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INDOOR TEST FOR THERMAL PERFORMANCE OF THE G. E. TC-100 LIQUID SOLAR COLLECTOR EIGHT- AND TEN-TUBE CONFIGURATION

Prepared by
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Under subcontract with IBM, Federal Systems Division, Huntsville, Alabama 35807

Contract NAS8-32036 with
National Aeronautics and Space Administration
George C. Marshall Space Flight Center, Alabama 35812

For the U. S. Department of Energy

U.S. Department of Energy
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1.0 PURPOSE

The purpose of this document is to present the test procedures used during the performance of an evaluation test program. The test program was established to obtain thermal performance data on the General Electric TC-100 eight tube and ten tube liquid solar collectors under simulation conditions. Each of the collectors was tested with and without the manufacturer's accessory manifold. The test program was accomplished by utilizing the MSFC Solar Simulator in accordance with the test requirements specified in Reference 2.1 and the procedures contained in Reference 2.2, except where noted in the test procedure to accommodate the unique requirements of vacuum tube collectors.

2.0 REFERENCES

2.1 ASHRAE 93-77 Method of Testing to Determine the Thermal Performance of Solar Collectors

2.2 HTCP-FA-SHAG-400 Procedure for Operation of the MSFC Solar Simulator Facility

3.0 COLLECTOR DESCRIPTION

Manufacturer: General Electric

Manufacturer's Address: P. O. Box 13601 Philadelphia, PA 19101

Model Number: TC-100 (8 tube, 10 tube)

Serial Number: 8 Tube (199658), 10 tube (Dwg. 298E44261, Ser. 2)

Reflector Mat'l: Coilzac (10 tube); Alglas (8 tube)

Type: Evacuated tube, with and without manufacturer's accessory manifold

Working Fluid: 35% (volume) Prestone and water

Gross Collector Area, Ft²: 17.41 (without manifold)

19.10 (with manifold)

Overall external dimensions:

Width, inches: 48.0

Length, inches: 57.25 (with manifold), 52.50 (without manifold)

Thickness, inches: 3.25

Aperture area, Ft²: 15.80

Collector Glazing: Evacuated tube

Weight, lbs: Empty - 60; Full - 62; Manifold - 15
This test program was performed to evaluate the thermal performance of the G.E. TC-100 eight and ten evacuated tube collectors, under simulated conditions. The ten tube collector, the predecessor of the eight tube collector, has a vee-trough reflector, and the eight tube collector has a parabolic trough reflector. Schematics of the ten and eight tube collectors are shown in Figures 1 and 2, respectively. The test conditions and the data obtained during the test program are listed in Tables I and II for the stagnation test results, with graphic presentations in Figures 3 and 4, respectively. Tables III and IV contain the data obtained for the thermal efficiency test results of the ten and eight tube configurations, respectively. The standard installation usage of the G.E. TC-100 collectors is without a cover, but due to special requirements in high vandalism areas the ten tube collector was tested with an acrylic cover plate and with a lexan cover plate to determine their effects on thermal efficiency. These results are presented in Table V for the acrylic and lexan covers. Figure 5 is a graphic comparison of the ten tube thermal efficiency with and without the covers. Figures 6 and 7 are graphical presentations of the ten and eight tube collectors with and without the accessory manifold. Figures 8 and 9 provide the thermal efficiency as a function of inlet temperature for the ten and eight tube collectors, respectively. Time constant and incident angle modifier tests were performed to determine the transient effects of time varying solar insolation on collector performance. The results of these tests are shown in Figures 10 and 11 for the time constant and incident angle modifier tests, respectively.

Normally, a nine point flux map is determined for a collector tested by a lamp array, but in the case of evacuated tubes, each tube works as an independent flat plate; therefore, three flux levels were taken for each tube. Typical flux maps are shown in Figures 12 and 13 for the ten and eight tube collectors, respectively. A comparison of the ten and eight tube thermal efficiencies with the manifold are shown in Figure 14.

In comparison, the eight tube configuration, which supercedes the ten tube, has a parabolic reflector which performs well at normal incidence angles (Figure 14) but is less efficient at angles larger than 20° (Figure 11); in fact, it is less effective at these angles than the original ten tube vee-trough reflector, as shown in Figure 11. This effect on projected all day performance is evident from comparison of data in Tables VII and IX.
5.0 TEST CONDITIONS AND TEST EQUIPMENT

5.1 Ambient Conditions

All tests will be performed at ambient conditions existing in MSFC Building 4619 at the time of the tests.

5.2 Instrumentation and Equipment

All test equipment and instrumentation to be used in the performance of this test program will comply with the requirements of MSFC MM 5300.4C, Metrology and Calibration. A standard test setup is depicted in Reference 2.2.

<table>
<thead>
<tr>
<th>Apparatus</th>
<th>Manufacturer/Model</th>
<th>Range/Accuracy</th>
</tr>
</thead>
<tbody>
<tr>
<td>Liquid Loop</td>
<td>MSFC Supplied</td>
<td>0.1 - 1.12 GPM</td>
</tr>
<tr>
<td>Flowmeter</td>
<td>Foxboro/1/2 - 2 C1T361</td>
<td>0.1 - 1.2 GPM + 1%</td>
</tr>
<tr>
<td>Platinum Resistance</td>
<td>Hycal</td>
<td>0 - 500°F + 0.1°F</td>
</tr>
<tr>
<td>Thermometer</td>
<td></td>
<td></td>
</tr>
<tr>
<td>Pressure Sensor</td>
<td>MSFC Supplied</td>
<td>0 - 5.0 PSI + 2%</td>
</tr>
<tr>
<td>Pyranometer</td>
<td>Eppley - PSP</td>
<td>0 - 800 BTU/Ft²•Hr (Class 1)</td>
</tr>
<tr>
<td>Fans</td>
<td>MSFC Supplied</td>
<td>N/A</td>
</tr>
<tr>
<td>Digital Printer</td>
<td>Doric - Digitrend 220</td>
<td>5 - 500 MV + 2%</td>
</tr>
<tr>
<td>Solar Simulator</td>
<td>MSFC Supplied</td>
<td>See Reference 2.2</td>
</tr>
<tr>
<td>Pressure Gauge</td>
<td>U. S. Gauge Co./Ashcroft</td>
<td>0 - 60 PSIG ± 1 PSI</td>
</tr>
</tbody>
</table>
6.0 TEST REQUIREMENTS AND PROCEDURES

6.1 Collector Preconditioning and Stagnation Test

6.1.1 Requirement

The collector shall be mounted on an outdoor passive test stand at an angle of 45° from the horizontal and facing south. The inlet and outlet ports to the collector shall be capped to prevent flow. The upper cap shall contain a small vent hole. The preconditioning shall consist of at least three days exposure during which the mean incident solar radiation measured in the plane of the collector shall be 1500 BTU/Ft²·day. During this preconditioning, the following data shall be recorded within two hours of solar noon when the insolation is constant and above a minimum of 200 BTU/Hr·Ft² in the plane of the collector. Data recorded shall be the average for at least a 20-minute period at quasi-steady state conditions.

