A METHOD FOR DETERMINING THE RATE OF HEAT TRANSFER FROM A WING OR STREAMLINE BODY

By CHARLES W. FRICK, Jr., and GEORGE B. McCULLOUGH

1945
# Aeronautic Symbols

## 1. Fundamental and Derived Units

<table>
<thead>
<tr>
<th>Metric</th>
<th>English</th>
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</thead>
<tbody>
<tr>
<td><strong>Symbol</strong></td>
<td><strong>Unit</strong></td>
</tr>
<tr>
<td>Length</td>
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<tr>
<td>Time</td>
<td>( t )</td>
</tr>
<tr>
<td>Force</td>
<td>( F )</td>
</tr>
<tr>
<td>Power</td>
<td>( P )</td>
</tr>
<tr>
<td>Speed</td>
<td>( V )</td>
</tr>
<tr>
<td></td>
<td></td>
</tr>
</tbody>
</table>

## 2. General Symbols

- **W** Weight = \( mg \)
- **g** Standard acceleration of gravity = \( 9.80665 \, \text{m/s}^2 \) or \( 32.174 \, \text{ft/sec}^2 \)
- **m** Mass = \( \frac{W}{g} \)
- **I** Moment of inertia = \( ml^2 \) (Indicate axis of radius of gyration \( k \) by proper subscript.)
- **\( \mu \)** Coefficient of viscosity

## 3. Aerodynamic Symbols

- **\( S \)** Area
- **\( S_w \)** Area of wing
- **\( G \)** Gap
- **\( b \)** Span
- **\( c \)** Chord
- **A** Aspect ratio = \( \frac{b^2}{S} \)
- **\( V \)** True air speed
- **\( q \)** Dynamic pressure = \( \frac{1}{2} \rho V^2 \)
- **\( L \)** Lift, absolute coefficient = \( \frac{L}{qS} \)
- **\( D \)** Drag, absolute coefficient = \( \frac{D}{qS} \)
- **\( D_p \)** Profile drag, absolute coefficient = \( \frac{D_p}{qS} \)
- **\( D_i \)** Induced drag, absolute coefficient = \( \frac{D_i}{qS} \)
- **\( D_r \)** Parasite drag, absolute coefficient = \( \frac{D_r}{qS} \)
- **\( C \)** Cross-wind force, absolute coefficient = \( \frac{C}{qS} \)

### Angles:

- **\( \alpha \)** Angle of attack
- **\( \epsilon \)** Angle of downwash
- **\( \omega \)** Angle of attack, infinite aspect ratio
- **\( \alpha_i \)** Angle of attack, induced
- **\( \alpha_s \)** Angle of attack, absolute (measured from zero-lift position)
- **\( \gamma \)** Flight-path angle
REPORT No. 830

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Moffett Field, Calif.
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Headquarters, 1500 New Hampshire Avenue NW., Washington 25, D. C.

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A METHOD FOR DETERMINING THE RATE OF HEAT TRANSFER
FROM A WING OR STREAMLINE BODY

By Charles W. Frick, Jr., and George B. McCullough

SUMMARY

A method for calculating the rate of heat transfer from the surface of an airfoil or streamline body is presented. A comparison with the results of an experimental investigation indicates that the accuracy of the method is good.

This method may be used to calculate the heat supply necessary for heat de-icing or in ascertaining the heat loss from the fuselage of an aircraft operating at great altitudes.

To illustrate the method, the total rate of heat transfer from an airfoil is calculated and compared with the experimental result.

INTRODUCTION

The calculation of the rate of heat transfer from the surface of bodies of aerodynamic shape is a problem for which no explicit solution is known to exist, although considerable attention has been given to the heat transfer from a heated flat plate into both laminar and turbulent flow regimes. It has been shown in reference 1 that the transfer of heat from the surface of a hot plate into an air stream flowing over the plate is primarily a boundary-layer problem. The extension of heat-transfer theory to permit the calculation of heat flow for an airfoil or streamline body is therefore a matter of calculating the boundary-layer characteristics which may be done by the methods of reference 2. The present report makes use of the results of references 1 and 2 to extend heat-transfer theory to wings and bodies for which pressure distributions may be calculated with accuracy. The derivation of the method is given in the appendix.

A limited experimental investigation of the method was made to determine the accuracy of the method in calculating the local rate of heat transfer into both the laminar and the turbulent boundary layer of an airfoil, and also to obtain a check on the computed total rate of heat transfer for the wing.

It is hoped that this method will facilitate a more accurate determination of the heat losses from wings in designing heat de-icing systems as well as from fuselages in the design of cabin-heating systems for aircraft operating at great altitudes.

