Integrated High Payoff Rocket Propulsion Technology (IHPRPT) SiC Recession Model

E.J. Opila
Glenn Research Center, Cleveland, Ohio
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Integrated High Payoff Rocket Propulsion Technology (IHPRPT)
SiC Recession Model

E.J. Opila
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Glenn Research Center
Cleveland, Ohio 44135

1.0 Summary

SiC stability and recession rates were modeled in hydrogen/oxygen combustion environments for the Integrated High Payoff Rocket Propulsion Technology (IHPRPT) program. The IHPRPT program is a government and industry program to improve U.S. rocket propulsion systems. Within this program SiC-based ceramic matrix composites are being considered for transpiration cooled injector faceplates or rocket engine thrust chamber liners. Material testing under conditions representative of these environments was conducted at the NASA Glenn Research Center, Cell 22. For the study described herein, SiC degradation was modeled under these Cell 22 test conditions for comparison to actual test results: molar mixture ratio, MR (O₂:H₂) = 6, material temperatures to 1700 °C, combustion gas pressures between 0.34 and 2.10 atm, and gas velocities between 8,000 and 12,000 fps. Recession was calculated assuming rates were controlled by volatility of thermally grown silica limited by gas boundary layer transport. Assumptions for use of this model were explored, including the presence of silica on the SiC surface, laminar gas boundary layer limited volatility, and accuracy of thermochemical data for volatile Si-O-H species. Recession rates were calculated as a function of temperature. It was found that at 1700 °C, the highest temperature considered, the calculated recession rates were negligible, about 200 μm/h, relative to the expected lifetime of the material. Results compared favorably to testing observations. Other mechanisms contributing to SiC recession are briefly described including consumption of underlying carbon and pitting. A simple expression for liquid flow on the material surface was developed from a one-dimensional treatment of the Navier-Stokes Equation. This relationship is useful to determine under which conditions glassy coatings or thermally grown silica would flow on the material surface, removing protective layers by shear forces. The velocity of liquid flow was found to depend on the gas velocity, the viscosity of gas and liquid, as well as the thickness of the gas boundary layer and the liquid layer. Calculated flow rates of a borosilicate glass coating compared well to flow rates observed for this coating tested on a SiC panel in Cell 22.

2.0 SiC Recession Calculation Input Parameters and Data

2.1 Combustion Gas Chemistry

The combustion gas environment for a weight mixture ratio MR = 6 (H₂:O₂) was chosen because this environment is representative of SiC panel testing that was conducted in the Rocket Combustion Lab, Cell 22, at the NASA Glenn Research Center also as part of the IHPRPT program. A schematic drawing and image of the test configuration and test panel is shown in Figure 2.1. Carbon fiber reinforced panels of overall dimensions 4 by 6 in., and exposed dimensions of approximately 3.5 in.³ were tested. The mixture ratio was hydrogen rich so that excess hydrogen was present in the combustion gas mixture. The combustion products were calculated using CEA (Chemical Equilibrium and Analysis) (MCB96). Inputs to this calculation include the MR and the relevant pressure for the Cell 22 test panel, a combustion chamber pressure (Pc) of 160 psi. The combustion gas chemistry is relatively insensitive to pressure and highly dependent on MR. The calculated results are shown in Table 2.1. Detailed results are found in Appendix A. The important results of the calculation are twofold. First, the primary products in the combustion environment are 60 percent H₂O(g) and 25 percent H₂(g). The second result of interest is that...
Figure 2.1.—Schematic drawing of the Cell 22 test configuration and test panel (left). Image of a panel under test (right). Drawing and image courtesy of O. Sudre, Q. Yang, and D. Marshall, Teledyne Scientific (SUD06).

<table>
<thead>
<tr>
<th>Combustion product gas</th>
<th>Percent of total products</th>
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<tr>
<td>H₂O</td>
<td>60</td>
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<tr>
<td>H₂</td>
<td>25</td>
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<tr>
<td>OH</td>
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<tr>
<td>O</td>
<td>0.95</td>
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<td>O₂</td>
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TABLE 2.1.—CALCULATED COMBUSTION PRODUCTS FOR MR = 6.0, Pc = 160 psi
[Results calculated using CEA (MCB96).]

the theoretical adiabatic gas temperature is 3354 K assuming complete mixing. In actual Cell 22 engine conditions, fuel and oxidant mixing is not uniform so that portions of the flow that are more fuel rich would be cooler, and those portions of the flow closer to the stoichiometric condition, MR = 8, would be hotter.

2.2 SiC Material Temperature

Material recession rates were calculated assuming SiC surface temperatures were between 1200 and 1700 °C. A maximum material temperature of 1700 °C was chosen for the calculations so that the silica film could be assumed to be solid and effects of silica melting (melting temperature of silica = 1723 °C) could be neglected. Liquid silica films are discussed in Section 6.0. Recession at lower temperatures was calculated to determine at which temperature recession becomes important, and to look at the temperature trends for SiC recession. Actual material temperatures in the Cell 22 tests exceeded 1700 °C on some portions of the test panels, however, high uncertainty exists in the measured material temperatures. Actual material temperatures are expected to be significantly lower than the theoretical adiabatic gas temperature 3354 K due to radiation and conduction heat losses from the panel.

2.3 Combustion Gas Pressure and Velocity

Pratt & Whitney provided gas pressures and velocities over the length of the test panel for the case of MR = 6 and Pc = 160 psi (STO07a). These data are shown in Table 2.2 in two sets of units. Recession rates were calculated at the leading edge and trailing edge of the panel at those conditions highlighted in yellow. Leading edge pressures were higher and velocities lower. Trailing edge pressures were lower and gas velocities higher as the gas expanded over the panel. These conditions are expected to bound the recession rates observed for this panel.
### TABLE 2.2.—COMBUSTION GAS PRESSURES AND VELOCITIES AS A FUNCTION OF POSITION ALONG TEST PANEL IN DIRECTION OF FLOW

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<tr>
<th>X (in.)</th>
<th>Pinf (psia)</th>
<th>Vinf (ft/sec)</th>
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### 2.4 Thermochemical Data for Volatile Si-O-H Species

Volatility of SiO2 (silica) or SiC results from the formation of stable gas species such as SiO(g), Si(OH)4(g), SiO(OH)2(g), and SiO(OH)(g) which consumes the starting material. The stability of these vapor species in the combustion environment was calculated using a free energy minimization technique. This calculation involves inputting the reactants SiO2 or SiC and the combustion gas reactants: H2O, H2, OH, H, O, and O2 into free energy minimization software, FACTSAGE (BAL02). The free energy minimization takes this reactant assemblage, and using thermochemical data for these species, calculates the equilibrium product assemblage with the lowest free energy, i.e., the most stable product combination. In order to calculate the partial pressures of these volatile Si-O-H(g) products, thermochemical data for all these species must be available in the software database. Data for the Si-O-H(g) species are not generally included in thermochemical databases, so data from various sources was input into the FACTSAGE database. Data for the following vapor species was input from the cited references: SiO(g) already present in FACT53 database (BAL02), Si(OH)4(g) (JAC05), SiO(OH)2(g) (JAC05), and SiO(OH)(g) (ALL95). These data are discussed in more detail in Section 4.3. The preferred recession rates reported here make use of the Allendorf (ALL95) data for SiO(OH)(g). Alternative calculations using the Krikorian data for SiO(OH)(g) (KRI70) are presented and discussed in Section 4.3.1.4.
3.0 Recession Calculations

3.1 Calculation of Volatile Species Partial Pressures

As mentioned in Section 2.4, FACTSAGE was used to calculate the equilibrium pressures of volatile species of Si-containing vapor species in the combustion environment at the leading and trailing edge panel conditions at material surface temperatures between 1200 and 1700 °C. A sample calculation is shown in Appendix B. Silica is assumed to be present on the surface of the SiC in all cases. The validity of this assumption is considered in detail in Section 4.1. The volatile species partial pressure results are summarized in Tables 3.1 and 3.2. The calculated partial pressures of the predominant Si-containing vapor species are reported as a function of temperature at the panel leading and trailing edge conditions. Percentages of the volatile products are also included on the right hand side of the table. The species comprising greater than 2 percent of the total volatile pressure were included in the recession calculations. These percentages are highlighted in yellow in the table. The calculated partial pressures of the volatile species are plotted in Figures 3.1 and 3.2 for the trailing and leading edge conditions, respectively.

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<th>Si(OH)</th>
<th>SiO(OH)2</th>
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<th>Ptotal</th>
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<th>XSiO(OH), Percent</th>
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<table>
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<tr>
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<th>Si(OH)4</th>
<th>Si(OH)</th>
<th>SiO(OH)2</th>
<th>SiO</th>
<th>Ptotal</th>
<th>XSi(OH)4, Percent</th>
<th>XSiO(OH), Percent</th>
<th>XSiO(OH)2, Percent</th>
<th>XSiO, Percent</th>
<th>Xtotal</th>
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<td>0.08</td>
<td>0.00</td>
<td>1.00</td>
</tr>
<tr>
<td>1250</td>
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<td>3.89E-08</td>
<td>9.95E-10</td>
<td>2.38E-05</td>
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<td>1.00</td>
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<td>1.87</td>
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<td>1.00</td>
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<tr>
<td>1500</td>
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<tr>
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<td>0.01</td>
<td>10.58</td>
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<td>1.00</td>
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<td></td>
</tr>
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</table>

TABLE 3.1—CALCULATED PARTIAL PRESSURES OF Si-O-H VOLATILE SPECIES AT MR = 6, P = 0.34 ATM, AS A FUNCTION OF PANEL SURFACE TEMPERATURE [Allendorf (ALL95) Data for SiO(OH)(g) (Preferred).]

TABLE 3.2—CALCULATED PARTIAL PRESSURES OF Si-O-H VOLATILE SPECIES AT MR = 6, P = 2.10 ATM, AS A FUNCTION OF PANEL SURFACE TEMPERATURE [Allendorf (ALL95) Data for SiO(OH)(g) (Preferred).]
It can be seen that $\text{Si(OH)}_4(g)$ dominates at the lower temperatures and higher pressures. At higher temperatures and lower pressures $\text{SiO}(g)$ becomes more important. While $\text{SiO(OH)}_2$ contributes to the overall volatility of silica, it is never the dominant species under these combustion conditions. Using the data of Allendorf for $\text{SiO(OH)}(g)$, this species never contributes significantly to silica volatility.