1. Insolation rate.
2. Ambient temperature.
3. Wind velocity and direction.
4. Absorber surface temperature at either 4 or 5 locations.

6.1.2 Procedure

1. Mount test specimen as described above.
2. Connect instrumentation.
3. Record data as described above.

6.1.3 Results

Preconditioning of the G.E. TC-100 collectors was not required, as each had been previously exposed for more than three days. The stagnation tests were not performed in the usual outdoor manner but were accomplished utilizing the solar simulator. This provided a transient temperature history profile for the tubes at a constant flux of 300 BTU/Hr·Ft². The steady state results obtained during these tests are contained in Tables I and II for the ten and eight tube configurations, respectively. The respective transient temperature history profiles are presented in Figures 3 and 4.
6.0 TEST REQUIREMENTS AND PROCEDURES (Continued)

6.2 Collector Time Constant Test

6.2.1 Requirements

The collector time constant shall be determined by abruptly reducing the solar flux to zero. This will be done with the inlet temperature adjusted to within \( +2^\circ\text{F} \) of ambient while the liquid is flowing at 0.22 GPM, which is the manufacturer's recommended flowrate.

The differential temperature across the collector shall be monitored to determine the time required to reach the condition of:

\[
\frac{\Delta T(t)}{\Delta T_i} = 0.368
\]

where \( \Delta T(t) \) is the differential temperature at time \( t \) after the solar flux is reduced to zero and \( \Delta T_i \) is the differential temperature prior to the power down of the solar simulator. The liquid to be used as the collector heat transfer medium shall be as specified by the manufacturer. If this liquid is not specified, use water as the fluid.

The following data will be recorded for the test:

2. Ambient temperature.
3. Inlet liquid temperature.
5. Liquid flow rate.

6.2.2 Procedure

1. Adjust the liquid flow rate to 0.22 GPM.*
2. Adjust the inlet temperature to ambient \( \pm 2^\circ\text{F} \).
3. Power up the solar simulator and establish a solar flux level of 300 BTU/Ft\(^2\)·Hr.
4. Establish wind speed of 7.5 mph.
5. Record data for five minutes at above stabilized conditions.
7. Record the change of \( \Delta T \) across the collector.

* This is the manufacturer's recommended flowrate for the collector.
6.0 TEST REQUIREMENTS AND PROCEDURES (Continued)

6.2.3 Results

The results obtained during the time constant tests are shown in Figure 10. The average insolation was approximately 265 BTU/Hr-Ft$^2$ for the ten tube test and approximately 295 BTU/Hr-Ft$^2$ for the eight cube test. The eight tube collector was tested with the manifold and the ten tube collector was tested without the manifold.
TEST REQUIREMENTS AND PROCEDURES (Continued)

6.3 Collector Thermal Efficiency Test

6.3.1 Requirements

Utilizing the MSFC Solar Simulator and the portable closed liquid loop, parametric performance evaluation data shall be recorded of the following test variables and conditions. The liquid to be used is the manufacturer's recommended heat transfer fluid. The test shall be performed using a mixture of 35% glycol by volume as the working fluid.

<table>
<thead>
<tr>
<th>Variable/Condition</th>
<th>Requirement Guideline</th>
</tr>
</thead>
<tbody>
<tr>
<td>1. Collector inlet liquid temperature differential above existing ambient temperature level</td>
<td>$0^\circ F, 50^\circ F, 100^\circ F, 150^\circ F, 200^\circ F$</td>
</tr>
<tr>
<td>2. Collector outlet liquid temperature</td>
<td>Measured data</td>
</tr>
<tr>
<td>3. Incident solar flux level liquid</td>
<td>250, 300 BTU/Hr·Ft² $^\circ F$</td>
</tr>
<tr>
<td>4. Liquid flow rate through collector</td>
<td>0.22 GPM</td>
</tr>
<tr>
<td>5. Wind speed</td>
<td>7.5 MPH</td>
</tr>
<tr>
<td>6. Ambient air temperature</td>
<td>Existing room condition</td>
</tr>
<tr>
<td>7. Pressure</td>
<td>Sufficient to prevent boiling</td>
</tr>
</tbody>
</table>

6.3.2 Procedure

1. Mount test specimen on test table at a 45° angle with reference to the floor.
2. Assure that simulator lamp array is adjusted to an angle of 45° with reference to the floor.
3. Using the procedure contained in Reference 2.2, align the test table so the test specimen's vertical centerline coincides with the vertical centerline of the lamp array and the distance from the top of the test specimen to the lens plane of the lamp array is 9 feet.
4. Insulate all liquid lines.
5. Connect instrumentation leads to data acquisition system.
6. Assure that data acquisition system is operational.
7. Perform sensor accuracy verification tests.
6.0 TEST REQUIREMENTS AND PROCEDURES (Continued)

6.3 Collector Thermal Efficiency Test (Continued)

6.3.2 Procedure (Continued)

8. Establish required wind speed.

9. Start liquid flow loop and establish the required flow rate.

10. Establish the required inlet temperature.

11. Power up solar simulator in accordance with Reference 2.2 and establish the required solar flux level. Take a flux reading at top, middle and bottom of each tube.

12. Record data for a minimum of five minutes at these stabilized conditions.

13. Repeat Steps 9 through 12 as necessary to complete all the required test conditions.

14. Upon completion of testing, power down simulator and liquid loop in accordance with Reference 2.2.

6.3.3 Results

The results of the thermal efficiency tests are shown in Tables III through V and are presented graphically in Figures 5 through 9.
6.0 TEST REQUIREMENTS AND PROCEDURES (Continued)

6.4 Incident Angle Modifier Test

6.4.1 Requirements

The collector incident angle modifier shall be determined by tilting the collector at 0°, 10°, 20°, 30°, 40°, and 50° with respect to the solar simulator surface. The liquid flow rate shall be 0.22 ± 0.002 GPM with the inlet temperature controlled to within ± 2°F of ambient. The insolation rate shall be 300 BTU/Ft²•Hr. The liquid to be used is the manufacturer's recommended fluid. If not specified, the tests shall be performed using water as the heat transfer medium. The following data shall be recorded during the tests.

