Current Status of Liquid Sheet Radiator Research

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CURRENT STATUS OF LIQUID SHEET RADIATOR RESEARCH

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ABSTRACT

Initial research on the external flow, low mass liquid sheet radiator (LSR), has been concentrated on understanding its fluid mechanics. The surface tension forces acting at the edges of the sheet produce a triangular planform for the radiating surface of width, W, and length, L. It has been experimentally verified that $L/W$ agrees with the theoretical result, $L/W = (We/8)^{1/2}$, where $We$ is the Weber number. Instability can cause holes to form in regions of large curvature such as where the edge cylinders join the sheet of thickness, $\tau$. The $W/\tau$ limit that will cause hole formation with subsequent destruction of the sheet has yet to be reached experimentally.

Although experimental measurements of sheet emissivity have not yet been performed because of limited program scope, calculations of the emissivity and sheet lifetime as determined by evaporation losses were made for two silicon based oils; D.C. 705 and Me2. Emissivities greater than 0.75 are calculated for $\tau \geq 200 \mu m$ for both oils. Lifetimes for Me2 are much longer than lifetimes for 705. Therefore, Me2 is the more attractive working fluid for higher temperatures ($T \geq 400$ K).

CURRENT STATUS OF LIQUID SHEET RADIATOR RESEARCH

Introduction

The liquid sheet radiator (LSR) is an external flow radiator similar in several ways to other external flow radiators such as the liquid droplet [1-3] (LDR) and liquid belt radiators [4,5]. All of these radiator concepts potentially have lower mass than solid wall radiators such as pumped loop and heat pipe radiators. They are also nearly immune to micrometeoroid penetration. However, the LSR has the additional advantage of simplicity. As a result of surface tension forces acting at the edges of the sheet, the sheet flow has a triangular shape (Fig.1) which is desirable as it allows collection of the flow at a single point. To obtain a similar triangular area for the LDR requires very accurate aiming of many ($10^4$ to $10^5$) droplet streams.
Simplicity of the LSR should also result in lower cost and mass for the LSR compared to the LDR and liquid belt radiators (LBR).

A major problem for all external flow radiators is the requirement that the working fluid have a very low (<10⁻⁸ Torr) vapor pressure to minimize evaporative losses. As a result, working fluids are limited to certain silicon based oils (such as used in diffusion pumps) for low temperatures (300 to 400 K) and liquid metals for higher temperatures [1].

Figure 1 is a schematic drawing of a liquid sheet flow. Surface tension forces at the two edges of the sheet push the edges toward the z axis. As a result, as the flow moves in the z direction the edge cross-sectioned area, $A_c$, grows. In order to satisfy mass continuity the edges approach each other and finally meet at the point $z = L$. Figure 2 is a photograph of a small scale sheet flow of Dow-Corning 704 oil in vacuum. The growth of the edge cylinders can be seen in this photograph. If a gas surrounded the sheet flow the associated drag force would tend to break up the sheet flow. Whether or not sheet breakup occurs depends on the velocity and ratio of the sheet liquid density to the surrounding gas density.

Currently the LSR is only at the research stage of development. No system hardware, other than the narrow slits used to form the sheets, has been developed. However, a schematic drawing of a possible LSR space radiator is shown in Fig. 3. This shows four sheet flows connected in parallel. The number of sheets required for an actual application will be determined by the heat load. The system consists of three main components; a slit ejector, a collector, and a pump to produce the necessary flow. In Fig. 3 a heat exchanger is shown between the thermal load and the sheet flows. This heat exchanger is not necessary if the thermal load is compatible with the sheet liquid. The temperature drop that occurs between the ejector and collector is very small so that the LSR behaves like a constant temperature radiator, similar to a heat pipe radiator.