### 3.2 Gas Boundary Limited Recession Calculation

The SiC recession is calculated assuming that it is caused by formation of volatile Si-O-H species and that the rate of recession is limited by transport of the product volatile species through a laminar gas boundary layer. This is shown schematically in Figure 3.3 and has been described in detail for SiC (OPI97).
Figure 3.3—Schematic illustration of SiC volatility limited by transport of Si-O-H(g) species through a laminar gas boundary layer for a flat plate geometry.

Assuming a flat plate geometry, the flux of volatile species, \( J \), is given by (GEI80, GAS92):

\[
J = 0.664 \left( \frac{\rho' v L}{\eta} \right)^{1/2} \left( \frac{\eta}{\rho' D} \right)^{1/3} \frac{DPM}{LRT}
\]  

(1)

The term in the first parentheses is the dimensionless Reynolds number, while the term in the second set of parentheses is the dimensionless Schmidt number. The symbols are defined in Table 3.3. The recession depends on gas pressures, temperature, and velocity.

<table>
<thead>
<tr>
<th>Symbol</th>
<th>Definition</th>
<th>Units</th>
<th>Comments</th>
</tr>
</thead>
<tbody>
<tr>
<td>( \rho' )</td>
<td>Density of gas boundary layer</td>
<td>g/cm²</td>
<td>Calculated from ideal gas law</td>
</tr>
<tr>
<td>( v )</td>
<td>Gas velocity</td>
<td>cm/sec</td>
<td>Combustion gas variable</td>
</tr>
<tr>
<td>( L )</td>
<td>Characteristic length</td>
<td>cm</td>
<td>Length of panel</td>
</tr>
<tr>
<td>( \eta )</td>
<td>Gas viscosity of boundary layer</td>
<td>g/(cm sec)</td>
<td>Obtained from tabulated values (SVE62)</td>
</tr>
<tr>
<td>( D )</td>
<td>Interdiffusion coefficient of volatile species in laminar boundary layer</td>
<td>cm²/sec</td>
<td>Calculated from Chapman Enskog Equation, see (GEI80)</td>
</tr>
<tr>
<td>( P )</td>
<td>Partial pressure of volatile species</td>
<td>atm</td>
<td>Predicted from thermodynamic data</td>
</tr>
<tr>
<td>( M )</td>
<td>Molecular weight of volatile species</td>
<td>g/mol</td>
<td></td>
</tr>
<tr>
<td>( R )</td>
<td>Gas constant</td>
<td>(cm² atm) /K mol</td>
<td></td>
</tr>
<tr>
<td>( T )</td>
<td>Absolute temperature</td>
<td>K</td>
<td>Material surface temperature variable</td>
</tr>
</tbody>
</table>

A sample recession calculation is shown in Appendix C. The assumptions made in the recession calculation Equation (1) are discussed in Appendix D. Required input to the recession calculation are the following: combustion gas pressure, material surface temperature, free stream combustion gas velocity, panel length, combustion gas viscosity (SVE62), force constants (SVE62) and collision integral (HIR54) for the volatile species and the boundary layer gas species (discussed in Appendix D), and the calculated equilibrium partial pressure of volatile Si-O-H species.

The recession attributed to the formation of each species as well as the overall recession rate in 1834 sec are reported in Table 3.4. This exposure time was chosen for comparison to GE Panel 1528-01-001-001 which actually endured nine exposures for a total plume exposure of 1834 sec. This panel is a standard matrix C/SiC panel with no oxidation protection coatings. The NASA GRC run numbers were 309 through 318. In the areas where the IR camera reported temperatures below 1723 °C, there was no measurable recession. The detectability limit of recession was estimated to be 1 mil (25 \( \mu \)m). The calculated recession rates show that about 4 mils (0.1 mm) recession is expected at the leading edge and approximately an order of magnitude less recession is expected at the trailing edge of the panel. The very low calculated recession values are consistent with the lack of observable recession temperatures below the melting point of SiO₂.
For prediction purposes the recession calculations have also been converted to rates. These SiC recession rates are found in Table 3.5.

<table>
<thead>
<tr>
<th>TC</th>
<th>Si(OH)₄</th>
<th>SiO(OH)₂</th>
<th>SiO</th>
<th>sum</th>
<th>Si(OH)₄</th>
<th>SiO(OH)₂</th>
<th>SiO</th>
<th>sum</th>
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<td>1200</td>
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<td>0.24</td>
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<td>30</td>
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<tr>
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<td>38</td>
<td>38</td>
</tr>
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<td>46</td>
<td>46</td>
<td>46</td>
</tr>
<tr>
<td>1500</td>
<td>0.42</td>
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<td>0.21</td>
<td>0.73</td>
<td>55</td>
<td>2</td>
<td>57</td>
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<td>1600</td>
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<td>0.31</td>
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<td>2.24</td>
<td>64</td>
<td>6</td>
<td>5</td>
<td>75</td>
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<td>0.86</td>
<td>8.02</td>
<td>9.46</td>
<td>74</td>
<td>18</td>
<td>27</td>
<td>119</td>
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### Table 3.5—Calculated SiC Recession Rates as a Function of Temperature at the Trailing (TE) and Leading (LE) Edge of the Panel

<table>
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<td>0.59</td>
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<td>1400</td>
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</tr>
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<td>1500</td>
<td>1.43</td>
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<td>1600</td>
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<td>1700</td>
<td>18.57</td>
<td>234</td>
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### 4.0 Validation of the Recession Model

Appendix D discusses the assumptions made in using Equation (1), the recession due to laminar boundary layer limited transport of volatile species from a flat plate of silica. However, the much larger question of the applicability of the model in general has not yet been discussed. Does a thermally grown layer of silica actually exist on the SiC surface or is the surface bare SiC? The gas boundary layer is assumed to limit the volatility of Si-O-H(g) species. At these high gas velocities, is the gas boundary layer thick enough to limit transport of volatile species or does free evaporation of volatile species occur? Additionally, the reliability of the available thermodynamic data for the Si-O-H(g) species is reviewed in this section, and the effects of an alternative source of data for SiO(OH)(g) are discussed.

### 4.1 Existence of a Silica Surface Layer on the SiC

The SiC recession model has been developed assuming that a thermally grown silica layer is present on the SiC surface so that volatility occurs by reactions such as:

$$
\text{SiO}_2 + 2\text{H}_2\text{O}(g) = \text{Si(OH)}_4(g)
$$

$$
\text{SiO}_2 + \text{H}_2\text{O}(g) = \text{SiO(OH)}_2(g)
$$

$$
\text{SiO}_2 + \frac{1}{2} \text{H}_2\text{O}(g) = \text{SiO(OH)}(g) + \frac{1}{4} \text{O}_2(g)
$$

$$
\text{SiO}_2 + \text{H}_2(g) = \text{SiO}(g) + \text{H}_2\text{O}(g)
$$

An alternative that was considered is that the combustion gases react directly with the SiC surface to form volatile species in an “active oxidation” type reaction such as:
The existence of SiO$_2$ on the SiC surface for MR = 6 conditions is shown to exist by a number of methods which are discussed in more detail in the following four subsections. First, FACTSAGE calculations to determine the equilibrium products were conducted for SiC plus the combustion gas reactants showing the stability of SiO$_2$ on SiC when the calculations made physical sense. Second, the oxide thickness was estimated based on the oxidation rate of SiC and the volatility rate of SiO$_2$. Third, these results were compared to EDS results obtained at Teledyne (CAL07). Finally, the combustion conditions were compared to the literature where active oxidation was observed in H$_2$/H$_2$O mixtures (KIM87).

### 4.1.1 FACTSAGE Calculations Indicate SiO$_2$ is Present on the SiC Surface

Calculations such as those described in Section 3.1 were also conducted with SiC as the reactant instead of SiO$_2$. The predicted equilibrium partial pressures of volatile Si-O-H species are shown in comparison to those predicted for a SiO$_2$ reactant in Table 4.1.

<table>
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<th>Input</th>
<th>Equilibrium solid</th>
<th>Equilibrium vapor species, atm</th>
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</thead>
<tbody>
<tr>
<td></td>
<td>SiO</td>
<td>Si(OH)$_2$</td>
</tr>
<tr>
<td>SiC, 0.34 atm</td>
<td>SiC$^{\circ}$</td>
<td>2.8×10$^{-4}$</td>
</tr>
<tr>
<td>SiC, 2.10 atm</td>
<td>SiC$^{\circ}$</td>
<td>1.8×10$^{-4}$</td>
</tr>
<tr>
<td>SiO$_2$, 0.34 atm</td>
<td>SiO$_2$</td>
<td>1.5×10$^{-2}$</td>
</tr>
<tr>
<td>SiO$_2$, 2.10 atm</td>
<td>SiO$_2$</td>
<td>1.5×10$^{-2}$</td>
</tr>
</tbody>
</table>

*Reactant water vapor is depleted in this calculation

There are several observations that were made regarding these calculated results. First, the partial pressures of volatile Si-O-H species were about 3 orders of magnitude larger when bare SiC was assumed. By examination of Equation (1), it can be seen that this would result in SiC recession rates that are also three orders of magnitude larger than those calculated, on the order of tens to hundreds of millimeters in the 1834 sec test time at 1700 °C. This was clearly not observed experimentally. Second, examination of the calculated results indicated water vapor was depleted in the calculations for the bare SiC surface. This is not representative of the flowing combustion gases where the water vapor is continually replenished. The calculations were then repeated for bare SiC with a fixed water vapor activity, i.e., water vapor was not allowed to be depleted. In this case the SiC was consumed and SiO$_2$ was predicted as the stable solid and all the Si-O-H partial pressure results were similar to those when SiO$_2$ was input as the condensed phase reacting surface. (As a note, when SiO$_2$ was input as the condensed phase reacting surface, the results were similar whether the water vapor activity was fixed or allowed to vary). These calculated results indicate that silica should form in the combustion environment MR = 6 and that the partial pressure of volatile Si-O-H species over silica is about three orders of magnitude less than the volatile Si-O-H partial pressure over SiC.