1. Collector tilt angles.
2. Ambient air temperature.
3. Collector inlet liquid temperature.
5. Collector differential temperature.
7. Incident solar flux level.
8. Liquid flow rate through the collector.

6.4.2 Procedure

1. Set up collector at required tilt angle.
2. Establish required flowrate.
3. Establish required inlet temperature.
4. Establish solar simulator flux level at 300 BTU/Ft²•Hr and measure the flux levels at 3 locations on each tube and record on data sheet.
5. Record data for five minutes at above stabilized conditions.
6. Repeat above steps as necessary to obtain required data for each tilt angle.

6.4.3 Results

The results of the incident angle modifier tests are presented in Tables VI and VII and are shown graphically in Figure 11.
7.0 ANALYSIS

7.1 Thermal Performance Test

The analysis of data contained in this report is in accordance with the National Bureau of Standards recommended approach. This approach is outlined below.

The efficiency of a collector is stated as:

\[ \eta = \frac{q_u}{I} = \frac{\dot{m} C_{tf} (t_{f,e} - t_{f,i})}{I} \]  

(1)

where:

- \( q_u \) = rate of useful energy extracted from the Solar Collector (BTU/Hr)
- \( A \) = Gross collector area (Ft²)
- \( I \) = Total solar energy incident upon the plane of the solar collector per unit time per unit area (BTU/Hr·Ft²)
- \( \dot{m} \) = Mass flow rate of the transfer liquid through the collector per unit area of the collector (Lbm/Ft²·Hr)
- \( C_{tf} \) = Specific heat of the transfer liquid (BTU/Lb·°F)
- \( t_{f,e} \) = Temperature of the transfer liquid leaving the collector (°F)
- \( t_{f,i} \) = Temperature of the transfer liquid entering the collector (°F)

Rewriting Equation (1) in terms of the total collector area yield:

\[ \eta = \frac{(\dot{m}A) C_{tf} (t_{f,e} - t_{f,i})}{(IA)} = \frac{\dot{m} C_{tf} (t_{f,e} - t_{f,i})}{P_i} \]  

(2)

Notice that:

- \( P_i = IA \) = Total Power Incident on the Collector.
- \( \dot{m}A = \dot{M} \) = Total Mass Flow Rate through the Collector.

Therefore, \( \dot{m} C_{tf} (t_{f,e} - t_{f,i}) \) = Total Power Collected by the Collector.
7.0 ANALYSIS (Continued)

7.1 Thermal Performance Test (Continued)

Substitution in Equation (2) results in:

\[ \% Eff. = \frac{P_{abs}}{P_{inc}} \times 100 \]  \hspace{1cm} (3)

where:

- \( P_{abs} \) = Total collected power
- \( P_{inc} \) = Total incident power

This value of efficiency is expressed as a percentage by multiplying by 100. This expression for percent efficiency is:

\[ \text{Collector Efficiency} = \frac{P_{abs}}{P_{inc}} \times 100 \]  \hspace{1cm} (4)

or, from Equation (2), collector efficiency is defined by the equation:

\[ \% \text{Eff.} = \frac{\dot{m} C_{tf} (t_{f,e} - t_{f,i})}{P_{i}} \times 100 \]  \hspace{1cm} (5)

Each term in Equation (5) was measured and recorded independently during the test. The calculated values of efficiency were determined at sixty-second intervals. The mean value of efficiency was determined over a five-minute period during which the test conditions remained in a quasi-steady state. Each five-minute period constitutes one "data point" as is graphically depicted on a plot of percent efficiency versus:

\[ \left( \frac{(t_{i} - t_{a})}{I} \right) \]

where:

- \( t_{i} \) = Liquid inlet temperature (°F)
- \( t_{a} \) = Ambient temperature (°F)
- \( I \) = Incident flux per unit area (BTU/HR·FT²)

The abscissa term \( \left( \frac{(t_{i} - t_{a})}{I} \right) \) was used to normalize the effect of operating at different values of \( I, t_{i} \) and \( t_{a} \).
Thermal performance tests were conducted for both the ten and eight tube configurations with and without the manufacturer's accessory manifold. Results for these tests are presented in Figures 6 through 9. The second-order polynomial to best describe the test results is given by:

\[
\text{Efficiency} = a_0 + a_1 \tau + a_2 \tau^2
\]

where:

\[
\tau = (T_i - T_a)/I
\]

The coefficients are listed below for the respective configuration:

**Flow Rate = 0.22 GPM**

<table>
<thead>
<tr>
<th></th>
<th>Ten Tube</th>
<th>Without Manifold</th>
<th>With Manifold</th>
</tr>
</thead>
<tbody>
<tr>
<td>(a_0)</td>
<td>0.479</td>
<td>0.398</td>
<td></td>
</tr>
<tr>
<td>(a_1)</td>
<td>-0.191</td>
<td>-0.145</td>
<td></td>
</tr>
<tr>
<td>(a_2)</td>
<td>-0.061</td>
<td>0.000</td>
<td></td>
</tr>
</tbody>
</table>

<table>
<thead>
<tr>
<th></th>
<th>Eight Tube</th>
<th>Without Manifold</th>
<th>With Manifold</th>
</tr>
</thead>
<tbody>
<tr>
<td>(a_0)</td>
<td>0.432</td>
<td>0.406</td>
<td></td>
</tr>
<tr>
<td>(a_1)</td>
<td>-0.078</td>
<td>-0.105</td>
<td></td>
</tr>
<tr>
<td>(a_2)</td>
<td>0.000</td>
<td>-0.030</td>
<td></td>
</tr>
</tbody>
</table>
7.0 **ANALYSIS (Continued)**

7.2 **Time Constant Test**

Two methods are proposed by ASHRAE 93-77 for conducting a time constant test; however, due to facility limitations, only the first method could be used. This method consisted of shutting down the simulator and maintaining a constant flow rate and inlet temperature while obtaining data.