SYMBOLS

The symbols used throughout this report and in the appendix are defined as follows:

- \( h \) heat-transfer coefficient, Btu/sq ft, \( ^\circ F \), sec
- \( k \) heat conductivity
- \( L \) length of streamline body
- \( M_t \) local Mach number, ratio of velocity just outside the boundary layer to local velocity of sound
- \( M_s \) free-stream Mach number, ratio of velocity of free stream to the velocity of sound in the free stream
- \( q_z \) local rate of heat transfer, Btu/sq ft, sec
- \( R_e \) Reynolds number based on wing chord \((Vc)/\nu\)
- \( R_e' \) Reynolds number based on body length \((VL)/\nu\)
- \( r \) radius to surface of streamline body at any point along the axis
- \( r_1 \) radius to surface of streamline body at point for which boundary layer is being computed
- \( s \) distance along the surface from the stagnation point
- \( \theta \) local temperature inside boundary layer, \( ^\circ F \), absolute
- \( \theta_o \) local temperature outside boundary layer, \( ^\circ F \)
- \( \theta_1 \) free-stream air temperature, \( ^\circ F \), absolute
- \( \theta_t \) local temperature inside boundary layer, \( ^\circ F \)
- \( \theta_L \) local temperature outside the boundary layer, \( ^\circ F \)
- \( \theta_f \) local temperature inside boundary layer at point for which boundary layer is being computed
- \( \delta \) local velocity just outside the boundary layer
- \( \delta_o \) local velocity just outside the boundary layer at point for which boundary layer is being computed
- \( \nu \) free-stream velocity
- \( v \) distance along the chord from the leading edge for an airfoil, or along the axis for a streamline body
- \( y \) distance normal to surface
- \( \alpha \) angle of attack, degrees
- \( \beta \) eddy heat conductivity
- \( \gamma \) ratio of specific heats
- \( \delta_L \) heat-transfer characteristic length for a laminar boundary layer
- \( \delta_T \) heat-transfer characteristic length for a turbulent boundary layer
- \( \epsilon \) eddy viscosity
- \( \eta \) turbulent boundary-layer parameter \((\eta = \sqrt{\nu U^2/\delta})\)
- \( \theta \) momentum thickness of boundary layer

\[
\theta = \int_0^\infty \frac{V - U}{U} \, \theta \, dy
\]
μ  absolute viscosity
ν  kinematic viscosity
ρ  air density
σ  Prandtl number \( \frac{c_p \mu}{k} \)
τ  surface shear

**APPARATUS**

Tests to determine the rate of heat transfer from a wing were made in the Ames 7- by 10-foot wind tunnel employing a heated, two-dimensional airfoil model.

**DESCRIPTION OF MODEL**

The model was a 7-foot chord NACA 65,2-016 airfoil which completely spanned the 7-foot dimension of the wind tunnel (fig. 1). Ordinates are given in table I.

![Figure 1: Heated airfoil model installed in the wind tunnel.](image)

<table>
<thead>
<tr>
<th>Percent Chord</th>
<th>x Inches</th>
<th>Percent Chord</th>
<th>y Inches</th>
</tr>
</thead>
<tbody>
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<td>0</td>
<td>0</td>
</tr>
<tr>
<td>.5</td>
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<td>1.423</td>
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<tr>
<td>1.50</td>
<td>1.059</td>
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</tr>
<tr>
<td>2.5</td>
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<td>2.057</td>
<td>.216</td>
</tr>
<tr>
<td>5.0</td>
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<td>3.543</td>
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</tr>
<tr>
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<td>4.316</td>
<td>.623</td>
</tr>
<tr>
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<td>4.954</td>
<td>.166</td>
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<tr>
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<td>5.958</td>
<td>.623</td>
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<td>7.010</td>
<td>.509</td>
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<tr>
<td>25</td>
<td>21.000</td>
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<tr>
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<tr>
<td>100</td>
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<td>12.696</td>
<td></td>
</tr>
</tbody>
</table>

Local unfairness of the model resulted in some minor variations in the pressure distribution, as shown in figure 3, but these were not of sufficient magnitude to induce transition to turbulence.

**METHOD OF HEATING**

The heated portion of the wing was divided into four compartments by spanwise bulkheads on which the heating elements, nine rows of ordinary 120-volt incandescent lamp bulbs, were mounted (fig. 2). The inside surface of the aluminum skin was painted a dull black to increase the absorption of radiant heat, but all other metal surfaces were bright.

The heat input appropriate to each compartment to give a temperature difference across the boundary layer of 100°F. at a Reynolds number of 13,000,000 was calculated by the method of this report. The size, number, and location of the bulbs within each compartment were such as to give the most nearly uniform skin temperature possible within the practical limitations of the design.

Power was supplied by a direct-current generator equipped with a remote voltage control which permitted a convenient means of adjusting the over-all applied voltage.

Free-stream air temperatures were calculated from average readings of three resistance-type thermometers located in the return passage a short distance ahead of the entrance cone. Adiabatic expansion through the entrance cone was assumed.
CONPUTATION OF HEAT TRANSFER

METHOD

The detailed analysis given in the appendix develops the following formulas, by which the local rate of heat transfer into both turbulent and laminar boundary layers may be computed. This method is applicable either to an airfoil or to a streamline body. The local rate for laminar flow is

\[ q_x = 0.700 \frac{k}{\delta_L} (t_v - t_a) \]  

(1a)

or the local heat-transfer coefficient is

\[ h_x = 0.700 \frac{k}{\delta_L} \]  

(1b)

and for the turbulent flow,

\[ q_x = 0.760 \frac{k}{\delta_T} (t_v - t_a) \]  

