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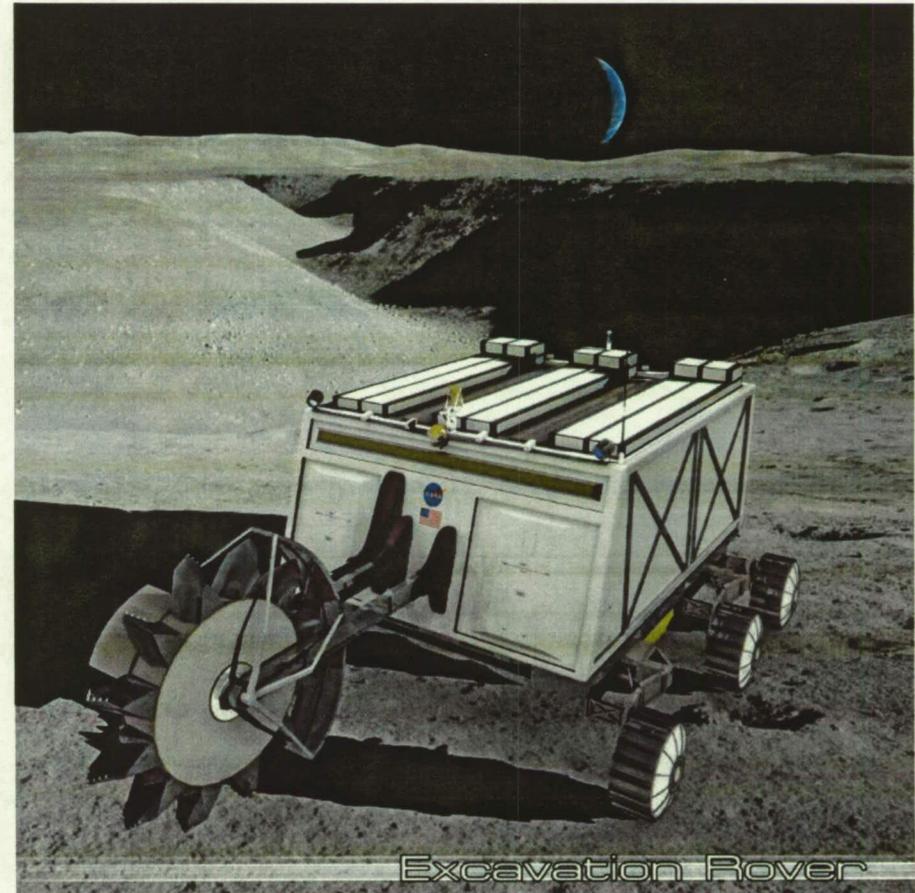


# Development of an Integrated RVC-LWRD System for RESOLVE



## ISRU Demonstration

- As exploration reaches new destinations, we have a greater need to live off the land
  
- ISRU plays a role in future mission architectures
  - Manufacture of propellants
  - Manufacture of life support consumables
  - Radiation shielding
  
- Since ISRU plays a key role, it would be extremely beneficial to demonstrate technology as early as possible





## NASA's Exploration Systems Architecture Study -- Final Report

### 4.2.1.2.4 Key Capabilities and Core Technologies

- Previous NASA architecture studies have included such destinations as the Moon, near-Earth asteroids, Mars, and the moons of Mars. A review of these previous studies illustrates the existence of a **common thread of key capabilities and core technologies** that are similar between destinations...
- • **ISRU**: Technologies for “living off the land” are needed to support a long-term strategy for human exploration. Key ISRU challenges include **resource identification and characterization**, excavation and extraction processes, **consumable maintenance and usage capabilities**, and advanced concepts for manufacturing other products from local resources;



# Brief RESOLVE Overview

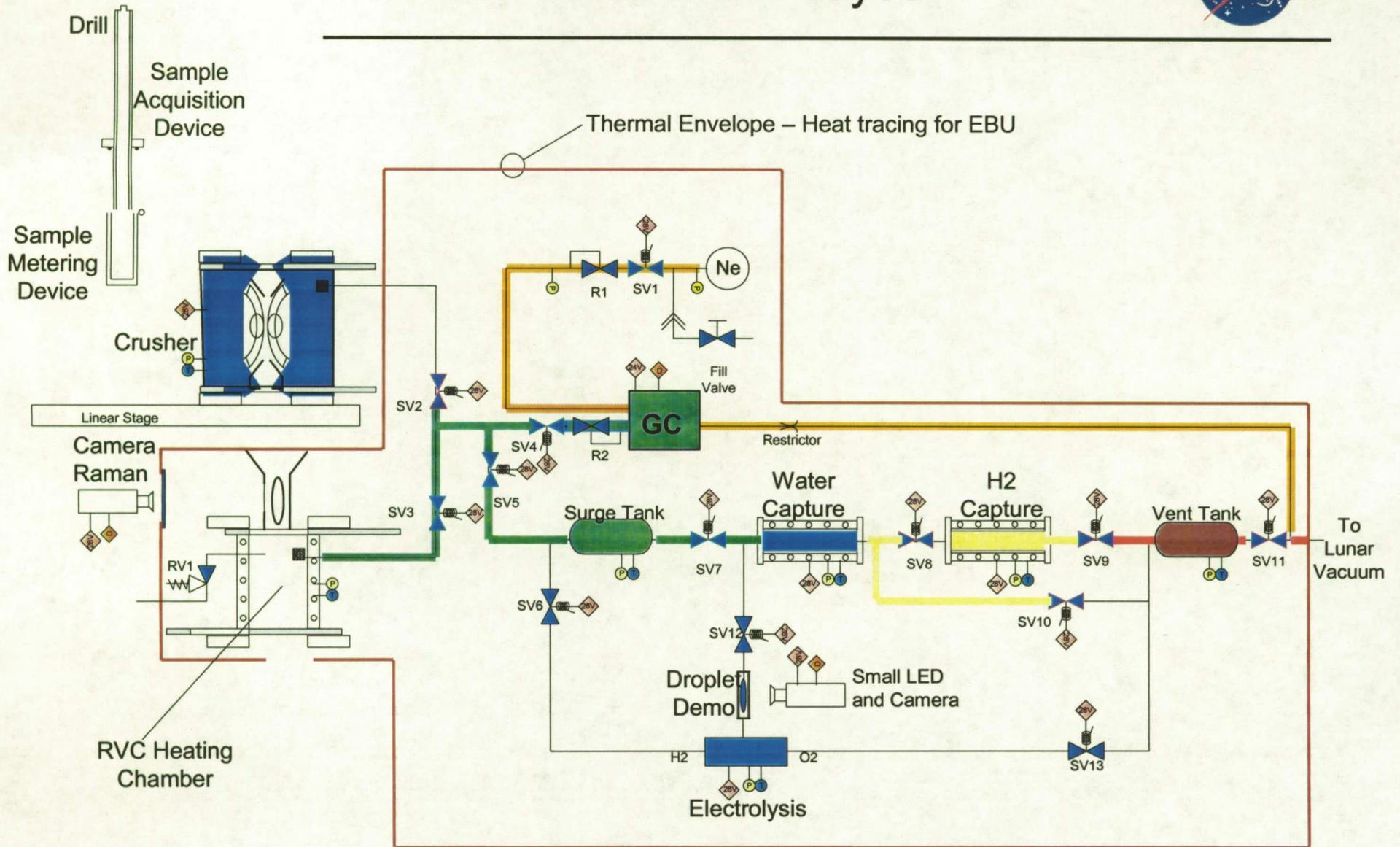


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- **RESOLVE - Regolith & Environment Science and Oxygen & Lunar Volatile Extraction**
  
- RESOLVE incorporates 5 modules
  - EBRC (Excavation and Bulk Regolith Characterization)
  - ERPC (Environment and Regolith Physical Characterization)
  - ROE (Regolith Oxygen Extraction)
  - RVC (Regolith Volatile Characterization)
  - LWRD (Lunar Water Resource Demonstration)
  
- Goal – identify and quantify volatiles, demonstrate ISRU, engage the public interest in ‘living off the land’ technology

# RESOLVE Layout





- Evaluation of system flow
  - Loop flow
    - ☞ Increase capture efficiency, but also increase time required to run the system
  - Straight flow
    - ☞ Loss of some efficiency but decrease operational time
  - Timing of solenoid valves
    - ☞ Length of time open
    - ☞ Time between openings

# Model of system



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- Model of gas moving through system to provide insight into overall operation of system
- Pressures equalize with each valve opening (assume ideal gas) and calculating resulting pressure if/when adsorption occurs

**HOW TO READ THE TABLE**

Description	LWRD Component					Mass of H2O/H2 absorbed
	Oven	Surge Tank	H2O bed	H2 Bed	Vent Tank	
Species Adsorbed (grams)			0.053566479	0.025156		→
Initial Pressure (atm)	3.413663					} <b>Initial values</b>
H2O (moles)	0.003375					
H2 (moles)	0.013403					
CO (moles)	0.000688					
N2 (moles)	9.64E-05					
SO2 (moles)	0.00158					
Total (moles)	0.000527					
Initial Pressure (atm)	2.275775	2.275775161				} <b>Values after the vessels reach equilibrium</b>
H2O (moles)	0.00225	0.001124888				
H2 (moles)	0.001053	0.004467809				
CO (moles)	0.000351	0.000229199				
N2 (moles)	0.013113	3.21453E-05				
SO2 (moles)	0.000351	0.000175728				
Total (moles)	0.013113	0.00655628				
Initial Pressure (atm)		1.831256511	1.831256511			} <b>Values after the vessels reach equilibrium</b>
H2O (moles)		0.000905168	0.00021972			
H2 (moles)		0.003595129	0.00087268			
CO (moles)		0.00043	4.47685E-05			
N2 (moles)		0.0005	6.27881E-06			
H2S (moles)		0.00042367	0.000102841			
SO2 (moles)		0.000141404	3.43243E-05			
Total (moles)		0.005275666	0.001280614			
Initial Pressure (atm)		0.714942477	0.714942			} <b>Values after the vessels reach equilibrium</b>
H2O (moles)		1.01446E-05	1.18E-05			
H2 (moles)		0.000402922	0.00047			
CO (moles)		2.06699E-05	2.41E-05			
N2 (moles)		0.000006	3.38E-06			
H2S (moles)		0.000005	5.54E-05			