### 4.1.2 Estimated Silica Thickness on SiC Surface From Rate Constants

During the recession of SiC, the surface is continually oxidized to silica, and this silica layer is continually volatilized to form Si-O-H vapor species. At long times a steady state condition is set up where the oxidation rate $k_p$ is equivalent to the volatilization rate $k_l$ so that a limiting oxide thickness, $x_L$, is achieved. This steady state oxide thickness and the time to achieve steady state $t_L$ can be calculated if the SiC oxidation rate and the SiO$_2$ volatilization rate are known (TED66, OPI03). The steady state oxide thickness is given by:

\[
\text{SiC + 2H}_2\text{O} = \text{SiO(g)} + \text{CO(g)} + 2\text{H}_2(\text{g})
\]  

\[
\text{SiC + 4H}_2\text{O} = \text{SiO(OH)}_2(\text{g}) + \text{CO(g)} + 3\text{H}_2(\text{g})
\]  

\[
\text{SiC + 5H}_2\text{O} = \text{Si(OH)}_4(\text{g}) + \text{CO(g)} + 3\text{H}_2(\text{g})
\]
\[ x_L = \frac{k_p}{2k_l} \]  \hspace{1cm} (9)

and the time to reach this limiting oxide thickness is given by, \( t_L \):

\[ t_L = \frac{k_p}{2(k_l)^2} \]  \hspace{1cm} (10)

These quantities have been estimated at 1700 °C based on parabolic rate constants that were extrapolated from lower temperatures and volatility rates that were calculated at 1700 °C. Details of this calculation and the assumptions made can be found in Appendix E. The results are summarized in Table 4.2.

**TABLE 4.2.—ESTIMATED OXIDE THICKNESS ON SiC PANEL UNDER MR = 6 COMBUSTION CONDITIONS**

<table>
<thead>
<tr>
<th></th>
<th>steady state oxide thickness, nm</th>
<th>time to reach steady state, sec</th>
</tr>
</thead>
<tbody>
<tr>
<td>Leading edge</td>
<td>19</td>
<td>0.1</td>
</tr>
<tr>
<td>Trailing edge</td>
<td>38</td>
<td>3</td>
</tr>
</tbody>
</table>

In summary, a silica layer thickness on the order of tens of nm is predicted to be present on the surface of SiC. This layer should protect the SiC from active oxidation type reactions.

### 4.1.3 Estimated Silica Thickness on SiC From EDS Measurements

Using the available EDS resources and without destructively analyzing the sample, Calabrese (CAL07) and coworkers were able to estimate the silica thickness on the surface of panel 1528-01-001-002 GE standard SiC seal coat tested for 16 min in Cell 22. By varying the electron accelerating voltage and calibrating the EDS oxygen signal to sampling volume for a silica film of known thickness, the silica film thickness near the leading edge of the SiC panel was estimated to be 10 nm. Portions of the panel downstream and in cooler areas had thicker estimated silica film thicknesses of 15 to 63 nm. The analyses were conducted on relatively large areas to prevent interpretation issues relative to the shape of the sampling volume. The actual pitted surface morphology suggests that there are inhomogeneities at a very small scale, but the analysis could not probe at that level of detail. The pitting will be discussed in more detail in Section 5.0. Nevertheless, the oxide thickness estimated from the experimental EDS results are in good agreement with the oxide thickness estimated from the rate constants in Section 4.1.2. The oxide thickness on the SiC panels in the flow stream is therefore likely on the order of tens of nanometers.

### 4.1.4 Comparison of Cell 22 Conditions to Active Oxidation Conditions Reported in the Literature

Active oxidation of SiC is known to occur in H\(_2\)/H\(_2\)O environments by reaction 6 as shown by Kim and Readey (KIM87). It has been demonstrated that the active to passive transition depends on the partial pressure of the oxidant (H\(_2\)O in this case), independent of the H\(_2\)O/H\(_2\) ratio (OPI95). These results were extrapolated to 1700 °C, for the purposes of the assumed temperature of the Cell 22 panel result modeling as shown in Figure 4.1. This plot is used to find the pressure at which the transition between two gas phase processes occurs. At lower oxidant pressures than the transition pressure SiO(g) is formed directly from SiC. At higher oxidant pressures than the transition pressure, SiO\(_2\) will form. However, this transition pressure is not a well-defined cut-off for weight loss by volatility reactions. It has been experimentally observed (KIM87) that weight loss will continue at higher pressures because of formation of a discontinuous silica scale as well as the reduction of silica to form SiO(g) by:

\[ \text{SiO}_2 = \text{SiO(g)} + \frac{1}{2} \text{O}_2(g) \]  \hspace{1cm} (11)

This is shown by Kim and Readey’s results in Figure 4.2.
Figure 4.1.—Active to passive transition for SiC forming SiO(g) as a function of oxidant partial pressure extrapolated to 1700 °C (OPI95).

Figure 4.2.—Active to passive transition pressures for SiC. From Kim and Readey (KIM87).

The solid symbols show the measured active to passive transition pressures. To the left of the maxima (low oxidant pressures), the weight loss rate increases with oxidant pressure as more SiO(g) is formed. To the right of the maxima, the weight loss rate decreases with oxidant pressure because more SiO₂(s) is formed, partially covering the surface. The rate of SiO(g) formation may also decrease as the reduction of SiO₂ becomes more unfavorable at higher oxidant pressures. At even higher oxidant pressures than shown on this plot, weight gain occurs as protective silica formation occurs. Extrapolating the maxima to 1700 °C and the active to passive transition pressure at 1700 °C, it can be seen where the Cell 22 conditions fall on this plot, as shown in Figure 4.3. From this plot, it is evident that the cell 22 conditions
Figure 4.3.—Active to passive transition data of Kim and Readey extrapolated to conditions of interest for Cell 22 tests.

MR = 6 are really quite oxidizing (60 percent H₂O/25 percent H₂) and are well within the oxidant pressure range where a film of SiO₂ is expected on the surface of SiC. Weight loss may still be possible as the SiO₂ film may be discontinuous or be lost by reaction of SiO₂ to form volatile species.

The data plotted in Figure 4.2 were determined at very low gas velocities, on the order of 1 cm/sec. From Wagner’s theory (WAG58), the active to passive transition oxidant pressure should be relatively independent of gas velocity. The flux of species \( X \), H₂O(g) inward to the SiC surface or SiO(g) outward from the surface, is given by:

\[
J_X = \frac{D_X P_X}{\delta_X RT}
\]  
(12)

The transition pressure is obtained by equating the flux of oxidant inward to the SiO(g) flux outward. So that:

\[
P_{\text{transition}}(\text{H}_2\text{O}) \propto \left( \frac{\delta(\text{H}_2\text{O})}{\delta(\text{SiO})} \right) \left( \frac{D(\text{SiO})}{D(\text{H}_2\text{O})} \right) P_{\text{eq}}(\text{SiO})
\]  
(13)

The velocity dependence of each flux is contained within the boundary layer thickness term, \( \delta \). In Figures 4.2 and 4.3, each temperature curve would be expected to shift up as the velocity increases. The SiO(g) flux will increase as the boundary layer thickness is decreased. However, it is expected that the gas boundary layer thickness would be similar for the oxidant and the SiO(g) so that the transition pressure should be independent of gas velocity. According to Wagner, each temperature curve in Figures 4.2 and 4.3 is not expected to move to the right or left as the velocity is increased.

In actual experimental observations, however, a small shift in the active to passive transition with velocity changes has been observed (NAR91) so that a velocity increase expands the passive regime to
lower oxidant pressures. This velocity dependence is not well understood but was explained as a change in the boundary layer ratio \( \frac{\delta(\text{oxidant})}{\delta(\text{SiO})} \) or a deviation from the equilibrium pressure, \( P(\text{SiO}) \), at the SiC surface (NAR91). Since this effect actually expands the passive regime, the Cell 22 conditions would remain well inside the passive regime even if velocity effects do occur.

In summary, the analyses in Sections 4.1.1 to 4.1.4 are in consistent agreement that a silica film should be present on the SiC surface in the Cell 22 conditions of interest. This aspect of the recession model is therefore believed to be accurate.

4.2 Gas Boundary Layer Limited Volatilization

The gas flow in Cell 22 (and other rocket engine environments) occurs at very high velocities, 8,000 to 12,000 fps. At these high gas velocities the gas boundary layer becomes very thin. The recession model assumes that volatility is limited by transport of volatile species through the gas boundary layer. It is important to understand how thin the gas boundary layer is under the Cell 22 test conditions and at what point volatility is better modeled by the free evaporation rate given by the Langmuir Equation. An expression for the gas boundary layer thickness is given by (GRA71):

\[
\frac{1.5 L}{Re^{1/2} Sc^{1/3}}
\]

where

\[
Re = \frac{\rho v L}{\eta}
\]

\[
Sc = \frac{\eta}{\rho D}
\]

First, the gas boundary layer thickness, \( \delta \), along length of panel was calculated using the local Reynolds number, \( Re_x \), for PC160MR60 provided by Jeff Stout (STO07b). The length averaged \( Re_L \) calculated using Equation (15) was also used to calculate the gas boundary layer thickness. The Reynolds numbers are reported in Appendix F. Both results are shown in Figure 4.4. The calculated gas boundary layer thickness varies from a few microns at the leading edge of the panel to a few hundred microns at the trailing edge of the panel. Again this is based on laminar flow. The exponent for the Reynolds number in the gas boundary layer calculation increases to 0.7 or 0.8 for turbulent flow (GAS92) which would decrease the boundary layer thickness. The Stout \( Re_x \) are just in the turbulent flow regime for all \( x \), assuming the laminar—turbulent flow transition occurs for \( Re = 3 \times 10^5 \). The \( Re_L \) calculated from Equation (15) transition from laminar to turbulent at about 5.5 cm (2.2 in.) from the leading edge of the panel. However, the assumption of laminar flow has little effect on the overall values of the gas boundary layer thickness.

For vanishingly thin boundary layers and high gas velocities the Hertz-Langmuir Equation can be used to calculate the flux of volatiles from a surface, \( J_L \). This equation is used to calculate the maximum evaporation reaction rate from thermodynamic data (SEA70, BAR67).

\[
J_L = P_{\text{SiOH}} \left( \frac{M_{\text{SiOH}}}{2\pi RT} \right)^{1/2}
\]
Figure 4.4.—Calculated gas boundary layer thickness as a function of test panel length.