According to the definition of time constant given in 93-77, it is the time required for the ratio of the differential temperature at time \( t \) to the initial differential temperature to reach .368. It can be expressed as:

\[
\frac{T_{f,e,\tau} - T_{f,i}}{T_{f,e,ini} - T_{f,i}} = .368
\]

If the inlet liquid temperature cannot be controlled to equal the ambient air temperature, then the following equation must be used:

\[
\frac{F_{RU}L \left( T_{f,i} - T_a \right) + \frac{mC_p}{A_g} \left( T_{f,e,\tau} - T_{f,i} \right)}{F_{RU}L \left( T_{f,i} - T_a \right) + \frac{mC_p}{A_g} \left( T_{f,e,ini} - T_{f,i} \right)} = .368
\]

where:

- \( T_{f,e,\tau} \): Exit liquid temperature at time \( \tau \)
- \( T_{f,i} \): Inlet liquid temperature
- \( T_{f,e,ini} \): Initial exit liquid temperature
- \( m \): Liquid mass flow rate, Lb/Hr
- \( C_p \): Specific heat of liquid, BTU/Lb.°F
- \( A_g \): Gross collector area, Ft²
- \( F_{RU}L \): Negative of the slope determined from the thermal efficiency curve

The inlet temperature was maintained within ± 2°F of the ambient, hence equation (1) was used for evaluation. From Figure 10 the time constant was determined to be 4 minutes and 16 seconds for the ten tube and 4 minutes and 35 seconds for the eight tube collector.
ANALYSIS (Continued)

7.3 Incident Angle Modifier Test

Two methods are proposed by ASHRAE 93-77 for incident angle modifier tests. For the MSFC Solar Simulator Facility, only method 1 (tilting the collector) is applicable. The collector was adjusted so that the incident radiation angles were 0°, 10°, 20°, 30°, 40°, and 50° to the normal of the collector surface. The collector was too large to tilt 60°.

According to 93-77, the incident angle modifier is defined as

\[ K(\gamma) = \frac{\eta}{F_R(\alpha)^n} \]

where \( \eta \) = efficiency at tilted angle.

\[ F_R(\alpha)^n = \text{Intercept of efficiency curve at normal incident angle} \]

For equation (1) to be applicable, the inlet liquid temperature must be controlled to within ±2°F of the ambient air temperature. In cases where the inlet liquid temperature cannot be controlled to within ±2°F, the following equation must be used to evaluate the incident angle modifier.

\[ K(\gamma) = \frac{\eta + F_{RUL}}{F_R(\alpha)^n} \frac{T_{f,i} - T_a}{1} \]

where

\( F_{RUL} \) is the negative of the slope determined from the thermal efficiency curve.

Tables VI and VII show that the inlet liquid temperatures were not all within ±2°F of ambient air temperature. Hence, equation (2) was used for evaluation.

Appropriate values of \( F_R(\alpha)^n \) and \( F_{RUL} \) were used for the ten and eight tube configurations. The results of these computations are shown plotted against incident angle in Figure 11.
7.0 ANALYSIS (Continued)

7.3 Incident Angle Modifier Test (Continued)

The purpose of the incident angle modifier is to allow a designer or analyst to predict the total daily energy output from the collector, as the sun tracks from east to west. Most collectors are more efficient at normal incidence than at other angles, but some are even more efficient at angles other than normal. The only common ground for comparing collectors should be the "all day efficiency" rather than FRαCγ. However, the prospective application of the collector also influences the value of "all day efficiency." That is, for low temperature applications such as space heating or domestic hot water, a typical flat plate collector may have an all day efficiency of 40%, but for solar cooling applications the all day efficiency might be 20%. Therefore, criteria should be established to rate each collector for space heating, domestic hot water, and solar cooling at a nominal location, because efficiencies are also dependent on outdoor ambient temperatures.

Evacuated tubes are effective for solar cooling applications; therefore, according to the procedure in NBSIR 78-1305A the all day efficiency of the ten tube collector is 28 per cent and 26 per cent for the eight tube collector for a typical solar cooling application. The selected site dependent data in conjunction with test data used in these determinations is shown in Tables VIII and IX. No standard criteria has been established for "all day efficiency"; and these calculations are dependent on system operating parameters, site data, time of year and daily weather; therefore, the above information should be viewed as interesting but not conclusive.
TABLE I

G.E. TC-100 TEN TUBE STAGNATION TEMPERATURES

(See Figure 3)

<table>
<thead>
<tr>
<th>TUBE NO.</th>
<th>2</th>
<th>2</th>
<th>2</th>
<th>7</th>
<th>7</th>
<th>7</th>
<th>9</th>
<th>9</th>
<th>9</th>
</tr>
</thead>
<tbody>
<tr>
<td>SENSRCR LOCATION</td>
<td>A</td>
<td>B</td>
<td>C</td>
<td>A</td>
<td>B</td>
<td>C</td>
<td>A</td>
<td>B</td>
<td>C</td>
</tr>
<tr>
<td>INSOLATION BTU/HR·FT²</td>
<td>329.8</td>
<td>287.0</td>
<td>310.4</td>
<td>309.2</td>
<td>291.4</td>
<td>313.1</td>
<td>314.7</td>
<td>315.5</td>
<td>298.8</td>
</tr>
<tr>
<td>TEMP. °F NO COVER</td>
<td>640</td>
<td>651</td>
<td>556</td>
<td>525</td>
<td>534</td>
<td>456</td>
<td>614</td>
<td>614</td>
<td>614</td>
</tr>
</tbody>
</table>

NOTE: Tube #7 was interchanged with tube #2 and was found to produce noticeably lower temperatures in that position also. Performance data reported for the ten tube collector may be somewhat lower than normal if tube #7 is determined to be low on collection capacity.
TABLE II

G.E. TC-100 EIGHT TUBE COLLECTOR
STAGNATION TEMPERATURES

(See Figure 4)

<table>
<thead>
<tr>
<th>Tube No.</th>
<th>1</th>
<th>1</th>
<th>1</th>
<th>8</th>
<th>8</th>
<th>8</th>
</tr>
</thead>
<tbody>
<tr>
<td>Sensor Location</td>
<td>A</td>
<td>B</td>
<td>C</td>
<td>A</td>
<td>B</td>
<td>C</td>
</tr>
<tr>
<td>Insolation BTU/HR-Ft²</td>
<td>314.7</td>
<td>275.6</td>
<td>292.0</td>
<td>277.9</td>
<td>285.3</td>
<td>277.9</td>
</tr>
<tr>
<td>Temperature °F</td>
<td>499.9</td>
<td>599.6</td>
<td>601.6</td>
<td>529.5</td>
<td>645.1</td>
<td>663.4</td>
</tr>
</tbody>
</table>
### TABLE III
**Thermal Performance Test Data for the G.E. TC-100 Ten Tube Collector Without Accessory Manifold**