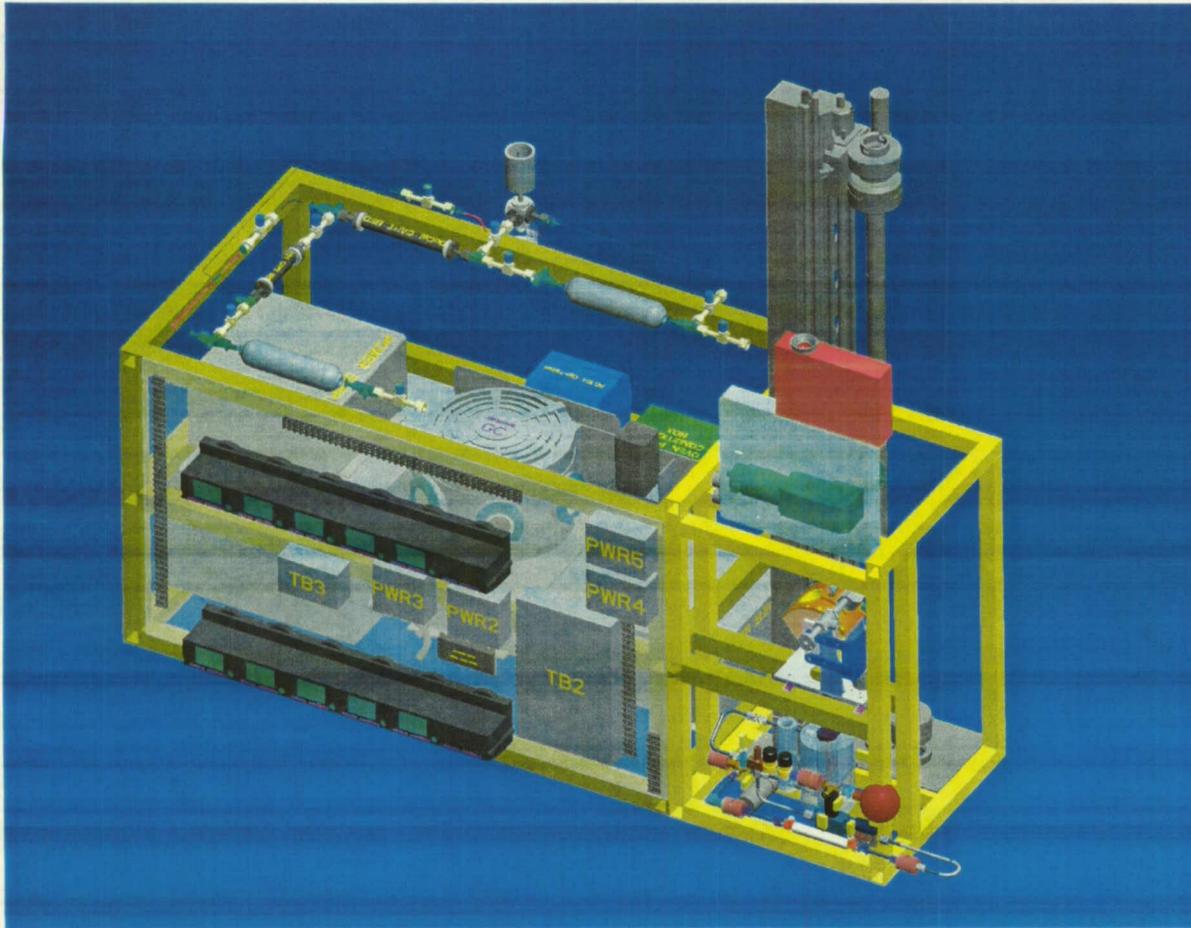
# User Interface – Inputs

Input Parameter Field				
Parameter	Name	Value	Units	Description
<b>Options for Simulation</b>	Simulation Mode	Multiple Loops		
	Minimum H2O adsorbed	0.05	grams	If H2O adsorbed is not a constrain, this number should be large (i.e. 1e10)
	Minimum H2 adsorbed	1.00E+10	grams	If H2 adsorbed is not a constrain, this number should be large (i.e. 1e10)
<b>Oven</b>	Volume	200	cm <sup>3</sup>	Volume of vessel
	Temperature	423	K	Temperature of vessel
	Minimum Pressure	5	torr	Minimum pressure change to re-pressurize the vessel
<b>Surge Tank</b>	Volume	100	cm <sup>3</sup>	Volume of vessel
	Temperature	423	K	Temperature of vessel
	Minimum Pressure	5	torr	Minimum pressure change to re-pressurize the vessel
<b>Dessicant Bed</b>	Volume	20	cm <sup>3</sup>	Volume of vessel
	Temperature	298	K	Temperature of vessel
	Minimum Pressure	5	torr	Minimum pressure change to re-pressurize the vessel
	Mass of absorbant	5	gram	Mass of water absorbant
<b>Hydride Bed</b>	Volume	20	cm <sup>3</sup>	Volume of vessel
	Temperature	298	K	Temperature of vessel
	Minimum Pressure	5	torr	Minimum pressure change to re-pressurize the vessel
	Mass of absorbant	0.5	gram	Mass of metal hydride
<b>Vent Tank</b>	Volume	200	cm <sup>3</sup>	Volume of vessel
	Temperature	298	K	Temperature of vessel
	Minimum Pressure	5	torr	Minimum pressure change to re-pressurize the vessel
	H <sub>2</sub> O	900	µg/g-regolith	

Run

Clear

# Model of RESOLVE System



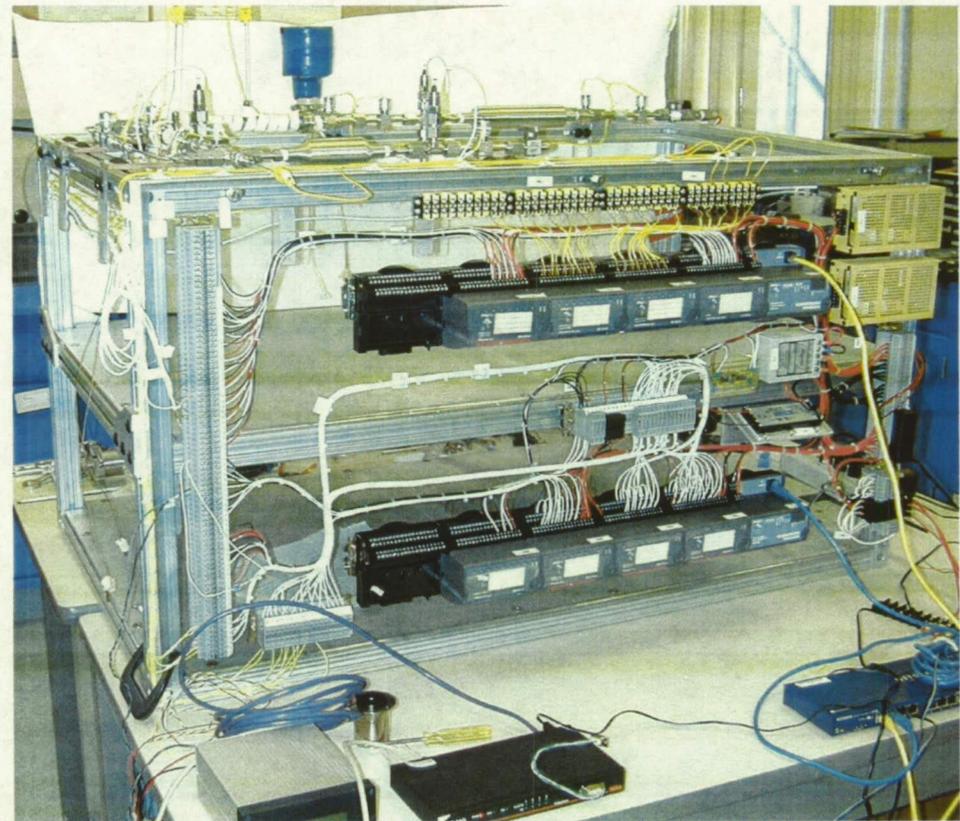
Pro-E drawings done by  
Victor Spencer - JSC

# Engineering Breadboard Unit (EBU)



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- Hardware is being assembled
  - GRC – vibrofluidization oven
  - KSC – GC and LWRD
  - NORCAT – drill, crusher
  - JSC – ROE
  - JPL – CHAMP RAMAN
  