By equating the Langmuir Flux and the boundary layer flux equations (Eqs. (17) and (1)) and solving for velocity, the gas velocity at the transition between boundary layer limited flux and Langmuir flux can be determined. Given this gas velocity, the boundary layer thickness at which volatilization is no longer transport limited can be calculated using Equation (14). This velocity is independent of the partial pressure of volatile species and depends only on gas boundary layer properties. These calculations can be found in Appendix G for the case where the surface material temperature is 1700 °C at the panel leading edge. The gas velocity at this transition is $7.35 \times 10^5$ m/sec, several hundred times larger than the maximum gas velocity in the Cell 22 tests, $3.6 \times 10^3$ m/sec. The gas boundary layer thickness where fluxes reach the Langmuir limit is about 1 µm, whereas even at the leading edge, the gas boundary layer is estimated to be 3 to 20 µm thick and increasing to several hundred µm thick by the panel trailing edge. These calculations therefore demonstrate that the use of a boundary limited volatilization model is accurate for the Cell 22 test conditions.

### 4.3 Evaluation of Thermochemical Data for Si-O-H(g)

The recession calculation will only be as good as the thermochemical data used for calculating the equilibrium partial pressures of volatile Si-O-H(g) species. The reliability of these data is therefore summarized here.

#### 4.3.1 SiO(g)

This species is well characterized and appears in all databases known to this author. The data from FACT53 (BAL02) were used for these calculations.

#### 4.3.2 Si(OH)$_4$(g)

While data for this species do not appear in any commercial databases, it has recently been well characterized by several groups (HAS92, ALL95, JAC05). There is good agreement between all studies for this species. The data of Jacobson et al. (JAC05) are used for these calculations.
4.3.3 SiO(OH)$_2$(g)

There are limited experimental data for this species (JAC05, HIL94, HIL98). Additional estimated data are given by Krikorian (KRI70). Preference is given to experimental data, therefore, the data of Jacobson et al (JAC05) have been used for these calculations. While these data are uncertain, there are no conditions where this species is predicted to dominate, thus the uncertainty of the stability of this vapor species is unlikely to affect the overall accuracy of the recession calculations.

4.3.4 SiO(OH)(g)

There is the most uncertainty for the thermodynamic data for this species. There is one possible identification of this species by experimental techniques (HIL94, HIL98) and three other sources of estimated (KRI70) or calculated data for this species (DAR93, ALL95). The thermochemical data for this vapor species, as well as the source of the data, are summarized in Table 4.3. The heats of formation fall into two groups, those in the range of –305 to –356 kJ/mol (DAR93, ALL95, HIL98, SAN07) as used in prior calculations and those around –500 kJ/mol (KRI70, HIL94). The two available values for $S^\circ$ (KRI70, ALL95) are in better agreement. Since the enthalpy data are so uncertain, the recession rates previously calculated using the preferred values computed by Allendorf et al. (ALL95) are compared to the recession rates obtained using the data estimated by Krikorian (KRI70). The Allendorf data are preferred in this case, since they give better agreement with experimental observations in Cell 22. However, an upper bound of SiC recession attributed to SiO(OH)(g) formation is obtained using the estimated data of Krikorian (KRI70).

Using the thermodynamic data for SiO(OH)(g) of Krikorian, the partial pressures of all volatile Si-O-H species were calculated between the temperatures of 1200 and 1700 °C for the Cell 22 conditions. The results are plotted for the Si-O-H species with the four highest partial pressures in Figures 4.5 and 4.6. Raw data can be found in Appendix G. The calculated partial pressures of SiO(OH)(g) are five to seven orders of magnitude lower using the data of Allendorf compared to the data of Krikorian. With the Allendorf data, SiO(OH)(g) does not contribute to volatility under any of the temperature and pressure conditions examined in these calculations whereas the SiO(OH)$_2$(g) vapor species does contribute to the overall recession. Using the Krikorian data for SiO(OH)(g), Si(OH)$_4$(g) still dominates at low temperature and high pressure conditions, but now SiO(OH)(g) exceeds the importance of SiO(g) at low pressures and high temperatures. The contributions of SiO(OH)$_2$(g) are now negligible. While the Allendorf data for SiO(OH)(g) are preferred due to the better agreement with experimental results, this comparison shows that greater uncertainty in recession calculations is present at the high temperature, low pressure conditions.

### TABLE 4.3.—THERMOCHEMICAL DATA AVAILABLE FOR SiO(OH)(g)

<table>
<thead>
<tr>
<th>Reference</th>
<th>$\Delta H^\circ_f$(TK), kJ/mol</th>
<th>$S^\circ$, J/mol</th>
<th>Method of determination</th>
<th>Comments</th>
</tr>
</thead>
<tbody>
<tr>
<td>Krikorian (KRI70)</td>
<td>–494±34, 0 K</td>
<td>---</td>
<td>Estimation</td>
<td>GEF available</td>
</tr>
<tr>
<td>Krikorian* (KRI70)</td>
<td>–503±4, 298 K</td>
<td>263</td>
<td>Estimation</td>
<td>Derived from GEF</td>
</tr>
<tr>
<td>Darling (DAR93)</td>
<td>–305±8, 298 K</td>
<td>---</td>
<td>Calculation</td>
<td>G2</td>
</tr>
<tr>
<td>Hildenbrand (HIL94)</td>
<td>–494±17, 298 K</td>
<td>---</td>
<td>Expt., mass spec</td>
<td></td>
</tr>
<tr>
<td>Allendorf (ALL95)</td>
<td>–313±6, 298 K</td>
<td>271</td>
<td>Calculation</td>
<td>BAC-MP4</td>
</tr>
<tr>
<td>Hildenbrand (HIL98)</td>
<td>&lt;–356, 298 K</td>
<td>---</td>
<td>Expt., mass spec</td>
<td>Revised from (HIL94)</td>
</tr>
<tr>
<td>Sandia (SAN07)</td>
<td>Same as (ALL95)</td>
<td></td>
<td></td>
<td>$C_p$(T) available</td>
</tr>
</tbody>
</table>

*aUsed in prior recession calculations
Figure 4.5.—Temperature dependence of Si-O-H vapor species at MR = 6, P = 0.34 atm. Krikorian (KRI70) estimated data for SiO(OH)(g) (not recommended).

Figure 4.6.—Temperature dependence of Si-O-H vapor species at MR = 6, P = 2.10 atm. Krikorian (KRI70) estimated data for SiO(OH)(g) (not recommended).

The calculated recession rates using the Krikorian data for SiO(OH)(g) are compared to those obtained using the Allendorf data for SiO(OH)(g) in Table 4.4. The overall calculated recession rates are similar at 1200 °C and about an order of magnitude lower at 1700 °C when the preferred Allendorf data are used for SiO(OH)(g).
TABLE 4.4.—CALCULATED SiC RECESSION DUE TO Si-O-H VOLATILITY FOR 1834 SEC EXPOSURE AT MR = 6 AT P = 2.10 ATM (LEADING EDGE) AND P = 0.34 ATM (TRAILING EDGE) OF PANEL IN CELL 22
[Comparison of Krikorian to Allendorf data for SiO(OH)(g).]

<table>
<thead>
<tr>
<th>TC</th>
<th>Si(OH)$_4$</th>
<th>SiO(OH)$_2$</th>
<th>SiO</th>
<th>Sum</th>
<th>Si(OH)$_4$</th>
<th>SiO(OH)$_2$</th>
<th>SiO</th>
<th>Sum</th>
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<td>----</td>
<td>0.27</td>
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<td>0.27</td>
<td>----</td>
<td>0.57</td>
<td>38</td>
<td>2</td>
<td>40</td>
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</tr>
<tr>
<td>1400</td>
<td>0.36</td>
<td>1.65</td>
<td>----</td>
<td>2.01</td>
<td>46</td>
<td>14</td>
<td>60</td>
<td></td>
</tr>
<tr>
<td>1500</td>
<td>0.42</td>
<td>8.35</td>
<td>----</td>
<td>8.77</td>
<td>55</td>
<td>68</td>
<td>123</td>
<td></td>
</tr>
<tr>
<td>1600</td>
<td>----</td>
<td>34</td>
<td>1.43</td>
<td>35.43</td>
<td>64</td>
<td>283</td>
<td>347</td>
<td></td>
</tr>
<tr>
<td>1700</td>
<td>----</td>
<td>123</td>
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<td>131.02</td>
<td>74</td>
<td>1024</td>
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</table>

with Allendorf data for SiO(OH) (PREFERRED)

<table>
<thead>
<tr>
<th>TC</th>
<th>Si(OH)$_4$</th>
<th>SiO(OH)$_2$</th>
<th>SiO</th>
<th>Sum</th>
<th>Si(OH)$_4$</th>
<th>SiO(OH)$_2$</th>
<th>SiO</th>
<th>Sum</th>
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</thead>
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<td>----</td>
<td>----</td>
<td>0.24</td>
<td>30</td>
<td>----</td>
<td>30</td>
<td></td>
</tr>
<tr>
<td>1300</td>
<td>0.30</td>
<td>----</td>
<td>----</td>
<td>0.30</td>
<td>38</td>
<td>----</td>
<td>38</td>
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</tr>
<tr>
<td>1400</td>
<td>0.36</td>
<td>0.03</td>
<td>0.02</td>
<td>0.41</td>
<td>46</td>
<td>----</td>
<td>46</td>
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<tr>
<td>1500</td>
<td>0.42</td>
<td>0.10</td>
<td>0.21</td>
<td>0.73</td>
<td>55</td>
<td>2</td>
<td>57</td>
<td></td>
</tr>
<tr>
<td>1600</td>
<td>0.50</td>
<td>0.31</td>
<td>1.43</td>
<td>2.24</td>
<td>64</td>
<td>6</td>
<td>5</td>
<td>75</td>
</tr>
<tr>
<td>1700</td>
<td>0.58</td>
<td>0.86</td>
<td>8.02</td>
<td>9.46</td>
<td>74</td>
<td>18</td>
<td>27</td>
<td>119</td>
</tr>
</tbody>
</table>

5.0 Other Mechanisms Contributing to SiC Degradation in Addition to Silica Volatility

Sudre and coworkers (SUD06) describe the failure of Cell 22 C/SiC test panels by a sequence of SiC cracking, pitting, grooving, oxidation of underlying carbon fibers, and eventual spallation of the SiC seal coat as shown in Figure 5.1. This mechanism results in greater recession rates than the volatility mechanism since the entire SiC coating tends to spall once the degradation occurs.