<p>| Ambient Air Temperature ($T_a$), °F | 73.2 | 76.9 | 74.4 | 77.4 | 78.5 | 75.6 | 75.1 | 83.3 | 79.2 | 76.6 | 77.0 | 79.8 | 72.0 | 78.0 | 85.6 | 80.1 |
|----------------------------------|------|------|------|------|------|------|------|------|------|------|------|------|------|------|------|------|------|
| Fluid Inlet Temperature ($T_i$), °F | 87.4 | 86.7 | 88.5 | 83.0 | 91.3 | 100.8 | 100.8 | 123.5 | 128.3 | 125.7 | 125.7 | 154.0 | 147.1 | 150.9 | 151.5 | 179.9 |
| Fluid Outlet Temperature ($T_o$), °F | 106.9 | 108.5 | 111.8 | 109.2 | 111.5 | 119.8 | 123.4 | 102.9 | 146.3 | 143.8 | 148.1 | 117.1 | 164.7 | 172.5 | 169.3 | 195.8 |
| Differential Fluid Temperature ($\Delta T$), °F | 19.5 | 21.8 | 23.3 | 26.2 | 20.2 | 19.0 | 22.6 | 19.4 | 18.0 | 18.1 | 22.4 | 17.2 | 17.6 | 21.8 | 17.8 | 15.9 |
| Total Solar Flux (I), BTU/Hr·Ft² | 248.4 | 246.3 | 329.8 | 229.1 | 249.5 | 246.2 | 229.9 | 324.9 | 524.8 | 524.2 | 224.6 | 229.3 | 246.2 | 247.5 | 299.3 | 249.5 | 246.2 |
| Flow Rate, GPM | 0.228 | 0.210 | 0.227 | 0.220 | 0.220 | 0.228 | 0.231 | 0.230 | 0.233 | 0.228 | 0.226 | 0.234 | 0.224 | 0.218 | 0.221 | 0.233 |
| ($T_i-T_a$)/I, °F·Hr·Ft²/BTU | .06 | .04 | .05 | .02 | .05 | .10 | .09 | .160 | .198 | .20 | .16 | .301 | .30 | .24 | .26 | .406 |
| Efficiency ($\eta$), % | 45.7 | 49.9 | 45.3 | 49.2 | 46.2 | 45.5 | 45.1 | 45.3 | 44.1 | 43.8 | 44.2 | 42.9 | 41.8 | 41.7 | 41.2 | 39.7 |</p>
<table>
<thead>
<tr>
<th>Ambient Air Temperature (Ta), °F</th>
<th>88.8</th>
<th>89.0</th>
<th>82.2</th>
<th>82.3</th>
<th>78.3</th>
</tr>
</thead>
<tbody>
<tr>
<td>Fluid Inlet Temperature (T1), °F</td>
<td>716.6</td>
<td>614.4</td>
<td>217.4</td>
<td>74.7</td>
<td>82.3</td>
</tr>
<tr>
<td>Fluid Outlet Temperature (T2), °F</td>
<td>739.0</td>
<td>655.1</td>
<td>194.6</td>
<td>105.4</td>
<td>104.2</td>
</tr>
<tr>
<td>Differential Fluid Temperature (ΔT), °F</td>
<td>22.4</td>
<td>20.9</td>
<td>19.9</td>
<td>22.6</td>
<td>22.6</td>
</tr>
<tr>
<td>Total Solar Flux (I), BTU/ft²</td>
<td>296.4</td>
<td>296.4</td>
<td>4296.4</td>
<td>299.9</td>
<td>2301.2</td>
</tr>
<tr>
<td>Flow Rate, GPM</td>
<td>0.22</td>
<td>0.22</td>
<td>0.22</td>
<td>0.23</td>
<td>0.23</td>
</tr>
<tr>
<td>Efficiency (η), %</td>
<td>0.38</td>
<td>0.36</td>
<td>0.39</td>
<td>0.35</td>
<td>0.40</td>
</tr>
</tbody>
</table>

TABLE III (Continued)
TABLE IV

THERMAL PERFORMANCE TEST DATA FOR THE G.E. TC-100 EIGHT TUBE COLLECTOR WITH ACCESSORY MANIFOLD

<table>
<thead>
<tr>
<th>Ambient Air Temperature ($T_a$), °F</th>
<th>85.8</th>
<th>82.9</th>
<th>80.1</th>
<th>79.4</th>
<th>78.4</th>
<th>77.2</th>
<th>76.0</th>
<th>81.8</th>
</tr>
</thead>
<tbody>
<tr>
<td>Fluid Inlet Temperature ($T_i$), °F</td>
<td>246.7</td>
<td>194.2</td>
<td>155.6</td>
<td>129.9</td>
<td>113.3</td>
<td>80.0</td>
<td>80.1</td>
<td>82.3</td>
</tr>
<tr>
<td>Fluid Outlet Temperature ($T_o$), °F</td>
<td>264.1</td>
<td>211.9</td>
<td>173.4</td>
<td>148.3</td>
<td>132.4</td>
<td>100.2</td>
<td>103.3</td>
<td>105.4</td>
</tr>
<tr>
<td>Differential Fluid Temperature ($\Delta T$), °F</td>
<td>17.4</td>
<td>17.7</td>
<td>17.8</td>
<td>18.4</td>
<td>19.1</td>
<td>20.2</td>
<td>23.2</td>
<td>23.1</td>
</tr>
<tr>
<td>Total Solar Flux (I), BTU/Hr·Ft²</td>
<td>267.1</td>
<td>267.1</td>
<td>252.6</td>
<td>252.6</td>
<td>252.6</td>
<td>252.6</td>
<td>291.2</td>
<td>295.2</td>
</tr>
<tr>
<td>Flow Rate, lb/min.</td>
<td>1.80</td>
<td>1.85</td>
<td>1.85</td>
<td>1.87</td>
<td>1.90</td>
<td>1.94</td>
<td>1.85</td>
<td>1.85</td>
</tr>
<tr>
<td>([T_i - T_a]/I) °F·Hr·Ft²/BTU</td>
<td>.602</td>
<td>.417</td>
<td>.299</td>
<td>.200</td>
<td>.138</td>
<td>.011</td>
<td>.014</td>
<td>.002</td>
</tr>
<tr>
<td>Efficiency ($\eta$)</td>
<td>34.1</td>
<td>35.3</td>
<td>36.9</td>
<td>38.1</td>
<td>39.8</td>
<td>42.2</td>
<td>48.5</td>
<td>39.5</td>
</tr>
</tbody>
</table>
TABLE IV (Continued)