- First cut at an integrated system, finding the kinks
  
- RVC-LWRD will be integrated and tested at KSC
  
- Integration will be at JSC in March-April timeframe

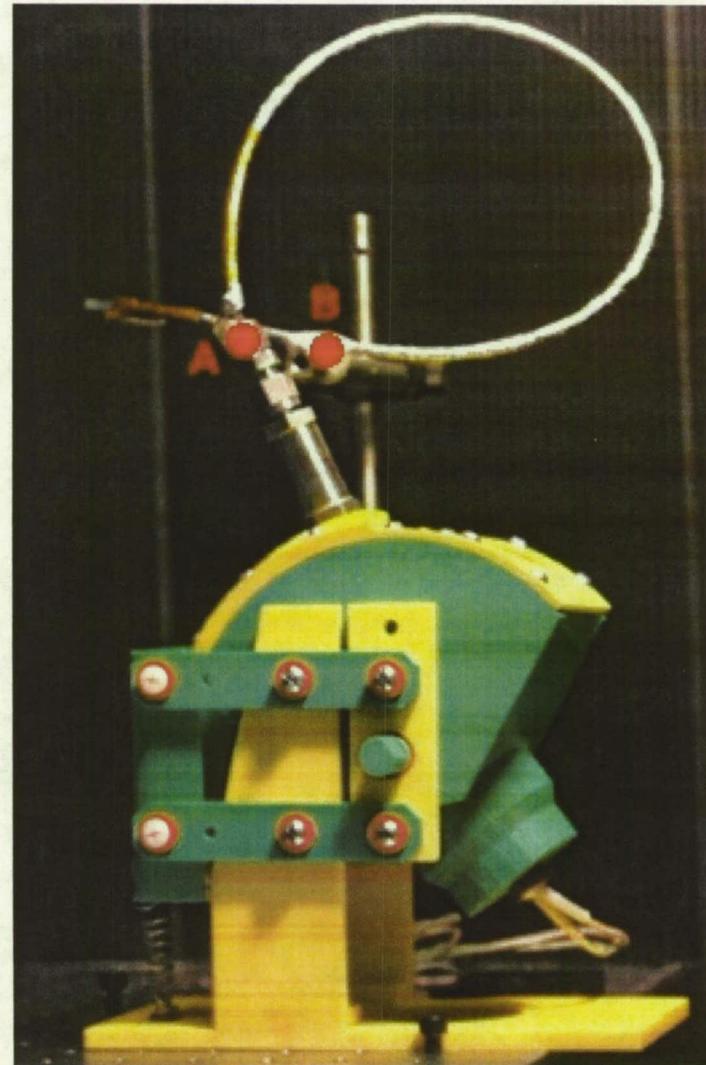




- The window for the RAMAN-CHAMP camera needs to be cleaned between samples to reduce contamination between the samples
  
- KSC's electrostatics group (led by Dr. Carlos Calle) has been developing dust removal techniques
  
- Transparent electrodes made of ITO (Indium Tin Oxide) will be placed on a sapphire window substrate, a voltage will be applied to clean the dust from the window surface
  
- Technology will be evaluated with real lunar soil



- Crushed regolith will be delivered through RAMAN viewing chamber into vibrofluidization oven
  
- Oven designed to evenly heat sample,
  - This is important for correlating the volatiles released with the temperature of the regolith
  - The temperature at which the volatiles are released will provide insight into the nature of their bonding
  
- GRC has done extensive testing on optimizing vibrofluidization parameters



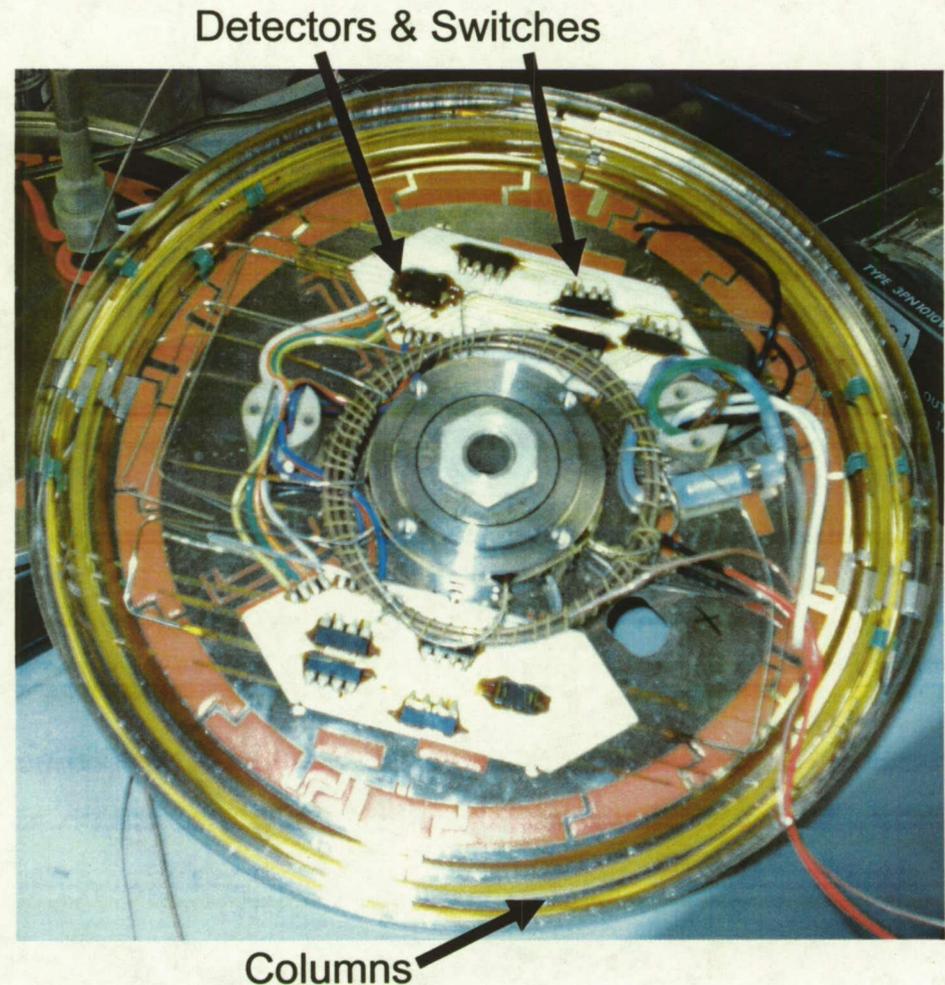
# RVC Gas Chromatograph



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- COTS Siemens GC MicroSAM, converted to Neon carrier gas
- Modified in house to optimize separation and detection of  $H_2$ , He,  $H_2O$ ,  $O_2$ , CO,  $CO_2$ ,  $CH_4$ ,  $H_2S$
- Water detection was challenging but modifications and heat tracing have allowed for quantitative analysis of concentrations from 1% to 20% of vapor phase composition (current limitation of generation system)
- Water limit of detection corresponds to approximately 0.05 wt % in regolith
- Current testing
  - Optimization of flow
  - Column temperatures

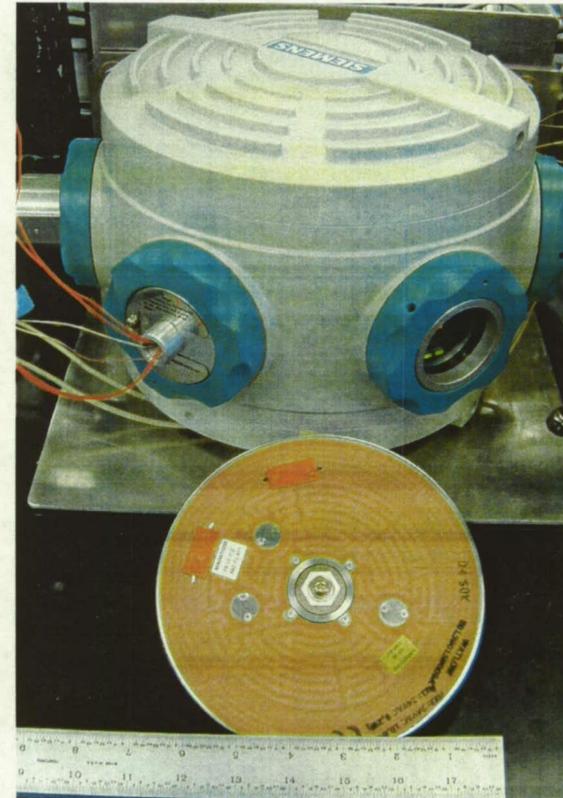
## Analysis Module of GC



# RVC-GC



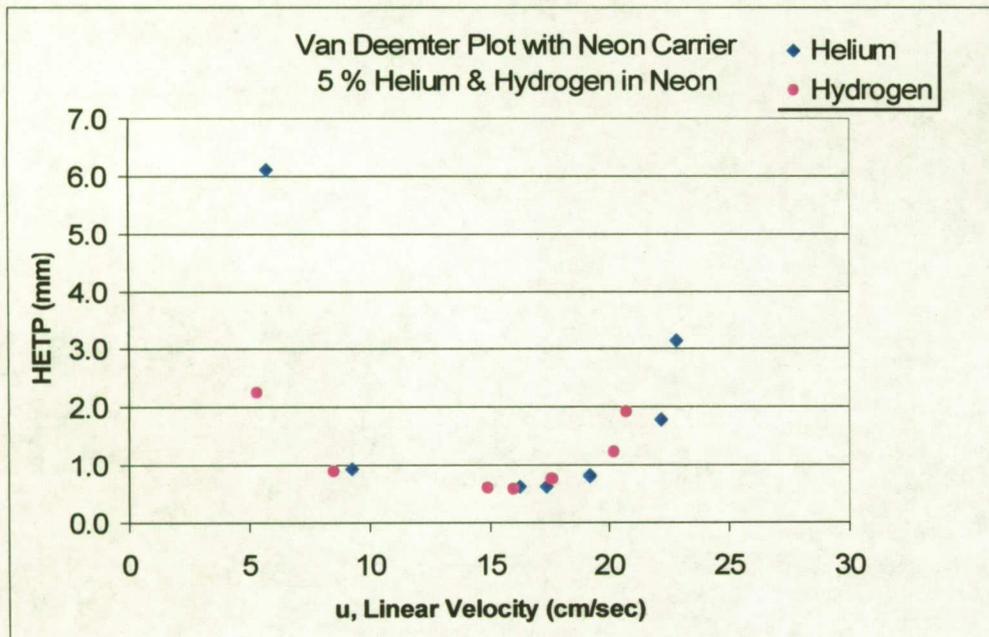
- Van Deemter plot generated to optimize pressure driven flows for best separation of components
  - The lower the HETP value, the better the separation on the column (height equivalent of a theoretical plate)