(2a)

or the local heat-transfer coefficient is

\[ h_x = 0.760 \frac{k}{\delta_T} \]  

(2b)

Heat transfer from an airfoil.—For the laminar boundary layer of an airfoil, \( \delta_L \) is computed as in reference 2 from the pressure distribution as follows:

\[ \delta_L = c \sqrt{\frac{5.3}{R_e} \left( \frac{V}{U} \right)^{1.17} \int_0^{r_e} \left( \frac{U}{V} \right)^{0.17} \frac{d}{c} \text{d} \xi} \]  

(3)

The turbulent boundary layer of an airfoil, \( \delta_T \) is computed as

\[ \delta_T = \frac{8.2 c}{R_e \left( \frac{U}{V} \right)} \]  

(4)

where \( \xi \) is the value of the turbulent boundary-layer parameter as determined by a step-by-step solution of the relationship of reference 3, given as

\[ \frac{d\xi}{dx} + \frac{6.13}{U} \frac{dU}{dx} = \frac{U}{v} f(\xi) \]  

(5)

The value of \( f(\xi) \) is given in table II as taken from reference 3, and may be plotted on semilogarithmic paper for ease in using.

<table>
<thead>
<tr>
<th>( \xi )</th>
<th>( 10^3 f(\xi) )</th>
<th>( \xi )</th>
<th>( 10^3 f(\xi) )</th>
</tr>
</thead>
<tbody>
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<td>14</td>
<td>221.6</td>
<td>17</td>
<td>146.1</td>
</tr>
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<td>19</td>
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<td>75.71</td>
<td>20</td>
<td>67.33</td>
</tr>
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<td>16.37</td>
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</tr>
<tr>
<td>25</td>
<td>14.41</td>
<td>28</td>
<td>9.69</td>
</tr>
</tbody>
</table>

**Figure 2**—Heated airfoil model showing heating lamps.

**Figure 3**—Chordwise pressure distribution. \( \alpha, 0^\circ; R_e, 11\times10^6. \)
Heat transfer from a streamline body.—For the laminar boundary layer of a streamline body, \( \delta_L \) is computed from reference 2 as

\[
\delta_L = L \sqrt{\frac{5.3}{R_e} \left( \frac{L}{r_1} \right) \left( \frac{V}{U} \right)^{1.17}} \int_0^{2h} \left( \frac{U}{r} \right) \left( \frac{V}{r} \right)^{1.17} d L
\]  

The turbulent boundary-layer heat-transfer length may be computed as

\[
\delta_T = \left( \frac{1.13}{r_1} \right) \frac{\delta}{R_e} \left( \frac{U}{V} \right)
\]

where \( \delta \) is determined as for an airfoil from the equation

\[
4.057 \left( \frac{U}{V} \right) (1 - 0.13 \frac{U}{V}) \left( \frac{U}{V} \right) \left( \frac{U}{L} \right)^{0.17} d L
\]

by the step-by-step process mentioned for calculating \( \delta_T \) for an airfoil.

Compressibility correction.—If the heat transferred is to be obtained at free-stream Mach numbers such that the aerodynamic temperature rise is an appreciable portion of the total temperature difference, a correction for aerodynamic heating should be made. The “heat-transfer temperature difference” to be used for a laminar boundary layer is

\[
(t_p - t_a) = (t_a - t_b) - 0.20 M_c T_b \left[ 1 - 0.13 \left( \frac{U}{V} \right) \right]
\]

and for turbulent flow

\[
(t_p - t_a) = (t_a - t_b) - 0.20 M_c^2 T_b
\]

where \( t_a - t_b \) is the desired temperature rise.

The total rate of heat transfer from an airfoil or streamline body may be found as follows:

1. Estimate the location of the transition point by the method of reference 4 for an increasing pressure gradient, or by reference 2 for a falling pressure gradient.

2. Calculations for the laminar region ahead of the transition point.
   (a) Compute the values of \( \delta_L \) along the surface to the transition point by equation (3) for an airfoil, or by equation (6) for a streamline body.
   (b) With these values and the desired temperature distribution corrected for compressibility, compute the local rates of heat transfer along the surface by equation (1a).

3. Calculations for the turbulent region behind the transition point.
   (a) From the value of \( \delta_L \) at the transition point compute \( \theta \), the momentum thickness as

\[
\theta = 0.280 \delta_L
\]

Using this value of \( \theta \), find the initial value of \( \zeta \) at the transition point as

\[
\zeta = 2.557 \log_{10} \left( \frac{U \theta}{r} \right)
\]

(b) With this initial value of \( \zeta \), calculate the values of \( \zeta \) along the surface by equation (5) for an airfoil, or by equation (8) for a streamline body. With these values of \( \zeta \), compute \( \delta_T \) along the surface by equation (4) for an airfoil, or by equation (7) for a streamline body.

(c) Using these values of \( \delta_T \) and the desired temperature difference across the boundary layer corrected for compressibility, compute the local rate of heat transfer along the surface by equation (2a).

4. Integrate these local rates of heat transfer along the chord for both laminar and turbulent regions to obtain the total rate of heat transfer.

HEAT-TRANSFER MEASUREMENTS

As mentioned in the Introduction, a limited number of heat-transfer tests were made on the heated wing model to check the accuracy of the theoretical method.