Initial research on the LSR has been directed at understanding the fluid mechanics of sheet flows [6,7]. There has also been a systems study [8] of the LSR in low power (2 kW) Closed Brayton (CBC) and Free Piston Stirling (FPS) cycles. In that study, with the LSR mass
estimated to be 1.5 kg/m² the LSR was shown to be quite compatible with FPS based space power systems, but not well matched with heat rejection temperature profiles of CBC power systems. However, general conclusions from the study confirmed the applicability of LSR to space power systems with near constant heat rejection temperatures, including Stirling, Rankine, Thermoelectric, and Thermionic power systems.

This paper presents the latest results for the scaling (L/W = sheet length/sheet width) and the geometry of the edge cylinders. Also, since emissivity and evaporative mass loss are the two most critical properties of a sheet radiator, results of an emissivity calculation and sheet lifetime results based on experimental evaporative loss rates for two possible oils that can be used in the LSR are presented. Finally, mention of LSR research currently in progress and important research yet to be done will be made.

Scaling Results

The surface tension force, dF, at the two edges of the sheet push the edges toward the z axis (Fig. 1). This force is proportional to the surface tension, σ, and inversely proportional to the radius of curvature R_c. As the flow moves in the z direction the edge cross-sectional area, A_z, grows. In order to satisfy mass continuity the edges approach each other and finally meet at the point z = L.
If the surface tension force per unit length, \( \frac{dF}{dz} \), is equated to the rate of momentum change per unit length, \( \rho u_e^2 \), where \( \rho \) is the density, \( \tau \) is the sheet thickness, and \( u_e \) is the edge velocity, then relations for \( u_e \) and \( L/W \) can be obtained [7].

\[
\begin{align*}
  u_e &= \left( \frac{2\sigma}{\rho \tau} \right)^{1/2} \\
  \frac{L}{W} &= \left( \frac{We}{8} \right)^{1/2}
\end{align*}
\]

(1)

For the case where there is no force (gravity for example) acting in the \( z \) direction the sheet thickness \( \tau \), is a constant. As a result the edge velocity, \( u_e \), will be constant [7] and:

\[
\frac{L}{W} = \left( \frac{We}{8} \right)^{1/2}
\]

(2)

Where the Weber number, \( We \), is defined as:

\[
We = \frac{\rho \tau w_o^2}{\sigma}
\]

(3)

where \( w_o \) is the velocity in the \( z \) direction. As can be seen from Eqs. (2) and (3), \( L/W \) is a linear function of velocity, \( w_o \).

A large amount of \( L/W \) data for D.C. 705 oil has been obtained in a vacuum facility [7] which can accommodate sheet flows with \( W \leq 25 \text{ cm} \) and \( L \leq 3.5 \text{ m} \). These results are shown in Fig. 4. Note the good agreement between the theoretical result (Eq. (2)) and the experimental data. For a practical radiator \( L/W = 10 \) so that \( We \approx 1000 \). The temperature dependence of \( \rho \) and \( \sigma \) for Dow-Corning 705 is given by [9]:

\[
\rho = 1569 - 1.625 \; T \; \text{kg/m}^3 \; \; \; T = \text{K}
\]

(4)

\[
\sigma = \left( 86.14 - \frac{T}{6.5} \right) \times 10^{-3} \; \text{n/m} \; \; \; T = \text{K}
\]

(5)

All the data in Fig. 4 was taken with \( T = 371 \text{ K} \). For D.C. 705 oil \( 0.025 < \sigma < 0.040 \; \text{n/m} \) for \( 400 > T > 300 \text{ K} \), which is the temperature range where the silicone oils have sufficiently low vapor pressure. For higher temperature operation liquid metals [1] are the only fluids with low enough vapor pressure to have minimal evaporative losses for space applications. The surface tension [1], \( \sigma \), of liquid metals is at least an order of magnitude larger (0.3 to 0.9 n/m) than that for silicone oils. Whereas, the densities of the liquid metals of interest range from one-half (lithium) the density of D.C. 705 to 12 times D.C. 705 density for mercury. Therefore, for a given sheet thickness, \( \tau \), the low density metals such as lithium and aluminum require a significantly higher velocity than a silicone oil to obtain the same Weber number. For a silicone oil \( w_o \approx 10 \text{ m/sec} \) yields \( We \approx 1000 \) for \( \tau = 200 \mu\text{m} \). However, for a low mass liquid metal such as lithium \( w_o \approx 60 \text{ m/sec} \) for \( We = 1000 \) and \( \tau = 200 \mu\text{m} \). The other liquid metals will require velocities of 10 to 60 m/sec to obtain \( We = 1000 \) for
\( \tau = 200 \, \mu m \). The higher velocities required by the liquid metals coupled with their higher densities translates to significantly larger pump power than that required for the silicone oils.