Figure 5.1.—Grooving and pitting of SiC surface after test in Cell 22. (Test panel GE 1528-01-001-002) Image courtesy of O. Sudre, Q. Yang, and D. Marshall, Teledyne Scientific (SUD06).
5.1 Cracking

Presumably the cracks in the SiC arise due to the thermal expansion mismatch of the carbon fibers and the SiC matrix/seal coat. For C/C composites coated with SiC, cracks have been observed to follow the weave pattern of the fibers and to occur at regular intervals based on the stresses generated during cool down from the processing condition. (JAC07). These stress states could be modeled for the C/SiC composite leading to an understanding of the crack width and spacing.

5.2 Pitting

Similar SiC pitting has been observed for SiC exposed in molten salts, chlorine, and H2-rich environments (JAC86, MAR88, JAC90). Pitting occurs at several locations:

1. Structural discontinuities (dislocations, high energy surfaces).
2. Areas without protective oxide such as areas where gaseous oxidation products disrupt the SiO2 scale. Since the estimated oxide layer thickness for the Cell 22 combustion conditions is only about 10 nm, it is likely this layer could be easily disrupted leading to more rapid attack. Once disrupted, the rate of attack should be much higher as predicted by the FACTSAGE calculations for bare SiC.
3. Areas where, due to poor combustion gas mixing, the local environment is more aggressive. Such poor mixing conditions could lead to higher temperatures where local environments are closer to the stoichiometric condition. The silica scale could be molten and locally swept away by shear forces. This mechanism is discussed in Section 6.0. Alternatively, poor mixing can also result in areas with lower water partial pressures where the combustion products are more fuel rich. These local areas could be more reducing leading to locally higher degradation rates.

5.3 Grooving

The observed grooving that occurs at the crack locations in the SiC seal coat is not understood. One possibility is that local turbulence due to the rough weave morphology of the surface causes flow instabilities and enhanced attack at these locations (SUD07). An alternative explanation is that water vapor diffuses down the pre-existing cracks and oxidation of the underlying carbon fibers occurs by the reaction:

\[ C + H_2O(g) = CO(g) + H_2(g) \] (18)

The product gases CO and H2 diffuse out through the cracks and create a locally more aggressive (reducing) environment in which active oxidation occurs. Both explanations for the observed grooving are speculation at this point and this effect requires additional understanding.

5.4 Oxidation of Underlying Carbon Fibers

A model for oxidation of C/C beneath a SiC seal coat has been developed (JAC07). At high temperatures, the oxidation rate of the underlying carbon is controlled by diffusion of the oxidant through the gas boundary layer and through the coating cracks. Since the surface carbon oxidation rate is fast relative to the oxidant transport rate, oxidation at the first available surface of the underlying carbon occurs, forming oxidation cavities beneath the cracks. Once these cavities reach dimensions of half the crack spacing, the overlying SiC will spall. The parameters that affect the oxidation rate are temperature, oxidant pressure, gas velocity, and crack width. This model could be extended to C/SiC with an overlying SiC seal coat by including oxidation of the SiC matrix.

In summary, a thermomechanical model of cracking in SiC sealed C/SiC in combination with a model of carbon fiber oxidation may be applicable to explain the observed behavior of the C/SiC panels tested in Cell 22.
6.0 Shear Flow of Liquid Layers at High Temperatures

Recession of solid phase silica layers was discussed in Sections 2.0 through 4.0. At material surface temperatures greater than the melting point of silica, 1723 °C (or lower temperatures in the presence of impurities), the liquid oxide film would be expected to flow due to shear forces of the flowing combustion gases on the liquid film. Similarly, for low melting borosilicate glass coatings, shear flow is expected to remove the liquid glass layer. Both shear flow of silica and glass coatings is expected to limit the protective capability of these layers by physically removing them. Therefore an understanding of the shear forces of the flowing combustion gases on the liquid films is needed.

6.1 Modeling Shear Flow of Liquids

A simple model to understand the effects of gas and liquid properties on the shear flow of a liquid film was developed with the help of David Jacqmin at GRC (JAQ07).

Assume the configuration for a gas film flowing over a liquid film on SiC as shown in Figure 6.1.

Here, the subscript \( g \) refers to gas and \( l \) refers to liquid. Start with one-dimensional Navier-Stokes equation for the liquid film:

\[
\rho \frac{dv}{dt} = -\frac{\partial p}{\partial z} + \eta \frac{d^2 v}{dz^2} \tag{19}
\]

Assume the velocity does not change with time and there are no pressure gradients. The first term on each side of Equation (19) is zero, leaving:

\[
0 = \eta \frac{d^2 v}{dz^2} \tag{20}
\]

BC: at \( z = 0, v_l = 0 \) \tag{21}

at \( z = h(x,t) \) \( \eta_g \frac{\partial v_g}{\partial z} = \eta_l \frac{\partial v_l}{\partial z} \) \tag{22}

The first boundary condition is the no slip condition for a fluid at a solid surface. The velocity of the liquid is zero at the SiC surface. The second BC is the same as \( \tau_g = \tau_l \), the shear stress in the liquid is equal to the shear stress in the gas at the interface. Also at this interface, \( v_g = v_l \). Here, \( \eta_g = f(T) \), \( T = f(x,t) \), \( T \neq f(z) \).

Figure 6.1.—Schematic illustration of liquid film used in shear flow model.
Assume the liquid velocity can be described by an equation of the form:

\[ v_l(z) = a + bz + cz^2 \]  (23)

If there is no pressure gradient in the glass then \( c = 0 \).

We also know \( a = 0 \) from the first boundary condition.

Taking the first derivative of the velocity equation, Eq. (23):

\[ \frac{\partial v_l}{\partial z} = b \]  (24)

We know from the second boundary condition that

\[ b = \frac{\eta_g}{\eta_l} \left( \frac{\partial v_g}{\partial z} \right) \]  (25)

and the result is that

\[ v_l = \frac{\eta_g}{\eta_l} \left( \frac{\partial v_g}{\partial z} \right) z \]  (26)

The term \( \frac{\partial v_g}{\partial z} \) can be approximated by the free stream gas velocity divided by the gas boundary layer thickness, both are known quantities. The following plots explore the effect of variations in liquid viscosity for gas boundary layer properties relevant to the Cell 22 tests. In the first plot, properties representative of a silica film with impurities at 1700 °C were assumed (Table 6.1, Figure 6.2). In the second case, properties representative of a borosilicate coating with impurities were assumed (Table 6.2, Figure 6.3).

<table>
<thead>
<tr>
<th>TABLE 6.1.—PARAMETERS USED TO ESTIMATE THE SHEAR FLOW VELOCITY OF A LIQUID SILICA FILM AT 1700 °C</th>
</tr>
</thead>
<tbody>
<tr>
<td>Silica film case</td>
</tr>
<tr>
<td>( \eta_{\text{gas}} ) = .............................................................. 6.56E-04 poise</td>
</tr>
<tr>
<td>( \eta_{\text{liquid}} ) = ............................................................. 107 poise</td>
</tr>
<tr>
<td>Liquid thickness = ............................................................... 1.00E-05 cm</td>
</tr>
</tbody>
</table>
Figure 6.2.—Velocity of liquid silica at 1700 °C due to shear forces from gas flow as a function of distance along the test panel.

Figure 6.3.—Liquid glass flow velocity due to shear forces from gas flow as a function of distance along the test panel. Calculated and measured velocity of borosilicate liquid compared to silica liquid at 1700 °C.

<table>
<thead>
<tr>
<th>TABLE 6.2.—PARAMETERS USED TO ESTIMATE THE SHEAR FLOW VELOCITY OF A LIQUID BOROSILICATE FILM AT 1700 °C REPRESENTATIVE OF THE APPLIED COATING</th>
</tr>
</thead>
<tbody>
<tr>
<td>Borosilicate coating case</td>
</tr>
<tr>
<td>( \eta_{\text{gas}} = 6.56 \times 10^{-4} ) poise</td>
</tr>
<tr>
<td>( \eta_{\text{liquid}} = 100 ) poise</td>
</tr>
<tr>
<td>Liquid thickness = ( 2.5 \times 10^{-2} ) cm</td>
</tr>
</tbody>
</table>
These calculated glass velocities are qualitatively reasonable. The borosilicate coating has been observed to flow during cell 22 testing, whereas no flow of the silica films have been observed. A comparison to actual measured flow rates is made in Section 6.2.

The glass viscosities used in the calculations were estimated from Figure 6.4 extrapolated to 1700 °C. Viscosities about one order of magnitude lower than those extrapolated from the plot were chosen to account for the effects of impurities found in combustion environments. Discussions with David Jarmon, GE, suggest the coating on the panel contains Corning 7740 borosilicate (or a similar glass) and the viscosity value chosen to represent the coating is a reasonable estimate (JAR07). In addition, the silica glass viscosity of 10^7 poise is in good agreement with values from Weiss (WEI84).

The total flux of glass, \( Q \), could also be calculated to estimate a removal rate of the glass coating or film, however, this flux was not calculated as part of this report.

\[
Q = \int v_f(z) \, dz = 1/2 \, h_2 \, \left( \frac{\partial v_f}{\partial z} \right) h^2
\]

(27)

### 6.2 Comparison of Observed and Modeled Shear Flow of Liquids

Footage of run 388, Cell 22, was obtained from Jeff Stout which showed the UTRC borosilicate glass coating flowing during test (STO07c). Individual frames of this .mpg file were captured at about 0.1 sec intervals between the times of 8 to 9.9 sec using Topaz Moment (TOP07). This 2 sec time interval was chosen just after the gain was reduced to lower the brightness of the movie image. The movement of four drops as a function of distance down the panel in the direction of flow was measured and is plotted in Figure 6.5. Photographs and time indices of the actual drops that were used can be found in Appendix H. The velocities of these four drops were very similar as shown in Figure 6.5 and an approximate average velocity of 2.5 cm/sec was obtained. The distance along the panel for which the drop velocity was monitored was typically 3 to 5 cm from the leading edge.