The experimental results are subject to several sources of error. All computed rates of heat transfer were based on the temperature distributions obtained at the center of the span, assuming that the spanwise variation was negligible. This was essentially true except for a small portion at each end of the wing. Precautions were taken to minimize the heat losses at the ends of the wing. These are not believed large since the design of the heating system allowed only slight transfer by convection, and the conduction of heat from the wing to its supports is negligible. Losses due to radiation from the wing have been computed as a maximum of 5 percent for the whole surface heated to 100°F, above the surroundings. This loss is not considered in the heat-transfer data.

For the purpose of computing heat transfer, the chordwise temperature distribution was computed and plotted as heat-transfer temperature difference \( t_p - t_a \); this is the observed temperature difference corrected for compressibility effect; that is, \( t_p \) is the temperature measured by a thermocouple in the skin minus the computed aerodynamic heating temperature rise. The value \( t_a \) is the free-stream air temperature (distinguished from the local temperature just outside the boundary layer of the wing, which will be higher or lower than \( t_a \) due to adiabatic variations caused by the velocity field of the wing).

RESULTS AND DISCUSSION

Heat-transfer tests of the wing were made in two parts, the first concerned with comparing computed and measured values of the local rate of transfer from the airfoil surface to laminar and turbulent boundary layers, and the second with checking the total rate of heat transfer from the airfoil.

The tests to measure the local rate of heat transfer were made at zero lift for two test Reynolds numbers, with free transition to obtain the heat-flow rate into a laminar boundary layer, and with transition fixed at 5-percent chord to determine the flow rate into a turbulent boundary layer. Figure 3 presents the pressure distribution over the wing at zero lift. The experimental procedure consisted in adjusting the heat input so that the skin temperatures were nearly constant along the chord. With this temperature distribution achieved, it was assumed that the second compartment of the wing, extending from 14.6-percent to 26.3-percent chord, was thermally isolated so that no flow of heat occurred in the skin or through the bulkheads. The
power input to this compartment was then measured by means of a voltmeter and an ammeter for comparison with the calculated rate of heat flow.

Figure 4 shows that the desired constant chordwise temperature distribution was attained for the laminar boundary layer, but the data of figure 5 for turbulent flow indicate that while the distribution was nearly constant from 10- to 30-percent chord, covering the region under consideration, the temperatures over the nose were excessively high. This came about through the heating difficulties resulting from the sudden change in heat-transfer coefficient at the point where transition was fixed. This type of distribution may have resulted in some change in the local values of the temperature gradient at the wing surface, though this effect should be small since no appreciable temperature gradient existed over the portion of the surface concerned, the boundaries of which are indicated by the dotted lines in the figures.

To obtain the computed values, the variation of the heat-transfer coefficient along the chord was calculated for each case as outlined under the section Method (results plotted in figs. 6 and 7). The heat input into the second compartment was then computed from the heat-transfer coefficient and experimentally measured temperature difference (corrected for compressibility heating effects). Both the measured and the computed values of heat input into the second compartment are listed in the following table:

<table>
<thead>
<tr>
<th>α (deg)</th>
<th>R_e x 10^4</th>
<th>Boundary layer</th>
<th>Calculated heat transfer (kw)</th>
<th>Measured input (kw)</th>
<th>Error (percent input)</th>
</tr>
</thead>
<tbody>
<tr>
<td>0</td>
<td>6.71</td>
<td>Laminar</td>
<td>0.861</td>
<td>0.875</td>
<td>1.6</td>
</tr>
<tr>
<td>0</td>
<td>10.72</td>
<td>Beam, do</td>
<td>0.948</td>
<td>0.928</td>
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</tr>
<tr>
<td>0</td>
<td>6. 96</td>
<td>Turbulent</td>
<td>3. 76</td>
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<td>.3</td>
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<td>Beam, do</td>
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<td>4. 01</td>
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</table>

The agreement is considered quite satisfactory, and is taken to indicate that the method for the computations of the heat transfer coefficient involves no serious errors despite the assumptions involved.

Further tests for the purpose of establishing the validity of the method as regards the total rate of heat flow from a wing were made at a lift coefficient of 0.55 and 8.60 million Reynolds number. In addition to a test with free transition,
a second condition simulating the formation of ice near the stagnation point by fixing transition at 5-percent chord on the lower surface was investigated. Heat input in both conditions was maintained at the maximum available from the apparatus, and no attempt was made to achieve a predetermined temperature rise or chordwise distribution. The chordwise temperature distribution obtained, corrected for the effects of compressibility heating, is plotted in figures 8 and 9.

The chordwise variation of heat-transfer coefficient was computed for both the transition-fixed and transition-free conditions, as outlined in Method. Tables III and IV present the computations for the transition-free condition and serve as an illustrative example. The pressure distribution used for these calculations is given in figure 10. The value of heat input was then computed by use of the experimental temperature distributions (corrected for com-

![Figure 8](image)

**Figure 8.**—Chordwise distribution of temperature difference, \((T_p - T_i)\). \(\alpha = 0^\circ\); transition free.

![Figure 9](image)

**Figure 9.**—Chordwise distribution of temperature difference, \((T_p - T_i)\). \(\alpha = 5^\circ\); transition fixed at 5 percent chord.