THERMAL PERFORMANCE TEST DATA FOR THE G.E. TC-100 EIGHT TUBE COLLECTOR WITH ACCESSORY MANIFOLD

<table>
<thead>
<tr>
<th>Ambient Air Temperature ($T_a$), °F</th>
<th>76.7</th>
<th>77.1</th>
<th>77.5</th>
<th>77.9</th>
<th>77.6</th>
<th>78.7</th>
<th>78.4</th>
<th>81.5</th>
<th>84.7</th>
</tr>
</thead>
<tbody>
<tr>
<td>Fluid Inlet Temperature ($T_i$), °F</td>
<td>106.1</td>
<td>109.2</td>
<td>131.1</td>
<td>128.2</td>
<td>144.5</td>
<td>151.9</td>
<td>197.8</td>
<td>250.3</td>
<td>281.3</td>
</tr>
<tr>
<td>Fluid Outlet Temperature ($T_o$), °F</td>
<td>128.2</td>
<td>131.8</td>
<td>152.8</td>
<td>150.6</td>
<td>165.7</td>
<td>173.2</td>
<td>217.7</td>
<td>268.7</td>
<td>296.3</td>
</tr>
<tr>
<td>Differential Fluid Temperature ($ΔT$), °F</td>
<td>22.1</td>
<td>22.6</td>
<td>21.7</td>
<td>22.4</td>
<td>21.2</td>
<td>19.2</td>
<td>19.9</td>
<td>18.4</td>
<td>15.0</td>
</tr>
<tr>
<td>Total Solar Flux (I), BTU/Hr·Ft²</td>
<td>291.2</td>
<td>298.1</td>
<td>291.2</td>
<td>298.1</td>
<td>291.2</td>
<td>298.1</td>
<td>291.2</td>
<td>297.9</td>
<td>267.1</td>
</tr>
<tr>
<td>Flow Rate', lb/min.</td>
<td>1.90</td>
<td>1.85</td>
<td>1.87</td>
<td>1.80</td>
<td>1.87</td>
<td>1.84</td>
<td>1.87</td>
<td>1.80</td>
<td>1.80</td>
</tr>
<tr>
<td>$(T_i - T_a)/I$ °F·Hr·Ft²/BTU</td>
<td>.101</td>
<td>.108</td>
<td>.184</td>
<td>.169</td>
<td>.233</td>
<td>.245</td>
<td>.410</td>
<td>.567</td>
<td>.736</td>
</tr>
<tr>
<td>Efficiency ($η$), %</td>
<td>39.8</td>
<td>38.8</td>
<td>38.2</td>
<td>37.9</td>
<td>38.4</td>
<td>37.2</td>
<td>36.7</td>
<td>32.3</td>
<td>30.4</td>
</tr>
</tbody>
</table>
TABLE IV (Continued)  
THERMAL PERFORMANCE TEST DATA FOR THE G.E. TC-100 EIGHT TUBE COLLECTOR WITHOUT ACCESSORY MANIFOLD

<table>
<thead>
<tr>
<th>Parameter</th>
<th>74.0</th>
<th>77.8</th>
<th>82.8</th>
<th>84.3</th>
<th>87.2</th>
<th>81.9</th>
<th>83.2</th>
<th>80.3</th>
</tr>
</thead>
<tbody>
<tr>
<td>Ambient Air Temperature ($T_a$), °F</td>
<td></td>
<td></td>
<td></td>
<td></td>
<td></td>
<td></td>
<td></td>
<td></td>
</tr>
<tr>
<td>Fluid Inlet Temperature ($T_i$), °F</td>
<td>82.2</td>
<td>149.2</td>
<td>204.2</td>
<td>252.5</td>
<td>250.6</td>
<td>203.9</td>
<td>150.1</td>
<td>85.2</td>
</tr>
<tr>
<td>Fluid Outlet Temperature ($T_e$), °F</td>
<td>102.5</td>
<td>168.2</td>
<td>221.6</td>
<td>269.8</td>
<td>272.1</td>
<td>227.0</td>
<td>173.1</td>
<td>111.0</td>
</tr>
<tr>
<td>Differential Fluid Temperature ($\Delta T$), °F</td>
<td>20.3</td>
<td>19.0</td>
<td>17.4</td>
<td>17.3</td>
<td>20.5</td>
<td>23.1</td>
<td>23.0</td>
<td>25.8</td>
</tr>
<tr>
<td>Total Solar Flux (I), BTU/Hr·Ft²</td>
<td>260.7</td>
<td>260.7</td>
<td>261.6</td>
<td>261.1</td>
<td>315.0</td>
<td>313.1</td>
<td>317.9</td>
<td>317.9</td>
</tr>
<tr>
<td>Flow Rate, lb/min.</td>
<td>1.83</td>
<td>1.83</td>
<td>1.90</td>
<td>1.80</td>
<td>1.80</td>
<td>1.70</td>
<td>1.83</td>
<td>1.75</td>
</tr>
<tr>
<td>($T_i - T_a$)/I °F·Hr·Ft²/BTU</td>
<td>0.031</td>
<td>0.274</td>
<td>0.464</td>
<td>0.656</td>
<td>0.519</td>
<td>0.390</td>
<td>0.210</td>
<td>0.015</td>
</tr>
<tr>
<td>Efficiency ($\eta$)</td>
<td>43.0</td>
<td>41.9</td>
<td>40.0</td>
<td>38.6</td>
<td>37.9</td>
<td>39.7</td>
<td>41.6</td>
<td>42.8</td>
</tr>
</tbody>
</table>
### TABLE V

THERMAL PERFORMANCE TEST DATA FOR THE G.E. TC-100 TEN TUBE COLLECTOR WITHOUT ACCESSORY MANIFOLD FOR A LEXAN COVER AND AN ACRYLIC COVER