GC with explosion proof case

Analysis module

- MicroSAM GC (top) in factory designed case will be stripped and the analysis module (bottom) will be isolated for use in FPU

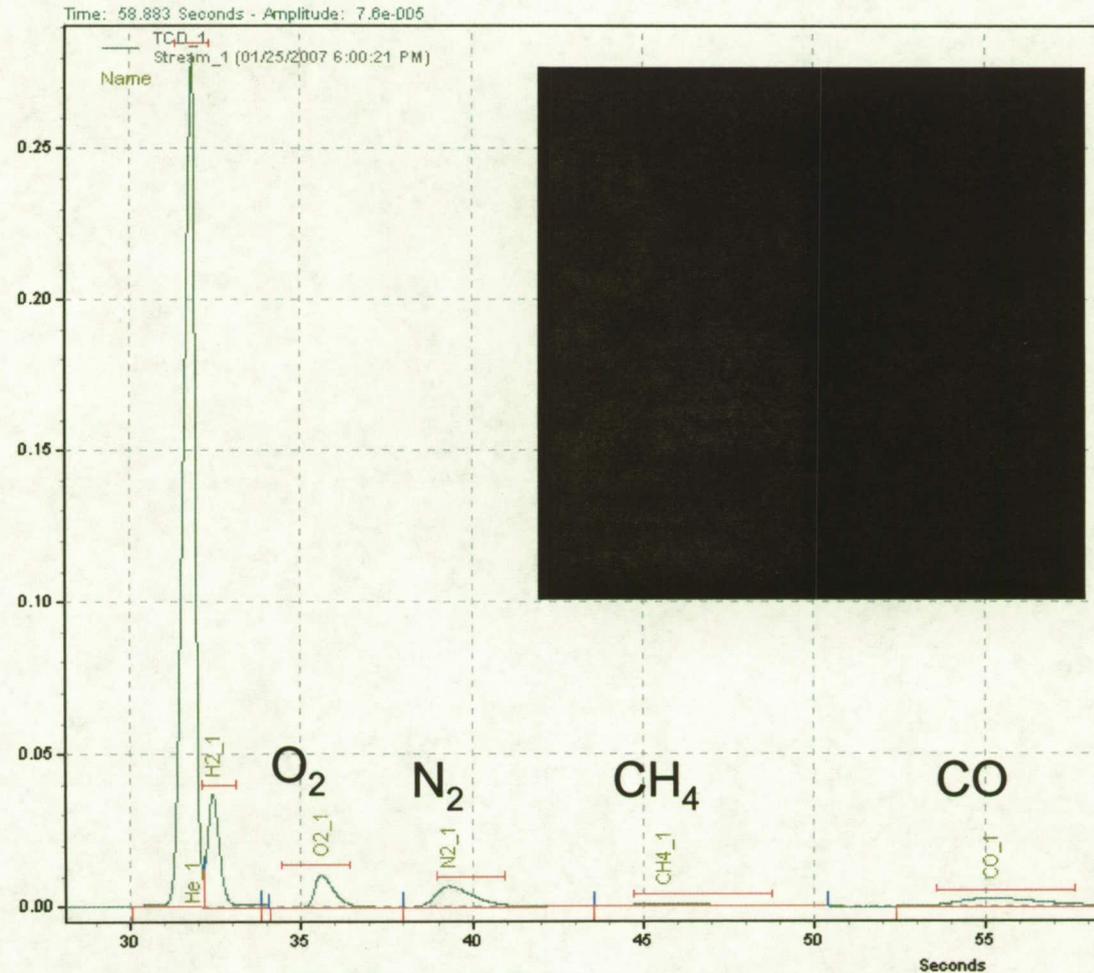
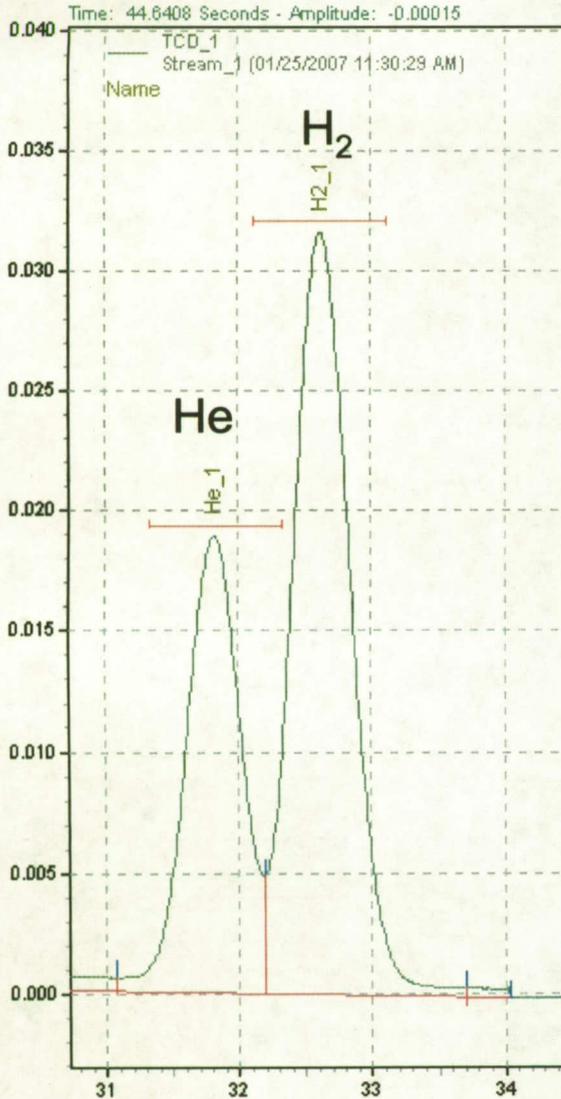




# Sample Chromatograms

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## ■ Sample containing He, H<sub>2</sub>, O<sub>2</sub>, N<sub>2</sub>, CH<sub>4</sub>, CO, H<sub>2</sub>O (inset)

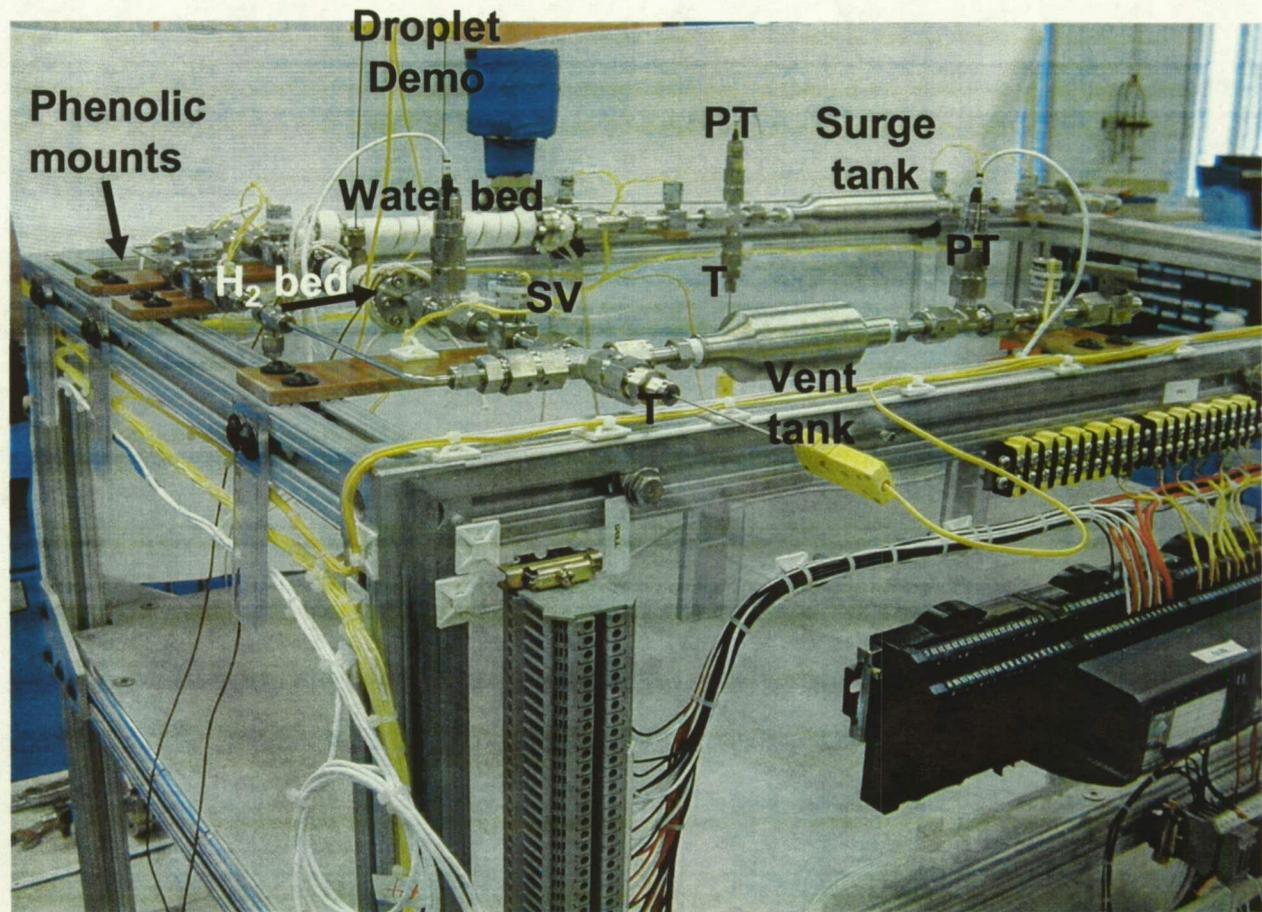


He/H<sub>2</sub> separation (5% each in Ne)