The experimental temperature distributions for the tests of the total rate of heat transfer show that the heat-transfer temperature difference varies to a marked degree along the chord (figs. 8 and 9). This variation violates one of the assumptions underlying the development of the method; that is, that the temperature difference is constant along the chord.

### TABLE III

**COMPUTATION OF HEAT-TRANSFER COEFFICIENT**

<table>
<thead>
<tr>
<th>Airfoil 65,2-016</th>
<th>(c_t=0.55)</th>
<th>(R_e=8,69 \times 10^5)</th>
<th>(M_t=0.183)</th>
</tr>
</thead>
<tbody>
<tr>
<td>Position</td>
<td>(\xi)</td>
<td>(\xi_i)</td>
<td>(\Delta T)</td>
</tr>
<tr>
<td>0.01</td>
<td>0.07</td>
<td>0.07</td>
<td>1.51</td>
</tr>
<tr>
<td>0.02</td>
<td>0.14</td>
<td>0.05</td>
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</tr>
<tr>
<td>0.03</td>
<td>0.21</td>
<td>0.07</td>
<td>1.54</td>
</tr>
<tr>
<td>0.04</td>
<td>0.28</td>
<td>0.06</td>
<td>1.52</td>
</tr>
<tr>
<td>0.05</td>
<td>0.35</td>
<td>0.14</td>
<td>1.50</td>
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<tr>
<td>0.06</td>
<td>0.42</td>
<td>0.14</td>
<td>1.48</td>
</tr>
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<td>0.07</td>
<td>0.49</td>
<td>0.14</td>
<td>1.46</td>
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<tr>
<td>0.08</td>
<td>0.56</td>
<td>0.15</td>
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<tr>
<td>0.09</td>
<td>0.63</td>
<td>0.15</td>
<td>1.39</td>
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<tr>
<td>0.1</td>
<td>0.67</td>
<td>0.15</td>
<td>1.36</td>
</tr>
<tr>
<td>0.2</td>
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<td>0.35</td>
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</tr>
<tr>
<td>0.3</td>
<td>1.01</td>
<td>0.35</td>
<td>1.20</td>
</tr>
<tr>
<td>0.4</td>
<td>1.21</td>
<td>0.35</td>
<td>1.13</td>
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<tr>
<td>0.5</td>
<td>1.31</td>
<td>0.35</td>
<td>1.01</td>
</tr>
</tbody>
</table>

### TABLE IV

**COMPUTATION OF HEAT-TRANSFER COEFFICIENT**

<table>
<thead>
<tr>
<th>Airfoil 65,2-016</th>
<th>(c_t=0.55)</th>
<th>(R_e=8,69 \times 10^5)</th>
<th>(M_t=0.183)</th>
</tr>
</thead>
<tbody>
<tr>
<td>Position</td>
<td>(\xi)</td>
<td>(\xi_i)</td>
<td>(\Delta T)</td>
</tr>
<tr>
<td>0.01</td>
<td>0.0</td>
<td>0.0</td>
<td>1.0</td>
</tr>
<tr>
<td>0.02</td>
<td>0.05</td>
<td>0.000100</td>
<td>32 \times 10^{-4}</td>
</tr>
<tr>
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<td>0.30</td>
<td>0.022</td>
<td>1 \times 10^{-3}</td>
</tr>
<tr>
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<td>0.021</td>
<td>1 \times 10^{-3}</td>
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<td>1 \times 10^{-3}</td>
</tr>
<tr>
<td>0.1</td>
<td>0.45</td>
<td>0.019</td>
<td>1 \times 10^{-3}</td>
</tr>
</tbody>
</table>

The experimental temperature distributions for the tests of the total rate of heat transfer show that the heat-transfer temperature difference varies to a marked degree along the chord (figs. 8 and 9). This variation violates one of the assumptions underlying the development of the method; that is, that the temperature difference is constant along the chord.
chord, which must be true if the transfer of heat at all points along the surface is analogous to the transfer of momentum. To what degree this assumption may be ignored has not been determined analytically, since the problem of considering the variation of temperature along the chord presents difficulties which have so far prevented a solution. The experimental results, however, indicate that the accuracy with which the total rate of heat transfer can be computed is not greatly impaired by the temperature variations experienced. Generalization of this result must await further experimental checks.

The accuracy with which the local rate of heat transfer may be computed in a rising pressure gradient is dependent upon the accuracy with which the surface shear may be determined. Squire and Young’s method (reference 3) assumes that the turbulent boundary layer in a rising pressure gradient exhibits the same characteristics as the fully developed turbulent layer of a flat plate. The extent to which the relationship between the surface shear, the momentum thickness, and the local velocity so derived remains valid is shown by the accuracy of the Squire and Young method in determining friction drag. It must be realized, however, that the method will fail if turbulent separation is imminent.