![Figure 6.4.—Viscosity of various glasses as a function of temperature (BRI07).](image)
Comparison of the measured velocity to the calculated velocity is quite good: 2.5 cm/sec measured versus 3.5 to 4.4/sec cm calculated as shown graphically in Figure 6.3. The drop velocities do tend to slow slightly as they travel down the length of the panel, as shown in Figure 6.5, consistent with the model. The calculated liquid velocity depends on the glass and gas viscosity as well as the liquid and gas layer thickness (Eq. (26)). Since the viscosity varies strongly with temperature and all other values remain relatively constant with temperature, the liquid velocity is most strongly influenced by the viscosity of the glass for a given combustion condition and panel configuration.
Appendix A.—CEA Calculated Combustion Products for MR = 6.0, Pc = 160 psi

*******************************************************************************
NASA-LEWIS CHEMICAL EQUILIBRIUM PROGRAM CEA, SEP. 4, 1997
BY BONNIE MCBRIDE AND SANFORD GORDON
*******************************************************************************

reac
oxid O2 wtfrac= 1 t(k)=298.15
fuel H2 wtfrac= 1 t(k)=298.15
prob case=test hp p(psi)=160 o/f=6.0
output siunits trace=1.e-15
end

OPTIONS: TP=F HP=T SP=F TV=F UV=F DETN=F SHOCK=F REFL=F INCD=F
RKT=F FROZ=F EQL=F IONS=F SIUNIT=T DEBUGF=F SHKDBG=F TRNSPT=F

TRACE= 1.00E-15 S/R= 0.000000E+00 H/R= 0.000000E+00 U/R= 0.000000E+00

P,BAR = 11.031569

REACTANT WT.FRAC (ENERGY/R),K TEMP,K DENSITY
EXPLODED FORMULA
O: O2 1.000000 -.988318E-06 298.15 .0000
O 2.00000
F: H2 1.000000 -.489101E-05 298.15 .0000
H 2.00000

SPECIES BEING CONSIDERED IN THIS SYSTEM
(CONDENSED PHASE MAY HAVE NAME LISTED SEVERAL TIMES)
l 6/97 *H l 5/89 HO2 tpis78 *H2
l 8/89 H2O l 2/93 H2O2 l 5/97 *O
tpis78 *OH tpsis89 *O2 l 5/90 03
l 8/89 H2O(s) l 8/89 H2O(L)

O/F = 6.000000

EFFECTIVE FUEL EFFECTIVE OXIDANT MIXTURE
ENTHALPY h(2)/R h(1)/R h0/R
(KG-MOL)(K)/KG -.24262412E-05 -.30886106E-07 -.37307969E-06

KG-FORM.WT./KG bi(2) bi(1) b0i
*O .00000000E+00 .62502344E-01 .53573438E-01
*H .99212255E+00 .00000000E+00 .14173179E+00

POINT ITN T O H
l 10 3354.366 -16.531 -10.113

THERMODYNAMIC EQUILIBRIUM COMBUSTION PROPERTIES AT ASSIGNED
PRESSURES
CASE = test

REACTANT WT FRACTION ENERGY TEMP
(SEE NOTE) KJ/KG-MOL K
OXIDANT O2 1.0000000 .000 298.150
FUEL H2 1.0000000 .000 298.150

O/F= 6.000000 %FUEL= 14.285714 R,EQ.RATIO= 1.322780 PHI,EQ.RATIO= 1.322780

THERMODYNAMIC PROPERTIES
P, BAR 11.032
T, K 3354.37
RHO, KG/CU M 5.1239-1
H, KJ/KG .53573438E-01
U, KJ/KG -2152.94
G, KJ/KG -64676.4
S, KJ/(KG)(K) 19.2813
M, (1/n) 12.954
(dLV/dLP)t -1.04587
(dLV/dLT)p 1.8364
Cp, KJ/(KG)(K) 13.6265
GAMMAs 1.1274
SON VEL, M/SEC 1557.9

MOLE FRACTIONS

*H 6.3300-2
H2O 3.1414-5
*H2 2.2154-4
H2O 6.0279-1
H2O2 5.3796-6
*O 9.4055-3
*OH 6.4026-2
*O2 8.8113-1
O3 7.7800-9

* THERMODYNAMIC PROPERTIES FITTED TO 20000.K

PRODUCTS WHICH WERE CONSIDERED BUT WHOSE MOLE FRACTIONS
WERE LESS THAN 1.000000E-15 FOR ALL ASSIGNED CONDITIONS

H2O(s) H2O(L)

NOTE. WEIGHT FRACTION OF FUEL IN TOTAL FUELS AND OF OXIDANT IN TOTAL OXIDANTS
Appendix B.—Sample FACTSAGE Calculation for the Reaction of \( \text{SiO}_2 \) and Combustion Gases at a Material Temperature of 1700 °C and the Panel Trailing Edge Pressure, 0.34 atm

\[
T = 1700.00 \, ^\circ\text{C} \\
P = 3.40000 \times 10^{-1} \, \text{atm} \\
V = 4.37502 \times 10^2 \, \text{dm}^3
\]

**STREAM CONSTITUENTS AMOUNT/mol**

<table>
<thead>
<tr>
<th>STREAM CONSTITUENT</th>
<th>AMOUNT/mol</th>
</tr>
</thead>
<tbody>
<tr>
<td>( \text{H}_2\text{O} )</td>
<td>6.0279E-01</td>
</tr>
<tr>
<td>( \text{H}_2 )</td>
<td>2.5154E-01</td>
</tr>
<tr>
<td>( \text{OH} )</td>
<td>6.4026E-02</td>
</tr>
<tr>
<td>( \text{H} )</td>
<td>6.3300E-02</td>
</tr>
<tr>
<td>( \text{O} )</td>
<td>9.4905E-03</td>
</tr>
<tr>
<td>( \text{O}_2 )</td>
<td>8.8113E-03</td>
</tr>
<tr>
<td>( \text{SiO}_2 )</td>
<td>1.0000E+00</td>
</tr>
</tbody>
</table>

**EQUIL AMOUNT MOLE FRACTION FUGACITY**

<table>
<thead>
<tr>
<th>P H _EQUIL</th>
<th>S H _EQUIL</th>
<th>G H _EQUIL</th>
<th>V N _EQUIL</th>
</tr>
</thead>
<tbody>
<tr>
<td>1.20059E+02</td>
<td>-8.98538E+05</td>
<td>4.05268E+02</td>
<td>-1.69819E+06</td>
</tr>
</tbody>
</table>

Data on 13 constituents marked with 'T' are extrapolated outside their valid temperature range.
Appendix C.—Example Recession Calculation for Combustion Gases at a Material Temperature of 1700 °C and the Panel Trailing Edge Pressure, 0.34 atm

SAA P&W case 18: SiO₂, 0.34 atm, 1700 °C.
Calculating k₁ for SiC in Cell 22 assuming Si(OH)₄, SiO(OH)₂ and SiO formation dominate.

First, define the system and sample parameters: O/F = 6.0
Gas parameters:
P := 0.34 atm
(4.93 psia)
T := 1973 K
v₁ := 3.565 \times 10^{-5} \text{ cm/sec}

sample length:
L := 16.34 cm
(6.43 in.)

Assume a boundary layer of water vapor at the surface of the SiC is rate controlling and calculate the Reynolds number.

M := 18 \text{ gm/mole}
R := 82.06 \text{ cm}^3\text{ atm/mole K}

\rho := \frac{P \cdot M}{R \cdot T}
\rho = 3.78 \times 10^{-5} \text{ gm/cm}^3

\eta(T) is the viscosity of the H₂O gas (Other components of the gas boundary layer are neglected here).
Individual viscosities are interpolated from NASA Technical Report R-132 by R.A. Svehla
\eta := 6.564 \times 10^{-4} \text{ gm/cm sec}

The Reynolds number is:
\text{Re}_1 := \frac{\rho \cdot v_1 \cdot L}{\eta}
\text{Re}_1 = 3.355 \times 10^5

Use Re=3\times10^5 as criterion for transition from laminar to turbulent.
The flow is laminar for smooth sample lengths of less than 5.75 in.
Calculate the interdiffusion coefficient for the water vapor and SiO gases.
The collision diameter, σ, and collision integral, Ω, must be calculated first.
A useful reference for these values is NASA Technical Report R-132 by R.A. Svehla.
σₐ := 2.641

collision diameter for H₂O in angstroms
$\sigma_B := 3.37 \text{Å}$

collision diameter for SiO in angstroms

$\sigma_{AB} := \frac{\sigma_A + \sigma_B}{2}$

$\sigma_{AB} = 3.008$

$\varepsilon_A := 809.1 \text{K}$

This value is $\varepsilon/\kappa$ for water vapor

$\varepsilon_B := 569 \text{K}$

This value is $\varepsilon/\kappa$ for SiO

$\varepsilon_{AB} := \sqrt{\varepsilon_A \cdot \varepsilon_B}$

$\varepsilon_{AB} = 678.512 \text{K}$

$T' := \frac{T}{\varepsilon_{AB}}$

$T' = 2.908$

$\Omega$ is then picked from a table on p. 20 of Mass Transfer by Sherwood et al. based on the value of $T'$. $\Omega := 0.9569$

The interdiffusion coefficient can now be calculated using the Chapman-Enskog Equation:

$M_A := 18$

The values are all entered without units here because the equation is formulated with the constant $0.0018583$ and $P(\text{atm})$, $T(\text{K})$, $\sigma(\text{angstroms})$, $M(\text{gm/mole})$

$M_B := 44$

$T := 1973$

$P := 0.34$

$D_{AB} := .0018583 \sqrt{\frac{1}{M_A} + \frac{1}{M_B}} \cdot \frac{T^2}{P \cdot \sigma_{AB}^2 \cdot \Omega}$

$D_{AB} = 15.484$

$D_{AB} := 15.484 \text{ cm}^2 \text{ sec}^{-1}$

The Schmidt number can now be calculated:

$Sc := \frac{\eta}{\rho \cdot D_{AB}}$

$Sc = 1.121$

The pressure and concentration of SiO are now needed: This information is based on SiO from FactSage.