Sheet Stability and Edge Cylinder Geometry

Another critical fluid mechanical problem is sheet stability. Linear stability theory for an infinite sheet \([11]\) predicts no instability (i.e., no solutions that grow in time). However, if the sheet is not planar everywhere, such as occurs at the sheet edge cylinders, then linear theory does predict growing solutions in the nonplanar regions. These results were obtained in a study that has not yet been completed and hence will be reported elsewhere. However, some highlights and general observations are discussed below.

Holes have been observed to form where the edge cylinder joins the sheet but are quickly swept downstream before they have a chance to grow significantly. However, as \( \tau \) decreases the hole growth rate will increase. It is expected that there will be a limit on \( W/\tau \) to insure that a hole will not form and then grow fast enough to eliminate the sheet. Experimentally this \( W/\tau \) limit has not been reached. However, an experiment is being set up to determine it.

Since instability is expected to occur in the edge cylinder region, a study of the edge cylinder geometry was made. In Fig. 5 a representation of the edge cylinder geometry at four \( z \) (flow direction) locations is shown. Experimentally it has been found that the edge cylinder geometry oscillates in the \( z \) direction between nearly a circle to a highly elliptical shape then a "peanut" like shape and finally back to nearly a circle as shown in Fig. 5.

<table>
<thead>
<tr>
<th>Slit width, ( W ) (cm)</th>
<th>Sheet length/slit width, ( L/W )</th>
</tr>
</thead>
<tbody>
<tr>
<td>0.125</td>
<td>0.00</td>
</tr>
<tr>
<td>0.1875</td>
<td>0.00</td>
</tr>
<tr>
<td>0.235</td>
<td>0.00</td>
</tr>
<tr>
<td>0.250</td>
<td>0.00</td>
</tr>
</tbody>
</table>

**Figure 4.** Comparison of theoretical and experimental sheet scaling.

\[ \sqrt{\text{We/8}} \]
Figure 5.—Schematic of edge cylinder variation in flow direction.

Figure 6.—Comparison of experimental and theoretical edge cross section dimensions.
The theoretical analysis predicts a nearly circular geometry for the edge cylinder. No highly elliptical or peanut like solutions were found. In Fig. 6 a comparison between the experimental and theoretical edge cylinder geometry results is made. Experimental results for three sheet thicknesses, \( \tau = 50 \), 80, and 100 \( \mu m \) are shown. The dimensionless width of the edge cylinder, \( \bar{r} = 2r/\tau \), and dimensionless maximum height of the edge cylinder, \( \eta_{\text{MAX}} = 2s/\tau \), are plotted as a function of the dimensionless edge cylinder cross sectional area, \( \bar{A}_c = 2A_c/\tau^2 = Wz/\tau L \) (from mass continuity and the fact that the sheet is triangular it can be shown that the edge cylinder area is a linear function of \( z \)). The results for the \( \tau = 100 \mu m \) sheet agree well with the model shown in Fig. 5. For small \( \bar{A}_c \) the experimental \( r \) and \( \eta_{\text{MAX}} \) values are close to the nearly circular theoretical results. (For a perfect circle \( r = 2 \eta_{\text{MAX}} \)). However, as \( \bar{A}_c \) increases, \( r \) increases while \( \eta_{\text{MAX}} \) decreases below the theoretical result, indicating the highly elliptical shape is being formed. Then at \( \bar{A}_c \approx 75 \), \( \bar{r} \) starts to decrease toward the theoretical result as \( \eta_{\text{MAX}} \) increases toward its theoretical result, indicating that a nearly circular shape is again being formed. Then, at \( \bar{A}_c \approx 100 \) the cycle begins again. Only from photographic results is it known that the peanut like shape occurs. For the \( \tau = 50 \) and 80 \( \mu m \) cases both \( \bar{r} \) and \( \eta_{\text{MAX}} \) remain above the theoretical result for all \( \bar{A}_c \). For \( \tau = 80 \mu m \) a single oscillation from nearly circular geometry to elliptical shape and then back to a circular shape can be seen. Whereas for \( \tau = 50 \mu m \) two such oscillations are seen.