The thickening of the turbulent boundary layer due to the rise in pressure acting on the displaced mass of fluid also is ignored by the assumption that the heat-transfer rate is proportional to the surface shear computed by Squire and Young’s method. Actually, the heat capacity of the boundary layer is increased by this thickening which tends to increase the rate of heat flow at the surface. This counteracts the effect of the profile distortion, resulting from the same cause, which reduces the surface shear since it tends to cause separation. But this effect, too, is negligible for all cases where Squire and Young’s method may be applied.

In concluding, it must be stated that while the method presented herein is subject to a number of broad assumptions in its development, the experimental evidence presented shows the total rate of heat flow may be calculated with reasonable accuracy.
CONCLUSIONS

The accuracy of the method for determining the rate of heat transfer from an airfoil is shown to be good by the results of a limited experimental investigation. Since the correctness with which the heat transfer can be computed is dependent mainly on the accuracy with which the boundary-layer characteristics may be determined, it is expected that the method possesses the same accuracy for computing heat-transfer rates from a streamlined body.

Although the development of the heat-transfer formulas is based on the assumption that the skin temperature remains constant along the surface, the experimental results show that for moderate temperature variations the precision is still good.

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APPENDIX

DERIVATI ON OF THE METHOD

1. Heat transfer into a laminar boundary layer.—The theory of heat transfer into a laminar boundary layer was first investigated by E. Pohlhausen for the case of incompressible flow along a flat plate maintained at a constant temperature (reference 1). Pohlhausen’s solution is developed by solving the differential equation for the temperature boundary layer by using Blasius’ solution for the velocity boundary layer.

In order to arrive at a solution for an airfoil in an incompressible fluid, it is necessary

(1) to assume that the temperature boundary-layer and the velocity boundary-layer profiles for the airfoil are related in the same manner as for Pohlhausen’s solution. (This is true if the temperature of the skin remains constant along the surface and if the thinning of the friction layer in a favorable pressure gradient due to the change in pressure acting on the displaced fluid is negligible.)

(2) to calculate the value of \( \frac{du}{dy} \) for the velocity boundary layer and then determine \( \frac{dt}{dy} \) with the relationship resulting from (1). (The solution of the problem for the temperature of the skin varying along the chord has been prevented because the difficulties so far have been found insurmountable.)

Pohlhausen’s expression for the temperature gradient in the boundary layer at the surface of the plate is given as

\[
\left( \frac{dt}{dy} \right)_{y=0} = -\frac{1}{2} \alpha(\sigma) \sqrt{\frac{U_p}{\mu x}} (t_f-t_0)
\]

The function \( \alpha(\sigma) \) is the first derivative of Pohlhausen’s function defining the temperature boundary layer which, for \( \sigma=1 \), is equivalent to the second derivative of Blasius’ function for the velocity boundary layer. Pohlhausen found that \( \alpha(\sigma) \) is accurately given by the relationship

\[
\alpha(\sigma) = 0.664 \sqrt{\sigma}
\]

then

\[
\left( \frac{dt}{dy} \right)_{y=0} = -0.332 \sqrt{\sigma} \sqrt{\frac{U_p}{\mu x}} (t_f-t_0)
\]

Now, for the Blasius boundary-layer distribution

\[
\left( \frac{du}{dy} \right)_{y=0} = 0.332 \sqrt{\frac{U_p}{\mu x}} U
\]

so that

\[
\left( \frac{dt}{dy} \right)_{y=0} = -\left( \frac{du}{dy} \right)_{y=0} \sqrt{\sigma} \sqrt{\frac{U_p}{\mu x}} (t_f-t_0)
\]

It is now necessary to determine \( \frac{du}{dy} \) for the airfoil at any chordwise position. For the Blasius profile

\[
\left( \frac{du}{dy} \right)_{y=0} = \frac{0.765 U}{\delta_L}
\]

where \( \delta_L \) is the thickness of the boundary layer where \( u=U \).

Substituting in the preceding equation

\[
\left( \frac{dt}{dy} \right)_{y=0} = 0.765 \sqrt{\sigma} \sqrt{\frac{U_p}{\mu x}} (t_f-t_0)
\]

or, taking \( \sigma=0.760 \) for air, the local rate of heat transfer is

\[
q_x = k \left( \frac{dt}{dy} \right)_{y=0} = 0.700 \frac{k}{\delta_L} (t_f-t_0)
\]

or the heat-transfer coefficient is

\[
h_x = 0.700 \frac{k}{\delta_L}
\]

The development in reference 5 of an expression for the heat-transfer rate based on Reynolds analogy gives results which are in complete agreement with the above if \( \sigma=1 \). However, the experimental results of reference 6 indicate that the expression \( \sqrt{0.760} \), that is, \( \sqrt{\sigma} \), is not in agreement with the theory and temperature gradients in the laminar layer. The two methods give results within 10 percent of each other, which is sufficient for practical cases.

The values of \( \delta_L \) for laminar flow may be determined both for an airfoil and a streamline body by the method of reference 2.

