump For Side One or Set Point For Side 2**: If this variable is input as an integer it identifies the side one sensor lump to be controlled to (a) the set point or (b) sensor lump supplied for side 2 (next input). If this variable is input as a real number, it represents a set point to which the side 2 sensor lump will be controlled.
9 - Sensor Lump For Side 2 or Set Point For Side 1: If this variable is input as an integer it identifies the side two sensor lump to be controlled to (a) the set point or (b) sensor lump temperature on side one (previous input). If this variable is a real number it represents a set point to which side 1 sensor lump will be controlled.

10 thru 15 - Polynomial Curve Fit Constants \( A_0, A_1, A_2, A_3, A_4, A_5, \): The steady state valve position on side one is given by (See Section 3.2.3.1)

\[
X_{1\text{ss}} = A_0 + A_1 \Delta T + A_2 (\Delta T)^2 + A_3 (\Delta T)^3 + A_4 (\Delta T)^4 + A_5 (\Delta T)^5
\]

16 - Valve Time Constant: The polynomial valve time constant as described in Section 3.2.3.1. If a valve is desired with no time lag, a time constant which is small compared to the problem time increment should be input (Must be greater than zero)

17 - Geometric Factor: (For a class code of 2 only) The value of the variable \( E \) where

\[
\Delta P_{\text{valve}} = E \frac{W^2}{X^2}
\]

See Section 3.2.3.2

Switching Valve

The list of variables to the right of the equal must be supplied in the following order:

1 - Entering Tube Number: The tube number of the tube supplying the flow to the valve.

2 - Exiting Tube Number On Side 1: The tube number of the tube leaving the valve on the side to be opened when the sensed temperature error becomes positive. If the valve is one sided and the characteristics of side 2 is desired (for instance, for a solar absorber bypass) this variable should be input as 0.

3 - Exiting Tube Number On Side 2: The tube number of the tube leaving the valve on the side to be opened when the sensed temperature error becomes negative. If the valve is one sided and the characteristics of the side 1 is desired (for instance, a radiator bypass) this variable should be set to 0.
4 - **Initial Valve Position For Side One, X1**: (Should be between X1max and X1min.) The side 2 initial position is (1.0 - X1).

5 - **Valve Operating Mode**: If = 1, the valve operates normally. If = 0, the valve does not operate but remains in its initial input position, X1.

6 - **Minimum Position for Side One, X1min**: Must be greater than 0.0. The maximum position for side 2 will be calculated by X2max = (1.0 - X1min). X1min must be less than X1max.

7 - **Maximum Position for Side One, X1max**: Must be less than 1.0 and greater than X1min. The minimum value for side 2 will be calculated by (1.0 - X1max)

8 - **Valve sensor lump**

9 - **T1, Side 1 off temperature, Side 2 on temperature**.

10 - **T2, Side 1 on temperature, Side 2 off temperature**.

11 - **Geometric Factor**: (For a valve class code 2 only) The valve of the variable E where

\[
\Delta P_{\text{valve}} = E \frac{w^2}{\chi^2}
\]

See Section 3.2.3.2
5.2.5 Curve Data

The tabulated curves and tables required by the input data blocks and user subroutines are supplied in the data block headed by:

$ CURVES

Curves may be supplied in any order in this block. Curves are identified by a curve number which contains within it a code identifying its independent variable. The last digit of each curve number is used to identify the curve type, and thus, a curve number must contain at least two digits.

The following types of curves are currently available.

<table>
<thead>
<tr>
<th>Curve Type</th>
<th>Description</th>
</tr>
</thead>
<tbody>
<tr>
<td>0</td>
<td>Any array of numbers real or integers which the user may need for the programming blocks or user subroutine.</td>
</tr>
<tr>
<td>1</td>
<td>A doublet array with time as the independent variable.</td>
</tr>
<tr>
<td>2</td>
<td>A doublet array with temperature as the independent variable.</td>
</tr>
<tr>
<td>3</td>
<td>A doublet array with flow rate as the independent variable.</td>
</tr>
<tr>
<td>4</td>
<td>A doublet array with Reynolds number as the independent variable.</td>
</tr>
<tr>
<td>5</td>
<td>A doublet array with pressure drop as the independent variable.</td>
</tr>
</tbody>
</table>

With these codes, the curve numbers 10, 20, 30, 100, 1000, etc., are simple arrays for the user programming. The curve numbers 11, 21, 31, 41, 101, 151, etc., are used to specify time dependent tabulated functions which are referred to in the $ NETWORK DATA or $ FLOW SYSTEMS blocks. The numbers 12, 22, 32 are temperature dependent curves, 13, 23, 33 are flow rate dependent curves, etc.

The input format for the curves consists of (1) supplying the integer curve number and (2) supplying the curve values starting on the card following that with the curve number. The curve values are input for field separated by commas. If more than one card is required to supply the curve values, a continuation code (any non-zero character) must be supplied in column 75 for each additional card added.
A user may set up any number of locations in a curve for storing data by supplying an S followed by the number of spaces desired. For instance the entry

10/S, 1000

would set up curve number 10 with 1000 blank spaces. This option may be used anywhere within a curve. For instance,

20/ 1., 3., S, 500, 2.0

would set up a curve with 1., 3., 500 blank spaces and 2.0. The user should not specify zero values for the S option.
5.2.6 User Programming Blocks

5.2.6.1 General Description

Four input blocks are available to the user for supplying problem logic and calling on available user subroutines. In these blocks the user may perform logical operations on the temperature network elements and, to a lesser extent, on the pressure network elements. The user also has access to the time parameters of the problem, the curves and 75 constant locations which may be used either as real numbers or integers.

The four blocks differ only in their heading title and the point in the problem sequencing where the logic of the block is called upon. The block titles are given below with a description of their location in the problem sequence.

<table>
<thead>
<tr>
<th>BLOCK TITLE</th>
<th>SEQUENCING</th>
</tr>
</thead>
<tbody>
<tr>
<td>$ CENTRAL</td>
<td>Logical operations performed only one time for the problem. Specifies the call to the temperature solution subroutine and any user calls preceding and following it.</td>
</tr>
<tr>
<td>$ PRETEMP</td>
<td>Logical operations performed prior to the temperature calculations on each iteration.</td>
</tr>
<tr>
<td>$ POSTTEMP</td>
<td>Logical operations performed following the temperature calculations and prior to the pressure/Flow calculations on each iteration.</td>
</tr>
<tr>
<td>$ OUTPUT</td>
<td>Logical operations to be performed on the print internal, WINC.</td>
</tr>
</tbody>
</table>

The location of the four user supplied logic blocks in relation to the overall problem flow is shown in Figure 9.

The input format for the user programming blocks is simply the FORTRAN V Computer programming language and thus, valid FORTRAN V statements may be used. The first 5 columns are reserved for statements numbers or a C in column 1 for comments. The * for comments cannot be used in the programming blocks. Per the FORTRAN language, the statements occur in columns 7 thru 72. Column 6 is used for continuation. User supplied statements for each block are combined with computer generated common and equivalence statements to form the following subroutines:

<table>
<thead>
<tr>
<th>PROGRAMMING BLOCK</th>
<th>SUBROUTINE</th>
</tr>
</thead>
<tbody>
<tr>
<td>CENTRAL</td>
<td>STEP 2</td>
</tr>
<tr>
<td>PRETEMP</td>
<td>PRETMP</td>
</tr>
<tr>
<td>POSTTEMP</td>
<td>POSTMP</td>
</tr>
<tr>
<td>OUTPUT</td>
<td>OUTPUT</td>
</tr>
</tbody>
</table>
XOT STEP 2

CENTRAL

USER SUPPLIED
LOGIC PRIOR TO
SOLUTION

CALL TO TEMP
SOLUTION (USER
SUPPLIED)

USER SUPPLIED
LOGIC FOLLOWING
SOLUTION

END

EXPLCIT OR
IMPLCIT

CALL PRETEMP

CALCULATE
NETWORK ELEMENTS

CALCULATE
TEMPS

TIME = TIME + DTIME

CALL POSTTEMP

CALL PFCS

PERFORM USER
LOGIC SUPPLIED IN PRETEMP

PERFORM USER
LOGIC SUPPLIED IN POSTTEMP

PERFORM FLOW BALANCE

CALL OUTPUT

PERFORM USER LOGIC
SUPPLIED IN OUTPUT

IF PRINT
INT

YES

CALL OUTPUT

PERFORM USER LOGIC
SUPPLIED IN OUTPUT

NO

IF TIME > STIME

OR ETIME > RTIME

ERROR

NO

YES

RETURN

FIGURE 9 - OVERALL STEP 2 FLOW FOR MOTAR
The user has access to a number of problem variables in each of the programming blocks. These variables are in labeled common for each of the blocks and thus a change in one block to the problem variables is communicated to all the other blocks and to the problems. Variables available include the temperature network elements, pressure network elements, problem time related variables, and user constants which may be used as integers or real numbers.

A list and description for the variables which may be referenced in any of the user programming blocks is given below:

<table>
<thead>
<tr>
<th>VARIABLE</th>
<th>DESCRIPTION</th>
</tr>
</thead>
<tbody>
<tr>
<td>T(I)</td>
<td>Temperature of temperature Node I</td>
</tr>
<tr>
<td>C(I)</td>
<td>Capacitance of temperature Node I</td>
</tr>
<tr>
<td>Q(I)</td>
<td>Heat Source for temperature Node I</td>
</tr>
<tr>
<td>U(I)</td>
<td>Conductance for conductor I</td>
</tr>
<tr>
<td>W(I)</td>
<td>Flow Rate for tube I</td>
</tr>
<tr>
<td>PR(I)</td>
<td>Pressure for pressure node I</td>
</tr>
<tr>
<td>G(I)</td>
<td>Pressure conductance for tube I</td>
</tr>
<tr>
<td>CURV(I)</td>
<td>Array contain all curve data</td>
</tr>
<tr>
<td>TIME</td>
<td>Problem time</td>
</tr>
<tr>
<td>STIME</td>
<td>Problem stop time</td>
</tr>
<tr>
<td>RTIME</td>
<td>Requested computer time (minutes)</td>
</tr>
<tr>
<td>WINC</td>
<td>Print interval</td>
</tr>
<tr>
<td>PINC</td>
<td>Plot interval for automatic plotting</td>
</tr>
<tr>
<td>CI or KI</td>
<td>Seventy-five (75) user variables which are communicated between the user subroutines. If used as a real number use the name CI. When used as an integer use the name KI. (CI and KI are equilvalenced)</td>
</tr>
<tr>
<td>C75 or K75</td>
<td></td>
</tr>
</tbody>
</table>

Any curve in the $ CURVES data may be addressed in any of the user blocks by use of the function LUTAB(I) where I is the curve number. The curve values are then obtained by addressing the array CURVE (J) where J = LUTAB(I). For example, if the fourth value of curve number 20 is desired, we would find it with the following two FORTRAN cards:
J = LUTAB (20)

C1 = CURV (J+4)

C1 will be assigned the values of the fourth location of curve number 20. This is the third data value, however, because the first location of each doublet table contains the number of points on the curve and the first location of a type zero curve contains the number of values. One must be careful when obtaining an integer value from a curve. Real variables should always be used when addressing curve since CURVE is real. However, the addressing variable, such as C1 above should be equivalenced to an integer variable name for use as an integer. If the fourth value of curve 20 were an integer in the example above, the variable name K1 would be used following the two statements since C1 and K1 are equivalenced.

The user may address the thermal network elements by addressing the arrays T, C, Q and U. The subscripts of T, C, and Q are the node numbers and the subscript of U is the conductor number. The $ PRETEMP block is located such that a definition by the user for any of the above variables overrides the computer definition prior to an iteration. A definition of these variables in any of the other blocks will be overridden by computer calculations however, except for (1) boundary temperatures, (2) constant capacitances and, (3) constant conductances. The Q values are set to zero prior to each iteration and thus a definition of Q in any block except $ PRETEMP or by the + ABSORBED HEAT block will be lost. The values of Q supplied in $ PRETEMP will be added to values calculated by options in + ABSORBED HEAT.

The user has limited access to three elements of the flow network in the programming blocks. Available are overall tube conductance G(I), tube flow rate, W(I), and node pressure PR(I). Only the value of G(I) may be controlled by the user and this may be performed only if the tube lump number supplied for the tube is zero (with only one tube lump). Then the user must specify the value of the conductance. The call to the operations of the $ POSTTMP block has been placed immediately prior to the call to PFCS, the pressure flow analysis subroutine, so that the user may modify the G's as desired. The other variables, PR and W may be used for sensing purposes or independent variables only.

5.2.6.2 User Subroutines

Numerous subroutines have been developed and assembled in MOTAR for direct application by the user in the User Programming blocks. These subroutines greatly extend the MOTAR capability giving the user immediate access to numerous temperature solution subroutines, application subroutines, mathematical analysis and solution subroutines, interpolation subroutines, Matrix analysis subroutines, and output subroutines. A large number of these subroutines were taken directly from the SINDA computer routine14,15. This includes most of the mathematical analysis and solution subroutines, interpolation subroutines, and Matrix analysis subroutines. All of the temperature solution subroutines, many of the application sub-
routines (enclosure radiation, cabin analysis, heat exchangers, inline heaters, etc.) and some of the output subroutines were conceived during MOTAR development. A brief description of the available user subroutines is given below for each category of subroutines. A detailed description of all the subroutines is given in Appendix A.

Temperature Solution Subroutines

Temperature solution subroutines are generated by the computer during the pre-processing phase based upon the requirements of the input data. If the $CENTRAL block is not included in the input (ie, no logic in this block) the computer will also generate a call to the appropriate transient temperature solution subroutine depending on the MPLCT code in columns 6 to 10 on parameter card 1. (If the code is 0, EXPLCT will be called, if 1, IMPLCT will be called). This call will be located in the processing phase main routine, STEP 2. If any logic appears in the $CENTRAL block, the user must supply the call to the temperature solution subroutine in $CENTRAL.

There are four potential temperature solution subroutines that may be specified by the user. The subroutines will actually be different from problem to problem since they are generated depending on the problem content. The temperature solution subroutines are:

1. EXPLCT - Performs the transient solution using the explicit method (two time increment options are available)

2. EXPSS - Performs the steady state solution for data stored in the explicit format

3. IMPLCT - Performs transient solution using the implicit method

4. IMPSS - Performs the steady state solution for data stored in the implicit format

EXPLCT and/or EXPSS must be used when the MPLCT code on parameter card 1 is a value of 0. IMPLCT and/or IMPSS routines must be used when the MPLCT code is 1. If the MPLCT code and the subroutine calls are inconsistent, the called subroutine will not be found and the problem will not be run.

The user may perform any number of calls to the transient or steady state subroutines or calls to both may exist in the same problem. For example, suppose a user desired to perform a parametric run in which the steady state solution is desired at TIME = 0. and a transient solution is desired starting at that condition for five different values of temperature for node ten. The logic in $CENTRAL when using explicit method of solution would be:
If using the implicit method of solution the calls would be

$ CENTRAL

DO 20 I = 1,5
TIME = 0.
CALL IMPSS
CALL IMPLCT
20 T(10) = T(10) + 25.

With this type of programming a large number of problems may be performed with a single run.

A more detailed description of the temperature solution subroutines is given in Appendix A .

Application Subroutines

Several subroutines are available to the user which provide capabilities for specific applications. These are listed below and described in detail in Appendix A.

RADIR - Calculates the script-F values for IR radiation within an enclosure and uses these values to obtain the heat transfer during the problem. Permits consolidation of several temperature nodes on a single surface.

RADSOL - Calculates the script F values for radiation from an extended source entering an enclosure and uses these values to obtain heat transfer during the problem. Permits consolidation of several temperature nodes on a single surface.

IRRADI
IRRARDE - Calculated the script-F values for IR radiation within an enclosure and uses these values to obtain the heat transfer during the problem.
SLRAD1 - Calculates the script-F values for radiation from an entering source external to the enclosure and uses these values to determine heat transfer during the problem.

EFFEMS - Calculates the script-F between parallel flat plates.

SCRFFA - Calculates the script-F values for infrared radiation within an enclosure.

HXEFF, HXCNF, HXCROS, HXPAR - Simulate heat exchanger performance under steady state conditions - Can be used to approximate transient conditions.

HTRINL - Simulates a fluid inline heater.

CABIN - Performs a heat and mass balance on a cabin gas considering any number of entering streams and condensation on the cabin wall.

ABLATS - Represents a simple ablation (sublimation) capability

LQSLTR - Accounts for the phase change energy of a melting or solidifying material

LQDVAP - Allows the user to simulate the addition of liquid to a node

Matrix Analysis Subroutines

Numerous Matrix subroutines are available to the user for performing computations and manipulation on matrices of numbers. The matrices are stored in the $ CURVES block and must be in the proper format. For subroutines assuming rectangular matrices this format consists of (1) an integer specifying the number of rows in the first array data value, (2) an integer specifying the number of columns in the second array data value and (3) the Matrix values in row order. For subroutines designed specifically for symmetric matrices the matrices are assumed to be stored in row order with each row starting with the diagonal value. The first value contains the size of the square Matrix and the second value isn't used. The format is,

\[
NC, N, BLANK, A(1,1)A(1,2), A(1,3) - - - - A(1,N) \\
A(2,2), A(2,3) - - - - A(2,N) \\
\vdots \\
A(N,N)
\]

A list of the matrix analysis subroutines available is given below. A detailed description of their use is given in Appendix A.

a) Special Matrix Generation

ZERO - Generates a matrix such that every element is zero

ONES - Generates a matrix such that every element is one.
UNITY Generates a square matrix such that the principal diagonal elements are unity and the remaining elements are zero.

SIGMA Generates a square matrix such that all elements on and below the principal diagonal are unity and the remaining elements are zero.

GENALP Generates a matrix such that every element is equal to a constant

GENCOL Generates a column matrix such that the first element is equal to X1 and the last element is equal to X2

FULSYM Forms a half symmetric matrix from a full square matrix

SYMFUL Forms a full square matrix from a half symmetric matrix

SYMFRC Forces symmetry upon a square matrix

DIAG Forms a full square matrix given a column or row matrix

UNDIAG Forms a row matrix from the diagonal elements of a square matrix

DIAGAD Adds the elements of a row matrix to the diagonal elements of a square matrix

b) Elemental Operations

ELEADD Adds corresponding elements of two matrices A and B to form a third Z (Matrix addition)

ELESUB Subtracts the corresponding elements of two matrices to form a third Z (Matrix subtraction)

ELEMUL Multiplies the corresponding elements of two matrices A and B to form a third Z

ELEDIV Divides the corresponding elements of two A and B matrices to form a third Z

ELEINV Obtains the reciprocal of each element of matrix A and places it in the corresponding location of another matrix Z

EFSIN Generates the sine of each elements of matrix A and places it in the corresponding location of another matrix Z

EFASN Generates the arcsine of each element of matrix A and places it in the corresponding location of another matrix Z

EFCOS Generates the cosine of each element of matrix A and places it in the corresponding location of another matrix Z
EFACS Generates the arccosine of each element of matrix (A) and places it in the corresponding location of another matrix (Z).

EFTAN Generates the tangent of each element of matrix (A) and places it in the corresponding location of another matrix (Z).

EFATN Generates the arctangent of each element of matrix (A) and places it in the corresponding location of another matrix (Z).

EFABS Generates the absolute value of each matrix (A) element.

EFLOG Generates the natural log of each (A) element.

EFSQR Generates the square root of each matrix (A) element.

EFEXP Generates the exponential of each matrix (A) element.

EFPOW Generates the power of each matrix (A) element.

ADDA LP Adds a constant to every element in a matrix.

ALPHAA Multiplies every element in a matrix by a constant.

MATRIX Allows a constant to replace a specific matrix element.

SCALAR Allows a specific matrix element to be placed into a constant location.

MATADD Adds a constant to a specific matrix element.

c) Matrix Operations/Solutions

INVRSE Inverts a square matrix.

MULT Multiplies two conformable matrices.

TRANS Forms the transpose (Z) from matrix (A).

AABB Sums two scaled matrices.

BTAB Performs the matrix operation \( (B)^t (A)(B) \).

BABT Performs the matrix operation \( (B)(A)(B)^t \).

DISAS Allows a user to operate on matrices in a partitioned manner by disassembling a submatrix (Z) from a parent matrix (A).

ASSM BL Allows a user to operate on matrices in a partitioned manner by assembling a submatrix (Z) into a parent matrix (A).
COLMLT
Multiplies each element in a column or row of matrix \( (A) \) by its corresponding element from the diagonal matrix \( (V) \) which is stored as a vector.

ROWMLT

SHIFT
Moves an entire matrix as is from one location to another.

REFLCT
Moves an entire matrix with the order of the column elements reversed from one location to another.

SHUFL
Allows the user to reorder the size of a matrix as long as the total number of elements remains unchanged.

COLMAX
Searches an input matrix to obtain the maximum or minimum values within each column.

COLMIN

SYMREM
Allows the SINDA user to operate on a simple row/column of a half symmetric matrix.

SYMREP

SYMDAD
Adds the elements of a vector array to the corresponding elements of the main diagonal of a half symmetric matrix.

SYMINV
Obtains the inverse of a half symmetric matrix.

POLMLT
Multiplies a given number of nth order polynomial coefficients by a similar number of mth order polynomial coefficients.

POLVAL
Evaluates the polynomial for the input complex number \( X + iY \), given a set of polynomial coefficients.

PLYEVL
Evaluates each polynomial for each \( X \) value, given a matrix with nth order polynomial coefficients and a column matrix of \( X \) values.

POLSOV
Calculates the complex roots, given a set of polynomial coefficients as the first row in a matrix.

JACOBI
Determines the eigenvalues and eigenvector associated with an input matrix \( (A) \).

d) Store and Recall

CALL
Retrieves matrices on magnetic tapes.

FILE
Stores matrices on magnetic tapes.

ENDMOP
Used in conjunction with subroutines CALL and FILE. Causes all matrices from the logical 19 tape to be updated onto the logical 18 tape.
LSTAPE Will output the name, problem number and size of every matrix stored on tape on logical 18.

e) Applications

MODES Solves a particular matrix dynamic vibration equation

MASS Generates an inertia matrix of a dynamic vibration system described in terms of deflections and rotations

STIFF Generates a stiffness matrix for a dynamic vibration system described in terms of deflections and rotations.

Interpolation Subroutines

Numerous interpolation subroutines are available to the user. Included are the capability for (a) linear interpolation of function one, two and three independent variables (b) parabolic interpolation of functions of one or two variables, and (c) lagrangian interpolations up to 50th order for one independent variable including extrapolation. Also included are options to take advantage of cyclic curves, point/slope interpolation and linear extrapolation options.

A summary of the interpolation subroutines is given below. They are discussed in detail in Appendix A.

a) Lagrangian Interpolation

LAGRAN Uses one doublet array. Performs interpolation for order up to 50.

LGRNDA Uses two singlet arrays. Performs interpolation for order up to 50.

b) Linear Interpolation - Single Variable

POL Used one doubled array - one format

D1DEG1 Uses one doublet array - another format

D1D1DA Uses two singlet arrays

D1D1WM Uses D1DEG1 and multiplies the interpolation by the Z value

D1MDA Uses D1D1DA and multiplies the interpolation by the Z value

D1MDG1 Uses the arithmetic mean of two input values as the independent variable; uses a doublet array

D1M1DA Same as D1MDG1 except two singlet arrays are used

D1M1WM Uses D1MDG1 and multiplies the interpolation by the Z value
D1MD1M Uses D1MDA and multiplies the interpolation by the Z value
D1DG11
D1D11M
D1D1M
D11DAL
D11D1M
D11MD1
D11MD1
D11M1M

Performs interpolation on an array of X's to obtain an array of Y's

Identical to D1DG11, D1D11M and D1D1M, except for the use of singlet arrays and call on D1D1DA

These are indexed subroutines which use the arithmetic mean of two input values as the independent variable

c) Linear Interpolation - Two Single Variables

CVQ1HT
CVQ1WM

Performs two single variable linear interpolations

d) Parabolic Interpolation - Single Variable

D1DEG2
D1D2DA
D1D2WM
D12MDA
D1MDG2
D1M2DA
D1M2WM
D1M2MD

Uses LAGRAN and a doublet array
Uses LGRNDA and two singlet arrays
Uses LAGRAN and multiplies the interpolation by the Z value
Uses LGRNDA and multiplies the interpolation by the Z value
Uses the arithmetic mean of two input values as independent variable; uses doublet array
Same as a D1MDG2 except two single arrays are used
Uses D1MDG2 and multiplies the interpolation by the Z Value
Uses D1M2DA and multiplies the interpolation by the Z value

e) Cyclical Interpolation Arrays

D11CYL
DA11CY
D12CYL
DA12CY
D11MCY
DA11MC
DA12CY
DA12MC

Reduces core storage requirements and uses linear interpolation
Identical to D11CYL and DA11CY except that parabolic interpolation is used
Identical to D12CYL and DA12CY except that the interpolation is multiplied by the value in address Z
Identical to D11MCY and DA11MC except that parabolic interpolation is used
f) Point Slope Interpolations

GSLOPE Generates a slope array so that point slope interpolation can be used.

PSINTR, PSNTWM Point slope interpolation

g) Bivariate Interpolations

BVSPSA BVSPDA Uses an input Y argument to address a bivariate array.

BVTRNI BVTRN2 Constructs a bivariate array of Y's versus X and Z from an input array of Z's versus X and Y.

D2DEG1 Performs bivariate linear interpolation.

D2DEG2 Performs bivariate parabolic interpolation.

D2D1WM Uses D2DEG1 and multiplies the interpolation by the W value.