All the data in Fig. 6 indicate an elliptical geometry with \( \bar{r} > 2 \eta_{\text{MAX}} \). The more flattened the cross section (\( \bar{r} \gg 2 \eta_{\text{MAX}} \)), the smaller the curvature (1/\( R_c \)) will be at the point where the edge joins the sheet. The instability growth rate is proportional to the curvature. Therefore, the flattened edge cross section regions are less likely than the more circular regions to result in hole formation.

Properties of Possible Silicone Oils for the LSR

Low vapor pressure is a necessity for the working fluid of an external flow radiator. However, for an efficient radiator the working fluid emissivity must also be large. Fortuitously, for the temperature range of interest (300 to 400 K) we find that the silicone oils, which are transparent to visible radiation, do have sufficiently high emissivity for space radiator applications. This emissivity results from a high absorption coefficient in the wavelength region (8 < \( \lambda \) < 15 \( \mu m \)) where most of the radiation occurs for temperatures of 300 to 400 K. In other words, the silicone oils behave like a black body in the 8 < \( \lambda \) < 15 \( \mu m \) region, as shown in Table 1.

Previously [7] the emissivity of Dow-Corning 705 oil (D.C. 705) was calculated based on measured transmission data. These results are shown in Fig. 7. However, the evaporation rate for 705 oil is higher than desired. Several new organosiloxane oils [10] have been developed that have much lower evaporation rates. The oil with the lowest evaporation rate is designated Me2 in Ref. 10. To evaluate the effect of the evaporation rate on the mass of a sheet radiator system, consider the lifetime, \( t_s \), of the sheet mass, \( M_s \).

\[
M_s = \rho A_{\text{RAD}} = \bar{m}_s \bar{t}_s \bar{A}_{\text{RAD}}
\]
TABLE 1.—ABSORPTION COEFFICIENT FOR DOW CORNING Me₂ OIL

<table>
<thead>
<tr>
<th>Wavelength range, μm</th>
<th>Absorption coefficient, a, μm⁻¹</th>
</tr>
</thead>
<tbody>
<tr>
<td>0 to 2.5</td>
<td>0</td>
</tr>
<tr>
<td>2.5 to 7.0</td>
<td>8.0×10⁻⁴</td>
</tr>
<tr>
<td>7.0 to 7.7</td>
<td>6.4×10⁻³</td>
</tr>
<tr>
<td>7.7 to 8.0</td>
<td>1.75×10⁻²</td>
</tr>
<tr>
<td>8.0 to 8.7</td>
<td>1.10×10⁻²</td>
</tr>
<tr>
<td>8.7 to 10.5</td>
<td>1.75×10⁻²</td>
</tr>
<tr>
<td>10.5 to 11.1</td>
<td>1.10×10⁻²</td>
</tr>
<tr>
<td>11.1 to 15.4</td>
<td>1.75×10⁻²</td>
</tr>
<tr>
<td>15.4 to 20.0</td>
<td>6.4×10⁻³</td>
</tr>
<tr>
<td>20.0 to 23.5</td>
<td>5.7×10⁻³</td>
</tr>
<tr>
<td>23.5 to 40</td>
<td>1.07×10⁻²</td>
</tr>
<tr>
<td>40 to 100</td>
<td>1.25×10⁻³</td>
</tr>
<tr>
<td>100 to ∞</td>
<td>0</td>
</tr>
</tbody>
</table>