2. Turbulent boundary layer.—The theory of heat transfer in eddyng flow as given by Dryden (reference 7) requires the introduction of several new concepts. If the equations of motion for turbulent flow are written by placing

\[ u = \bar{u} + u' \]
\[ v = \bar{v} + v' \]
\[ w = \bar{w} + w' \]

where the bars indicate mean values and the primes indicate fluctuations, and these values substituted into the equations of motion for steady flow, similarity between equations so developed and the steady-flow equations can be shown by introducing a value of eddy viscosity \( \epsilon \). Similarly, the concept of eddy heat conductivity, \( \beta \), is introduced by placing \( t = t + t' \), in the equations of the temperature field.
These values of eddy viscosity, $\epsilon$, and eddy conductivity, $\beta$, however, do not have the same properties as $\mu$ and $k$ since they vary from point to point in the flow. Nevertheless, $\epsilon$ and $\beta$ can be shown to vary in the same manner from point to point in the fluid. This is done by introducing Prandtl’s concept of a mixing length; that is, a length of path followed by a fluid particle before it becomes lost in the mass of eddying fluid.

It is therefore shown if the shear, $\tau' = -\rho u'v'$, then

$$\tau = \epsilon \frac{d\bar{u}}{dy} + \rho \beta \left( \frac{d\bar{u}}{dy} \left| d\bar{u} \right| \right)$$

or that

$$\epsilon = \rho \beta \frac{d\bar{u}}{dy}$$

in which the mixing length $l$ varies from point to point in the fluid. Now, if the eddy heat transfer is considered to be $-c_\rho \beta T'$, then the eddy heat conductivity is equal to $c_\rho \beta \left( \frac{d\bar{u}}{dy} \right)$ or equal to $c_\rho \beta$, provided the mixing length for heat transfer is considered to be the same as the mixing length for the transfer of shearing stress. Dryden states that available experimental data show that the mixing lengths near a wall are closely equivalent for transfer of heat and momentum, but that the relationship falls down, for instance, in the wake of a heated body. Since the present case concerns heat transfer from a wall to eddying flow in a boundary layer, it is believed that this relationship is acceptable.

For turbulent flow, it has been shown that the Prandtl number is equal to unity; that is,

$$\frac{c_{\mu\text{ turb}}}{k_{\text{ turb}}} = 1$$

If the Prandtl number is unity, then the thermal and dynamic boundary layers have the same profile (reference 6). If we make the same assumptions as in step (1) for the laminar boundary layer, we may write

$$\left( \frac{dt}{dy} \right)_{y=0} = - \left( \frac{d\bar{u}}{dy} \right) \frac{(t_p - t_0)}{U}$$

where $U$ is the velocity outside the friction layer. (This relationship is dependent on the assumption that the temperature along the surface remains constant as for step (1) for the laminar boundary layer, and that the thickening of the boundary layer due to the increasing pressures acting on the displaced mass of fluid and the distortion of the profile thus resulting is negligible.)

Now

$$q_x = -\beta \left( \frac{dt}{dy} \right)_{y=0}$$

but

$$\beta = c_\rho \beta$$

so that

$$q_x = -c_\rho \beta \left( \frac{dt}{dy} \right)_{y=0}$$

or

$$q_x = +c_\rho \beta \left( \frac{dt}{dy} \right)_{y=0} \frac{(t_p - t_0)}{U}$$

since the surface shear

$$\tau_0 = \epsilon \left( \frac{du}{dy} \right)_{y=0}$$

$$q_x = c_\rho \tau_0 \frac{(t_p - t_0)}{U}$$

This is the same formula developed by Reynolds for flow in pipes (reference 7).

So it is seen that the problem of calculating the rate of heat transfer in turbulent flow is primarily a problem of calculating the surface shear along the airfoil. This may be done by the method of reference 3, in which Squier and Young write the relationship

$$q_x = c_\rho \frac{\rho U^2}{\xi}$$

where

$$\xi = 2.557 \log \left( \frac{4.075 U}{\nu} \right)$$

$\theta$ being the momentum thickness of the boundary layer. (This relationship is developed from von Kármán’s formula for the skin friction experience by a flat plate with a fully developed turbulent boundary layer. This assumption becomes less and less true as the turbulent boundary-layer profile of an airfoil becomes changed in shape and approaches separation in a steep pressure recovery.) Substituting for $\tau_0$

$$q_x = \frac{c_\rho \rho U^2}{\xi} \frac{(t_p - t_0)}{U}$$

or

$$q_x = \frac{c_\rho \rho U^2}{\xi} \frac{k \mu V}{\xi^2} \frac{\mu V}{c} \frac{(t_p - t_0)}{U}$$

$$q_x = \frac{c_\rho \mu k V \xi^2 \xi}{c} \frac{(t_p - t_0)}{U}$$

where $\mu$ and $k$ are values for uneddyng flow. Substituting for $\frac{c\mu}{k}$ the value for air, 0.760,

$$q_x = 0.760 \frac{k}{c} \frac{R_e}{U V} \frac{(t_p - t_0)}{U}$$

or considering $\frac{q_x}{(t_p - t_0)} = \frac{V}{\delta_T}$, a characteristic length for the turbulent boundary layer,

then

$$q_x = 0.760 \frac{k}{\delta_T} \frac{(t_p - t_0)}{U}$$

and

$$h_x = -0.760 \frac{k}{\delta_T}$$

In calculating $\delta_T$, $\xi$ may be computed by the step-by-step solution of the equations of reference 3 for an airfoil or streamline body.
3. Compressibility effects on heat transfer.—Since the foregoing analysis has been made for incompressible flow, the effect of aerodynamic heating must be dealt with if the heat transfer is to be accurately obtained. The effect of compressibility may be considered, to a first approximation, simply as influencing the heat-transfer temperature difference to be used in the above-developed equations; that is, a part of any desired increase in the skin temperature will result from aerodynamic heating, and this part of the temperature increase involves no expenditure of heat.