## EBU Hardware

- EBU configuration laid out to allow for easy access to system
  - Wire tracing
  - Leak checks
  - Heat tracing
    - Calculations to estimate power and chose best gauge of wire have been done
- Insulation
  - Polyimide foam
  - Durablanket (ceramic fiber) high temp insulation

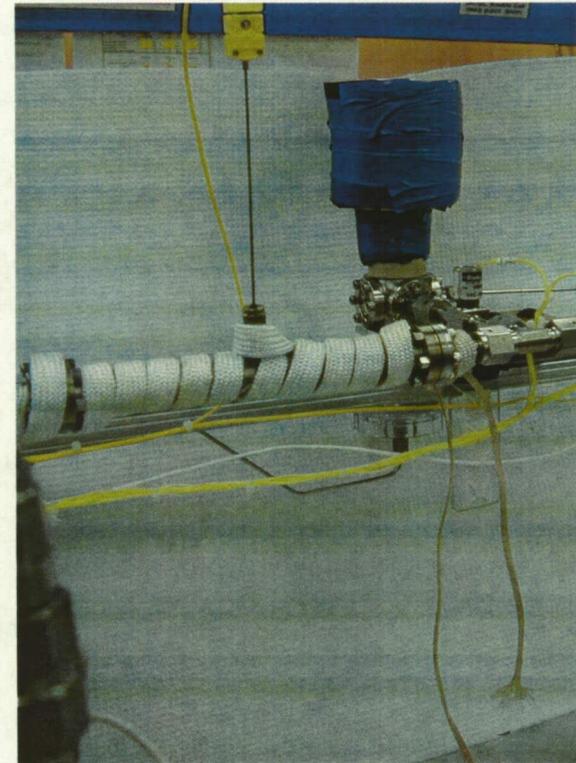


# Heat Tracing Challenges



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- Goal – prevent condensation of water in system while capturing volatiles
- Cold spots in system would allow for condensation which would skew GC analysis of volatiles
- Thermal imaging camera will be used to analyze heat tracing
  
- Challenge – solenoid valves (normally closed)
  - maximum operating temp of ~100degC observed when continuously operated, only two must be continuously operated
  - In an insulated system they would overheat, however they need to be heat traced to prevent condensation
  - For FPU latching solenoid valves are preferred to avoid this problem



High temperature heat tape on water capture bed



## Water Vapor generation

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- Currently Miller Nelson or in house vapor generation system used
- First cut evaluation will be done with mixed gases and injected water with no simulant
  - Preliminary tests with water and simulant indicate clumping will be a problem for vibrofluidization oven
- Goal will be to dope simulant with hydrated salts that release water vapor for analysis at elevated temperatures
- current oven design is limited to 150°C, this puts an upper bounds on the amount of water vapor we'd see in the system (VP of water at 150°C is ~70 psi)

Desorption  
temps of  
selected  
hydrated  
salts from  
STA runs



- Several options explored
  - LN<sub>2</sub> cold trap
    - + efficiently captures water
    - not selective, will condense other volatiles (contamination for electrolysis)
  - Molecular sieves
    - + reversible water capture
    - capture based on size, not selective
  - Hydrated salts
    - + selective adsorption
    - slower than LN<sub>2</sub> trap

Picture of LN<sub>2</sub>,  
molecular  
sieves and  
hydrated salts

Integration with ROE – current  
system will need to capture  
~1g of water

# Hydrogen Capture

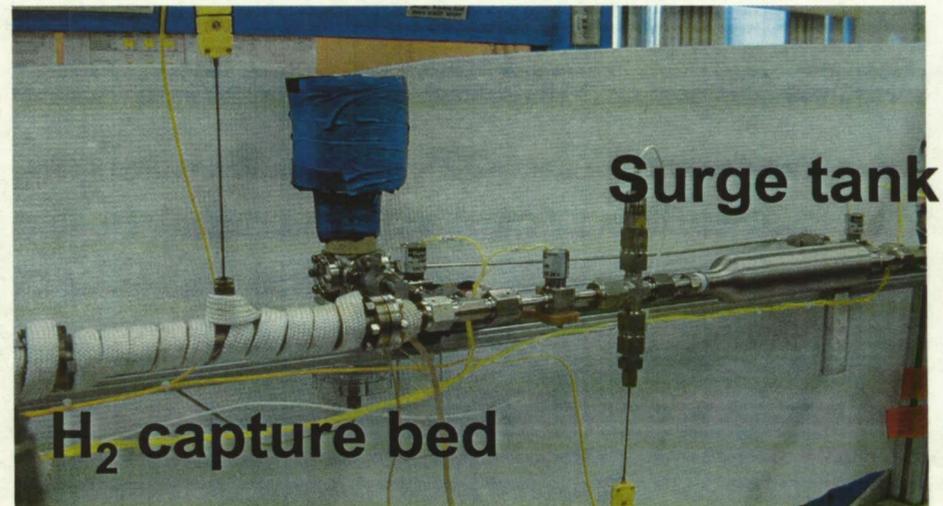
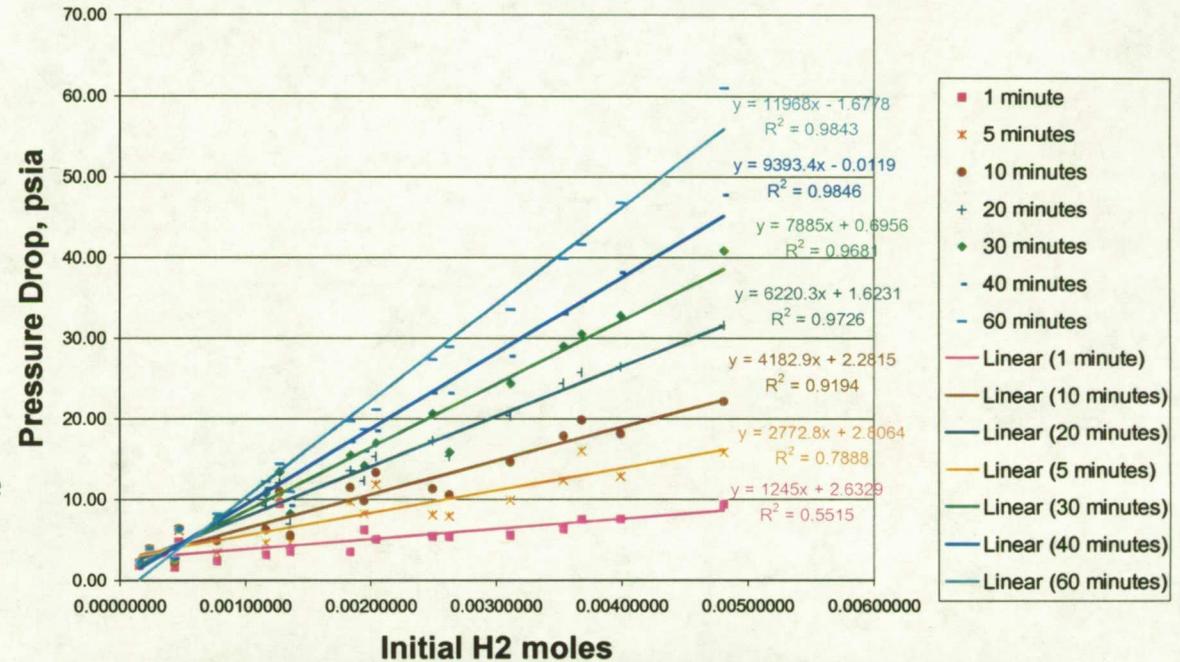


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Pressure Drop vs. Initial H2 moles

## ■ Metal hydrides explored

- ZrNi most stable of evaluated hydrides in air, least susceptible to contamination
- Equilibrium vapor pressure vs desorption temperature trade off explored for ZrNi
- Kinetics of ZrNi outweigh the slightly higher equilibrium vapor pressure at elevated temperatures, adsorption performed  $\sim 160^{\circ}\text{C}$