D2D2WM Uses D2DEG2 and multiplies the interpolation by the W value.

D2MXD1 Identical to D2DEG1 and D2DEG2 except that the arithmetic mean of two X values is used as the X independent variable.

D2MXD2 Identical to D2DEG1 and D2DEG2 except that the arithmetic mean of two X values is used as the X independent variable.

h) Trivariate Interpolations

D3DEG1 D3D1WM Performs trivariate linear interpolation.

i) Linear Extrapolation

ITRATE Linearly extrapolates a new guess on the basis of Zero error.

Output Subroutines

A number of subroutines are available to the user which permit the generation of printed, plotted or tape output for various situations in addition to the standard printing and plotting options. These subroutine provide the capability for printing individual values arrays and matrices; for plotting; and for writing and reading from magnetic tapes. The available subroutines are summarized below and described in detail in Appendix.
a) **Network Printout**

<table>
<thead>
<tr>
<th>Command</th>
<th>Description</th>
</tr>
</thead>
<tbody>
<tr>
<td>TPRNT</td>
<td>Prints thermal node temperature</td>
</tr>
<tr>
<td>CPRNT</td>
<td>Prints thermal capacitances</td>
</tr>
<tr>
<td>QPRNT</td>
<td>Prints the nodal heat flow values</td>
</tr>
<tr>
<td>UPRNT</td>
<td>Prints thermal conductances</td>
</tr>
<tr>
<td>DTPRNT</td>
<td>Prints the time increments</td>
</tr>
<tr>
<td>COPRNT</td>
<td>Prints the thermal network capacitances, heat flow values,</td>
</tr>
<tr>
<td></td>
<td>time increment and the conductances</td>
</tr>
<tr>
<td>WPRNT</td>
<td>Prints flow rates</td>
</tr>
<tr>
<td>PPRNT</td>
<td>Prints pressures</td>
</tr>
<tr>
<td>VPRNT</td>
<td>Prints valve positions</td>
</tr>
</tbody>
</table>

b) **Floating Point**

<table>
<thead>
<tr>
<th>Command</th>
<th>Description</th>
</tr>
</thead>
<tbody>
<tr>
<td>PRINT</td>
<td>Allows individual floating point numbers to be printed for reference</td>
</tr>
<tr>
<td>PRINTL</td>
<td>temperature, capacitance, etc.</td>
</tr>
</tbody>
</table>

c) **Array Printout**

<table>
<thead>
<tr>
<th>Command</th>
<th>Description</th>
</tr>
</thead>
<tbody>
<tr>
<td>GENOUT</td>
<td>Allows the output of any array of integers, floating point, or both</td>
</tr>
<tr>
<td>GENI</td>
<td>Prints out an array of integer</td>
</tr>
<tr>
<td>GENR</td>
<td>Prints out an array of real numbers</td>
</tr>
<tr>
<td>PRINTA</td>
<td>Allows the user to printout an array of values five to the line</td>
</tr>
<tr>
<td>PRNTMA</td>
<td>Allows the user to print up to 10 arrays in a column format</td>
</tr>
<tr>
<td>PUNCHI</td>
<td>Enables a user to punch out an array of data values in any desired format</td>
</tr>
</tbody>
</table>

d) **Plot Package**

<table>
<thead>
<tr>
<th>Command</th>
<th>Description</th>
</tr>
</thead>
<tbody>
<tr>
<td>PRNPLT</td>
<td>Prints out a plot on the line printer</td>
</tr>
<tr>
<td>PLOTX1</td>
<td>Call upon a large package of subroutines specifically for the SC-4060</td>
</tr>
<tr>
<td>PLOTX2</td>
<td></td>
</tr>
<tr>
<td>PLOTX3</td>
<td></td>
</tr>
<tr>
<td>PLOTX4</td>
<td></td>
</tr>
</tbody>
</table>

e) **Tape Input/Output**

<table>
<thead>
<tr>
<th>Command</th>
<th>Description</th>
</tr>
</thead>
<tbody>
<tr>
<td>READ</td>
<td>Enables the user to read and write arrays of data as binary information</td>
</tr>
<tr>
<td>WRITE</td>
<td>on magnetic tape</td>
</tr>
</tbody>
</table>
f) Matrix Output

LIST: Prints the elements of a matrix and identifies each by its row and column number.

PUNCH: Punches out a matrix, size n*n, one column at a time in any desired format.

SYMLST: Prints out and identifies the element values of a half symmetric matrix.

9) Special

PNTABL: Provides output information for users of subroutine ABLATS.
Mathematical Subroutines

Several user subroutines are provided for mathematical operations and solutions. Capabilities provided the user include integration, root determination of cubic and quartic equations, polynomial calculation, simultaneous equation solution, least squares curve fit, and complex number calculations. These subroutines are summarized below.

a) Area Integration

SMPINT  Performs area integration by Simpson’s rule and trapezoidal rule using equal increments
TRPZD    Performs area integration by the trapezoidal rule with non-uniform increments

b) Roots

NEWTRT   Utilizes Newton's method to obtain one root of a cubic or quartic equation
NEWRT4

(c) Polynomial/Simultaneous Linear Equations

PLYNML   Calculates the value of the dependent variable for an Nth order polynomial
PLYARY   PLYAWM
SIMEQN   Solves a set of linear equations (10 or less) by the factorized inverse method

(d) Curve Fit/Temperature Derivative

LSTSQU   Performs a least squares curve fit to an arbitrary number of X, Y pairs to yield a polynomial equation of up to order 10

Complex Variable Subroutines

a) Multiplication Operation

CMPXMP   Multiplies two complex numbers or the corresponding elements of arrays of complex numbers
CMPYI

b) Division Operation

CMPPXDV  Divides two complex numbers or the corresponding elements of complex numbers
CDIVI

c) Roots

CMPXSR   Obtains the complex square root of a complex number or array of complex numbers
CSQRI
Array Data Handling Subroutines

The capability of the MOTAR user to manipulate data stored in the $CURVES$ data is enhanced by use of numerous array data manipulation subroutines. The subroutines available are listed below and described in detail in Appendix A.

(a) Addition Operation

ADDARY Adds the corresponding elements of two specified length arrays to form a third array

ARYADD Adds a constant value to every element in an array to form new array

SUMARY Sums an array of floating point values

(b) Subtraction Operation

SUBARY Subtracts the corresponding elements of one array from another to form a third array

ARYSUB Subtracts a constant value from every element in an array to form a new array

(c) Multiplication Operation

MPYARY Multiplies the corresponding elements of two arrays to form a third array

ARYMPY Multiplies each element of an array by a constant value to form a new array

SCLDEP Multiplies the dependent or independent variables of a doublet type interpolation array

SCLIND

(d) Division Operation

DIVARY Divides the elements of one array into the corresponding elements of another array to produce a third array

ARYDIV Divides each element of an array by a constant value to produce a new array

ARYINV Inverts each element of an array in its own location

ARINDV Divides each element of an array into a constant value to form a new array

ADARIN Calculates one over the sum of inverses of an array of values

(e) Distribution of Array Data

SHFTV Shifts a sequence of data from one array to another
SHFTVR  Shifts a sequence of data from one array and places data in reverse order in another array
FLIP    Reverses an array in its own array location
GENARY  Generates an array of equally incremented ascending values
BLDARY  Builds an array from a variable number of arguments in the order listed
BRKARY  Distributes values from within an array to a variable number of arguments in the order listed
BKARAD  
STOARY  Places a value into or takes a value out of a specific array location
ARYSTO  
STFSEQ  Stuff a constant value into a specified length array or group of sequential locations
STFSQS  
SLDARY  Moves array data values back one or two positions and updates the last one or two values
SLDARD  
STORMA  Constructs historical data arrays during a transient analysis

(f) Singlet/Doublet Array Generation
SPLIT   Separates a doublet array into two singlet arrays
JOIN    Combines two singlet arrays into a doublet array
SPREAD  Applied interpolation subroutine DIDIDA to two singlet arrays to obtain an array of dependent variables versus an array of independent variables

(g) Comparison Operation
MAXDAR  Obtains the absolute maximum difference between corresponding elements of two arrays of equal length N
MXDRAL  

5.3 SPECIAL INPUT/OUTPUT FEATURES

Described below are the features available on MOTAR to permit the utilization of the magnetic tape capability of the Univac 1108 computer on input and/or output. Described are the data on tape with edit capabilities, restarting from and generating a restart tape, generating a history tape, starting from a history tape, plotting from a history tape and using flux curves from magnetic tapes.

5.3.1 Data on Tape with Edit

The input data described in Section 5.2.3 thru 5.2.6 must be supplied to the computer in the form of punched cards on the original run.
However, the data may be stored on magnetic tape for input to subsequent runs by use of the Data Tape with Edit feature which is available on MOTAR. This feature increases the convenience and effectiveness of the use since the handling of large decks are not required. Also, the reliability of the tape reader is much higher than that for the card reader.

The EDIT routine is called by parameter INDATA input in columns 4 and 5 on parameter card 2. Possible inputs are:

1. **INDATA = 0**, All data is supplied on cards.

2. **INDATA = 1**, All data is supplied on cards and the card images are written on tape on unit B. (Should be specified as an output tape on job card)

3. **INDATA = 2**, Use data input on tape on unit C with desired changes on cards to write a new data tape on Unit B. (C is input tape and B is output tape)

4. **INDATA = 3**, Use the data read in from unit B without change. Parameter cards 1 and 2 are read in from cards. (B is input tape)

If INDATA =-2, or -3, the card images on Unit B are punched.

When INDATA =+2, the deck set-up consists of parameter cards 1 and 2, the EDIT control cards (described below), and the new data cards (with the same format as the cards being replaced).

The EDIT control cards, used only when INDATA has a value of +2 are:

<table>
<thead>
<tr>
<th>COLUMN</th>
<th>FORMAT</th>
<th>NAME</th>
<th>DESCRIPTION</th>
</tr>
</thead>
<tbody>
<tr>
<td>1</td>
<td>A1</td>
<td>ID</td>
<td>* in column 1 identifies the card as an EDIT control card</td>
</tr>
<tr>
<td>6-15</td>
<td>I10</td>
<td>K3</td>
<td>Card number of first card to be removed if K3 is positive and K4&gt;0. If K3 is negative K31 is the card number of the card for which a merge correction will be performed. If K4 is blank or zero, cards change cards between this card and the next EDIT Control card will be add immediately following card K3.</td>
</tr>
<tr>
<td>16-25</td>
<td>I10</td>
<td>K4</td>
<td>Card number of last card to be removed prior to inserting the change cards in the data. If K3 is negative, K4 is ignored.</td>
</tr>
</tbody>
</table>
As mentioned above, when K3 is negative, the merge option of edit is used. With this option the change card submitted after (K3) will be read in 5 column fields. For each 5 column field on the change card that is blank, no change will occur to the same field on the original card. If any characters occur in a 5 column field that field on the original card will be replaced with the characters on the change card for the merged card. A $ in the 5th column of a 5 column field will cause that field to be blanked on the new merged card.

5.3.2 Dump and Restart Option

MOTAR is set up so that the problem is dumped on the third file of Unit I when either (1) the requested computer time, RTIME, or (2) the problem stop time, STIME, is exceeded. If the user assigns an output tape on Unit I this unit will contain the dumped information (on the second file) and must be saved if the problem is to be restarted. If restarting is planned the user must also save the K tape which contains the compiled computer generated program.

When restarting a problem the user supplies the I tape from a previous run on the problem to be restarted as an input L tape positioned to the proper file (usually the third file). Also, the K tape received previously on output is assigned as an input unit K on restart. The deck setup for restart is described in Section 5.4.1.

When more than one call is made to a temperature solution routine (EXPLCT or IMPLCT) the dump information for each call is contained on the odd file of Unit I starting with the third. That is, the first call will dump on the third file; the second call on the fifth file, etc. The even files contain history information discussed in Section 5.3.3.

5.3.3 History Tape Options

The history tape contains information to permit automatic plotting of problem temperatures, flow rates, and pressures and valve positions as a function of time. This tape is written to permit the user to obtain the analysis results in the convenient plotted form with a minimum of user effort. A second feature of the history tape is the ability of the user to start a new problem from any time point for which data is written (start from history tape option) The format of the history tape, plotting from the history tape and starting from the history tape are described below.

5.3.3.1 History Tape Format

History records are always written on the even files of Unit I with one history file for each call to a transient temperature solution subroutine (EXPLCT or IMPLCT). Normally problems will have only one call and thus, the history records are written on the second file with the dump for restart (Section 5.3.2) written on the third file. If the history files are to be saved for future use, the user must assign and save an I output tape

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in the control cards (See Section 5.4.1) when making the run.

The history tape file on Unit I contains a number of logical records equal to the number of history times plus two. The first record contains a title and an integer count of the number of items to be written on the history tape. The second thru the next-to-last records contain the information to written on the history tape with a record for each time point. The history write interval, PINC, is specified on parameter card 2, columns 41 thru 50. When this interval is zero, it is set to the stop time minus the initial time so that two time points are plotted (at start and end of the problem).

The format for the history tape is as follows:

Record No. 1
Title (Written internally) including date and time of run in 12A6 format, 0, 0, 0, 0, 0, No. of pressure nodes, number of valve positions, 0, 0, 0, number of tubes, 0, 0, number of nodes.

Record No. 2
Initial problem time pressures, valve positions, flow rates, node temperatures

Record No. 3
Second history time, pressures, valve positions, flow rates, Node temperatures

Record No. N+1 (Where N = number of history time slices to be written)
Last history time, Pressures, Valve positions, Flow rates, Node temperatures

Record No. N+2
Same as last record except time is negative.

5.3.3.2 Plotting From History Tape
The data written on the history tape may be used to generate SC.4020 CRT plots of the pressures, valve positions, flow rates and/or node.
temperatures versus time. To accomplish this the user must submit a separate run using the plot routine, PLOTA, with the history tape as an input. In addition the user may combine the points of two or more history tapes into one so that the results of several runs may be presented on one plot frame. This may be performed using either the PLOTA routine or the MCOMB routine. The MCOMB routine will shift the time point in addition to combining tapes if desired. The user may also plot the results of two separate runs on the same frame for comparison by using the routine COMPAR. Care must be taken when using this routine since a linear interpolation is performed at the comparison times prior to plotting.

The input descriptions for the routines PLOTA, MCOMB, and COMPAR are described in Appendix C.

5.3.3.3 Starting From a History Tape

The user may use the history tape data to start a problem. When using this option the problem input data supplied either on cards or on a data tape (using options 5.3.1) is input along with a history tape containing the desired starting conditions. A non-zero input in columns 8 and 9 of parameter card 3 and a value for TMPTIM in 61 thru 70 of parameter card 2 will cause the temperatures and valve positions to be read from the history tape on unit H at the first time point on the tape following TMPTIM. These new values will replace those of the original input. When using this option, there must be a one-to-one correspondence between the temperature nodes, and values in the model and on the history tape. Otherwise, the user may modify the model at will making this a very useful option.

5.3.4 Flux Tape Option

Incident heat curves may be read from tape by putting a non-zero value in column 6 of parameter card 3.

Restrictions on this option are:

(1) The initial block of curve data must be input on cards or data

(2) Particular curves must have the same number of points on each block of data read in as were input on cards initially

(3) Each curve may have a different number of points

(4) The curve data must be read in the same order the curves are in the data deck

(5) The first point on each curve in each block of data must be the same as the last point on that curve in the previous block of data
All incident heat curves must be in a single block by themselves.

The data is read from a binary tape which has the following format:

Record No. 1
First Read Time

Record No. 2
Number of points on Curve No. 1 (Integer), Integer 1, Curve 1 independent variables, Curve 1 dependent variables, Number of points on Curve 2, Integer 1, Curve 2 independent variables, Curve 2 dependent variables, etc. for all curves.

Record No. 3
Second Read Time

Record No. 4
Same as Record No. 2

Record No. 5
Same as Record No. 1 but for the third read time.

Etc. until all blocks of data are on tape.

The amount of data which can be read in from tape is unlimited. The amount of data which can be read in a given block is dependent upon the data space available in the computer. It is possible to restart a problem which reads incident heat curve data from tape. The tape rewinds when the program is restarted; however, when the program calls for more incident heat curve data, it searches for the proper program time before reading. To use this option the flux tape must first be generated by G. E. routine LTVFTP which writes a flux tape in the proper format for use in the LTV routines. Incident heat start-up cards are also generated by this routine.

The following operations should be performed when using the flux tape option:

1. Set flux tape code (NFLXCD) to one in column 6 of parameter card 3.

2. Input start-up incident heat curves for all incident heats that will be read from the flux tape. Also, label all such curves as curve type.
(3) Assign the incident heat flux tape as input tape E.

5.4 RUN SUBMISSION REQUIREMENTS

This section describes procedures required to submit a MOTAR run on NASA/MSC Univac 1108 Computer. Included are (1) the card deck setup requirements (2) methods for estimating the amount of computer run time and and page output requirements and (3) methods for estimating storage requirements to establish maximum problem size.

5.4.1 Deck Setup Requirements

The MOTAR input data described in section 5.2 must be combined with the required system control cards prior to submitting a run on the NASA/MSC Univac 1108 computer. The required control cards differ depending upon the input/output options and the corresponding devices required for a given problem.

Two fundamentally different types of runs may be made with MOTAR. These are (1) the runs in which the input data is supplied on cards or an input data tape (startup runs), and (2) runs which use a previously generated compressed data tape, and program elements as input (restart runs).

The deck setup for runs with the input data supplied by cards or data tape is shown in Table VIII. Included in the list shown in Table VIII are all the I/O unit that can possibly be assigned which include units A, B, C, E, F, H, I, and K. All of these units, except A, are optional and thus would not all be required for most problems. All may be used if required however. A description of the I/O devices is given below.

A is the device (logical Unit 1) to which the basic program tape should be assigned. It is always an input tape.

B is the device (logical Unit 2) to which the final data tape (after editing) is assigned. When INDATA, parameter card number 2, is 1 or 2, B is an output tape. When INDATA is 3 B is an input tape.

C is the device (logical Unit 3) to which the data tape to be edited is assigned. C is required only when INDATA=3 and is always an input tape when assigned.

E is the device (logical Unit 7) to which the flux tape is assigned when NFLXCD, parameter card 3 is ≠ 0. E is always an input.

F is reserved for making program edits to A.
TABLE VIII: Deck Setup for Runs with Input Data on Cards or Data Tape

<table>
<thead>
<tr>
<th>RUN</th>
<th>MSG</th>
<th>PLT</th>
<th>ASC, A = XXXX</th>
<th>ASG B = DATA or XXXX</th>
<th>ASG C = XXXX</th>
<th>ASG E = XXXX</th>
</tr>
</thead>
<tbody>
<tr>
<td></td>
<td></td>
<td>(Required only if user plotting subroutines are used)</td>
<td></td>
<td></td>
<td></td>
<td></td>
</tr>
<tr>
<td></td>
<td></td>
<td></td>
<td></td>
<td></td>
<td></td>
<td></td>
</tr>
</tbody>
</table>

Optional Assign Cards

7.8z - RUN
7.8n - MSG
7.8 - PLT (Required only if user plotting subroutines are used)
7.8 - ASC, A = XXXX
7.8 - ASG B = DATA or XXXX
7.8 - ASG C = XXXX
7.8 - ASG E = XXXX
7.8 - ASG F = PFC
7.8 - ASG H = XXXX
7.8 - ASG I = DUMP
7.8 - ASG K = PROG
7.8 - ASG L
7.8 - XQT CUR
   - TRW A
   - IN A
   - TRI A
   - TOC
7.8 - XQT STEP1
   (Parameter Card No. 1)

Input data deck or data edits

7.8 - FOR, K STEP2, STEP2
7.8 - FOR, K TEMPR, TEMPR
7.8 - FOR, K PRETMP, PRETMP
7.8 - FOR, K POSTMP, POSTMP
7.8 - FOR, K OUTPUT, OUTPUT
7.8 - FOR, K TEMPSS, TEMPSS

User Subroutines
TABLE VIII CONTINUED

<table>
<thead>
<tr>
<th>78</th>
<th>XQT</th>
<th>CUR</th>
</tr>
</thead>
<tbody>
<tr>
<td></td>
<td>TRW</td>
<td>K</td>
</tr>
<tr>
<td></td>
<td>DUT</td>
<td>K</td>
</tr>
<tr>
<td></td>
<td>TEF</td>
<td>K</td>
</tr>
<tr>
<td></td>
<td>ERS</td>
<td></td>
</tr>
<tr>
<td></td>
<td>TRW</td>
<td>K</td>
</tr>
<tr>
<td></td>
<td>IN</td>
<td>K</td>
</tr>
<tr>
<td></td>
<td>TRI</td>
<td>K</td>
</tr>
</tbody>
</table>

Required only if restarting is planned on future runs

<table>
<thead>
<tr>
<th>78</th>
<th>XQT</th>
<th>STEP 2</th>
</tr>
</thead>
<tbody>
<tr>
<td></td>
<td></td>
<td>(PARAMETER CARD 2)</td>
</tr>
<tr>
<td></td>
<td></td>
<td>(PARAMETER CARD 3)</td>
</tr>
<tr>
<td>78</td>
<td></td>
<td>EOF</td>
</tr>
</tbody>
</table>
H is the device (logical Unit 10) to which the history tape is assigned when NEWTMP≠0. H is always an input tape.

I is the device (logical Unit 11) which is assigned for writing history records for future plotting and for writing the dump for restart. I is always an output tape.

K is the device (logic Unit 13) which will contain the basic program from Unit A, plus the programs generated during the preprocessing phase. K should be saved as an output tape if restarting is planned in the future. If no restarting is planned, K should be assigned to a Fostran file.

L is the device (logical Unit 14) which contains the compressed data for input to the processing phase. On a restart run, it is an input tape; on other runs it is a Fostran file.

In addition to the above, two FH 432 drum files - M and N are used during the preprocessing phase. Thus, the user should identify the fact that two such files are needed on the MSG card.

The deck setup for runs with the input data supplied by a compressed data tape or restart tape is shown in Table IX. For this type of run, Units A and L are required and units E, F, H, and I are optional. The units are the same as described above.

5.4.2 Estimation of Computer Time and Output

The computer time required for a MOTAR run using the EXPLCT routine on the Univac 1108 may be estimated by the following relation:

\[
CTIME = \frac{STIME - TIME}{DTIME} \left[ \frac{(NODES) FC}{810,000} \left(1+2 \cdot VFP\right) + 1.23 \times 10^{-5}
\right.
\]

\[
\left. + \frac{HFC}{306,000} + \frac{NCC}{75,600} + \frac{NFL}{104,400} \right]
\]

Where

- CTIME = the required computer time in minutes
- STIME = the problem stop time in the problem units
- TIME = the initial problem time in the problem units
- DTIME = the problem time increment
<table>
<thead>
<tr>
<th>RUN</th>
<th>MSG</th>
<th>PLT</th>
<th>ASG_A = XXXX</th>
<th>ASG_E = XXXX</th>
<th>ASG_F = PCF</th>
<th>ASG_H = XXXX</th>
<th>ASG_I = DUMP</th>
<th>ASG_L = START</th>
<th>XQT_CUR</th>
<th>PEF_L/2</th>
<th>TRW_A</th>
<th>IN_A</th>
<th>TRI_A</th>
<th>TOC</th>
<th>XQT_STEP 2</th>
<th>EOF</th>
</tr>
</thead>
</table>

Optional Control Cards
PTIME = the problem print interval.

NODES = the number of nodes in the problem

FC = the sum of the conduction conductors plus the number of radiation conductors divided by number of NODES

FVP = the approximate fraction of capacitance and conductors that contain variable properties

NFC = Number of flow conductors

NCC = number of convection conductors

NFL = number of fluid lumps

For the Univac 1106, CTIME should be multiplied by approximately 1.7. The time required for the IMPLCT solution routine is given by,

$$\text{CTIME} = \frac{\text{STIME} - \text{TIME}}{\text{DTIME}} \left[ \frac{(\text{NODES}) \text{ FC}}{150,000} (1+2 \text{ FVP}) + \frac{\text{NFC}}{85,000} + \frac{\text{NCC}}{21,000} + \frac{\text{NFL}}{104,400} \right]$$

The above estimates do not include any provisions for user programmer subroutine time. Additional time should be allowed for any such programs.

The number of page of printed output using the standard output options may be estimated as follows,

$$\text{NP} = \frac{\text{NTUBES} + \text{NPN} + \text{NODES}}{170} \cdot \frac{\text{STIME} - \text{TIME}}{\text{PTIME}}$$

Additional pages should be allowed for any output subroutines or write statements specified by the user in addition to the standard.

5.4.3 Data Storage Requirements

The basic storage requirements for a thermal problem using the EXPLCT solution subroutine is given by:
\[
\text{NSPTH} = 5\times \text{NODES} + 3\times \text{NTC} + 4\times \text{NCC} + 3\times \text{NFC} + 3\times \text{NSPCC} + 3\times \text{NTSPC} + 3\times \text{NAH} \\
+ 4\times \text{NCURY} + \text{SNPTS} + \text{ISANFS} + 7\times (\text{NSUBS} + 1) + (\text{MXPNSS} - 1)^2 + 6\times \text{NTBS} + 21 \times (\text{MXPNSS} - 1) + 10\times \text{NFLTPS} + 20\times \text{NVLVS} + \text{NPN} + 4\times \text{NFL}
\]

Where

- **NSPTH** = total thermal space required
- **NODES** = number of nodes required
- **NTC** = total number of conductors
- **NCC** = number of convection conductor
- **NFC** = number of flow conductors
- **NSPCC** = number of special option conduction conductors (not constant)
- **NTSPC** = number of types of special capacitances (each group entry is a type)
- **NAH** = number of specified absorbed heat values
- **NCURV** = the total number of curves
- **SNPTS** = the sum of the number of points
- **NFS** = the number of flow systems
- **NSUBS** = the number of subsystems
- **MXPNSS** = the number of pressure nodes in the subsystem with the maximum number of pressure nodes
- **NTBS** = the number of flow tubes
- **NFLTPS** = the number of fluid lump types
- **NVLVS** = the number of valves
- **NPN** = the number of pressure nodes
- **NFL** = the number of fluid lumps

The storage requirements for a thermal problem using the IMLCT method of solution is that given above plus 2*NTC.