Figure 7.—Calculated emissivity of Dow Corning silicone oils for temperatures of 300 and 400 K.
Therefore,

$$t_v = \frac{\rho r}{m_v}$$  \hspace{1cm} (7)

where $m_v$ is the evaporation rate in kg/m$^2$ sec and $A_{RAD}$ is the total radiating area. If $t_L$ is the desired lifetime of the sheet radiator then the required extra fluid mass, $M_{ST}$, that must be available to make up for evaporation loss is the following.

$$M_{ST} = M_s \left(\frac{t_L}{t_v}\right)$$ \hspace{1cm} (8)

Using the experimental results for D.C. 705 and Me$_2$ [9,10], $t_v$ was calculated as a function of temperature, $T$. For D.C. 705 the mass loss rate, $m_v$, was calculated using the experimental vapor pressure which was curve fit with the following expression [9].

$$\log_{10} \rho_v = 12.31 - \frac{6490}{T} \hspace{1cm} T = K, \rho_v = Torr$$ \hspace{1cm} (9)

Assuming the evaporation rate is given by Knudsen effusion, then

$$\dot{m}_v = \frac{1}{4} \rho \left(\frac{8kT}{\pi m}\right)^{\frac{1}{2}} = \rho \left(\frac{m}{2\pi kT}\right)^{\frac{1}{2}}$$ \hspace{1cm} (10)

where $m$ is the mass of an oil molecule (atomic weight of D.C. 705 = 546). Equations (4) and (10) were used to calculate $t_v$ for D.C. 705. However, experimental results [10] for $m_v$ that are curve fit with the following expression were used for Me$_2$.

$$\log_{10} \dot{m}_v = 13.82 - \frac{10197}{T} \hspace{1cm} T = K, \dot{m}_v = Kg/m^2 sec$$ \hspace{1cm} (11)

Also, experimental results [10] for $\rho$ are curve fit with the following result

$$\rho = 1221 - 0.8878 T \hspace{1cm} Kg/m^3$$ \hspace{1cm} (12)

and are used to calculate $t_v$ for Me$_2$. It should be noted that $\dot{m}_v$ calculated using Eq. (10) for Dow-Corning 704 oil in Ref. 10 is an order of magnitude greater than the experimental values for $m_v$. If this same result holds true for D.C. 705 then the calculated values of $\dot{m}_v$ using Eq. (10) may be an overestimate. As a result, the calculated lifetimes, $t_v$, for D.C. 705 may be greatly underestimated.

Results of the $t_v$ calculations are shown in Fig. 8 for $\tau = 100, 200,$ and $300$ $\mu$m. For Me$_2$ the evaporative loss is so low that $t_v > 10$ yr for $T < 440$ K. Thus, the required extra fluid, $M_{ST} < M_s$ for $t_L < 10$ yr for $T \approx 440K$. For $T \leq 400$ K, $M_{ST} < 0.01 M_s$ for $t_L = 10$ yr. In this case ($T < 400$ K) negligible extra fluid mass is required. For D.C. 705 oil the evaporation rate is much higher. As a result, for $t_L = 10$ yr the temperature, $T < 300$ in order for $M_{ST} < 0.1M_s$. 

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From these results we would conclude that Me2 will make a better working fluid than D.C. 705. However, the emissivity must also be considered.