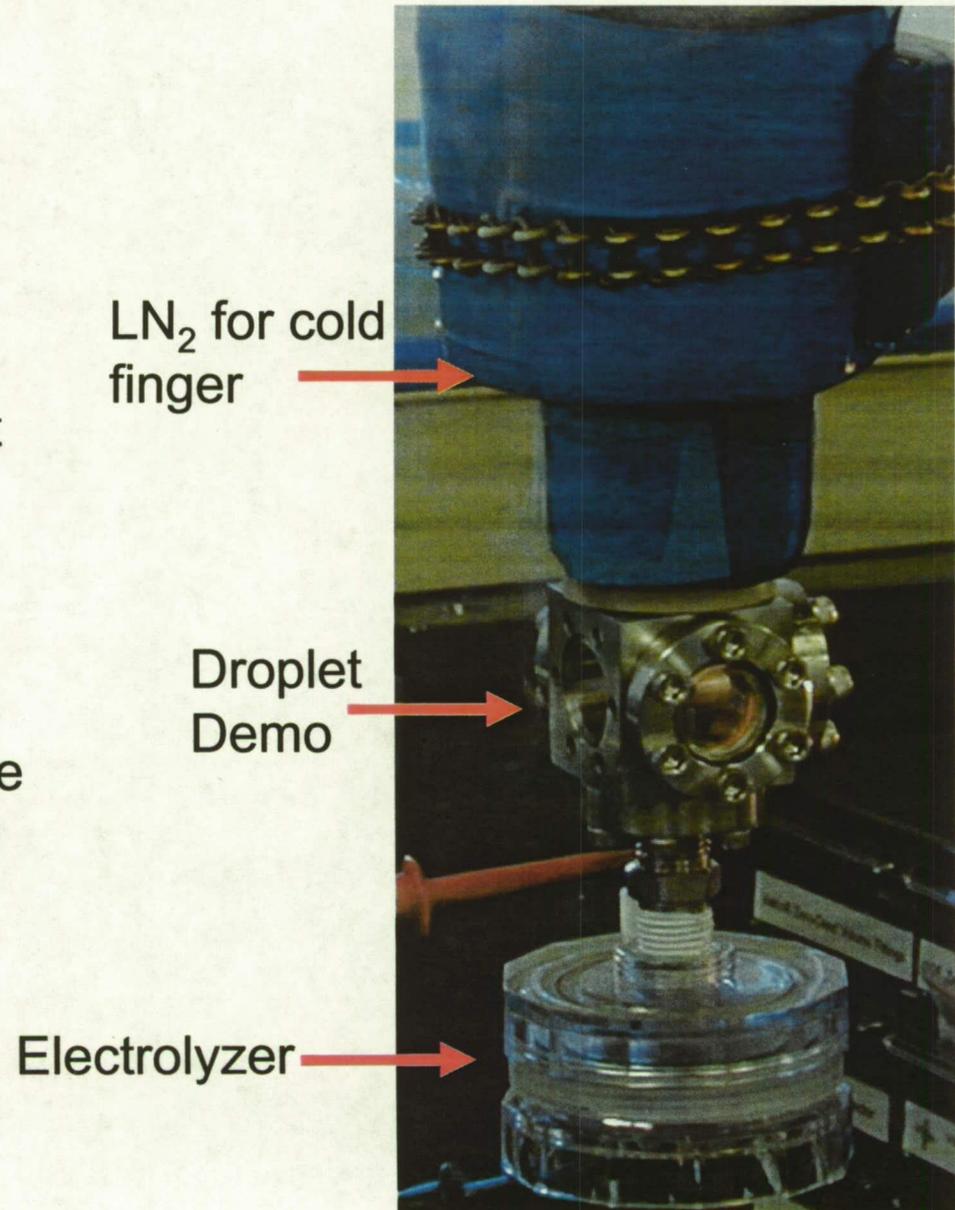


# Water Droplet Demo and Electrolysis



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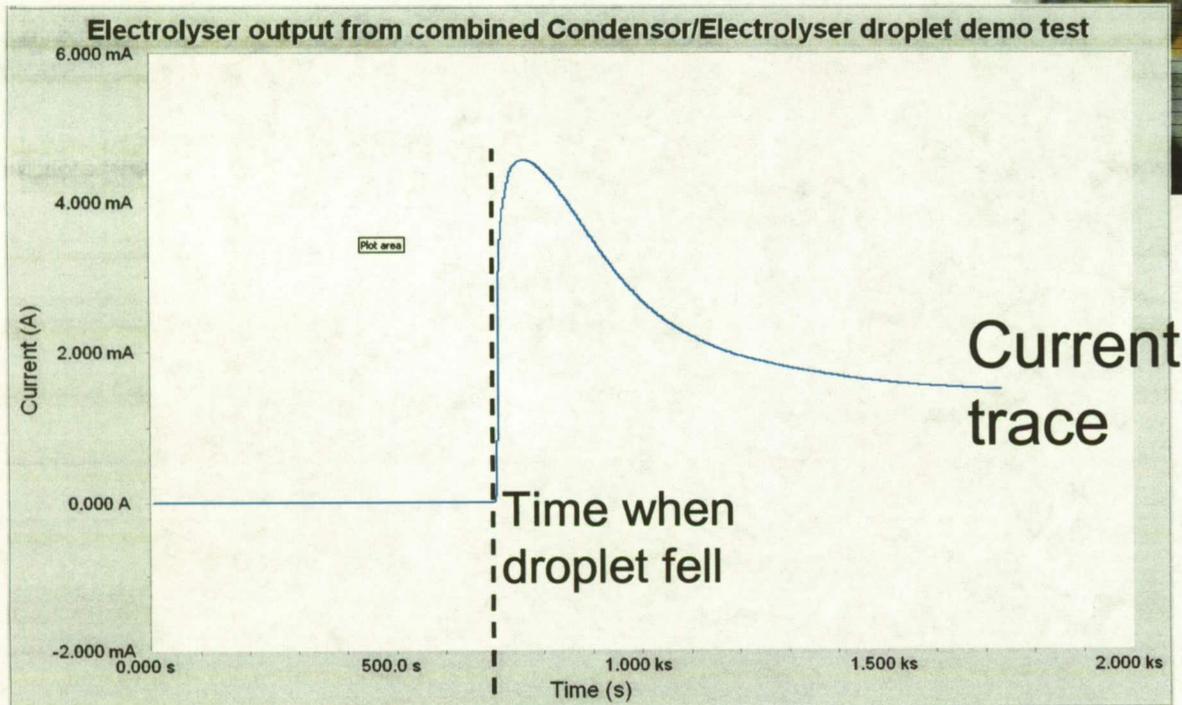
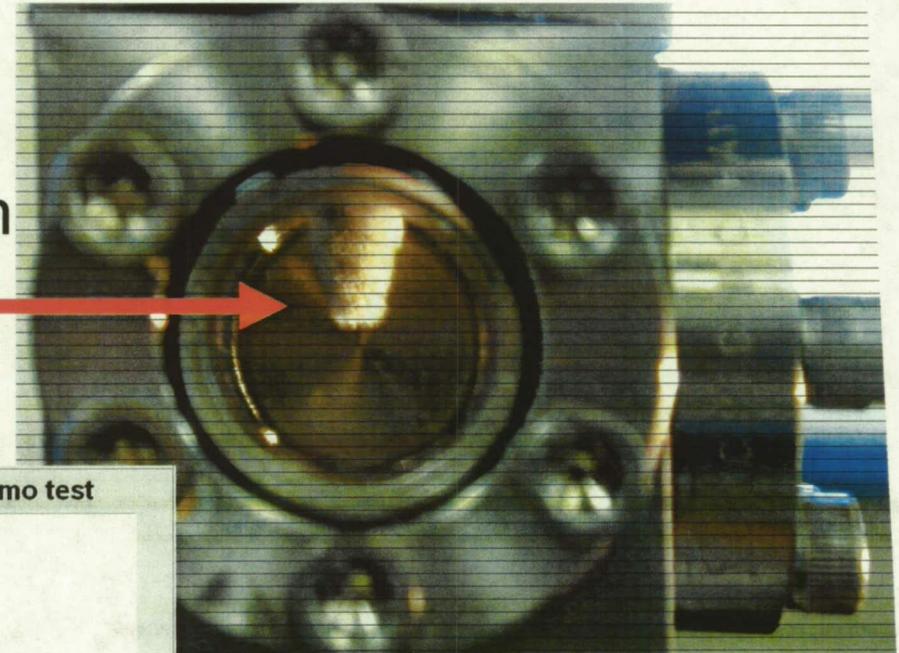
- Currently LN<sub>2</sub> used to cool cold finger for water condensation
- Droplet demo tested, when the cold finger is warmed a droplet will form on the tip of the condenser and fall into the electrolyzer
- Electrolyzer records an increase in current corresponding to the time the droplet fell