5.5 OUTPUT DESCRIPTION

Two types of standard output are available with MOTAR. The first is a normal print at the input print. The second is a check out print.
which occurs on every iteration when requested (When NCKOUT on parameter card 3 in non-zero). This checkout print consists of a normal print plus a considerable amount of addition information which is useful in checking out the input data deck. The checkout print formats for the EXPLCT and IMPLCT solution subroutines are different.

In addition to the two standard output options available on MOTAR, the user may specify any of a large number of user output subroutines these are not described in this section but a description may be found in Appendix A.

The normal MOTAR printing, the EXPLCT checkout printing, the EXPLCT checkout printing and the IMPLCT checkout printing are described below.

5.5.1. Normal Printing

Some examples of normal printing are given in the sample problems described in Appendix B. A explanation of the terms appearing in the normal print is given below. The units are always the problems units.

The beginning of a print interval is indicated by the printout of the time parameters. This is followed in order by the flow rates per tube, the pressures per pressure node, the valve positions per valve and the temperatures per node. These are described below as they appear.

Time Parameters

MISSION TIME - The mission time in the problem units

COMPUTATION INTERVAL - The computation time increment in the problem units

COMPUTER TIME - The amount of computer time used to this point (since the XQT SETP2) in minutes

Flow Rates

Flow rates are printed in numerical order by tube in the problem units. Five flow rates are output on each line with the tube number of the fifth flow rate printed to the right of it.

Pressures

Pressures are printed in numberical order by pressure node in the problem units. Five pressures are printed out per line with the pressure node number of the fifth pressure printed out to the right of it.
Valve Positions

The valve positions are listed one to a line in order of valve number. Each is identified with its number.

Temperatures

Temperatures are printed out in numerical order of the node numbers. The output is the problem unit. Temperatures are printed out five to a line with the lump number of the last temperature on each line printed just to the right of it.

5.5.2 EXPLCT Checkout Printing

The checkout printing may be used to examine internally calculated values such as heat transfer coefficients, frictional and bend loss pressure drops, and maximum time increments. An examination of the time increments for each lump may reveal that certain lumps which are not thermally important to the solution have small time increments. In that case the time increment may be selected such that fewer iterations are required. Care should be exercised that the lumps with overridden time increments do not affect the transient analysis.

An explanation of the terms appearing in the checkout printing for the EXPLCT routine is given below:

CHECKOUT PRINT FOR PRESSURE-FLOW COMPUTATION SUBROUTINE

<table>
<thead>
<tr>
<th>Term</th>
<th>Description</th>
</tr>
</thead>
<tbody>
<tr>
<td>MPASS</td>
<td>Number of temperature iterations between pressure balance</td>
</tr>
<tr>
<td>MXPASS</td>
<td>Maximum number of passes to balance in PFCS</td>
</tr>
<tr>
<td>NSS</td>
<td>Number of Subsystems in this system</td>
</tr>
<tr>
<td>LOCI</td>
<td>Starting location in the subsystem data for the subsystems of this system</td>
</tr>
<tr>
<td>NVLOC</td>
<td>Starting location in the valve data for the valves of this system</td>
</tr>
<tr>
<td>LOCP</td>
<td>Starting location in the pump data for the pumps of this system</td>
</tr>
<tr>
<td>TOL</td>
<td>Subsystem solution tolerance</td>
</tr>
<tr>
<td>EPS</td>
<td>Relaxation tolerance for numerical equation solution</td>
</tr>
<tr>
<td>NTB</td>
<td>Tube number</td>
</tr>
<tr>
<td>W(NTB)</td>
<td>Flow rate in tube NTB</td>
</tr>
<tr>
<td>NFRM</td>
<td>Upstream pressure node for tube NTB</td>
</tr>
<tr>
<td>NTO</td>
<td>Downstream pressure node for tube NTB</td>
</tr>
<tr>
<td>NF</td>
<td>Number of fluid lumps in tube NTB</td>
</tr>
<tr>
<td>LN</td>
<td>Fluid lump number</td>
</tr>
<tr>
<td>T(LN)</td>
<td>Temperature of fluid lump number LN</td>
</tr>
<tr>
<td>LOC4</td>
<td>Location in the fluid lump data array for lump LN data</td>
</tr>
<tr>
<td>WP</td>
<td>Wetted perimeter of lump number LN</td>
</tr>
</tbody>
</table>
CSA2 - Flow cross-sectional area squared for lump LN
MFF - Method code for determining friction for lump LN
HL - Number of head losses in fluid lump LN
FL/D - Fluid lump length divided by diameter for lump LN
RO - Density of fluid lump LN
MU - Viscosity of fluid lump LN
RE - Reynolds number of fluid lump LN
FFC - Friction factor coefficient for fluid lump LN
FF - Friction factor for fluid lump LN
R(LN) - Flow resistance for fluid lump LN
PCHK - Pressure at the upstream node for tube NTB
KPASS - Number of passes thru the system
NPASS - Pass number for balancing subsystem
INLT - Inlet tube number for the subsystem
NPR - Specified pressure node for the subsystem
NT - Number of tubes in the subsystem
LOC2 - The starting location in the tube data for the tubes of this subsystem
LOC3 - The starting location in the fluid lump data for the fluid lumps in this subsystem
NP - Number of pressure nodes in the subsystem
NTU - Number of tubes upstream of subsystem
G(NTB) - Flow conductor for tube NTB

Time Parameters

MISSION TIME - The mission time in the problem units
COMPUTATION INTERVAL - The computer time increment in the problem units
COMPUTER TIME - The amount of computer time used at this point (since XQT STEP2) in minutes

Flow Rates

Flow rates are printed in numerical order by tube in the problem units. Five flow rates are printed per line with the number of the fifth being identified by an integer at the end of the line.

Pressures

Pressures are printed in numerical order by pressure node in the problem units. Five pressures are printed out per line with the pressure node number of the fifth pressure printed out to the right of it.

Valve Positions

The valve positions are listed one to a line in order of valve number. Each is identified with its number.
Temperatures

Temperatures are printed out in numerical order of the node number. The output is in the problem units. Temperatures are printed out five to a line with the lump number of the last temperature on each line printed to its right.

Capacitances

Capacitances are printed out in numerical order of the node number. The output is in the problem units. These are printed out five to a line with the lump number of the last capacitance on each line printed to its right.

Heat Storage Rates

Heat storage rates are printed out in numerical order of the node number. The output is in the problem units. These are printed out five to a line with the lump number of the last rate on each line printed to its right.

Conductances

Conductances are printed out in numerical order of the conductor number. The output is in the problem units. These are printed out five to a line with the conductor number of the last conductor on each line printed to its right.

Time Increments

Time increments which are used in the temperature calculation are printed out in numerical order of the node number. The output is in the problem time units. These are printed out five to a line with the lump number of the last time increment on each line printed to its right.

CHECKOUT PRINT FOR FLOW CONDUCTOR COMPUTATION SUBROUTINE

NC - Conductor number
NFL - Lump number of the "from" lump
NTL - Lump number of the "to" lump
T(NFL) - Temperature of the from lump
KODEF - Code specifying method for obtaining flow rate
CP - Specific heat
## CHECKOUT PRINT FOR CONVECTION CONDUCTOR COMPUTATION SUBROUTINE

<table>
<thead>
<tr>
<th>Abbreviation</th>
<th>Description</th>
</tr>
</thead>
<tbody>
<tr>
<td>NC</td>
<td>Conductor number</td>
</tr>
<tr>
<td>NFL</td>
<td>Fluid lump number</td>
</tr>
<tr>
<td>NTBL</td>
<td>Tube lump number</td>
</tr>
<tr>
<td>NFS</td>
<td>Flow system number</td>
</tr>
<tr>
<td>NTB</td>
<td>Tube number</td>
</tr>
<tr>
<td>MHTC</td>
<td>Code for identifying method for heat transfer coefficient calculation</td>
</tr>
<tr>
<td>LOC5</td>
<td>Location in the type data array for the flow data for this lump</td>
</tr>
<tr>
<td>AHT</td>
<td>Heat transfer area</td>
</tr>
<tr>
<td>F1</td>
<td>Entry length laminar flow multiplying factor</td>
</tr>
<tr>
<td>F2</td>
<td>Fully developed laminar flow multiplying factor</td>
</tr>
<tr>
<td>T(NFL)</td>
<td>Fluid lump temperature</td>
</tr>
<tr>
<td>CP</td>
<td>Specific heat</td>
</tr>
<tr>
<td>VIS</td>
<td>Viscosity</td>
</tr>
<tr>
<td>CON</td>
<td>Conductivity</td>
</tr>
<tr>
<td>W(NTB)</td>
<td>Flow rate in tube NTB</td>
</tr>
<tr>
<td>WP</td>
<td>Wetted perimeter</td>
</tr>
<tr>
<td>RE</td>
<td>Reynold's number</td>
</tr>
<tr>
<td>PR</td>
<td>Prandtl number</td>
</tr>
<tr>
<td>D</td>
<td>Hydraulic Diameter</td>
</tr>
<tr>
<td>H</td>
<td>Heat transfer coefficient</td>
</tr>
<tr>
<td>X/D</td>
<td>Distance from tube entrance divided by hydraulic diameter</td>
</tr>
<tr>
<td>U(NC)</td>
<td>Calculated conductor value</td>
</tr>
<tr>
<td>ST</td>
<td>Station number when MHTC = 3, otherwise, zero</td>
</tr>
</tbody>
</table>
5.5.3 IMPLCT Checkout Printing

The checkout printing for the IMPLCT routine is identical to that for the EXPLCT routine given in Section 5.5.2 with the additions described below.

**CHECKOUT PRINT FOR IMPLICIT TEMPERATURE CALCULATION SUBROUTINE**

- **Npass** - The pass number in obtaining the temperature solution
- **Node** - The temperature node number
- **T(Node)** - The temperature of NODE
- **RHS(Node)** - The right hand side for NODE as given by the right hand side of Equation 14
- **C(Node)/TINC** - The capacitance of NODE divided by the problem time increment
- **Qsum(Node)** - The value given by RHS(Node) minus the second term on the left side of Equation 14
- **USum(Node)** - The coefficient of $T_i^{n+1}$ in Equation 14
- **Deltat** - The temperature change for the pass for NODE after applying the overrelaxation parameter
- **Tnew** - The temperature of NODE following the pass
6.0 REFERENCES


APPENDIX A

USER SUBROUTINES

1.0 INTRODUCTION

This appendix presents a description of all user subroutines currently available in MOTAR. Table A-1 presents the location of each of the seven categories of subroutines. Table A-2 presents an alphabetical listing of the user subroutines with the corresponding page numbers.

Table A-1

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### 2.0 SUBROUTINE DESCRIPTION

#### 2.1 TEMPERATURE SOLUTION SUBROUTINES (Computer generated and vary from problem-to-problem)

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<th>Description</th>
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<td>Calculates transient temperatures using the explicit method of solution. Two time increment options are available.</td>
<td>A-5</td>
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<tr>
<td>EXPSS</td>
<td>Calculates the steady state temperature distribution using data stored for explicit problem.</td>
<td>A-7</td>
</tr>
<tr>
<td>IMPLCT</td>
<td>Calculates transient temperatures using the implicit methods of solution including mid-difference, backward difference or any point between.</td>
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<td>Calculates steady state temperature distribution using data stored for implicit problems.</td>
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SUBROUTINE NAME: EXPLCT

PURPOSE:

This subroutine obtains the transients temperatures using the explicit forward differencing solution method described in Section 3.1.2.1. The calculations for each node are given by equation (12) and the stability criteria is given by equation (13). Two options are available for application of the stability criteria. There are

1. Override or Floating Option - (Specified by 0 in columns 11 through 20 of parameter card 2):

   Temperature calculation is made for each lump using the input time increment or the maximum stable increment (equation 13), whichever is smaller.

2. No Overriding Option - (Specified by a nonzero entry for TINCMN in columns 11 through 20 of parameter card 2):

   Temperature calculations for all lumps are made using the input time increment or the smallest maximum stable increment whichever is smaller (all lumps use the same increment). A minimum value for the time increment is specified by the user and the problem is terminated if the maximum stable increment drops below the input minimum.

EXPLCT is generated during the preprocessing phase of MOTAR based upon the input data and thus will vary in actual form from problem to problem, depending upon the requirements. A functional flow chart is shown in Figure A-1, which shows the order of calculations including the calls to the user programming blocks. Many of the operations shown will not be present when the data doesn't require them.

RESTRICTIONS:

Must be called from the $CENTRAL block. MPLCT code in columns 6 to 10 of parameter card 1 must be 0 or blank.

CALLING SEQUENCE: EXPLCT
FIGURE A-1: FUNCTIONAL FLOW CHART OF SUBROUTINE EXPLCT
SUBROUTINE NAME: \textsc{expss}

PURPOSE:

This subroutine obtains the steady state temperature distribution for problems with the data stored in the explicit format. It is compatible with the \textsc{explct} subroutine and, thus, may be used on the same problem. It iterates the basic transient explicit temperature equation (Equation 12) to a solution while holding time constant. Convergence is accelerated by applying the maximum stable time increment given by Equation 13 to each node. This method results in a block iterative solution method. Compared with subroutine \textsc{impss}, the convergence is slower but less storage space for the data is required.

A functional flow chart for \textsc{expss} is shown in Figure A-2.

RESTRICTIONS:

MPLCT code in columns 6 thru 10 of parameter card 1 must be 0. Must be called from \$CENTRAL

CALLING SEQUENCE: \textsc{expss}

SUBROUTINE NAME: \textsc{implct}

PURPOSE:

This subroutine calculates the transient temperature distribution using the implicit method of solution discussed in Section 3.1.2.2. Either backward difference, mid-difference or any point in between may be specified by the value of ALPHA in columns 16 thru 20 of parameter card 3, which is constrained to be between 0.5 and 1.0. When ALPHA is 1.0 the solution is backward-difference; when ALPHA is 0.5 the solution is mid-difference. A modified version of the successive-point-over relaxation iteration method is used for equation solution. The over-relaxation parameter, ORP, is supplied in columns 26 thru 30, and the solution tolerance DTMXA is supplied in columns 21 thru 25, both on parameter card 3.

Figures A-3 and A-4 provide functional flow charts of \textsc{implct} and \textsc{tempi} which is called from \textsc{implct}. As may be seen, the \$PRETEMP operations are preformed during the relaxation loop of \textsc{tempi}, and thus, the user calls in \$PRETEMP are considered during relaxation. The user may not reference the C array from \$PRETEMP when using \textsc{implct} but may perform operations on the Q, U, and T arrays. C operations may be performed in the \$POSTTEMP block.

RESTRICTIONS:

MPLCT code in column 10 of parameter card 1 must be 1. \textsc{implct} must be called from \$CENTRAL. The C array is not available to the user in the \$PRETEMP operations block.

CALLING SEQUENCE: \textsc{implct}
EXPSS

CALCULATE INITIAL CONDITIONS

CALCULATE ALL TIME DEPENDENT COEFFICIENTS, ABSORBED HEAT VALUES AND TEMPERATURES

CALCULATE TEMPERATURE DEPENDENT COEFFICIENTS AND ABSORBED HEAT

PERFORM $ PRETEMP OPERATIONS

PERFORM TEMPERATURE CALCULATIONS

PERFORM $ POSTTEMP OPERATIONS

IS TEMPERATURE CHANGE LESS THAN INPUT TOLERANCE

NO

IS NO. OF ITERATIONS GREATER THAN MAX VALUE

NO

IS ETIME > RTIME

NO

PERFORM STD PRINTOUT; PERFORM $ OUTPUT OPERATIONS

RETURN

YES

WRITE ERROR MESSAGE

YES

WRITE ERROR MESSAGE
PERFORM $ OUTPUT OPERATIONS

INITIALIZE PROBLEM

DETERMINE CAPACITANCES, CONDUCTORS AND ABSORBED HEATS, AT MEAN TIME

DETERMINE RIGHT HAND SIDE OLD TIME

ADVANCE TIME

INTERPOLATE FOR TIME DEP. TEMPS

CALL TEMP SOLUTION SUBROUTINE, TEMPI

PERFORM $ POSTTEMP OPERATIONS

PERFORM PRESSURE/ FLOW BALANCE

IS TIME > STIME

NO

IS ETIME > RTIME

YES

WRITE MESSAGE

WRITE ON HISTORY TAPE, DUMP TAPE AND OUTPUT

RETURN

WRITE HISTORY TAPE

YES

TIME FOR OUTPUT

NO

TIME TO WRITE HISTORY TAPE

YES

NO

FIGURE A-3: FUNCTIONAL FLOW CHART OF IMPLCT

A-9
TEMPI

INITIALIZE CONSTANTS

LPASS = TRUE

IS DTMX.GT.PTMA

CALL $ PRETEMP OPERATIONS AT NEW TIME

NO

YES

IS NODE NO. ≤ 0

YES

LPASS = .FALSE.

NO

CALCULATE NEW NODE TEMP

IS TEMP CHANGE GT THAN TOL

NO

SET NODE NO. NEGATIVE

YES

IS THIS LAST NODE

YES

IS THE MAXIMUM CHANGE GT. TOL

NO

SET NODE NOS. POSITIVE

YES

IS LPASS TRUE

NO

RETURN

FIGURE A-4: FUNCTIONAL FLOW CHART OF TEMPI
SUBROUTINE NAME: IMPLSS

PURPOSE:

This subroutine calculates the steady state temperature distribution for problems with the data stored in the implicit format. It is compatible with IMPLCT in that data stored for either may be used with the other. Thus, IMPLCT and IMPLSS may be used on the same problem.

Subroutine IMLSS performs the same basic iteration procedure performed in IMPLCT except the time is held constant and the capacitance is assumed to be zero. Functional flow charts of IMPLSS and TEMPSS which it calls are shown in Figure A-5 and A-6.

The values of the overrelaxation parameter, ORP, and the solution tolerance, DTMXA, are supplied on parameter card 3.

RESTRICTIONS:

IMPLCT code in column 10 of parameter card 1 must be 1. IMPLSS must be called from $CENTRAL. The C array is not available to the user in the $PRETEMP operations block.

CALLING SEQUENCE: IMPLSS
IMPLSS

INITIALIZE PROBLEM

DETERMINE ABSORBED HEATS, AT MEAN TIME

DETERMINE RIGHT HAND SIDE OLD TIME

INTERPOLATE FOR TIME DEP. TEMPS

CALL TEMP SOLUTION SUBROUTINE TEMPSS

PERFORM $ POSTTEMP OPERATIONS

PERFORM PRESSURE/FLOW BALANCE

PERFORM STOP

PERFORM $ OUTPUT

RETURN

WRITE ERROR

FIGURE A-5: FUNCTIONAL FLOW CHART OF IMPSS
INITIALIZE CONSTANTS

LPASS = TRUE

IS DTMX.GT.PTMA

YES

IS NODE NO. <= 0

YES

LPASS = .FALSE.

NO

CALCULATE NEW NODE TEMP

IS TEMP CHANGE GT THAN TOL

YES

NO

THIS LAST NODE

YES

IS THE MAXIMUM CHANGE GT TOL

YES

NO

SET NODE NOS. POSITIVE

IS LPASS TRUE

YES

NO

RETURN

FIGURE A-5: FUNCTIONAL FLOW CHART OF TEMPS
## 2.2 APPLICATION SUBROUTINES

### Thermal Radiation Exchange

<table>
<thead>
<tr>
<th>Subroutine</th>
<th>Description</th>
<th>PAGE</th>
</tr>
</thead>
<tbody>
<tr>
<td>RADIR</td>
<td>Calculates the script FA values for IR radiation within an enclosure and uses these values to obtain the heat transfer due to radiation. Permits consolidation of several nodes on one radiating surface.</td>
<td>A-15</td>
</tr>
<tr>
<td>IRRADI</td>
<td>Simulates a radiosity network within a multiple grey surface enclosure containing a non-absorbing media.</td>
<td>A-17</td>
</tr>
<tr>
<td>IRRADE</td>
<td>Simulates a radiosity network within a multiple grey surface enclosure containing a non-absorbing media.</td>
<td>A-17</td>
</tr>
<tr>
<td>RADSOL</td>
<td>Calculates the script FA values for non-infrared radiation in an enclosure and uses these values to obtain heat transfer during the problem. Permits consolidation of several nodes on one radiating surface.</td>
<td>A-18</td>
</tr>
<tr>
<td>SLRADI</td>
<td>Similar to IRRADI and IRRADE but designed to solve for the solar heating rates within an enclosure.</td>
<td>A-20</td>
</tr>
<tr>
<td>SLRADE</td>
<td>Similar to IRRADI and IRRADE but designed to solve for the solar heating rates within an enclosure.</td>
<td>A-20</td>
</tr>
<tr>
<td>EFFEMS</td>
<td>Calculates the effective emissivity between parallel flat plates.</td>
<td>A-20</td>
</tr>
<tr>
<td>SCRPFA</td>
<td>Obtains the script FA value for radiant transfer within an enclosure.</td>
<td>A-21</td>
</tr>
</tbody>
</table>

### Heat Exchanger and Heater

<table>
<thead>
<tr>
<th>Subroutine</th>
<th>Description</th>
<th>PAGE</th>
</tr>
</thead>
<tbody>
<tr>
<td>HXEFF</td>
<td>Simulates heat exchangers under steady state conditions for constant effectiveness, counter flow, cross flow, and parallel flow conditions respectively.</td>
<td>A-22/A-26</td>
</tr>
<tr>
<td>HXCTN</td>
<td>Simulates heat exchangers under steady state conditions for constant effectiveness, counter flow, cross flow, and parallel flow conditions respectively.</td>
<td>A-22/A-26</td>
</tr>
<tr>
<td>HXCROS</td>
<td>Simulates heat exchangers under steady state conditions for constant effectiveness, counter flow, cross flow, and parallel flow conditions respectively.</td>
<td>A-22/A-26</td>
</tr>
<tr>
<td>HXPAR</td>
<td>Simulates heat exchangers under steady state conditions for constant effectiveness, counter flow, cross flow, and parallel flow conditions respectively.</td>
<td>A-22/A-26</td>
</tr>
<tr>
<td>HEATER</td>
<td>Simulates heat exchangers under steady state conditions for constant effectiveness, counter flow, cross flow, and parallel flow conditions respectively.</td>
<td>A-22/A-26</td>
</tr>
</tbody>
</table>

### Cabin Analysis

<table>
<thead>
<tr>
<th>Subroutine</th>
<th>Description</th>
<th>PAGE</th>
</tr>
</thead>
<tbody>
<tr>
<td>CABIN</td>
<td>Performs a heat and mass balance on a cabin gas considering any number of entering streams and condensation on the cabin wall.</td>
<td>A-28</td>
</tr>
</tbody>
</table>

### Phase Change

<table>
<thead>
<tr>
<th>Subroutine</th>
<th>Description</th>
<th>PAGE</th>
</tr>
</thead>
<tbody>
<tr>
<td>ABLATS</td>
<td>Represents a simple ablation (sublimation) capability.</td>
<td>A-32</td>
</tr>
<tr>
<td>LQSLTR</td>
<td>Accounts for the phase change energy of a melting or solidifying material.</td>
<td>A-34</td>
</tr>
<tr>
<td>LQDVAP</td>
<td>Allows the user to simulate the addition of liquid to a node.</td>
<td>A-35</td>
</tr>
</tbody>
</table>
SUBROUTINE NAME: RADIR

PURPOSE:

RADIR calculates the script-F values for infrared radiation heat transfer within an enclosure and uses these values to obtain the heat transfer during the problem. Several temperature nodes may be combined on a single surface for radiation heat transfer purposes. Also, the user may analyze problems with specular, diffuse or combinations of specular and diffuse radiation. See Section 3.1.3.5 for definitions and detailed description of methods.

RADIR calculates the script-F values on the initial call. This is performed by the procedure outlined in Section 3.1.3.5, Equations 23, 25 and 31. These values are stored for future use in the A6 array supplied by the user. The heat flux values are then calculated on all iterations by:

1. Calculating the temperature of each surface using equation 34
2. Calculating the absorbed heat for each node by the relation of equation 33

The value given by equation 35 is added to the conductor sum for each node so that the proper conveyence time increment may be obtained. As many enclosures as desired may be analyzed but each enclosure requires a different call to RADIR. RADIR must be called in $PRETEMP.

RESTRICTIONS:

Must be called from $PRETEMP

CALLING SEQUENCE:

RADIR (A1(IC), A2(IC), A3(IC), A4(IC), A5(IC), A6(IC))

Where the arrays are formatted:

A1(IC), n, SN1, SA1, NN1, SN2, SA2, NN2, ............ SNn, SAN, NNn
A2(IC), SE1, SE2------SEn
A3(IC), SR1, SR2------SRn
A4(IC), SNF1, SNT1, ETF1, SNF2, SNT2, ETF2,------SNFm, SNTm, ETFm
A5(IC), NNO(1,1), AN(1,1), NNO(1,2), AN(1,2)----NNO(1,NN1), AN(1,NN1),
       NNO(2,1), AN(2,1), NNO(2,2), AN(2,2)----NNO(2,NN2), AN(2,NN2),
       ...........
       ...........
       NNO(n,1), AN(n,1), NNO(n,2), AN(n,2)----NNO(n,NNn), AN(n,NNn)
A6(IC), S, NSPACE
The following definitions apply in the above calling sequence.