Material temp of 1973K was used to calculate $P_{SiO}$

$P_{SiO} := 1.5 \cdot 10^{-5} \text{ atm}$

The concentration of SiO is then:

$M_B := 44 \cdot \frac{\text{gm}}{\text{mole}}$
Now the flux of SiO from a flat plate can be calculated:

\[ J := \frac{1}{0.664 \text{Re}^{2/3}} \frac{1}{\text{Sc}^{2/3}} \cdot \text{D}_{AB} \rho \text{SiO} \]

\[ J = 1.543 \times 10^{-6} \frac{\text{gm}}{\text{cm}^2 \cdot \text{sec}} \]

\[ J = 5.557 \frac{\text{mg}}{\text{cm}^2 \cdot \text{hr}} \]

\[ J_{\text{SiC}} := \frac{J}{3.21 \times 10^3 \frac{\text{mg}}{\text{cm}^3}} \cdot \frac{40}{44} \]

\[ J_{\text{SiC}} = 4.371 \times 10^{-6} \frac{6 \text{ mm}}{\text{sec}} \]

\[ t := 1834 \text{ sec} \]

\[ X_{\text{SiC}} := J_{\text{SiC}} \cdot t \]

\[ X_{\text{SiC}} = 8.017 \times 10^{-3} \text{ mm} \]

Calculate the interdiffusion coefficient for the water vapor and SiO(OH)\(_2\) gases.

The collision diameter, \( \sigma \), and collision integral, \( \Omega \), must be calculated first.

A useful reference for these values is NASA Technical Report R-132 by R.A. Svehla.

\[ \sigma_A := 2.641 \]

collision diameter for H\(_2\)O in angstroms

\[ \sigma_B := 4.293 \]

collision diameter for SiO(OH)\(_2\) in angstroms, use average of values for SiO\(_2\) and Si(OH)\(_4\)

\[ \sigma_{AB} := \frac{\sigma_A + \sigma_B}{2} \]

\[ \sigma_{AB} = 3.467 \]

\[ \varepsilon_A := 809.1 \text{ K} \]

This value is \( \varepsilon/\kappa \) for water vapor

This value is \( \varepsilon/\kappa \) for the average of values for SiO\(_2\) and Si(OH)\(_4\) as an estimate for SiO(OH)\(_2\)

\[ \varepsilon_B := 1563 \text{ K} \]

\[ \varepsilon_{AB} := \sqrt{\varepsilon_A \varepsilon_B} \]

\[ \varepsilon_{AB} = 1.125 \times 10^3 \text{ K} \]
\( T' := \frac{T}{\varepsilon_{AB}} \)

\( T' = 1.754 \)

\( \Omega \) is then picked from a table on p. 20 of Mass Transfer by Sherwood et al. based on the value of \( T' \).

\( \Omega := 1.127 \)

The interdiffusion coefficient can now be calculated using the Chapman-Enskog Equation:

\[
D_{AB} := 0.0018583 \sqrt{\frac{1}{M_A} + \frac{1}{M_B} \cdot \frac{T}{T'}^2 \left( \frac{1}{P \cdot \sigma_{AB}^2 \cdot \Omega} \right)}
\]

\( D_{AB} = 9.246 \) cm\(^2\) sec\(^{-1}\)

\( D_{AB} := 9.246 \frac{cm^2}{sec} \)

\( P := 0.34 \) atm

\( T := 1973 \) K

\( M_A := 18 \frac{gm}{mole} \)

\( M_B := 78 \frac{gm}{mole} \)

\( R := \frac{82.06 cm^3 \cdot atm}{mole \cdot K} \)

\( \rho := \frac{P \cdot M}{R \cdot T} \)

\( \rho = 3.78 \times 10^{-5} \frac{gm}{cm^3} \)

The Schmidt number can now be calculated:

\[
Sc := \frac{\eta}{\rho \cdot D_{AB}}
\]

\( Sc = 1.878 \)

The pressure and concentration of SiO(OH)\(_2\) are now needed: Nate's transpiration data for SiO(OH)\(_2\) are used in conjunction with the Allendorf \( C_p \) data.

\( P_{SiOOH2} := 1.77 \times 10^{-6} \) atm

The concentration of SiO(OH)\(_2\) is then:

\( M_B := 78 \frac{gm}{mole} \)

\( T := 1973 \) K
Now the flux of SiO(OH)$_2$ from a flat plate can be calculated:

\[
J = \frac{1}{0.664 \, R \cdot e_\perp^2 \cdot S_e^3 \cdot D_{AB} \cdot \rho_{SiOH2}} \]

\[
J = 2.289 \times 10^{-7} \frac{\text{gm}}{\text{cm}^2 \cdot \text{sec}}
\]

\[
J = 0.824 \frac{\text{mg}}{\text{cm}^2 \cdot \text{hr}}
\]

\[
J_{SiC} = J \cdot \frac{40}{3.21 \cdot 10^3 \cdot \frac{\text{mg}}{\text{cm}^3}}
\]

\[
J_{SiC} = 4.677 \times 10^{-7} \frac{7 \text{ mm}}{\text{sec}}
\]

\[
t := 1834 \text{ sec}
\]

\[
X_{SiC} = J_{SiC} \cdot t
\]

\[
X_{SiC} = 8.578 \times 10^{-4} \text{ mm}
\]

Calculate the interdiffusion coefficient for the water vapor and Si(OH)$_4$ gases.

The collision diameter, \( \sigma \), and collision integral, \( \Omega \), must be calculated first.

A useful reference for these values is NASA Technical Report R-132 by R.A. Svehla.

\( \sigma_A := 2.641 \) collision diameter for H$_2$O in angstroms

\( \sigma_B := 4.880 \) collision diameter for Si(OH)$_4$ in angstroms

use data for SiF$_4$ as best approximation

\[
\sigma_{AB} := \frac{\sigma_A + \sigma_B}{2}
\]

\( \sigma_{AB} = 3.76 \)

\( \varepsilon_A := 809.1 \text{ K} \)

This value is \( \varepsilon/\kappa \) for water vapor

\( \varepsilon_B := 171.9 \text{ K} \)

This value is \( \varepsilon/\kappa \) for SiF$_4$ as an approximation for Si(OH)$_4$

\[
\varepsilon_{AB} := \sqrt{\varepsilon_A \cdot \varepsilon_B}
\]

\( \varepsilon_{AB} = 372.94 \text{ K} \)
\[ T' := \frac{T}{\varepsilon_{AB}} \]
\[ T' = 5.29 \]

\( \Omega \) is then picked from a table on p. 20 of Mass Transfer by Sherwood et al. based on the value of \( T' \).
\[ \Omega := 0.8336 \]

The interdiffusion coefficient can now be calculated using the Chapman-Enskog Equation:
\[ M_A := 18 \]

The values are all entered without units here because the equation is formulated with the constant \( 0.0018583 \) and \( P(\text{atm}), T(\text{K}), \sigma(\text{angstroms}), M(\text{gm/mole}) \).
\[ M_B := 96 \]
\[ T := 1973 \]
\[ P := 0.34 \]

\[ D_{AB} := 0.0018583 \left( \frac{1}{M_A} + \frac{1}{M_B} \right) \frac{3}{T^2} \frac{1}{P \cdot \sigma_{AB}^2 \cdot \Omega} \]
\[ D_{AB} = 10.437 \]

\[ D_{AB} := 10.437 \text{ cm}^2 \text{ sec}^{-1} \]

The Schmidt number can now be calculated:
\[ Sc := \frac{\eta}{\rho \cdot D_{AB}} \]
\[ Sc = 1.664 \]

The pressure and concentration of \( \text{Si(OH)}_4 \) are now needed:
This information is based on Nate's paper with data input to FactSage.

Material temp of 1973K was used to calculate \( P_{\text{Si(OH)}_4} \)
\[ P_{\text{SiOH4}} := 1.4 \times 10^{-6} \text{ atm} \]

The concentration of \( \text{Si(OH)}_4 \) is then:
\[ M_B := 96 \text{ gm/mole} \]
\[ T := 1973 \text{ K} \]
\[ \rho_{\text{SiOH4}} := \frac{P_{\text{SiOH4}} M_B}{R \cdot T} \]
\[ \rho_{\text{SiOH4}} = 8.301 \times 10^{-10} \text{ gm/cm}^3 \]

Now the flux of \( \text{Si(OH)}_4 \) from a flat plate can be calculated:
\[ J := \frac{1}{2} \frac{1}{Sc} \frac{1}{3} D_{AB} \rho_{\text{SiOH4}} \]
\[ J := \frac{0.664 \text{ Re}}{\text{Sc}} \cdot \frac{\text{Sc}}{3} \cdot \frac{D_{AB}}{L} \rho_{\text{SiOH4}} \]
\[ J = 2.416 \times 10^{-7} \text{ gm} \text{ cm}^{-2} \text{ sec} \]

\[ J = 0.87 \frac{\text{mg}}{\text{cm}^2 \cdot \text{hr}} \]

\[ J_{\text{SiC}} := \frac{J}{3.21 \times 10^3 \frac{\text{mg}}{\text{cm}^3}} \cdot 40 \]

\[ J_{\text{SiC}} = 3.136 \times 10^{-7} \frac{\text{mm}}{\text{sec}} \]

\[ t := 1834 \text{ sec} \]

\[ X_{\text{SiC}} := J_{\text{SiC}} \cdot t \]

\[ X_{\text{SiC}} \text{ is the recession in time } t \]

\[ X_{\text{SiC}} = 5.752 \times 10^{-4} \text{ mm} \]
Appendix D.—Assumptions Made in Calculating Recession With Equation (1)

Several assumptions have been made in this calculation. First, the density of the gas boundary layer is calculated assuming it is entirely water vapor. This is a reasonable assumption since the combustion gases are composed of 60 percent water vapor.

Second, it is assumed that the gas boundary layer is laminar. This is also a reasonable assumption. The Reynolds number has been calculated for each condition (see Appendix C) and compared to \( \text{Re} = 3 \times 10^5 \), the criterion for transition from laminar to turbulent flow. In all cases, the Reynolds number is less than this quantity for most of the length of the panel. Surface roughness is expected to result in more turbulent flow. If the gas boundary layer is turbulent the major effect on the calculated recession is to increase the exponent on the Reynolds number from 0.5 to 0.7, thus an increased dependence on the gas velocity is expected. However, the overall recession is only expected to increase by a small factor, so trends indicated by the calculated recession based on laminar flow are expected to hold true.