<table>
<thead>
<tr>
<th></th>
<th>With Lexan Cover</th>
<th>With Acrylic Cover</th>
</tr>
</thead>
<tbody>
<tr>
<td>Ambient Air Temperature (T_a), °F</td>
<td>79.6 83.1 85.7 79.0 84.2</td>
<td>80.2 82.2 85.7 78.5 84.7</td>
</tr>
<tr>
<td>Fluid Inlet Temperature (T_i), °F</td>
<td>91.1 123.5 151.7 175.8 242.0</td>
<td>91.1 123.7 151.7 175.8 242.8</td>
</tr>
<tr>
<td>Fluid Outlet Temperature (T_e), °F</td>
<td>110.1 140.4 167.2 190.9 252.4</td>
<td>109.5 141.0 167.8 190.7 253.5</td>
</tr>
<tr>
<td>Differential Fluid Temperature (\Delta T), °F</td>
<td>19.0 16.9 15.5 15.1 10.4</td>
<td>18.4 17.3 16.1 14.9 10.7</td>
</tr>
<tr>
<td>Total Solar Flux (I), BTU/Hr·Ft²</td>
<td>249.5 249.5 249.5 249.5 249.5</td>
<td>249.5 249.5 249.5 249.5 249.5</td>
</tr>
<tr>
<td>Flow Rate, GPM</td>
<td>0.216 0.221 0.224 0.221 0.224</td>
<td>0.222 0.222 0.223 0.224 0.220</td>
</tr>
<tr>
<td>(\frac{(T_i-T_a)}{I}) °F·Hr·Ft²/BTU</td>
<td>0.05 0.16 0.26 0.38 0.65</td>
<td>0.05 0.16 0.26 0.38 0.65</td>
</tr>
<tr>
<td>Efficiency (\eta), %</td>
<td>42.5 39.1 36.7 35.3 24.7</td>
<td>42.3 40.2 38.0 35.3 24.1</td>
</tr>
<tr>
<td>Angle</td>
<td>0°</td>
<td>10°</td>
</tr>
<tr>
<td>-------</td>
<td>----</td>
<td>-----</td>
</tr>
<tr>
<td>Ambient Air Temperature (T&lt;sub&gt;a&lt;/sub&gt;, °F)</td>
<td>82.2</td>
<td>78.5</td>
</tr>
<tr>
<td>Fluid Inlet Temperature (T&lt;sub&gt;i&lt;/sub&gt;, °F)</td>
<td>93.6</td>
<td>93.5</td>
</tr>
<tr>
<td>Fluid Outlet Temperature (T&lt;sub&gt;f&lt;/sub&gt;, °F)</td>
<td>111.9</td>
<td>111.7</td>
</tr>
<tr>
<td>Differential Fluid Temperature (ΔT&lt;sub&gt;f&lt;/sub&gt;, °F)</td>
<td>18.3</td>
<td>18.2</td>
</tr>
<tr>
<td>Total Solar Flux (I), BTU/HR-Ft&lt;sup&gt;2&lt;/sup&gt;</td>
<td>243.0</td>
<td>231.3</td>
</tr>
<tr>
<td>Flow Rate, GPM</td>
<td>0.230</td>
<td>0.227</td>
</tr>
<tr>
<td>Efficiency (η), %</td>
<td>44.7</td>
<td>46.4</td>
</tr>
<tr>
<td>Adjusted Efficiency Ratio K&lt;sub&gt;A&lt;/sub&gt;</td>
<td>.96</td>
<td>1.004</td>
</tr>
</tbody>
</table>
TABLE VII
INCIDENT ANGLE MODIFIER TEST DATA
FOR THE G.E. TC-100 EIGHT TUBE COLLECTOR

<table>
<thead>
<tr>
<th>Angle</th>
<th>0°</th>
<th>10°</th>
<th>20°</th>
<th>30°</th>
<th>40°</th>
<th>50°</th>
<th>0°</th>
<th>0°</th>
<th>0°</th>
</tr>
</thead>
<tbody>
<tr>
<td>Ambient Air Temperature ((T_a)), °F</td>
<td>83.6</td>
<td>80.4</td>
<td>84.1</td>
<td>79.3</td>
<td>84.5</td>
<td>79.0</td>
<td>77.2</td>
<td>76.0</td>
<td>81.8</td>
</tr>
<tr>
<td>Fluid Inlet Temperature ((T_i)), °F</td>
<td>93.3</td>
<td>89.6</td>
<td>93.5</td>
<td>88.9</td>
<td>93.0</td>
<td>88.9</td>
<td>80.0</td>
<td>80.1</td>
<td>82.3</td>
</tr>
<tr>
<td>Fluid Outlet Temperature ((T_e)), °F</td>
<td>117.3</td>
<td>111.4</td>
<td>114.3</td>
<td>104.3</td>
<td>105.3</td>
<td>98.4</td>
<td>100.2</td>
<td>103.3</td>
<td>105.4</td>
</tr>
<tr>
<td>Differential Fluid Temperature ((\Delta T)), °F</td>
<td>24.0</td>
<td>21.8</td>
<td>20.8</td>
<td>15.4</td>
<td>12.3</td>
<td>9.5</td>
<td>20.2</td>
<td>23.2</td>
<td>23.1</td>
</tr>
<tr>
<td>Total Solar Flux ((I)), BTU/Hr·Pt²</td>
<td>290.2</td>
<td>289.8</td>
<td>274.1</td>
<td>249.3</td>
<td>220.7</td>
<td>181.2</td>
<td>252.6</td>
<td>291.2</td>
<td>295.2</td>
</tr>
<tr>
<td>Flow Rate, lb/min.</td>
<td>1.80</td>
<td>1.95</td>
<td>1.80</td>
<td>1.90</td>
<td>1.80</td>
<td>1.86</td>
<td>1.94</td>
<td>1.85</td>
<td>1.85</td>
</tr>
<tr>
<td>Efficiency ((\eta)), %</td>
<td>41.2</td>
<td>39.5</td>
<td>37.8</td>
<td>32.4</td>
<td>27.7</td>
<td>27.7</td>
<td>42.2</td>
<td>40.1</td>
<td>39.5</td>
</tr>
<tr>
<td>Adjusted Efficiency Ratio (K&lt;\bar{\kappa})</td>
<td>1.025</td>
<td>0.983</td>
<td>0.942</td>
<td>0.810</td>
<td>0.695</td>
<td>0.683</td>
<td>1.040</td>
<td>0.990</td>
<td>0.970</td>
</tr>
</tbody>
</table>
TABLE VIII
G.E. TC-100 TEN TUBE CALCULATED ALL DAY EFFICIENCY

<table>
<thead>
<tr>
<th>CALCULATION STEPS</th>
<th>HOUR OF THE DAY, SOLAR TIME</th>
<th>DAILY TOTAL</th>
</tr>
</thead>
<tbody>
<tr>
<td></td>
<td>6-7</td>
<td>7-8</td>
</tr>
<tr>
<td>1. Inlet fluid temp. to collector, $t_f,i$</td>
<td>185</td>
<td>185</td>
</tr>
<tr>
<td>2. Ambient air temp., $t_a$</td>
<td>73</td>
<td>74</td>
</tr>
<tr>
<td>3. Incident radiation on collector plane, $I_T$</td>
<td>6</td>
<td>60</td>
</tr>
<tr>
<td>(Table A2, ASHRAE 93-77)</td>
<td></td>
<td></td>
</tr>
<tr>
<td>3a. $T_f - T_a / I_T$ (°F-yr-ft²/BTU)</td>
<td>18.0</td>
<td>1.85</td>
</tr>
<tr>
<td>4. Collector thermal efficiency at normal incidence, determined in accordance with Sections 8.3.2 and 8.5 of ASHRAE 93-77 and using data from Lines 1, 2 and 3</td>
<td>0</td>
<td>.16*</td>
</tr>
<tr>
<td>5. Incident angle between direct solar beam and outward drawn normal to collector plane, $\theta_d$</td>
<td>90</td>
<td>75</td>
</tr>
<tr>
<td>6. Incident angle modifier, determined in accordance with Sections 0.3.3 &amp; 8.6 of ASHRAE 93-77 and using the value of $\theta$ from Line 5</td>
<td>-</td>
<td>.55*</td>
</tr>
<tr>
<td>7. Energy output from collector [Line 3 $\times$ Line 4 $\times$ Line 6]</td>
<td>5.3</td>
<td>31.4</td>
</tr>
<tr>
<td>8. Collector thermal efficiency, Line 7/Line 3</td>
<td></td>
<td></td>
</tr>
</tbody>
</table>