<table>
<thead>
<tr>
<th>Variable</th>
<th>Description</th>
</tr>
</thead>
<tbody>
<tr>
<td>A1, A2, ..., A6</td>
<td>Location for arrays supplied in the $CURVE block. The user must use the LUTAB function to find the location (see Section 5.2.5)</td>
</tr>
<tr>
<td>n</td>
<td>The number of surfaces</td>
</tr>
<tr>
<td>SN1, SN2, ..., SNn</td>
<td>Node number for surfaces - must be boundary nodes</td>
</tr>
<tr>
<td>SA1, SA2, ..., SAN</td>
<td>Total area for each surface</td>
</tr>
<tr>
<td>NN1, NN2, ..., NNn</td>
<td>Number of temperature nodes on each surface</td>
</tr>
<tr>
<td>SE1, SE2, ..., SEN</td>
<td>Emissivity values for each surface</td>
</tr>
<tr>
<td>SR1, SR2, ..., SRn</td>
<td>Diffuse reflectivity values for each surface</td>
</tr>
<tr>
<td>SNF1, SNT1, EFT1</td>
<td>Connections data: Surface number from, surface number to, E value from SNF1 to SNT1, etc.</td>
</tr>
<tr>
<td>NNO(X,Y)</td>
<td>Temperature node numbers on surfaces; Node number Y on surface X</td>
</tr>
<tr>
<td>NSPACE</td>
<td>Number of spaces needed to store script-FA values - NSPACE must be an integer values of ( \frac{n}{2(n+1)} )</td>
</tr>
<tr>
<td>m</td>
<td>The number of surface connections</td>
</tr>
</tbody>
</table>
THERMAL RADIATION EXCHANGE

SUBROUTINE NAMES: IRRADI or IRRADE

PURPOSE:

These subroutines simulate a radiosity network* within a multiple gray diffuse surface enclosure containing a non-absorbing media. The input is identical for both subroutines. However, IRRADE utilizes explicit equations to obtain the solution by relaxation and IRRADI initially performs a symmetric matrix algebra inverse and thereafter obtains the exact solution implicitly by matrix multiplication. The relaxation criteria of IRRADE is internally calculated and severe enough so that both routines generally yield identical results. However, IRRADE should be used when temperature varying emissivities are to be considered and IRRADI should be used when the surface emissivities are constant. Both subroutines solve for the J node radiosity, obtain the net radiant heat flow rates to each surface and return them sequentially in the last array that was initially used to input the surface temperatures. The user need not specify any radiation conductors within the enclosure.

RESTRICTIONS:

The Fahrenheit system is required. The arbitrary number of temperature arguments may be constructed by a preceding BLDARY call. The emissivity, area, temperature-Q and upper half FA arrays must be in corresponding order and of exact length. The first data value of the FA array must be the integer number of surfaces and the second the Stefan-Boltzmann constant in the proper units and then the FA floating point values in row order. The diagonal elements (even if zero) must be included. As many radiosity subroutine calls as desired may be used. However, each call must have unique array arguments. The user should follow the radiosity routine by SCALE, BRKARY or BKARAO to distribute the Q's to the proper source location.

CALLING SEQUENCE: IRRADI(AA(IC),Ae(IC),AFA(IC),ATQ(IC))

or

IRRADE(AA(IC),Ae(IC),AFA(IC),ATQ(IC))

where the arrays are formatted as follows:

AA(IC),A1,A2,A3,A4,...,AN
Ae(IC),e1,e2,e3,e4,...,eN
AFA(IC),N,a,FA(1,1),FA(1,2),FA(1,3),FA(1,4),FA(1,5),...,FA(1,N)
FA(2,2),FA(2,3),FA(2,4),FA(2,5),...,FA(2,N)
FA(N-2,N-2),FA(N-2,N-1),FA(N-2,N)
FA(N-1,N-1),FA(N-1,N)
FA(N,N).

ATQ(IC),T1,T2,T3,...,TN

where FA(1,2) is defined as A(1)*F(1,2). After the subroutine is performed the ATQ array is ATQ(IC),Q1,Q2,Q3,...,QN.

Since FA(1,2)=FA2(2,1) only the upper half triangle of the full FA matrix is required. IRRADI inverts this half matrix in its own area, hence approximately 300 surfaces may be considered using MBTAR on a 65K core machine.

SUBROUTINE NAME:  RADSOL

PURPOSE:

RADSOL calculates a pseudo script-F for radiation from an external source entering an enclosure and uses these values to calculate the net heat transfer to each node due to the entering source. A number of temperature nodes may be combined on a single surface for radiation purposes. Also, problems with specular, diffuse, or combinations of specular and diffuse radiation may be analyzed. Section 3.1.3.5 should be consulted for definitions and descriptions of methods.

RADSOL calculates the pseudo script-F values on the initial call. This is performed by equations 38, 40, and 44 of section 3.1.3.5. The values are stored in the A7 array supplied by the user. The heat flux values are then calculated on each iteration by equations 45 and 46.

The user may analyze as many enclosures as desired by supplying a call statement for each enclosure. Also, a user may analyze several wavelength bands of radiation for any enclosure by supplying a call statement (and appropriate data) for each wavelength bands.

RESTRICTIONS:

Must be called from the $PRETEMP operations.

CALLING SEQUENCE:

RADSOL (A1(IC),A2(IC),A3(IC),A4(IC),A5(IC),A6(IC),A7(IC)

Where the arrays are formed:

A1(IC), n,SN1,SA1,NN1,SN2,SA2,NN2, - - - - - - - - Snn,SNn,SAAn,NNn
A2(IC),SE1,SE2, - - - - - - - - SEn
A3(IC),SR1,SR2, - - - - - - - - SRn
A4(IC),SHT1,SHT2, - - - - - - - - SHTn
A5(IC),SNFL1,SNFL1,EFL1,SNFL2,SNFL2,EFL2, - - - - SFm,SNm,EFLm
A6(IC),NNO1,1,1,AN1,1,NNO1,2,1,AN1,2, - - - - - - NNO1,NN1,1,AN1,NN1,1,

NNO2,1,1,AN2,1,NNO2,2,1,AN2,2, - - - - - - NNO2,NN2,1,AN2,NN2,1,

NNO(n,1),AN(n,1),NNO(n,2),AN(n,2) - - - - - - NNO(n,NNn),AN(n,NNn)
A7(IC), S, NSPACE

The following definitions apply in the above calling sequence
A1,A2,.....A6  Location for arrays supplied in the $CURVE block. The user must use the LUTAE function to find the location (See Section 5.2.5)

n = the number of surfaces

SN1,SN2,...SNN  Node number for surfaces must be boundary nodes

SA1,SA2,...SAN  Total area for each surface

NN1,NN2,...NNN  Number of temperature nodes on each surface

SE1,SE2,...SEN  Emissivity values for each surface

SR1,SR2,...SRN  Diffuse reflectivity values for each surface

SHT1,SHT2,...SHTN  Incident heat flow on surfaces may be curve 1, 2, --- n or constant

SNF1,SNT1,EFT1  Connections data: Surface number from surface number to, E value from SNF1 to SNT1, etc.

NNO(X,Y)  Temperature node numbers on surfaces: Node number Y on surface X

NSPACE  Number of spaces needed to store script-FA values - NSPACE must be an integer values of n/2(n+1)
SUBROUTINE NAMES: SLRADI or SLRADE

PURPOSE:

These subroutines are very similar to IRRADI and IRRADE but are designed to solve for the solar heating rates within an enclosure. SLRADI inverts a half symmetric matrix in order to obtain implicit solutions, while SLRADE obtains solutions explicitly by relaxation. SLRADE should be used when temperature varying solar absorptivities are to be considered. The second data value of the AFA array must be the solar constant in the proper units. The AT array allows the user to input the angle (degrees) between the surface normal and the surface-sun line. The AI array allows the user to input an illumination factor for each surface which is the ratio from zero to one of the unshaded portion of the surface. The solar constant (S), AT and AI values may vary during the transient for both routines. No input surface temperatures are required. The absorbed heating rates are returned sequentially in the AQ array, the user may utilize SCALE, BRKARY or BKARAD to distribute the heating rates to the proper source locations.

RESTRICTIONS:

These routines are independent of the temperature system being used. All of the array arguments must reference the integer count set by the SINDA preprocessor and be of the exact required length. As many calls as desired may be made but each call must have unique array arguments.

CALLING SEQUENCE:

SLRADI(AA(IC), AT(IC), AFA(IC), AT(IC), AI(IC), AQ(IC))

or

SLRADE(AA(IC), AT(IC), AFA(IC), AT(IC), AT(IC), AQ(IC))

SUBROUTINE NAME: EFFEMS

PURPOSE:

This subroutine calculates the effective emissivity E between parallel flat plates by the following equation:

\[ E = \frac{1.0}{1.0/E1 + 1.0/E2 - 1.0} \]

where \( E1 \) and \( E2 \) are the emissivities of the two surfaces under consideration.

RESTRICTIONS:

Arguments must be floating point numbers.

CALLING SEQUENCE:

EFFEMS(E1, E2, E)
THERMAL RADIATION EXCHANGE

SUBROUTINE NAME: SCRPFA

PURPOSE:

To obtain the script FA value for radiant transfer within an enclosure. The input arrays are formatted as shown for subroutines IRRADI and IRRADE. The second data value in the AFA array is used as a final multiplier, if 1.0 the script FA values are returned; if the script FA values are returned. The script FA values are returned in the ASFA array which is formatted identical to the AFA array and may overlay it.

RESTRICTIONS:

All array arguments must reference the integer count set by the MOTAR preprocessor and all arrays must be exactly the required length.

CALLING SEQUENCE: SCRPFA(AA(IC),Ac(IC),AFA(IC),ASFA(IC))

NOTE: Subroutine SYMLST(ASFA(IC)+3,ASFA(IC)+1) may be called to list the matrix values and identify them by row and column number. This routine and the implicit radiosity routine finalize the half symmetric coefficient matrix and call on SYMINV(AFA(IC)+3,AFA(IC)+1) to obtain the symmetric inverse.
SUBROUTINE NAME: HXEFF

PURPOSE:

This subroutine obtains the heat exchanger effectiveness either from a user constant or from a biariant curve of effectiveness versus the flow rates on the two sides. The effectiveness thus obtained is used with the supplied flow rates, inlet temperatures and fluid properties to calculate the outlet temperatures using the methods described in Section 3.1.3.2. The user may specify a constant effectiveness by supplying a real number and may use the LUTAB*function to specify the effectiveness as a biariant function of the two flow rates. The user also supplies flow rates, specific heat values, inlet temperatures and a location for the outlet temperatures for each of the two sides. The flow rate array may be referenced to obtain flow rates and the temperature array may be used for temperatures. The LUTAB function may be used to obtain the specific heat values from a temperature dependent curve or a constant value may be supplied.

RESTRICTIONS:

HXEFF should be called in the $PRETEMP operations block. The value for EFF, the first argument must never be zero.

CALLING SEQUENCE:

HXEFF(EFF,W1,W2,CP1,CP2,TIN1,TIN2,TOUT1,TOUT2)

Where EFF - is (1) the effectiveness if real, (2) LUTAB (IEFF)

Where EFF - is (1) the effectiveness if real, (2) LUTAB (IEFF)

W1,W2 - are the flow rates for side 1 and 2 respectively. May reference the flow rate array, W(I) where I is the tube number

CP1,CP2 - are the specific heat value for side 1 and side 2 fluid respectively. Constant values may be input or LUTAB may be used to reference curves in $CURVES

TIN1,TIN2 - are inlet lump temperatures - Usually T(LI1) and T(LI2) where LI1 and LI2 are the inlet lumps on side 1 and side 2

TOUT1,TOUT2 - are the outlet lump temperature locations where the calculated values will be stored

* See page 114
SUBROUTINE NAME: HXCNT

PURPOSE:

This subroutine calculates the heat exchanger using the relation described in Section 3.1.3.2 for a counter flow type exchanger. The value of UA used in the calculations may be specified as a constant by supplying a real number or it may be specified as a bivariant function of the two flow rates by using the LUTAB*function. The user also supplies flow rates, specific heat values, inlet temperatures and a location for the outlet temperatures for each of the two sides. The flow rate array may be referenced to obtain flow rates and the temperature array may be used for temperatures. The LUTAB function may be used to obtain the specific heat values from a temperature dependent curve or a constant value may be supplied.

RESTRICTIONS:

HXCNT should be called in the $PRETEMP operations block. The value for UA, the first argument must never be zero.

CALLING SEQUENCE:

HXCNT(UA,W1,W2,CP1,CP2,TIN1,TIN2,TOUT1,TOUT2)

Where

UA - is (1) the heat exchanger conductance if real, (2) LUTAB (IUA) where IUA is a curve number of a bivariant curve of conductance versus W1 and W2 (See page A-60A)

W1,W2 - are the flow rates for sideline side 2 respectively. May reference the flow rate array, W(I) where I is the tube number

CP1,CP2 - are the specific heat values for side 1 and 2 fluid respectively. Constant values may be input or LUTAB may be used to reference curves in $CURVES

TOUT1-TOUT2 - are the outlet lump temperature locations where the calculated values will be stored

* See page 114
Subroutine Name: HXCROS

Purpose:

This subroutine calculates the heat exchanger using the relations described in Section 3.1.3.2 for a counter flow type exchanger. The value of UA used in the calculations may be specified as a constant by supplying a real number or it may be specified as a bivariant function of the two flow rates by using the LUTAB*function. Any one of the following four types of cross flow exchangers may be analyzed (see Section 3.1.3.2 for the relations):

1) Both steams unmixed
2) Both streams mixed
3) Stream with smallest MCp product unmixed
4) Stream with largest MCp product unmixed

The type is specified by the last argument in the call statement. Also supplies flow rates, specific heat values, inlet temperatures and a location for the outlet temperatures for both sides. The flow rate array may be referenced to obtain flow rates and the temperature array may be used for temperatures. The LUTAB function may be used to obtain the specific heat values from a temperature dependent curve or a constant value may be supplied.

Restrictions:

HXCROS should be called in the $PRETEMP operations block. The value for UA, the first argument must never be zero.

Calling Sequence:

HXCROS(UA, W1, W2, CP1, CP2, T1N1, T1N2, TOUT1, TOUT2, K)

Where

UA - is (1) the heat exchanger conductance if real, (2) LUTAB(IUA) where IUA is a curve number of a bivariant curve of conductance versus W1 and W2.

W1, W2 - are the flow rates for side 1 and side 2 respectively. May reference the flow rate array, W(I) where I is the tube number.

CP1, CP2 - are the specific heat values for side 1 and side 2 fluid respectively. Constant values may be input or LUTAB may be used to reference curves in $CURVES.

* See page 114
TIN1,TIN2 - are inlet lump temperatures - Usually T(LI1) and T(LI2) where LI1 and LI2 are the inlet lumps on side 1 and side 2

TOUT1,TOUT2 - are the outlet lump temperature locations where the calculated values will be stored

K is the code specifying type of cross flow exchanger:

- Both steams unmixed: K=1
- Both streams mixed: K=2
- Stream with small WCp Unmixed: K=3
- Stream with large WCp unmixed: K=4
SUBROUTINE NAME: HXPAR

PURPOSE:

This subroutine calculates the heat exchanger using the relation described in Section 3.1.3.2 for a parallel flow type exchanger. The value of UA used in the calculations may be specified as a constant by supplying a real number or it may be specified as a bivariant function of the two flow rates by using the LUTAB*function. The user also supplies flow rates, specific heat values, inlet temperatures and a location for the outlet temperatures for each of the two sides. The flow rate array may be referenced to obtain flow rates and the temperature array may be used for temperatures. The LUTAB function may be used to obtain the specific heat values from a temperature dependent curve or a constant value may be supplied.

RESTRICTIONS:

HXPAR should be called in the $PRETEMP operations block. The value for UA, the first argument must never be zero.

CALLING SEQUENCE:

HXPAR(UA,W1,W2,CP1,CP2,TIN1,TIN2,TOUT1,TOUT2)

Where

- UA: is (1) the heat exchanger conductance if real, (2) LUTAB (IUA) where IUA is a curve number of a bivariant curve of conductance versus W1 and W2. (See page A-60A)
- W1,W2: are the flow rates for side 1 and 2 respectively. May reference the flow rate array, W(I) where I is the tube number
- CP1,CP2: are the specific heat values for side 1 and side 2 fluid respectively. Constant values may be input or LUTAB may be used to reference curves in $CURVES
- TIN1,TIN2: are inlet lump temperatures - Usually T(LI1) and T(LI2) where LI1 and LI2 are the inlet lumps on side 1 and side 2
- TOUT1,TOUT2: are the outlet lump temperature locations where the calculated values will be stored

* See page 114
SUBROUTINE NAME: HEATER

PURPOSE:
This subroutine simulates an electrical heater with a control system which turns the heater on when the sensor lump temperature falls below the "heater on" temperature TON, and turns the heater off when the sensor lump rises above the heater off temperature, TOFF. When the heater is on, the input Q value is added to the Q location specified by the user. When the heater is off, the no heat is added.

RESTRICTIONS:
HEATER must be called in the $PRETEMP operations block.

CALLING SEQUENCE:
HEATER (TSEN,TON,TOFF,HT,Q)

Where
TSEN is the sensed temperature
TON is the heater on temperature
TOFF is the heater off temperature
HT is the heater heat rate
Q is the location for storing the heat
SUBROUTINE NAME: CABIN

PURPOSE:

This subroutine performs a thermal and mass balance on a cabin air system. The cabin air is assumed to be a two component gas mixture with one condensible component and one noncondensible component. The cabin air is assumed to be well mixed so that the temperature and specific humidity are constant throughout. The cabin may contain any number of entering streams each with different temperature and humidity conditions. The cabin air may transfer heat to its surroundings any number of nodes with the heat transfer coefficient obtained by one of the three options:

1. User input coefficient
2. Relations for flow over a flat plot
3. Relations for flow over a tube bundle

The relations describing the second and third options are given in Section 3.1.3.4. The mass transfer coefficient for determining the rate of condensation or evaporation is determined by the Lewis relation which related the mass transfer coefficient directly to the connection heat transfer coefficient. By the Lewis Relation, if the diffusion coefficient is approximately equal to the thermal diffusivity, the Sherwood number is approximately equal to the Nusselt number, thus giving a direct relation. (See Section 3.1.3.4 for details) Mass and heat transfer rates are determined at each node that interfaces the cabin gas as well at entering and exiting streams and a new cabin gas temperature and humidity is determined each iteration based upon the heat and mass balance. An account is kept of the condensate on the walls when condensation occurs but the condensate is assumed to remain stationary and not flow to other wall nodes.

Limits are applied when necessary to prevent more condensation than the vapor existing under severe transient condition and to prevent evaporation of more liquid than exists at each wall lump.

As many cabins as desired may be analyzed in a given problem, but each must contain separate input information.

RESTRICTIONS:

CABIN must be called in $PRETEMP

CALLING SEQUENCE:

CABIN (A1, A2, A3, TC, A5, A6, A7, A8)
Where

A1 is an array location * in $CURVES of an array containing the entering flow rate information. The format of the array is:

\[
NS, FR_1, PSI, TE_1, FR_2, PSI_2, TE_2 \ldots FR_{ns}, PSI_{ns}, TE_{ns}
\]

A2 is an array location * in $CURVES of an array containing curve numbers in $CURVES for property values. The format of the array is:

\[
NFLC, NMUO, NMUV, NCPV, NKO, NKV, NLAT
\]

A3 is an array location in $CURVES of an array containing pertinent constants. The format of the array is:

\[
RA, RV, VC, PC, XC, WV, PSIC, PO, TO, CONV
\]

\(T_c\) is the cabin gas temperature which must be a boundary node.

A5 is the location in $CURVES of an array containing node numbers and connection heat transfer coefficient values for nodes surrounding the cabin gas. The format of the array is:

\[
LN_1, HA_1, LN_2, HA_2 \ldots LN_{n1}, HA_{n1}
\]

A6 is the location in $CURVES of an array containing node numbers and information to permit calculation of convection coefficients for flat plates. The format is:

\[
LN_1, XX_1, XI_1, AI_1, VIW_1, LN_2, XX_2, XI_2, AI_2, \\
VIW_2, \ldots LN_{n2}, XX_{n2}, XI_{n2}, AI_{n2}, VIW_{n2}
\]

A7 is the $CURVES location of an array containing node numbers and information to permit calculation of convection coefficients for tube bundles. The format is:

\[
LN_1, DI_1, AI_1, VIW_1, LN_2, DI_2, AI_2, VIW_2, \ldots LN_{n3}, \\
DI_{n3}, AI_{n3}, VIW_{n3}
\]

A8 is a working space array which must contain a number of spaces equivalent to three times the sum of the number of nodes with input heat transfer coefficients plus the number using flat plot relations plus the number using tube bundles.

* See page 114
The following symbol definitions apply in the above:

- **NS**: Number of incoming streams
- **FR<sub>i</sub>**: Entering flow rate for stream <i>i</i>
- **PSI<sub>i</sub>**: Specific humidity for entering stream <i>i</i>
- **TE<sub>i</sub>**: Temperature of entering stream <i>i</i>
- **NFLC**: Curve number for circulation flow rate vs time
- **NMUO**: Curve number for noncondensible viscosity vs temperature
- **NMUV**: Curve number for condensible viscosity vs temperature
- **NCPO**: Curve number for noncondensible specific heat vs temperature
- **NCPV**: Curve number for condensible specific heat vs temperature
- **NKO**: Curve number for noncondensible thermal conduction vs temperature
- **NKV**: Curve number for condensible thermal conduction vs temperature
- **NLAT**: Curve number for latent heat of condensible vs temperature
- **RA**: Gas constant for non-condensible component
- **RV**: Gas constant for condensible component
- **VC**: Cabin volume
- **PC**: Cabin Pressure
- **WC**: Initial vapor weight in cabin
- **PSIC**: Initial specific humidity for cabin
- **LN<sub>i</sub>**: Cabin wall lump
- **HA**: Heat transfer coefficient times area
- **n1**: Number of wall lumps which have input HA values
- **n2**: Number of wall lumps which have HA calculated by flat plate relations
- **n3**: Number of wall lumps which have HA calculated by tube bundle relations
- **XX<sub>i</sub>**: Distance from leading edge for flat plate heating for <i>i</i>th flat plate node
- **XI<sub>i</sub>**: Length of flat plate in flow direction for <i>i</i>th flat plate node
AI_i
Heat transfer area for flat plate or tube node

DI_i
Tube outside diameter for tubes in the bundle for ith tube node

VIWO
Ratio of velocity at the lump to the circulation flow rate

To
The reference temperature to be used for estimating the saturation pressure of the condensible component. Should be near the range of saturation temperature expected

Po
The saturation pressure at To for the condensible component

CONV
Conversion factor to make the quantity XLAM/Rv/To dimensions less where XLAM is the latent heat of vaporization and Rv is the gas constant for the vapor. If XLAM is BTU/lb, Rv is FT-LB/°R and To is °R, CONV=778.
PHASE CHANGE

SUBROUTINE NAME: ABLATS

PURPOSE:
To provide a simple ablation (sublimation) capability for the SINDA user. The user constructs the 3-D network without considering the ablative. Then in $POSTTEMP he simulates 1-D ablative attachments by calling ABLATS. ABLATS constructs the 1-D network and solves it by implicit forward-backward differencing (Crank-Nicholson method) using the time step set by the execution subroutine. Separate ablation arrays (AA) must be used for each ABLATS call. Required working space is obtained from unused program common. Several ABLATS calls thereby share unused common. The user must call subroutine PNTABL (AA) in the OUTPUT CALLS to obtain ablation totals and temperature distribution.

RESTRICTIONS:
ABLATS must be called in POSTTEMP and may be used with any execution subroutine. Subroutines DIDEGI and NEWTR4 are called. All units must be consistent. The Fahrenheit system is required. Temperature varying material property arrays must not exceed 60 doublets. Bivariate material properties may be simulated by calling BVSPSA prior to ABLATS. Cross-sectional area is always considered unity. Thermal conductivity, Stefan-Boltzmann constant and density units must agree in area and length units.

CALLING SEQUENCE: ABLATS(AA(IC),R,CP,G,T,C)

where

- C is the capacitance location of the 3-D node attached to.
- T is the temperature location of the 3-D node attached to.
- G is the location of the material thermal conductivity or the starting location (integer count) of a doublet G vs T array.
- CP is the location of the material specific heat or the starting location (integer count) of a doublet C_p vs T array.
- R is the location of the material density or the starting location (integer count) of a doublet R vs T array.
- AA(IC) is the starting location of the ablation array which must be formatted as follows:
AA(IC)+1  the ablative line number, a user specified identification integer.
2  integer number of sublayers (NSL) desired, ABLATS subtracts from this the number of sublayers ablated.
3  the initial temperature of the material, ABLATS replaces this with the outer surface temperature, always in degrees F.
4  the impressed outer surface heating rate per unit area, radiation rates not included.
5  material thickness; this is replaced by the sublayer thickness.
6  surface area of the 3-D node attached to, need not be unity.
7  ablation temperature, degrees F.
8  heat of ablation.
9  Stefan-Boltzmann constant in consistent units.
10  surface emissivity
11  space "sink" temperature, degrees F.
12  SPACE,N  where N equals NSL + 4.