# Water Droplet - Electrolyzer

Ice formation on  
cold finger in  
droplet demo





## Electrolyzer

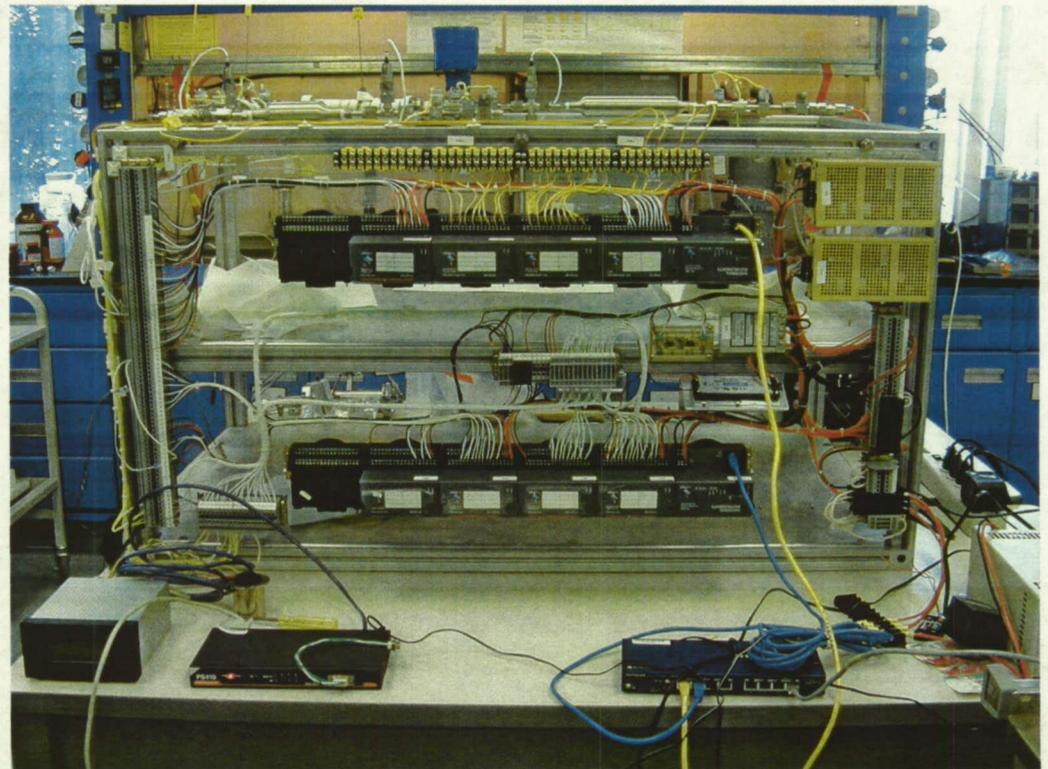
- Trade off between designing for a drop vs 1g of water

Pictures of initial electrolyzer designs and testing with 40uL in dry cell

# Computer Control



- Documentation has been placed into Microstation (CAD)
- Manual interface is operational and supporting initial testing and data recording
- Process of integrating shaker control software into our system control software
  
- Next steps
  - Working on heater control loops
  - To integrate system into rover we will need to go to compact fieldpoint (\$) or Xiphos (\$\$\$)
  - Flow charts for automated processes are being constructed



# Manual Control Interface



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ResolveHMI\_Manual.vi

File Edit View Project Operate Tools Window Help

**Data Logging**

ON OFF

Data Log Interval: 10

Logging Indicator Light

**Test Name**  
test not named

**Current Time**  
2/7/2007 1:25:09 PM

**Elapsed Time**  
0 00:06:19

**Boost**  
OFF

Boost may be hidden upon completion of debug.

The diagram illustrates a complex industrial process flow. It starts with a 'From Crusher' input leading to a series of valves (SV2, SV3, SV4, SV5). The flow then passes through a 'GC' (Gas Chromatograph) unit, which is connected to a 'Ne' (Neon) gas source and a 'GC' control panel. The main process line includes an 'Oven' with multiple temperature sensors (T11-T16) and a 'Surge Tank' with a pressure sensor (P3) and temperature sensor (T1). This is followed by two 'H2O\_Bed' and 'H2\_Bed' units, each with their own temperature sensors (T2, T3) and pressure sensors (P4, P5). The flow then goes through an 'Electrolyzer' unit with various sensors (E1, T5, P7, V1) and a 'Vent Tank' with a pressure sensor (P6) and temperature sensor (T4). The final output is directed 'To Lunar Vacuum' through valve SV11. Numerous other valves (SV1-SV13) and sensors (P1, P2, P7, T12-T14) are distributed throughout the system.

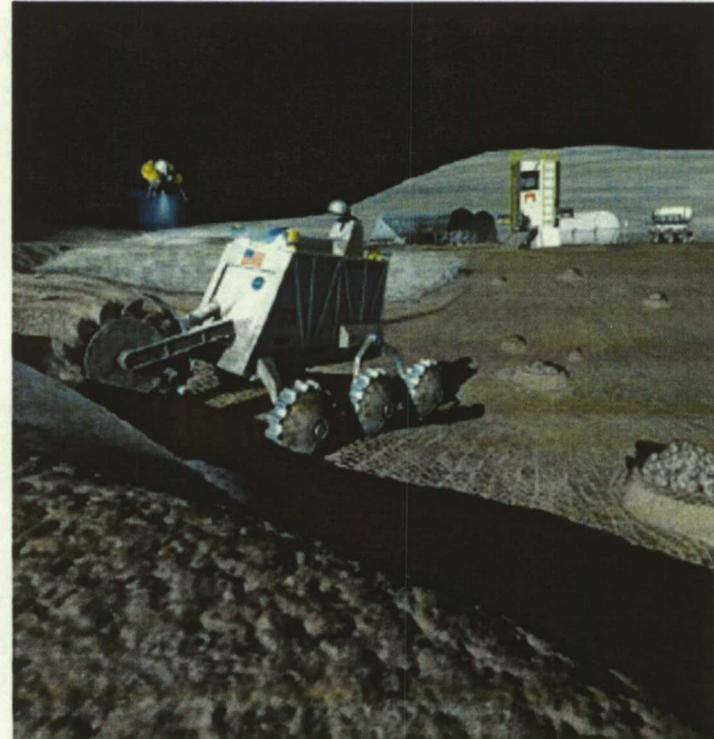
**Comments**

Submit Comment

## Conclusion

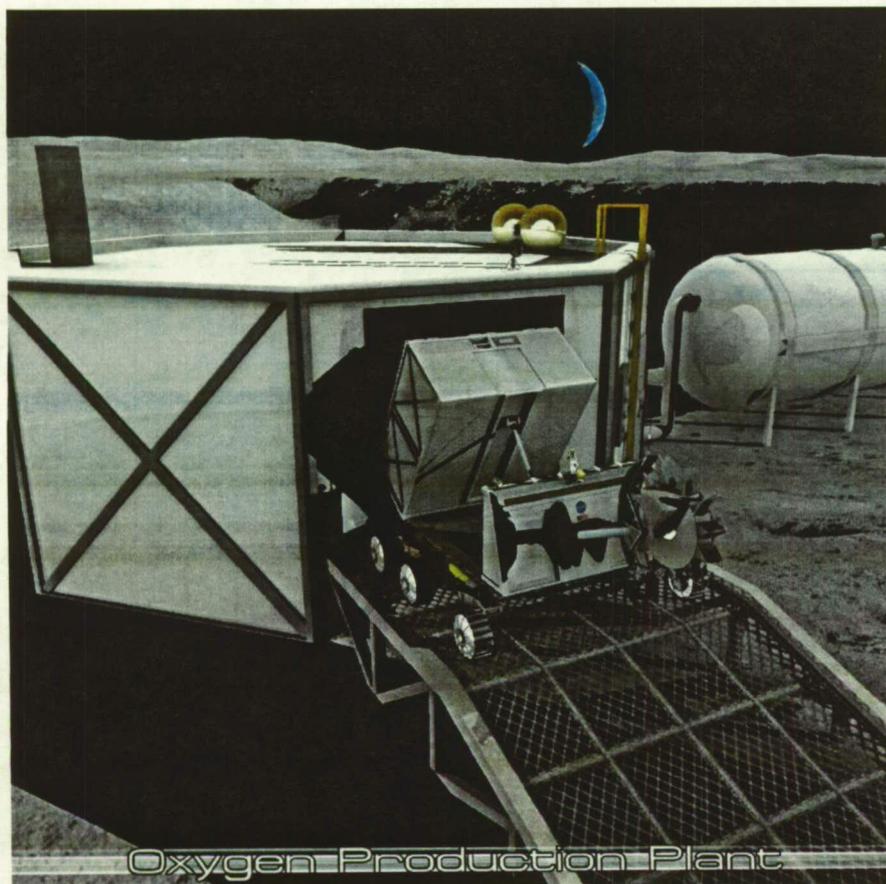


- EBU integration currently in progress
- Future goals and changes required for FPU identified
- Current RESOLVE goals of volatile characterization and demonstration of ISRU will be met with the EBU and optimized for FPU