Third, in the calculation of the interdiffusion coefficient of the volatile Si-O-H species in the gas boundary layer, assumptions have been made about the force constants: collision diameter and \( \frac{\varepsilon}{k} \) of the Si-O-H gas molecules. The force constants for SiO(g) are found in Svehla’s report (SVE62) and the collision integral is interpolated using the tabulated values in Hirschfelder (HIR54). The force constant data for SiF\(_4\)(g) from Svehla are used as an approximation for Si(OH)\(_4\)(g). This is expected to be a fairly good assumption since OH groups are often compared to halide groups. The average collision diameter and \( \frac{\varepsilon}{k} \) data of SiF\(_4\)(g) and SiO\(_2\)(g) from Svehla are used for SiO(OH)\(_2\)(g). This may not be a good assumption, however, it is known that gas phase diffusion coefficients do not vary much, so inaccuracies in the collision diameter and \( \frac{\varepsilon}{k} \) for SiO(OH)\(_2\)(g) are expected to have very little effect on the overall calculated recession rates.
Appendix E.—Estimation of Oxide Thickness on SiC

SAA P&W. SiC recession in cell 22

Estimate silica thickness for case 3 and case 4, where silica is assumed to be on the surface of the SiC.

First estimate parabolic oxidation rate, $k_p$ assuming:
Deal and Grove temperature dependence for transport of H$_2$O through silica, 68 kJ/mol

Using data from Opila, J.Am.Ceram.Soc. 82 [3] 625 (1999) - oxidation rate of SiC in water vapor at 1400 °C, PH$_2$O = 0.9 atm, $k_p = 3.5 \times 10^{-3}$ mg$^2$/cm$^4$ h

First convert $k_p$ to units of silica thickness growth rate:

$$ k_{1400} = 3.5 \times 10^{-3} \times 168 $$
this expression is in mg$^2$/cm$^4$ h

$$ k_{1400} = 0.588 $$
this expression is in $\mu^2$/h

solve for pre-exponential

$$ R := 8.31447; $$
in J/K mol

$$ T := 1673 $$
in degrees K

$$ k_{T_0} := \frac{k_{1400}}{\exp \left( \frac{-68000}{R \cdot T} \right)} $$

$$ k_{T_0} = 78.062 $$
now at 1700°C:

$$ T := 1973 $$

$$ k_{1700} := k_{T_0} \cdot \exp \left( \frac{-68000}{R \cdot T} \right) $$

$$ k_{1700} = 1.237 $$
this expression is in $\mu^2$/h

Now assume that $k_p$ varies with PH$_2$O to the exponent of 1 (molecular diffusion of H$_2$O in silica).
The value just determined was in 0.9 atm PH$_2$O

$$ k_{p_{0}} := \frac{k_{1700}}{0.9} $$

$$ k_{p_{0}} = 1.374 $$
this value is valid for $k_p$ at 1 atm PH$_2$O

Case 3, $P_{\text{total}} = 0.34$ atm
Case 4, $P_{\text{total}} = 2.10$ atm
at MR=6, PH$_2$O = 0.6*$P_{\text{total}}$

$$ \text{pH}_2\text{O}_3 := 0.6 \times 0.34 $$
$$ \text{pH}_2\text{O}_3 = 0.204 $$

$$ \text{pH}_2\text{O}_4 := 0.6 \times 2.10 $$
$$ \text{pH}_2\text{O}_4 = 1.26 $$

$$ k_{p_{3}} := k_{p_{0}} \cdot \text{pH}_2\text{O}_3 $$
$$ k_{p_{3}} = 0.28 $$
Now assume oxidation rates are one order of magnitude larger due to impurities in the combustion environment:

\[ kp_3 \text{real} := kp_3 \cdot 10 \]
\[ kp_4 \text{real} := kp_4 \cdot 10 \]

This expression is in \( \mu^2/h \)

These recession rates are due to \( \text{SiO}, \text{Si(OH)}_4 \) and \( \text{SiO(OH)}_2 \) formation. Units in microns/1834 sec. converted to microns/h. Converting from SiC recession to SiO\(_2\) recession (factor of 2).

\[ kl_3 := (9.46) \cdot 2 \cdot \frac{3600}{1834} \]
\[ kl_3 = 37.138 \]

\[ kl_4 := (119) \cdot 2 \cdot \frac{3600}{1834} \]
\[ kl_4 = 467.176 \]

Now the limiting oxide thickness for each case:

\[ x_L := \frac{kp_3 \text{real}}{2 kl_3} \]
\[ x_L = 0.038 \mu m \]

\[ x_L := \frac{kp_4 \text{real}}{2 kl_4} \]
\[ x_L = 0.019 \mu m \]

Now the time to reach steady state is calculated

\[ t_L := \frac{kp_3 \text{real}}{2 kl_3^2} \]
\[ t_L = 1.016 \times 10^{-3} \text{ sec} \]

\[ t_L := \frac{kp_4 \text{real}}{2 kl_4^2} \]
\[ t_L = 3.966 \times 10^{-5} \text{ sec} \]
Appendix F.—Calculated Gas Boundary Layer Thickness as a Function of Test Panel Length

<table>
<thead>
<tr>
<th>Distance along panel, cm</th>
<th>( \text{Re}_L ) Eq. (15)</th>
<th>( \delta ) from ( \text{Re}_L ), ( \mu m )</th>
<th>( \text{Re}_x ) Stout</th>
<th>( \delta ) from ( \text{Re}_x ), ( \mu m )</th>
</tr>
</thead>
<tbody>
<tr>
<td>0.167896</td>
<td>15279.35</td>
<td>19.61556</td>
<td>510361</td>
<td>3.418329</td>
</tr>
<tr>
<td>0.404908</td>
<td>35775.34</td>
<td>30.9155</td>
<td>507806</td>
<td>8.185199</td>
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Appendix G.—Calculation of Gas Velocity at Transition From Boundary Layer Limited Volatilization to Free Evaporation

Calculate the gas velocity and boundary layer thickness when a boundary layer limited flux is equal to the Langmuir flux

\[ J_L = P_{SiO} \left( \frac{M_{SiO}}{2\pi RT} \right)^{1/2} \]

All these terms are known for a given temperature and gas chemistry.

For the boundary layer flux expression, \( J_b \), all terms are known for a given temperature and gas chemistry to enable the velocity to be solved. Equate \( J_L \) and \( J_b \). \( P_{SiO} \) is found in both expressions and cancels.

Determine \( v \) and \( \delta \) for case 2: Bare SiC, leading edge of panel

\[
\rho := 2.335 \times 10^{-4} \text{ gm cm}^{-3}
\]
\[ P_{SiO} := 1.3 \times 10^{-1} \text{ atm} \]
\[ M_{SiO} := 44 \text{ gm mole} \]
\[ R := 82.06 \text{ cm}^{-3} \text{ atm mole K} \]
\[ T := 1973 \text{ K} \]
\[ L := 0.17 \text{ cm} \]
\[ D := 2.507 \text{ cm}^2 \text{ sec}^{-1} \]
\[ Sc := 1.121 \]
\[ \eta := 6.564 \times 10^{-4} \text{ gm cm sec}^{-1} \]

\[
v := \left( \frac{P_{SiO} \sqrt{M_{SiO}}}{2\pi \cdot R \cdot \rho \cdot T} \right)^2 \frac{L}{0.664 \sqrt{\frac{1}{\rho \cdot \eta} \cdot \frac{1}{Sc^3} \cdot \frac{P_{SiO} \cdot M_{SiO}}{D}}} \]
\]
\[ v = 9.483 \times 10^5 \text{ m s}^{-1} \]

gas velocity in cell 22 at leading edge is \( 2.5 \times 10^3 \text{ m/s} \)

\[ Re := \frac{\rho \cdot v \cdot L}{\eta} \]

What would the boundary layer thickness be for this velocity?

\[
\delta := \frac{1.5L}{Re^2 \cdot Sc^3} \]
\[ \delta = 1.025 \times 10^{-6} \text{ m} \]
For a boundary layer thickness of 1 micron, the Langmuir flux applies. This is independent of the pressure of the volatile species, and depends primarily on the boundary layer properties.
Appendix H.—Calculated Partial Pressures of Si-O-H Volatile Species as a Function of Panel Surface Temperature. Krikorian (KRI70) Data for SiO(OH)(g) (Not Recommended)

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Appendix I.—Photos of Borosilicate Glass Droplets on Panel 388 Tracked for Liquid Velocity Measurements. Flow is From Left to Right. The Horizontal Black Lines in the Images are Artifacts of the Software

Figure I1.—Drops A (left) and D (right), 8.903 sec.  
Figure I2.—Drop B, 9.307 sec.  
Figure I3.—Drop C, 8.500 sec.
**Title:** Integrated High Payoff Rocket Propulsion Technology (IHPRPT) SiC Recession Model

**Authors:** Opila, E., J.

**Abstract:**
SiC stability and recession rates were modeled in hydrogen/oxygen combustion environments for the Integrated High Payoff Rocket Propulsion Technology (IHPRPT) program. The IHPRPT program is a government and industry program to improve U.S. rocket propulsion systems. Within this program SiC-based ceramic matrix composites are being considered for transpiration cooled injector faceplates or rocket engine thrust chamber liners. Material testing under conditions representative of these environments was conducted at the NASA Glenn Research Center, Cell 22. For the study described herein, SiC degradation was modeled under these Cell 22 test conditions for comparison to actual test results: molar mixture ratio, MR (O₂:H₂) = 6, material temperatures to 1700 °C, combustion gas pressures between 0.34 and 2.10 atm, and gas velocities between 8,000 and 12,000 fps. Recession was calculated assuming rates were controlled by volatility of thermally grown silica limited by gas boundary layer transport. Assumptions for use of this model were explored, including the presence of silica on the SiC surface, laminar gas boundary layer limited volatility, and accuracy of thermochemical data for volatile Si-O-H species. Recession rates were calculated as a function of temperature. It was found that at 1700 °C, the highest temperature considered, the calculated recession rates were negligible, about 200 µm/h, relative to the expected lifetime of the material. Results compared favorably to testing observations. Other mechanisms contributing to SiC recession are briefly described including consumption of underlying carbon and pitting. A simple expression for liquid flow on the material surface was developed from a one-dimensional treatment of the Navier-Stokes Equation. This relationship is useful to determine under which conditions glassy coatings or thermally grown silica would flow on the material surface, removing protective layers by shear forces. The velocity of liquid flow was found to depend on the gas velocity, the viscosity of gas and liquid, as well as the thickness of the gas boundary layer and the liquid layer. Calculated flow rates of a borosilicate glass coating compared well to flow rates observed for this coating tested on a SiC panel in Cell 22.

**Subject Terms:**
SiC, Recession, Combustion

**Security Classification:**
SiC; Recession; Combustion

**Confidentiality:**
Unclassified-Unlimited

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