**NOTE:** The outer surface radiation loss is integrated over the time step.

**DYNAMIC STORAGE REQUIREMENTS:**

This subroutine requires 3* (NSL+1) dynamic storage core locations.
PHASE CHANGE

SUBROUTINE NAME: LQSLTR

PURPOSE:

This subroutine accounts for the phase change energy of a melting or solidifying material. The temperature limits for the reaction must be specified (over at least a 1 degree range) and the phase change energy supplied as a constant rate over the range (Btu/°F). The network is constructed to include the capacitance effects of the phase change material. The network solution subroutines are allowed to calculate incorrect answers based on capacitance effects only; a call to LQSLTR in POSTTEMP then performs a corrector operation to account for any phase change occurring (reversibility allowed) and returns corrected temperatures. The user is required to store the old temperature of the material (in POSTTEMP) and supply it as an argument to LQSLTR. This subroutine has a "D0" loop built in and can be applied to several sequential nodes at once.

RESTRICTIONS:

The number of sequential nodes that this subroutine is to be applied to must be supplied as the integer N. All other arguments must be or address data values.

CALLING SEQUENCE: LQSLTR(N, TL, TH, S(DV), C(DV), T0(DV), TN(DV))

where

- \( N \) is the integer number of nodes to be operated on
- \( TL \) is the low temperature of the range
- \( TH \) is the high temperature of the range
- \( S(DV) \) is the first value of the phase change energy rate
- \( C(DV) \) is the first value of the nodal capacitances
- \( T0(DV) \) is the first value of the old temperatures
- \( TN(DV) \) is the first value of the new temperatures
PHASE CHANGE

SUBROUTINE NAME: LQDVAP

PURPOSE:

This subroutine allows the user to simulate the addition of liquid to a node. The network data is prepared as though no liquid exists at the node and is solved that way by the network execution subroutine. Then LQDVAP, which must be called in POSTTEMP, corrects the nodal solution in order to account for the liquid. If the nodal temperature exceeds the boiling point of the liquid, it is set to the boiling point.

The excess energy above that required to reach the boiling point is calculated and considered as absorbed through vaporization. If the liquid is completely vaporized the subroutine deletes its operations. The method of solution holds very well for explicit solutions, but may introduce some error when large time steps are used with implicit solutions.

RESTRICTIONS:

This subroutine must be called in POSTTEMP.

CALLING SEQUENCE: LQDVAP (T,C,A(IC))

where
- T is the temperature location of the node.
- C is the capacitance location of the node.
- A + 1 contains the initial liquid weight.
- 2 contains the liquid specific heat.
- 3 contains the liquid vaporization temperature.
- 4 contains the liquid heat of vaporization.
- 5 receives the liquid vaporization rate (weight/time)
- 6 receives the liquid vaporization total (total weight)
- 7 contains the liquid initial temperature.
2.3 MATRIX SUBROUTINES

Input Format

Unless otherwise noted, the matrices require input as positive numbered arrays with integer number of rows and columns as the first two data values followed by floating point element values in row order.

Special Matrix Generation

<table>
<thead>
<tr>
<th>Subroutine</th>
<th>Description</th>
</tr>
</thead>
<tbody>
<tr>
<td>ZEROØ</td>
<td>Generates a matrix such that every element is zero.</td>
</tr>
<tr>
<td>ONES</td>
<td>Generates a matrix such that every element is one.</td>
</tr>
<tr>
<td>UNITY</td>
<td>Generates a square matrix such that the principal diagonal elements are unity and the remaining elements are zero.</td>
</tr>
<tr>
<td>SIGMA</td>
<td>Generates a square matrix such that all elements on and below the principal diagonal are unity and the remaining elements are zero.</td>
</tr>
<tr>
<td>GENALP</td>
<td>Generates a matrix such that every element is equal to a constant.</td>
</tr>
<tr>
<td>GENCØL</td>
<td>Generates a column matrix such that the first element is equal to X1 and the last element is equal to X2.</td>
</tr>
<tr>
<td>FULSYM</td>
<td>Forms a half symmetric matrix from a full square matrix.</td>
</tr>
<tr>
<td>SYMFUL</td>
<td>Forms a full square matrix from a half symmetric matrix.</td>
</tr>
<tr>
<td>SYMFRC</td>
<td>Forces symmetry upon a square matrix.</td>
</tr>
<tr>
<td>DIAG</td>
<td>Forms a full square matrix given a column or row matrix.</td>
</tr>
<tr>
<td>UNDIAG</td>
<td>Forms a row matrix from the diagonal elements of a square matrix.</td>
</tr>
<tr>
<td>DIAGAD</td>
<td>Adds the elements of a row matrix to the diagonal elements of a square matrix.</td>
</tr>
</tbody>
</table>

Elemental Operations

<table>
<thead>
<tr>
<th>Subroutine</th>
<th>Description</th>
</tr>
</thead>
<tbody>
<tr>
<td>ELEADD</td>
<td>Adds corresponding elements of two matrices [A] and [B] to form a third [Z] (Matrix addition).</td>
</tr>
<tr>
<td>ELESUB</td>
<td>Subtracts the corresponding elements of two matrices to form a third [Z] (Matrix subtraction).</td>
</tr>
</tbody>
</table>
ELEMUL Multiplies the corresponding elements of two matrices [A] and [B] to form a third [Z] (this is NOT matrix multiplication) ........................................ A-42

ELEDIV Divides the corresponding elements of two [A] and [B] matrices to form a third [Z] (this is NOT matrix division) ........................................ A-42

ELEINV Obtains the reciprocal of each element of matrix [A] and place it in the corresponding location of another matrix [Z] ........................................ A-42

EFSIN Generates the sine of each element of matrix [A] and places it in the corresponding location of another matrix [Z] ........................................ A-43

EFASN Generates the arcsine of each element of matrix [A] and places it in the corresponding location of another matrix [Z] ........................................ A-43

EFCOS Generates the cosine of each element of matrix [A] and places it in the corresponding location of another matrix [Z] ........................................ A-43

EFACS Generates the arccosine of each element of matrix [A] and places it in the corresponding location of another matrix [Z] ........................................ A-43

EFTAN Generates the tangent of each element of matrix [A] and places it in the corresponding location of another matrix [Z] ........................................ A-43

EFATN Generates the arctangent of each element of matrix [A] and places it in the corresponding location of another matrix [Z] ........................................ A-43

EFABS Generates the absolute value of each matrix [A] element ........................................ A-44

EFLLOG Generates the natural log of each [A] element ........................................ A-44

EFSQR Generates the square root of each matrix [A] element ........................................ A-44

EFEXP Generates the exponential of each matrix [A] element ........................................ A-44

EFPOW Generates the power of each matrix [A] element ........................................ A-44

ADDALP Adds a constant to every element in a matrix ........................................ A-45

ALPHAA Multiplies every element in a matrix by a constant ........................................ A-45

MATRIX Allows a constant to replace a specific matrix element ........................................ A-45
<table>
<thead>
<tr>
<th>SCALAR</th>
<th>Allows a specific matrix element to be placed into a constant location.</th>
<th>A-45</th>
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</thead>
<tbody>
<tr>
<td>MATADD</td>
<td>Adds a constant to a specific matrix element</td>
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Matrix Operations/Solutions

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<th>INVRSE</th>
<th>Inverts a square matrix</th>
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<tr>
<td>MULT</td>
<td>Multiplies two conformable matrices</td>
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<tr>
<td>TRANS</td>
<td>Forms the transpose ([Z]) from matrix ([A])</td>
<td>A-47</td>
</tr>
<tr>
<td>AABB</td>
<td>Sums two scaled matrices</td>
<td>A-47</td>
</tr>
<tr>
<td>BTAB</td>
<td>Performs the matrix operation ([B]^t [A][B])</td>
<td>A-48</td>
</tr>
<tr>
<td>BABT</td>
<td>Performs the matrix operation ([B][A][B]^t)</td>
<td>A-48</td>
</tr>
<tr>
<td>DISAS</td>
<td>Allows a user to operate on matrices in a partitioned manner by disassembling a submatrix ([Z]) from a parent matrix ([A]).</td>
<td>A-48</td>
</tr>
<tr>
<td>ASSMBL</td>
<td>Allows a user to operate on matrices in a partitioned manner by assembling a submatrix ([Z]) into a parent matrix ([A]).</td>
<td>A-48</td>
</tr>
<tr>
<td>C0LMLT</td>
<td>Multiplies each element in a column or row of matrix ([A]) by its corresponding element from the diagonal matrix ([V]) which is stored as a vector.</td>
<td>A-49</td>
</tr>
<tr>
<td>R0WMLT</td>
<td></td>
<td></td>
</tr>
<tr>
<td>SHIFT</td>
<td>Moves an entire matrix as is from one location to another.</td>
<td>A-49</td>
</tr>
<tr>
<td>REFLCT</td>
<td>Moves an entire matrix with the order of the column elements reversed from one location to another</td>
<td>A-49</td>
</tr>
<tr>
<td>SHUFL</td>
<td>Allows the user to reorder the size of a matrix as long as the total number of elements remains unchanged.</td>
<td>A-50</td>
</tr>
<tr>
<td>C0LMAX</td>
<td>Searches an input matrix to obtain the maximum or minimum values within each column.</td>
<td>A-50</td>
</tr>
<tr>
<td>C0LMIN</td>
<td></td>
<td></td>
</tr>
<tr>
<td>SYMREM</td>
<td>Allows the SINDA user to operate on a simple row/column of a half symmetric matrix.</td>
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<tr>
<td>SYMREP</td>
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<td></td>
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<tr>
<td>SYMDAD</td>
<td>Adds the elements of a vector array to the corresponding elements of the main diagonal of a half symmetric matrix.</td>
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<tr>
<td>SYMINV</td>
<td>Obtains the inverse of a half symmetric matrix.</td>
<td>A-51</td>
</tr>
</tbody>
</table>
POLMLT Multiplies a given number of nth order polynomial coefficients by a similar number of mth order polynomial coefficients. A-52

POLVAL Evaluates the polynomial for the input complex number X + iV, given a set of polynomial coefficients. A-52

PLYEVL Evaluates each polynomial for each X value, given a matrix with nth order polynomial coefficients and a column matrix of X values. A-52

POLSØV Calculates the complex roots, given a set of polynomial coefficients as the first row in a matrix. A-53

JACØBI Determines the eigenvalues and eigenvector associated with an input matrix [A]. A-53

Store and Recall

CALL Retrieves matrices on magnetic tape. A-54

FILE Stores matrices on magnetic tape. A-54

ENDMØP Used in conjunction with subroutines CALL and FILE. Causes all matrices from the logical 19 tape to be updated onto the logical 18 tape. A-55

LSTAPE Will output the name, problem number and size of every matrix stored on tape on logical 18. A-55

Applications

MØDES Solves a particular matrix dynamic vibration equation. A-56

MASS Generates an inertia matrix of a dynamic vibration system described in terms of deflections and rotations. A-57

STIFF Generates a stiffness matrix for a dynamic vibration system described in terms of deflections and rotations. A-58
SPECIAL MATRIX GENERATION

SUBROUTINE NAMES: ZERØ or ØNES

PURPOSE:

These subroutines generate a matrix [Z] such that every element is zero or one respectively.

RESTRICTIONS:

The matrix to be generated must contain exactly enough space in addition to having the integer number of rows and columns as the first two data values. The NR and NC arguments are the integer number of rows and columns respectively.

CALLING SEQUENCE:

ZERO(NR,NC,Z(IC))
or ØNES(NR,NC,Z(IC))

SUBROUTINE NAMES: UNITY or SIGMA

PURPOSE:

These are square matrix generation subroutines. UNITY generates a square matrix such that the main diagonal elements are one and all other elements are zero. SIGMA generates a square matrix such that all elements on and below the main diagonal are one and the remaining elements are zero.

RESTRICTIONS:

The matrix [Z] to be generated must contain exactly enough space in addition to having the integer number of rows and columns as the first two data values. The integer number of rows and columns are equal and must be input as the argument N.

CALLING SEQUENCE:

UNITY(N,Z(IC))
or SIGMA(N,Z(IC))

SUBROUTINE NAMES: GENALP or GENCOL

PURPOSE:

These are special matrix generation subroutines. GENALP will generate a matrix such that every element is equal to a constant C. GENCOL will generate a column matrix such that the first element is equal to X1 and the last element is equal to X2. The intermediate elements receive equally incremented values such that a linear relationship is established between row number and element value.

RESTRICTIONS:

The NR and NC arguments refer to the integer number of rows and columns respectively. X1, X2, and C must be floating point values. The generated matrices must contain exactly enough space in addition to having the integer number of rows and columns as the first two data values.

CALLING SEQUENCE:

GENALP(NR,NC,C,Z(IC))
or GENCOL(X1,X2,NR,Z(IC))
**SPECIAL MATRIX FORMULATION**

**SUBROUTINE NAMES:**  
**FULSYM** or **SYMFUL**

These subroutines allow the SINDA user to form a half symmetric matrix from a full square matrix or form a full square matrix from a half symmetric matrix, respectively. The arguments must address the matrix array integer count set by the preprocessor, the array lengths must be exact.

**RESTRICTIONS:**

The half symmetric matrix must be formatted as shown for subroutine **IRRADH** (Section 6.8) and the full square matrix must conform to the standard format.

**CALLING SEQUENCE:**  
**FULSYM**(*SM(IC),FM(IC))  
**SYMFUL**(*SM(IC),FM(IC))

Where *FM is the full matrix and *SM is the symmetric matrix.

**SUBROUTINE NAME:**  
**SYMFRC**

**PURPOSE:**

This subroutine may be used to force symmetry upon a square matrix. The main diagonal elements are untouched and all others are treated as follows:

\[ x = (a_{ij} + a_{ji}) / 2.0 \]
\[ a_{ij} = x; a_{ji} = x \]

**RESTRICTIONS:**

The addressed matrix must be square and formatted as described in Section 4.2.2.3

**CALLING SEQUENCE:**  
**SYMFRC(A(IC))**

**SUBROUTINE NAMES:**  
**DIAG** or **UNDIAG** or **DIAGAD**

**PURPOSE:**

Given a 1*1 or 1*N matrix [Y], subroutine **DIAG** forms a full square N*N matrix [Z]. The [Y] values are placed sequentially on the main diagonal of [Z] and all off diagonal elements are set to zero. Subroutine **UNDIAG** forms a 1*1 matrix [Y] from the diagonal elements of an N*N matrix [Z]. Subroutine **DIAGAD** adds the elements of a 1*N matrix [Y] to the diagonal elements of an N*N matrix [Z].

**RESTRICTIONS:**

Both matrices must have exactly enough space and contain their integer number of rows and columns as the first two data values.

**CALLING SEQUENCE:**  
**DIAG(V(IC),Z(IC))**  
**UNDIAG(Z(IC),V(IC))**  
**DIAGAD(V(IC),Z(IC))**
ELEMENTAL OPERATIONS

SUBROUTINE NAMES: ELEADD or ELESUB

PURPOSE:
These subroutines add or subtract the corresponding elements of two matrices respectively.

\[
[z]_{ij} = [a]_{ij} \pm [b]_{ij}
\]

RESTRICTIONS:
All matrices must be of identical size and have the integer number of rows and columns as the first two data values. The \([z]\) matrix may be overlayed into the \([a]\) or \([b]\) matrix.

CALLING SEQUENCE: ELEADD(\(A(IC), B(IC), Z(IC)\))
or ELESUB(\(A(IC), B(IC), Z(IC)\))

SUBROUTINE NAMES: ELEMUL or ELEDIV

PURPOSE:
These subroutines multiply or divide the corresponding elements of two matrices respectively.

\[
[z]_{ij} = [a]_{ij} \times [b]_{ij}
\]

RESTRICTIONS:
All matrices must be of identical size and have the integer number of rows and columns as the first two data values. The \([z]\) matrix may be overlayed into the \([a]\) or \([b]\) matrix.

CALLING SEQUENCE: ELEMUL(\(A(IC), B(IC), Z(IC)\))
or ELEDIV(\(A(IC), B(IC), Z(IC)\))

SUBROUTINE NAME: ELEINV

PURPOSE:
This subroutine obtains the reciprocal of each element of the \([a]\) matrix and places it in the corresponding element location of the \([z]\) matrix.

\[
z_{ij} = 1.0/a_{ij}
\]

RESTRICTIONS:
The matrices must be of identical size and have the integer number of rows and columns as the first two data values. The \([z]\) matrix may be overlayed into the \([a]\) matrix.

CALLING SEQUENCE: ELEINV(\(A(IC), Z(IC)\))
ELEMENTAL OPERATIONS

SUBROUTINE NAMES: EFSIN or EFASN

PURPOSE:
These subroutines perform elementary functions on all of the $[A]$ matrix elements as follows:

$$z_{ij} = \sin(a_{ij}) \quad \text{or} \quad z_{ij} = \arcsin(a_{ij})$$

RESTRICTIONS:
The matrices must be identical in size and have the integer number of rows and columns as the first two data values. The $[Z]$ matrix may be overlayed into the $[A]$ matrix.

CALLING SEQUENCE:
EFSIN(A(IC),Z(IC))

or
EFASN(A(IC),Z(IC))

SUBROUTINE NAMES: EFCOS or EFACS

PURPOSE:
These subroutines perform elementary functions on all of the $[A]$ matrix elements as follows:

$$z_{ij} = \cos(a_{ij}) \quad \text{or} \quad a_{ij} = \arccos(a_{ij})$$

RESTRICTIONS:
The matrices must be identical in size and have the integer number of rows and columns as the first two data values. The $[Z]$ matrix may be overlayed into the $[A]$ matrix.

CALLING SEQUENCE:
EFCOS(A(IC),Z(IC))

or
EFACS(A(IC),Z(IC))

SUBROUTINE NAMES: EFTAN or EFATN

PURPOSE:
These subroutines perform elementary functions on all of the $[A]$ matrix elements as follows:

$$z_{ij} = \tan(a_{ij}) \quad \text{or} \quad z_{ij} = \arctan(a_{ij})$$

RESTRICTIONS:
The matrices must be of identical size and have the integer number of rows and columns as the first two data values. The $[Z]$ matrix may be overlayed into the $[Z]$ matrix.

CALLING SEQUENCE:
EFTAN(A(IC),Z(IC))

or
EFATN(A(IC),Z(IC))
ELEMENTAL OPERATIONS

SUBROUTINE NAMES: EFABS or EFL\text{OG} or EFSQR

PURPOSE:

These subroutines perform elementary functions on all of the \([A]\) matrix elements as follows respectively:

\[
    z_{ij} = |a_{ij}| \quad \text{or} \quad z_{ij} = \log_e(a_{ij}) \quad \text{or} \quad a_{ij} = \sqrt{a_{ij}}
\]

RESTRICTIONS:

The matrices must be identical in size and have the integer number of rows and columns as the first two data values. All in the \([A]\) matrix must be positive for EFL\text{OG} or EFSQR.

CALLING SEQUENCE: 
EFABS(A(IC),Z(IC))
EFL\text{OG}(A(IC),Z(IC))
EFSQR(A(IC),Z(IC))

SUBROUTINE NAMES: EFEXP or EFP\text{OW}

PURPOSE:

These subroutines perform elementary functions on all of the \([A]\) matrix elements as follows:

\[
    z_{ij} = e^{a_{ij}} \quad \text{or} \quad z_{ij} = a_{ij}^\alpha
\]

RESTRICTIONS:

The matrices must be identical in size and have the integer number of rows and columns as the first two data values. The \([Z]\) matrix may be overlayed into the \([A]\) matrix. The exponent \(\alpha\) may be an integer or floating point number. However, if any elements in \([A]\) are negative then \(\alpha\) must be an integer.

CALLING SEQUENCE: 
EFEXP(A(IC),Z(IC))
or EFP\text{OW}(A(IC),\alpha,Z(IC))
ELEMENTAL OPERATIONS

SUBROUTINE NAMES: ADDALP or ALPHAA

PURPOSE:
To add a constant to or multiply a constant times every element in a matrix.

\[ z_{ij} = C + a_{ij} \quad \text{or} \quad z_{ij} = C \times a_{ij} \]

RESTRICTIONS:
The matrices must have exactly enough space and contain the integer number of rows and columns as the first two data values. C and all elements must be floating point numbers. The [Z] matrix may be overlayed into the [A] matrix.

CALLING SEQUENCE: ADDALP(C,A(IC),Z(IC))

or ALPHAA(C,A(IC),Z(IC))

SUBROUTINE NAMES: MATRIX or SCALAR or MATADD

PURPOSE:
The subroutine MATRIX allows a constant to replace a specific matrix element, subroutine SCALAR allows a specific matrix element to be placed into a constant location, and subroutine MATADD adds a constant to a specific matrix element. The integers I and J designate the row and column position of the specific element.

\[ z_{ij} = C \quad \text{or} \quad C = z_{ij} \quad \text{or} \quad z_{ij} = z_{ij} + C \]

RESTRICTIONS:
The matrix must have the integer number of rows and columns as the first two data values. Checks are made to insure that the identified element is within the matrix boundaries.

CALLING SEQUENCE: MATRIX(C,I,J,Z(IC))

or SCALAR(Z(IC),I,J,C)

or MATADD(C,I,J,Z(IC))
MATRIX OPERATIONS AND SOLUTIONS

SUBROUTINE NAME: INVRSE

PURPOSE:

To invert a square matrix.

\[ n \times n \quad n \times n = n \times n \]

given \([A] \), \([z] = [A]^{-1}\)

RESTRICTIONS:

The matrices must be square, identical in size and contain the integer number of rows and columns as the first two data values. The output matrix \([A]\) may be overlayed into the \([A]\) matrix.

CALLING SEQUENCE: INVRSE(A(IC),Z(IC))

DYNAMIC STORAGE REQUIREMENTS:

This subroutine requires \(n\) dynamic storage allocations.

SUBROUTINE NAME: MULT

PURPOSE: To multiply two conformable matrices together.

\[ m \times n \quad m \times p \quad p \times n \]

\([z] = [A] \times [B], \quad z_{ij} = a_{ik} \times b_{kj}\)

RESTRICTIONS:

The matrices must have exactly enough space and contain their integer number of rows and columns as the first two data values. If \([A]\) and \([B]\) are square, \([z]\) may be overlayed into either of them.

CALLING SEQUENCE: MULT(A(IC),B(IC),Z(IC))

DYNAMIC STORAGE REQUIREMENTS:

This subroutine requires \(n \times m\) dynamic storage locations.
MATRIX OPERATIONS AND SOLUTIONS

SUBROUTINE NAME: TRANS

PURPOSE: Given a matrix \([A]\) form its transpose as \([Z]\)

RESTRICTIONS:
Both matrices must have exactly enough space and contain their integer number of rows and columns as the first two data values. The output matrix \([Z]\) may be overlayed into the \([A]\) matrix.

CALLING SEQUENCE: TRANS(A(IC),Z(IC))

DYNAMIC STORAGE REQUIREMENTS:
This subroutine requires \(n \times m\) dynamic storage locations.

SUBROUTINE NAME: AABB

PURPOSE: To sum two scaled matrices:

\[
[Z] = C1[A] + C2[B], \quad Z_{ij} = C1a_{ij} + C2b_{ij}
\]

RESTRICTIONS:
All matrices must be of identical size, contain exactly enough space and contain the integer number of rows and columns as the first two data values. The output matrix \([Z]\) may be overlayed into either of the input matrices.

CALLING SEQUENCE: AABB(C1,A(IC),C2,B(IC),Z(IC))
MATRIX OPERATIONS AND SOLUTIONS

SUBROUTINE NAMES: BTAB or BABT

PURPOSE:
To perform the following matrix operations, respectively:

\[ \begin{bmatrix} Z \end{bmatrix} = \begin{bmatrix} B \end{bmatrix}^T \begin{bmatrix} A \end{bmatrix} \begin{bmatrix} B \end{bmatrix} \]

or

\[ \begin{bmatrix} Z \end{bmatrix} = \begin{bmatrix} B \end{bmatrix} \begin{bmatrix} A \end{bmatrix}^T \begin{bmatrix} B \end{bmatrix} \]

RESTRICTIONS:
The matrices must be conformable, contain exactly enough space and contain the integer number of rows and columns as the first two data values. Subroutines MULT and TRANS are called on.

CALLING SEQUENCE: BTAB(A(IC), B(IC), Z(IC))

or BAPT(A(IC), B(IC), Z(IC))

DYNAMIC STORAGE REQUIREMENTS:
Due to subroutines MULT and TRANS this subroutine temporarily requires 2*m*n+6 dynamic locations.

SUBROUTINE NAMES: DISAS or ASSMBL

PURPOSE:
These subroutines allow a user to operate on matrices in a partitioned manner by disassembling a submatrix \([z]\) from a parent matrix \([A]\) or assembling a submatrix \([z]\) into a parent matrix \([A]\).

RESTRICTIONS:
The \(I\) and \(J\) arguments are integers which identify (by row and column number respectively) the upper left hand corner position of the submatrix within the parent matrix. All matrices must have exactly enough space and contain the integer number of rows and columns as the first two data values. The \(NR\) and \(NC\) arguments are the integer number of rows and columns respectively of the disassembled submatrix. If the submatrix exceeds the bounds of the parent matrix an appropriate error message is written and the program terminated.