To calculate the emissivity of Me2, the experimental spectral transmission data [10] for 100 and 200 μm films was used. This calculation is similar to the one for D.C. 705 [7]. The experimental spectral transmission data is divided into wavelength bands of constant transmittance. From the experimental transmittance the absorption coefficient for each of the wavelength bands is calculated using the spectral transmittance relation for an infinite sheet [6,7,12].

\[
T_\lambda = 2E_3(a_\lambda \tau)
\]

where \(a_\lambda\) is the absorption coefficient and \(E_3(x)\) is the exponential integral.

\[
E_3(x) = \int_0^x u e^{-u} \, du
\]

Knowing \(a_\lambda\) the emissivity, \(\varepsilon\), can then be calculated [12].

\[
\varepsilon = \int_0^{\infty} \varepsilon_c \varepsilon_{\lambda b} \frac{d\lambda}{\sigma_{SB} T^4}
\]

where \(\sigma_{SB}\) is the Stefan-Boltzmann constant \((5.67 \times 10^{-8} \text{ W/m}^2 \text{ K}^4)\) and \(\varepsilon_{\lambda b}\) is the black body hemispherical spectral emissive power [12] and the spectral emittance is the following [12].

\[
\varepsilon_\lambda = 1 - T_\lambda = 1 - 2E_3(a_\lambda \tau)
\]
For the temperature range of interest (300 to 400 K), \( e_b \rightarrow 0 \) for \( \lambda \leq 4 \mu m \) and \( \lambda \geq 70 \mu m \). Therefore, to calculate \( e \), it is necessary to know \( a_\lambda \) in the spectral region \( 4 \leq \lambda \leq 70 \mu m \). The experimental transmission data of Ref. 10 was split into 13 wavelength bands and the absorption coefficient for each of these bands was determined as described above. These results are shown in Table 1. Using this data the integral in Eq. (11) is split into 13 wavelength bands with \( e_\lambda \) constant within each band. The emissivity can then be calculated using the tabulated values of

\[
F_{\lambda,T,A,T} = \frac{1}{\sigma_{SB} T^4} \int_{\lambda,T}^{\lambda,T} e_\lambda d\lambda
\]

from Ref. 12. The results of this calculation for Me\(_2\) are compared to the \( e \) results for D.C. 705 in Fig. 7. As can be seen, D.C. 705 has a higher emissivity than Me\(_2\). However, even for Me\(_2\), \( e > 0.75 \) for \( \tau > 200 \mu m \). Thus, the high absorption coefficient in the wavelength region \( 8 < \lambda < 15 \mu m \) (Table 1) results in acceptable emissivity even though the silicone oils are transparent in the visible wavelength region. For temperatures close to 300 K where evaporation loss for 705 is small, the larger values of \( e \) make D.C. 705 more attractive as a working fluid than Me\(_2\). However, for \( T = 400 \) K the evaporation loss for D.C. 705 is too large and Me\(_2\) is the more desirable working fluid.

**RESEARCH IN PROGRESS AND RESEARCH TO BE DONE**

Currently research is concentrated in two areas. First, the stability limit of the sheet flow is being experimentally determined. As discussed earlier, there is a limit on \( W/\tau \) to insure that holes will not form and destroy the sheet. A stability analysis is also being carried out to compare sheet stability predictions with the experimentally measured \( W/\tau \) limit. The main component of the experimental apparatus is a variable slit with limits of \( 10 \mu m < \tau < 100 \mu m \).

The second area being experimentally investigated is the sheet emissivity. Using the facility described in Ref. 7 the emissivity of D.C. 705 oil will be measured, pending program funding. The emissivity will be determined by measuring the enthalpy, i.e., temperature change of the fluid between the slit and the coalescence point.

Collection of the sheet flow at the coalescence point is the remaining area for research. However, a large amount of collector work [13-15] for the liquid droplet radiator (LDR) may be applicable to the LSR. It may be possible to recover some of the kinetic energy of the sheet flow with a collector that is designed like a subsonic diffuser of a wind tunnel. The collector is the remaining undefined component for an LSR system. Before a prototype LSR can be built, the collector problem must be solved.

**CONCLUSION**

The fluid mechanics of liquid sheet flows has been extensively researched. Scaling of the flow has been found to satisfy the theoretical result \( L/W = [We/8]^{1/2} \). Stability of the flow is currently being investigated. The limit on \( W/\tau \) is being experimentally determined.
Emissivity, $\varepsilon$, and sheet lifetime, $t_\nu$, resulting from evaporation loss have been calculated for two possible LSR working fluids. In the case of D.C. 705 silicone oil, its larger emissivity and acceptable lifetime at $T \approx 300$ K make it attractive for use at the lower temperatures. However, at $T \approx 400$ K the lifetime for D.C. 705 is short ($< 1$ yr), so that Dow-Corning Me$_2$, which has $t_\nu > 10^3$ yr at 400 K, becomes the more desirable fluid.