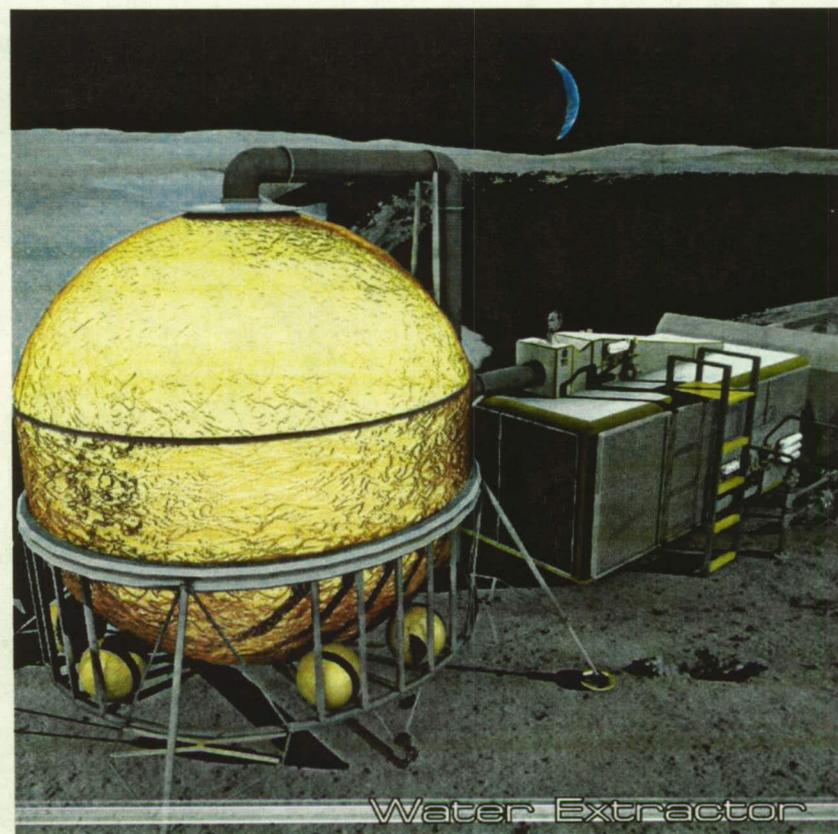




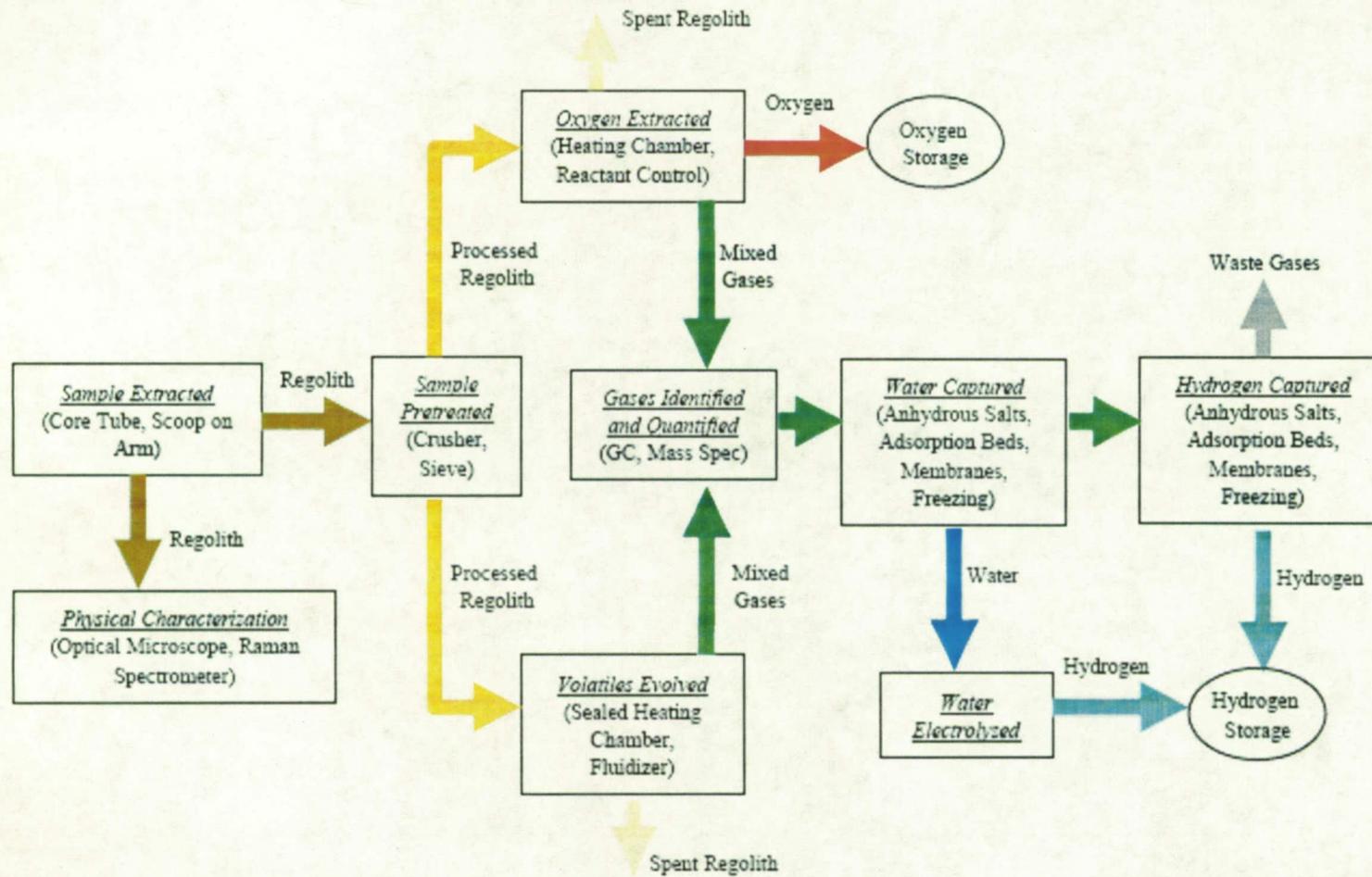
- **Key Functional Requirements and GR&As** The following key functional requirements and GR&As were used for the study, with emphasis placed on ensuring that the architecture approach was consistent with the Cycle 3 ESAS architecture and mission assumptions.
- ISRU: Capable of utilizing locally produced propellants.
  
- This initial strategy corresponds to the “pointer” location shown in **Figure 4-54** (which appears later in the report in **Section 4.3.5, Lunar Surface Traffic Model**), and serves as a starting point for the analysis of outpost deployment strategies. A number of key a
  - Precursor missions have accomplished the following tasks:
    - • Demonstrated ISRU technologies such as O<sub>2</sub> production, H<sub>2</sub>/H<sub>2</sub>O extraction, and excavation of regolith; and
    - • Developed an enhanced lunar gravity potential model.

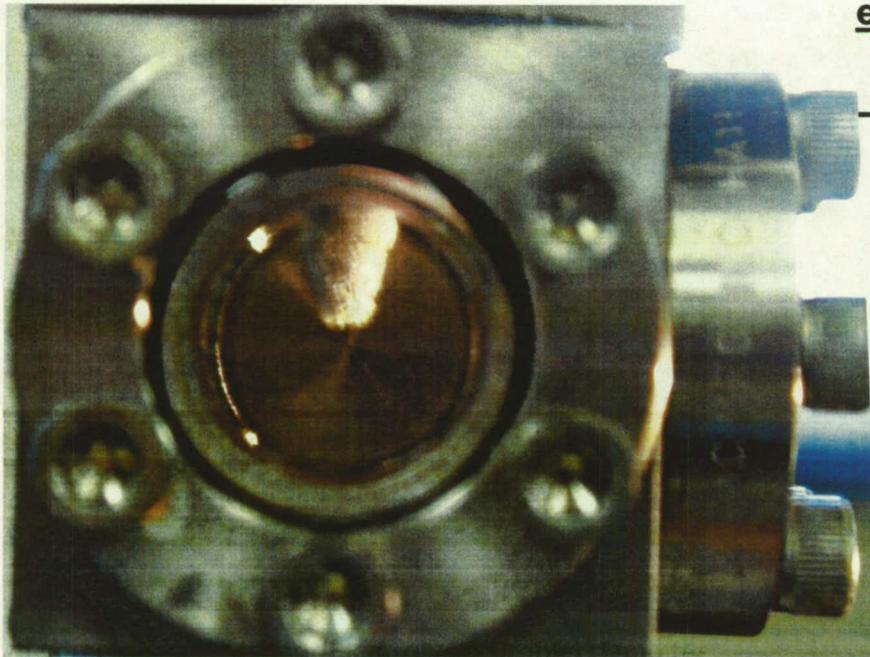


Oxygen Production Plant

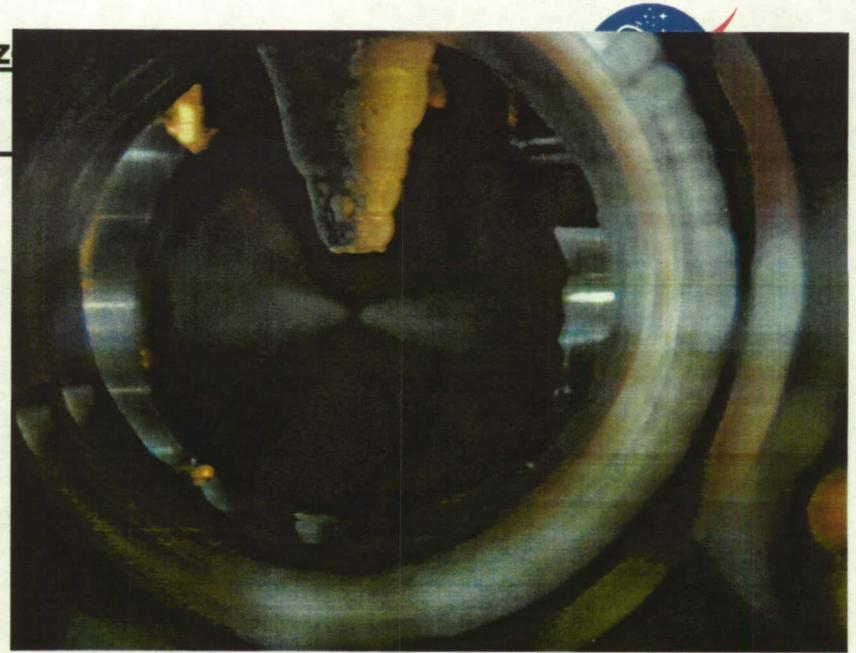


Water Extractor





electrolyz



Electrolyser output from combined Condensor/Electrolyser droplet demo tes