Example: 32°N Lat. Avg. - Clear Skies 42° Tilt

* Estimated or extrapolated values.
# TABLE IX

**G.E. TC-100 EIGHT TUBE CALCULATED ALL DAY EFFICIENCY**

<table>
<thead>
<tr>
<th>CALCULATION STEPS</th>
<th>HOUR OF THE DAY, SOLAR TIME</th>
<th>DAILY TOTAL</th>
</tr>
</thead>
<tbody>
<tr>
<td></td>
<td>6-7</td>
<td>7-8</td>
</tr>
<tr>
<td>1. Inlet fluid temp. to collector, ( tf,i )</td>
<td>185</td>
<td>185</td>
</tr>
<tr>
<td>2. Ambient air temp., ( t_a )</td>
<td>73</td>
<td>74</td>
</tr>
<tr>
<td>3. Incident radiation on collector plane, ( I_T ) <em>(Table A2, ASHRAE 93-77)</em></td>
<td>6</td>
<td>60</td>
</tr>
<tr>
<td>3a. ( T_{fi}-T_a/\sqrt{I_T} ) <em>(oF-\sqrt{Btu/ft^2}/BTU)</em></td>
<td>18.1</td>
<td>1.85</td>
</tr>
<tr>
<td>4. Collector thermal efficiency at normal incidence, determined in accordance with Sections 8.3.2 and 8.5 of ASHRAE 93-77 and using data from Lines 1, 2 and 3</td>
<td>0</td>
<td>0.21*</td>
</tr>
<tr>
<td>5. Incident angle between direct solar beam and outward drawn normal to collector plane, ( \Theta_d )</td>
<td>90</td>
<td>75</td>
</tr>
<tr>
<td>6. Incident angle modifier, determined in accordance with Sections 8.3.3 &amp; 8.6 of ASHRAE 93-77 and using the value of ( \Theta ) from Line 5</td>
<td>0</td>
<td>0.40*</td>
</tr>
<tr>
<td>7. Energy output from collector [Line 3 x Line 4 x Line 6]</td>
<td>5.0</td>
<td>27.8</td>
</tr>
<tr>
<td>8. Collector thermal efficiency, Line 7/Line 3</td>
<td></td>
<td></td>
</tr>
</tbody>
</table>

Example: 32°N Lat. Avg. - Clear Skies

*Estimated or extrapolated values.

42° Tilt
Sensors were mounted in tubes 2, 7, and 9 at the positions of A, B, and C.

Figure 1. G.E. TC-100 Ten Tube Solar Collector Configuration
Gross Area = 19.1 Ft²
With Manifold
Gross Area = 17.41 Ft²
Without Manifold
Aperture Area = 15.80 Ft²

Temperature Sensors 80 and 81 were used for efficiency calculations for the no-manifold case.

Figure 2. Instrumentation Locations for the G.E. TC-100 Eight Tube Solar Collector Test
Figure 3. Stagnation Temperature History for the G.E. TC-100 Ten Tube Solar Collector.
Notes: (1.) 300 BTU/Hr-Ft²
(2.) Air Vent Located on Outlet Near Tube 1 (See Figure 1)

Figure 4. Stagnation Temperature History for the G.E. TC-100 Eight Tube Solar Collector
Figure 5. Thermal Efficiency of the G.E. TC-100 Ten Tube Collector
With Cover Plate

Notes: Wind @ 7.5 MPH
35% Glycol by Volume
250 BTUH
0.22 GPM Flowrate
Without Manifold, Gross Area = 17.41 ft²
Figure 6. Thermal Efficiency of the G.E. TC-100 Ten Tube Collector with and Without the Accessory Manifold
Second Order Curve Fit, Gross Area = 19.1 Ft$^2$ With Manifold
Based on Aperture Area - 15.8 Ft$^2$
Flow Rate - 0.22 GPM
Wind @ 7.5 MPH
35% Glycol by Volume
Ambient Temperature 75°F to 85°F

Figure 8. Thermal Efficiency of the G.E. TC-100 Ten Tube Solar Collector As a Function of Inlet Temperature
Figure 9. Thermal Efficiency of the G.E. TC-100 Eight Tube Solar Collector as a Function of Inlet Temperature

- Second Order Curve Fit
- Gross Area = 19.1 ft² With Manifold
- Gross Area = 17.41 ft² Without Manifold
- Based on Aperture Area - 15.8 ft²
- Flow Rate - 0.22 GPM
- Wind at 7.5 MPH
- 35% Glycol by Volume
- Ambient Temperature 75°F to 85°F
Figure 10. Time Constant Test of the Gil: TC-100 Ten and Eight Tube Solar Collectors

<table>
<thead>
<tr>
<th>Time (Minutes)</th>
<th>Without Manifold</th>
<th>With Manifold</th>
</tr>
</thead>
<tbody>
<tr>
<td>1</td>
<td></td>
<td>A</td>
</tr>
<tr>
<td>2</td>
<td></td>
<td>A</td>
</tr>
<tr>
<td>3</td>
<td></td>
<td>A</td>
</tr>
<tr>
<td>4</td>
<td></td>
<td>A</td>
</tr>
<tr>
<td>5</td>
<td></td>
<td>A</td>
</tr>
<tr>
<td>6</td>
<td></td>
<td>A</td>
</tr>
<tr>
<td>7</td>
<td></td>
<td>A</td>
</tr>
</tbody>
</table>

<table>
<thead>
<tr>
<th>Differential Temperature (°F)</th>
<th>20</th>
<th>10</th>
<th>0</th>
</tr>
</thead>
</table>

Eight Tube Configuration (295 Btu/h)
Ten Tube Configuration (265 Btu/h)
Figure 14. Comparison of the G.E. TC-100 Ten and Eight Tube Collector Efficiencies