The temperature field near the heated surface of an airfoil or body of revolution operating at high Mach numbers may be determined by superposing the heat-transfer temperature field on that due to the friction heating as in reference 8. Eckert (reference 9) has shown that the temperature field due to aerodynamic heating for \( \sigma = 1 \) may be expressed as

\[
t = t_L + \frac{\gamma - 1}{2} M^2_L T_L \left[ 1 - \left( \frac{u}{U} \right)^2 \right]
\]

or

\[
t = t_0 + \frac{\gamma - 1}{2} M^2_0 T_0 - \frac{\gamma - 1}{2} M^2_L T_L \left( \frac{u}{U} \right)^2
\]

Superposing this on the temperature field for heat transfer, which may be given as

\[
t = t_p - (t_p - t_0) \frac{u}{U}
\]

the combined temperature field is

\[
t = t_p - (t_p - t_0) \left( \frac{u}{U} \right) + \frac{\gamma - 1}{2} M^2_0 T_0 - \frac{\gamma - 1}{2} M^2_L T_L \left( \frac{u}{U} \right)^2
\]

It is evident that at \( y = 0 \)

\[
\left( \frac{dt}{dy} \right)_{y=0} = \frac{t_p - t_0}{U} \left( \frac{du}{dy} \right)_{y=0}
\]

which indicates that the heat transfer corresponds to the heat-transfer temperature field, so that for compressible flow the only correction necessary is that of correcting the skin temperature for the rise in temperature due to aerodynamic heating.

Eckert has shown that the temperature of the surface due to compressibility effects \( t_M \), is

\[
t_M = t_L + \sqrt{\frac{\gamma - 1}{2}} M^2_L T_L
\]

or

\[
t_M = t_0 + \frac{\gamma - 1}{2} M^2_0 T_0 - \frac{\gamma - 1}{2} M^2_L T_L + \sqrt{\frac{\gamma - 1}{2}} M^2_L T_L
\]

The heat-transfer temperature difference for the laminar region, \( \sigma = 0.760 \), is then

\[
(t_p - t_0) = (t_p - t_0) - 0.2 M^2_0 T_0 \left[ 1 - 0.13 \left( \frac{U}{V} \right)^2 \right]
\]

and for the turbulent region, \( \sigma = 1 \)

\[
(t_p - t_0) = (t_p - t_0) - 0.2 M^2_0 T_0
\]

REFERENCES

Positive directions of axes and angles (forces and moments) are shown by arrows.

<table>
<thead>
<tr>
<th>Axis</th>
<th>Symbol</th>
<th>Force (parallel to axis) symbol</th>
<th>Moment about axis</th>
<th>Angle</th>
<th>Velocities</th>
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</thead>
<tbody>
<tr>
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<td></td>
<td>Designation</td>
<td>Positive direction</td>
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<td>Linear (component along axis)</td>
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<td>Z</td>
<td>Yawing</td>
<td>N</td>
<td>Yaw</td>
<td>w</td>
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</table>

Absolute coefficients of moment

\[ C_i = \frac{L}{qbS} \quad C_n = \frac{M}{qcS} \quad C_s = \frac{N}{qbS} \]

(rolling) (pitching) (yawing)

Angle of set of control surface (relative to neutral position), \( \delta \). (Indicate surface by proper subscript.)

4. PROPELLER SYMBOLS

- **\( D \)**: Diameter
- **\( p \)**: Geometric pitch
- **\( p/D \)**: Pitch ratio
- **\( V' \)**: Inflow velocity
- **\( V_s \)**: Slipstream velocity
- **\( T \)**: Thrust, absolute coefficient \( C_T = \frac{T}{\rho n^3 D^4} \)
- **\( Q \)**: Torque, absolute coefficient \( C_Q = \frac{Q}{\rho n^2 D^5} \)

- **\( P \)**: Power, absolute coefficient \( C_P = \frac{P}{\rho n^3 D^5} \)
- **\( C_s \)**: Speed-power coefficient \( = \frac{\delta}{\rho V^2} \sqrt{\frac{P}{n^3}} \)
- **\( \eta \)**: Efficiency
- **\( n \)**: Revolutions per second, rps
- **\( \phi \)**: Effective helix angle \( = \tan^{-1}\left(\frac{V}{2\pi n\rho} \right) \)

5. NUMERICAL RELATIONS

- 1 hp = 76.04 kg·m/s = 550 ft·lb/sec
- 1 metric horsepower = 0.9863 hp
- 1 mph = 0.4470 mps
- 1 mps = 2.2369 mph
- 1 lb = 0.4536 kg
- 1 kg = 2.2046 lb
- 1 mi = 1,609.35 m = 5,280 ft
- 1 m = 3.2808 ft