CALLING SEQUENCE: DISAS(A(IC), I, J, NR, NC, Z(IC))

or ASSMBL(Z(IC), I, J, A(IC))
MATRIX OPERATIONS AND SOLUTIONS

SUBROUTINES NAMES: C0LMLT or R0WMLT

PURPOSE:
To multiply each element in a column or row of matrix [A] by its corresponding element from the matrix [V] which is conceptually a diagonal matrix but stored as a vector; i.e., 1*N or N*1 matrix. The matrix [Z] is the product.

RESTRICTIONS:
The matrices must have exactly enough space and contain the integer number of rows and columns as the first two data values. The matrices being multiplied must be conformable.

CALLING SEQUENCE: C0LMLT(A(IC), V(IC), Z(IC))

or R0WMLT(V(IC), A(IC), Z(IC))

SUBROUTINE NAMES: SHIFT or REFLCT

PURPOSE:
These subroutines may be used to move an entire matrix from one location to another. SHIFT moves the matrix exactly as is and REFLCT moves it and reverses the order of the elements within each column. The last element in each column becomes the first and the first becomes the last, etc.

RESTRICTIONS:
The matrices must be of identical size and the integer number of rows and columns must be the first two data values. The [Z] matrix may be overlaid into the [A] matrix.

CALLING SEQUENCE: SHIFT(A(IC), Z(IC))

or REFLCT(A(IC), Z(IC))

DYNAMIC STORAGE REQUIREMENTS:
REFLCT uses three dynamic storage locations plus an additional one for each row.
**MATRIX OPERATIONS AND SOLUTIONS**

**SUBROUTINE NAME:** SHUFL

**PURPOSE:**

This subroutine allows the user to reorder the size of a matrix as long as the total number of elements remains unchanged. The row order input matrix \([A]\) is transposed to achieve column order and then reformed as a vector by sequencing the columns in ascending order. This vector is then reformed into a column order matrix by taking a column at a time sequentially from the vector. The newly formed column matrix is then transposed and output as the row order matrix \([z]\).

**RESTRICTIONS:**

The matrices must be identical in size and have their respective integer number of rows and columns as the first two data values. The number of rows times columns for \([A]\) must equal the number of rows times columns of \([z]\).

**CALLING SEQUENCE:** SHUFL(A(IC),Z(IC))

**SUBROUTINE NAMES:** COLMAX or COLMIN

**PURPOSE:**

These subroutines search an input matrix to obtain the maximum or minimum values within each column respectively. These values are output as a single row matrix \([A]\) having as many columns as the input matrix \([A]\).

**RESTRICTIONS:**

Each matrix must have its integer number of rows and columns as the first two data values.

**CALLING SEQUENCE:** COLMAX(A(IC),Z(IC))

or COLMIN(A(IC),Z(IC))
MATRIX OPERATIONS AND SUBROUTINES

SUBROUTINE NAMES: SYMREM or SYMREP

PURPOSE:

These subroutines allow the SINDA user to operate on a single row/column of a half symmetric matrix. SYMREM will remove a particular row/column from the half symmetric matrix and place it into an array of the exact length to hold it. SYMREP will take an array and replace it into a specific row/column of the half symmetric matrix.

RESTRICTIONS:

The half symmetric matrix must be formatted as shown for subroutine IRRADI in Section 4.2.2.3. The integer K must designate the row/column to be operated on. If K is an integer zero, the main diagonal will be removed or replaced.

CALLING SEQUENCE: SYMREM(K,SM(IC),A(IC)) or SYMREP(K,A(IC),SM(IC))

SUBROUTINE NAME: SYMDAD

PURPOSE:

This subroutine will add the elements of a vector array to the corresponding elements of the main diagonal of a half symmetric matrix. If any of the elements is less than zero, they are set to zero.

RESTRICTIONS:

The half symmetric matrix must be formatted as shown for subroutine IRRADI in Section 6.8. The vector array must be input as a positive array and be the same length as the matrix order.

CALLING SEQUENCE: SYMDAD(VA(IC),SM(IC))

SUBROUTINE NAME: SYMINV

PURPOSE:

This subroutine obtains the inverse of a half symmetric matrix matrix which is also symmetric and returns it in the same area as the input matrix. This subroutine is called internally by subroutines SCRPFA, IRRADI and SLRADI.

RESTRICTIONS:

This subroutine contains no error checks, exercise extreme caution when using it.

CALLING SEQUENCE: SYMINV(A(DV),N)

Where A(DV) addresses the 1,1 element and N is the matrix order.
MATRIX OPERATIONS AND SOLUTIONS

SUBROUTINE NAME: POLMLT

PURPOSE:

This subroutine performs the multiplication of a given number of nth order polynomial coefficients by a similar number of mth order polynomial coefficients. The polynomials must be input as matrices with the number of rows equal and each row receives the following operation:

\[(c_1, c_2, c_3, \ldots, c_k) = (a_1, a_2, \ldots, a_n) \times (b_1, b_2, \ldots, b_m), k = m+n-1\]

RESTRICTIONS:

The matrices must have exactly enough space and contain their integer number of rows and columns as the first two data values.

CALLING SEQUENCE: POLMLT(A(IC), B(IC), C(IC))

SUBROUTINE NAME: POLVAL

PURPOSE:

Given a set of polynomial coefficients as the first row of matrix [A], this subroutine evaluates the polynomial for the input complex number \(X + iY\). The answer is returned as \(U + iV\).

RESTRICTIONS:

[A] may be m*n but only the first row is evaluated.

CALLING SEQUENCE: POLVAL(A(IC), X, Y, U, V)

SUBROUTINE NAME: PLYEVL

PURPOSE:

Given a matrix [A] containing an arbitrary number, NRA, of the nth order polynomial coefficients and a column matrix [X] containing an arbitrary number, NRX, of X values, this subroutine evaluates each polynomial for each X value. The answers are output as a matrix [Z] of size NRX*NRA. Each set of polynomial coefficients in [A] is a row in ascending order. An X value evaluated for the polynomial creates a row in [Z] where the column number agrees with the polynomial row number.

RESTRICTIONS:

The matrices must have exactly enough space and contain their integer number of rows and columns as the first two data values.

CALLING SEQUENCE: PLYEVL(A(IC), X(IC), Z(IC))
MATRIX OPERATIONS AND SOLUTIONS

**SUBROUTINE NAME:** POLSOV

**PURPOSE:**

Given a set of polynomial coefficients as the first row in matrix \([A]\), size \((m,n+1)\), this subroutine calculates the complex roots which are returned as matrix \([Z]\), size \((n,2)\). Column 1 contains the real part and column 2 the imaginary part of the roots.

**RESTRICTIONS:**

This subroutine presently is limited to \(n = 20\). It internally calls on RTPOLY and utilizes some double precision.

**CALLING SEQUENCE:** POLSOV \((A(IC), Z(IC))\)

**SUBROUTINE NAME:** JACOBI

**PURPOSE:**

This subroutine will find the eigenvalues \([E]\) and eigenvector matrix \([Z]\) associated with an input matrix \([A]\).

\[
\begin{bmatrix}
[A] & [Z] = [Z] & [E]
\end{bmatrix}
\]

**RESTRICTIONS:**

The matrices must have exactly enough space and contain their integer number of rows and columns as the first two data values. Note that matrix \([E]\) is a diagonal matrix but is stated as a vector.

**CALLING SEQUENCE:** JACOBI \((A(IC), E(IC), Z(IC))\)

**DYNAMIC STORAGE REQUIREMENTS:**

This subroutine requires \(2*n*n+6\) dynamic storage locations.
The ability to store and retrieve matrices from tape is easily achieved through the use of the FILE and CALL subroutines. Matrices are identified by an alphanumeric name, integer problem number and the core address of or for the matrix. The CALL subroutine searches the Matrix Input Tape and brings the desired matrix into core. The FILE subroutine writes a matrix onto the Matrix Output Tape. Subroutine ENDMØP causes all matrices from the Matrix Output Tape to be updated onto the Matrix Input Tape. In case of duplicate matrices, the one from the Output Tape replaces the one on Input Tape. A matrix which has been filed cannot be called until an ENDMØP operation has been performed. To create a new tape the user merely sets control constant NØCØPY nonzero and has a scratch tape mounted for the Input Tape. The user should check the section on control cards and deck setup to determine control card requirements.

SUBROUTINE NAMES: CALL or FILE

PURPOSE:

To allow the user to retrieve or store matrices on magnetic tape as described above. The H argument must be a six-character alphanumeric word and N must be an integer number, both of which are used to identify the matrix.

RESTRICTIONS:

See above. The matrix must have exactly enough space and contain the integer number of rows and columns as the first two data values.

CALLING SEQUENCE: CALL(H,N,A(IC))

or FILE(A(IC),H,N)

DYNAMIC STORAGE REQUIREMENTS:

Each of these routines requires 256 words of dynamic storage.
STORE AND RECALL

SUBROUTINE NAMES: ENDMØP or LSTAPE

PURPOSE:

Subroutine ENDMØP should be used in conjunction with subroutines CALL and FILE; see above. It causes matrices which have been filed by FILE on the Matrix Output Tape to be updated onto the Matrix Input Tape. A call to subroutine LSTAPE will cause the output of the name, problem number and size of every matrix stored on the Matrix Input Tape.

RESTRICTIONS:

See above.

CALLING SEQUENCE: ENDMØP

or LSTAPE

DYNAMIC STORAGE REQUIREMENTS:

Each of these routines requires 256 words of dynamic storage.
APPLICATION -- DYNAMIC VIBRATION

SUBROUTINE NAME: MOPES

PURPOSE:

This subroutine solves the following dynamic vibration equation

\[ [A] \cdot [Z] = [B] \cdot [Z] \cdot \frac{1}{2} \cdot \frac{1}{W} \]

where \([A]\) is the input inertia matrix associated with the kinetic energy and \([B]\) is the input stiffness matrix associated with the strain energy. \([Z]\) is the output eigenvector matrix associated with the frequencies of vibration \(W\), which are output in radians/sec as \([R]\) and in cycles/sec as \([C]\), both \([R]\) and \([C]\) are \(n\times n\) diagonal matrices but stored as vectors.

RESTRICTIONS:

The matrices must have exactly enough space and contain their integer number of rows and columns as the first two data values. Subroutine JACOBI is called on.

CALLING SEQUENCE: MOPES(A(IC),B(IC),Z(IC),R(IC),C(IC))

DYNAMIC STORAGE REQUIREMENTS:

This subroutine requires \(3\times n\times n+9\) dynamic storage locations. An amount equal to \(2\times n\times n+6\) of these locations is required by subroutine JACOBI.
APPLICATION -- DYNAMIC VIBRATION

SUBROUTINE NAME: MASS

If a dynamic vibration problem is referred to a set of coordinates consisting of the deflections, $\xi_i$, and the rotations, $\theta_i$, at $N$ collocation points along the beam under consideration, then this subroutine generates the $2N \times 2N$ inertia matrix $[A]$ which appears in the following expression for kinetic energy:

$$T = \frac{1}{2} \begin{bmatrix} \xi_1 & \ldots & \xi_n & \dot{\xi}_1 & \ldots & \dot{\xi}_n & \theta_1 & \ldots & \theta_n \end{bmatrix} [A] \begin{bmatrix} \xi_1 \\ \vdots \\ \xi_n \\ \theta_1 \\ \vdots \\ \theta_n \end{bmatrix}$$

RESTRICTIONS:

The mass and inertia data input to this subroutine are to be supplied as piecewise continuous slices; however, these arrays may be of arbitrary size and different in length from each other. The number of collocation points, $N$, which determines the ultimate size, $2N \times 2N$, of the output inertia matrix, is also chosen arbitrarily.

CALLING SEQUENCE: MASS$(X(IC), DMPL(IC), RIPL(IC), CM(IC), A(IC))$

where $X$ is the matrix $(N \times 1)$ of collocation points referred to an arbitrary origin.

$DMPL$ is the matrix $(NDM \times 4)$ of distributed mass per unit length slices, where
- Col 1 is the location of the rear of a slice.
- Col 2 is the location of the front of a slice.
- Col 3 is the mass value at the rear of the slice.
- Col 4 is the mass value at the front of the slice.

$RIPL$ is the matrix $(NRI \times 4)$ of distributed rotary inertia per unit length slices. The columns here are similar to $DMPL$.

$CM$ is the matrix $(NCM \times 4)$ of concentrated mass items, where
- Col 1 is the attach point location for each item.
- Col 2 is the mass at this location.
- Col 3 is the location of its center of gravity.
- Col 4 is the moment of inertia about the C. or G.

$A$ is the output $(2N \times 2N)$ inertia matrix.

NOTE: Having application to $DMPL$, $RIPL$ and $CM$, it is noted that the location of the values may not go beyond the limits of the collocation points in either direction.

A-57
SUBROUTINE NAME: STIFF

If a dynamic vibration problem is referred to a set of coordinates consisting of the deflections, $\xi_i$, and the rotations, $\theta_i$, at N collocation points along the beam under consideration, then this subroutine generates the 2N by 2N stiffness matrix $[K]$ which appears in the following expression for the strain energy:

$$U = \frac{1}{2} \left\{ \xi_1 \ldots \xi_n \theta_1 \ldots \theta_n \right\} [K] \left\{ \xi_1 \ldots \xi_n \theta_1 \ldots \theta_n \right\}$$

RESTRICTIONS:

The stiffness and shear data input to this subroutine are to be supplied as piecewise continuous slices; however, these arrays may be of arbitrary size and different in length from each other. The number of collocation points, N, which determine the ultimate size, 2N by 2N, of the output stiffness matrix, is also chosen arbitrarily.

CALLING SEQUENCE: STIFF(X(IC),EI(IC),GA(IC),K(IC))

where $X$ is the matrix (N x 1) of collocation points referred to an arbitrary origin.

$EI$ is the matrix (NEI x 4) of bending stiffness slices, where
Col 1 is the location of the rear of a slice.
Col 2 is the location of the front of a slice.
Col 3 is the stiffness value at the rear of a slice.
Col 4 is the stiffness value at the front of a slice.

$GA$ is the matrix (NGA x 4) of shear stiffness slices, where
the columns here are similar to those for the EI distribution.

$K$ is the output stiffness matrix size 2N by 2N.

NOTE: Having application to $EI$ and $GA$, it is noted that the location of the values may not go beyond the limits of the collocation points in either direction.
2.4 INTERPOLATION/EXTRAPOLATION SUBROUTINES

Lagrangian Interpolation

LAGRAN Uses one doublet array. A-61
LGRNDA Uses two singlet arrays A-61

Linear Interpolation - Single Variable

D1DEG1 Uses one doublet array. A-62
POL Uses one array with independent variables followed by dependent variables A-63
D1D1DA Uses two singlet arrays A-62
D1D1WM Uses D1DEG1 and multiplies the interpolation by the Z value A-64
D11MDA Uses D1D1DA and multiplies the interpolation by the Z value A-64
D1MDG1 Uses the arithmetic mean of two input values as the independent variable; uses a doublet array A-64
D1M1DA Same as D1MDG1 except two singlet arrays are used A-64
D1M1WM Uses D1MDG1 and multiplies the interpolation by the Z value A-64
D1M1MD Uses D1M1DA and multiplies the interpolation by the Z value A-64
D1DG1I Performs interpolation on an array of X's to obtain an array of Y's A-65
D1DIM1 Identical to D1DG1I, D1DIM and D1DIM1, except for the use of singlet arrays and call on D1D1DA A-65
D1MDI These are indexed subroutines which use the arithmetic mean of two input values as the independent variable A-66
D1DIM Identical to D1MDI, D1DIM1, D1DIM, and D1DIM1, except for the use of singlet arrays and call on D1D1DA A-66

Linear Interpolation - Two Single Variables

CVQ1HT Performs two single variable linear interpolations A-66
CVQ1WM

Parabolic Interpolation - Single Variable

D1DEG2 Uses LAGRAN and a doublet array A-67
D1D2DA Uses LGRNDA and two singlet arrays A-67
D1D2WM Uses LAGRAN and multiplies the interpolation by the Z value A-67
D12MDA Uses LGRNDA and multiplies the interpolation by the Z value A-67
D1MDG2 Uses the arithmetic mean of two input values as independent variable; uses doublet array A-67
D1M2DA Same as D1MDG2 except two single arrays are used A-68
D1M2WM Uses D1MDG2 and multiplies the interpolation by the Z value A-68
D1M2MD Uses D1M2DA and multiplies the interpolation by the Z value A-68
Cyclical Interpolation Arrays

D11CYL \text{Reduces core storage requirements and uses linear interpolation.} \text{A-69}

DA11CY \text{Identical to D11CYL and DA11CY except that parabolic interpolation is used.} \text{A-69}

D12CYL \text{Identical to D11CYL and DA11CY except that parabolic interpolation is used.} \text{A-69}

DA12CY \text{Identical to D11MCY and DA11MC except that parabolic interpolation is used.} \text{A-70}

D11MCY \text{Identical to D12CYL and DA12CY except that parabolic interpolation is multiplied by the value in address Z.} \text{A-70}

DA11MC \text{Identical to D11MCY and DA11MC except that parabolic interpolation is used.} \text{A-70}

Point Slope Interpolations

GSL0PE \text{Generates a slope array so that point slope interpolation can be used.} \text{A-71}

PSINTR \text{Point slope interpolation.} \text{A-71}

PSNTWM

Bivariate Interpolations

BVSPSA \text{Uses an input Y argument to address a bivariate array.} \text{A-72}

BVSPDA \text{Constructs a bivariate array of Y's versus X and Z from an input array of Z's versus X and Y.} \text{A-72}

BVTRN1 \text{Performs bivariate linear interpolation.} \text{A-73}

BVTRN2 \text{Performs bivariate parabolic interpolation.} \text{A-73}

D2DEG1 \text{Uses D2DEG1 and multiplies the interpolation by the W value.} \text{A-73}

D2D2WM \text{Uses D2DEG2 and multiplies the interpolation by the W value.} \text{A-73}

D2MXD1 \text{Identical to D2DEG1 and D2DEG2 except that the arithmetic mean of two X values is used as the X independent variable.} \text{A-74}

D2MXD2 \text{Identical to D2DEG1 and D2DEG2 except that the arithmetic mean of two X values is used as the X independent variable.} \text{A-74}

D2MX1M \text{Identical to D2D1WM and D2D2WM except that the arithmetic mean of two X values is used as the X independent variable.} \text{A-74}

D2MX2M

Trivariate Interpolations

D3DEG1 \text{Performs trivariate linear interpolation.} \text{A-75}

D3D1WM

Linear Extrapolation

LTRATE \text{Linearly extrapolates a new guess on the basis of Zero error.} \text{A-75}

A-60
The following are the formats for bivariant and trivarant arrays.

**Bivariate**

This type of array is used to represent a function of two independent variables: \( Z = (X,Y) \). Data values for a bivariate array are input in the following order:

\[
\begin{align*}
&n, \ X_1, \ X_2, \ldots, \ X_n \\
&Y_1, \ Z_{11}, \ Z_{12}, \ldots, \ Z_{1n} \\
&Y_2, \ Z_{21}, \ Z_{22}, \ldots, \ Z_{2n} \\
&\vdots \\
&Y_m, \ Z_{m1}, \ Z_{m2}, \ldots, \ Z_{mn}
\end{align*}
\]

where: \( n = \) Number of \( X \) values (integer)

\( m = \) Number of \( Y \) values (this value is not input explicitly)

\( Z_{ji} = f(X_i, Y_j); \) \( X, Y, \) & \( Z = \) floating point values

\( X_i \) (\( i = 1, 2, \ldots, n \)) is strictly increasing in \( i \).

\( Y_j \) (\( j = 1, 2, \ldots, m \)) is strictly increasing in \( j \).

The value of \( m \) is not input explicitly because the value of \( n \) (input as the first data value) and the number of points (generated by the preprocessor) are sufficient to define the location of any element in the array.

**Trivariate Array**

This type of array may be thought of as two or more bivariate arrays, where each bivariate array is associated with a third independent variable. Trivariate arrays are used to represent functions of the form \( F = f(X,Y,Z) \) for the purpose of evaluating such functions by interpolation. The data values in a trivariate array are input in the following order:

\[
\begin{align*}
&N_{X1}, N_{Y1}, Z_1, X_1, X_2, \ldots, X_n \\
&Y_1, F_{11}, F_{12}, \ldots, F_{1n} \\
&Y_2, F_{21}, F_{22}, \ldots, F_{2n} \\
&\vdots \\
&Y_m, F_{m1}, F_{m2}, \ldots, F_{mn} \\
&N_{X2}, N_{Y2}, Z_2, X_1, X_2, \ldots, X_j \\
&Y_1, F_{11}, F_{12}, \ldots, F_{1j} \\
&Y_2, F_{21}, F_{22}, \ldots, F_{2j} \\
&\vdots \\
&Y_k, F_{k1}, F_{k2}, \ldots, F_{kj} \\
&N_{X3}, N_{Y3}, Z_3, \ldots, \ldots, \ldots
\end{align*}
\]

A trivariate array may contain as many bivariate "sheets" as desired. The number of \( X \) and \( Y \) values in each sheet must be specified as integers \( N_X \) and \( N_Y \), respectively. \( N_X \) and \( N_Y \) need not be the same for all sheets.
LAGRANGIAN INTERPOLATION

SUBROUTINE NAMES: LAGRN or LGRNDA

PURPOSE:

These subroutines perform Lagrangian interpolation of up to order 50. The first requires one doublet array of \( x, y \) pairs while the second requires two singlet arrays, one of \( x' \)s and the other of \( y' \)s. They contain an extrapolation feature such that if the \( x \) value falls outside the range of the independent variable the nearest dependent \( y \) variable value is returned and no error is noted.

\[
y = P_n(x) = \sum_{k=0}^{n} y_k \prod_{i=0, i\neq k}^{n} \frac{x - x_i}{x_k - x_i}, \quad n = 1,2,3,...,50\text{max}.
\]

RESTRICTIONS:

All values must be floating point except \( N \) which is the order of interpolation plus one and must be an integer. The independent variable values must be in ascending order.

CALLING SEQUENCE:

LAGRN\((x,y,A(IC),N)\)

or

LGRNDA\((x,y,AX(IC),AY(IC),Y)\)

NOTE:

A doublet array is formed as follows:

\[
X_1, Y_1, X_2, Y_2, X_3, Y_3, \ldots, X_N, Y_N
\]

and singlet arrays are formed as follows:

\[
X_1, X_2, X_3, \ldots, X_N
\]

\[
Y_1, Y_2, Y_3, \ldots, Y_N
\]
LINEAR INTERPOLATION - SINGLE VARIABLE

SUBROUTINE NAME: D1DEG1

PURPOSE:

This subroutine performs single variable linear interpolation on a doublet array of X,Y pairs.

RESTRICTIONS:

All values must be floating point numbers. The X independent variable values in the doublet array must be in ascending order.

CALLING SEQUENCE: D1DEG1(X,A(IC),Y)

where:  
X = Input value of independent variable  
A = Doublet array of X,Y pairs  
Y = Output value of dependent variable

SUBROUTINE NAME: D1D1DA

PURPOSE:

This subroutine performs single variable linear interpolation on a pair of singlet arrays containing corresponding values of X and Y.

RESTRICTIONS:

All values must be floating point numbers. The X independent variable values in the AX array must be in ascending order. The number of values in the AX and AY arrays must be the same.

CALLING SEQUENCE: D1D1DA(X,AX(IC),AY(IC),Y)

where:  
X = Input value of the independent variable  
AX = Singlet array of X values  
AY = Singlet array of Y values corresponding to the X values in AX  
Y = Output value of the dependent variable
FUNCTION NAME: POL

PURPOSE:

This function subroutine performs single variable linear interpolation on a single array consisting of all the independent variables followed by all the dependent variables. The first location of the array contains the number of independent variables, the second contains an integer 1 (at the start) followed by all the independent variables and all the dependent variables. POL is useful for performing single variable interpolation on curves that are not type zero curves that are set up during the preprocessing phase.

RESTRICTIONS:

The first location must contain the number of independent variables and the second curve location contains the integer 1. The independent variables are next followed by the dependent variables. Note that POL is a function.

CALLING SEQUENCE: POL (A,X)

Where A is the array location

X is the value of the independent variable

Since POL is a function it must appear on the right of the equal of a Fortran statement.
LINEAR INTERPOLATION - SINGLE VARIABLE

SUBROUTINE NAMES: D1D1WM or D11MDA

PURPOSE:

These subroutines perform single variable linear interpolation by calling on D1DEG1 or D1D1DA respectively. However, the interpolated answer is multiplied by the values addressed as Z prior to being returned as Y.

RESTRICTIONS:

Same as D1DEG1 or D1D1DA and Z must be a floating point number.

CALLING SEQUENCE: 

D1D1WM(X, A(IC), Z, Y)

or D11MDA(X, AX(IC), AY(IC), Z, Y)

SUBROUTINE NAMES: D1MDG1 or D1M1DA

PURPOSE:

These subroutines use the arithmetic mean of two input values as the independent variable for linear interpolation. They require a doublet or two singlet arrays respectively.

RESTRICTIONS:

See D1DEG1 or D1D1DA as they are called on respectively.

CALLING SEQUENCE:

D1MDG1(X1, X2, A(IC), Y)

or D1M1DA(X1, X2, AX(IC), AY(IC), Y)

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LINEAR INTERPOLATION - SINGLE VARIABLE

SUBROUTINE NAMES: D1M1WM or D1M1MD

PURPOSE:

These subroutines use the arithmetic mean of two input values as the independent variable for linear interpolation. The interpolated answer is multiplied by the Z value prior to being returned as Y.

RESTRICTIONS:

Same as D1MDG1 or D1M1DA and Z must be a floating point number.