Currently an experimental measurement of the sheet emissivity is being planned. The remaining research problem that has not been studied is the collection of the sheet flow.

NOMENCLATURE

- $A_c$: Cross-sectional area of edge cylinder, $m^2$
- $A_{RAD}$: Total radiating area of sheet = WL, $m^2$
- $a\lambda$: Spectral absorption coefficient, $m^{-1}$
- $E_\lambda(x)$: Exponential integral defined by Eq. (14)
- $e_b$: Black body hemispherical spectral emissive power, $W/m^2 \mu m$
- $k$: Boltzmann constant, $1.38 \times 10^{-23}$ J/k
- $L$: Length of sheet in flow direction, m
- $M_s$: Mass of sheet fluid, kg
- $M_{ST}$: Required extra fluid mass to make up for evaporation loss, kg
- $m$: Mass of oil molecule of sheet fluid, kg
- $m_e$: Evaporation rate for sheet fluid, $kg/m^2 \sec$
- $p_e$: Vapor pressure of sheet fluid, $n/m^2$
- $R_c$: Radius of curvature, $m^{-1}$
- $r$: Width of edge cylinder in $x$ direction, m
- $s$: Height of edge cylinder in $y$ direction, m
- $T$: Temperature of sheet fluid, K
- $T\lambda$: Spectral transmission coefficient of sheet fluid
- $t_\nu$: Lifetime of sheet fluid, yr
- $t_{L}$: Desired lifetime of sheet radiator system, yr
- $u_e$: Velocity of sheet edge in $x$ direction, $m/\sec$
- $W$: Width of sheet, m
- $We$: Weber number for sheet flow = $\rho \tau w_o^2$
- $w_o$: Sheet flow velocity in $z$ direction
- $x$: Coordinate in plane of sheet and perpendicular to flow direction ($z$)
- $y$: Coordinate perpendicular to plane of sheet and perpendicular to flow direction ($z$)
- $z$: Coordinate in plane of sheet and in flow direction
- $\varepsilon$: Sheet emissivity
- $\varepsilon_\lambda$: Spectral emittance
- $\eta$: Dimensionless sheet edge cylinder height = $2s/r$
- $\lambda$: Wavelength, m
- $\rho$: Density of sheet fluid, $kg/m^3$
- $\sigma$: Surface tension of sheet fluid, $n/m$
- $\sigma_{SB}$: Stefan-Boltzmann constant, $5.67 \times 10^{-8}$, $W/m^2 K^4$
- $\tau$: Thickness of sheet, m
REFERENCES


Initial research on the external flow, low mass liquid sheet radiator (LSR), has been concentrated on understanding its fluid mechanics. The surface tension forces acting at the edges of the sheet produce a triangular planform for the radiating surface of width, W, and length, L. It has been experimentally verified that \( L/W = \left( \frac{W_e}{8} \right)^{1/2} \), where \( W_e \) is the Weber number. Instability can cause holes to form in regions of large curvature such as where the edge cylinders join the sheet of thickness, \( \tau \). The \( W_e/\tau \) limit that will cause hole formation with subsequent destruction of the sheet has yet to be reached experimentally. Although experimental measurements of sheet emissivity have not yet been performed because of limited program scope, calculations of the emissivity and sheet lifetime as determined by evaporation losses were made for two silicon based oils; Dow Corning 705 and Me 2. Emissivities greater than 0.75 are calculated for \( \tau \geq 200 \mu m \) for both oils. Lifetimes for Me 2 are much longer than lifetimes for 705. Therefore, Me 2 is the more attractive working fluid for higher temperatures (T \( \geq 400 \) K).