CALLING SEQUENCE: D1M1WM(X1,X2,A(IC),Z,Y) or D1M1MD(X1,X2,A(IC),A(Y(IC)),Z,Y)

SUBROUTINE NAMES: D1DG1I or D1D1IM or D1D1MI

PURPOSE:

These subroutines perform single variable linear interpolation on an array of X's to obtain an array of Y's. D1D1IM multiplies all interpolated values by a constant Z value while D1D1MI allows a unique Z value for each X value. They all call on D1DEG1.

RESTRICTIONS:

The number of input X's must be supplied as the integer N and agree with the number of Y and Z locations where applicable. Z values must be floating point numbers.

CALLING SEQUENCE: D1DG1I(N,X(DV),A(IC),Y(DV))

or D1D1IM(N,X(DV),A(IC),Z,Y(DV))

or D1D1MI(N,X(DV),A(IC),Z(DV),Y(DV))

SUBROUTINE NAMES: D11DAI or D11DIM or D11MDI

PURPOSE:

These subroutines are virtually identical to D1DG1I, D1D1IM and D1D1MI respectively. The difference is that they require singlet arrays for interpolation and call on D1IDA.

RESTRICTIONS:

Same as D1DG1I, D1D1IM and D1D1MI.

CALLING SEQUENCE: D11DAI(N,X(DV),A(IC),A(Y(IC)),Y(DV))

or D11DIM(N,X(DV),A(IC),A(Y(IC)),Z,Y(DV))

or D11MDI(N,X(DV),A(IC),A(Y(IC)),Z(DV),Y(DV))
LINEAR INTERPOLATION – SINGLE VARIABLE/TWO SINGLE VARIABLES

SUBROUTINE NAMES: D1IMD1 or D1IMWM or D1IMIM

PURPOSE:

These are indexed subroutines which use the arithmetic mean of two input values as the independent variable for linear interpolation. The array of answers (y) produced are left as is (D1IMD1), are all multiplied by a single factor (D1IMWM), or each answer is multiplied by a separate factor.

RESTRICTIONS:

The interpolation array addressed must have an even number of input values and the independent variables must be in ascending order. These routines call up D1D1WM. N is the number of times the operation is to be performed.

CALLING SEQUENCE:

D1IMD1(N,X1(DV),X2(DV),A,Y(DV))

or D1IMWM(N,X1(DV),X2(DV),A,Z,Y(DV))

or D1IMIM(N,X1(DV),X2(DV),A,Z(DV),Y(DV))

LINEAR INTERPOLATION – TWO SINGLE VARIABLES

SUBROUTINE NAMES: CVQ1HT or CVQ1WM

PURPOSE:

These subroutines perform two single variable linear interpolations. The interpolation arrays must have the same independent variable X and dependent variables of, let’s say, R(X) and S(X). Additional arguments of Z, Z and T complete the data values. The post interpolation calculations are respectively:

\[ Y = S(X) \times (R(X) - T) \]

or \[ Y = Z \times S(X) \times (R(X) - T) \]

RESTRICTIONS:

Interpolation arrays must be of the doublet type and have a common independent variable. All values must be floating point numbers.

CALLING SEQUENCE:

CVQ1HT(X, AR(IC), AS(IC), T, y)

or CVQ1WM(X, AR(IC), AS(IC), T, Z, y)
PARABOLIC INTERPOLATION - SINGLE VARIABLE

SUBROUTINE NAMES: D1DEG2 or D1D2DA

PURPOSE:

These subroutines perform single variable parabolic interpolation. The first requires a double array of \( X, Y \) pairs while the second requires singlet arrays of \( X \) and \( Y \) values. They call on subroutines LAGRAN and LGRNDA respectively.

RESTRICTIONS:

See LAGRAN or LGRNDA respectively.

CALLING SEQUENCE:

D1DEG2(\( X, A(IC), Y \))

or

D1D2DA(\( X, AX(IC), AY(IC), Y \))

SUBROUTINE NAMES: D1D2WM or D12MDA

PURPOSE:

These subroutines perform single variable parabolic interpolation by calling on LAGRAN or LGRNDA respectively. However, the interpolated answer is multiplied by the value addressed as \( Z \) prior to being returned as \( Y \).

RESTRICTIONS:

Same as LAGRAN or LGRNDA and \( Z \) must be a floating point number.

CALLING SEQUENCE:

D1D2WM(\( X, A(IC), Z, Y \))

or

D12MDA(\( X, AX(IC), AY(IC), Z, Y \))

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PARABOLIC INTERPOLATION - SINGLE VARIABLE

SUBROUTINE NAMES: D1MDG2 or D1M2DA

PURPOSE:

These subroutines use the arithmetic mean of two input values as the independent variable for parabolic interpolation. They require a doublet or two singlet arrays respectively.

RESTRICTIONS:

See LAGRAN or LGRNDA as they are called on respectively.

CALLING SEQUENCE:

D1MDG2(X1, X2, A(IC), Y)
or D1M2DA(X1, X2, AX(IC), AY(IC), Y)

SUBROUTINE NAMES: D1M2WM or D1M2MD

PURPOSE:

These subroutines use the arithmetic mean of two input values as the independent variable for parabolic interpolation. The interpolated answer is multiplied by the Z value prior to being returned as Y.

RESTRICTIONS:

Same as D1MDG2 or D1M2DA and Z must be a floating point number.

CALLING SEQUENCE:

D1M2WM(X1, X2, A(IC), Z, Y)
or D1M2MD(X1, X2, AX(IC), AY(IC), Z, Y)
CYCLICAL INTERPOLATION ARRAYS

SUBROUTINE NAMES: D11CYL or DA11CY

PURPOSE:

These subroutines reduce core storage requirements for cyclical interpolation arrays. The arrays need cover one period only, and the period (PR) must be specified as the first argument. Linear interpolation is performed, and the independent variable must be in ascending order.

RESTRICTIONS:

All values must be floating point. Subroutine INTREC is called on by both D11CYL and DA11CY, then D1DEG1 or D1D1DA respectively.

CALLING SEQUENCE: D11CYL(PR, X, A(IC), Y)

or DA11CY(PR, X, AX(IC), AY(IC), Y)

SUBROUTINE NAMES: D12CYL or DA12CY

PURPOSE:

These subroutines are virtually identical to D11CYL and DA11CY except that parabolic interpolation is performed.

RESTRICTIONS:

See D11CYL and DA11CY. Subroutines LAGRAN and LGRNDA respectively are called on.

CALLING SEQUENCE: D12CYL(PR, X, A(IC), Y)

or DA12CY(PR, X, AX(IC), AY(IC), Y)
CYCLICAL INTERPOLATION ARRAYS

SUBROUTINE NAMES: D11MCY or DA11MC

PURPOSE:

These subroutines are virtually identical to D11CYL and DA11CY except that the interpolation is multiplied by the floating point 2 value prior to being returned as y.

RESTRICTIONS:

Call on subroutines D1DEG1 and D1D1DA respectively.

CALLING SEQUENCE:

D11MCY(PR,X,A(IC),Z,Y)

or DA11MC(PR,X,AX(IC),AY(IC),Z,Y)

SUBROUTINE NAMES: D12MCY or DA12MC

PURPOSE:

These subroutines are virtually identical to D11MCY and DA11MC except that parabolic interpolation is performed.

RESTRICTIONS:

Calls on subroutines LAGRAN and LGRNDA respectively.

CALLING SEQUENCE:

D12MCY(PR,X,A(IC),Z,Y)

or DA12MC(PR,X,AX(IC),AY(IC),Z,Y)
POINT SLOPE INTERPOLATION

SUBROUTINE NAMES: GSLØPE

PURPOSE:

This subroutine will generate a slope array so that point slope interpolation subroutines can be used instead of standard linear interpolation subroutines. The user must address two singlet type arrays and a singlet slope array will be produced.

RESTRICTIONS:

The X independent variable array must be in ascending order. All arrays must be of equal length and contain floating point numbers.

CALLING SEQUENCE:

GSLØPE(AX(IC),AY(IC),AS(IC))

SUBROUTINE NAMES: PSINTR or PSNTWM

PURPOSE:

These subroutines perform linear interpolation and require arrays of the Y points and slopes which correspond to the independent variable X array. All values must be floating point numbers. PSNTWM multiplies the interpolated answer by Z prior to returning it as Y.

RESTRICTIONS:

The independent X and dependent Y and slope arrays must be of equal length.

CALLING SEQUENCE:

PSINTR(X,AX(IC),AY(IC),AS(IC),Y)

or

PSNTWM(X,AX(IC),AY(IC),AS(IC),Z,Y)
BIVARIATE INTERPOLATION

SUBROUTINE NAMES: BVSPSA or BVSPDA

PURPOSE:

These subroutines use an input Y argument to address a bivariate array and pull off a singlet array of Z's corresponding to the X's or pull off a doublet array of X, Z values, respectively. The integer count for the constructed arrays must be exactly N or 2*N respectively. To use the singlet array for an interpolation call the X array can be reached by addressing the N in the bivariate array.

RESTRICTIONS:

As stated above, and all values must be floating point.

CALLING SEQUENCE: BVSPSA(Y,BA(IC),AZ(IC))

or BVSPDA(Y,BA(IC),AXZ(IC))

SUBROUTINE NAMES: BVTRN1 or BVTRN2

PURPOSE:

These subroutines construct a bivariate array of Y's versus X and Z from an input bivariate array of Z's versus X and Y. BVTRN1 should be used when the Z values increase with increasing Y values and BVTRN2 when the Z values decrease with increasing Y values.

RESTRICTIONS:

The user must appropriately place the X and Z values and spaces for Y's in the array to be constructed. These subroutines will fill the Y spaces. The new array can differ in size from the old. Subroutine D1DEG1 is called and its linear extrapolation feature applies.

CALLING SEQUENCE: BVTRN1(BA0(IC),BAN(IC))

or BVTRN2(BA0(IC),BAN(IC))

* See page A-60A
BIVARIATE INTERPOLATION

SUBROUTINE NAMES: D2DEG1 or D2DEG2

PURPOSE:

These subroutines perform bivariate linear and parabolic interpolation respectively. The arrays must be formatted as shown for Bivariate Array Format.*

RESTRICTIONS: For D2DEG1 , N>2,M>2 See Bivariate
For D2DEG2 , N>3,M>3 Array Format

CALLING SEQUENCE: D2DEG1(x,y,BA(IC),Z)
or D2DEG2(x,y,BA(IC),Z)

SUBROUTINE NAMES: D2D1WM or D2D2WM

PURPOSE:

These subroutines perform bivariate* linear or parabolic interpolation by calling on D2DEG1 or D2DEG2 respectively. The interpolated answer is multiplied by the \( \nu \) value prior to being returned as \( Z \).

RESTRICTIONS:

Same as D2DEG1 or D2DEG2 and \( \nu \) must be a floating point value.

CALLING SEQUENCE: D2D1WM(x,y,BA(IC),\( \nu \),Z)
or D2D2WM(x,y,BA(IC),\( \nu \),Z)

* See page A-60A
**BIVARIATE INTERPOLATION**

**SUBROUTINE NAMES:** D2MXD1 or D2MXD2

**PURPOSE:**

These subroutines are virtually identical to D2DEG1 and D2DEG2 except that the arithmetic mean of two X values is used as the X independent variable for interpolation.

**RESTRICTIONS:**

Same as D2DEG1 or D2DEG2.

**CALLING SEQUENCE:**

D2MXD1$(X1,X2,Y,BA(IC),Z)$

or

D2MXD2$(X1,X2,Y,BA(IC),Z)$

**SUBROUTINE NAMES:** D2MX1M or D2MX2M

**PURPOSE:**

These subroutines are virtually identical to D2D1WM and D2D2WM except that the arithmetic mean of two X values is used as the X independent variable for interpolation.

**RESTRICTIONS:**

Same as D2D1WM and D2D2WM.

**CALLING SEQUENCE:**

D2MX1M$(X1,X2,Y,BA(IC),W,Z)$

or

D2MX2M$(X1,X2,Y,BA(IC),W,Z)$
TRIVARIATE INTERPOLATION

SUBROUTINE NAMES: D3DEG1 or D3D1WM

PURPOSE:

These subroutines perform trivariate linear interpolation. The interpolation array must be constructed as shown for Trivariate Array Format.* Subroutine D2DEG1 is called on which calls on D1DEG1. Hence, the linear extrapolation feature of these routines applies. Subroutine D3D1WM multiplies the interpolated answer by F prior to returning it as T.

RESTRICTIONS:

See Trivariate Array Format.* F must be a floating point value.

CALLING SEQUENCE:

D3DEG1(X,Y,Z,TA(IC),T)

or D3D1WM(X,Y,Z,TA(IC),F,T)

LINEAR EXTRAPOLATION

SUBROUTINE NAME: ITRATE

PURPOSE:

Given two old guesses and their corresponding errors, this routine linearly extrapolates a new guess on the basis of zero error.

E

E_0

E_n

0

G

G_n'

G_n

G_o

The new guess and error are positioned in the old locations and the extrapolated new guess is returned in the new guess location.

RESTRICTIONS:

If the error function being plotted has changes of slope, the user must insure that his guesses are quite accurate or divergence will be assured.

CALLING SEQUENCE: ITRATE(E_0,G_0,E_n,G_n)

* See page A-60A

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2.5 OUTPUT SUBROUTINES

Network Printout

TPRNT  Prints thermal node temperature
CPRNT  Prints thermal capacitances
QPRNT  Prints the nodal heat flow values
UPRNT  Prints thermal conductances
DPRNT  Prints the time increments
COPRNT Prints the thermal network capacitances, heat flow values, time increment and the conductances
WPRNT  Prints flow rates
PPRNT  Prints pressures
VPRNT  Prints valve positions

Floating Point

PRINT } Allows individual floating point numbers to be printed for reference temperature, capacitance, etc.

Array Printout

PRINTA Allows the user to printout an array of values five to the line
PRNTMA Allows the user to print up to 10 arrays in a column format
PRNTMI Enables a user to punch out an array of data values in any desired format
GENOUT Prints out any general array containing both integers and real numbers
GENI Prints out an array of integer
GENR Prints out an array of real numbers

Plot Package

PRNPLT Prints out a plot on the line printer
PL0TX1
PL0TX2
PL0TL1 Call upon a large package of undocumented subroutines specifically for the SC-4060
PL0TL2
PL0TX3
PL0TX4
SC-4060 Plot Symbol Dictionary
SC-4020 Plot Symbol Dictionary

Tape Input/Output

READ } Enables the user to read and write arrays of data
WRITE } as binary information on magnetic tape
Matrix Output

LIST       Prints the elements of a matrix and identifies each by
           its row and column number.................................. A-87.

PUNCH      Punches out a matrix, size n*n, one column at a time
           in any desired format........................................ A-88

SYMLST     Prints out and identifies the element values of a
           half symmetric matrix........................................ A-88

Special

PNTABL     Provides output information for users of subroutine
           ABLATS....................................................... A-88
Network Printout Subroutines

SUBROUTINE NAMES: TPRNT, CPRNT, QPRNT, UPRNT, DPRNT, or COPRNT

PURPOSE:

These subroutines provide the user with the ability to printout the elements of the thermal network. The purpose of each is listed below.

TPRNT Prints all the thermal network temperatures in the T array
CPRNT Prints all the thermal network capacitance in the C array
QPRNT Prints all the values in the Q array
UPRNT Prints all the conductance values in the U array
DPRNT Prints all the values in the DTAU (time increment) array
COPRNT Calls CPRNT, QPRNT, UPRNT and DPRNT

These subroutines are normally called in the OUTPUT block but may be called from other operations blocks. However, an excessive amount of output may occur if they are called from PRETMP or POSTMP.

RESTRICTIONS:

NONE

CALLING SEQUENCE: TPRNT, CPRNT, QPRNT, UPRNT, DPRNT or COPRNT
SUBROUTINE NAMES: WPRNT, PPRNT, or VPRNT

PURPOSE:

These subroutines provide the user with the ability to printout the fluid flow rate, the pressure of the pressure nodes, and valve positions. WPRNT prints flow rates; PPRNT prints pressures, and VPRNT prints valve positions. These subroutines are normally called from the OUTPUT block but may be called from other operations blocks if desired.

RESTRICTIONS: NONE

CALLING SEQUENCE: WPRNT, PPRNT, or VPRNT
FLOATING POINT PRINTOUT

SUBROUTINE NAMES: PRINT or PRINTL

PURPOSE:
These subroutines allow individual floating point numbers to be printed. The arguments may reference temperature, capacitance, source locations, conductors, or unique array locations. In addition, subroutine PRINTL allows each value to be preceded or labeled by a six-character alphanumeric word. The number of arguments is variable but the "label" array (LA) used for PRINTL should contain a Hollerith label for each argument.

RESTRICTIONS:
Integers must first be floated.

CALLING SEQUENCE: PRINT(T,C,Q,G,K,...,A+)
or PRINTL(LA(DV),T,C,Q,G,K,...,A+)

ARRAY PRINTOUT

SUBROUTINE NAME: PRINTA

PURPOSE:
This subroutine allows the user to print out an array of values, five to the line. The integer array length N and the first data value location must be specified. Each value receives an indexed label. The user must supply a six-character alphanumeric word L to be used as a common label and an integer value M to begin the index count.

RESTRICTIONS:
The array values to be printed must be floating point numbers. If L is supplied as a literal Hollerith data value (instead of a reference to a user constant containing same), it must be entered in FORTRAN-compatible H-type notation (e.g., 4HTEMP).

CALLING SEQUENCE: PRINTA(L,A(DV),N,M)
If the label was the word 'TEMP', N was 3 and M was 6, the line of output would look as follows:

TEMP ( 6)value TEMP ( 7)value TEMP ( 8)value
SUBROUTINE NAME: PRNTMA or PRNTMI

PURPOSE:

This subroutine allows the user to print out up to 10 arrays in a column format. The individual elements are not labeled but each column receives a two-line heading of 12 alphanumeric characters/line. The two-line heading must be supplied as a single array of four words, six characters each. The user must supply the starting location of each label array and value array. The number of values in each value array must agree and be supplied as the integer $n$. The value arrays must contain floating point numbers.

RESTRICTIONS:

Labels must be alphanumeric while values must be floating point. All floating point value arrays must contain the same number of values.

CALLING SEQUENCE:

$\textit{PRNTMA}(n, \text{LA1(DV)}, \text{VA1(DV)}, \text{LA2(DV)}, \text{VA2(DV)}, ...)$

$\textit{PRNTMI}(n, \text{LA1(DV)}, \text{VA1(DV)}, \text{LA2(DV)}, \text{VA2(DV)}, ...)$

$\textit{VA1}$ only must address an array of integers for subroutine $\textit{PRNTMI}$.

ARRAY PRINTOUT

SUBROUTINE NAME: PUNCHA

PURPOSE:

This subroutine enables a user to punch out an array of data values in any desired format. The $F$ argument must reference a FORTRAN FORMAT which has been input as an array, including the outer parenthesis but deleting the word FORMAT.* The second argument must address the first data value of the array of sequential values. The third argument, $N$, must be the integer number of data values in the array.

CALLING SEQUENCE:

$\textit{PUNCHA}(F(DV), A(DV), N)$
SUBROUTINE NAMES: GENOUT, GENI or GENR

PURPOSE:

These subroutines print out arrays of numbers 10 to a line. GENOUT prints either real numbers, integer or both. GENI and GENR print integers and real number arrays respectively. The integer are written in a I9 format and the real numbers in a E12.4 format.

RESTRICTIONS:

GENI writes arrays of integers only. GENR writes arrays of real numbers only.

CALLING SEQUENCE:

```
GENOUT (A, ISTRT, ISTOP, 'NAME')
GENI    (A, ISTRT, ISTOP, 'NAME')
GENR    (A, ISTRT, ISTOP, 'NAME')
```

Where

- A is the array location
- ISTRT is the first value in A being written
- ISTOP is the last value in A being written
- 'NAME' is a title of 22 Hallerith words for identification
PLOT PACKAGE

SUBROUTINE NAME: PRNPLT

PURPOSE:

This subroutine will print out a plot of data on the line printer. It is intended primarily for plotting temperature histories which were accumulated in the OUTPUT CALLS block. One or two curves of up to 100 points each may be plotted on each frame (page). Y-axis scaling is automatic. No units are associated with the X-axis, and no X values are used; one point is plotted for each print wheel position along the X-axis. Points on the first curve will be printed as 'X's, and points on the second curve will be printed as 'O's. Where points overlap, an asterisk, '*', is printed.

RESTRICTIONS:

If NA and/or NB is greater than 100, only the first 100 points in the corresponding array of Y-values (YA and/or YB) will be plotted. The argument LP normally has a value of 50 when standard 11 x 14 computer paper is used. The smallest Y increment represented by a line is one unit, so the narrowest range covered by the Y axis will be LP units. One graph only may be plotted on a single page. When a point to be plotted has a value which lies exactly between the values associated with two adjacent lines, then the point will be printed on both lines.

CALLING SEQUENCE:

PRNPLT(TT(DV),NA,YA(DV),TA(DV),NB,YB(DV),TB(DV),LP)

where:

TT = Main title (4 Hollerith words)
NA = Number of points for the first curve
(integer; must be greater than zero)
YA = Y values for the first curve
TA = Title for the first curve (4 Hollerith words)
NB = Number of points for the second curve
(may be zero)
YB = Y values for the second curve
TB = Title for the second curve (4 Hollerith words)
LP = Number of printer lines which may be used to plot values
(at least two less than the number of lines on a page)
PLOT PACKAGE

SUBROUTINE NAMES: PL0TX1 or PL0TX2 or PL0TL1 or PL0TL2

PURPOSE:

These FORTRAN V coded quick plot subroutines call upon a large package of undocumented subroutines specifically for the SC-4060. They will produce up to four graphs per frame and several variables may be plotted per graph. A suitable grid will be drawn with certain lines emphasized. The grid lines will have reasonable numerical indicia and centered title will be printed for both axes and at the top of the graph.

PL0TX1 and PL0TL1 will compute the minimum and maximum values of the stored X and Y arrays to be plotted and call upon PL0TX2 or PL0TL2 which use the values as grid limits for the graph. The user may set the grid limits by calling PL0TX2 and PL0TL2 directly. The X, Y and top titles (XT, YT and TT respectively) must consist of nine alphanumeric words of six characters each.

RESTRICTIONS:

The user should consult Appendix D to check tape designation requirements. The X and Y values must be floating point numbers. The user must call subroutine PLTND after all his plotting is done. No limit may be zero for log plots.

CALLING SEQUENCE:

PL0TX1(N,IS,TX(DV),TY(DV),TT(DV),NP,AX(DV),AY(DV))

or

PL0TX2(N, XL,XR,YB,YT,IX,TX(DV),TY(DV),TT(DV),NP,AX(DV),AY(DV))

or

PL0TL1(N,IS,TX(DV),TY(DV),TT(DV),NP,AX(DV),AY(DV),LM)

PL0TL2(N, XL,XR,YB,YT,IS,TX(DV),TY(DV),TT(DV),NP,AX(DV),AY(DV),LM)

where: N is the integer number of graphs per frame (1,2,3 or 4);
\( IS \) is the integer identifying the plotting symbol (1-144)
TX is the address of the X title
TY is the address of the Y title
TT is the address of the top title
NP is the integer number of XY values or points to be plotted; if negative the points will be connected by straight lines.
AX is the address of the X array
AY is the address of the Y array
XL is the floating point X axis left limit
XR is the floating point X axis right limit
YB is the floating point Y axis bottom limit
YT is the floating point Y axis top limit
LM is an integer identifying the log plotting mode; if less than zero plot log X versus linear Y, if equal to zero plot log X versus log Y, if greater than zero plot linear X versus log Y
PL0TX3 or PL0TX4

PURPOSE:

These subroutines are similar to PL0TX1 and PL0TX2 but have six additional arguments which allow the user to modify the grid as desired.

RESTRICTIONS:

See PL0TX1 and PL0TX2.

CALLING SEQUENCE:

\[
\text{PL0TX3}(N, IS, TX(DV), TY(DV), TT(DV), NP, AS(DV), AY(DV), DX, DY, L, M, I, J) \\
\text{or} \\
\text{PL0TX4}(N, XL, XR, YB, YT, IS, TX(DV), TY(DV), TT(DV), NO, AX(DV), AY(DV), DX,} \\
DY, LM, I, J)
\]

where the arguments are identical to PL0TX1 and PL0TX2 except for

- **DX, DY**: these floating point values are used in spacing the grid lines which are centered on the zero values. If zero, no grid lines will be drawn.
- **L, M**: these integers cause every \( L \)th vertical and \( M \)th horizontal grid line to be redrawn for emphasis. If zero, no grid lines will be emphasized. If negative, a square grid will be produced.
- **I, J**: these integers cause every \( I \)th vertical and \( J \)th horizontal grid line to be labeled with its value. If zero, no grid lines will be labeled. If negative, the labels will be placed outside the grid, otherwise they will appear on the zero axis.
**PLOT PACKAGE**

**SC-4060 PLOT SYMBOL DICTIONARY**
(for use with quick plot subroutines only)

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A-85
SC-4020 PLOT SYMBOL DICTIONARY

(to be used at installations, such as NASA/MSC, where an SC-4060 is used to simulate an SC-4020)

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**TAPE INPUT/OUTPUT**

**SUBROUTINE NAMES:** READ or WRITE

**PURPOSE:**

These subroutines enable the user to read and write arrays of data as binary information on magnetic tape. The first argument \( L \) must be the integer number of the logical tape being addressed. The second argument \( X \) must address the first data value of the array to be written out or starting location for data to be read into. The third argument \( N \) must be an integer. For WRITE, it is the number of data values to be written on tape as a record. For READ, it is the number of data values to be read in from tape from the next record, not necessarily the entire record.

**RESTRICTIONS:**

The user should check Appendix D to determine which logical tapes are available and control card requirements. All processed information must be in binary.

**CALLING SEQUENCE:**

\[
\text{READ}(L, X(DV), N) \\
\text{or} \quad \text{WRITE}(L, X(DV), N)
\]

---

**MATRIX PRINTOUT**

**SUBROUTINE NAME:** LIST

**PURPOSE:**

This subroutine prints the elements of a matrix \([A]\) and identifies each by its row and column number. The user must supply an alphanumeric name \( ALP \) and integer number \( NUM \) to identify the matrix. This is to maintain consistency with subroutines FILE and CALL.

**RESTRICTIONS:**

The matrix must have its integer number of rows and columns as the first two data values.

**CALLING SEQUENCE:**

\[
\text{LIST}(A(IC), ALP, NUM)
\]
SUBROUTINE NAME: PUNCH

PURPOSE:
This subroutine punches out a matrix \([A]\), size \(n \times m\), one column at a time in any desired format. The argument \(\text{FOR}\) must reference a FORTRAN format statement that has been input as a positive array. It must include the outer parenthesis but not the word F\(\text{ORMAT}\). The argument \(\text{HEAD}\) must be a single BCD word used to identify the matrix. Each column is designated and restarts use of the F\(\text{ORMAT}\) statement.

RESTRICTIONS:
The matrix \([A]\) must have exactly enough space and contain the integer number of rows and columns as the first two data values.

CALLING SEQUENCE: 
PUNCH(A(IC),HEAD,\text{FOR}(IC))

DYNAMIC STORAGE REQUIREMENTS:
This subroutine required \(n+3\) dynamic storage locations.

SUBROUTINE NAME: SYMLST

PURPOSE:
To print out and identify the element values of a half symmetric matrix. This output subroutine is most generally used with subroutine SCRPFA.

CALLING SEQUENCE: 
SYMLST(A(DV),N)

where \(A(DV)\) addresses the 1,1 element and \(N\) is the matrix order.

SPECIAL

SUBROUTINE: PNTABL

PURPOSE:
To provide output information for users of subroutine ABLATS. The ABLATS routine performs ablative simulation calculations but since it is called in $\text{POSTTEMP}$, it performs no output. The user must call PNTABL in the $\text{OUTPUT}$ block and reference the ablative array of the ABLATS call. When the ablative material is expended, ABLATS will call PNTABL directly and will also cause current problem time to be printed.

RESTRICTIONS:
This routine is called in conjunction with subroutine ABLATS only, see Section 2.2

CALLING SEQUENCE: 
PNTABL(AA(IC))
2.6 MATHEMATICAL SOLUTION SUBROUTINES

Area Integration

SMPINT  Performs area integration by Simpson's rule and
TRPZD   trapezoidal rule using equal increments. .......... A-90

TRPZDA  Performs area integration by the trapezoidal rule
         with non uniform increments. ...................... A-90

NEWRT4  Utilizes Newton's method to obtain one root of a
         cubic or quartic equation. ......................... A-91

Polynomial/Simultaneous Linear Equations

PLYNML  Calculates the value of the dependent variable for
PLYARY  an Nth order polynomial. ............................ A-92
PLYAWM

SIMEQN   Solves a set of linear equations (10 or less) by the
         factorized inverse method. ........................ A-92

Curve Fit/Temperature Derivative

LSTSQU  Performs a least squares curve fit to an arbitrary
         number of X,Y pairs to yield a polynomial
         equation of up to order 10 .......................... A-93

Complex Variable Analysis

CMPXSR  Obtains the complex square root of a complex number
CSQRI   or array of complex numbers. ........................ A-93

CMPXMP  Multiplies two complex numbers or the corresponding
CMPYI   elements of arrays of complex numbers.  .......... A-93

CMPXDV  Divides two complex numbers or the corresponding
CDIVI   elements of complex numbers.  .................... A-93
AREA INTEGRATION

SUBROUTINE NAMES: SMPINT or TRPZD

PURPOSE:

These subroutines perform area integrations by Simpson's rule and the trapezoidal rule respectively. Simpson's rule requires that an odd number of points be supplied. If an even number of points is supplied, SMPINT will apply the trapezoidal rule to the last incremental area but Simpson's rule elsewhere. The respective operations are:

\[ A = DX \times (Y_1 + 4Y_2 + 2Y_3 + 4Y_4 + \ldots + Y_N)/3 \]

or

\[ A = DX \times (Y_1 + 2Y_2 + 2Y_3 + 2Y_4 + \ldots + Y_N)/2 \]

RESTRICTIONS:

The DX increment must be uniform between all the Y points. All values must be floating point except N which must be an integer.

CALLING SEQUENCE: SMPINT(N,DX,Y(DV),A)

or TRPZD(N,DX,Y(DV),A)

SUBROUTINE NAME: TRPZDA

PURPOSE:

This subroutine performs area integration by the trapezoidal rule. It should be used where the DX increment is not uniform between the Y values but the corresponding X value for each Y value is known. The operation performed is as follows:

\[ A = \frac{1}{2} \sum (x_i - x_{i-1}) \times (y_i + y_{i-1}) \], \quad i = 2,N

All values must be floating point numbers except the array length N which must be an integer.

CALLING SEQUENCE: TRPZDA(N,X(DV),Y(DV),A)
ROOTS

SUBROUTINE NAMES: NEWTRT or NEWRT4

PURPOSE:

These subroutines utilize Newton's method to obtain one root of a cubic or quartic equation respectively. The root must be in the neighborhood of the supplied initial guess and up to 100 iterations are performed in order to obtain an answer within the specified tolerance. If the tolerance is not met, an answer of $10^{38}$ is returned. The respective equations are:

\[ f(X) = A1 + A2 \cdot X + A3 \cdot X^2 + A4 \cdot X^3 = 0.0 \pm T \]

or

\[ g(X) = A1 + A2 \cdot X + A3 \cdot X^2 + A4 \cdot X^3 + A5 \cdot X^4 + 0.0 \pm T \]

where \( X \) starts as the initial guess \( RI \) and finishes as the final answer \( RF \). \( T \) is the tolerance.

RESTRICTIONS:

All data values must be floating point numbers.

CALLING SEQUENCE: NEWTRT(A(DV), T, RI, RF) OR NEWRT4(A(DV), T, RI, RF)
POLYNOMIAL/SIMULTANEOUS LINEAR EQUATIONS

SUBROUTINE NAMES: PLYNML or PLYARY or PLYAWM

PURPOSE:

These subroutines calculate Y from the following polynomial equation:

\[ Y = A_1 + A_2 x + A_3 x^2 + A_4 x^3 + \ldots + A_N x^N \]

or

\[ Z = Y^* W \]

The number of terms is variable but all the A coefficients must be input no matter what their value.

RESTRICTIONS:

All values must be floating point numbers except for the degree of polynomial N which must be integer.

CALLING SEQUENCE:

- PLYNML(\(X, A_1, A_2, A_3, \ldots, A_N, Y)\)
- PLYARY(\(N, X, A(DV), Y)\)
- PLYAWM(\(N, X, A(DV), W, Z)\)

SUBROUTINE NAME: SIMEQN

PURPOSE:

This subroutine solves a set of up to 10 linear simultaneous equations by the factorized inverse method. The problem size and all input and output values are communicated as a single specially formatted positive input array. The array argument must address the matrix order (\(N\)) which is input by the user. The first data value must be the integer order of the set (or size of the square matrix) followed by the coefficient matrix \(A\) in column order, the boundary vector \(B\) and space for the solution of vector \(S\).

\[ \begin{bmatrix} A \\ S \end{bmatrix} = \begin{bmatrix} B \end{bmatrix} \]

RESTRICTIONS:

The integer count and matrix size must be integers, all other values must be floating point. The coefficient matrix is not modified by SIMEQN. Hence, changes to \(B\) only allow additional solutions to be easily obtained.

CALLING SEQUENCE:

SIMEQN(A(DV))

where the array is formatted exactly as follows:

\( N, A(1,1), A(1,2), \ldots, A(N,N), B1, \ldots, Bn, S1, \ldots, SN \)
CURVE FIT/TEMPERATURE DERIVATIVE

SUBROUTINE NAME: LSTSQU

PURPOSE:

This subroutine performs a least squares curve to fit to an arbitrary number of X, Y pairs to yield a polynomial equation of up to order 10. Rather than using a double precision matrix inverse, this subroutine calls on the subroutine SIMEQN to obtain a simultaneous solution.

RESTRICTIONS:

All values must be floating point numbers except \( N \) and \( M \) which must be integers. \( N \) is the order of the polynomial desired and is one less than the number of coefficients desired. \( M \) is the array length of the independent \( X \) or dependent \( Y \) values.

CALLING SEQUENCE: LSTSQU(\( N \), \( M \), \( X(DV) \), \( Y(DV) \), \( A(DV) \))

DYNAMIC STORAGE REQUIREMENTS:

This subroutine requires \( 2*M \) dynamic storage core locations.

SUBROUTINE NAMES: CMPXSR or CSQRI

PURPOSE:

These subroutines obtain the complex square root of a complex number or an array of complex numbers respectively. Their respective operations are:

\[
A + iB = \sqrt{C + iD} \quad , \quad i = \sqrt{-1}
\]

or

\[
A_j + iB_j = \sqrt{C_j + iD_j} \quad , \quad j = 1, N
\]

RESTRICTIONS:

All numbers must be floating point except \( N \) which must be an integer.

CALLING SEQUENCE: CMPXSR(\( C \), \( D \), \( A \), \( B \))

or CSQRI(\( N \), \( C(DV) \), \( D(DV) \), \( A(DV) \), \( B(DV) \))
SUBROUTINE NAMES: CMPXMP or CMPYI

PURPOSE:

These subroutines will multiply two complex numbers or the corresponding elements of arrays of complex numbers. Their respective operations are:

\[ A + iB = (C + iD)(E + iF), \quad i = \sqrt{-1} \]

or \[ A_j + iB_j = (C_j + iD_j)(E_j + iF_j), \quad j = 1, N \]

RESTRICTIONS:

All numbers must be floating point except for \( N \) which must be an integer.

CALLING SEQUENCE:

CMPXMP\((C,D,E,F,A,B)\)

or \( \text{CMPYI}(N,C(DV),D(DV),E(DV),F(DV),A(DV),B(DV)) \)

DIVISION OPERATION

SUBROUTINE NAMES: CMPXDV or CDIVI

PURPOSE:

These subroutines will divide two complex numbers or the corresponding elements of arrays of complex numbers. Their respective operations are:

\[ A + iB = (C + iD)/(E + iF), \quad j = \sqrt{-1} \]

or \[ A_j + iB_j = (C_j + iD_j)/(E_j + iF_j), \quad j = 1, N \]

RESTRICTIONS:

All numbers must be floating point except for \( N \) which must be an integer.

CALLING SEQUENCE:

CMPXDV\((C,D,E,F,A,B)\)

or \( \text{CDIV}(N,C(DV),D(DV),E(DV),F(DV),A(DV),B(DV)) \)
2.7 ARRAY OPERATIONS AND MANIPULATIONS

Addition Operation

ADDARY Adds the corresponding elements of two specified length arrays to form a third array. A-97
ARYADD Adds a constant value to every element in an array to form a new array. A-97
SUMARY Sums an array of floating point values A-97

Subtraction Operation

SUBARY Subtracts the corresponding elements of one array from another to form a third array. A-98
ARYSUB Subtracts a constant value from every element in an array to form a new array. A-98

Multiplication Operation

MPYARY Multiplies the corresponding elements of two arrays to form a third. A-98
ARYMPY Multiplies each element of an array by a constant value to form a new array. A-98
SCLDEP Multiplies the dependent or independent variables of a doublet type interpolation array. A-99
SCLIND

Division Operation

DIVARY Divides the elements of one array into the corresponding elements of another array to produce a third array. A-99
ARYDIV Divides each element of an array by a constant value to produce a new array. A-99
ARYINV Inverts each element of an array in its own location. A-100
ARINDV Divides each element of an array into a constant value to form a new array. A-100
ADARIN Calculates one over the sum of inverses of an array of values. A-

Distribution of Array Data

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SHFTVR  Shifts a sequence of data from one array and places data in reverse order in another array. ................. A-101
FLIP    Reverses an array in its own array location ............... A-101
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BLDARY  Builds an array from a variable number of arguments in the order listed ................................. A-102
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Singlet/Doublet Array Generation

SPLIT    Separates a doublet array into two singlet arrays .... A-105
JOIN     Combines two singlet arrays into a doublet array. .... A-105
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Comparison Operation

MAXDAR  MXDRAI Obtains the absolute maximum difference between corresponding elements of two arrays of equal length N. ................................................. A-106
ADDITION OPERATION

SUBROUTINE NAMES: ADDARY or ARYADD

PURPOSE:
Subroutine ADDARY will add the corresponding elements of two specified length arrays to form a third array. Subroutine ARYADD will add a constant value to every element in an array to form a new array. Their respective operations are:

\[ Ai = Bi + Ci \quad , \quad i = 1,N \]

or

\[ Ai = Bi + C \quad , \quad i = 1,N \]

RESTRICTIONS:
All data values to be operated on must be floating point numbers. The array length \( N \) must be an integer.

CALLING SEQUENCE: ADDARY\((N,B(DV),C(DV),A(DV))\)

or

ARYADD\((N,B(DV),C,A(DV))\)

The answer array may be overlayed into one of the input array areas.

SUBROUTINE NAME: SUMARY

PURPOSE:
To sum an array of floating point values:

\[ S = \sum Ai \quad , \quad i = 1,N \]

RESTRICTIONS:
The values to be summed must be floating point numbers and the array length \( N \) must be an integer.

CALLING SEQUENCE: SUMARY\((N,A(DV),S)\)
SUBTRACTION OPERATION

SUBROUTINES NAMES: SUBARY or ARYSUB

PURPOSE:

Subroutine SUBARY will subtract the corresponding elements of one array from another to form a third array. Subroutine ARYSUB will subtract a constant value from every element in an array to form a new array. Their respective operations are:

\[ A_i = B_i - C_i, \quad i = 1,N \]

or

\[ A_i = B_i - C, \quad i = 1,N \]

RESTRICTIONS:

All data values to be operated on must be floating point numbers. The array length \( N \) must be an integer.

CALLING SEQUENCE:

\[ \text{SUBARY}(N,B(DV),C(DV),A(DV)) \]

or

\[ \text{ARYSUB}(N,B(DV),C,A(DV)) \]

The answer array may be overlayed into one of the input array areas.

MULTIPLICATION OPERATION

SUBROUTINE NAMES: MPYARY or ARYMPY

PURPOSE:

Subroutine MPYARY will multiply the corresponding elements of two arrays to form a third. Subroutine ARYMPY will multiply a constant value times each element of an array to form a new array. Their respective operations are:

\[ A_i = B_i \times C_i, \quad i = 1,N \]

or

\[ A_i = B_i \times C, \quad i = 1,N \]

RESTRICTIONS:

All data values to be operated on must be floating point numbers. The array length \( N \) must be an integer.

CALLING SEQUENCE:

\[ \text{MPYARY}(N,B(DV),C(DV),A(DV)) \]

or

\[ \text{ARYMPY}(N,B(DV),C,A(DV)) \]

The answer array may be overlayed into one of the input array areas.
MULTIPLICATION OPERATION

SUBROUTINE NAMES: SCLDEP or SCLIND

PURPOSE:

These subroutines will multiply the dependent or independent variables of a doublet type interpolation array respectively. Their respective operations are:

\[ A_i = X \cdot A_i \quad i = 2, 4, 6, 8, \ldots, n \]

or

\[ A_i = X \cdot A_i \quad i = 1, 3, 5, 7, \ldots, n-1 \]

RESTRICTIONS:

All values must be floating point. The arrays must be referenced with the integer count form.

CALLING SEQUENCE:

SCLDEP(A(IC), X)

or

SCLIND(A(IC), X)

DIVISION OPERATION

SUBROUTINE NAMES: DIVARY or ARYDIV

PURPOSE:

Subroutine DIVARY will divide the elements of one array into the corresponding elements of another array to produce a third array. Subroutine ARYDIV will divide each element of an array by a constant value to produce a new array. Their respective operations are:

\[ A_i = B_i / C_i \quad i = 1, N \]

or

\[ A_i = B_i / C \quad i = 1, N \]

RESTRICTIONS:

All data values to be operated on must be floating point numbers. The array length \( N \) must be an integer.

CALLING SEQUENCE:

DIVARY(\( N, B(DV), C(DV), A(DV) \))

or

ARYDIV(\( N, B(DV), C, A(DV) \))

The answer array may be overlayed into one of the input array areas.
DIVISION OPERATION

SUBROUTINE NAMES: ARYINV or ARINDV

PURPOSE:

Subroutine ARYINV will invert each element of an array in its own location. Subroutine ARINDV will divide each element of an array into a constant value to form a new array. Their respective operations are:

\[ A_i = 1.0/A_i \quad , \quad i = 1, N \]

or

\[ A_i = B/C_i \quad , \quad i = 1, N \]

RESTRICTIONS:

All data values must be floating point numbers. The array length \( N \) must be an integer.

CALLING SEQUENCE:

\[ \text{ARYINV}(N, A(DV)) \]

or

\[ \text{ARINDV}(N, C(DV), B, A(DV)) \]

(The ARINDV answer array may be overlayed into the input array area.)

SUBROUTINE NAME: ADARIN

PURPOSE:

Subroutine ADARIN will calculate one over the sum of inverses of an array of values. This subroutine is useful for calculating the effective conductance of series conductors. The operations are:

\[ Y = 1.0/\sum(1./X_i) \quad , \quad i = 1, 2, \ldots, N \]

RESTRICTIONS:

All data values must be floating point numbers. The array length \( N \) must be an integer.

CALLING SEQUENCE:

\[ \text{ADARIN}(N, X(DV), Y) \]
DISTRIBUTION OF ARRAY DATA

SUBROUTINE NAMES: SHFTV or SHFTVR or FLIP

PURPOSE:
Subroutine SHFTV will shift a sequence of data from one array to another. Subroutine SHFTVR will shift a sequence of data from one array and place it in another array in reverse order. Subroutine FLIP will reverse an array in its own array location. Their respective operations are:

\[ A(i) = B(i), \quad i = 1, N \]

or \[ A(N-i+1) = B(i), \quad i = 1, N \]

or \[ A(i)_{\text{new}} = A(n-i+2)_{\text{old}}, \quad i = 2, n+1 \]

RESTRICTIONS:
The data values to be shifted or reversed in order may be anything. The \( N \) must be an integer.

CALLING SEQUENCE: SHFTV (N, B(DV), A(DV))

or SHFTVR (N, B(DV), A(DV))

or FLIP (A(IN))

The answer array may not be overlayed into the input array.

SUBROUTINE NAME: GENARY

PURPOSE:
This subroutine will generate an array of equally incremented ascending values. The user must supply the minimum value, maximum value, number of values in the array to be generated and the space for the generated array.

RESTRICTIONS:
All numbers must be floating point.

CALLING SEQUENCE: GENARY (B(DV), A(DV))

where \[ B(1) = \text{minimum value} \]

\[ B(2) = \text{maximum value} \]

\[ B(3) = \text{length of array to be generated (floating point)} \]
DISTRIBUTION OF ARRAY DATA

SUBROUTINE NAME: BLDARY

PURPOSE:
This subroutine will build an array from a variable number of arguments in the order listed. The operation performed is:

\[ A_i = X_i , \quad i = 1, n \]

RESTRICTIONS:

Data may be of any form. The subroutine obtains the integer array length \( n \) by counting the arguments.

CALLING SEQUENCE:

\[ \text{BLDARY}(A(DV), X_1, X_2, X_3, \ldots, X_n) \]

SUBROUTINE NAME: BRKARY or BKARAD

PURPOSE:

These subroutines will distribute values from within an array to a variable number of arguments in the order listed. The first places the value into the location while the second adds it to what is in the location. Respective operations are:

\[ X_i = A_i , \quad i = 1, n \]

or \[ X_i = X_i + A_i , \quad i = 1, n \]

RESTRICTIONS:

Floating point numbers must be used for BKARAD. The integer array length \( n \) is obtained by the routines by counting the number of arguments.

CALLING SEQUENCE:

\[ \text{BRKARY}(A(DV), X_1, X_2, X_3, \ldots, X_n) \]

or \[ \text{BKARAD}(A(DV), X_1, X_2, X_3, \ldots, X_n) \]

SUBROUTINE NAMES: STØARY or ARYSTØ

PURPOSE:

These subroutines will place a value into or take a value out of a specific array location respectively. Their respective operations are:

\[ A_i = X , \quad i = N , \quad N > 0 \]

or \[ X = A_i , \quad i = N , \quad N > 0 \]

RESTRICTIONS:

The value may be anything but \( N \) must be an integer.

CALLING SEQUENCE:

\[ \text{STØARY}(N, X, A(DV)) \]

or \[ \text{ARYSTØ}(N, X, A(DV)) \]
SUBROUTINE NAMES: STFSEQ or STFSQS

PURPOSE:

Both subroutines will stuff a constant data value into a specified length array or group of sequential locations. STFSEQ expects the constant data value to be in the first array location while STFSQS requires it to be supplied as an additional argument. The respective operations performed are:

\[ A_i = A_1, \quad i = 2, N \]

or

\[ A_i = B, \quad i = 1, N \]

RESTRICTIONS:

\( N \) must be an integer but the constant data value may be integer, floating point or alpha-numeric.

CALLING SEQUENCE:

STFSEQ(\( A(DV), N \))

or

STFSQS(\( B, N, A(DV) \))
DISTRIBUTION OF ARRAY DATA

SUBROUTINE NAMES: SLDARY or SLDARD

PURPOSE:

These subroutines are useful for updating fixed length interpolation arrays during a transient analysis. The array data values are moved back one or two positions, the first one or two values discarded and the last one or two values updated respectively. The "sliding array" thus maintained can then be used with standard interpolation subroutines to simulate transport delay phenomena. Their respective operations are:

\[ A_i = A_{i+1}, \quad i = 2, N \]

and \[ A_i = X, \quad i = N + 1 \]

or \[ A_i = A_{i+2}, \quad i = 2, N-1 \]

and \[ A_i = X \text{ and } A_{i+1} = Y, \quad i = N \]

RESTRICTIONS:

The addressed arrays must have the array integer count \( N \) as the first value. For SLDARD, \( N \) must be even.

CALLING SEQUENCE:

SLDARY(\( X, A(IC) \))

SLDARD(\( X, Y, A(IC) \))

SUBROUTINE NAME: STØRMA

PURPOSE:

This subroutine is useful for constructing historical data arrays during a transient analysis. It can take the place of several STØARY calls. The operations are as follows:

\[ A_1(\( N \)) = X_1 \]
\[ A_2(\( N \)) = X_2 \]
\[ A_3(\( N \)) = X_3 \]
\[ \vdots \]

RESTRICTIONS:

\( N \) must be or reference an integer, the \( X \)'s may be any value.

CALLING SEQUENCE: STØRMA(\( N, X_1, A_1(DV), X_2, A_2(DV), X_3, A_3(DV), \ldots \))

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SINGLET/DOU BLET ARRAY GENERATION

SUBROUTINE NAMES: SPLIT or JOIN

PURPOSE:

These subroutines separate a doublet array into two singlet arrays or combine two singlet arrays into a doublet array respectively. Their respective operations are:

\[ B_1 = A_{2i-1}, \quad 1 = 1, N \]
\[ C_i = A_{2i}, \quad 1 = 1, N \]

or

\[ A_{2i-1} = B_i, \quad 1 = 1, N \]
\[ A_{2i} = C_i, \quad 1 = 1, N \]

RESTRICTIONS:

The arrays may contain any values but \( N \) must be an integer. \( N \) is the length of the \( B \) and \( C \) arrays and the \( A \) array must be the length of \( 2N \).

CALLING SEQUENCE:

SPLIT\((N,A(DV),B(DV),C(DV))\)

or

JOIN\((N,B(DV),C(DV),A(DV))\)

SUBROUTINE NAME: SPREAD

PURPOSE:

This subroutine applies interpolation subroutine DIDIDA to singlet arrays to obtain an array of dependent variables versus an array of independent variables. It is extremely useful for obtaining singlet arrays of various dependent variables with a corresponding relationship to one singlet independent variable array. The dependent variable arrays thus constructed can then be operated on by array manipulation subroutines in order to form composite or complex functions. Doublet arrays can first be separated with subroutine SPLIT and later reformed with subroutine JOIN.

RESTRICTIONS:

All data values must be floating point except \( N \) which must be the integer length of the array to be constructed. The arrays fed into DIDIDA for interpolation must start with the integer count. \( X \) is for independent and \( Y \) is for dependent. \( I \) is for input and \( O \) is for output.

CALLING SEQUENCE:

SPREAD\((N,X(IC),Y(IC),XI(DV),YO(DV))\)
COMPARISON OPERATION

SUBROUTINE NAMES: MAXDAR or MXDRAL

PURPOSE:

These subroutines will obtain the absolute maximum difference between corresponding elements of two arrays of equal length N. The array values must be floating point numbers. The operation performed is

\[ D = \max_{i=1}^{N} |A_i - B_i| \]

Subroutine MXDRAL also locates the position P between 1 and N where the maximum occurs.

RESTRICTIONS:

The N argument must be an integer. The D and P arguments are returned as floating point numbers.

CALLING SEQUENCE:

MAXDAR(N,A(DV),B(DV),D)

or

MXDRAL(N,A(DV),B(DV),D,P)